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HTO and selenate diffusion through compacted Na-, Na–Ca-, and Ca-montmorillonite

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### Publication Date

2024-09-01

### DOI

10.1016/j.apgeochem.2024.106090

### Supplemental Material

<https://escholarship.org/uc/item/1zt6x3mz#supplemental>

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1     **HTO and Selenate Diffusion Through Compacted Na-, Na-**  
2                     **Ca-, and Ca-Montmorillonite**

3

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11

## 12 Abstract

13 Radionuclide transport in smectite clay barrier systems used for nuclear waste disposal is controlled by  
14 diffusion, with adsorption significantly retarding transport rates. While a relatively minor component of  
15 spent nuclear fuel,  $^{79}\text{Se}$  is a major driver of the safety case for spent fuel disposal due to its long half-life  
16 ( $3.3 \times 10^5$  yr) and its low adsorption to clay ( $K_D < 10$  L/kg), thus a thorough understanding of Se diffusion  
17 through clay is critical for understanding the long-term safety of spent fuel disposal systems. Through-  
18 diffusion experiments with tritiated water (HTO, conservative tracer) and Se(VI) were conducted with a  
19 well-characterized, purified montmorillonite source clay (SWy-2) under a constant ionic strength (0.1 M)  
20 and three different electrolyte compositions:  $\text{Na}^+$ ,  $\text{Ca}^{2+}$ , and a  $\text{Na}^+$ - $\text{Ca}^{2+}$  mixture at pH 6.5 in order to  
21 probe the effects of electrolyte composition and interlayer cation composition on clay microstructure,  
22 Se(VI) aqueous speciation, and ultimately diffusion. The results were modeled using a reactive transport  
23 modeling approach to determine values of porosity ( $\epsilon$ ),  $D_e$  (effective diffusion coefficient), and  $K_D$   
24 (distribution coefficient for adsorption). HTO diffusive flux was higher in Ca-montmorillonite ( $D_e = 1.68 \times$   
25  $10^{-10} \text{ m}^2 \text{ s}^{-1}$ ) compared to Na-montmorillonite ( $D_e = 7.83 \times 10^{-11} \text{ m}^2 \text{ s}^{-1}$ ). This increase in flux is likely due  
26 to a greater degree of clay layer stacking in the presence of  $\text{Ca}^{2+}$  compared to  $\text{Na}^+$ , which leads to larger  
27 inter-particle pores. Overall, the Se(VI) flux was much lower than the HTO flux due to anion exclusion,  
28 with Se(VI) flux following the order Ca ( $D_e = 1.03 \times 10^{-11} \text{ m}^2 \text{ s}^{-1}$ ) > Na-Ca ( $D_e = 2.12 \times 10^{-12} \text{ m}^2 \text{ s}^{-1}$ ) > Na  
29 ( $D_e = 1.28 \times 10^{-12} \text{ m}^2 \text{ s}^{-1}$ ). These differences in Se(VI) flux are due to a combination of factors, including  
30 (1) larger accessible porosity in Ca-montmorillonite due to clay layer stacking and smaller electrostatic  
31 effects compared to Na-montmorillonite, (2) larger accessible porosity for neutral-charge  $\text{CaSeO}_4$  species  
32 which makes up 32% of aqueous Se(VI) in the pure Ca system, and (3) possibly higher Se(VI) adsorption  
33 for Ca-montmorillonite. Through a combination of experimental and modeling work, this study highlights  
34 the compounding effects that electrolyte and counterion compositions can have on radionuclide transport  
35 through clay. Diffusion models that neglect these effects are not transferable from laboratory  
36 experimental conditions to *in situ* repository conditions.

37

## 38 Keywords

39 Selenium diffusion; radioactive waste; interlayer cation; engineered barriers; anion exclusion

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41

## 42 1. Introduction

43 Smectite clays, 2:1 layer-type phyllosilicate minerals, are the primary clay minerals found in  
44 bentonite and an important component of engineered barrier systems used for geologic storage of  
45 radioactive waste. Long-term nuclear waste disposal repositories must be capable of isolating  
46 radioactive waste over the time scales necessary for the decay of long-lived radioactive isotopes  
47 ( $> 10^6$  years). Smectite clays are good barriers for radioactive waste due to their swelling  
48 capacity, ability to seal cracks, low hydraulic conductivity, and their high adsorption capacity for  
49 radionuclides. Montmorillonite is a common smectite mineral which has been widely studied. It  
50 has a large specific surface area ( $\sim 750 \text{ m}^2/\text{g}$ ), cation exchange capacity ( $\sim 1 \text{ mol}_c/\text{kg}$ ), and  
51 strongly-sorbing surface complexation sites on clay edge surfaces.

52 Natural smectites contain interlayer cations, including primarily  $\text{Na}^+$ ,  $\text{Ca}^{2+}$ , and  $\text{Mg}^{2+}$ , which  
53 balance the negative permanent charge arising from isomorphic substitution in the phyllosilicate  
54 structure. The interlayer cation composition of smectite clays, including montmorillonite, affects  
55 the hydration and swelling properties of the clays (Bleam, 1990; Honorio et al., 2017; Laird and  
56 Shang, 1997; Salles et al., 2013; Subramanian and Nielsen Lammers, 2022; Teich-McGoldrick et  
57 al., 2015). For example, the presence of  $\text{Na}^+$  in the interlayer leads to a higher degree of swelling  
58 compared to  $\text{Ca}^{2+}$  due to differences in the sizes and hydration energies of the cations. Natural  
59 smectites can have a wide range of interlayer cation compositions; Missana et al. (2018) studied  
60 bentonites currently under investigation for use in nuclear waste repositories and found  $\text{Na}^+$   
61 comprised  $<1$  to 90% of the interlayer cation composition, with  $\text{Ca}^{2+}$  and  $\text{Mg}^{2+}$  making up  
62 the bulk of the remainder. Groundwater intrusion into bentonite barriers can also alter the  
63 interlayer cation composition through cation exchange.

64 In compacted clay, solute transport is controlled by diffusion, and adsorption of solutes to the  
65 clay can significantly retard transport. While uranium is the primary constituent of radioactive  
66 waste, selenium ( $^{79}\text{Se}$ ) is a major driver of the safety case for nuclear waste disposal due to its  
67 long half-life ( $3.3 \times 10^5$  yr) and presence as relatively mobile anionic species under a range of  
68 chemical conditions (e.g.,  $\text{HSe}^-$ ,  $\text{SeO}_3^{2-}$ ,  $\text{SeO}_4^{2-}$ ). Se redox chemistry is complex, with oxidation  
69 states ranging from -II to +VI over environmentally relevant conditions. While Se(-II) and Se(0)  
70 are relatively immobile due to the formation of low solubility precipitates, Se(IV) and Se(VI)  
71 exist as the oxyanions selenite ( $\text{SeO}_3^{2-}$ ) and selenate ( $\text{SeO}_4^{2-}$ ) and are highly mobile in water due

72 to their high solubility. During deep geologic disposal of nuclear waste, the near field  
73 environment is characterized by a relatively short oxic period, followed by anoxic conditions.  
74 However, there is significant uncertainty and range in the Eh values expected, which will depend  
75 on numerous factors including the host rock type, bentonite composition, and waste canister  
76 corrosion. This makes it difficult to predict the speciation of Se in engineered barriers, however  
77 selenite and selenate are considered to be the dominant Se aqueous species released during  
78 oxidation of spent nuclear fuel (Ma et al, 2019; Chen et al., 1999). Se adsorption to clay minerals  
79 is quite low compared to other important radionuclides such as U.  $K_D$  values for selenite  
80 adsorption to smectite are in the range of 1-10 L/kg (Missana et al., 2009; Montavon et al., 2009)  
81 compared to values up to  $10^4$  for U(VI) (Tournassat et al., 2018). Selenite and selenate  
82 adsorption to the clay minerals kaolinite and Ca-montmorillonite were studied by Bar-Yosef and  
83 Meek (1987) over the pH range 4-8. Both selenite and selenate adsorption decreased with  
84 increasing pH, with very low or negligible adsorption above pH 8. Selenate adsorption to  
85 kaolinite was lower than selenite adsorption (Bar-Yosef and Meek, 1987).

86 Selenite diffusion through bentonite has been investigated in several studies (García-Gutiérrez et  
87 al., 2001; Idemitsu et al., 2016; Wang et al., 2016; Wu et al., 2017). Idemitsu et al. (2016)  
88 measured apparent diffusion coefficient ( $D_a$ ) values of  $2.5 \times 10^{-11}$  to  $1.9 \times 10^{-13}$  m<sup>2</sup>/s over a range  
89 of dry bulk densities (0.8-1.6 kg/L), ionic strengths (0.01-1.0 M NaCl), and temperatures (10-  
90 55°C) for purified bentonite consisting of 99% montmorillonite. Measured  $D_a$  values for bulk  
91 bentonite (*i.e.*, with lower smectite content) under similar conditions are 1-2 orders of magnitude  
92 higher (Sato et al., 1995; Wu et al., 2014). Due to the lower adsorption of selenate compared to  
93 selenite, selenate  $D_a$  values are expected to be even higher than observed for selenite, although  
94 we could find no studies on selenate diffusion through bentonite in the literature.

95 In this paper, we present experimental and modeling results from tritiated water (HTO) and  
96 Se(VI) through-diffusion experiments using a well-characterized, purified montmorillonite  
97 source clay (SWy-2) with different interlayer cation compositions ( $\text{Na}^+$  and  $\text{Ca}^{2+}$ ). Previous  
98 studies have observed higher diffusive flux of HTO (González Sánchez et al., 2008) and  $\text{ReO}_4^-$   
99 (Wu et al., 2018) through Ca-montmorillonite compared to Na-montmorillonite. Selenate, with a  
100 charge of -2 and minimal adsorption, provides an opportunity to further probe anion diffusion  
101 (*i.e.*, for divalent species) in Na and Ca-montmorillonite systems and provide direct information

102 on  $^{79}\text{Se}$  transport through clay barriers. Experiments were conducted under a single ionic strength  
103 (0.1 M) and three different electrolyte compositions representing pure  $\text{Na}^+$ , pure  $\text{Ca}^{2+}$ , and a  $\text{Na}^+$ -  
104  $\text{Ca}^{2+}$  mixture in order to probe the effects of electrolyte composition and interlayer cation  
105 composition on clay microstructure,  $\text{Se(VI)}$  aqueous speciation, and ultimately diffusion.

## 106 **2. Materials and Methods**

### 107 **2.1 Clay Samples**

108 Selenium diffusion experiments were conducted using a well-characterized montmorillonite  
109 source clay (SWy-2) obtained from the Clay Minerals Society. The montmorillonite was purified  
110 in order to remove minor impurities (quartz, feldspars, and calcite). The purification procedure  
111 was adapted from Tinnacher et al. (2016). The procedure included the following major steps: (1)  
112 dialysis against sodium acetate at pH 5 for carbonate mineral dissolution, (2) dialysis against  
113  $\text{NaCl}$  to remove acetate and complete  $\text{Na}$ -saturation, (3) dialysis against water to remove excess  
114 salts, and (4) centrifugation to remove quartz and feldspar particles greater than  $2\ \mu\text{m}$ .  
115 Montmorillonite (50 g) was suspended in 1 L of 1 M sodium acetate solution buffered at pH 5  
116 with acetic acid, placed into pre-rinsed dialysis tubing (SpectraPor7, 8 kDa), and dialyzed against  
117 acetate buffer for 1 week, changing dialysis solution daily. The acetate buffer dialysis solution  
118 was then replaced with 1 M  $\text{NaCl}$  (dialyzed for 3 days), then with MilliQ water (dialyzed for two  
119 weeks), again changing dialysis solution daily. The clay suspensions were then transferred into  
120 plastic bottles and diluted and dispersed in MilliQ water to reach a clay concentration of  
121 approximately 15 g/L, and centrifuged at  $1000 \times g$  for 7 minutes. This centrifugation speed and  
122 time was deemed sufficient to remove all particles  $> 2\ \mu\text{m}$  as calculated from Stoke's Law. The  
123 replicate  $< 2\ \mu\text{m}$  clay fractions were then combined into a glass beaker, dried at  $60^\circ\text{C}$  and ground  
124 in ball mill with tungsten carbide balls.

125 In order to maintain constant aqueous porewater chemical conditions and interlayer cation  
126 composition during the diffusion experiments, purified montmorillonite was pre-equilibrated  
127 with the appropriate background electrolyte prior to packing in diffusion cells. 2 g of purified  
128 clay was suspended in 100 mL of electrolyte solution and the clay suspension was transferred to  
129 pre-rinsed dialysis tubing (SpectraPor7, 8 kDa). Clay samples were dialyzed against 1 L of  
130 background electrolyte for 1.5 weeks, changing dialysis solution at least 3 times and manually

131 adjusting pH daily. Once the pH remained between 6.45-6.55 within 24 hours, the background  
132 electrolyte solution was replaced with MilliQ water, and dialysis was continued for 5 days,  
133 changing the MilliQ water daily. After dialysis was complete, the clay suspension was  
134 transferred to 40 mL polycarbonate centrifuge tubes and centrifuged at  $39\,000 \times g$  for 20  
135 minutes. The supernatant was removed and the clay was dried at  $60^{\circ}\text{C}$  and ground in ball mill  
136 with tungsten carbide balls and stored at room temperature prior to packing the cells. At the time  
137 of packing, a subsample of each clay was dried at  $150^{\circ}\text{C}$  to determine the moisture content.

138 The cation exchange capacity (CEC) and exchangeable cation composition was measured using  
139 the hexamine cobalt(III) chloride method (Hadi et al., 2013). Triplicate samples of 50 mg dry  
140 clay were weighed into centrifuge tubes and 10 mL of 15 mM hexamine cobalt(III) chloride  
141 solution was added. Samples were mixed on an end-over-end sample rotator for 2 hours, then  
142 centrifuged at  $39,000 \times g$ . Solution samples were analyzed for major cations (Ca, Mg, K, and Na)  
143 by ICP-MS and the cation exchange capacity was calculated from the sum of cations released  
144 from the hexamine cobalt solution corrected for any soluble salts released during the water  
145 extracts. CEC is expressed as mmol/g (mmol of charge per gram dry clay) and cation  
146 composition is expressed as the charge fraction for each cation.

## 147 **2.2 Characterization of Filters**

148 In order to accurately model diffusion through clay, the diffusion properties of the filters used in  
149 the diffusion cell must be explicitly considered. Therefore, diffusive properties of the filters were  
150 measured using custom-built filter diffusion cells based on a modified design of Aldaba et al.  
151 (2014). The cells consisted of two polycarbonate reservoirs with a filter connecting the two  
152 reservoirs. The filter is held in place with O-rings on each side and the two reservoirs are held  
153 together in a base plate. A one-hole silicone stopper was fitted in the top of each reservoir with a  
154 conductivity probe inserted through the hole to monitor solute diffusion. In addition, a small  
155 needle (22 G) was inserted through each stopper to allow venting and pressure equalization with  
156 the atmosphere. Without this venting needle, a small pressure differential can develop between  
157 the two cells due to slight differences in stopper insertion, causing water to flow between the two  
158 cells. Filters were made of PEEK with a PCTFE ring (IDEX # OC-815). The filters had an  
159 overall diameter of 0.95 cm, filter diameter of 0.74 cm, thickness of 0.16 cm,  $5\ \mu\text{m}$  pore size, and  
160 porosity of 0.26 according to the manufacturer.

161 The diffusion of sodium chloride was measured using this experimental setup in five replicate  
162 experiments. The filter was soaked in MilliQ water to remove air bubbles. 45 mL of MilliQ  
163 water was then added to each reservoir and allowed to equilibrate for at least 3 h. The low- and  
164 high-concentration reservoirs were then spiked with 5 mL MilliQ water or 1 M NaCl,  
165 respectively to start the experiment. This resulted in a concentration of 0.1 M NaCl in the high-  
166 concentration reservoir. Both reservoirs were stirred constantly throughout the experiment. The  
167 electrical conductivity of each reservoir was monitored with a conductivity probe and  
168 automatically logged every 30 min. The conductivity probes were calibrated with known  
169 concentrations of NaCl. During one experiment, 0.125 mL subsamples from each reservoir were  
170 collected and analyzed for Na by ICP-MS in order to verify that the conductivity measurements  
171 were accurately representing Na concentration. The measured Na concentrations agreed within  
172 3% for the two methods.

### 173 **2.3 Diffusion coefficient of filters**

174 The cumulative mass (mol) of NaCl in the low-concentration reservoir was plotted over time (s).  
175 This results in a pseudo-linear breakthrough curve for the first ~100 h during which the  
176 concentration of NaCl in the high-concentration reservoir did not change significantly. The curve  
177 was fit with a linear regression and the effective diffusion coefficient ( $D_e$ ) was determined using  
178 the slope ( $a$ ) from the equation given by

$$D_e = \frac{a L}{A C_0} \quad \text{Equation 1}$$

179 where  $L$  is the thickness of the filter,  $A$  is the cross-sectional area of the filter, and  $C_0$  is the initial  
180 concentration in the high-concentration reservoir.

181 Effective diffusion coefficients measured for filters depend on the characteristics of both the  
182 filter and the solute, according to:

$$D_e = \frac{\varepsilon}{G} D_0 = \tau \varepsilon D_0 \quad \text{Equation 2}$$

183

184 where  $D_0$  is the bulk diffusion coefficient of a solute in water, while  $G$  (or  $1/\tau$ ) is a geometric  
185 factor that accounts for the geometry of the filter pore network.  $\tau$  is often referred to as the



186 tortuosity although it lumps together the true tortuosity and the constrictivity of the material. In  
187 this filter diffusion experiment  $D_0$  refers to the co-diffusion of  $\text{Na}^+$  and  $\text{Cl}^-$  ( $1.61 \times 10^{-9} \text{ m}^2\text{s}^{-1}$ ),  
188 which is calculated from the diffusion coefficients of  $\text{Na}^+$  and  $\text{Cl}^-$ , ( $1.33 \times 10^{-9}$  and  $2.03 \times 10^{-9}$ ,  
189 respectively at  $25^\circ\text{C}$ ; Li and Gregory (1974) according to Cussler (2009) (see details in the SI).  
190 Diffusion coefficients of aqueous species were calculated using the filter parameters and the  
191 known  $D_0$  values for those aqueous species.  $D_0$  values at  $25^\circ\text{C}$  for HTO and  $\text{SeO}_4^{2-}$  were taken at  
192  $2.30 \times 10^{-9} \text{ m}^2 \text{ s}^{-1}$  and  $9.46 \times 10^{-10} \text{ m}^2 \text{ s}^{-1}$  respectively.

## 193 **2.4 Diffusion Experiments**

194 Through-diffusion experiments were conducted with purified, pre-equilibrated montmorillonite  
195 at a dry bulk density ( $\rho_d$ ) of approximately  $1.3 \text{ kg L}^{-1}$  corresponding to a total porosity ( $\varepsilon$ ) of  
196 approximately 0.5 according to:

$$\varepsilon = 1 - \frac{\rho_d}{\rho_g} \quad \text{Equation 3}$$

197

198 where  $\rho_g$  is the crystal density of clay mineral layers (*i.e.*, grain density). For montmorillonite,  $\rho_g$   
199 is approximately  $2.84 \text{ kg L}^{-1}$  (Bourg et al., 2006; Tournassat and Appelo, 2011). The dry bulk  
200 density ( $\rho_d$ ) is expressed in terms of the  $150^\circ\text{C}$  oven dry weight of clay. There were some small  
201 differences in the calculated bulk density and porosity for the three diffusion cells because of  
202 differences in the moisture content of the clay at the time of packing (Table 2.).

203 The diffusion cells used for experiments are based on the design of (Van Loon et al., 2003), with  
204 dimensions adjusted to accommodate smaller samples (Figure S1). The clay plug inside the  
205 diffusion cells had a diameter of 9.5 mm and a length of 5 mm. Cells were machined in-house  
206 using PEEK (polyether ether ketone) plastic at Lawrence Berkeley National Laboratory.

207 Experiments were conducted under a single ionic strength (0.1 M) and three different electrolyte  
208 compositions: 0.1 M NaCl, 0.033 M  $\text{CaCl}_2$ , and 0.085 M NaCl + 0.005 M  $\text{CaCl}_2$ , representing  
209 pure  $\text{Na}^+$ , pure  $\text{Ca}^{2+}$ , and a  $\text{Na}^+$ - $\text{Ca}^{2+}$  mixture, respectively. All experiments were performed at  
210 room temperature ( $23^\circ\text{C}$ ) at pH 6.5. The pre-equilibrated dry clay samples were weighed into  
211 PEEK diffusion cells and compacted using a custom PEEK packing rod.

212 The diffusion experiments were conducted in three phases: (1) saturation, (2) tritiated water  
213 (HTO) diffusion, and (3) Se(VI) diffusion. The clay was saturated by circulating 200 mL of  
214 background electrolyte at both ends of the cell at approximately 1 mL/min using a peristaltic  
215 pump for 40-42 days. After the saturation period, the HTO through-diffusion phase was started  
216 by replacing the background electrolyte solutions with a high HTO reservoir containing  
217 background electrolyte spiked with 1110 Bq mL<sup>-1</sup> HTO (200 mL) at one end and a low HTO  
218 reservoir containing only background electrolyte (20 mL) at the other end. The high-  
219 concentration reservoir was sampled at the beginning and the end of the HTO diffusion  
220 experiment and did not change significantly over that time period. The low HTO reservoir was  
221 changed at time intervals of 3-36 h, and the HTO concentration was measured in the low  
222 reservoir samples by liquid scintillation counting. An in-house-built autosampler using a 3D  
223 printer (Crealty Ender 3Pro) as the base was used to change the low reservoir samples at regular  
224 time intervals. The HTO concentration in the low reservoir never exceeded 0.5% of the  
225 concentration in the high reservoir. The HTO diffusion was continued for 16 days. After this  
226 period, the high-concentration reservoir was replaced with a Se(VI)-spiked solution containing  
227 1.0 mM sodium selenate in the background electrolyte with a total volume of 190 mL, marking  
228 the start of the Se(VI) diffusion experiment. The low-concentration reservoirs containing only  
229 background electrolyte (5-10 mL) were changed at time intervals of 12-48 h for the first 44 days,  
230 then 48-170 h for the remaining 33 days, and Se concentrations were measured by ICP-MS. Se  
231 concentrations in the low reservoir never exceeded 1% of the concentration in the high reservoir.  
232 Subsamples of the high-concentration Se(VI) reservoir were collected at the beginning and end  
233 of the experiment and did not change significantly over the experiment.

234 At the end of the Se(VI) diffusion period, the diffusion cells were disassembled and the clay plug  
235 was extruded using the PEEK packing rod and sliced into thin slices. The thickness of the clay  
236 slices was measured using a digital caliper with a precision of 0.1 mm. Clay slices ranged in  
237 thickness from 0.3 to 0.9 mm. The clay slices were placed into 20 mL glass scintillation vials and  
238 dried at 150°C for 24 hours. The dried clay was extracted with 5 mL of 0.5 M trace metal grade  
239 hydrochloric acid for 3 days, then centrifuged at 39 000 × g for 20 min and filtered through a  
240 0.45 μm PVDF syringe filter. Selenium concentrations were measured in the acid extracts by  
241 ICP-MS. Se concentrations in the clay profiles are expressed in mmol Se per liter of total  
242 porosity ( $C_{\text{Se\_pore}}$ ), calculated using the following equation:

$$C_{Se\_pore} = \frac{1000 \times C_{Se\_solid} \times \rho_d}{\varepsilon} \quad \text{Equation 4}$$

243

244 Where  $C_{Se\_solid}$  is the concentration of Se extracted per gram of dry clay (in  $\text{mmol g}^{-1}$ ).

## 245 **2.5 Analytical Techniques**

246 Samples were analyzed for Se by ICP-MS (Perkin-Elmer Elan DRC II) after acidification and  
 247 dilution with ultrapure (ultrapure grade) 0.15 M nitric acid and internal standard addition. Selenium  
 248 was measured using oxygen as the cell gas in DRC mode and using Rh as an internal standard.  
 249 Spike recoveries with known concentrations of Se were run every 5 samples, and recoveries  
 250 ranged from 0.80-1.25. Independent QC samples were run every 10 samples, with recoveries  
 251 ranging from 0.9-1.1. HTO samples were analyzed using liquid scintillation counting (Perkin-  
 252 Elmer Liquid Scintillation Analyzer Tri-Carb 2900TR) by mixing 4 mL of sample with 18 mL of  
 253 Ultima Gold XR liquid scintillation cocktail and counting until the relative standard deviation  
 254 was 2% or for a maximum of 90 minutes.

## 255 **2.6 Modeling Approach**

256 Normalized mass flux ( $J_N$ , in  $\text{m day}^{-1}$ ) reaching the low-concentration reservoir is most  
 257 frequently calculated in the literature using:

$$J_N = \frac{C_{low}V_{low}}{C_{high}A \cdot \Delta t} \quad \text{Equation 5}$$

258 where  $C_{low}$  is the concentration in the low-concentration reservoir,  $C_{high}$  is the concentration in  
 259 the high-concentration reservoir,  $V_{low}$  is the volume of the low-concentration reservoir (from ~5  
 260 to ~20 mL depending on the sampling event),  $A$  is the cross-sectional area of the diffusion cell  
 261 ( $0.709 \text{ cm}^2$ ), and  $\Delta t$  is the time interval since the previous sampling event. This approximation is  
 262 applicable for cases in which tracer concentration in the high reservoir does not change  
 263 significantly over the course of the experiment (i.e., tracer source is considered infinite) and the  
 264 tracer concentration in the low reservoir remains near zero (Yaroshchuk et al., 2008). However,  
 265 for modeling purposes, this representation presents some problems (discussed in detail in  
 266 Tournassat et al. (2023)), which include differences in time-integrated fluxes,  $J_N$ , compared to  
 267 instantaneous fluxes calculated with the analytical solution of the diffusion equations.  $J_N$  values

268 may also oscillate with time because of the irregular pattern of sampling events during the  
 269 experiment. A reactive transport modeling approach makes it possible to consider all  
 270 experimental features such as the above-mentioned problems, as well as varying boundary  
 271 conditions, the presence of filters, the presence of an O-ring in the filters, the replacement of the  
 272 low-concentration reservoir with time, *etc.* (Tournassat et al., 2023). In addition, a reactive  
 273 transport modeling approach allows comparison of the modeling results directly to the raw  
 274 experimental data, *i.e.* the tracer concentrations measured in each of the collected vials at all  
 275 sampling times. For these reasons, all clay sample diffusion experiments were modeled using the  
 276 reactive transport model CrunchClay (Steeffel and Tournassat, 2021; Tournassat and Steeffel,  
 277 2021; Tournassat et al., 2020). The consideration of an O-ring in the filters necessitated carrying  
 278 out the calculations with a 2D-axisymmetric geometry (Tournassat et al., 2023).

279 CrunchClay was used in combination with the CrunchEase interface (Tournassat et al., 2023) to  
 280 estimate clay diffusive properties within the framework of a classical  $\varepsilon - D_e - K_D$  modeling  
 281 approach, where  $\varepsilon$  is the diffusion porosity (-),  $D_e$  is the effective diffusion coefficient ( $\text{m}^2 \text{s}^{-1}$ ,  
 282 see Equation 2) and  $K_D$  ( $\text{L kg}^{-1}$ ) is the distribution coefficient that accounts for reversible and  
 283 linear adsorption processes. We assumed that HTO was present only in solution and that Se was  
 284 present in solution (with  $c$  = aqueous concentration) and on surfaces (with  $C_{surf}$  in  $\text{mol kg}_{\text{solid}}^{-1}$ ) so  
 285 that  $C_{tot}$  (in  $\text{mol m}_{\text{medium}}^{-3}$ ) can be expressed as:

$$C_{tot} = c\varepsilon + C_{surf}\rho_d \quad \text{Equation 6}$$

286 We assumed that the Se surface concentration  $C_{surf}$  was linearly related to the aqueous  
 287 concentration through  $C_{surf} = cK_D$  (with  $K_D$  in  $\text{m}^3_{\text{water}} \text{kg}_{\text{solid}}^{-1}$ ) and that the adsorption process  
 288 was instantaneous and reversible. Based on this assumption,

$$C_{tot} = c\varepsilon + cK_D\rho_d. \quad \text{Equation 7}$$

289 It was further assumed that the media were homogeneous. Hence  $D_e$ ,  $\varepsilon$ ,  $\rho_d$  and  $K_D$  are independent  
 290 of  $x$ , and Fick's second law of diffusion reduces to:

$$\frac{\partial c}{\partial t} = \frac{\tau\varepsilon D_0}{\varepsilon + \rho_d K_D} \frac{\partial^2 c}{\partial x^2} = \frac{D_e}{\alpha} \frac{\partial^2 c}{\partial x^2} \quad \text{Equation 8}$$

291

292 where  $\alpha$  is the rock capacity factor.

293 The dimensions of the diffusion cells are available in the Supporting Information (Figure S1).

294 The exact same dimensions were considered in our reactive transport simulations, which can be  
295 reproduced by the readers using the CrunchEase GUI made freely available on Github

296 (<https://github.com/Tournassat/CrunchEaseForAll>).

297 In the following, the agreement of the model with the experimental data is shown on the raw data  
298 (concentration measurements in vials) and the experimental time-averaged flux  $J_N$  as a function  
299 of experimental conditions is only shown for comparison.

## 300 **3. Results and Discussion**

### 301 **3.1 Filter Diffusion Properties**

302 In order to characterize the baseline performance of the reaction cell, diffusion of NaCl through  
303 PEEK filters was measured in five replicate experiments. An example plot of cumulative NaCl  
304 mass in the low reservoir over time is shown in Figure S2. There was an initial lag period,  
305 followed by a linear increase in NaCl in the low reservoir. This linear portion of the  
306 breakthrough curve was used to calculate the effective diffusion coefficient of  $\text{Na}^+$  and  $\text{Cl}^-$   
307 through the filter according to Equation 1, resulting in a measured  $D_e$  of  $6.1 \times 10^{-11} \pm 0.29 \times 10^{-11}$   
308  $\text{m}^2 \text{s}^{-1}$ .

309 Given the known values for  $\varepsilon$  and  $D_0$  (Table S1), we calculated  $G$  to be  $6.82 \pm 0.33$  ( $\tau = 0.147 \pm$   
310  $0.007$ ). The measured  $D_e$  value was lower than for stainless steel filters with a similar pore size  
311 ( $1.6 \times 10^{-10} \text{ m}^2 \text{ s}^{-1}$ ) (Aldaba et al., 2014).  $G$  and  $\varepsilon$  were slightly lower for the PEEK filters used in  
312 this experiment compared to those used by Aldaba et al. (2014), which had a smaller nominal  
313 pore size of  $1 \mu\text{m}$ .

### 314 **3.2 Clay Cation Composition**

315 The total cation exchange capacity of the clay after purification was  $0.833 \pm 0.04 \text{ mmol}_c/\text{g}$ . The  
316 cation composition for the Na, Na-Ca, and Ca exchanged clays is shown in Table 1. The cation  
317 composition is expressed as a % of charge ( $100 \times \text{mmol}_c \text{ cation per gram/CEC}$  in  $\text{mmol}_c/\text{g}$ ). The

318 Na-Ca clay contained 72% (by charge) Ca. A very small amount (1%) of exchangeable Mg was  
319 present in all three clays and no K was detected.

320 **Table 1. Exchangeable cation composition of clays expressed as a charge % of the CEC.**

Clay	Na (% charge)	Ca (% charge)	Mg (% charge)
Na	98.3 ± 0.6	0.5 ± 0.6	1.2 ± 0.0
Na-Ca	26.8 ± 0.2	72.2 ± 0.2	1.0 ± 0.0
Ca	1.6 ± 0.3	97.5 ± 0.2	0.9 ± 0.1

321

322

### 323 **3.3 Tritiated water (HTO) diffusion**

324 HTO diffusion reached a steady state after approximately 100 h, with steady-state fluxes  
325 increasing in the order Na, Na-Ca, and Ca (Figure 1). A precise estimation of the  $\tau$  and  $D_e$  values  
326 of HTO was achieved by modeling the data with the assumption that the total porosity was  
327 accessible to HTO (Figure 1 and Table 2). The influence of the variations in sampling time  
328 intervals and sample vial volumes during the experiment is almost perfectly captured by our  
329 modeling approach (raw data available in the SI), thus giving confidence in the modeled  $\tau$  and  $D_e$   
330 values.

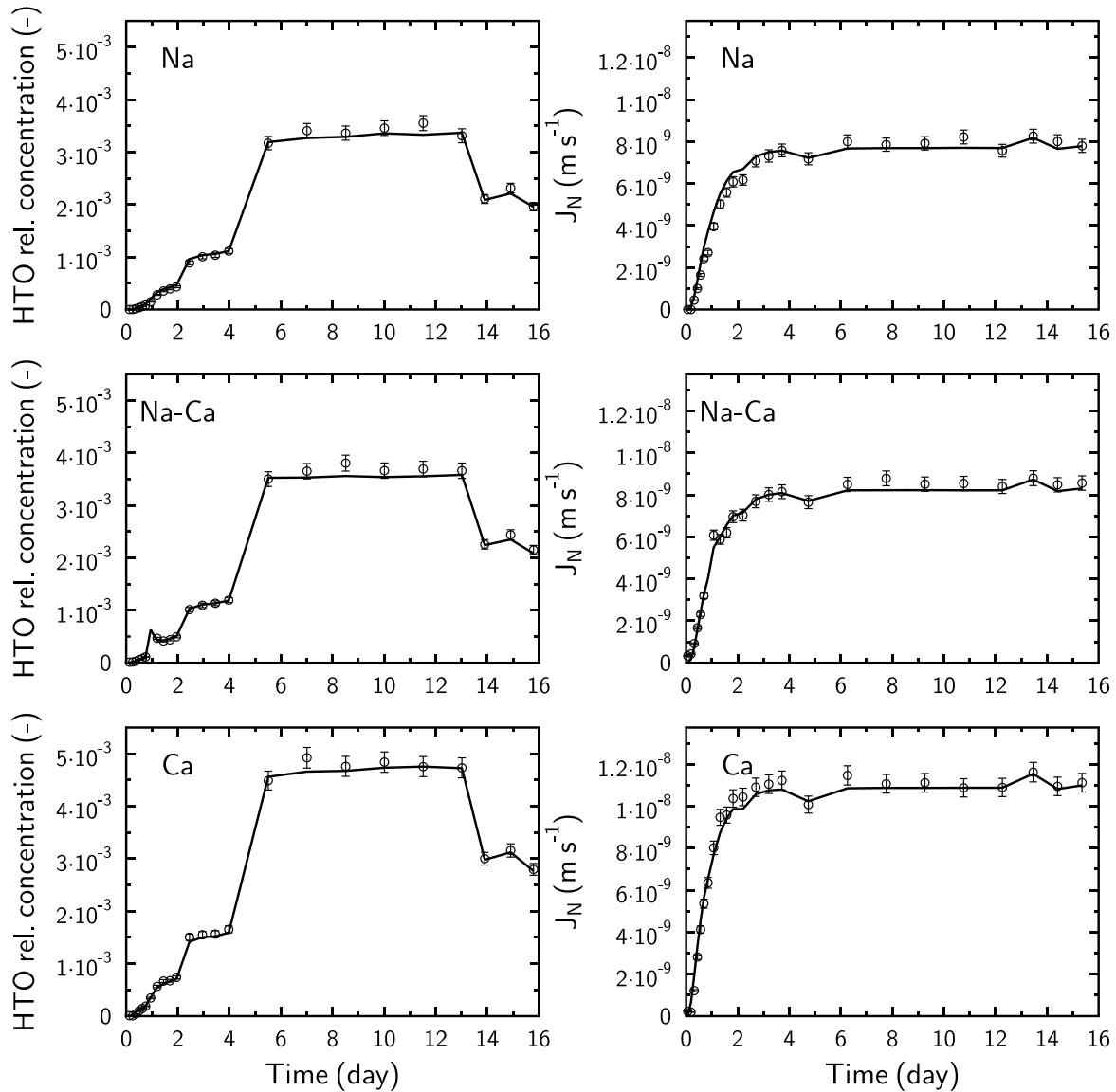
331 The small difference between the Na ( $\tau_{\text{HTO}} = 0.065$ ) and Na-Ca ( $\tau_{\text{HTO}} = 0.070$ ) cells might be  
332 attributed to small differences in cell packing ( $\rho_d = 1.35$  vs.  $\rho_d = 1.28 \text{ kg L}^{-1}$  for Na and Na-Ca  
333 cells respectively). Differences in bulk density will affect not only the total porosity, but also the  
334 sample microstructure responsible for the geometrical factor affecting diffusion processes.  
335 Archie's law relates the effective diffusion coefficient to the porosity and an empirical  
336 cementation factor,  $m$ , that captures the change of the geometrical factor as a function of porosity  
337 changes:

$$D_e = D_0 \varepsilon^m \quad \text{Equation 9}$$

338 Despite its empirical nature, Archie's law or its extended version (Van Loon and Mibus, 2015) is  
339 often able to quantitatively describe the evolution of the effective diffusion coefficient of HTO in  
340 clayey materials. The difference between the Na ( $\tau_{\text{HTO}} = 0.065$ ) and Na-Ca ( $\tau_{\text{HTO}} = 0.070$ ) cells

341 can be described by considering a cementation factor of  $m \sim 3$ , which is compatible with the  
342 cementation factors commonly reported for bentonite samples (Van Loon and Mibus, 2015).  
343 However, the difference between the Na-Ca ( $\tau_{\text{HTO}} = 0.070$ ) and Ca ( $\tau_{\text{HTO}} = 0.13$ ) cells cannot be  
344 attributed to the small difference in cell packing only. A cementation factor of  $m \sim 10$  would be  
345 necessary, which does not fall in the range of values reported for montmorillonite. A reasonable  
346 explanation of the observed difference lies in the difference of microstructure of Na- and Ca-  
347 exchanged montmorillonite samples: the presence of exchangeable Ca promotes the formation of  
348 thicker layer stacks (“tactoids”) compared to Na (Segad et al., 2012), which in turn promotes the  
349 presence of larger interparticle pores (Holmboe et al., 2012; Ohkubo et al., 2021), hence  
350 increasing the diffusivity of the material (Melkior et al., 2009; Tournassat et al., 2011;  
351 Tournassat et al., 2016).

352



353

354 **Figure 1. Left: HTO normalized concentrations in the low-concentration reservoir as a**  
 355 **function of time. Right: HTO normalized flux as a function of time. Na, Na-Ca, and Ca**  
 356 **refers to the three different salt background and clay conditioning conditions. Circles:**  
 357 **experimental data; lines: results of the  $\epsilon - D_e$  models (Table 2.). Error bars are**  
 358 **representative of the analytical error on the HTO measurements (2 standard deviations).**

359

360 **Table 2. Summary of measured diffusion cell parameters, including bulk density ( $\rho_a$ ), total**  
 361 **porosity ( $\epsilon_{tot}$ , calculated from Equation 3), along with reference model fitted parameters ( $\tau$ ,**



362  $D_e$ ,  $\alpha_{Se}$ ), assuming  $K_D = 0 \text{ L kg}^{-1}$  for both HTO and Se(VI). Note that  $\alpha_{HTO}$  is equivalent to  
 363  $\varepsilon_{HTO}$  and  $\varepsilon_{tot}$ . Uncertainties on the  $D_e$  value were estimated from model envelop curves and  
 364 experimental error bars.

Cell	$\rho_d$ ( $\text{kg L}^{-1}$ )	$\varepsilon_{tot} = \varepsilon_{HTO} = \alpha$ HTO (-)	$\tau_{HTO}$ (-)	$D_{e,HTO}$ ( $10^{-12} \text{ m}^2 \text{ s}^{-1}$ )	$\alpha_{Se} =$ $\varepsilon_{Se,max}$ (-)	$\tau_{Se,min}$ (-)	$D_{e,Se}$ ( $10^{-12} \text{ m}^2 \text{ s}^{-1}$ )
Na	1.35	0.524	0.065	$78 \pm 4$	0.0983	0.0138	$1.3 \pm 0.3$
Na-Ca	1.28	0.551	0.070	$89 \pm 4$	0.140	0.0160	$2.1 \pm 0.5$
Ca	1.24	0.562	0.13	$168 \pm 8$	0.450	0.0250	$10.6 \pm 2.3$

365

### 366 3.4 Selenate diffusion

367 The normalized flux for Se(VI) reached steady state after approximately 300 h, with the Ca-  
 368 montmorillonite showing the highest normalized flux (Figure 2). The steady-state flux of Se was  
 369 much lower than that of HTO in all three cells. Total Se concentrations in clay slices also  
 370 followed the trend  $\text{Na} < \text{Na-Ca} < \text{Ca}$  (Figure 3). Se concentrations in the clay slice closest to the  
 371 high-concentration reservoir (at  $\sim 4.5\text{-}5.0 \text{ mm}$ ) were 0.18, 0.25, and 0.77 mM for the Na, Na-Ca,  
 372 and Ca cells, respectively. The observed variations in Se concentration/flux may result from both  
 373 differences in effective porosity for Se and from changes in Se adsorption in the presence of  
 374 increasing Ca concentrations. The profiles in all three cells were linear with depth as expected  
 375 for steady-state conditions.

376 Through-diffusion data makes it possible to extract a single set of  $\alpha$ ,  $D_e$  values for each tracer in  
 377 one experiment (Crank, 1975; Van Loon et al., 2003). However, it does not provide enough  
 378 constraints to extract a single set of  $\varepsilon$ ,  $K_D$ , and  $\tau$  values and additional data and/or hypotheses are  
 379 necessary to derive these three quantities independently. In the first attempt, the  $K_D$  values for  
 380 Se(VI) were set to zero. In this condition, the fitted porosity and tortuosity values take their  
 381 maximum and minimum value respectively ( $\varepsilon_{max} = \alpha$  and  $\tau_{min}$ ; Table 2). The corresponding fitted  
 382 parameters made it possible to almost perfectly reproduce the diffusion data (Figure 2 and Figure  
 383 3).

384 In Na-montmorillonite, clay layers are negatively charged and part or all of the porosity is  
385 influenced by the presence of an electrical double layer (EDL) that forms at the surface, and in  
386 which the solution is not electroneutral (Tournassat and Steefel, 2019). Negatively charged  
387 species, including  $\text{SeO}_4^{2-}$ , are depleted in the EDL-influenced portion of the porosity because of  
388 their interaction with the negative electrostatic potential field created by the surfaces of  
389 montmorillonite. This process, often called anion-exclusion, is also responsible for a higher  
390 geometrical factor,  $G$  (or  $1/\tau$ ), for anions compared to neutral tracers such as HTO, because pore  
391 throats, which are responsible for the pore network connectivity, may partially or totally exclude  
392 anions, thus ascribing longer diffusion pathways to anions compared to neutral species.  
393 Consequently,  $\tau_{\text{Se}} \leq \tau_{\text{HTO}}$  and it is possible to define a minimum accessible porosity value for Se  
394 corresponding to  $D_{e,\text{Se}} = \tau_{\text{HTO}} \times \varepsilon_{\text{Se},\text{min}} \times D_{0,\text{Se}}$ . This minimum porosity corresponds itself to a  
395 maximum  $K_{\text{D}}$  value according to  $\alpha_{\text{Se}} = \varepsilon_{\text{Se},\text{min}} + \rho_{\text{d}} K_{\text{D},\text{max}}$  (Table 3). We note that the very low  
396  $K_{\text{D},\text{max}}$  values ( $\ll 1$ ) in Table 3 are nearly impossible to measure in batch experiments.

397 The calculated minimum value of  $\text{SeO}_4^{2-}$  accessible porosity ( $\varepsilon_{\text{Se},\text{min}} = 0.021$ ) was similar to the  
398 values reported for  $\text{Cl}^-$  in similar compacted Na-montmorillonite materials (Tournassat and  
399 Appelo, 2011).  $\text{Cl}^-$  does not adsorb on clay mineral surfaces, and thus, the difference between  
400 total porosity values and  $\text{Cl}^-$  accessible porosity values reported in the literature are truly  
401 representative of the excluded volume for monovalent anions. However, one would expect an  
402 increased exclusion for  $\text{SeO}_4^{2-}$  compared to  $\text{Cl}^-$  because of their difference in charge. This  
403 surprisingly high Se(VI) accessible porosity in the Na-montmorillonite sample may be partly  
404 explained by the presence of aqueous and exchanged  $\text{Mg}^{2+}$  which originates from a limited  
405 dissolution of the clay layers (Orucoglu et al., 2018). The formation of  $\text{MgSeO}_4$  ion pairs, which  
406 are neutral and, thus not excluded from the EDL, would then explain the lower value of Se(VI)  
407 exclusion than expected.  $\text{Mg}^{2+}$  was a minor component (1%) of exchangeable cations at the  
408 beginning of the experiment (Table 1). However, we did not measure exchangeable cations on  
409 the clay at the end of the experiment or aqueous  $\text{Mg}^{2+}$  during the diffusion experiment, therefore  
410 are unable to confirm the formation of  $\text{MgSeO}_4$  ion pairs. The lowering of Se exclusion from the  
411 EDL could also be related to an increased ion pairing in the EDL compared to bulk water  
412 conditions (Appelo et al., 2010), which in turn would increase the apparent accessible porosity of  
413 Se.

414

415 **Table 3. Summary of constraints on Se diffusion parameters in Na-, Na-Ca-, and Ca-**  
 416 **montmorillonite.  $K_{D,max}$  values are given in L kg<sup>-1</sup>.**

Cell	$\varepsilon_{Se,min}$	$K_{D,max}$	$\varepsilon_{Se,min}$ considering CaSeO <sub>4</sub> ion pair formation	$K_{D,max}$ considering CaSeO <sub>4</sub> ion pair formation
Na	0.021	0.057	-	-
Na-Ca	0.032	0.084	0.036	0.081
Ca	0.086	0.29	0.18	0.22

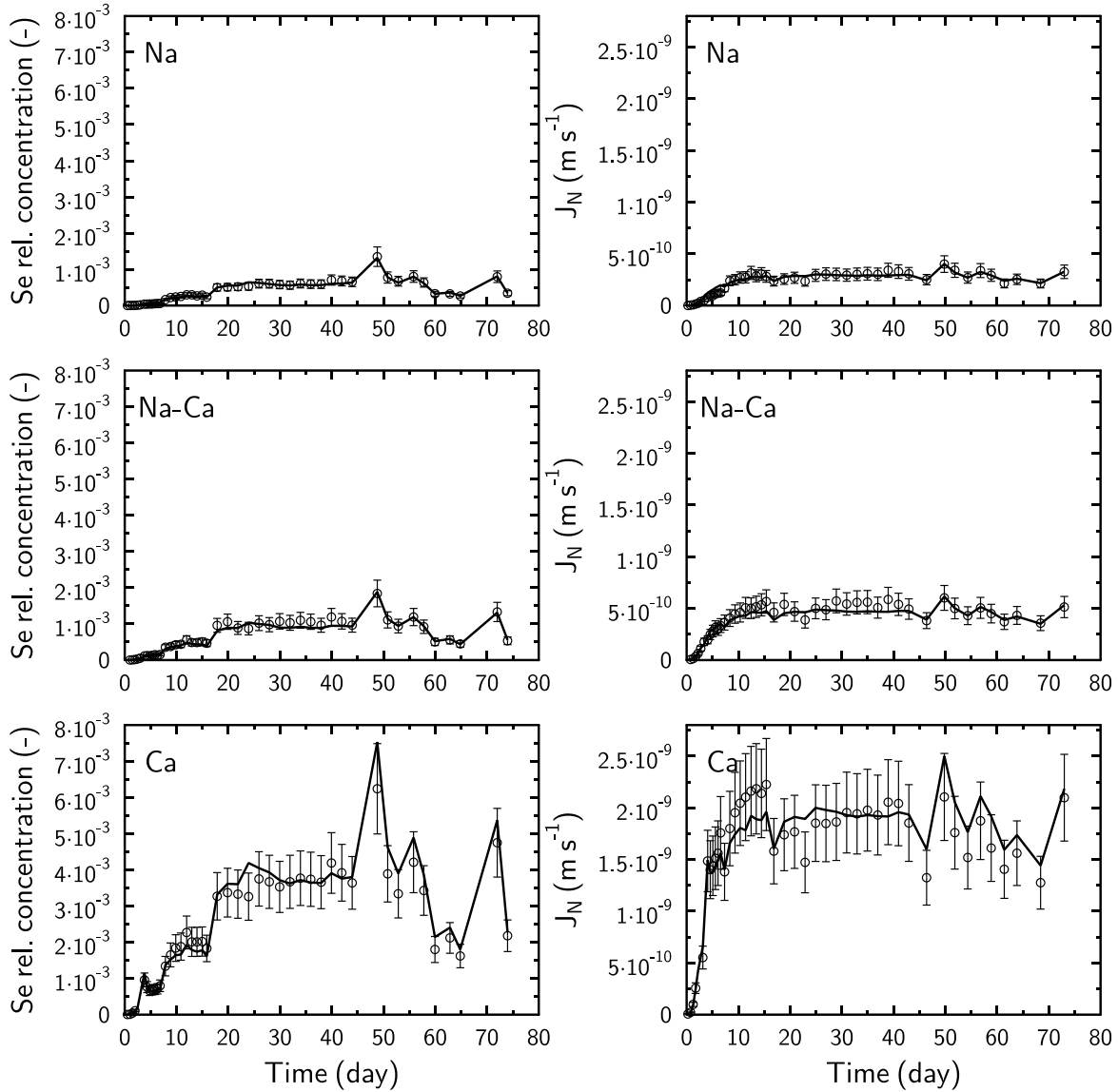
417

418 In the Ca-montmorillonite sample, the minimum accessible porosity was found to be 0.086. This  
 419 higher accessible porosity for Ca-montmorillonite compared to the Na-montmorillonite sample  
 420 can be explained by a combination of the following effects: the presence of wider interparticular  
 421 pores, which increases the average anion accessible porosity (Tournassat et al. 2016) and a  
 422 decrease of the magnitude of the negative electrostatic potential field in the presence of divalent  
 423 cations (Ca<sup>2+</sup>). However, the presence of CaSeO<sub>4</sub> aqueous complexes which are neutral and thus  
 424 not repelled from clay mineral surfaces will also affect the minimum accessible porosity, which  
 425 is not accounted for in the above estimate ( $\varepsilon_{Se,min}$  of 0.086 for Ca). Aqueous speciation  
 426 calculation carried out with the Thermochemie database (Giffaut et al., 2014;  
 427 <https://www.thermochemie-tdb.com/>) indicates that 32% of the total Se concentration is present  
 428 in the form of CaSeO<sub>4</sub> in a 0.033 M CaCl<sub>2</sub> background solution. Equivalently, at least 32% of the  
 429 total porosity is accessible to Se in this neutral form, *i.e.* a revised minimum accessible porosity  
 430 of  $0.32 \times 0.56 = 0.18$ , giving in turn a revised  $K_{D,max}$  value of 0.22 L kg<sup>-1</sup> (Table 3.). Assuming  
 431 that the  $D_0$  value for CaSeO<sub>4</sub> is similar to that of CaSO<sub>4</sub> ( $D_0 = 4.71 \cdot 10^{-10} \text{ m}^2 \text{ s}^{-1}$  available from the  
 432 PHREEQC.dat database), a  $\tau_{Se,max}$  value of 0.115 can be deduced.

433 In the Na-Ca cell, with 0.005 M CaCl<sub>2</sub> + 0.085 M NaCl background solution, 6.6% of the total  
 434 aqueous Se(VI) is in the form of CaSeO<sub>4</sub>, leading to a minimum accessible porosity of  $\varepsilon_{Se,min} =$   
 435  $0.066 \times 0.55 = 0.036$ . The corresponding  $\tau_{Se,max}$  value is 0.123, which is very similar to the value  
 436 found for the Ca-montmorillonite sample.

437 The above analysis highlights the importance of a good knowledge of the aqueous speciation to  
 438 understand and predict the diffusion properties of Se and provides realistic constraints for the  
 439 ranges of  $\varepsilon_{Se}$ ,  $K_{DSe}$ , and  $\tau_{Se}$ .

440



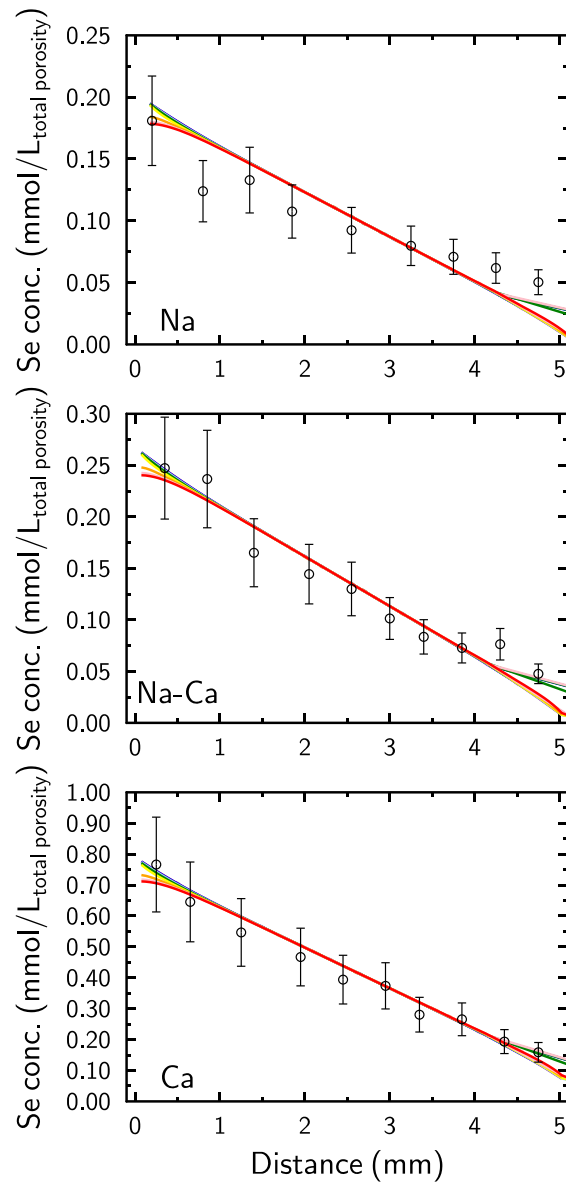
441

442 **Figure 2. Left: Se normalized concentrations in the low-concentration reservoir as a**  
 443 **function of time. Right: Se normalized flux as a function of time. Na, Na-Ca, and Ca refers**  
 444 **to the three different salt background and clay conditioning conditions. Circles:**  
 445 **experimental data; lines: results of the  $\varepsilon - D_e - K_D$  models (Table 2.) where  $K_D$  is assumed**

446 to be 0. Error bars are representative of the analytical error on the Se measurements. The  
447 y-axis scale is the same for all conditions to ease a direct comparison.

448

449



450

451 **Figure 3. Total Se profiles in clay at the end of diffusion experiments. Se concentrations are**  
452 **expressed as a concentration in the total porewater volume. Circles: experimental data;**  
453 **lines: simulated profiles using the same  $\alpha_{Se}$  and  $D_{e,Se}$  as in Figure 2. The different colors are**

454 **indicative of the different profile positions in the radial direction (the red color is for the**  
455 **central grid-cells on the symmetry axis). Error bars represent the analytical error (2**  
456 **standard deviations). Note that the concentrations at the downstream boundary do not**  
457 **tend to zero because of the O-ring and the presence of tubings (i.e., ‘dead volumes’) in**  
458 **which the tracers are accumulating between sampling events.**

459

## 460 **4. Conclusions**

461 An increase of Ca/Na ratio in solution and on clay surfaces is responsible for an increase in HTO  
462 and selenate diffusivity in montmorillonite samples. The increase of HTO diffusivity can be  
463 explained by a change of microstructure leading to an increase of the  $\tau_{\text{HTO}}$  value. These changes  
464 will affect the transport of all radionuclides through clay barriers, including Se. In addition, the  
465 aqueous speciation of Se(VI) has a large effect on Se transport. Se(VI) diffusion is limited by  
466 anion exclusion due to the formation of the negatively charged species  $\text{SeO}_4^{2-}$ . However, in the  
467 presence of  $\text{Ca}^{2+}$ , the formation of  $\text{CaSeO}_4$  neutral ion pairs, which can access a larger portion of  
468 the total porosity, increases selenate diffusivity. While additional insights about the exact  
469 distribution of the interlayer and interparticle porosities and the influence of the diffuse layer on  
470 selenate ion pair formation would be necessary to build a comprehensive mechanistic model for  
471 selenate diffusion in montmorillonite samples, we provide constraints on model parameters that  
472 can be used to predict a range of Se(VI) transport in engineered barrier systems. Our analysis  
473 highlights that Se(VI) diffusion parameters (*e.g.*, effective diffusion coefficients) obtained with  
474 simplified laboratory systems cannot be transferred to the simulation of a repository if *in situ*  
475 geochemical conditions, especially ionic strength and major element concentrations (*e.g.*, Ca),  
476 are different from the laboratory conditions. Furthermore, these results have similarly important  
477 implications for the diffusion of other radionuclides which are present as anions or mixed-  
478 species in waste repositories, including Se(IV) ( $\text{HSeO}_3^-$ ,  $\text{SeO}_3^{2-}$ ), U(VI) (*e.g.*,  $\text{UO}_2(\text{OH})_3^-$ ,  
479  $\text{UO}_2(\text{OH})_4^{2-}$ ), Mo(VI) ( $\text{MoO}_4^{2-}$ ) and others. Radionuclide aqueous speciation together with the  
480 presence of an EDL must be explicitly taken into account in the model in order to accurately  
481 predict their transport. The results also emphasize the need to understand the overall chemical  
482 evolution of repository conditions as changes in aqueous speciation due to many factors (*e.g.*,

483 mineral dissolution/precipitation or groundwater penetration) can change the mobility of  
484 important species.

## 485 **Supplementary Material**

486 Supplementary information, including diffusion cell schematics and additional information about  
487 measuring diffusive properties of the filters is provided in a separate file and is available free of  
488 charge online.

## 489 **Data Availability**

490 Raw experimental data used in this manuscript is available on Mendeley Data (Fox et al., 2024).

## 491 **Acknowledgements**

492 This work was supported by the Spent Fuel and Waste Science and Technology Program, Office  
493 of Nuclear Energy of the US Department of Energy under contract number DE-AC02-  
494 05CH11231 with Lawrence Berkeley National Laboratory.

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