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Investigating Temperature Effects on Both Aerobic and Anaerobic Batch Growth of E.coli

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Publication Date

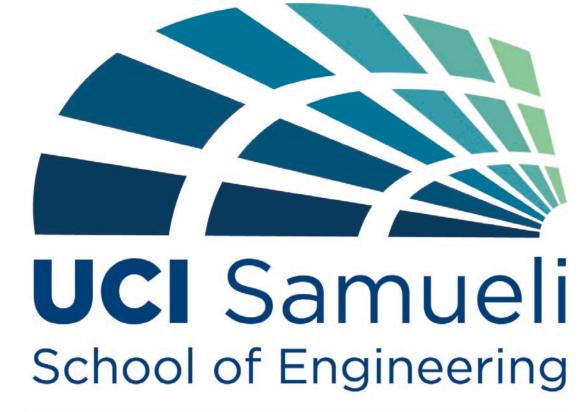
2022-03-21

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Investigating Temperature Effects on Both Aerobic and Anaerobic Batch Growth of E.coli



Blue Team 11

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University of California, Irvine

Experiment Overview

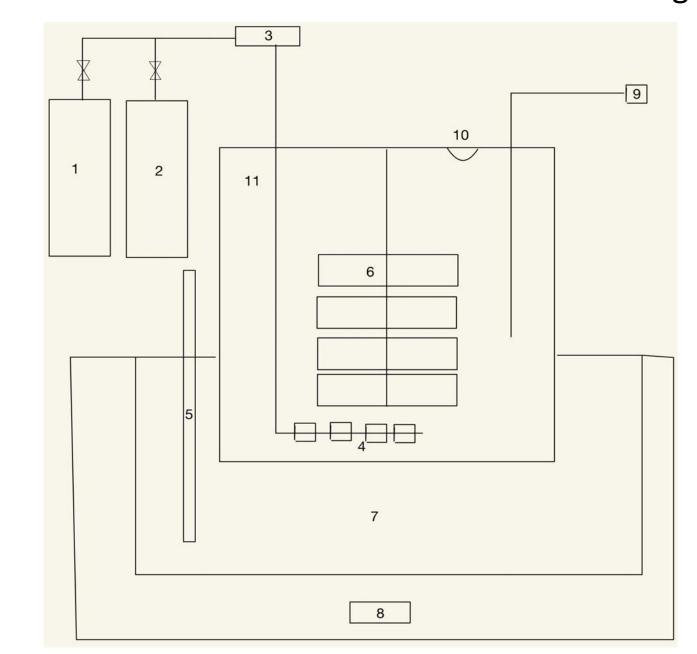
Technology Bioreactors are vessels that host

reactions involving living organisms. They also allow for mass production processes.



Objectives

Additionally, investigate



Applications

Climbing diabetic's demand for insulin introduced two new alternate methods of administration: inhalation and oral route which require a much higher dose since they do not enter the blood stream directly. Since insulin is a protein, it requires a host organism to produce it. The main hosts for human insulin has been predominantly E.coli and Saccharomyces cerevisiae. Mass production of insulin is needed to accommodate increasing diabetics' demands. Thus, insulin producing E.coli is best cultivated in bioreactors.

Hypotheses

Study the differences between aerobic The best temperature for E.coli growth is 37 °C as they and anaerobic cell growth of E.coli. exist naturally at body temperature in the intestines of optimal humans and animals. Therefore, as temperature temperature conditions by testing above deviates from 37 °C, growth rates and doubling times and below the optimal temperature, 37 will deteriorate. Aerobic conditions will demonstrate better growth rates and lower doubling times since it can extract more energy from its environment and grow faster.

- 1. Air Tank (Aerobic)
- 2. Nitrogen Tank (Anaerobic)
- 3. Pressure meter (25 PSI)
- 4. Aerator (2 SCFM)
- 5. Thermometer
- 6. Stirrer (290 RPM)
- 7. Water bath
- 8. Temperature control
- 9. Sample collecting valve 10.Inlet for LB broth and E.coli feed
- 11.Bioreactor

Theory

$$substrates + cells \rightarrow$$

$$extracellular\ products + more$$

$$cells$$

$$\Sigma S + X \rightarrow \Sigma P + nX$$

$$\mu_R \equiv \frac{1}{N} \frac{dN}{dt}$$

 μ_R : net replication rate (h^{-1}) N: Cell number Concentration

$$\frac{dN}{dt} = \mu RN, \quad N = N0 \text{ at } t = 0$$

$$\ln\left(\frac{N}{N_0}\right) = \mu_R t \text{ or } N = N_0 \exp(\mu_R t)$$

-50

Time (min)

$$\tau d = \frac{ln2}{\mu_R}$$

τd : Doubling time

Summary of Trials and Procedure

| (1) Aerobic, 30°C | (4) Anaerobic, 30°C |
|-------------------|---------------------|
| (2) Aerobic, 37°C | (5) Anaerobic, 37°C |
| (3) Aerobic, 45°C | (6) Anaerobic, 45°C |

Fill bioreactor with 1.25 L of broth. Heat water bath to desired temperature. Turn on stirrer to 290 rpm. Introduce gas set at 2 SCFH and 25 psi. Add 125 mL seed culture to reactor to begin experiment. Sample 5 mL every 10 minutes starting at t=0. Blank spectrophotometer with LB medium. Transfer 3 mL of sample to cuvette and obtain OD measurements as each experiment progresses. Rinse and repeat for different temperatures and whether aerobic or anaerobic.

Results

Aerobic Data • 30 C • 37 C • 45 C [1/h] 0.894 46.5 0.402 103.5 • • • • • •

Time [min] Growth Phases: Experimental vs Literature 0.8 0.7 0.6 0.4-0.5 0.4 0.4 0.3 0.2 0.1 Time (hr) [2]

Discussion

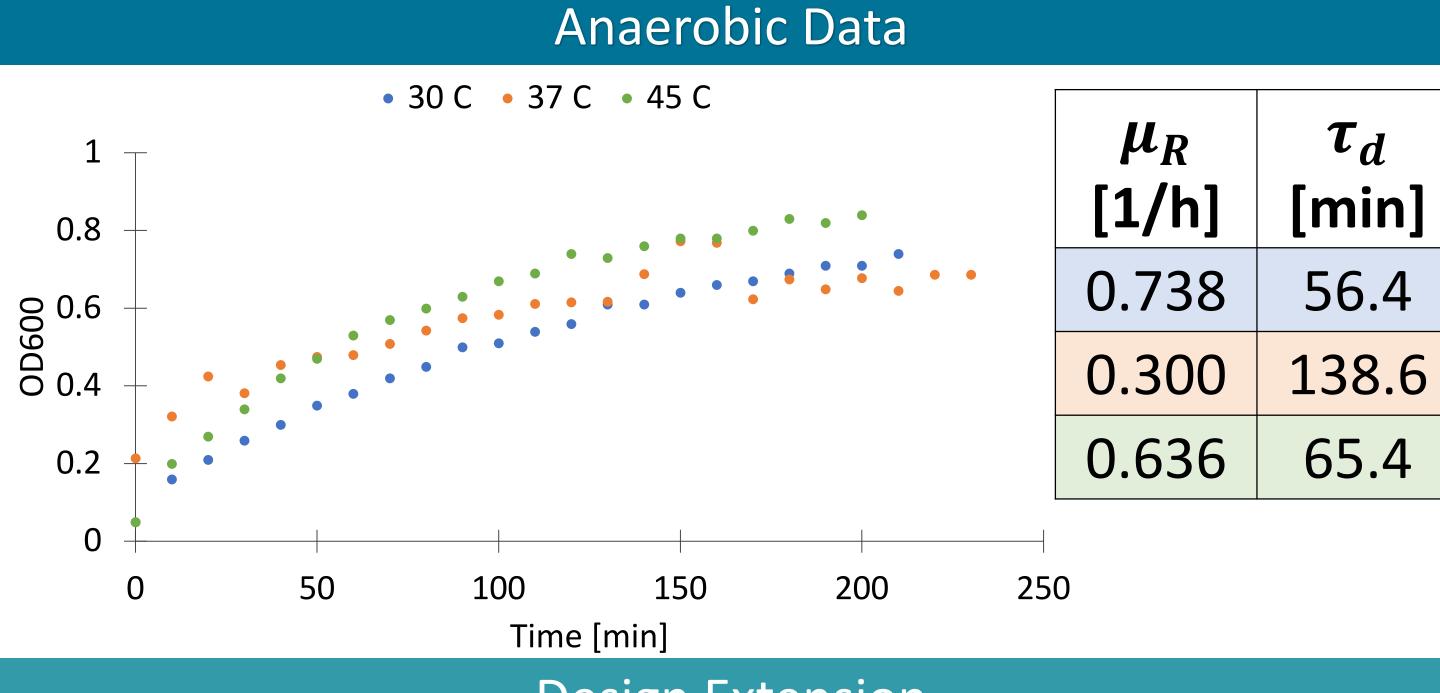
The basis of growth rate and doubling time values hinges on choosing when exponential growth phase occurs. Considering numerous published experiments were conducted over long periods of time, sometimes days, there is no solid basis for deciding whether these trials have reached exponential growth phase at all; one can argue that many of these experiments only reached an extended lag phase. Ultimately, the results obtained do not disprove the hypotheses. In order to make these claims, a single experiment must be run for the entire lifetime of a cell culture in order to rationally identify the exponential growth phase of each experiment.

Conclusion

Both hypothesis were not proven right or wrong. The results obtained suggests that growth rate/doubling time improves at lower temperatures; however, the reliability of these data sets need further investigation to make definitive conclusions about optimal growth conditions. Furthermore, future work includes longer reruns of aerobic and anaerobic experiments at 30 C and 37 C, respectively. Additionally need to verify cell number density with cell mass concentration by purifying cells and obtaining reliable dry cell masses for every sample taken at different conditions.

Acknowledgements

We would like to thank Professor Daniel Knight, Mr. Steve, and the chemical engineering class of 2022!



Design Extension

How many batch bioreactors are needed to satisfy the demand of Insulin per day in Irvine?

Design Constraints:

| Diabetic Population in Irvine [2] | 37,096 |
|-----------------------------------|------------------------|
| Insulin Consumption [4] | 2.45 mg / person / day |
| Insulin Demand | 90.9 g/day |

Assumptions:

| Conditions | Aerobic @ 37°C |
|-------------------------------------|------------------------------------|
| Conversion Factor [5] | $2.4*10^9$ cells / mL / unit OD600 |
| Cell Dry Weight [1] | $3 * 10^{-13}$ g / cell |
| Bioreactor Volume | 1000 L (90 % Capacity) |
| # of Bioreactors | 8 (parallel) |
| Lysogeny Broth: Seed Culture | 873:27 |
| Trials per Reactor | 4 / day |
| Delta OD (37 C aerobic) | 0.600 |
| Time per trial | 240 min |

Design Approach:

| Time of Four Trials | 16 hours |
|-----------------------|------------------------|
| Time for Disinfecting | 6 hours |
| Total Time | 22 operation hours/day |

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