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1 *Physical Modeling of Coupled Heat Transfer and Water Flow in Soil-Borehole Thermal*
2 *Energy Storage Systems in the Vadose Zone*

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9 **ABSTRACT**

10 This paper focuses on characterization of the heat transfer and water flow processes in
11 physical models of borehole heat exchanger arrays in unsaturated soil layers. The overall goal is
12 to develop a dataset that can be used to validate coupled thermo-hydraulic flow models needed to
13 simulate the efficiency of heat transfer in soil-borehole thermal energy storage (SBTES) systems.
14 Two bench-scale physical models that consist of a triangular array of vertical heat exchangers
15 within a layer of unsaturated silt were constructed in insulated cylindrical tanks to evaluate the
16 impact of different boundary conditions on the heat transfer and water flow processes in the silt
17 during heat injection into the array. In one model, the heat exchangers were placed at a radial
18 location that is 26% of the tank radius, while in the other model the heat exchangers were placed
19 on the inside of the tank wall. During circulation of heated fluid through the heat exchangers, the
20 changes in soil temperature and volumetric water content along the centerline of the array at
21 different depths were measured using dielectric sensors. The thermal conductivity and specific
22 heat capacity of the silt were also monitored using a thermal probe at the center of the silt layer
23 at mid-height. Permanent drying was observed for the soil within the array with the smaller

2

24 spacing, while an increase in water content was observed in the array with a spacing equal to the
25 container diameter. An increase in thermal conductivity of the soil was observed within the array
26 in the case of larger spacing, while the opposite was observed in the case of the smaller spacing.
27 The results indicate the possible formation of a convective cell within the larger array as water is
28 driven inwards from the heat exchangers. They indicate the importance of couple heat transfer
29 and water flow in SBTES systems in the vadose zone.

30 **Keywords:** Borehole thermal energy storage, Coupled heat transfer and water flow, Laboratory
31 physical modeling, Unsaturated soil

32 INTRODUCTION

33 Soil-borehole thermal energy storage (SBTES) systems are an approach to provide efficient
34 renewable resource-based thermal energy to heat buildings (Gabrielsson et al. 2000; Sibbitt et al.
35 2007; Zhang et al. 2012; McCartney et al. 2013). They function similar to conventional ground-
36 source heat pump (GSHP) systems, where fluid is circulated within a closed-loop pipe network
37 installed in vertical boreholes to shed or absorb heat from the surrounding subsurface. Different
38 from conventional GSHP system, SBTES systems are configured to store thermal energy
39 collected from solar thermal panels during the summer, and discharge the heat to buildings
40 during the winter. The temperature of the ground within the array increases from its ambient
41 temperature (approximately 10-20 °C) to 60-90 °C during heat injection due to thermal inertia of
42 the soil. The maximum temperature a soil can reach is governed by volumetric heat capacity of
43 the soil. A higher value of the volumetric heat capacity implies a longer time for the system to
44 reach equilibrium. SBTES systems are a convenient alternative to other energy storage systems

45 as they are relatively inexpensive, involve storage of renewable energy (solar thermal energy),
46 and are space efficient as they are underground.

47 One challenge with SBTES systems is the need to improve the efficiency of heat transfer into
48 and out of the array of geothermal boreholes. Zhang et al. (2012) analyzed the heat exchange
49 processes at the Drake Landing site, an example of a successful SBTES project in Alberta,
50 Canada, and found that the efficiency of heat transfer (defined as the amount of heat extracted
51 divided by the amount of heat injected) is approximately 27%. Although the efficiency of heat
52 transfer is low, the SBTES system at the Drake Landing site has provided more than 90% of the
53 heating to 52 houses over the past several years (Sibbitt et al. 2007; 2012). This is an important
54 point to consider as the thermal energy being stored in the SBTES system is obtained freely from
55 a renewable source with a low cost.

56 An opportunity to enhance the efficiency of SBTES systems is to install them in the vadose
57 zone (the unsaturated zone of soil above the water table). It has been shown that the latent heat of
58 phase change enhances the heat transfer process in unsaturated soil layers, and that convection
59 plays a major role in transporting thermal energy in unsaturated soils subject to a temperature
60 gradient (Cass et al. 1984). In the case of SBTES systems in the vadose zone, it is possible to
61 take advantage of phase change phenomena in the pore water to obtain greater heat injection and
62 extraction rates by formation of a convective cell between the borehole heat exchangers. A
63 convection cell will form in an unsaturated soil layer because as the pore water around the heat
64 exchanger array is heated, it will vaporize and move upward due to buoyancy and toward colder
65 regions away from the heat source. The water then condenses at a cold boundary, releasing latent
66 energy. The water will then flows downward due to gravity and back toward the dry soil around
67 the heat source in response to the suction gradient. During this flow process, enhanced heat

68 transfer will occur when latent energy is absorbed by the water during vaporization and released
69 during condensation. The mechanisms of heat transfer and water flow in the analogous
70 convective cell expected within a borehole heat exchanger array is shown in 2-dimensions in
71 Figure 1. Sakaguchi et al. (2009) observed the formation of a convective cell in an unsaturated
72 soil layer and observed an increase in apparent thermal conductivity with increasing temperature
73 and explained this increase in terms of the latent heat transfer processes occurring in the soil. Lu
74 (2001) found that the rate of heat transfer in a convective cell in an unsaturated soil layer may be
75 up to 10 times faster than assuming that heat conduction is the only mode of heat transfer.

76 An example of the possible heat transfer and water flow processes associated with the
77 formation of a convective cell within the context of the boundary conditions of an SBTES
78 installed in the vadose zone is shown in Figure 2. The SBTES system incorporates an insulated
79 hydraulic barrier at the soil surface, which is necessary as the long-term performance of the
80 SBTES system may be affected by upward water loss from within the borehole array due to
81 evaporation and thermally-induced water flow. Downward heat flow into the soil below the water
82 table is not restricted, but the lower thermal conductivity of the unsaturated soil outside of the
83 array may provide an insulating effect to help retain heat within the array.

84 To better understand the behavior of SBTES systems in the vadose zone, the impacts of
85 latent and sensible heat transfer associated with phase change and flow of pore water on the
86 transfer and storage of heat within a geothermal borehole array in an unsaturated silt layer are
87 investigated in this study. Specifically, physical models consisting of a layer of unsaturated silt
88 compacted atop a layer of saturated sand in an insulated, cylindrical tank were constructed to
89 observe these processes during heat injection. Three steel “U”-tube pipes were inserted through
90 the silt layer into the top of the sand layer to simulate an array of geothermal borehole heat

91 exchangers. In one model, the heat exchangers were placed at a radial location that is 26% of the
92 tank radius, while in the other model the heat exchangers were placed on the inside of the tank
93 wall.

94 During the tests, heated fluid was circulated through the steel pipes to inject heat into the silt
95 layer at a constant rate. The boundary conditions in the test are selected to simulate the behavior
96 of the soil between the borehole array shown in Figure 2, knowing that the lateral heat loss and
97 water transfer out of the array were not properly simulated in the array with the heat exchangers
98 on the inside of the container wall. Sensors to monitor changes in temperature, volumetric water
99 content and thermal conductivity were placed in the silt layer at strategic locations to monitor the
100 changes in the thermo-hydraulic properties of the soil and to infer mechanisms of coupled heat
101 transfer and water vapor flow.

102 **MATERIALS**

103 The physical modeling experiments were performed on a layered system involving a 62-mm-
104 thick layer of Nevada sand having a porosity of 0.43 overlain by a 500-mm-thick layer of
105 unsaturated, compacted Bonny silt having a porosity of 0.47. Nevada sand is classified as SP
106 according to the Unified Soil Classification System (USCS) and a porosity of 0.43 corresponds to
107 a relative density of 60%. Bonny silt is classified as ML (inorganic silt) according to the USCS
108 and has a specific gravity of 2.65. The optimum water content and the maximum dry unit weight
109 corresponding to the standard Proctor compaction effort are 13.6% and 16.3 kN/m³, respectively.
110 The initial thermal conductivity for compacted Bonny silt under these conditions is
111 approximately 1.2 W/(m·K), although this value is likely to change with variations in degree of
112 saturation and temperature (Smits et al. 2013).

113 **EXPERIMENTAL SETUP AND PROCEDURES**

114 Schematics of the physical models of the SBTES systems fabricated to study coupled heat
115 transfer and water flow in the unsaturated soil layers are shown in Figure 3. The cylindrical
116 aluminum container has a diameter of 603 mm and a height of 554 mm. The base of the
117 container has two ports on opposite sides to permit inflow and outflow of water into the base of
118 the container for control of the water table. One of the ports was connected to a constant-head
119 Mariotte bottle to maintain the water table at the top of the sand layer.

120 The first step in preparing the physical model was to place a layer of Nevada sand at the
121 bottom of the container using air pluviation. A thin filter fabric was placed over the surface of the
122 sand to prevent its mixing with the overlying silt layer. Next, the silt layer was compacted in
123 seven lifts to achieve a void ratio of 0.90 (porosity of 0.47) that is uniform with depth. Three of
124 U-tubes having an outside diameter of 6 mm and an inside diameter of 2 mm, and a length of 560
125 mm were buried during the compaction. The distance between the inlet and outlet pipes is
126 approximately 75 mm. The 5TE dielectric sensors for measurement of temperature and
127 volumetric water content and SH-1 thermal needle for measurement of the thermal conductivity
128 of the silt with the KD2Pro system (all obtained from Decagon Devices of Pullman, WA), along
129 with the closed-loop heat exchangers were placed in the silt layer during compaction at the
130 locations shown in Figure 3. The dielectric sensors were placed at a vertical spacing of 85 mm
131 apart along radial center of the soil layer. The thermal needle was placed at mid-height of the silt
132 layer at the center of the container. After all the lifts and sensors were placed in the soil, EL-
133 USB-2LCD relative humidity/temperature sensors manufactured by Lascar Electronics were placed
134 on the soil surface as well as in the same room as the experiment. Next, several layers of plastic
135 wrap were placed on the soil surface to minimize loss of water to the laboratory air due to
136 evaporation. The top and sides of the container were then wrapped in insulation with 2 layers to

137 minimize heat loss from the soil layer. The four type-K thermocouple profile probes, each
138 containing six thermocouples at a spacing of 30 mm) were pushed through the insulation into the
139 compacted silt layer at different radial distances summarized in Table 1.

140 A schematic of the physical model and the temperature control system is shown in Figure 4.
141 A high-temperature water pump was used to circulate water through a temperature-regulated
142 heated reservoir and into the array of steel closed-loop “U”-tube heat exchangers. The heated
143 reservoir is pressurized to minimize the chances for air bubbles from stopping the operation of
144 the pump under high temperatures. In order to see how much heat is transferred in the soil, pipe
145 plug thermocouples probes (Model TC-J-NPT-G-72 from Omega, Inc.) were also used to measure
146 the temperature of the water going into and out of the heat exchanger tubes. After saturation of the
147 sand layer, heated water was circulated through the heat exchanger pipes. More details of the
148 testing setup are provided in Traore (2013).

149 **RESULTS**

150 Two heat injection tests were performed on identical soil layers with borehole heat exchanger
151 arrays having radial spacings of 80 and 300 mm from the center of the container. Although the
152 dielectric sensors and the thermal conductivity sensor were placed at the same locations in the
153 center of silt layer in both tests, the radial locations of the thermocouple profile probes were
154 different. A summary of the radial distances of the closed loop heat exchanger tubes and the
155 thermal sensor probes in both tests is also shown in Table 1. The entering and exiting
156 temperatures of the water in the borehole heat exchangers are shown in Figures 5(a) and 5(b) for
157 Tests 1 and 2, respectively. At steady-state, the entering and exiting water temperatures were
158 approximately 85 and 80 °C for Test 1, while they were 86 and 79 °C for Test 2. The flow rate of
159 the water circulating through the heat exchanger tubes was 0.38 l/s in both tests, and was

160 assumed to be steady throughout the tests. The slight difference in the temperature difference
161 reflects a greater heat flux into the soil layer in Test 2, for reasons that will be discussed later.
162 However, the heat exchangers had similar average temperatures in both tests.

163 The temperatures at the surface of the soil layers and within the laboratory are shown in
164 Figures 6(a) and 6(b) for Tests 1 and 2, respectively, while the relative humidity values of the
165 soil surface (beneath the hydraulic barrier) and the ambient laboratory are shown in Figures 6(c)
166 and 6(d) for Tests 1 and 2, respectively. The ambient temperature and relative humidity of the
167 laboratory oscillate on a daily basis due to the operation of the heating and cooling system, while
168 the temperature and relative humidity at the surface of the soil layer beneath the hydraulic barrier
169 and insulation layer reach stable values (50 °C and 70%, respectively, after 10 hours in Test 1
170 and 45 °C and 70%, respectively, after 30 hours in Test 2). To minimize heat loss
171 from the setup, insulation was placed over the hydraulic barrier so only slight
172 oscillations in the room temperature were observed to affect the soil surface
173 temperatures.

174 The changes in temperature at the depths of the five dielectric sensors installed in the center
175 of the silt layer are shown in Figures 7(a) and 7(b) for Tests 1 and 2, respectively. In both tests,
176 the tests started at an ambient laboratory temperature of 26 °C, and it ranged between 26 and 29
177 °C. The temperatures at the center of the silt layer reached a stable value after approximately 30
178 hours of operation for Test 1, but they didn't reach a stable value until after approximately 60
179 hours for Test 2. This can be attributed to the wider spacing. The corresponding changes in
180 volumetric water content are shown in Figures 7(c) and 7(d) for Tests 1 and 2, respectively. The
181 volumetric water content values inferred from the dielectric sensors were corrected to account

182 for temperature effects as follows: $\theta_w = \theta_{w,\text{measured}} - 0.001725\Delta T$, where ΔT is the change in
183 temperature at the location of each sensor. In Test 1, a brief increase in volumetric water content
184 at the center of the array is observed, after which a steady decrease in water content occurs for
185 the remainder of the test. This occurred as water was initially driven away from the heat
186 exchangers toward the center of the array, after which water was driven outward from the array.
187 In Test 2, a steady increase in volumetric water content at the center of the array is observed.
188 This may have occurred because water loss to the outside of the array was prevented by the
189 container (and thus the array) in Test 2, but also because of the possible formation of a
190 convective cell within the array where water was rising upward from the water table.

191 The average changes in temperatures with depth from each of the thermocouple profile
192 probes installed at different radial distances from one of the heat exchangers are shown in
193 Figures 8(a) and 8(b) for Tests 1 and 2. As expected, the thermocouple profile probes indicate
194 that temperatures of the soil decrease with radial distance from the heat exchangers. This
195 information is useful for assessment of the thermal conductivity of the soil outside of the array,
196 which will be presented later.

197 Profiles of temperature with depth along the center of the soil layer are shown in Figures 9(a)
198 and 9(b) for Tests 1 and 2, respectively. In both tests, the smallest temperatures were observed at
199 the bottom and top of the silt layer due to upward and downward heat loss, while the highest
200 changes in temperatures were observed at mid-height. The lower temperatures in the wider
201 borehole array may be due to the greater loss of heat through the boundary of the container due
202 to the contact between the boreholes and the metal heat exchangers. The greater uniformity of
203 temperature with depth in Test 2 have occurred due to the convective mixing within the soil
204 array. Profiles of volumetric water content are shown in Figures 9(c) and 9(d) for Tests 1 and 2,

205 respectively. The water content was relatively uniform with depth in Test 1, and upward water
206 flow due to capillary rise was not observed. In addition to a steady increase in water content in
207 Test 2, the soil closer to the water table was observed to become wetter with time. This is due to
208 both capillary rise and potentially to a greater amount of upward water vapor flow due to
209 buoyancy. Although water was visually observed to condense at the soil surface in both
210 experiments, downward liquid water flow due to gravity was not observed to be significant
211 compared to the rate of upward vapor flow. Longer testing times may have revealed this
212 phenomenon. Alternatively, testing of the small-scale model in a geotechnical centrifuge may
213 help better replicate the roles of capillary rise and downward liquid water flow so that they are
214 more representative of field conditions in a full-scale SBTES system.

215 The apparent thermal conductivity and specific heat capacity of the unsaturated silt measured
216 using the thermal needle probe embedded at the center of the profile are shown in Figures 10(a)
217 and 10(b) for Tests 1 and 2, respectively. In Test 1, the thermal conductivity at the center of the
218 array was observed to increase up to $1.35 \text{ W}/(\text{m}\cdot\text{K})$ for a brief period that corresponds to the
219 peak in volumetric water content. After this point, the apparent thermal conductivity of the soil
220 within the array was observed to decrease slowly to a value of approximately $0.55 \text{ W}/(\text{m}\cdot\text{K})$. The
221 specific heat capacity increases slightly after the volumetric water content starts to decrease, after
222 which it decreases to a value of $1.5 \text{ MJ}/(\text{m}^3\cdot\text{K})$. This implies that the maximum heat storage
223 within the array decreases over time as the degree of saturation within the array decreases.
224 Different behavior was noted in Test 2. The apparent thermal conductivity was observed to
225 increase slowly throughout the test to a steady value of $1.22 \text{ W}/(\text{m}\cdot\text{K})$. The specific heat capacity
226 was also observed to increase during the first 220 hours of operation until it reached a steady
227 value of $2.05 \text{ MJ}/(\text{m}^3\cdot\text{K})$. Post-test evaluation of the gravimetric water content distribution in the

228 soil layer in Test 1 indicates that water in the soil within the array was observed to move outside
 229 of the array into the surrounding soil in Test 1. A distinct zone of drying was not observed in the
 230 soil layer in Test 2.

231 ANALYSIS

232 To analyze the heat transfer and water flow in the vadose zone within the closed-loop heat
 233 exchangers array, the coupling between the different thermo-hydraulic properties of the
 234 unsaturated soil must be characterized. Relationships between the apparent thermal conductivity,
 235 specific heat capacity, temperature, and degree of saturation are shown in the Figure 11. The
 236 degree of saturation was calculated from the change in volumetric water content ($\Delta S = S_0 - \Delta\theta/n$,
 237 where S_0 is the initial degree of saturation and n is the porosity of the soil). The results indicate
 238 the apparent thermal conductivity is sensitive to both degree of saturation as well as temperature
 239 (Smits et al. 2013). The specific heat capacity appears to be relatively insensitive to temperature
 240 and is more closely related to the degree of saturation.

241 Although the apparent thermal conductivity of the mass of soil outside of the heat exchanger
 242 array was not measured directly, it can be estimated from the average soil temperature values
 243 measured using the thermocouple profile probes by assuming that conduction is the mode of heat
 244 transfer so that Fourier's law can be used to estimate the thermal conductivity. Specifically the
 245 form of Fourier's law governing conductive heat transfer in soil away from a cylindrical heat
 246 source is given as follows (Carslaw and Jaeger 1959):

$$247 \quad \dot{Q} = -2\pi Rl\lambda \left[\frac{dT}{dr} \right] \quad (1)$$

248 where \dot{Q} (W) is the heat transfer rate, λ (W/m K) is the soil thermal
 249 conductivity, l (m) is the total length of the borehole, R (m) is the radius of

250 the borehole, and $\left[\frac{dT}{dr}\right]$ (K/m) is the temperature gradient in the soil defined
 251 from the thermocouple measurements at different radial locations. The term
 252 $2\pi Rl$ (m²) is the average surface area of a heat exchanger borehole from
 253 which heat is transferred. The value of \dot{Q} can be estimated by assuming that
 254 convection is the main heat transfer process in the flowing fluid within the
 255 array using the following equation:

$$256 \quad \dot{Q} = \dot{V}_w \rho_w C_w (T_{in} - T_{out}) \quad (2)$$

257 where \dot{V} is the volumetric flow rate of water in ml/s, ρ_w is the density of water (1 g/ml), C_w is the
 258 specific heat capacity of water equal to 4183 J kg⁻¹ K⁻¹, and T_{in} and T_{out} are the temperatures of
 259 the water entering and exiting the heat exchanger loops, respectively. The equation for the
 260 apparent thermal conductivity of the soil outside of the array can be estimated by combining
 261 Equations (1) and (2), as follows:

$$262 \quad \lambda = \frac{\dot{V} \rho C (T_{in} - T_{out})}{-2\pi Rl \left[\frac{dT}{dr}\right]} \quad (3)$$

263 The apparent thermal conductivity of the soil outside of the heat exchanger array in Test 1
 264 can be compared with that of the soil within the heat exchanger array, as shown in Figure 12. It
 265 is clear that the apparent thermal conductivity of the soil outside of the borehole heat exchanger
 266 array increased during the test, likely due to the gradual wetting of the soil due to thermally-
 267 induced water flow out of the array. Although this comparison was not possible for Test 2 as the
 268 heat exchangers were located at the edge of the container, the comparison for Test 1 confirms the
 269 importance of considering thermally induced water flow on the heat transfer processes in SBTES
 270 systems in the vadose zone.

271 The results in Figure 10 and 11 confirm that the thermal conductivity is closely related to the
272 degree of saturation. Thermally-induced water flow will lead to an increase in apparent thermal
273 conductivity of the soil, leading to an increase in heat transfer into the soil. For Test 1 (80 mm
274 array spacing) the degree of saturation decreases at a change in temperature of 31 °C, leading to a
275 corresponding decrease in apparent thermal conductivity. The heat transfer within the heat
276 exchanger array causes water to flow out of the soil within the array in the form of water vapor.
277 As a result, the soil pores within the array are filled with air, which is a poor heat conductor.
278 Conduction becomes the main mode of heat transfer within the borehole heat exchangers array,
279 and heat transfer into the array decreases. Different from the results in Test 1, the presence of the
280 extra water due to thermally-induced water flow and capillary rise within the array in Test 2 led
281 to a sustained increase in apparent thermal conductivity in the soil layer.

282 A comparison of the change in the degree of saturation at the center of the soil layers in Tests
283 1 and 2 is shown in Figure 13. A decrease in the degree of saturation within the array in Test 1
284 occurred as water was permanently driven from the center of the array, which means that this
285 spacing may be too small to induce a convective cell within the array. In Test 2, after the degree
286 of saturation reached a steady value, the thermal conductivity was observed to continue
287 increasing. This is further evidence that a convective cell may have formed within the array.

288 For simplicity of comparison of the tests in this study, the soil volume within the array is
289 defined as the soil within the radius of the heat exchangers. This definition is necessary as the
290 array with wider spacing in Test 2 is surrounded by a no-flow boundary. However, it differs from
291 the definition of the array for a SBTES system in the field, which will incorporate some of the
292 soil outside of the array itself because this heat can still be accessed during heat extraction (Baser

293 and McCartney 2015). Nonetheless, the heat transferred into the array as a function
 294 of time can be estimated using Equation (2). The heat transfer is expected to
 295 be initially transient until the soil reaches a constant temperature and water
 296 flow ceases. The transient process may be nonlinear due to the effects of
 297 thermally induced water flow in the soil. At large times, it is expected that
 298 the amount of heat injected will equal the amount of heat lost from the array
 299 as the soil has reached its heat capacity. The rate of heat loss from the array
 300 in Test 1 can also be estimated using Equation (1), considering the
 301 temperature gradient between the array and the soil outside of the array.
 302 The thermal conductivity of the soil outside of the array calculated from
 303 Equation (3) can be used in the heat loss calculation in the case of Test 1.
 304 The rate of heat loss from the array in Test 2 is different due to the presence
 305 of the insulated container adjacent to the heat exchangers. In this case, the
 306 steady state heat loss rate from the container can be estimated as follows
 307 (Gabrielsson et al. 2000):

$$308 \quad \dot{Q} = \frac{\lambda_{cont} A_{cont} (T_g - T_a)}{d} \quad (4)$$

309 where \dot{Q} is rate of heat loss from the container (W), λ_{cont} is the thermal
 310 conductivity of the container (W/(m•K)), A_{cont} is the surface area of the
 311 container sides (m²), d is the thickness of the container, T_g represents the
 312 boundary temperature of the array (K), and T_a the mean temperature at the
 313 outer wall of the container (K). The boundary temperature is assumed to be
 314 equal to the mean temperature of the soil within the array and a reasonable
 315 estimation of T_a is the mean temperature of the ambient air.

316 The rates of heat injection and heat loss from the arrays in Tests 1 and 2 are presented in
317 Figure 14(a) and 14(b), respectively. In both tests, the heat injection rate initially has a high
318 value as the temperature gradient between the heat exchangers and the relatively cool soil is
319 high. The heat injection rate then drops over time as the temperature within the array increases
320 until reaching a relatively constant value after approximately 30 hours for Test 1 and after 60
321 hours for Test 2. The spike in heat transfer rate in Test 1 occurred as the circulation pump shut
322 off accidentally for a moment. The gradual increase in the heat loss from the array in Test 1 is
323 associated with the thermally induced water flow out of the array, making this soil more
324 conductive to heat. The rate of heat loss from the array in Test 2 is steady as the temperature of
325 the soil and the outside of the container were relatively constant during the test. At steady state, it
326 is clear that more heat is transferred to the unsaturated silt within the array in Test 2 than in Test
327 1. This is primarily due to the greater amount of soil to be heated within the array in Test 2, but
328 may be due partially to the enhanced thermal properties of the unsaturated soil associated with
329 convective processes.

330 In either test, the heat storage can be defined with energy balance within the array
331 corresponds to the difference in the cumulative amounts of heat injected into the soil and the
332 amount of heat lost from the array, which can be defined as follows:

$$333 \quad Q_{stored} = Q_{injected} - Q_{lost} \quad (5)$$

334 The cumulative heat injection and loss along with the corresponding heat storage in Tests 1 and 2
335 are shown in Figures 15(a) and 15(b). The total heat storage in Test 1 is observed to initially
336 increase due to the transient effects at the beginning of the test, but is then observed to decrease
337 due to the steady heat injection at the same time as the increase in heat loss. Due to the high heat
338 loss, the heat storage appears to tend toward a maximum value of 253 MJ. The heat storage in

339 Test 2 also initially increases steeply, but after 60 hours increases at a steady rate after
340 approximately 60 hours. Although the soil reached a steady temperature and water content
341 profile, the heat storage did not reach a stable value, possibly due to inaccuracies in calculating
342 the temperature gradient across the container wall in Equation 4. The results from the tests are
343 summarized in Table 2. Despite the different durations of the two tests, they were performed
344 until the water flow within the array stabilized. Despite the difference in durations, a greater
345 amount of heat had been injected into the array in Test 2 after 30 hours of heating (the time when
346 Test 1 was stopped), which can be attributed to the role of coupled heat transfer and water flow
347 in this test, and potentially the formation of a convective cell in the array.

348 **CONCLUSIONS**

349 The role of coupled water and heat transfer in unsaturated soil layers was assessed in this
350 study to better understand the behavior of soil-borehole thermal energy storage (SBTES) systems
351 installed in the vadose zone. The results from two tests involving three closed-loop heat
352 exchangers at radial spacing of 80 and 300 mm in the 500 mm-thick layer of unsaturated silt are
353 reported, which provide useful information for the validation of thermo-hydraulic flow
354 simulations. In each test, water with a temperature of approximately 80 °C was circulated
355 through the heat exchangers to inject heat into the unsaturated soil layer. In both tests, the
356 apparent thermal conductivity was observed to depend on the degree of saturation of the soil and
357 the temperature. For the borehole array with the smaller spacing, permanent drying of the soil
358 within the array was observed shortly after heating started. A convective cell was not formed in
359 this array, and heat transferred into the array was observed to decrease over time as the soil
360 dried. Further, the rate of heat loss from the borehole array to the surrounding soil was observed
361 to increase with time as thermally induced water flow away from the array carried more heat out

362 of the array than into the array. For the borehole array with the larger spacing, the soil layer
363 experienced an increase in water content over time, indicating superior heat transfer due to
364 coupling between water flow and heat transfer. The soil within the array with wider spacing was
365 observed to steadily increase in degree of saturation and thermal conductivity, which
366 corresponds to the greater rate of heat injection in this test. A slight increase in the specific heat
367 capacity was also observed. The heat storage, defined as the difference between the cumulative
368 amounts of heat injected and lost from borehole array, was greater in the array with larger
369 spacing where outward water flow was prohibited by the container. Not only was there a larger
370 zone of soil, but the rate of heat was greater in the array with a larger spacing. This occurred as
371 there was a larger zone of soil within the array and because the soil experienced a greater
372 increase in water content within the area during heating due to coupled heat transfer and water
373 flow into the array.

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410

411 FIGURE CAPTIONS

412 Figure 1. Mechanisms of heat transfer and water flow within a convection cell formed within an
413 array of geothermal heat exchangers in the vadose zone

414 Figure 2. Heat transfer and water flow processes in the vadose zone within the context of the
415 boundary conditions representative of SBTES systems

416 Figure 3. Elevation and plan views of the soil container showing instrumentation and expected
417 heat transfer processes in the physical model (note: one heat exchanger is shown out of plane
418 in the elevation views for emphasis): (a) Small array; (b) Large array

419 Figure 4. Schematic of the overall experimental setup

420 Figure 5. Inlet and outlet fluid temperatures: (a) Test 1; (b) Test 2

421 Figure 6. Temperature and relative humidity at the soil surface (under the hydraulic barrier) and
422 in the laboratory (a) Temperature in Test 1; (b) Temperature in Test 2; (c) Relative humidity
423 in Test 1; (d) Relative humidity in Test 2

424 Figure 7. Time series of dielectric sensor data: (a) Change in temperature in Test 1; (b) Change
425 in temperature in Test 2; (c) Change in volumetric water content in Test 1; (d) Change in
426 volumetric water content in Test 2

427 Figure 8. Change in average soil temperatures with depth at different horizontal distances from
428 the center of the borehole heat exchanger array: (a) Test 1; (b) Test 2

429 Figure 9. Profile data from the dielectric sensors embedded in the center of the soil layer at
430 different depths: (a) Change in temperature in Test 1; (b) Change in temperature in Test 2; (c)
431 Change in volumetric water content in Test 1; (d) Change in volumetric water content in Test
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- 433 Figure 10. Time series from the thermal conductivity sensor embedded in the middle of the
434 unsaturated soil layer: (a) Test 1; (b) Test 2
- 435 Figure 11. Pictures of the excavated soil layer after heating: (a) Test 1; (b) Test 2
- 436 Figure 12. Apparent thermal conductivity, specific heat capacity, and degree of saturation with
437 the change in temperature at the center of the borehole array: (a) Test 1; (b) Test 2
- 438 Figure 13. Comparison of thermal conductivity inside and outside the borehole array in Test 1
- 439 Figure 14. Degree of saturation as a function of borehole heat exchanger spacing
- 440 Figure 15. Heat transfer rates: (a) Test 1; (b) Test 2
- 441 Figure 16. Evaluation of the energy balance: (a) Test 1; (b) Test 2
- 442

443 Table 1. Details of the physical modeling tests on SBTES systems with different array spacings

Test	Dry density (kg/m ³)	Initial volumetric water content (m ³ /m ³)	Initial degree of saturation (m ³ /m ³)	Porosity (m ³ /m ³)	Borehole array radial spacing (mm)	Radial locations of thermocouple profile probes			
						r ₁	r ₂	r ₃	r ₄
1	1400	0.236	0.40	0.47	80	110	160	210	260
2	1400	0.233	0.40	0.47	300	300	250	200	150

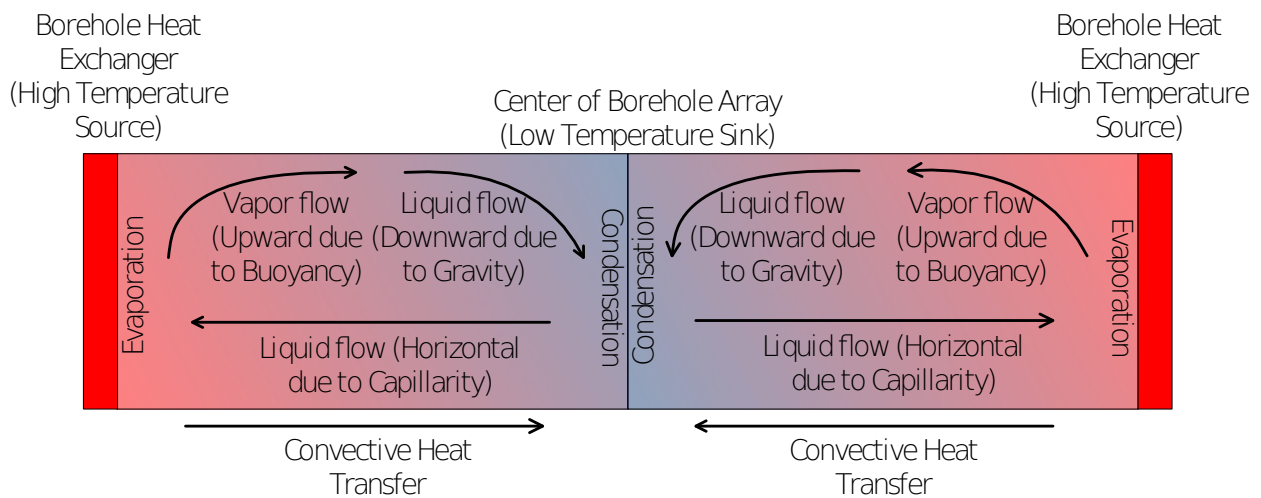
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445 Table 2. Summary of the estimated heat transfer and heat storage calculations

446 for both tests

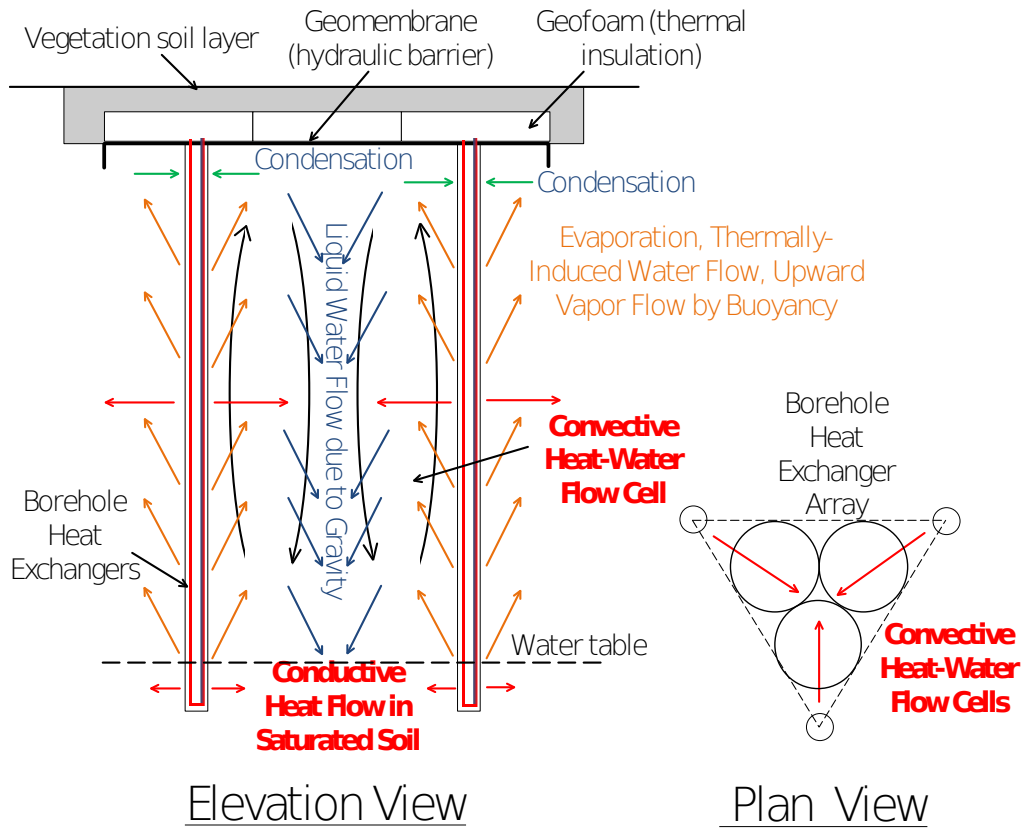
Test	Spacing (mm)	Duration until reaching stable water content (hours)	Average steady-state heat transfer (W)	Average steady-state heat loss (W)	Total heat injected (MJ)	Total heat lost (MJ)	Total heat stored (MJ)
2	300	715	975	399	2364	915	1449

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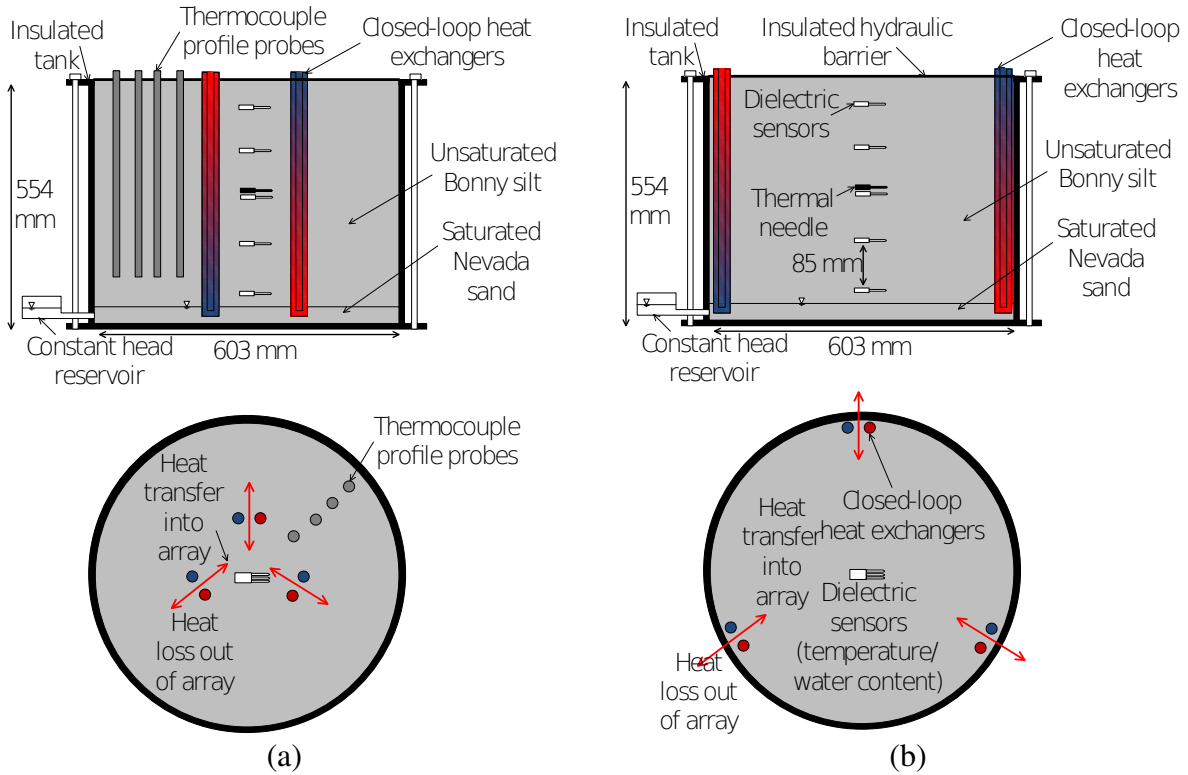
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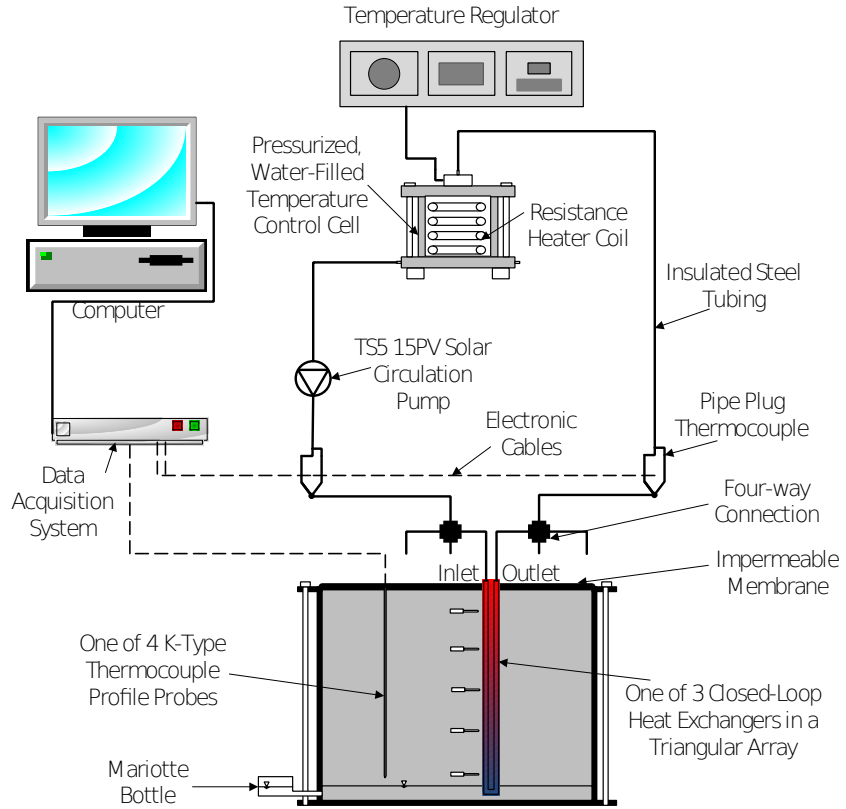


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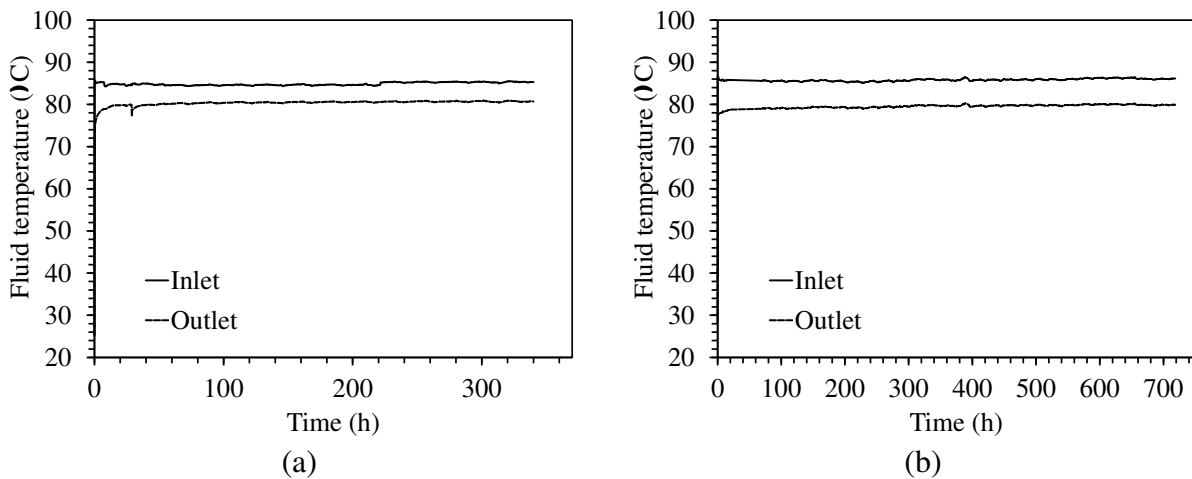
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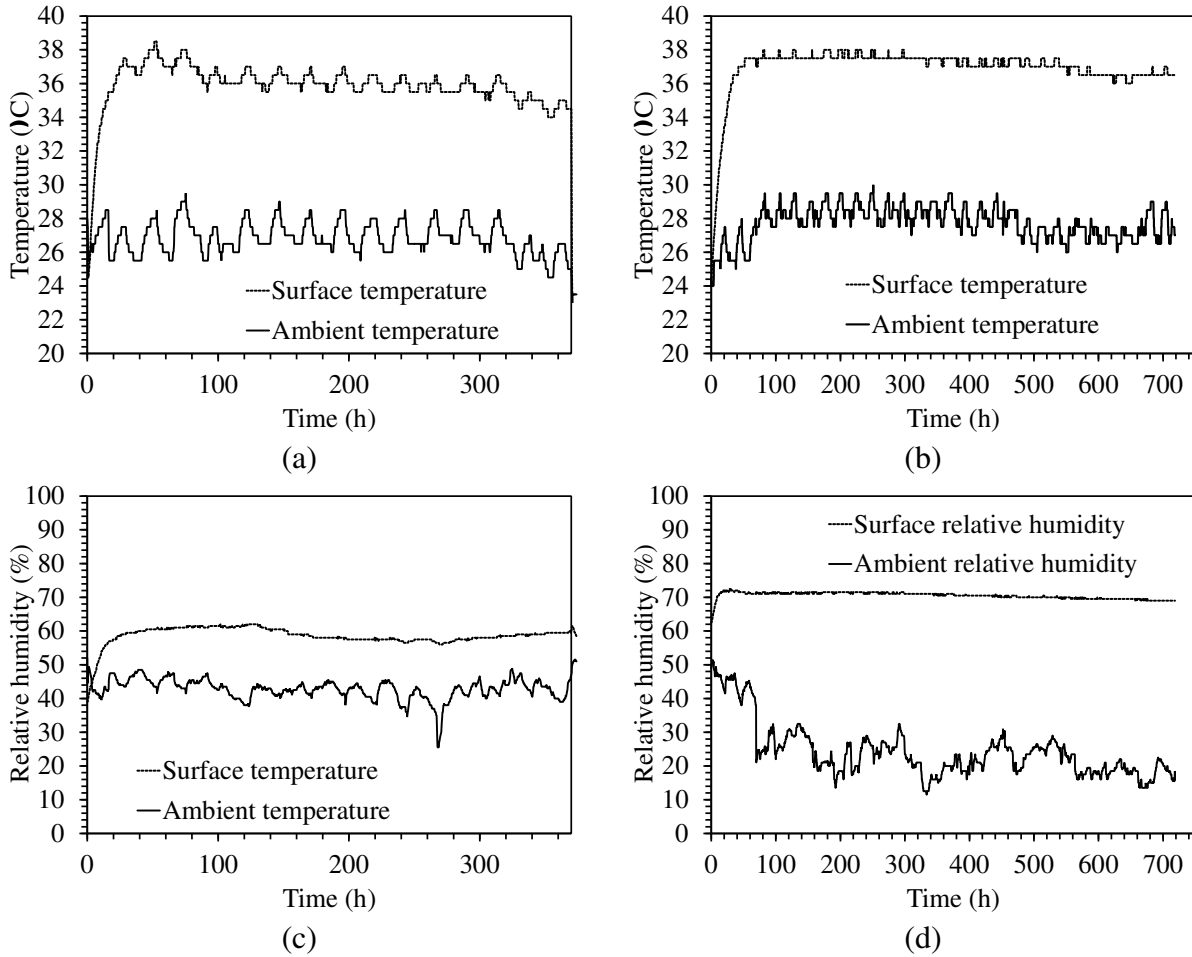
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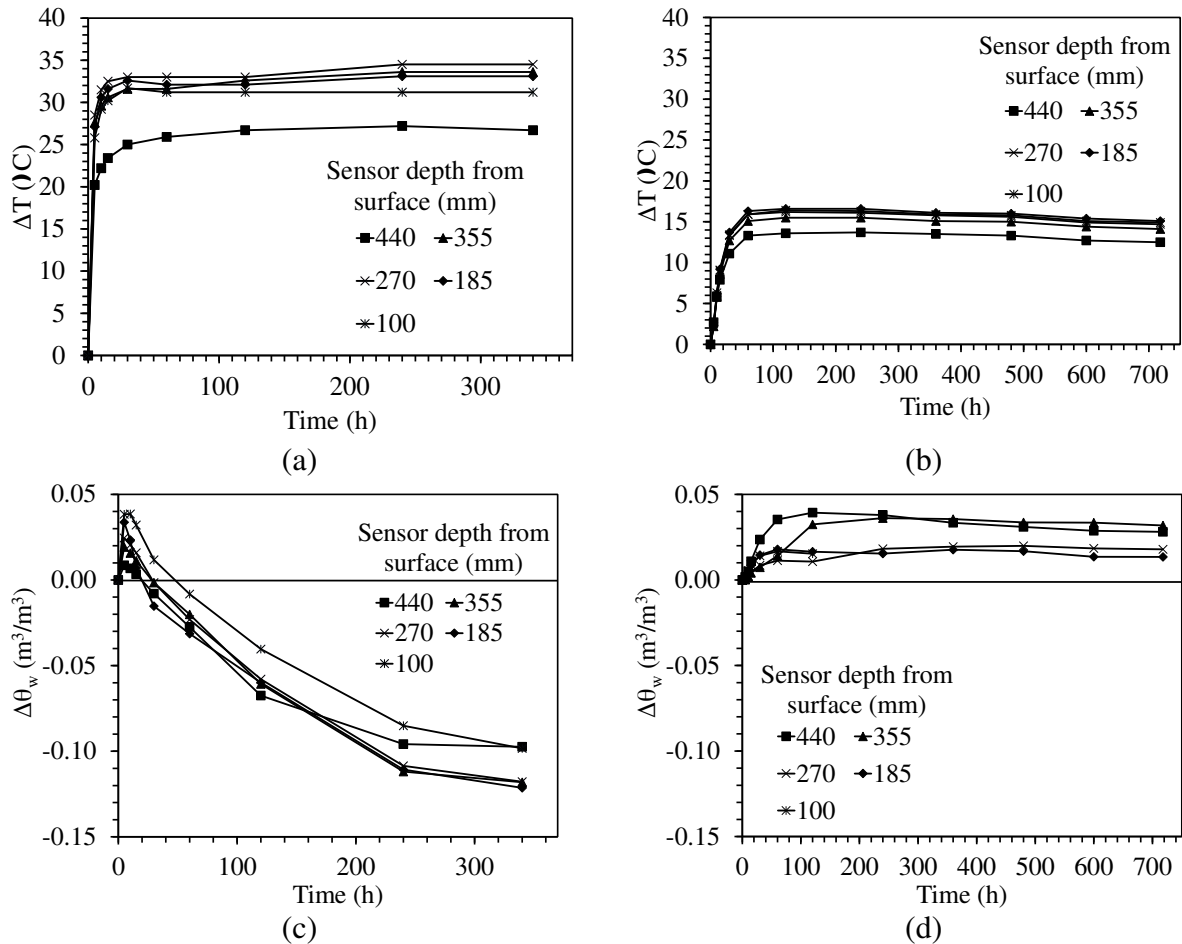
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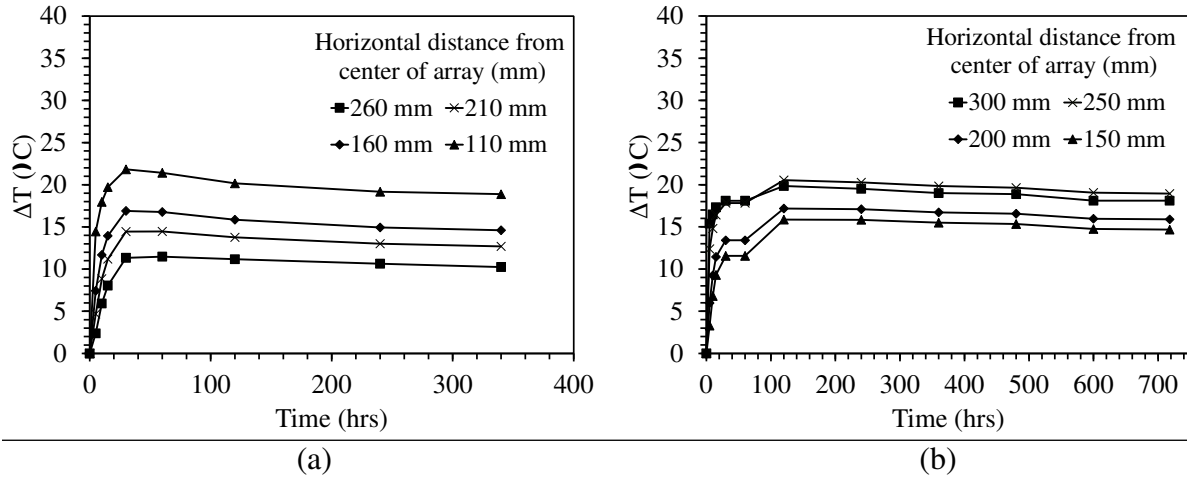
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 468

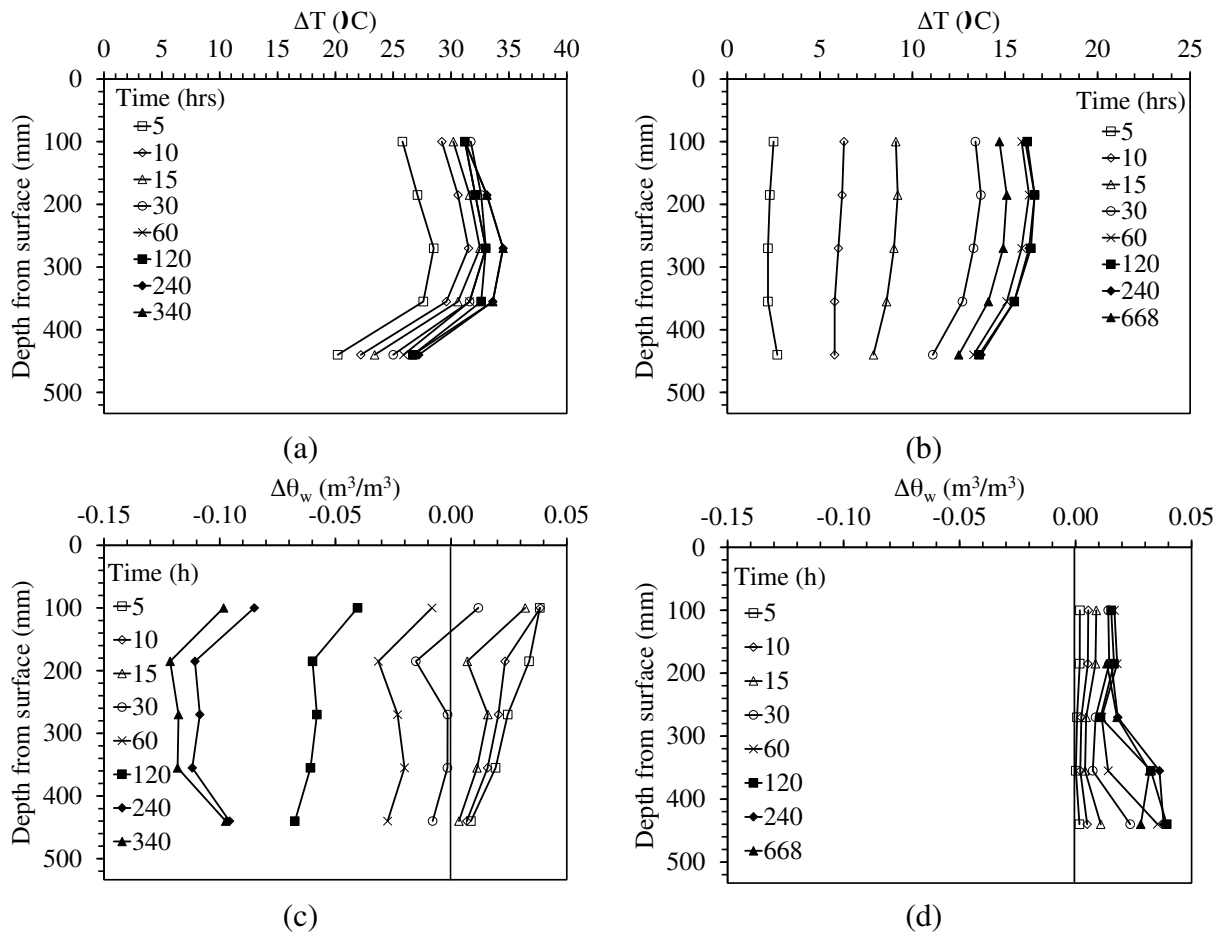


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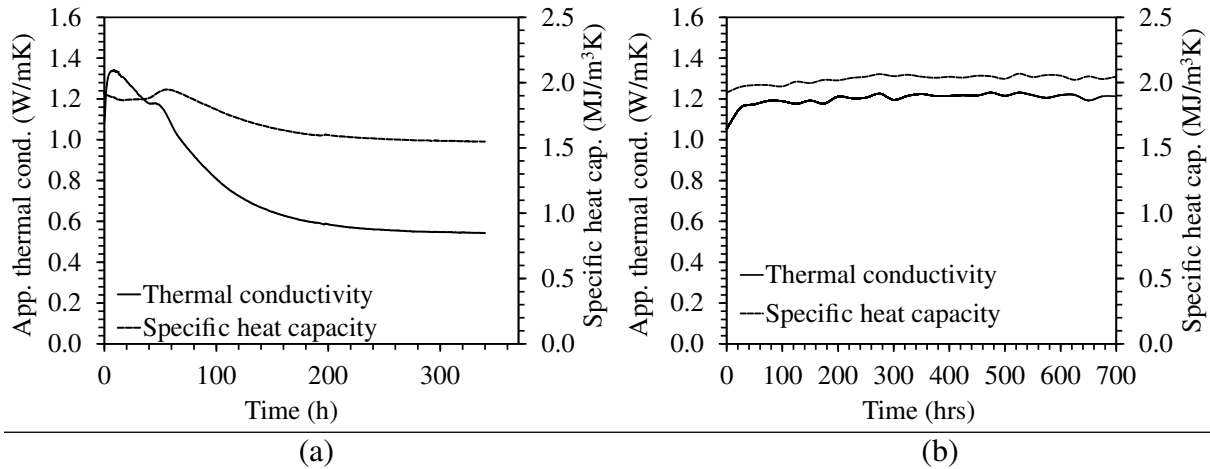
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 476 Test 2
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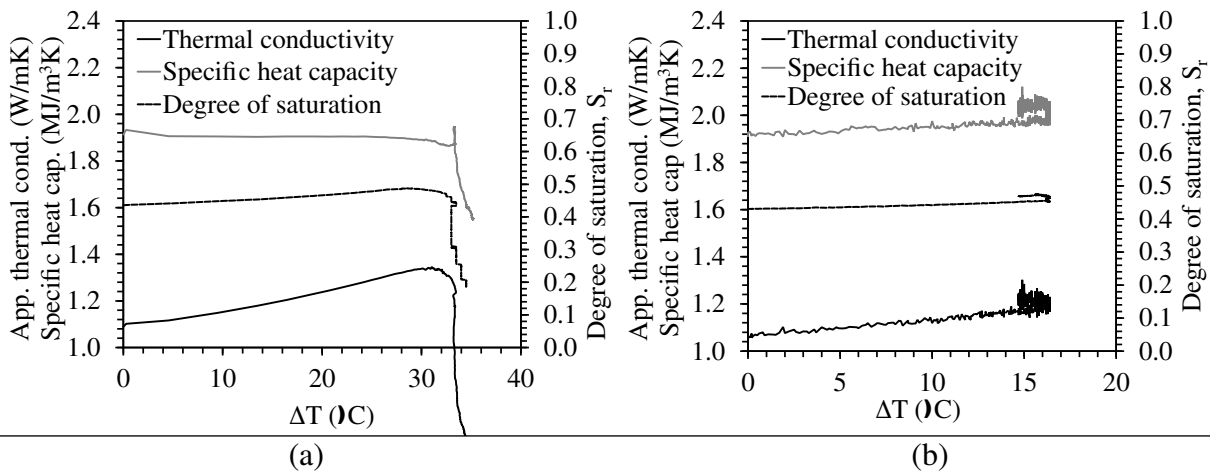


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479 Figure 10. Time series from the SH-1 thermal sensor embedded in the middle of the unsaturated

480 soil layer: (a) Test 1; (b) Test 2

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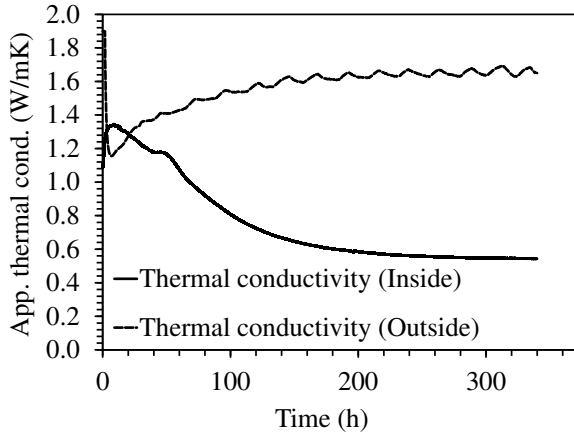
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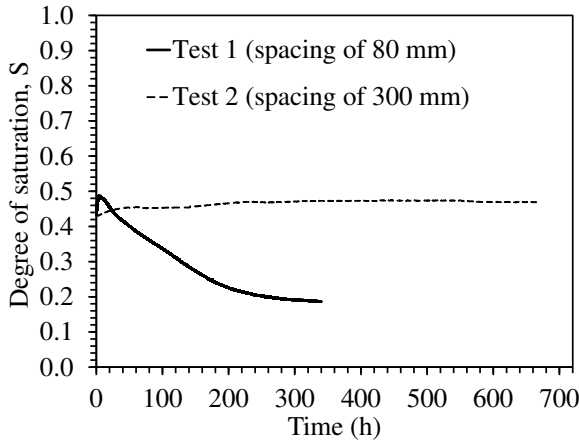
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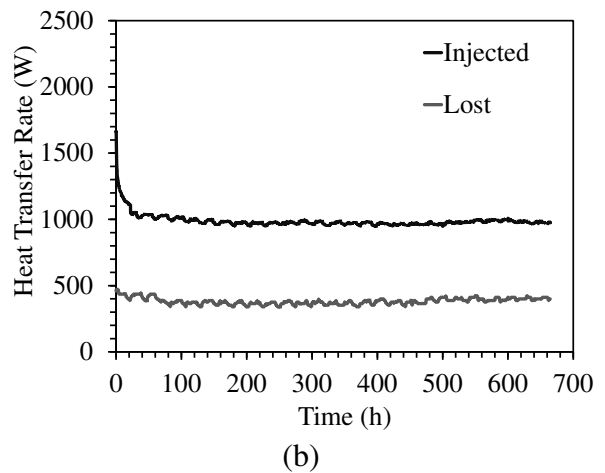
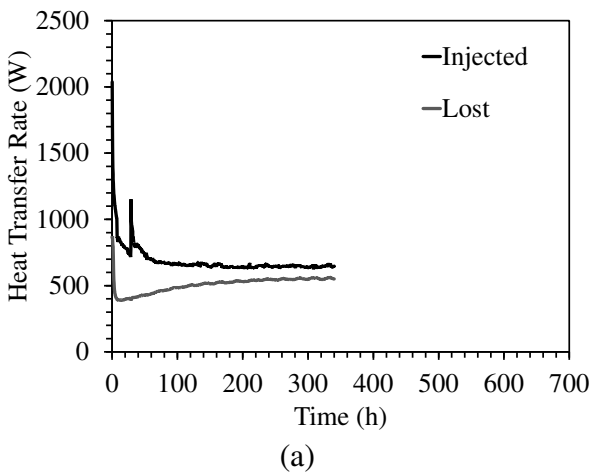
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489 Figure 12. Comparison of the soil thermal conductivity inside (from thermal conductivity sensor)
 490 and outside (from Fourier's analysis) the borehole array in Test 1

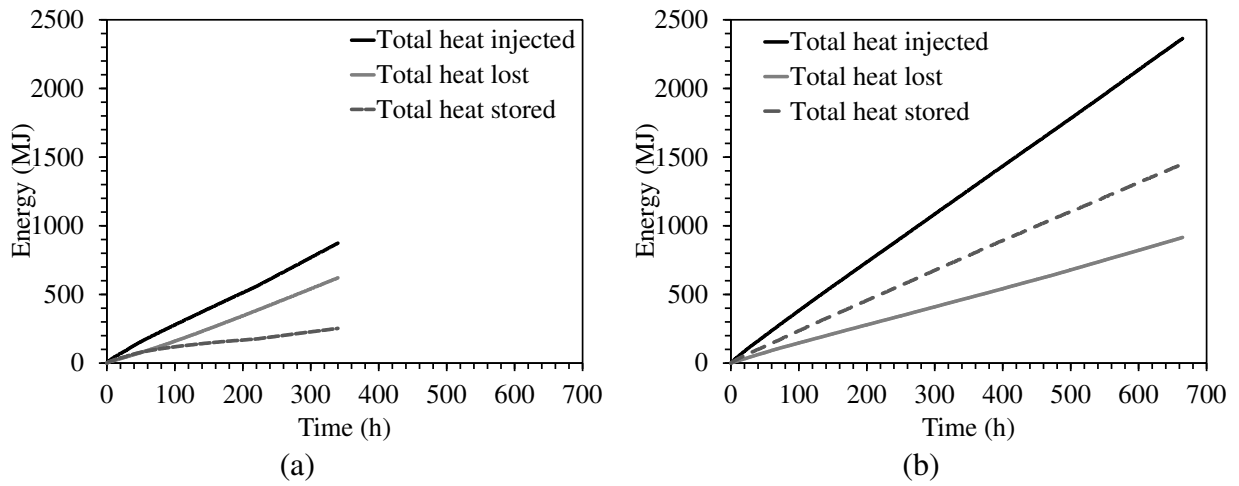


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492 Figure 13. Degree of saturation as a function of borehole heat exchanger spacing in Tests 1 and 2



493 Figure 14. Heat transfer rates: (a) Test 1; (b) Test 2



494 Figure 15. Evaluation of the energy balance: (a) Test 1; (b) Test 2