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ELECTROCHEMICAL EVALUATION OF NEW FLUOROSULFONIC AND FLUOROPHOSPHONIC ACIDS AS FUEL CELL ELECTROLYTES: ANNUAL REPORT, MAY 1, 19S7 - APRIL 30, 1988

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# Lawrence Berkeley Laboratory

UNIVERSITY OF CALIFORNIA

# Materials & Chemical Sciences Division

Electrochemical Evaluation of New Fluorosulfonic and Fluorophosphonic Acids as Fuel Cell Electrolytes: Annual Report, May 1, 1987–April 30, 1988 RECEI LAWRENCE

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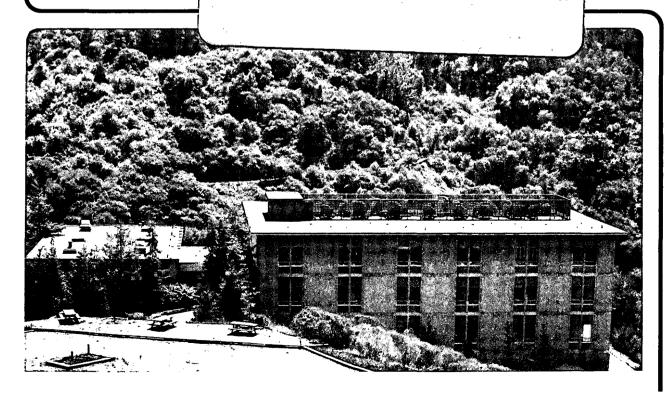
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June 1988

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# ELECTROCHEMICAL EVALUATION OF NEW FLUOROSULFONIC AND FLUOROPHOSPHONIC ACIDS AS FUEL CELL ELECTROLYTES

Annual Report

April 1987 - April 1988

Prepared by

M.H. Saffarian and P.N. Ross

Materials and Chemical Sciences Division Lawrence Berkeley Laboratory University of California Berkeley California 94720

For

GAS RESEARCH INSTITUTE

Contract no. 5086-260-1229

GRI Project Manager Daniel A. Scarpiello

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#### RESEARCH SUMMARY

Title

ELECTROCHEMICAL EVALUATION OF NEW FLUOROSULFONIC AND FLUOROPHOSPHONIC ACIDS AS FUEL CELL ELECTROLYTES

Contractor

Lawrence Berkeley Laboratory

GRI contract No.

5086-260-1229

Principal Investigator

P.N. Ross

Report Period

April 1987 - April 1988

Objective

To evaluate a series of new fluorosulfonic and fluorophosphonic acid as alternative fuel cell electrolytes having superior performance than phosphoric acid.

Technical Perspective

Phosphoric acid, the electrolyte currently in use in acid H<sub>2</sub>-O<sub>2</sub> fuel cells, suffers from several limitations. It is desirable to identify new electrolytes that have electrochemical and physical properties superior to those of phosphoric acid such as faster kinetics for oxygen reduction, higher oxygen solubility and lower anion adsorption on the platinum catalyst. Moreover, they should possess high ionic conductivities, low vapor pressures, electrochemical and thermal stabilities and low contact angles with Teflon, characteristics of phosphoric acid.

Results

A number of new fluorosulfonic and fluorophosphonic acids have been evaluated as candidates for fuel cell electrolytes. Oxygen reduction data on smooth platinum

electrodes indicate that the addition of the new electrolytes to 85% phosphoric acid increases the oxygen solubility in the mixture. Solubility of  $(CF_3SO_2)_2CH_2$  n in water is quite good. Aqueous solutions of monosulfonic acids with a terminal  $SF_5$  group such as  $SF_5CHFCF_2SO_3H$ , are highly soluble in water and show high ionic conductivities, especially at elevated temperatures. The performance of the oxygen cathode of the fuel cell in 85% phosphoric acid containing 1.3%  $[HSO_3(CF_2)_2]_2O$  is superior to that of pure phosphoric acid.

Technical Approach

The procedure for the evaluation of new acids was a two stage process, the first stage being physicochemical property measurements (equivalent weight, state of hydration, conductivity of aqueous solutions) and preliminary electrochemical property measurement using cyclic voltammetry. If the results in the first stage appeared promising, further electrochemical evaluation was begun using either the purified acid by itself in pH = 1 solutions (if a sufficient quantity of acid were available) or the purified acid added to pre-purified 85% phosphoric acid, and measurement of oxygen reduction kinetics either in a rotating disk electrode (RDE) cell or in a small (1 ml) fuel cell.

Project Implications

The electrochemical evaluation and characterization of fluorinated acid electrolytes is a critical element of the advanced electrolyte research program. Significant progress has been made in purification of samples which has resulted in more meaningful electrochemical measurements. Liquid electrolyte problems still unresolved for a number of new acids evaluated include high vapor pressure and wetting of Teflon. The third year of this contract will involve continued evaluation and characterization of new compounds synthesized by GRI contractors.

GRI Project Manager

D.A. ScarpielloManager, Catalysis ResearchPhysical Sciences Department

#### INTRODUCTION:

A variety of fluorosulfonic and fluorophosphonic acids were evaluated in the last year. The procedure used in this evaluation was a two-stage process, the first stage being physical-chemical property measurements (equivalent weight, state of hydration, conductivity of aqueous solutions) and preliminary electrochemical property measurement using cyclic voltammetry. If the results in the first stage appeared promising, further electrochemical evaluation was begun using either the purified acid by itself in pH = 1 solutions (if a sufficient quantity of acid were available) or the purified acid added to pre-purified 85% phosphoric acid, and measurement of oxygen reduction kinetics either in a rotating disk electrode (RDE) cell or in a small (1 ml) fuel cell.

#### EXPERIMENTAL:

All electrolytes were prepared either with Harleco ultra-pure water or with highly pure water obtained by circulating distilled water through Milli-Q (Waters) water purification unit. Purity of newly synthesized acids was checked by recording cyclic voltammograms in dilute acid solutions having pH = 1. Different platinum electrodes and cell configurations were used in cyclic voltammetric measurements. Preliminary experiments were conducted either on a platinum cylinder electrode or on platinum flags of different sizes. The selection of a given electrode was based on the quantity of the sample supplied by the synthetic chemist. Several glass cells were fabricated in order to accommodate various solution volumes ranging from 1 to 200 milliliters. A large (compared to working electrode) platinum flag served as counter electrode. In oxygen reduction

experiments, this electrode was directly inserted into the cell solution. The potential of the working electrode was monitored with respect to a dynamic hydrogen electrode (DHE) in a separate compartment, connected to the main cell via a luggin capillary. A reversible hydrogen electrode (RHE) requiring only 0.5 ml of solution, was used for samples which were supplied in small quantities. This reference electrode was filled with the test solution and then hydrogen was electrochemically generated at the platinized platinum electrode.

In oxygen reduction kinetics measurements, two different cells and conditions were used. For purified solutions of the acids, nominally pH 1 were examined in a 200 ml glass cell. A standard Pine Instruments Pt RDE and Pine rotor were used. Measurements of acid mixtures with 85% phosphoric acid were done in a small Teflon fuel cell with 1 cm<sup>2</sup> active area commercial fuel cell Pt Electrodes (Prototech). The temperature for the fuel cell data was typically 100°C. Some acid mixture experiments were also performed in the RDE cell by adding the new acids to 0.7M or 0.1M phosphoric acid solutions.

Purity of the new acids was tested by recording a cyclic voltammogram in dilute aqueous solution (pH 1) and comparing the results with that of purified phosphoric or sulfuric acid. This was done before each of the "super acids" was tested.

A PAR 273 or Pine RDE4 potentiostat/galvanostat was used in cyclic voltammetry experiments. Rotating disk electrode and fuel cell data were collected by PAR 273 in the remote mode, using an IBM PC as the host computer.

The results of cyclic voltammetry experiments are described in the following section. All acids received for electrochemical evaluation are listed in Table 1. The geometrical areas of electrodes used:  $6.8 \text{ cm}^2$  (Figs. 2,9,12),  $3.96 \text{ cm}^2$  (Figs. 3,6,8,14),  $3.76 \text{ cm}^2$  (Figs. 10,11,13,15) and  $0.05 \text{ cm}^2$  (Actual, Figs. 4,5).

#### A- CYCLIC VOLTAMMETRY DATA:

Figure 1 illustrates the rotating cylinder electrochemical cell. The cell requires only 30 ml of solution, suitable for electrochemical evaluation of new super acids. The large ratio of surface area (6.8 cm<sup>2</sup>) to electrolyte volume was intended for minimizing the effect of impurities. Although this was true for the stationary electrode, the quality of oxygen reduction kinetics data was lower than those obtained using a rotating disk electrode.

Figure 2 shows cyclic voltammogram of Pt in purified 0.7M (pH 1) phosphoric acid solution saturated with purified nitrogen. This voltammogram was used for the comparison of Pt behavior in the new super acids. The well-defined oxide formation and reduction regions and symmetrical hydrogen adsorption-desorption peaks are typical of a solution free from any adsorbable or electroactive impurities. Cleanliness of electrode and cell assembly was also checked with 0.1N sulfuric acid. The corresponding cyclic voltammogram is shown in figure 3.

Figure 4 and 5 show the cyclic voltammograms of Pt in 0.18M solution of  $CF_3(CF_2)_2CH_2OCF_2CF_2SO_3H$  and 0.25M solution of  $CF_3CH_2OCF_2CF_2SO_3H$ , saturated with  $N_2$ , respectively. These acids were received as yellow-brown liquids of less than 1g each. These solutions had a strong odor. Significant amount of impurities were present in each acid. Considering the small quantities provided, no purification procedure was attempted.

Cyclic voltammogram of Pt in 0.016M solution of  $(CF_3SO_2)_2$   $CH_2$  is shown in Figure 6. This acid was received as a crystalline white solid. The sample was less than one gram. Cyclic voltammetry data indicates the presence of some oxidizable impurities in the solution. Because of small amount of material available, no further study was conducted.

Figure 7 shows the voltammogram of 0.1N (0.05M) solution of  $(HO_3S(CF_2)_2)_2O$  saturated with  $N_2$ . This acid was received as a viscous clear liquid. The equivalent weight was determined to be 178. Based on the molecular formula, the equivalent of an anhydrous sample would be 189. The discrepancy indicates the presence of a significant amount of a lower molecular weight acid. Cyclic voltammetric data indicate that the sample contains considerable amount of impurities. Several grams of acid were available, so a purification procedure was done.

The acid was treated with hydrogen peroxide and refluxed at 80 °C for several hours. The solution was then boiled down to a viscous liquid which solidified upon cooling to a white gelatin. A small amount of liquid was present. The equivalent weight of purified acid was measured to be 181. This indicates that some of the lower molecular weight acid has been preferentially removed, but significant amounts likely remained. Cyclic voltammogram of Pt after purification is shown in figure 8, indicating that a significant improvement has been achieved. The amount of acid left after first purification, was just enough to be used as an additive to 85% phosphoric acid for fuel cell testing. Results of the fuel cell experiments will be shown in section C.

Cyclic voltammetry of Pt in 0.05M (based on the theoretical formula weight) solution of  $(HO)_2P(O)OCH_2(CF_2)_4CH_2OP(O)(OH)_2$  is shown in figure 9. The measured pH of this solution was ca. 1.2. The solution as-prepared contained tiny droplets of "oil" which settled out after a few hours and were removed. Appearance of a peak at 0.85 V, the shapes of oxide formation/reduction waves and poor resolution of hydrogen adsorption regions are clear evidence for an impure electrolyte. No significant improvement was produced by cycling for a few hours, or by constant current electrolysis with Pt electrodes at  $5mA/cm^2$  for 2 days. While purging the solution with  $N_2$  to remove dissolved hydrogen and oxygen and recording cyclic voltammogram, a vigorous reaction started suddenly which rapidly heated the solution to ca.  $70^{\circ}C$ .

Hydrogen peroxide treatment was applied in order to purify this acid. After removing exess water, a two-phase viscous solution containing a small amount of a crystalline material was obtained. It is known that perfluorinated alkylphosphonic acids are hydrolytically unstable, specially at high temperatures, and decompose to the corresponding alcohol according to the following reaction:

Our observations can be explained on the basis of such a decomposition reaction.

Two samples of two monosulfonic acids, each containing a terminal SF5 group were supplied by Prof. Gard of Portland State University as white solids. The cyclic voltammogram of Pt in 0.1M solution of SF<sub>5</sub>CH<sub>2</sub>SO<sub>3</sub>H is shown in

Figure 10. This sample is reasonably clean and the small amount of impurities can be easily removed by hydrogen peroxide treatment. Figure 11 illustrates the voltammogram of Pt in 0.118M solution of SF<sub>5</sub>CHFCF<sub>2</sub>SO<sub>3</sub>H. Both solutions were readily dissolved in water and have high proton conductivities. More of these acids was requested for further investigations.

A sample of disulfonic acid,  $(CF_2)_6(SO_3H)_2$ , was received as a white solid. The equivalent weight of the acid as-received was determined by titration to be 535. An aqueous 0.05M solution of was prepared, having a measured pH of 1.18. The cyclic voltammetry curve for this solution is shown in Figure 12. After 48 hours of continuous cycling, the appearance of the voltammetry curves improved considerably (curve B), characteristics of removal of oxidizable impurities. The conductivity of 0.05M solution saturated with air at 90 °C was 55 mmhos, a much higher conductivity than a pH 1 solution of TFEDSA at the same conditions. This acid was considered to be promising and production of a larger quantity was requested. More data on the oxygen reduction kinetics on smooth and supported platinum electroes will be shown in subsequent sections.

There was enough of this acid, so it was purified by hydrogen peroxide treatment. The cyclic voltammogram of Pt in the purified 0.05M solution is shown in Figure 13. The current in the oxide formation region is still high indicating the presence of some impurities. It seems that this one-stage purification procedure is not sufficient enough to remove all impurities. Subsequently, we adopted a two-stage purification procedure as suggested by Case Western Reserve University. More data on this acid is presented in section B.

A long-chain monosulfonic acid,  $C_8F_{17}SO_3H$ , was received as a white powder. The equivalent weight was determined to be 533 by titration with 0.01N sodium hydroxide solution. A 50 ml 0.091N solution of this acid was prepared. The measured pH of this solution was 1.1. This solution was extremely foamy, making difficult simple procedures such as purging with nitrogen. A cyclic voltammogram of 0.091N solution of this acid is shown in Figure 14. This is one of the highest quality voltammograms which we have observed in the synthesized acids. This acid was purified by hydrogen peroxide treatment. A viscous liquid was obtained after heating the solution in order to remove the excess water. The concentration of this solution was found to be 1.2M by titration. If heating is continued, a "crsytalline liquid" is formed. Figure 15 shows the cyclic voltammogram of 0.1N solution after purification which indicates the sample is reasonably clean.

At this point in our study, only two acids in reasonable quantities, have shown both sufficiently interesting physical properties and reasonable purity to warrant further evaluation, and those are  $C_8F_{17}SO_3H$  and  $(CF_2)_6(SO_3H)_2$ . In the following section, our results on the oxygen reduction studies at smooth platinum electrodes are described. For convenience, we will refer to thes acids as  $C_8$  and  $C_6$ , respectively.

#### B: OXYGEN REDUCTION KINETICS MEASUREMENTS

All chemicals were purified with H<sub>2</sub>O<sub>2</sub> and H<sub>2</sub>-Pt black treatment as recommended by CWRU. Except for the filteration of Pt black, Teflon (PFA) bottles were used in order to minimize the solution contact with glass. A

significant improvement on the purity level of 85%  $H_3PO_4$  was observed when compared to a single-stage hydrogen peroxide treatment. In the case of  $C_8$  acid (and  $C_6$ , to a lesser extent ), some problems were encountered. The aqueous solution of this acid acts as a strong surfactant. Decomposition of hydrogen peroxide was quite slow due to the formation of a very tiny gas bubbles which continued to evolve for several days and formed a foam layer on the top of the solution.

For all measurements a rotating disk electrode (geom. area =  $0.46 \text{ cm}^2$ ) was used. The electrode was polished with alumina (final stage, 0.05 um) to a mirror finish. It was washed, degreased, cleaned in 1:1  $\text{HNO}_3/\text{H}_2\text{SO}_4$  and finally rinsed thoroughly with ultrapure water. A reversible hydrogen electrode, filled with the test solution served as the reference electrode. A platinum flag was used as counter electrode.

The activity of smooth platinum for oxygen reduction was tested in 0.1M solution solution of  $C_6$  and the results were compared to those obtained for 0.1M phosphoric acid. The electroreduction of oxygen in 85%  $H_3PO_4$  containing low concentrations of  $C_6$  and  $C_8$  has been also carried out. Cyclic voltammetry and rotating disk electrode techniques have been used to study the effect of the perfluorosulfonic acids as additives to 85%  $H_3PO_4$  on the oxygen reduction on smooth Pt.

Cyclic voltammogram of Pt in purified 0.1M phosphoric acid is shown in Fig. 16 as a reference for comparison. It has all the characteristics of an impurity-free electrolyte.

Figure 17 shows the cyclic voltammogram of Pt in a 0.1N solution of

unpurified C<sub>6</sub> acid saturated with N<sub>2</sub>. The shape of the voltammogram indicates the presence of impurities in the solution. The current in the oxide formation region is higher than expected and the hydrogen adsorption-desorption peaks are completley suppressed. A brown thin film was formed on the electrode surface when the potential was cycled between 0.02V to 1.5V for few hours. This film which was not dissolved in 1:1 HNO<sub>3</sub>/H<sub>2</sub>SO<sub>4</sub> was similar to the one reported previously when a Pt cylinder electorde with a higher surface area was used. The cyclic voltammogram of Pt in purified (twice) 0.087N solution of C<sub>6</sub> is shown in figure 18. No film formation was experinced in the purified solution indicating that this is due to the presence of impurities in the original solution. The shape of the peaks in the oxide and hydrogen adsorption-desorption regions of figure 18 are indicatives of a much cleaner solution. In figure 19 the voltammograms for the two purified acids are compared.

The oxide formation in the dilute  $C_6$  acid solution starts at a more cathodic potential and the currents for both oxide formation region and its reduction, are higher relative to dilute phosphoric acid. This is the result of the weaker adsorption of the sulfonic acid compared to phosphoric acid.

Figures 20 and 21 show the cyclic voltammograms of Pt in O<sub>2</sub>-saturated solutions of 0.1M H<sub>3</sub>PO<sub>4</sub> and 0.087N (CF<sub>2</sub>)<sub>6</sub>(SO<sub>3</sub>H) <sub>2</sub> respectively. The electrode was activated by applying potential pulses between 0.2V and 1.2V. The potential then stepped to 1.2V and scanned cathodically at 10 mV/s. The first as well as the third cycle (steady-state) is shown for each solution. Although the onset of the oxygen reduction starts at more anodic potential for sulfonic acid, the peak potential shifts in the cathodic direction and peak intensity

decreases. This might be due to the traces of impurities left in the solution. For  $H_3PO_4$  solution, the peak potential remains constant while its intensity increases upon cycling. The steady-state peak intensities are almost the same for both solutions, indicating the comparable oxygen solubilities in the dilute solutions.

Oxygen reduction experiments also were carried out in pure  $85\%~\mathrm{H_3PO_4}$  and a mixture containing  $0.45\%~(\mathrm{CF_2})_6(\mathrm{SO_3H})_2$  in 85% phosphoric acid. The corresponding cyclic voltammograms in the  $\mathrm{O_2}$  saturated  $\mathrm{H_3PO_4}$  solutions before and after the addition of C6 acid are shown in figure 22.

The polarization curves were recorded at different rotation rates as indicated in figure 23 for 85%  $\rm H_3PO_4$ . The electrode was activated by application of 5 pulses (20 sec.) between 0.2V and 1.5V, then the potential stepped to 1.0V and I-E curves recorded at 10 mV/s in the cathodic direction. The slight increase observed in the limiting disk currents at E < 0.35V results from initial adsorption of hydrogen as can be seen in figure 22.

After recording I-E curves in 85% H<sub>3</sub>PO<sub>4</sub>, solid C6 acid was added to the cell. The concentration of C<sub>6</sub> acid was found to be 0.45%. The low concentration was chosen because the solubility of C6 acid in 85% H<sub>3</sub>PO<sub>4</sub> is quite low and foam formation at higher concentrations makes the measurement less reliable. The mixture was purged with oxygen overnight at a low rate due to formation of foam bubbles. As figure 22 shows, there is no significant difference upon the addition of C<sub>6</sub> to H<sub>3</sub>PO<sub>4</sub> at this low concentration. Polarization curves for oxygen reduction in the mixture were recorded following the same procedure described for H<sub>3</sub>PO<sub>4</sub>. It can be seen that limiting currents for the mixture in figure 24 are higher at all rotation rates in the presence of C<sub>6</sub> acid. This is due to the higher

oxygen solubility in the mixture relative to 85% phosphoric acid.

On the other hand, the onset of oxygen reduction in the mixture coincides with that of pure phosphoric acid and no cathodic shift in the reduction potential is observed as might be expected with an enhancement in kinetics.

We also examined the effect of on the kinetics of oxygen reduction in 0.7M phosphoric acid with the RDE. In particular, we wanted to see if were an increase in the limiting current with  $C_8$  addition, indicative of higher oxygen solubility. Figures 25 and 26 compare the results in purified phosphoric acid after addition of the as-received  $C_8$  to a level of 0.01M. Formation of huge amount of foam makes the measurement unreliable at high rotation rates. Although the limiting currents are not much different at low rotation rates, the kinetics currents are clearly lower in the mixture. Similar results were obtained when a small amount of purified  $C_8$  was added to 85% phosphoric acid.

Oxygen reduction kinetics in a purified 85% phosphoric acid solution was compared with that of C<sub>8</sub> acid as an additive (0.42%) to phosphoric acid. The corresponding voltammograms are shown in figure 27. The currents in the Pt oxidation and reduction regions are higher in the mixture. The oxygen solubility in 85% H<sub>3</sub>PO<sub>4</sub> increases upon addition of C<sub>8</sub>. This can be easily seen by comparing the magnitude of the limiting current at 400RPM in the polarization curves shown in figures 28 and 29. Formation of foam bubbles which forces the solution out of cell makes the measurements at higher rotation rates unreliablie. Therefore, polarization curves for the mixture were recorded at 100 and 400 RPM. Although the limiting current is higher for the mixture at 400 RPM, the oxygen

reduction potentials have been shifted quite significantly to more cathodic potentials, even though  $C_8$  concentration in the mixture is low. The same phenomenon has been previously observed in 0.7M  $H_3PO_4$  solution containing 1% C8 acid. Due to the availability of small quantity of purified  $C_8$  acid, it was used as an additive.

#### C- FUEL CELL MEASUREMENTS

Fuel cell experiments were conducted in a small Teflon cell. Electrodes were high surface area standard gas diffusion (Prototech) with 1 cm<sup>2</sup> active area. Polarization curves were recorded at 100 °C using pure hydrogen and oxygen at atmospheric pressure.

The effect of  $C_8F_{17}SO_3H$ , as additive to 85% phosphoric acid, on the performance of the fuel cell cathode was investigated for mixtures containing 0.5% to 25% of the as-received monosulfonic acid. It was not possible to collect any meaningful data in the concentration range of 2% to 25%. The oxygen reduction reaction became mass-transport controlled immediately after the application of a galvanostatic pulse, even at low current densities. At the same time, the cell resistance increased from 1.6 ohm in pure phosphoric acid to 2.6 ohm for the 25% sulfonic acid in the mixture. By lowering the concentration of  $C_8$  to 0.5%, a measurable gain in potential was observed, when a galvanostatic sweep of 2 mA/sec was applied to the cell.

The I-E curves are shown in Figure 30. Cell potentials were corrected for IR drop by measuring the cell resistance using either a Wayne Kerr bridge or current interrupt technique. Increasing the sulfonic acid concentration to 1% in

the mixture resulted in an increase in the cathode polarization.

The fuel cell performance was deteriorating with time, which was probably due to the flooding of the electrode structure. Additional experiments were performed in purified solutions but similar problems were experienced. No reliable data could be collected when purified 45% C<sub>8</sub> was introduced into the cell, because of continuous drifting of the cell potential. The cell resistance started to increase with time and would reach as high as 250 ohms. Addition of fresh acid would decrease the cell resistance for a short period of time. Titration of the "gel" remained in the cell after few hours of operation indicated loss of water from the cell which, in turn, resulted in a lower conductance. A layer of detergent was found on the gas side of the oxygen cathode as the result of wetting of the the Teflon structure of the electrode.

Solubility of the  $C_6$  acid in water is quite low (0.1M) and its aqueous solutions are not suitable for fuel cell testing at high temperatures. The results of fuel cell measurements for a 1% solution of  $C_6$  in 85% phosphoric acid were not different from the data collected in pure 85%  $H_3O_4$ , within the experimental error. Figure 31 shows the current-potential data in the range of 0.01 to 100 mA, collected point-by-point in 85% phosphoric acid containing 2% disulfonic acid. It indicates that addition of  $C_6$  to phosphoric acid slightly lowers the fuel cell performance. More experiments will be conducted for lower sulfonic acid concentration in the mixture.

Figure 32 shows the polarization data for oxygen reduction in purified phosphoric acid containing 1.3% [HSO<sub>3</sub>(CF<sub>2</sub>]<sub>2</sub>O. The cathode polarization is lower by about 10 mV at currents greater than 1 mA. There was not enough

sample available to study the fuel cell performance of the pure acid or as additive to phosphoric acid at other concentrations. Synthesis of more acid was requested.

#### D: CONDUCTIVITY MEASUREMENTS

Specific conductivities have been measured for a number of new acids using a Wayne Kerr Autobalance Universal Bridge B642, over a temperature range between 25 to 90 °C. Temperature of air saturated solutions was controlled to + 0.5 °C using a water bath. The measured conductivity data for 0.05 M (pH 1) solutions of  $(CF_2)_6(SO_3H)_2$  and  $[(OH)_2P(O)OCH_2(CF_2)_2]_2$  are shown in Figure 33. The conductivity of the latter acid is much lower compared to phosphoric acid in the whole temperature range studied. The disulfonic acid solution has higher conductivities than phosphoric acid at temperatures above 70 °C. Comparison of the conductivity data for two monosulfonic acids having a terminal SF<sub>5</sub> group and a symmetrical disulfonic acid with an ether linkage are illustrated in figure 34. Both mono- and disulfonic acids have higher conductivities than phosphoric acid at high tempratures. A 0.12N solution of SF<sub>5</sub>CHFCF<sub>2</sub>SO<sub>3</sub>H has the highest conductivity, at elevated temperatures, among all acids studied.

#### CONCLUSIONS

Electrochémical evaluation of a variety of new fluorosulfonic and fluorophosphonic acids have been conducted. The experimental results should be used as guidelines for the synthesize of new acids. The acids tested, in general, have higher oxygen solubilities compared to phosphoric acid. However, long-chain monosulfonic acids such as  $C_8F_{17}SO_3H$  are not suitable as fuel cell electrolytes

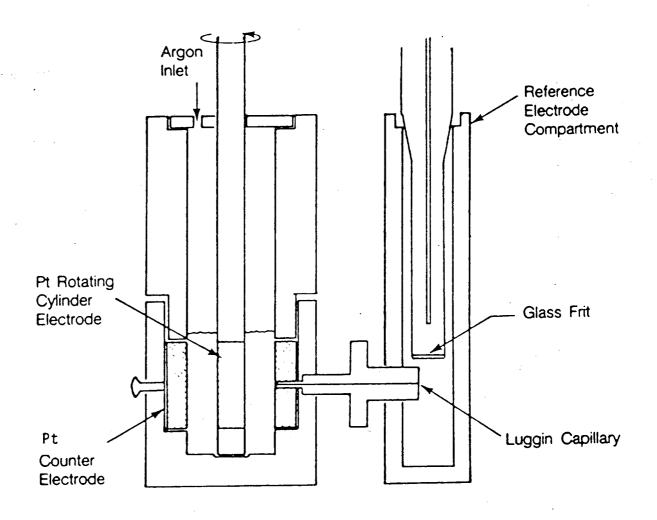
due to their tendency to wet the Teflon structure of the gas diffusion electrodes. Flooding of the fuel cell electrodes has been experienced with several acids having a terminal CF<sub>3</sub> group. Disulfonic acids of the type (HSO<sub>3</sub>)<sub>2</sub>(CF<sub>2</sub>)<sub>n</sub> do not wet Teflon. On the other hand, the vapor pressures of acids containing a few CF<sub>2</sub> groups are high and increasing the fluoroalkyl chain-length in order to lower vapor pressure, results in a decrease in their water solubilities.

A disulfonic acid,  $[HSO_3(CF_2)_2]_2O$  containing an ether linkage, shows high water solubility and superior activity for oxygen reduction compared to phosphoric acid when it is used as an additive. Short-chain mono sulfonic acids containing a terminal  $SF_5$  group have high conductivities and good water solubilities. Reasonable quantities of these acids are needed to fully investigate their usefulness as fuel cell electrolytes.

### TABLE 1

## LIST OF NEW ACIDS RECEIVED FOR TESTING

- 1. Professor G. Gard, Portland State University
  - a) C<sub>8</sub>F<sub>17</sub> SO<sub>3</sub>H
- b) (CF<sub>3</sub>SO<sub>2</sub>)<sub>2</sub> CH<sub>2</sub>
  - c)  $(CF_2)_6(SO_3H)_2$
  - d)  $SF_5CH_2SO_3H$  .  $H_2O$
  - e)  $SF_5CHF CF_2SO_3H \cdot H_2O$
- 2. Professor J. Shreeve, University of Idaho
  - a)  ${\rm HO_3S(CF_2)_2~O(CF_2)_2~SO_3H}$
  - b)  $CF_3CH_2O(CF_2)_2 SO_3H$
  - c)  $CF_3(CF_2)_2$   $CH_2O(CF_2)_2$   $SO_3H$
  - d)  $(H0)_2P(0)OCH_2$   $(CF_2)_4$   $CH_2O(0)P(OH)_2$
- 3. Professor D. Des Marteau, Clemson University
  - a)  $C_4F_9S0_2N(H)S0_2CF_3$
  - $\cdot$  b)  $(CF_3SO_2N(H)SO_2CF_2CF_2)_2$



XBL 854-2323

Fig. 1
Rotating Cylinder Electrochemical Cell.

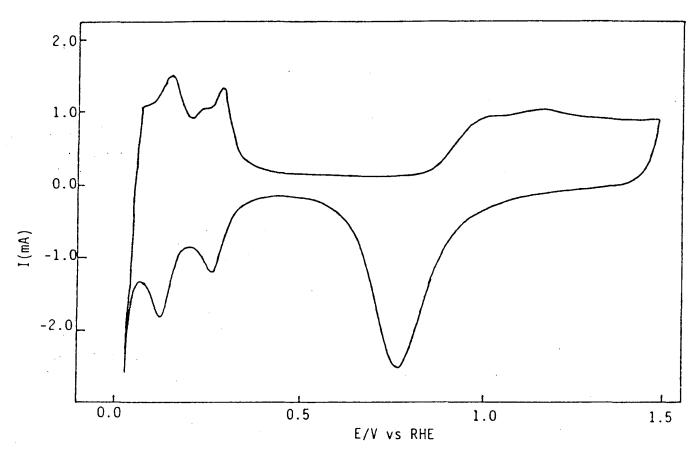


Fig. 2. Cyclic voltammogram of Pt in purified 0.7M  ${
m H_3PO_4}$  saturated with  ${
m N_2}$ . Scan rate = 100 mV/sec.

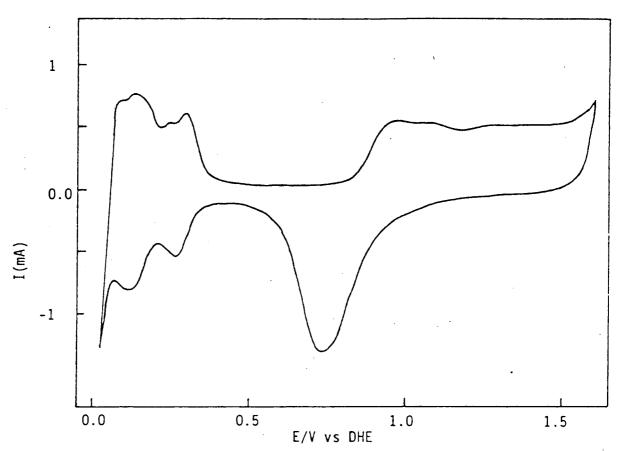


Fig. 3. Cyclic voltammogram of Pt in 0.1M  $\rm H_2SO_4$  saturated with  $\rm N_2$ . Scan rate = 100 mV/sec.

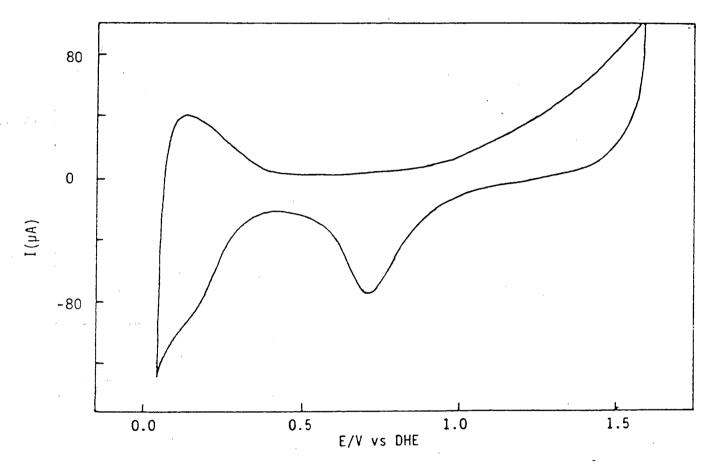


Fig. 4. Cyclic voltammogram of Pt in  $0.18 \text{M} \text{ CF}_3(\text{CF}_2)_2 \text{CH}_2 \text{O} \text{ CF}_2 \overline{\text{CF}}_2 \text{SO}_3 \text{H}.$ 

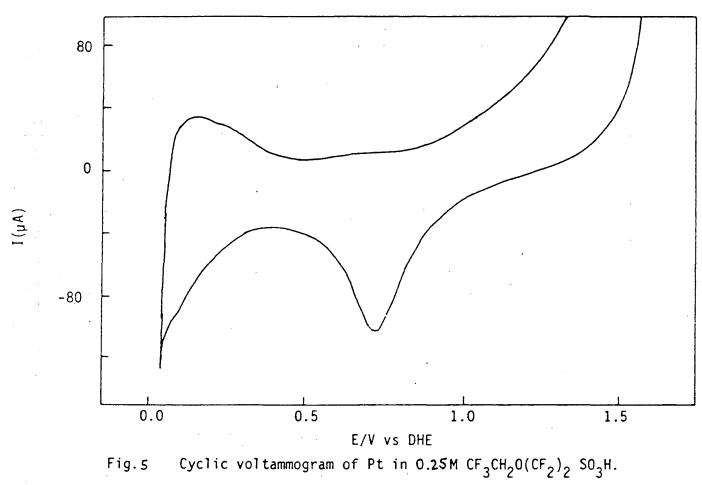


Fig. 5

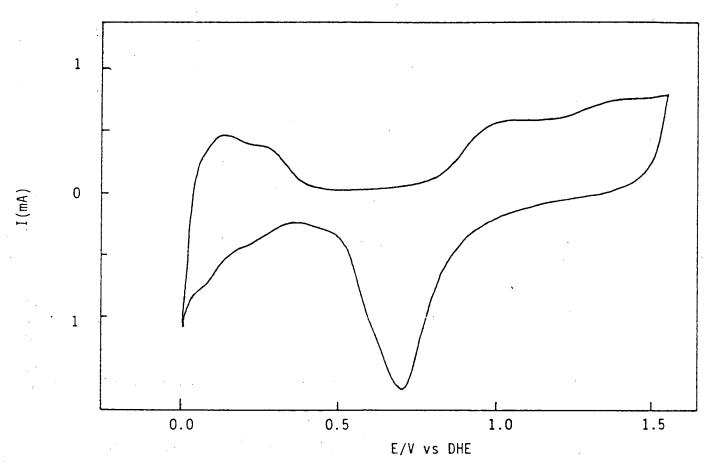


Fig. 6. Cyclic voltammogram of Pt in 0.016M  $(CF_3SO_2)_2CH_2$ .

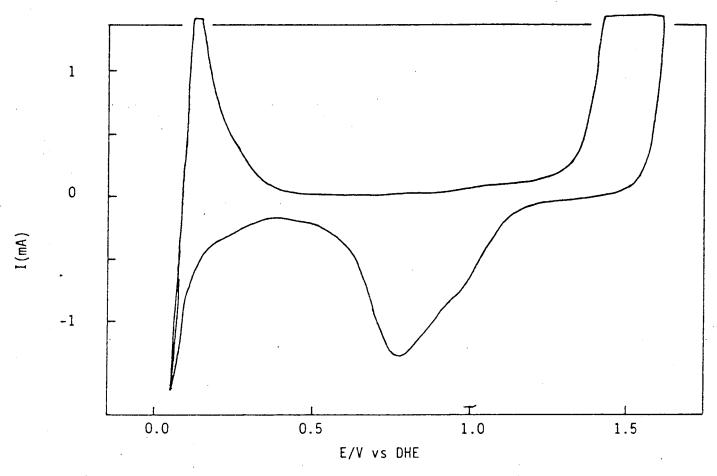


Fig. 7. Cyclic voltammogram of Pt in 0.05M  $(HSO_3(CF_2)_2)_20$ .

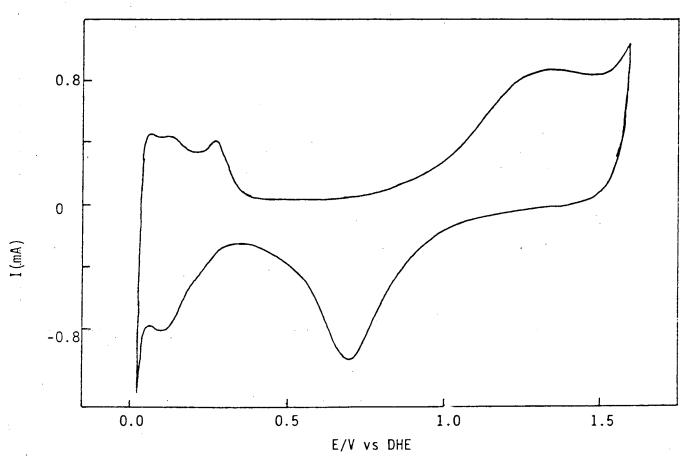


Fig. 8. Cyclic voltammogram of Pt in 0.05M  $({\rm HSO_3(CF_2)_2})_2$ 0 after  ${\rm H_2O_2}$  treatment.

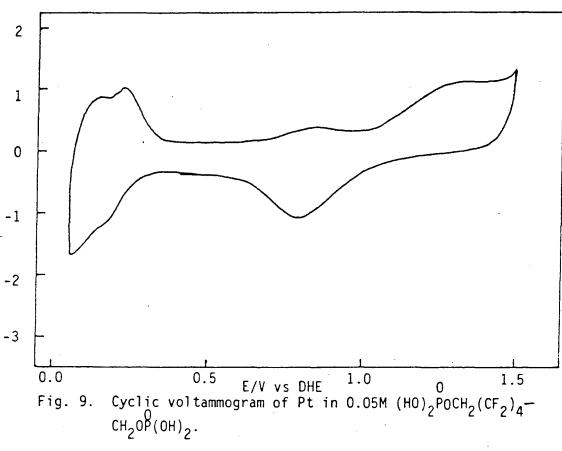


Fig. 9.

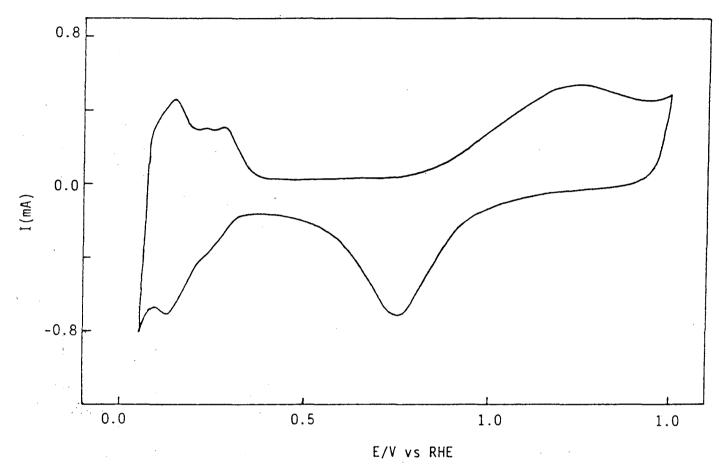


Fig. 10. Cyclic voltammogram of Pt in 0.1M  $\rm SF_5$   $\rm CH_2SO_3H \cdot H_2O$ .

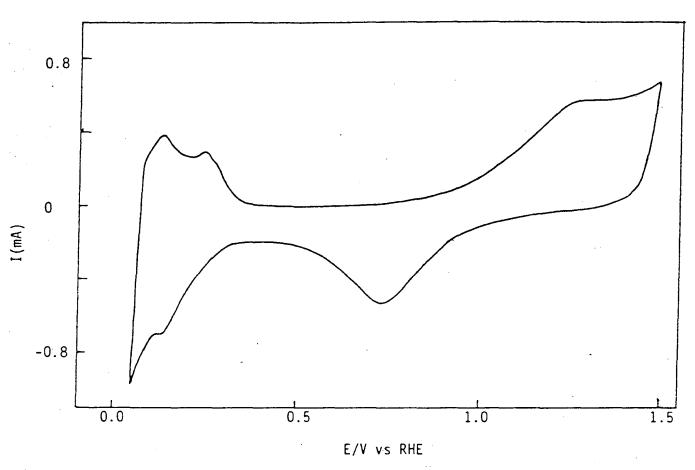


Fig. 11. Cyclic voltammogram of Pt in 0.118M  $\mathrm{SF_5CHFCF_2}$   $\mathrm{SO_3H.}$   $\mathrm{H_2O.}$ 

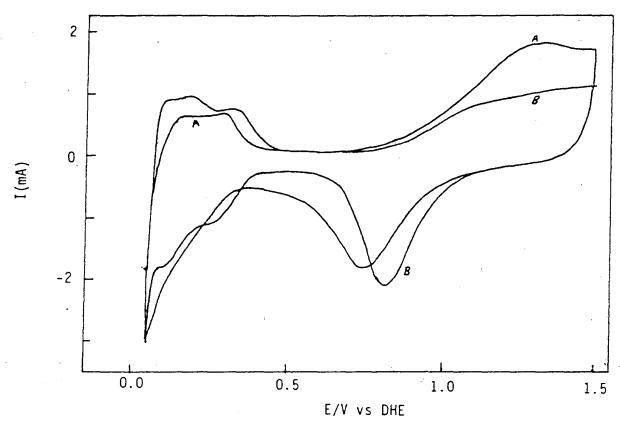


Fig. 12. Cyclic voltammogram of Pt in 0.05M  $(CF_2)_6$   $(SO_3H)_2$  (A), and after 48 hours of continuous cycling the electrode potential (B).

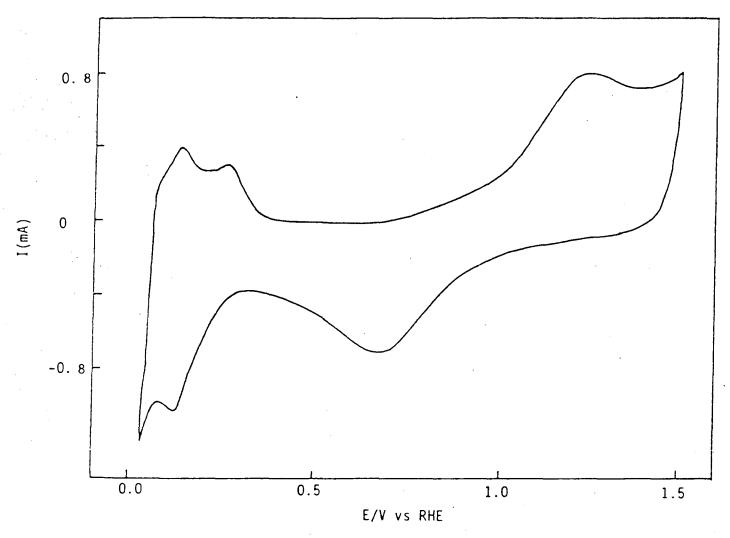
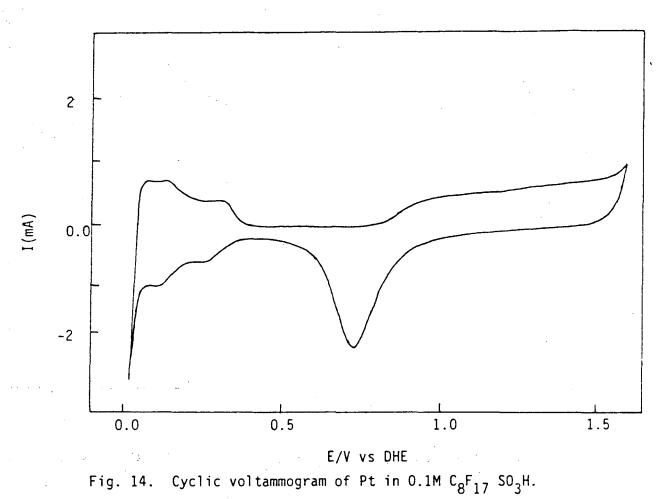


Fig. 13. Cyclic voltammogram of Pt in 0.05M  $({\rm CF_2})_6$   $({\rm SO_3H})_2$  after  ${\rm H_2O_2}$  treatment.



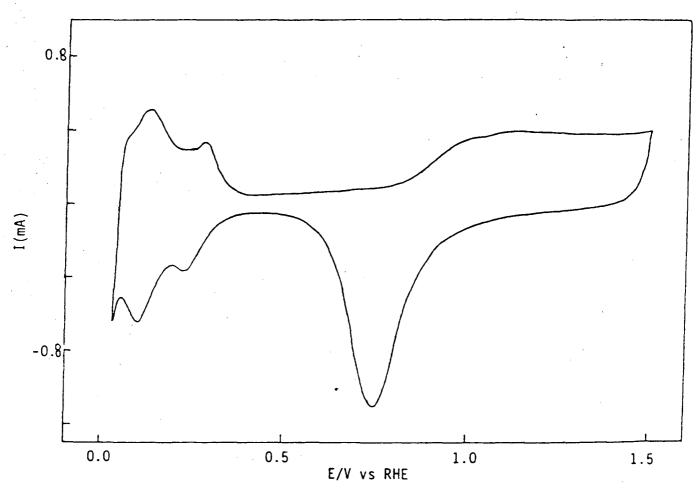


Fig. 15. Cyclic voltammogram of Pt in 0.1M  ${\rm C_8F_{17}~SO_3H~after~H_2O_2}$  treatment.

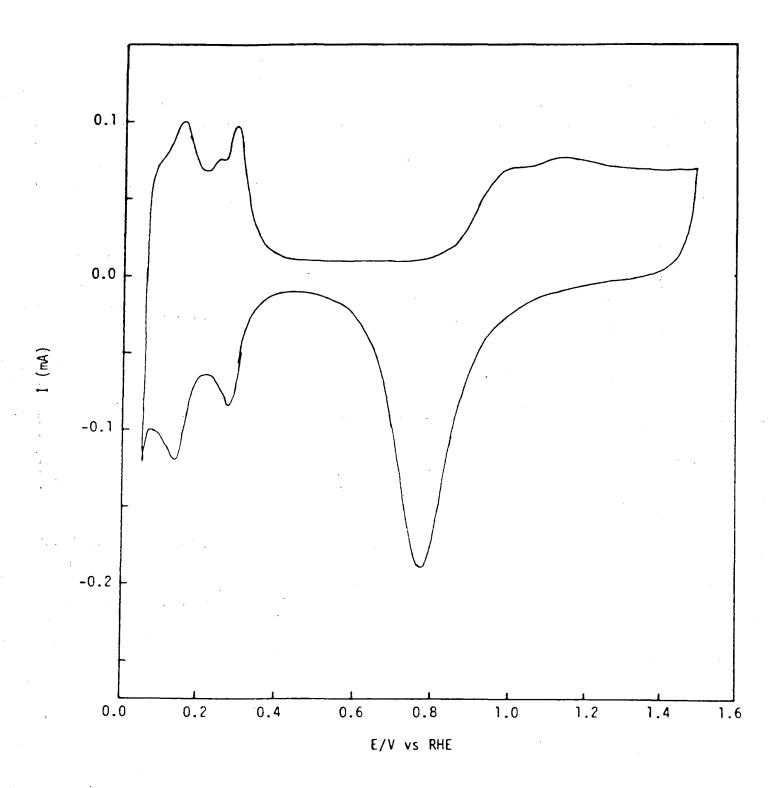


Figure 16 Cyclic voltammogram of Pt in 0.1M  $\rm H_3PO_4$  saturated with  $\rm N_2.$  scan rate: 100 mV/sec

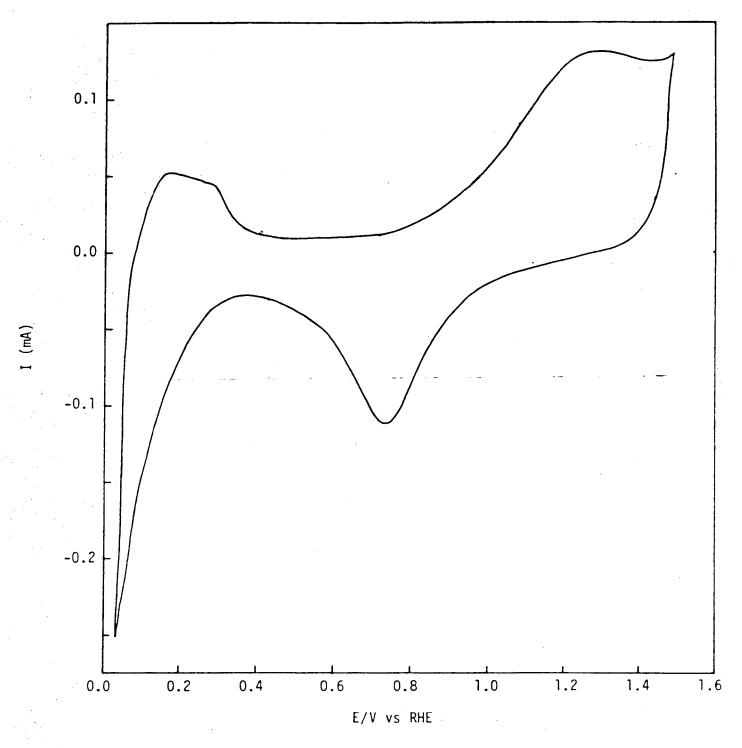


Figure 17 Cyclic voltammogram of Pt in 0.1N (CF $_2$ ) $_6$ (SO $_3$  H) $_2$  saturated with N $_2$  before purification, scan rate: 100 mV/sec

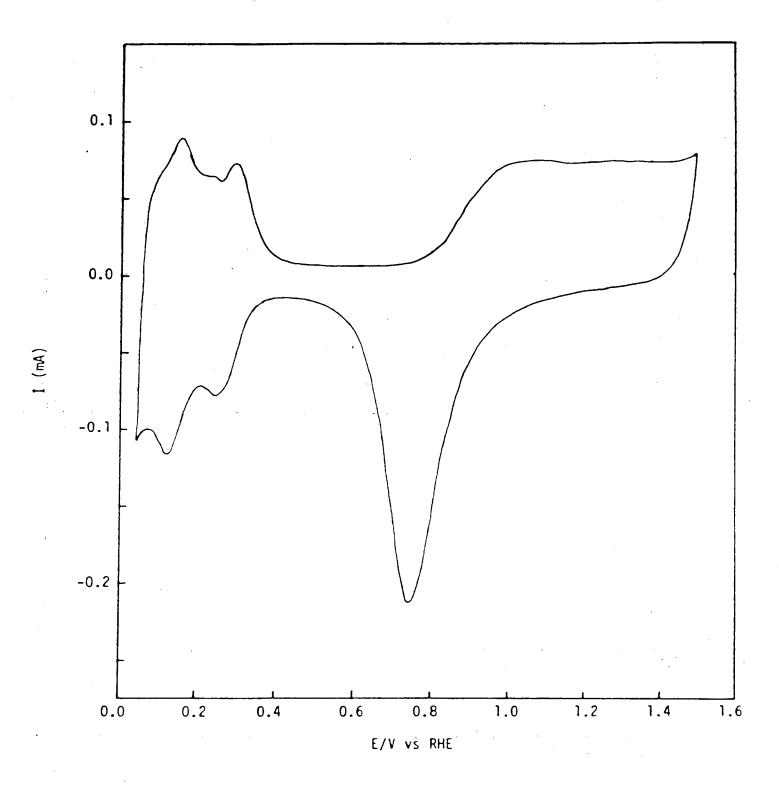


Figure 18 Cyclic voltammogram of Pt in 0.087N (CF  $_2)_6 \ ({\rm SO_3H})_2$  saturated with N  $_2$  after purification, scan rate; 100 mV/sec

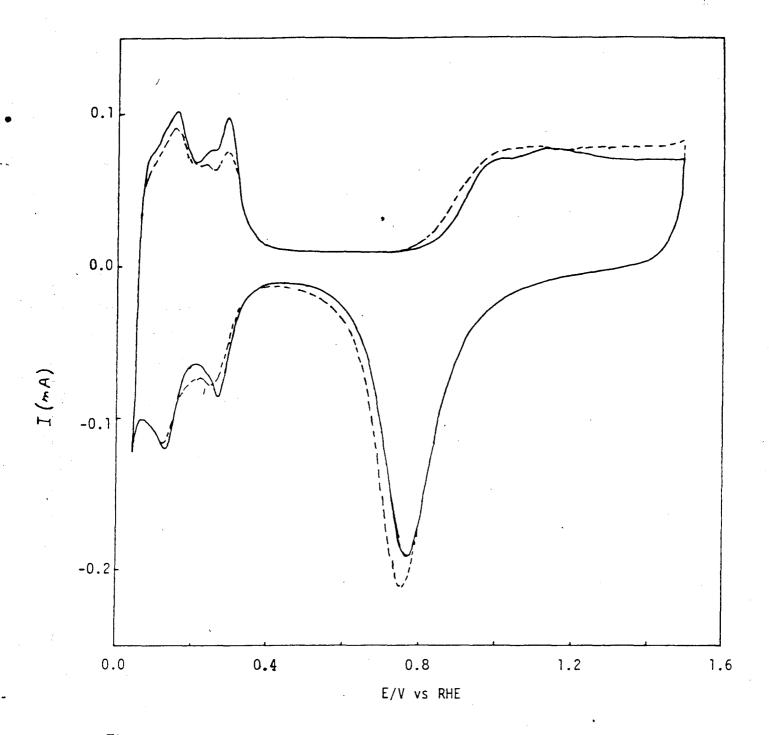


Figure 19 Cyclic voltammograms of Pt in 0.1M  $H_3PO_4$  (----) and 0.087N  $(CF_2)_6(SO_3H)_2$  (-----) saturated with  $N_2$  scan rate: 100 mV/sec

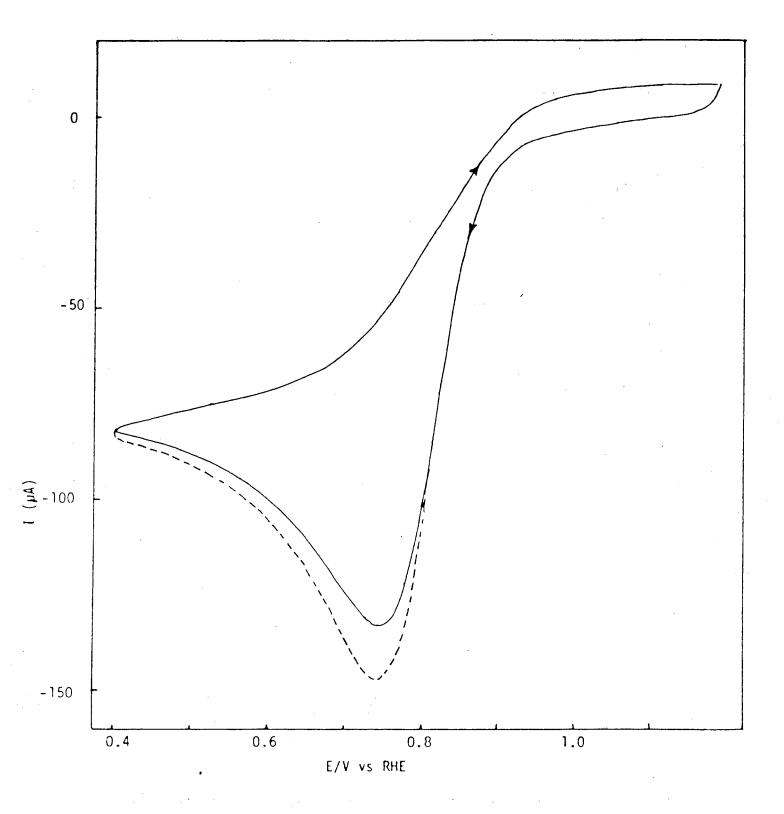


Figure 20 Cyclic voltammogram of Pt in 0.1M  $H_3PO_4$  solution saturated with  $O_2$ :

Scan rate = 10 mV/sec

first cycle ----- third cycle

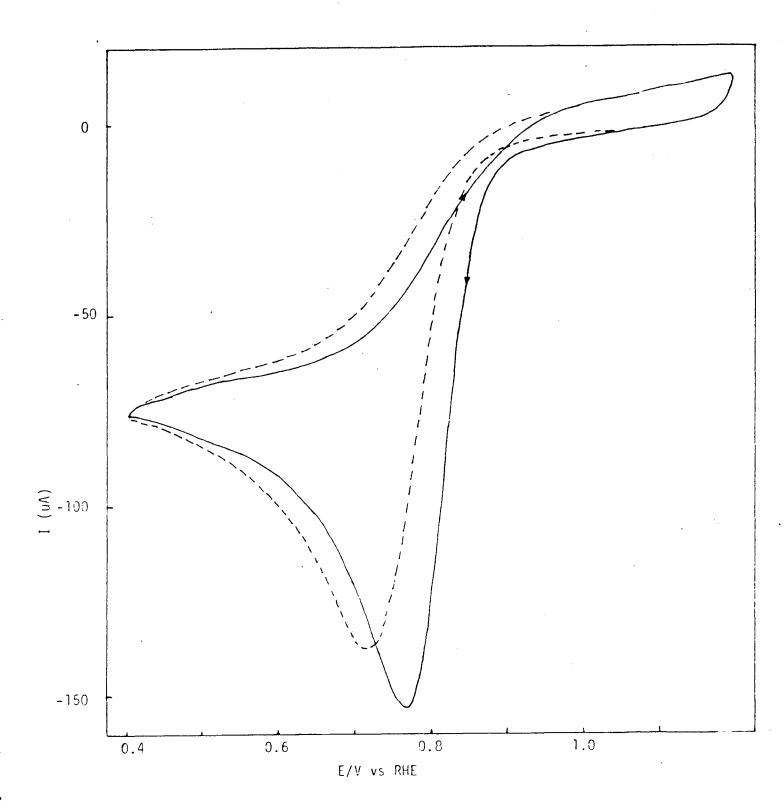


Figure 21 Cyclic voltammogram of Pt in 0.087N (CF $_2$ ) $_6$  (SO $_3$ H) $_2$  saturated with O $_2$ .

scan rate: 10 mV/sec

first cycle

----- third cycle

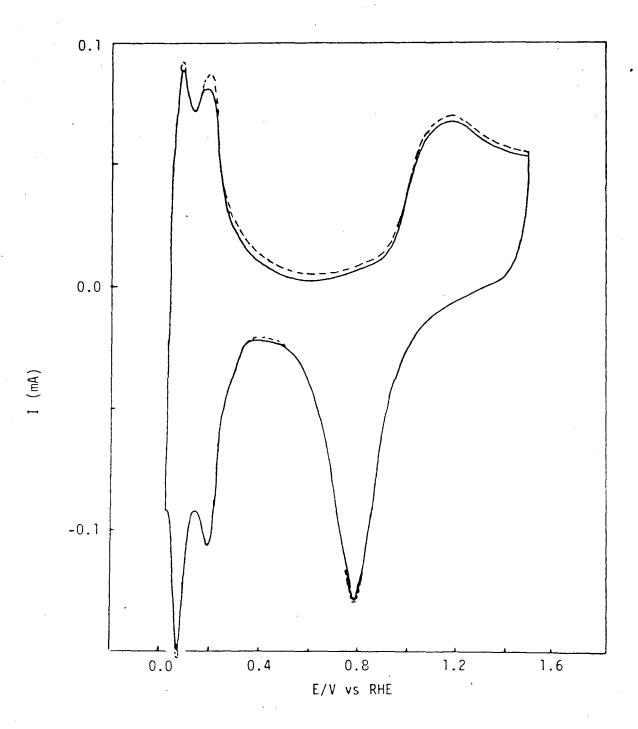


Figure 22 Cyclic voltammograms of Pt in O<sub>2</sub>-saturated solutions of 85%  $\rm H_3PO_4$  before (-----) and after addition of  $\rm (CF_2)_6(SO_3H)_2$  (-----). Scan rate: 100 mV/sec

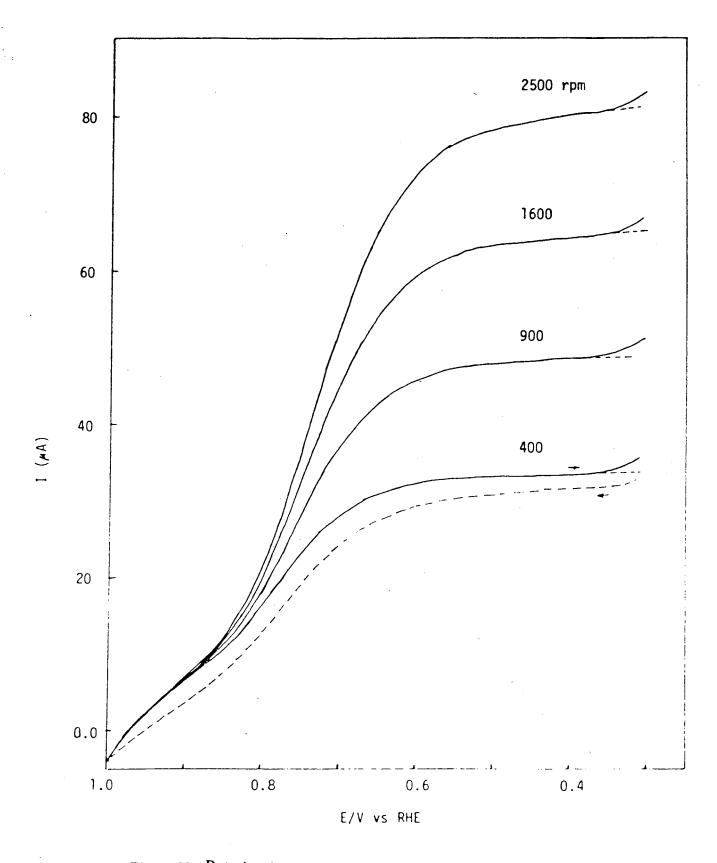


Figure 23 Rotating disk data for  $O_2$  reduction on Pt in 85%  $H_3PO_4$ . scan rate: 10 mV/sec

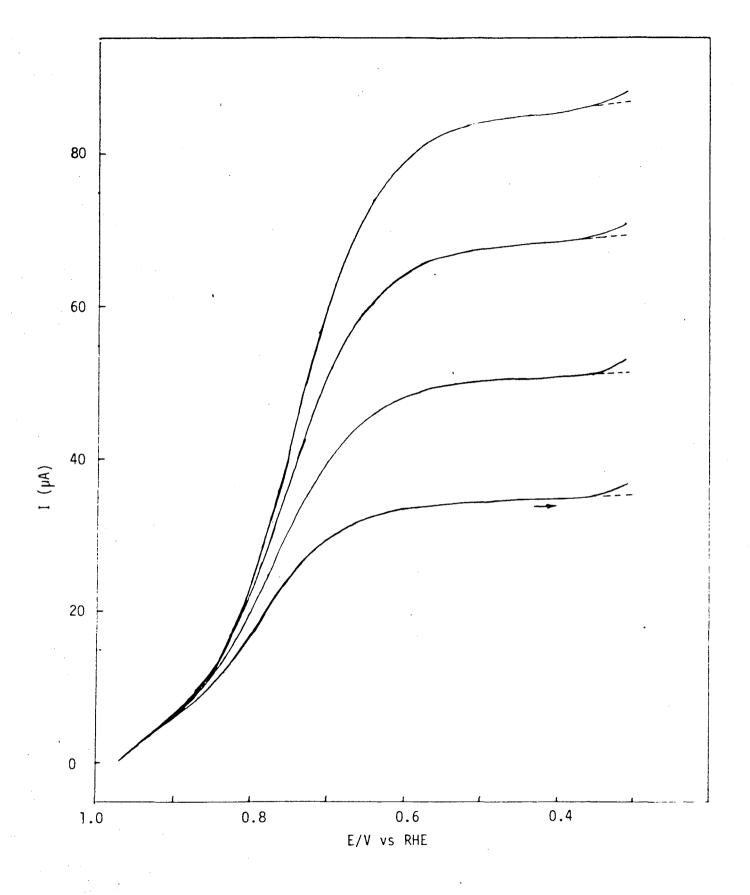
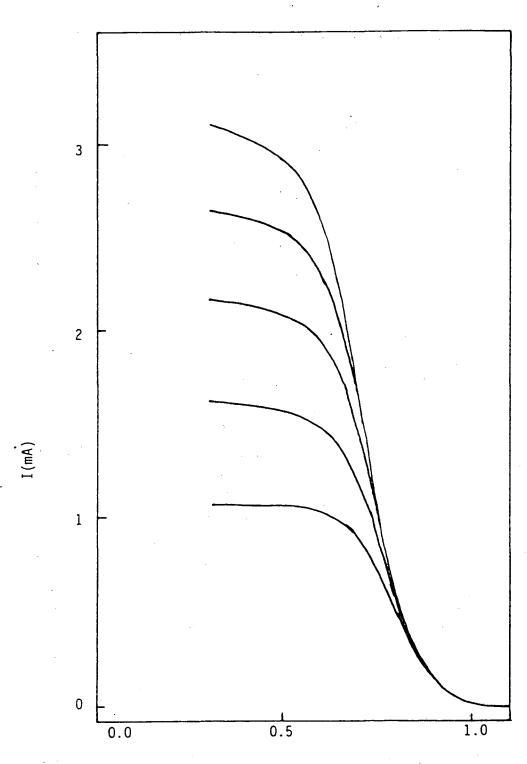
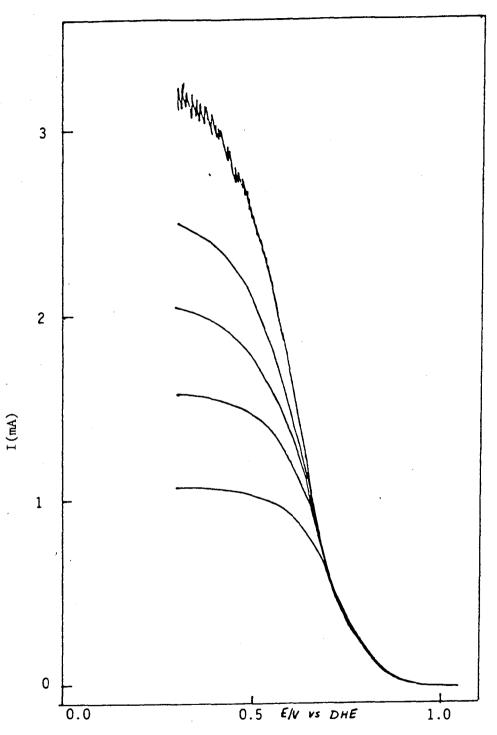


Figure 24 Rotating disk data for  $O_2$  reduction on Pt in 85%  $H_3PO_4$  solution containing 0.45%  $(CF_2)_6(SO_3H)_2$ . Scan rate: 10 mV/sec.



 $_{\rm Figure~25}$  Oxygen reduction on Pt rotating disk electrode in 0.7M  $\rm H_3PO_4$  . Scan rate 10 mV/sec.



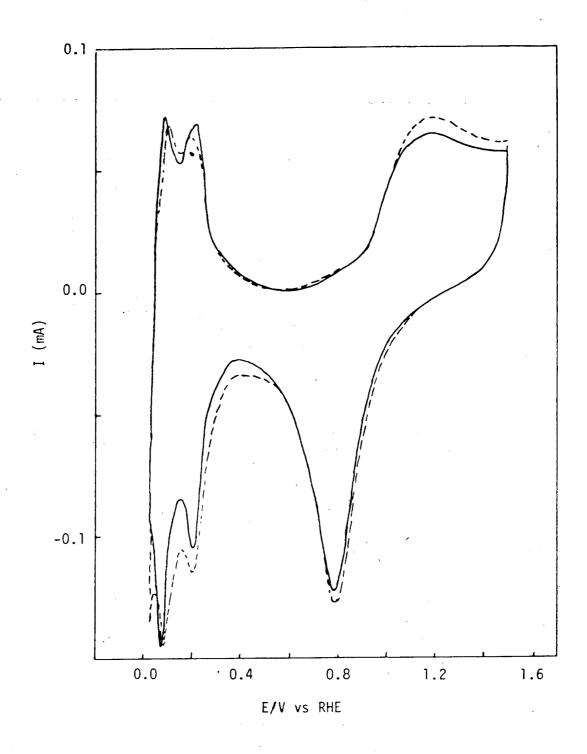


Figure 27 Cyclic voltammograms of Pt in 85%  $H_3PO_4$  (——) and 85%  $H_3PO_4 + 0.45\%$   $C_8F_{17}SO_3H$  (-----) solutions saturated with  $N_2$ . Scan rate: 100 mV/sec.

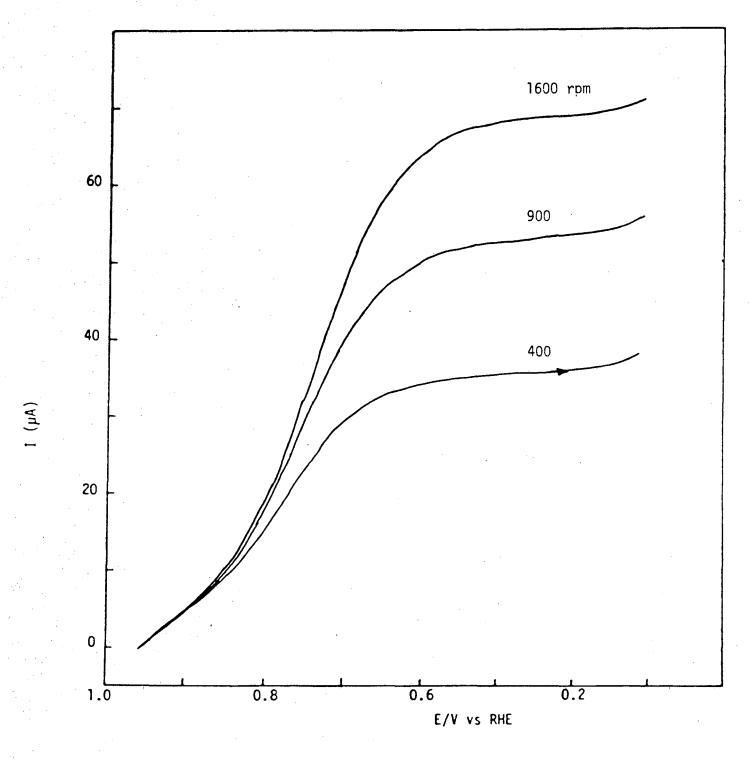


Figure 28 Rotating disk data for  $O_2$  reduction in 85%  $H_3PO_4$ . Scan rate: 10 mV/sec.

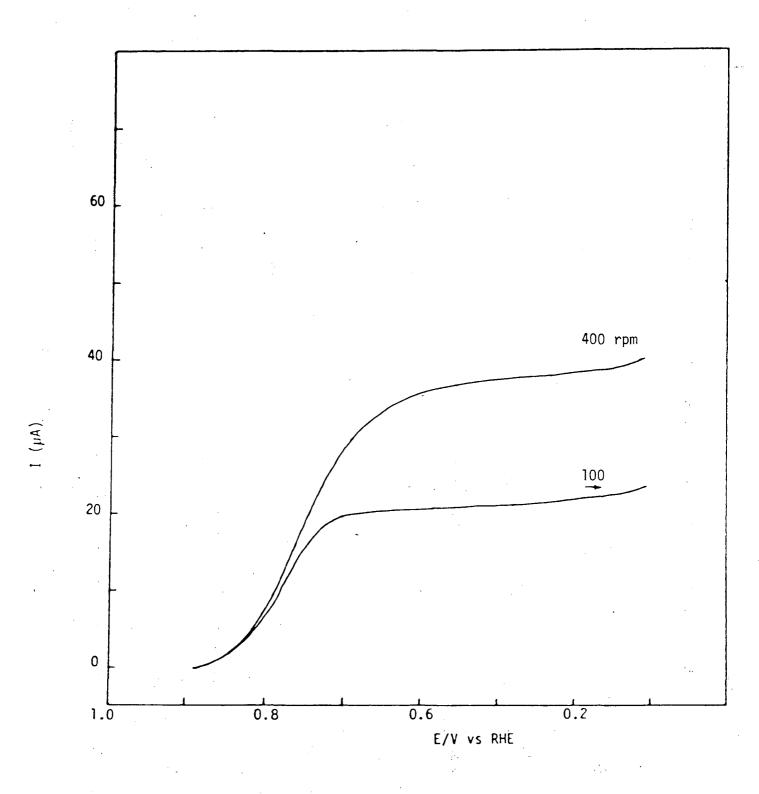
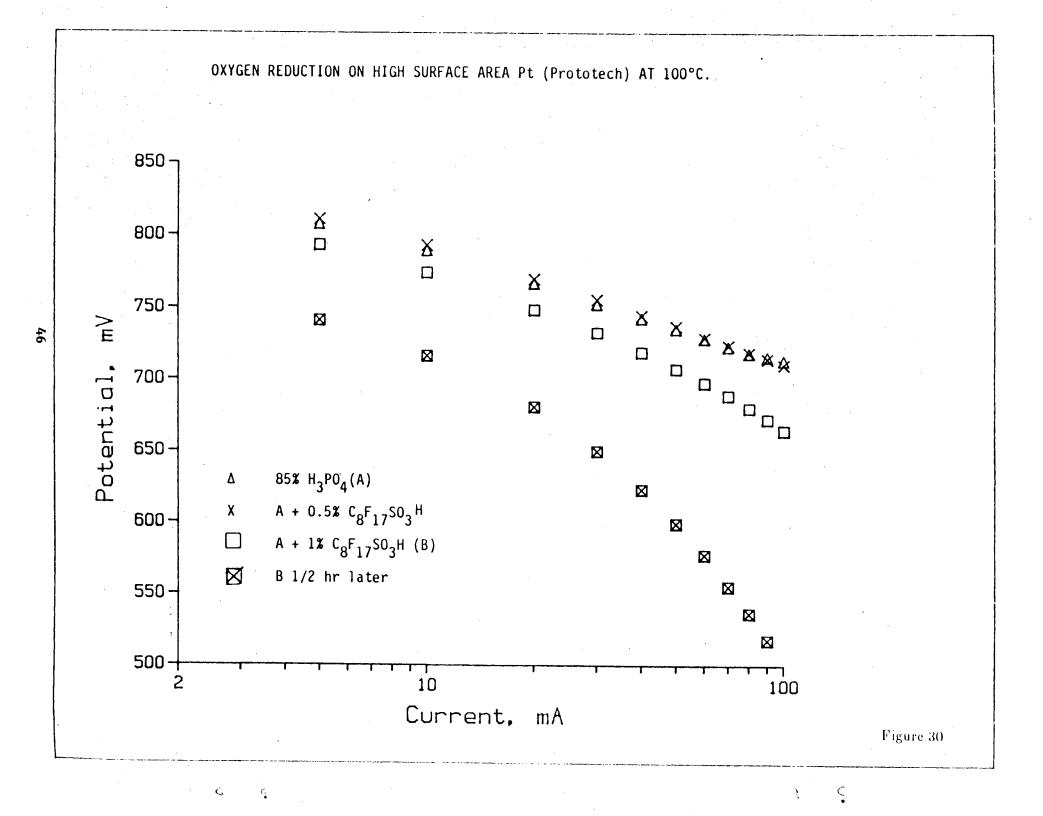
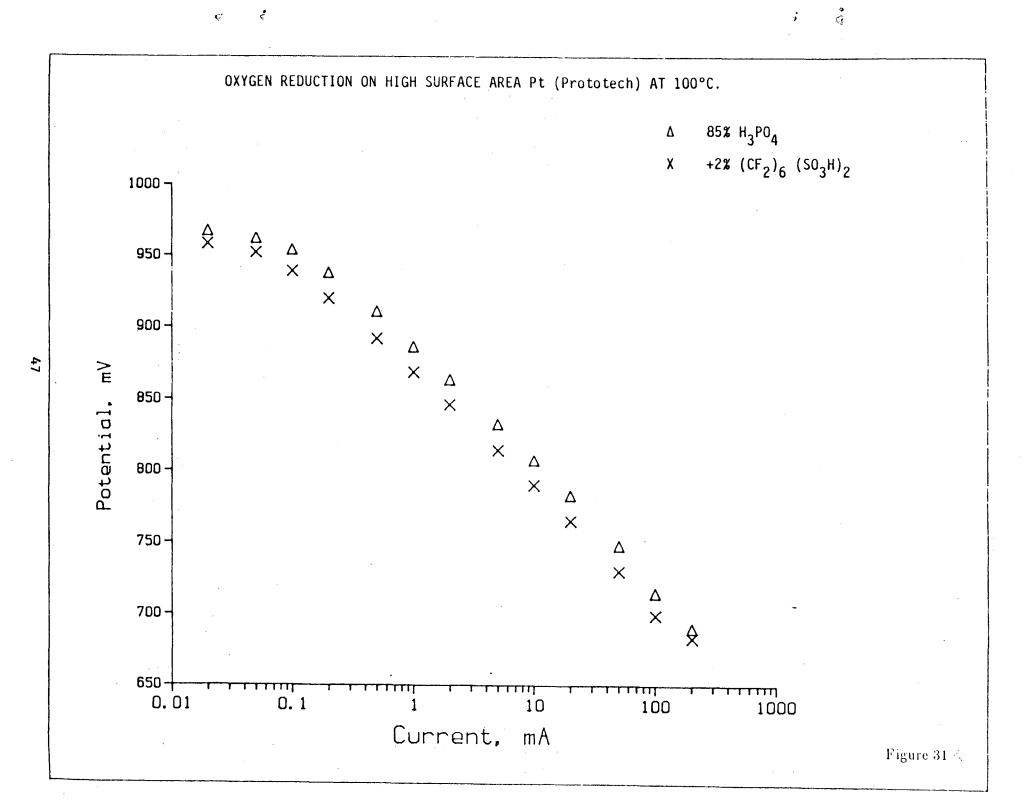


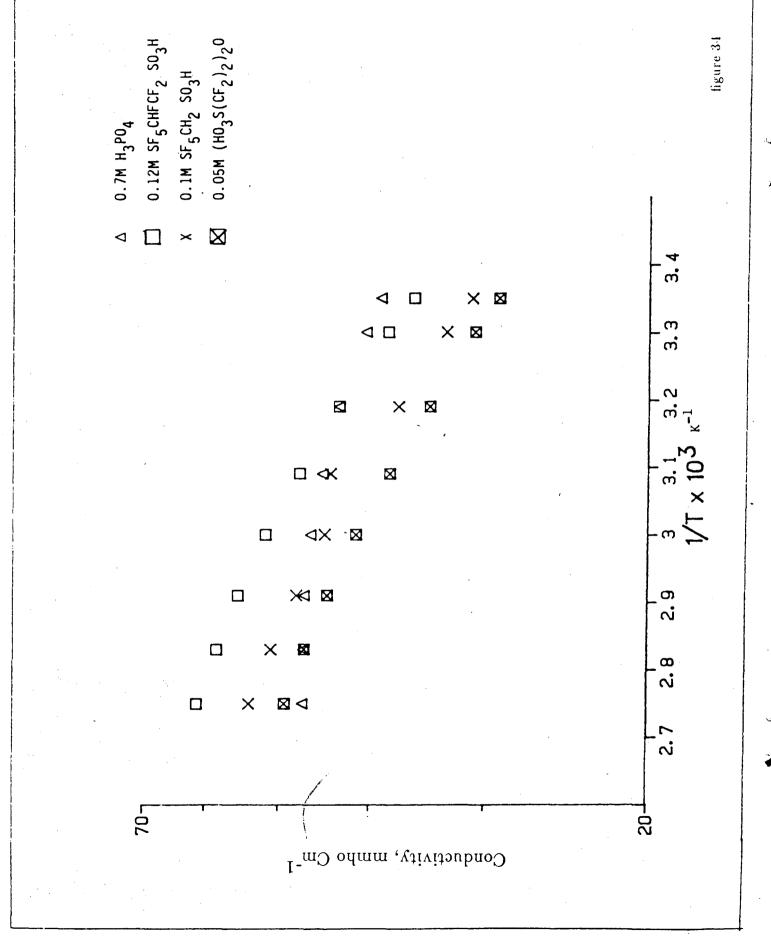
Figure 29 Rotating disk data for O2 reduction in 85%  ${\rm H_3PO_4}$  solution containing 0.42%  ${\rm C_8F_{17}SO_3H}$ . Scan rate: 10 mV/sec.





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