## **Lawrence Berkeley National Laboratory**

**Recent Work**

### **Title**

Vapor-liquid Equilibria for Binary Solutions of Some Comb Polymers Based on Poly(Styrene-co-Maleic Anhydride) in Acetone, Methanol and Cyclohexane

**Permalink** <https://escholarship.org/uc/item/3sv015bd>

### **Author**

Mio, Cristina

**Publication Date** 1997-04-01



## ERNEST ORLANDO LAWRENCE BERKELEY NATIONAL LABORATORY

LBNL-40163  $UC-401$ Preprint

Vapor-Liquid Equilibria for Binary **Solutions of Some Comb Polymers Based on Poly(Styrene-co-Maleic** Anhydride) in Acetone, Methanol and Cyclohexane

Christina Mio, K.N. Jayachandran, and John M. Prausnitz **Chemical Sciences Division** 



#### **DISCLAIMER**

This document was prepared as an account of work sponsored by the United States Government. While this document is believed to contain correct information, neither the United States Government nor any agency thereof, nor The Regents of the University of California, nor any of their employees, makes any warranty, express or implied, or assumes. any legal responsibility for the accuracy, completeness, or usefulness of any information, apparatus, product, or process disclosed, or represents that its use would not infringe privately owned rights. Reference herein to any specific commercial product, process, or service by its trade name, trademark, manufacturer, or otherwise, does not necessarily constitute or imply its endorsement, recommendation, or favoring by the United States Government or any agency thereof, or The Regents of the University of California. The views and opinions of authors expressed herein do not necessarily state or reflect those of the United States Government or any agency thereof, or The Regents of the University of California.

> Ernest Orlando Lawrence Berkeley National Laboratory is an equal opportunity employer.

#### **DISCLAIMER**

This document was prepared as an account of work sponsored by the United States Government. While this document is believed to contain correct information, neither the United States Government nor any agency thereof, nor the Regents of the University of California, nor any of their employees, makes any warranty, express or implied, or assumes any legal responsibility for the accuracy, completeness, or usefulness of any information, apparatus, product, or process disclosed, or represents that its use would not infringe privately owned rights. Reference herein to any specific commercial product, process, or service by its trade name, trademark, manufacturer, or otherwise, does not necessarily constitute or imply its endorsement, recommendation, or favoring by the United States Government or any agency thereof, or the Regents of the University of California. The views and opinions of authors expressed herein do not necessarily state or reflect those of the United States Government or any agency thereof or the Regents of the University of California.

#### LBNL-40163 UC-401

## Vapor-Liquid Equilibria for Binary Solutions of Some Comb Polymers Based on Poly(Styrene-co-Maleic Anhydride) in Acetone, Methanol and Cyclohexane

Cristina Mio, K. N. Jayachandran and John M. Prausnitz

Department of Chemical Engineering

University of California, Berkeley

and

Chemical Sciences Division

Lawrence Berkeley National Laboratory

Berkeley, CA 94720, USA

This work was supported by the Director, Office of Energy Research, Office of Basic Energy Sciences, Chemical Sciences Division of the U.S. Department of Energy under Contract Number DE-AC03-76SF00098.

/

## **Vapor-Liquid Equilibria for Binary Solutions of Some Comb Polymers Based**

**on Poly(Styrene-co-Maleic Anhydride) in Acetone, Methanol and Cyclohexane** 

**Cristina Mio+, K. N. Jayachandran# and John M. Prausnitz\*** 

Chemical Engineering Department University of California, Berkeley and Chemical Sciences Division Lawrence Berkeley National Laboratory Berkeley, CA 94720

#### **Abstract**

Vapor-liquid equilibria have been measured for comb and linear polymers using a gravimetricsorption method in the temperature range 50 to 70  $\degree$ C. Polymers were poly(styrene-co-maleic anhydride) with alkyl side chains of different length (C5, C12, C22) and poly(styrene-co-maleic anhydride) and poly( maleic anhydride). Solvents were acetone, methanol, and cyclohexane.

Due to different chemical structures, the phase behavior of the comb-polymer solutions strongly depends on the ratio backbone/side chains. Freed's lattice-cluster theory gives a good representation of the data.

*Keywords:* Vapor-Liquid Equilibria; Comb Polymer, Lattice-Cluster Theory.

<sup>&</sup>lt;sup>+</sup> On leave from Istituto Impianti Chimici, Università di Padova, Italy

<sup>#</sup> Polymer Division, Indian Institute of Chemical Technology, Hyderabad 500 007, India

<sup>\*</sup> to whom correspondence should be addressed

#### **INTRODUCTION**

Vapor-liquid equilibrium (VLE) data for polymer-solvent solutions are useful for a variety of applications e. g. surface acoustic-wave sensors, polymeric membrane-separation processes, polymer devolatilization, and vapor-phase photografting (Baker et al. (1987), Ballantine and Wohltjen (1989), High and Danner (1990), Kubota et al. (1990), Maeda et al. (1991), Matsumoto et al. (1991)).

In recent publications (Gupta and Prausnitz, 1995, 1996), we reported VLE data for some solutions of copolymers. In this work we report experimental VLE data for some solutions of comb polymers, that is, macromolecules where several side chains (teeth) are attached to a backbone. A few applications of comb polymers have been reported in the literature: Cowie and Sadaghianizadeh (1990) and Takebe et al. (1993) used comb poly(ethylene oxide) and comb polyesters as media for solid polyelectrolytes; Li et al. (1992) studied stability of colloidal alumina suspensions using a hydrophobically modified comb-like polymer; and Radke et al. ( 1996) suggest the use of comb polymers, instead of linear block polymers, as thermoplastic elastomers. Graft copolymers are easier to synthesize than linear block copolymers; their branched structure leads to decreased melt viscosities, thereby facilitating polymer processing. Comb polymers are also added to blends of immiscibile polymers as compatibilizers to improve mechanical properties and structural integrity of a composite material (Israel et al. (1995), Gersappe et al. (1994)).

We studied three combs with the same backbone (styrene-maleic anhydride copolymer); the teeth were alkyl chains of different length (pentyl (C5), dodecyl (C12), behenyl (C22) chains). The comb polymers were mixed with acetone at 50 and 70 °C, or with cyclohexane or methanol at 60 °C. For comparison, we also studied VLE for two linear polymers, poly(styrene-co-maleic anhydride) (PSMA) and homopolymer poly(maleic anhydride) (PMA) in acetone at 50 and methanol at 60 °C.

#### EXPERIMENTAL APPARATUS AND PROCEDURE

We measured VLE for several binary polymer-solvent systems using a gravimetric-sorption method described by Panayiotou and Vera (1984) and by Gupta and Prausnitz (1995).

Figure 1 shows a schematic drawing of the apparatus. It is kept in an air bath maintained at constant temperature within 0.3 ° C.

Each of the three cells in the glass chamber contains one fused-quartz spring attached to an aluminum pan with the polymer sample. Because the gravimetric technique is a classical static method that requires a long time to reach equilibrium, data acquisition is accelerated by obtaining data simultaneously for three different polymers with the same solvent at the same temperature.

The springs (Ruska Instruments Corp., Houston, TX) have a sensitivity of 1 mg/mm and a maximum load limit of 250 mg. In this range, the elongation of the spring is linear with respect to weight. The springs were calibrated to obtain the relation between length and mass. The length of each spring is measured with a cathetometer with a precision of 0.05 mm; therefore, the precision in the mass measurement, 0.05 mg, gives an uncertainty of about 2% in the liquid-phase composition in the composition range 1 to 50 weight percent solvent. As the weight percent solvent rises, this uncertainty declines.

At the beginning of the experiment, a small quantity of the polymer (15 to 25 mg) is loaded into each aluminum pan. After drying the polymer under vacuum to remove moisture, oligomers or solvents, the length of the spring is measured and the dry polymer mass is calculated.

Solvent vapors are introduced by opening and closing the valve that connects the evacuated chamber to the liquid-solvent flask.

The system is allowed to attain equilibrium for several (usually 6 to 12) hours. Equilibrium is attained when the length of the spring remains constant. The total mass of the system polymer+solvent is calculated from the elongation of the spring; the weight fraction of the solvent in the liquid phase is then obtained. The pressure of the system is read from the mercury manometer with a precision of 1 torr. At the low pressures (below 1 bar, or slightly above) used here, no polymer is in the vapor phase. All readings were taken with increasing pressure.

Reliability of the apparatus and procedure was established by reproducing published experimental VLE data for polystyrene-chloroform and polystyrene-acetone (Bawn and Wajid (1956)) at 50  $\rm ^{\circ}C.$ 

To minimize the temperature effect on VLE data, we plot the solvent activity, that is, the ratio of the system pressure to the saturation pressure of the pure solvent  $(PP<sub>1</sub><sup>S</sup>)$ , as a function of liquidphase composition. Solvent saturation pressures were obtained from the Property Data Bank, Appendix A of Reid et al. (1987).

#### **MATERIALS**

Solvents characteristics are given in Table 1. Solvents were degassed by a freeze/thaw procedure described by Panayiotou and Vera (1984).

The polymers had polydisperse molecular weights (polydispersity ca. 1.2). They were used without further fractionation because the influence of polymer molecular weight on VLE is negligible if the degree of polymerization is high.

The structure of the comb-polymer repeat unit is:



The molecular weight of the backbone polymer is 116,000. The backbone is the copolymer poly(styrene-co-maleic anhydride) (PSMA). The alkyl side chains were attached by esterification of the anhydride group with alcohols (1-pentanol, 1-dodecanol, 1-docosanol). The yield of the reaction was approximately 50%; therefore, the molecular weights of the combs CS, C12, C22 are approximately 156,000, 213,000 and 293,400, respectively.

To compare VLE data for solutions of combs with those for solutions of the copolymer backbone (PSMA) and with those for solutions of the homopolymer poly(maleic anhydride) (PMA), we obtained PMA (MW=lO,OOO) from Polysciences, Inc. Warrington, PA (catalog number=02348). Table 2 shows the binary systems studied.

#### RESULTS AND DISCUSSION

Table 3 gives experimental results.

The polymers studied are different from each other in both geometric structure and chemical composition. Therefore, it is not possible to understand separately how either of these differences affects the VLE behavior of the polymer solutions. However, because the degree of branching is light, we expect that the experimental results are primarily determined by the chemical compositions of the copolymers.

Because the backbone of every comb contains oxygen atoms of the anhydride groups, it is likely that polar solvents, like acetone or methanol, are good solvents. However, if the solvent is nonpolar, e.g. cyclohexane, it is a good solvent for the alkyl side chains.

Figures 2, 3 and 4 show the affinity of cyclohexane for the teeth, and of methanol or acetone for the backbone. In each figure we plot data for the same solvent with different polymers. The amount of acetone and methanol absorbed by the polymer increases with decreasing side chain length, while the opposite holds for non-polar cyclohexane. The lines are calculated using Flory-Huggins theory or lattice-cluster theory.

In Figures 5, 6 and 7, the same results are shown, but this time, in each plot there is one single type of comb polymer with three solvents. These figures show that all the polymers absorb more acetone than methanol. The length of the side chain has no effect because the behavior of these two polar solvents is mostly influenced by the carboxyl group rather than by the alkyl chain.

By contrast, as the length of the side chain rises, the curve for cyclohexane data shifts from left to right with respect to the data for acetone and methanol.

Most of our data are reasonably well represented by classical Flory-Huggins theory which does not take into account the geometric architecture of the polymer. In addition to Flory interaction parameter  $\chi$ , only the ratio r of the molar volume of the polymer to that of the solvent is required in the relation:

$$
\mathbf{R} \mathbf{T} \ln \frac{\mathbf{P}}{\mathbf{P}_1^s} = \mathbf{R} \mathbf{T} \ln \mathbf{a}_1 = \mathbf{R} \mathbf{T} \left( \ln \phi_1 + \left( 1 - \frac{1}{r} \right) \phi_2 + \chi \phi_2^2 \right)
$$
 (1)

where R is the gas constant, T is the temperature, P is the system pressure,  $P_1$ <sup>S</sup> is the pure-solvent saturation pressure,  $a_1$  is the solvent activity,  $\phi_1$  is the solvent volume fraction and  $\phi_2$  is the polymer volume fraction.

Because we do not know the densities of the polymers, we set the density of the combs equal to 1  $g/cm<sup>3</sup>$  to transform the measured weight fractions to volume fractions. This approximation does not bring appreciable error. Flory's interaction parameter  $\chi$  was fitted to our VLE data. The results are shown in Figures 2, 3, and 4 where lines are calculated, symbols are experimental. We do not show the results for comb C5-cyclohexane because the experimental data scatter and because the solvent absorbed was less than 15%.

Flory  $\chi$  values are reported in Table 3 where y is the alkyl side-chain weight fraction in the comb. Figure 8 shows  $\chi$  as a function of comb chemical composition. The dependence of  $\chi$  on the weight fraction of alkyl groups in the copolymer is clear; the trend for polar solvents is opposite to that for the non-polar solvent.

Ten Brinke (1983) suggested the relation:

$$
\chi = y \cdot \chi_{AC} + (1 - y) \cdot \chi_{AB} - y(1 - y) \cdot \chi_{BC}
$$
 (2)

for a system containing solvent A and copolymer  $(C_y B_{1-y})$  where y denotes the copolymer composition expressed in volume fraction; we used y as weight fraction. We let B stand for the backbone repeat unit and C for the alkyl side chain. Figure 8 shows that  $\chi$  is a nearly linear function of y indicating that the quadratic term in Equation (2) is negligible. We expect the interactions between the polar backbone and nonpolar teeth to be highly unfavorable, i. e.  $\chi_{BC} > 0$ . However, due to steric hindrance, the effective  $\chi_{BC}$  is close to zero. Because of the geometry of the comb polymers, B and C units are too far to "feel" each other's presence.-

Recently, Lue and Prausnitz (1997) applied Freed's lattice-cluster theory (LCT) to describe concentrated dendritic-polymer solutions. This theory, developed by Freed and coworkers (1989, 1992, and references therein), provides a systematic expansion of the partition function for polymers on a lattice. Unlike the original Flory theory, Freed's theory does not use a mean-field approximation. Lue and Prausnitz showed that· according to LCT, the geometric structure of polymer molecules does not significantly affect the activity of the solvent in solution if the polymer molecules can interpenetrate. Therefore, we fitted our data with LCT for linear polymers. The equations are reported in the Appendix. The only adjustable parameter is the interaction parameter *X·* Figures 2, 3 and 4 show that by removing Flory's mean-field approximation, LCT gives a better representation of the data. Table 4 gives the *X* values from the fit. As with the Flory-Huggins equation,  $\chi$  is a linear function of the weight fraction of the comb's teeth.

The  $\chi$  values from LCT are lower than those from Flory-Huggins theory. Flory's  $\chi$  is often interpreted as the sum of two contributions, the enthalpy and the entropy contribution:

$$
\chi = \chi_{\rm H} + \chi_{\rm S} \tag{3}
$$

The entropic contribution to  $\chi$  follows, in part, from inadequacies of the Flory-Huggins entropy of mixing. Flory-Huggins theory gives only a first approximation of the configurational entropy of mixing; this approximate entropy gives rise to the first two terms of the sum on the right-hand side of Equation (1). However, LCT provides an improved configurational entropic contribution to the solvent chemical potential [Equation (A2) in the Appendix]. LCT gives for  $\chi_s$ :

$$
\chi_s = a^{(0)} - a^{(1)}(1 - 2\phi_2) - a^{(2)}\phi_2(2 - 3\phi_2)
$$
 (4)

(See Appendix for explanations of the symbols). For the systems studied here, for the investigated concentration range,  $\chi_s$  is between 0.198 and 0.230.

Figure 9 shows results for PSMA and PMA with methanol. (We did not obtain data for polystyrene (PS), the other homopolymer of PSMA, because we expect that PS does not absorb a polar solvent like methanol.) Copolymer PSMA absorbs more than each of the two homopolymers PS and PMA. Similar behavior was reported previously (Gupta and Prausnitz (1996)) where it was attributed to "intramolecular repulsion" between . unlike copolymer segments. Ten Brinke et al. (1983) and Paul and Barlow (1984) studied this "intramolecular repulsion" effect in polymer blends. They observed that in a homopolymer+random copolymer  $(A+BC)$  blend, miscibility may occur even if the parent homopolymers B and C are not miscible with A, i. e. if binary interactions A-B and A-C are not exothermic (positive  $\chi_{AB}$  and  $\chi_{AC}$  in Equation (2)). This conclusion is supported by the observation that addition of homopolymer A to copolymer BC dilutes the unfavorable interactions between the two copolymer units (i.e. positive  $\chi_{\text{Bc}}$ ), leading to net exothermic mixing (negative  $\chi$ ). In our case, B and C are styrene and maleic anhydride and the role of the homopolymer (A) is taken by the solvent.

#### **CONCLUSIONS**

VLE data have been obtained for PMA, PSMA and three comb-like polymers in acetone, cyclohexane and methanol. The combs have PSMA as backbone and alkyl side chains of different length (C5, C12, C22). The amount of solvent absorbed by the comb is mainly affected by the comb's ratio of non-polar teeth/polar backbone. This observation is confrrmed by the linear dependence of the Flory's interaction parameter  $\chi$  on the chemical compositions of the combs. Methanol is more soluble in copolymer PSMA than in either of the parent homopolymers, consistent with previous observations for some other copolymer/solvent systems.

#### **ACKOWLEDGMENTS**

This work was supported by the Director, Office of Energy Research, Office of Basic Energy Sciences, Chemical Sciences Division of the U.S. Department of Energy under Contract No. DE-AC03-76SF00098, by the National Science Foundation, and by the Donors of the Petroleum

Research Fund administered by the American Chemical Society. Cristina Mio thanks the Rotary Foundation of Rotary International for the award of an Academic-Year Scholarship.

 $\overline{9}$ 

#### **APPENDIX**

In lattice-cluster theory, polymer architecture is characterized by a set of seven parameters, known as counting indecies: M,  $N^{(1)}$ ,  $N^{(2)}$ ,  $N^{(3)}$ ,  $N^{(1)}$ ,  $N^{(1,1)}$ , and  $N^{(1,2)}$ . M is the number of segments in each molecule (analogous to r in the Flory-Huggins equation).  $N^{(1)}$  is the number of bonds in each molecule.  $N^{(2)}$  is the number of consecutive bonds. Two consecutive bonds are bonds with a site in common.  $N^{(3)}$  is the number of ways three consecutive bonds can be chosen.  $N^{(1)}$  is the number of ways three bonds intersect.  $N^{(1,1)}$  is the number of nonconsecutive bonds.  $N^{(1,2)}$  is the number of ways in which a consecutive pair of bonds and a single bonds, with no sites in common with the two consecutive bonds, can be chosen. For example, for 2,2-dimethyl pentane (each site is a methyl or methylene group):  $M=7$ ,  $N^{(1)}=6$ ,  $N^{(2)}=8$ ,  $N^{(3)}=4$ ,  $N^{(1)}=4$ ,  $N^{(1,1)}=14$ , and  $N^{(1,2)}=12$ . For a linear polymer,  $N^{(1)}$  is (M-1),  $N^{(2)}$  is (M-2),  $N^{(3)}$  is (M-3),  $N^{(1)}$  is zero,  $N^{(1,1)}$  is (M-2)(M-3)/2, and  $N^{(1,2)}$  is  $(M-3)(M-4)$ .

In the following equations,  $\beta$  is equal to  $(k_B T)^{-1}$ , where  $k_B$  is the Boltzmann constant. Upon mixing, the change in chemical potential of the solvent,  $\Delta \mu_1$ , is:

$$
\Delta \mu_1 = \Delta \mu_1^{\text{ath}} + \Delta \mu_1^{\text{int}} \tag{A1}
$$

where  $\Delta \mu_1^{ath}$ , the change in chemical potential for an athermal solution, is:

$$
\beta \Delta \mu_1^{a\text{th}} = \ln(1 - \phi_2) + \left(1 - \frac{1}{M}\right)\phi_2 + a^{(0)}\phi_2^2 - a^{(1)}\phi_2^2(1 - 2\phi_2) - a^{(2)}\phi_2^3(2 - 3\phi_2)
$$
(A2)

and  $\Delta \mu_1^{\text{int}}$ , the contribution of attractive interactions, is:  $\beta \Delta \mu_1^{\text{int}} = A^{(1)} {\phi_2}^2 - (A^{(2)} + B^{(3)}) {\phi_2}^2 (1 - {\phi_2}) (1 - 3 {\phi_2}) - A^{(3)} {\phi_2}^2 (1 - {\phi_2}) (1 - 2 {\phi_2}) \left(1 - 9 {\phi_2} + 10 {\phi_2}^2\right)$  $-A^{(4)}\phi_2^2(1-\phi_2)(1-27\phi_2+138\phi_2^2-294\phi_2^3+306\phi_2^4-126\phi_2^5)$ +(B<sup>(1)</sup> + B<sup>(2)</sup>)2 $\phi_2^2(1-\phi_2) - B^{(4)}2\phi_2^3(1-\phi_2)(1-2\phi_2)$  (A3)  $-C^{(1)}2\phi_2^2(1-\phi_2)(1-2\phi_2)(3-4\phi_2)+C^{(2)}3\phi_2^2(1-\phi_2)^2$  $-C^{(3)}\phi_2^2(1-\phi_2)^2(1-10\phi_2+15\phi_2^2)+C^{(4)}4\phi_2^2(1-\phi_2)^3$ 

The a<sup>(i)</sup> parameters depend only on the architecture of the polymer molecule:

$$
a^{(0)} = \frac{1}{z} [K^{(1)}]^2 + \frac{1}{z^2} \Biggl\{ -4K^{(1)}K^{(2)} + \frac{8}{3} [K^{(1)}]^3 - 2K^{(1)}K^{(3)} + [K^{(2)}]^2 - 2K^{(1)}(K^{(1,2)} - K^{(1)}K^{(2)}M) + 2[K^{(1)}]^4 + 2[K^{(1)}]^2 (K^{(1,1)} - [K^{(1)}]^2M) - 6K^{(1)}K^{(1)} \Biggr\};
$$
  
\n
$$
a^{(1)} = \frac{1}{z^2} \Biggl\{ \frac{8}{3} [K^{(1)}]^3 + 2[K^{(1)}]^4 + 2[K^{(1)}]^2 (K^{(1,1)} - [K^{(1)}]^2M) \Biggr\};
$$
  
\n
$$
a^{(2)} = \frac{1}{z^2} 2[K^{(1)}]^4
$$
 (A4)

and

$$
A^{(1)} = \frac{\beta \varepsilon z}{2}; \quad A^{(2)} = -\frac{(\beta \varepsilon)^2 z}{4}; \quad A^{(3)} = -\frac{(\beta \varepsilon)^3 z}{12}; \quad A^{(4)} = -\frac{(\beta \varepsilon)^4 z}{48};
$$
  
\n
$$
B^{(1)} = -\beta \varepsilon K^{(1)}; \quad B^{(2)} = \frac{\varepsilon}{z} \Big( 2K^{(2)} + K^{(3)} + 3K^{(\perp)} + K^{(1,2)} - K^{(1)}K^{(2)}M \Big);
$$
  
\n
$$
B^{(3)} = -\frac{2\beta \varepsilon}{z} K^{(1)} \Big( 2K^{(1)} + K^{(1,1)} - [K^{(1)}]^2 M \Big); \quad B^{(4)} = -\frac{4\beta \varepsilon}{z} [K^{(1)}]^3;
$$
  
\n
$$
C^{(1)} = -\frac{(\beta \varepsilon)^2}{2} K^{(1)}; \quad C^{(2)} = -(\beta \varepsilon)^2 K^{(2)}; \quad C^{(3)} = -(\beta \varepsilon)^2 [K^{(1)}]^2;
$$
  
\n
$$
C^{(4)} = -\frac{(\beta \varepsilon)^2}{2} \Big( K^{(1,1)} - [K^{(1)}]^2 M \Big)
$$
  
\n(A5)

where  $K^{(i)} = N^{(i)} / M$  (i=1, 2, 3, or  $\perp$ ) and  $K^{(i,j)} = N^{(i,j)} / M$  (i=1, or 2),  $\phi_1$  and  $\phi_2$  are volume fraction of solvent and polymer respectively, z is the lattice coordination number, here set equal to 6, and E, the parameter that characterizes the attractive interactions in the system, is related to Flory-Huggins  $\chi$  by  $\chi = \frac{\beta \varepsilon z}{2}$ .

#### REFERENCES

Ballantine, D. S. and Wohltjen, H., 1989. Surface Acoustic-Wave Devices for Chemical Analysis. *Anal. Chern.* 61: 704A.

f.

Baker, R. W.; Yoshiska, N.; Mohr, J. M. and Khan, A. J., 1987. Separation of Organic Vapors from Air. J. *Mernbr. Sci.* 31: 259.

Bawn, C. E. H. and Wajid M. A., 1956. High Polymer Solutions. Part 7. Vapor Pressure of Polystyrene Solutions in Acetone, Chloroform and Propyl Acetate. *Trans. Faraday Soc.,* 52: 1658.

Cowie, J. M.G. and Sadaghianizadeh, K., 1990. Effect of Side Chain Length and Crosslinking on the AC Conductivity of Oligo (ethyleneoxide) Comb-Branch Polymer-Salt Mixtures. *Solid State Ionics,* 42: 243.

Freed, K. F. and Bawendi, M.G., 1989. Lattice Theories of Polymeric Fluids. J. *Phys. Chern.,* 93: 2196.

Gersappe, D.; Irvine, D.; Balazs, A. C.; Liu, Y.; Sokolov, J.; Rafailovich, M.; Schwarz, S. and Peiffer, D. G. (1994). The Use of Graft Copolymers to Bind Immiscible Blends. *Science,* 265: 1072.

Gupta, R. B. and Prausnitz J. M., 1995. Vapor-Liquid Equilibria of Copolymer plus Solvent and Homopolymer plus Solvent Binaries: New Experimental Data and Their Correlation. J. *Chern Eng. Data,* 40: 784.

Gupta, R. B. and Prausnitz J. M., 1996. Vapor-Liquid Equilibria for Copolymer-Solvent Systems: Effect of Intramolecular Repulsion. *Fluid Phase Equil.,* 117: 77.

High, M.S. and Danner, R. P., 1990. Prediction of Solvent Activities in Polymer Solutions. *Fluid Phase Equil.* 55: 1.

Israel, R.; Foster, D. P. and Balazs, A. C., 1995. Designing Optimal Comb Compatibilizers: AC and BC Combs at an *AlB* Interface. *Macromolecules,* 28: 218.

Kubota, H.; Yoshino, N. and Ogiwara, Y., 1990. Vapor-Phase Photographting on Low-Density Polyethylene Film in Binary Monomer System. J. *Appl. Pol. Sci.,* 39: 1231.

Li, C.; Yu, X. and Somasundaran, P., 1992. Effect of Comb-like Amphiphilic Polymer on the Stability of Alumina Dispersions. *Colloids and Surface,* 69: 155.

Lue, L. and Prausnitz, J. M., 1997. Structure and Thermodynamics of Homogeneous-Dendritic-Polymer Solutions: Computer Simulation, Integral Equation, and Lattice-Cluster Theory. (Submitted for publication to *Macromolecules).* 

Maeda, Y.; Tsuyumoto, M.; Karakane, H. and Tsugaya, H., 1991. Separation of Water-Ethanol Mixture by Pervaporation through Hydrolyzed Polyacrylonitrile Hollow Fiber Membranes. *Polymer J.*, 23:501.

Matsumoto, K.; Ishii, K.; Kuroda, T.; Inoue, K. and lwama, A., 1991. Membrane Process for Organic Vapor Recovery from Air. *Polym.* J., 23: 491.

Nemirovsky, A. M.; Dudowicz, J. and Freed, K. F., 1992. Dense Self-interacting Lattice Trees with Specified Topologies: from Light to Dense Branching. *Physical Review* A, 45: 7111.

Panayiotou, C. P. and Vera, J. H., 1984. Thermodynamics of Polymer-Polymer-Solvent and Block Copolymer-Solvent Systems. I. Experimental Systems. *Polym.* J., 16: 89.

Paul, D. R. and Barlow, J. W., 1984. A Binary Interaction Model for Miscibility of Copolymers in Blends. *Polymer,* 25: 487.

Radke, W.; Roos, S.; Helga, M.S. and Muller, A. H. E., 1996. Acrylic Thermoplastic Elastomers and Comb-Shaped Poly(methyl methacrylate) via the Macromonomer Technique. *Macrom. Symp.,* 101: 19.

Reid, R. C.; Prausnitz, J. M. and Poling, B. E., 1987. The Properties of Gases and Liquids. Fourth Edition, New York; McGraw-Hill.

Takebe, Y.; Hochi, K. and Shirota, Y., 1993. Ionic Conductivities ·of Hybrid Films Composed of Comb Polymers Containing Esters as Pendant Groups and Lithium Trifluoromethane Sulfonate. *Solid Stcite Ionics,* 60: 125.

ten Brinke, G.; Karasz, F. E. and MacKnight, W. J., 1983. Phase Behavior in Copolymer Blends: Poly(2,6-dimethyl-1,4-phenylene oxide) and Halogen-Substituted Styrene Copolymers. *Macromolecules,* 16: 1827.





Table 2. Systems studied



### Table 3.

Vapor-liquid equilibrium data for comb (C5, C12, C22) and linear (PMA, PSMA) polymers

 $P=$  pressure;  $P_1^s$  = saturated vapor pressure

 $w_1$  =solvent weight fraction in the liquid phase



Solvent: Acetone;  $T=50^{\circ}C$ ;  $P_1^s = 612$  torr

Solvent: Acetone;  $T=50^{\circ}C$ ;  $P_1^s = 612$  torr

$W_1$ (PMA)	$w_1$ (PSMA)	$P$ (torr)
0.058	0.098	215.5
0.107	0.144	278.0
0.184	0.181	336.5
0.259	0.217	389.0
0.278	0.229	400.0
0.361	0.286	454.0
0.500	0.379	489.0

$W_1$ (C5)	$W_1$ (C12)	$W_1$ (C22)	P (torr)
0.015	0.022	0.024	230.0
0.032	0.039	0.036	317.5
0.050	0.053	0.050	408.5
0.076	0.073	0.063	494.5
0.109	0.102	0.085	587.0
0.151	0.137	0.110	679.5
0.206	0.183	0.142	786.0
0.255	0.222	0.173	857.5
0.294	0.254	0.194	896.0

Solvent: Acetone; T=70°C;  $P_1^s = 1196$  torr

Solvent: Cyclohexane; T=60 $^{\circ}$ C; P<sub>1</sub><sup>s</sup>= 390 torr

(C5) $W_1$	$W_1$ (C12)	(C22) $W_1$	P (torr)
	0.010	0.024	50.5
0.004	0.022	0.033	76.5
0.006	0.037	0.057	10.0
0.018	0.059	0.071	13.5
0.019	0.065	0.094	15.5
0.025	0.086	0.119	18.5
0.047	0.113	0.154	218.0
0.054	0.144	0.191	251.5
0.066	0.179	0.235	279.0
0.108	0.231	0.290	300.5
0.126	0.308	0.370	326.5

Solvent: Methanol; T=60°C;  $P_1^s$  = 635 torr



(PMA) $W_1$	(PSMA) $W_1$	$P$ (torr)
0.024	0.068	127.5
0.044	0.094	175.5
0.078	0.122	229.5
0.118	0.170	286.5
0.147	0.206	339.0
0.179	0.239	393.0
0.203	0.263	434.5
0.248	0.300	484.5
0.306	0.343	505.0

Solvent: Methanol;  $T=60^{\circ}C$ ;  $P_1^s = 635$  torr

		Acetone at 50 $\degree$ C <b>FH/LCT</b>	Methanol at 60 $\degree$ C <b>FH/LCT</b>	Cyclohexane at 60 $\degree$ C <b>FH/LCT</b>
C <sub>5</sub>	0.253	0.405/0.240	0.601/0.423	1.370/1.274
C12	0.446	0.506/0.366	0.780/0.685	0.660/0.529
C22	0.595	0.812/0.721	1.155/1.064	0.385/0.225
<b>PSMA</b>		0.158/-0.013	$0.052/-0.132$	--

Table 4. Flory's interaction parameter using Flory-Huggins (FH) and Lattice-Cluster Theory (LCT)

y = alkyl side-chain weight fraction in the comb.

#### List of Figures

Figure 1. Experimental apparatus for vapor-liquid equilibra for polymer/solvent systems.

Figure 2. Activity of acetone in comb C5, comb C12, comb C22 and linear PSMA polymers at 50 °C; symbols, experimental; lines, calculations using Flory-Huggins equation (-) and Lattice-Cluster theory (----).

Figure 3. Activity of methanol in comb C5, comb C12, comb C22 and linear PSMA polymers at 60 °C; symbols, experimental; lines, calculations using Flory-Huggins equation  $(-)$  and Lattice-Cluster theory  $(---)$ .

Figure 4. Activity of cyclohexane in comb C5, comb C12, comb C22 and linear PSMA polymers at 60 °C; symbols, experimental; lines, calculations using Flory-Huggins equation  $(-)$  and Lattice-Cluster theory (----).

Figure 5. Activity of acetone at 50 °C, cyclohexane at 60 °C, methanol at 60 °C in comb C5.

Figure 6. Activity of acetone at 50 °C, cyclohexane at 60 °C, methanol at 60 °C in comb C12.

Figure 7. Activity of acetone at 50 °C, cyclohexane at 60 °C, methanol at 60 °C in comb<sup>-</sup>C22.

Figure 8. Flory's interaction parameter  $(\chi)$  versus weight fraction of alkyl side-chains in comb polymers (y).

Figure 9. Activity of methanol in PMA and PSMA at 60 °C.



# Figure 1





Figure 3





- - Figure 5



 $\frac{1}{2}$ 

Figure 6



 $\overline{\phantom{0}}$ 



Figure 8



 $30<sub>o</sub>$ 

ERNEST ORLANDO LAWRENBE BERKELEY NATIONAL LASORATORY ONE OVELOVEDN ROAD | BERKELEY, GALIFORNIA 94720

 $\bullet$ 

J.

Repurch for the U.S. Deputment of thregy under Contract No. (DIACOB-ICHOODS)