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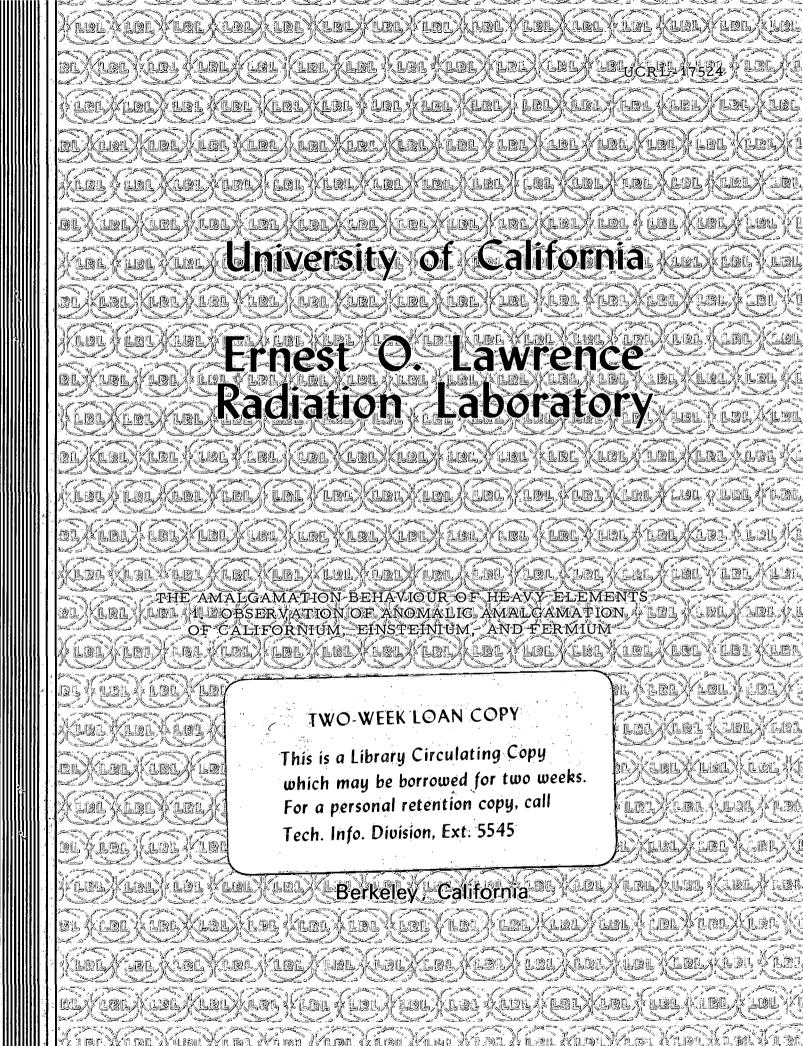
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# **Publication Date**

1967-05-01



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AEC Contract No. W-7405-eng-48

THE AMALGAMATION BEHAVIOUR OF HEAVY ELEMENTS

1. OBSERVATION OF ANOMALIC AMALGAMATION OF CALIFORNIUM, EINSTEINIUM, AND FERMIUM

Jaromír Malý

May 1967

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1. OBSERVATION OF ANOMALIC AMALGAMATION OF CALIFORNIUM, EINSTEINIUM, AND FERMIUM\*

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The extraction of rare earths, which have somewhat stable 2+ valence (like Eu, Sm, Yb), in alkali metals amalgams is well known (1,2,3,4,5,6). Related methods which transfer these rare earth elements into the amalgams by the electrolysis of water solutions containing alkali metals, acetates and citrates, is also well described in a number of papers (1,7,8,9,10,11).

Some of these papers demonstrate methods for the purification of Yb or Sm and Eu from neighbor elements, by means of sodium amalgam extraction. Europium, Sm, and Yb may preferentially replace Na in amalgams, often with a yield of more than 50% in one extraction when the other rare earths, which have not double valences, are extracted (1,2,3,4,6,13,14) or electrolyzed (8,9,10,15,16) with  $\lesssim 10X$  less amount.

With the exception of actinium (17,18) the literature does not describe the application of these separation methods to the group of actinides. Some experiments were performed, which demonstrate the possibility of using the sodium amalgam method of separation of some transuranium elements

<sup>\*</sup>This work was performed under the auspices of the U.S. Atomic Energy Commission

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from the others. The initial experiments used conditions applied to lanthanides separations (4,15,16) and may not be the optimal for the transuranium
elements separation. Described below are some typical experiments, which
show the possibility of high preferential extraction of Cf,E and Fm in
sodium amalgam, or the possibility of electrolytic separation of Cf, E and
Fm on a mercury cathode in comparison with Pu, Am, Cm, and Bk which remains
mostly in the original solution.

# Experimental

The extraction experiments. The "a mixture", a solution containing approximately equal  $\alpha$  activities of <sup>239</sup>Pu, <sup>241</sup>Am, <sup>244</sup>Cm, <sup>252</sup>Cf, and eventually <sup>252</sup>Es was prepared in 0.5 MHCl at a level of about 1000  $\alpha$  dpm/20 $\lambda$  total activity (excluding  $^{252}$ E, whose  $\alpha$ -activity was only  $10^{-3}$  of total  $\alpha$ -activity). The <sup>249</sup>Bk solution and <sup>169</sup>Yb solution were prepared similarly, <sup>249</sup>Bk in 0.5 MHCl, the 169 Yb from natural ytterbium irradiated in the reactor and dissolved in a solution containing lM NH<sub>4</sub>Cl, 0.5 M HCl and  $\sim$ 17  $\mu$ g Yb<sub>2</sub>O<sub>3</sub> in 5 $\lambda$ . Both solutions contained  $\sim 5,000$  dpm  $\beta \gamma/min$  per  $5\lambda$  and were measured in a windowless counter. The 252 Fm, 149 Tb, and 151 Dy were prepared in the HTIAC by irradiation of  $^{248}$ Cm with  $^{12}$ C, Sm with  $^{12}$ C, and Ce with  $^{16}$ O, respectively. The recoil of Fm, Tb, or Dy atoms were caught on a Pt disc from which they were washed with 40λ of "α mixture". The sodium amalgam contained 3.5-4.0 milliequivalents Na/ml was prepared by dissolving small pieces of fresly cut sodium metal in the mercury. For every extraction experiment 20 $\lambda$  to 40 $\lambda$  of " $\alpha$ mixture" were mixed in 3 ml cone with 5% of either 169 Yb or 247 Bk solution, 5λ of &I ammonium acetate, 150λ of 7M sodium acetate and 3λ of LaCl,

solution, containing 300 μgm La<sub>2</sub>0<sub>3</sub>. To this mixture were added by short spitzer every 1 min ~ 50% of sodium amalgam from a second 3 ml cone; altogether 250% of amalgam were added in 3-4 portions. The amalgam and tracercontaining sodium acetate solution were mixed intensively by sucking in and out of the spitzer (40-50 times during 4 minutes). Foaming and hydrogen evolution occur on introduction of the first portion of amalgam, but by the fourth the foaming usually stops and a precipitate of  $La(OH)_3$  appears in the solution. After 4 min of extraction the mercury was separated from the original solution and washed twice with 300% of 6M NH OH. The extracted elements were back-extracted from the mercury into 400λ's of 6 M HCL. After the solution was neutralized to pH4 (methylred indicator) the activities were plated out on a Pt disc. After washing and flaming, the Pt disc was analyzed for  $\beta$ -activities in a windowless counter and for  $\alpha$ -activities in an  $\alpha$ -grid chamber in connection with a 200 channel analyzer, which identified the amounts of 149<sub>Tb</sub>, 151<sub>Dy</sub>, 239<sub>Pu</sub>, 241<sub>Am</sub>, 244<sub>Cm</sub>, 252<sub>Cf</sub>, 255<sub>E</sub>, and 252<sub>Fm</sub>. The original amounts before extraction of the various elements were determined in a similar way using 1/10 of the original sodium acetate-tracer solution. In the case of short-lived isotopes (149 and 151 Dy), these isotopes were identified by \alpha-energy and half-life measurements and usually the sample from extraction was measured along with the original solution simultaneously on two grid  $\alpha$ -chambers connected with two 200 channel pulse analysers.

The La(OH)3 which precipitated at the end of extraction and contained most of the nonextracted actinides and rare earths, was usually

analyzed similarly for its content of nonextracted isotopes, to obtain the total balance of radioactivity.

The electrolytic experiments. For electrolysis, the same mixture was used as in the sodium amalgam extraction, or else the 5λ of 8M ammonium acetate in this mixture was replaced by 5λ of tertiary sodium citrate which was 0.5M in  $Na^{\dagger}$  as it is mentioned in the last column of Table II. This mixture was diluted before electrolysis with 200% of H<sub>2</sub>O and 200% of 7M sodium acetate to  $600\lambda$  of electrolyte. A glass tube with a cross section ~1 cm2, with Pt contact at the bottom, covered with 600% of pure polarographic mercury was used for electrolysis. Above the mercury was 600% of electrolyte and a Pt anode with a single spiral of ~3 mm diam, dipping ~2 mm in the electrolyte. All electrolyses were performed on air. The electrolyzer was gently shaken during electrolysis to help mix the electrolyte. During electrolysis the electrolyzer was immersed in a beaker containing water at 15°C. The electrolysis was carried out for 30 min at a potential of 5 V and a current of 20-25 mA dc. At the end of electrolysis the steady bubbling of hydrogen from the cathode indicated the presence of sodium amalgam in the mercury. After electrolysis the mercury was separated from the supernatant solution and treated exactly the same way as the mercury after sodium extraction (i.e., washed 2X with  $\mbox{HN}_{\mbox{\scriptsize h}}\mbox{OH}$ , decomposed with HCl, neutralyzed, and electroplated).

# Results and Discussion

Table I presents a summary of the sodium amalgam extraction experiments. Conditions were identical except for the addition of various amounts of HCl to the solutions just prior to adding the amalgam, as noted in the last column of Table I. The initial pH was 6.0-7.0, without any addition of HCl; with the addition of the 75λ of MHClthe pH dropped only to 5.0-6.0. Larger amounts of hydrogen were evolved from the more acid solutions. In all cases the final pH was >10-11 and a clearly visible precipitate of La(OH)3 appeared.

The data of Table I clearly show that Cf, E, and Fm are extracted with sodium amalgam very similarly to Yb (and the other lanthanides which exhibit 2+ valency). The actinide homologs of Sm and Eu - Pu and Am - are extracted poorly (< 10%), relative to Yb and Cf, but comparably to the light lanthanides, like La, Ce, Pr, and Nd (14).

Berkelium is the least extracted of the actinides tested. In this respect it resembles terbium, which shows very low extraction. However, dysprosium, the lanthanide analog of Cf shows very low extraction in the same experiment in which Cf shows high extraction, ~1000 times better than Dy, and close to Sm or Eu in the lanthanide family. Comments in the literature (14) about nonextractibility of all heavier lanthanides, starting from gadolinium (with exclusion of Yb) and the Onsott's work (10) concerning the very slow electrodeposition -long after Yb and Tb-of Dy, Ho and Er (in the same sequence), indicates that Ho and Er should be less extractable than Dy. However, the actinide analoges of Ho and Er, the elements E and Fm, are

extracted even better than Yb as shown in Table I. The results of four electrolytic experiments are shown in Table II below. Experiments 1 and 2 were performed with the addition of 5 $\lambda$  of 0.5N tertiary sodium citrate; 3. and 4. were done with the addition of 50 $\lambda$  of 3MHCl to the original mixture. La(OH)<sub>3</sub> precipitation was not observed in experiments 3 or 4.

The results in Table II are very close to those in Table I. The data are compared in Table III (mean values from Tables I and II). The yields relative to californium are observed to be the same to within less than a factor of two, when compared with the more acid extraction experiments. The main result — the preferential extraction of Cf, E, and Fm with ~10 times enrichment, relatively to Pu, Am, Cm, and Bk, in one extraction step, was observed in all experiments.

# Conclusion

The results in Table I and II show that Cf, E, and Fm could be extracted or separated by electrolysis about 10-30 times more efficiently than lighter actinides.

Both kinds of experiments presented above are very similar to the known results with preferential extraction in sodium amalgam (2,3,4,5) or preferential electrolytic separation on mercury cathode of double valent rare earths, Sm, Eu, and Yb (15,16).

Several authors (15, 16) explain this preference in electrolysis by a mechanism in which they suppose that probably first the Yb, Eu, and Sm are reduced in 2+ state, before the preferential electrolysis occurs.

It seems logical to expect therefore that in the family of actinides Fm, E,

or Cf may form a +2 valence. It will be most interesting to extend the above presented extraction and electrolysis experiments to Mv and No, or to the lower actinides, to know more about the amalgamation, eventually about the tendency to 2+ state in whole actinide family. The experiments in this direction are now in progress.

## Acknowledgments

The author would like to express deep gratitude to Professor B. B. Cunningham and Dr. A. Ghiorso for their encouraging and valuable assistance during the work.

The author is deeply indebted to Professor G. T. Seaborg for his continuous support of this work and many valuable suggestions, which he sent during this work by correspondence. The author appreciates the very good work of all the staff of HILAC and the assistance of Dr. Matti Nurmia during the irradiation.

The author would like to express his gratitude to IAEA in Vienna for financial support of this work by IAEA research grant in Lawrence Radiation Laboratory.

TABLE I

Sodium Amalgam Extraction
of Lanthanide and Actinide Elements

nent	149 <sub>Tb</sub>	151 <sub>Dy</sub>	169 <sub>Yb</sub>	239 <sub>Pu</sub>	241 <sub>Am</sub>	244 Cm	249 <sub>Bk</sub>	252 <sub>Cf</sub>	252 <sub>.E</sub>	252 <sub>Fm</sub>	HCl	add	ed .	
ratio to xtracted														
						· · · · · · · · · · · · · · · · · · ·	<u> </u>			•	•	• .		
6			29	4.9.	3.3			40						
tio to Cf			0.725	0.125	0.082	0.037	ri Harisana	1.000						en e
<b>%</b> -			33	2.3	2.1	1.8		45	and the second of the Alpha Second of the second of the	90				
tio to Cf			0.732	0.051	0.047	0.040	,	1.00		2.00			•	
<b>%</b>				2.7	2.3.	2.2	0.5	39		57				
tio to Cf				0.047	0.040	0.039	0.013	1.00		1.46		•		
76				5.6	3.3	3.3	0.9	51	50		50λ	of	3M H	ci -
tio to Cf			-	0.11	0.065	0.065	0.018	1.00	0.98	•	** h*;	٠٠.		
%				6.7	5.4	<b>3.1</b>	1.4	60	61		50λ	of	зм н	Cl.
tio to Cf				0.112	0.090	0.068	0.023	1.00	0.98					•
<i>t</i> 6	0.15		62	5.1	3.0	2.6		68			<b>75</b> λ	of :	em H	Cl
•	0.0022		0.912	0.075	0.044	0.038		1.00					•	, .
•		·			1.5	2.3	·:	50			75λ	of i	em H	Cl ´
•		•	1.06	· * * * * * * * * * * * * * * * * * * *	0.030	0.046		1.00						*,
	en e	0.06	50					95			75λ	of	RM H	Cl
		•				**		•				٠	· ·	•
										5 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	75x	of	RM H	21
		0.0006	0.530	· · · · · · · · · · · · · · · · · · ·		0.053		1.000						
	tio to Cf	tracted ratio to xtracted xp. No.  tio to Cf  tio to Cf	tracted ratio to xtracted xp. No.  tio to Cf  0.0022  0.14   tio to Cf  0.0028   0.06  tio to Cf  0.0006	tracted ratio to extracted xp. No.  29 tio to Cf	tracted ratio to extracted xp. No.  29 4.9.  tio to Cf 0.725 0.125  tio to Cf 0.732 0.051  2.7  tio to Cf 0.047  5.6  tio to Cf 0.11  6.7  tio to Cf 0.12  tio to Cf 0.12  tio to Cf 0.022 0.912 0.075  1.06 0.054  1.06 0.054  1.06 0.054  1.06 0.054  1.06 0.054  1.06 0.054  1.06 0.054  1.06 0.054  1.06 0.054  1.06 0.054  1.06 0.054  1.06 0.054  1.06 0.054  1.06 0.054  1.06 0.054  1.06 0.054  1.06 0.054  1.06 0.054	tracted ratio to xtracted xp. No.  29 4.9. 3.3 tio to Cf 0.725 0.125 0.082  33 2.3 2.1 tio to Cf 0.732 0.051 0.047  2.7 2.3 tio to Cf 0.047 0.040  5.6 3.3 tio to Cf 0.11 0.065  6.7 5.4 tio to Cf 0.0022 0.912 0.075 0.044  53 2.7 1.5 tio to Cf 0.0028 1.06 0.054 0.030  0.06 50 16.9 7.9 tio to Cf 0.0006 0.526 0.179 0.083	tracted ratio to extracted xp. No.  29	tracted ratio to extracted xp. No.	tracted ratio to extracted xp. No.	tracted ratio to extracted xxp. No.  29 4.9. 3.3 1.5 40 tio to cf 0.725 0.125 0.082 0.037 1.000  2 33 2.3 2.1 1.8 45 tio to cf 0.732 0.051 0.047 0.040 1.00  2 2.7 2.3 2.2 0.5 39 tio to cf 0.047 0.040 0.039 0.013 1.00  3 5.6 3.3 3.3 0.9 51 50 tio to cf 0.012 0.065 0.065 0.018 1.00 0.98  3 6.7 5.4 *.1 1.4 60 61 tio to cf 0.022 0.912 0.075 0.044 0.038 1.00 0.98  3 62 5.1 3.0 2.6 68 tio to cf 0.0028 1.06 0.0912 0.075 0.044 0.038 1.00  3 0.06 50 16.9 7.9 5.7 95 tio to cf 0.0028 0.006 0.526 0.179 0.083 0.060 1.000	tracted ratio to extracted xp. No.	tracted ratio to extracted xp. No.	tracted ratio to tarracted xxp. No.  \$	tracted ratio to to tracted xp. No.  \$ 29

TABLE II

Electrolysis of Lanthanide and Actinide Elements

Element Yield of electro- lysed	169 <sub>Yb</sub>	239 <sub>Pu</sub>	241 <sub>Am</sub>	244 <sub>Cm</sub>	249 <sub>Bk</sub>	252 <sub>Cf</sub>	252 <sub>E</sub>	252 <sub>Fm</sub>	Added in electro-lyser
elements in Exp.									
1. %	27	4.7	2.2	2.1		49		80	5λ 0.5N
Ratio to Cf	0.55	0.096	0.045	0.043		1.00		1.63	Nacitrate
2. %	- -	3.6	1.8	4.8	0.3	38		67	5λ 0.5N
Ratio to Cf		0.095	0.097	0.126	0.008	1.00		1.76	Nacitrate
3. %	•	5,1	3.2	5.2	1.6	71	75	-	5λ 3MHCl
Ratio to Cf		0.072	0.045	0.073	0.022	1.00	1.056		
4. %	•	5.3	2.8	4.8	0.6	55	60		5λ 3MHCl
Ratio to Cf		0.096	0.051	0.087	0.011	1.00	1.09	1	

TABLE III

Comparison of Sodium Amalgam Extraction and Electrolysis of
Lanthanide and Actinide Elements

Element	Tb	Dy Yb	Pu	Am	Cm	Bk Cf	E Fm
Yield of							
extracted elements							
mean value	0.0025 0	.0006 0.748	0.102	0.062	0.050 0	.018 1.000	0.98 1.73
extraction			1. · · · · · · · · · · · · · · · · · · ·				
mean value from	•	~0.55	0.090	0.047	0.082 0	.014 1.000	1.072 1.69
electrolysis							

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