

# 1 **Water content of carbon dioxide at hydrate forming conditions**

2 Jonathan D. Wells<sup>a</sup>, Ahmad A.A. Majid<sup>a,b</sup>, Jefferson L. Creek<sup>a</sup>, E. Dendy Sloan<sup>a</sup>,

3 Sharon E. Borglin<sup>c</sup>, Timothy J. Kneafsey<sup>c</sup>, and Carolyn A. Koh<sup>a\*</sup>

4 <sup>a</sup> Center for Hydrate Research, Chemical and Biological Engineering

5 Department, Colorado School of Mines, Golden, Colorado 80401, USA. Email:

6 [ckoh@mines.edu](mailto:ckoh@mines.edu)

7 <sup>b</sup> Faculty of Chemical & Natural Resources Engineering, Universiti Malaysia

8 Pahang, Malaysia

9 <sup>c</sup> Lawrence Berkeley National Laboratory, 1 Cyclotron Rd, Berkeley, CA

10 94720, USA

11

## 12 **Abstract**

13        There is an interest to ensure sub-saturated water content in lines  
14 containing carbon dioxide in applications such as enhanced oil recovery and  
15 carbon sequestration, to reduce risks of hydrate blockage and corrosion. The  
16 water content of carbon dioxide at various temperature and pressures has  
17 been measured in the past, but there is no consistent set of measurements  
18 that could be used for carbon dioxide storage and transportation design  
19 work. The solubility of water in a carbon dioxide rich gas phase at hydrate  
20 forming conditions was measured in this work. Pressures ranged from 12.06  
21 to 29.30 bar along two isotherms, 1°C and -7°C, all within the gaseous

22 carbon dioxide and hydrate stability zone. For the first time in these types of  
23 measurements, the solid phase was also characterized and confirmed to be  
24 carbon dioxide hydrate via X-ray computed tomography, simultaneous with  
25 water content measurements of the gas phase. Once carbon dioxide hydrate  
26 conversion had reached a maximum value (65% estimated by X-ray  
27 computed tomography), the equilibrium water content was measured. Prior  
28 to reaching this maximum carbon dioxide hydrate conversion, the water  
29 content in carbon dioxide was observed to decrease as liquid water  
30 converted to carbon dioxide hydrate. This slow conversion to hydrate,  
31 metastability of the hydrate phase, or unexpected phases may be  
32 responsible for the large discrepancy between prior data sets for similar  
33 carbon dioxide water content measurements.

#### 34 **Keywords**

35 Carbon dioxide, clathrate hydrate, water content, metastability, X-ray  
36 Computed Tomography

#### 37 **1. Introduction**

38 Various applications, like enhanced oil recovery and carbon  
39 sequestration, depend on flowing nearly pure carbon dioxide through lines.  
40 With anthropogenic carbon emissions on the rise every year, there are lots of  
41 efforts being made to remove carbon dioxide from the atmosphere before  
42 irreversible damage is done.[1-4] While there are various techniques for  
43 capturing carbon dioxide from the atmosphere into a concentrated stream so

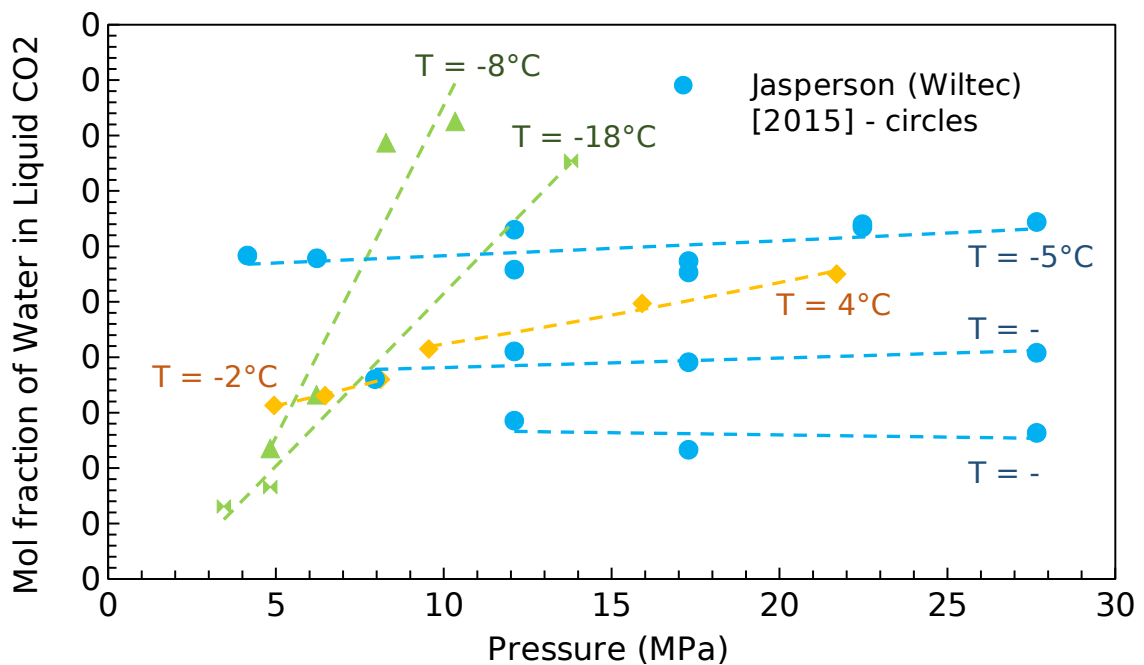
44 that is may be sequestered, in nearly all of them carbon dioxide must be  
45 transported from where it is captured to where it will be stored.[5-7] [8] In  
46 particular for subsea applications, carbon dioxide will have to be transported  
47 through the ocean at low temperatures and high pressures.[9,10] It is  
48 important that these lines stay clear and maintain flow, as downtime is both  
49 expensive and can pose safety concerns.[11]

50       Even in a nearly pure carbon dioxide stream, gas hydrate can form and  
51 accumulate with very small (ppm) amounts of water in the line.[12] Gas  
52 hydrates are ice-like crystalline compounds that form at the thermodynamic  
53 conditions found in many gas pipelines, allowing hydrates to form in and  
54 potentially block gas flow lines.[12] Hydrates are both costly to remove from  
55 a line and also pose a large safety hazard for operation, so they must be  
56 carefully managed or preferably avoided.[13,14] In gas transportation with  
57 already low water content, like carbon dioxide, it is common to dry gas below  
58 the water saturation pressure to avoid a free water phase and hydrate  
59 formation.[15,16] In order for this drying scheme to work, the water content  
60 of gas in equilibrium with hydrate must be accurately known so the gas may  
61 be dried below this value to prevent any formation.

62       The carbon dioxide hydrate phase boundary is well understood. Initial  
63 measurements began in the Donald L. Katz group in the 1940s[17] and have  
64 continued with others up through 2000.[18-20] Values are well established  
65 and in good agreement for the P-T location of the phase boundary. More  
66 recent carbon dioxide hydrate data has been published, but mostly in gas

67 mixtures as applications like hydrate based separations and carbon  
68 sequestration have received more focus.[21,22]

69 While P-T equilibrium measurements for hydrates are quite common,  
70 very few studies consider the water content of the bulk gas phase. In  
71 particular, for carbon dioxide, there are only a few data sets in the open  
72 literature, many of which are in disagreement with one other as seen in  
73 Figure 1.



74

75 Figure 1- Literature data for saturated water content in liquid carbon dioxide as a function of pressure.  
76 Each linear fit represents an isotherm given next to line. Blue circles are from Wiltec<sup>23</sup>, orange  
77 diamonds are from Chapoy<sup>20</sup>, and green triangles are from Song & Kobayashi<sup>19</sup>.

78 The Kobayashi group was one of the first to make these measurements  
79 in 1986, utilizing a stirred autoclave equilibrium cell.[23] The liquid CO<sub>2</sub>  
80 phase water content data shows a strong, unexpected, function of pressure

81 for water content as seen by the triangles in Figure 1. Further data showing  
82 this same trend was presented in a 2019 GPA Midstream technical report  
83 from Song et al. [24] More recently in 2011, Chapoy et al. measured the  
84 water content of carbon dioxide, and showed no dependence on pressure in  
85 a static (non-flowing) cell with impeller mixing (diamonds in Figure 1).[25]  
86 Similarly, data from Burgass et al., all collected below the ice point, show  
87 almost no function of pressure in the liquid phase CO<sub>2</sub> water content  
88 measurements.[26] In addition, other groups have made this measurement,  
89 like the work done by Seo et al. and Youseff et al that do not show this  
90 strong pressure dependence.[27,28] Most recently, two more groups in 2015  
91 showed this same weak function of pressure, one using a static cell at Korea  
92 University, and another in a flowing system at Wiltec (circles in Figure 1).[29]  
93 In all of these experiments measuring water content over carbon dioxide  
94 hydrate, only the gaseous or liquid carbon dioxide phase was ever evaluated.  
95 None of these studies considered evaluating the solid phase to determine  
96 whether it is hydrate, metastable hydrate, or metastable ice/liquid water.

97 Hydrate and ice metastability are both well documented phenomena.  
98 [30–33] In particular, for carbon dioxide hydrate, Ripmeester's group  
99 observed that ice can exist longer than 2 days at conditions where carbon  
100 dioxide hydrate is the thermodynamically stable solid phase.[34]  
101 Additionally, these different water phases (liquid, ice, or hydrate) may have  
102 different vapor pressures. For this reason, it is important to ensure that the

103 solid phase is hydrate, while measuring the saturated water content of the  
104 bulk carbon dioxide gas phase.

105         There are various analytical in-situ techniques for determining ice,  
106 hydrate, or liquid water existence. For example, Raman spectrometry has  
107 been successfully used in the past to discriminate between different hydrate  
108 structures.[35] However, Raman measures conditions at a very small  
109 sample spot (few microns) and the conventional method would be  
110 challenging to also measure equilibria conditions during in a macroscopic  
111 system. Conversely, X-ray computed tomography (CT) can distinguish  
112 differences in densities within an entire system in a very short time.[36,37]  
113 Density differences are large enough to differentiate phases during carbon  
114 dioxide hydrate formation in the X-ray CT scanner. While water has a  
115 specific gravity of 1, that of ice is slightly lower at 0.9, and for carbon dioxide  
116 hydrate it is slightly higher at 1.1.[38]

117         In this work, the water content of carbon dioxide at hydrate forming  
118 condition is measured, while the water phase is simultaneously characterized  
119 in situ. Previous works have shown large discrepancies between reported  
120 CO<sub>2</sub> water content values, and no work was performed to distinguish  
121 between potential metastable solid phases. Differences in the water content  
122 of CO<sub>2</sub> literature values may be due to the presence of a metastable liquid  
123 water or ice phase instead of actual carbon dioxide hydrate. In addition to  
124 making water content measurements, this work investigates the  
125 metastability of water at hydrate forming conditions based on X-ray CT data

126 collected simultaneously with water content measurements, and high  
127 pressure differential scanning calorimetry (HP-DSC) experiments to confirm  
128 and quantify the formation of hydrate.

## 129 **2. Materials and Methods**

130 In all tests, deionized water was utilized to form the carbon dioxide  
131 hydrate. Carbon dioxide was used as the hydrate guest molecule throughout  
132 this work, at a purity of 99.9995% obtained from Airgas. The column packing  
133 was made from chenille fabric (100% cotton), available off the shelf at any  
134 fabric store.

### 135 2.1 Packed Column

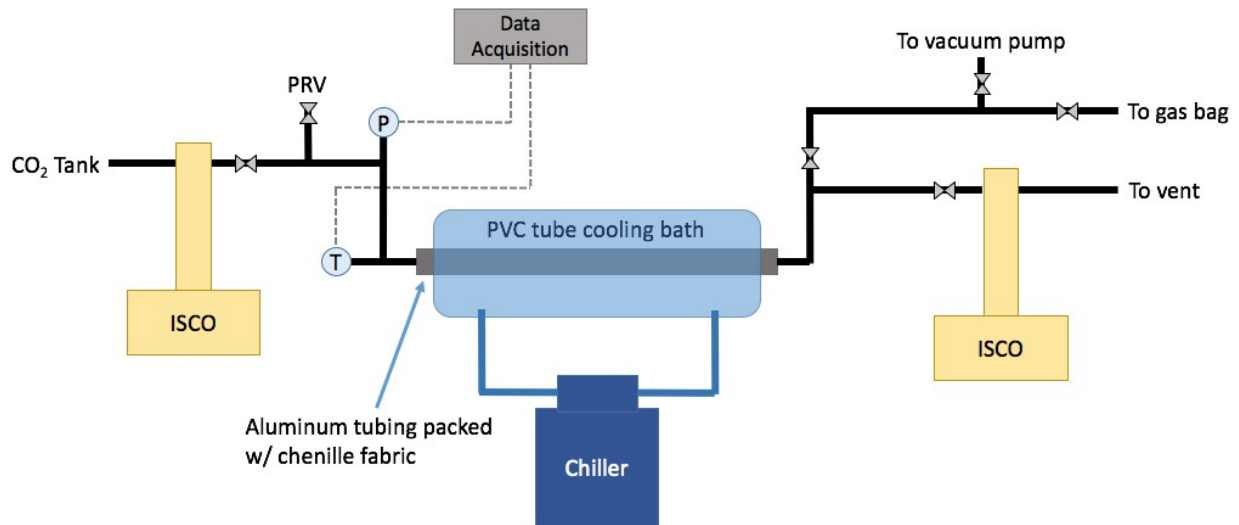
136 In this study a packed column flowing apparatus was constructed to  
137 make phase equilibrium measurements, similar to that used by Jasperson et  
138 al.[29] Water content of the effluent carbon dioxide stream was monitored  
139 via gas chromatography (GC) at Lawrence Berkeley National Laboratory  
140 (LBNL) and gas chromatography mass spectrometry (GCMS) at the Colorado  
141 School of Mines (CSM) to ensure steady state was achieved. This  
142 continuously flowing setup eliminates much of the sampling difficulty present  
143 in a static cell.

144 An overview of the apparatus is given in Figure 2. Pressure and  
145 temperature were both measured at the inlet to the testing section. The key  
146 section is the aluminum tubing in the center (1.27 cm ID x 45.72 cm long)  
147 filled with the chenille packing. Carbon dioxide hydrate is assumed to form

148 only in this section, as it is the only place where water is present. The test  
149 section is packed with chenille fabric to increase the surface area over which  
150 carbon dioxide hydrate formation occurs. Chenille was used as packing  
151 since it does not have a microporous structure that may prevent water from  
152 converting to carbon dioxide hydrate, and it is X-ray transparent, as is the  
153 aluminum used for tubing in the testing section. This trait was important to  
154 be able to use the X-ray CT to quantify the water phase.

155         In most phase equilibria measurements, getting representative  
156 samples at equilibrium conditions is a major challenge. For the work  
157 performed at LBNL, an isolated section of tubing at the outlet was utilized to  
158 obtain a sample of the outlet gas. After evacuating this section, it was filled  
159 with a carbon dioxide gas sample from the effluent of the column and then  
160 heated to 110°C. After heating, the sample section filled with the heated  
161 carbon dioxide was then opened to a gas bag. Because the gas bag was  
162 only partially filled, the pressure in the bag was atmospheric. From the gas  
163 bag, a syringe was used to inject an aliquot of the sample onto a Shimadzu  
164 GC-8A gas chromatograph (GC) with a Hayesep Q packed column and  
165 thermal conductivity detector (TCD) to detect the water content of the  
166 carbon dioxide gas.





167

168 *Figure 2- Schematic of the packed column apparatus developed to measure phase equilibria at hydrate*  
 169 *forming conditions. From gas bag, sample was injected into GC for water content analysis at LBNL or*  
 170 *directly to GCMS (no bag) at CSM.*

171 For the experiments performed at CSM, the equilibria apparatus and  
 172 GCMS are in close proximity to each other, so a small (1.5875 mm) heated  
 173 line from the outlet of the aluminum testing section directly to the GCMS was  
 174 utilized instead of a gas bag. This small change ensures a representative  
 175 equilibrium sample is being injected into the GC column and eases the  
 176 sampling procedure. Analysis at CSM was done with an Agilent 6890 Gas  
 177 Chromatograph with an Agilent 5973 Mass Selective Detector and pneumatic  
 178 gas injection valve. Aside from the above, the VLE saturation columns used  
 179 at LBNL and CSM are identical.

180 To operate the packed column, the chenille fabric was first saturated  
 181 with water, then loaded into the tubing. Thermal equilibrium was then  
 182 reached at 1°C before the system was pressurized to 29.3 bar with carbon

183 dioxide to achieve hydrate forming conditions. Pressure (Transamerica 0-  
184 1500 psi transducer, 09384/CEC-1000-04) and temperature (Omega  
185 Engineering Type T thermocouple, TMQSS-062U-18) conditions were then set  
186 to the desired experimental values. To sample, the sampling section was  
187 first evacuated via a vacuum pump (Hitachi 160VP Direct Drive Rotary  
188 Vacuum) before being filled with sample and then heated to 110°C to ensure  
189 the whole sample was vaporized and to prevent condensation of water on  
190 tubing line. Finally, an aliquot of the collected sample was transferred to the  
191 GC (or GCMS at CSM) for sampling via gas bag (or directly to the heated  
192 sample line at CSM).

## 193 2.2 X-ray Computed Tomography (CT)

194 While measuring water content, the aluminum testing section was on  
195 the table of a GE Lightspeed 16 medical CT scanner at LBNL with X-rays of  
196 120 kV potential. X-ray CT allows three-dimensional density distributions to  
197 be collected of the testing section while flowing CO<sub>2</sub> and measuring water  
198 contents at the outlet. With knowledge on the different densities between  
199 ice, liquid water, and carbon dioxide hydrate, the phases present inside the  
200 testing section can be determined.[39,40] The resolution of densities  
201 collected depends on the voxel size of 0.625 x 0.195 x 0.195 mm which  
202 results in 550 slices per scan, which in all took 2 minutes to complete.

## 203 2.3 High Pressure Differential Scanning Calorimetry (HP-DSC)

204 A Setaram  $\mu$ -DSC VIIa micro-differential scanning calorimeter was  
205 utilized to measure water conversion to carbon dioxide hydrate. The HP-DSC  
206 has a maximum pressure of 154 bar and operating temperature of -45 to 120  
207 °C. In the work, measurements began by loading 1 cm x 1 cm section of  
208 chenille fabric (same as column packing) into the cell. ~15 mg of water was  
209 then added onto the fabric. To form carbon dioxide hydrate, the sample was  
210 pressurized to the test condition (29.3 bar), and then cooled to 1 °C at a rate  
211 of 0.5 °C /min. The temperature was held at 1 °C for various times (16, 24,  
212 42 hrs) to evaluate the amount of carbon dioxide hydrate formed at different  
213 times. The temperature was increased slowly at a rate of 0.1 °C /min up to  
214 room temperature after an initial hold period to melt the carbon dioxide  
215 hydrate crystals so that the conversion could be evaluated.

216

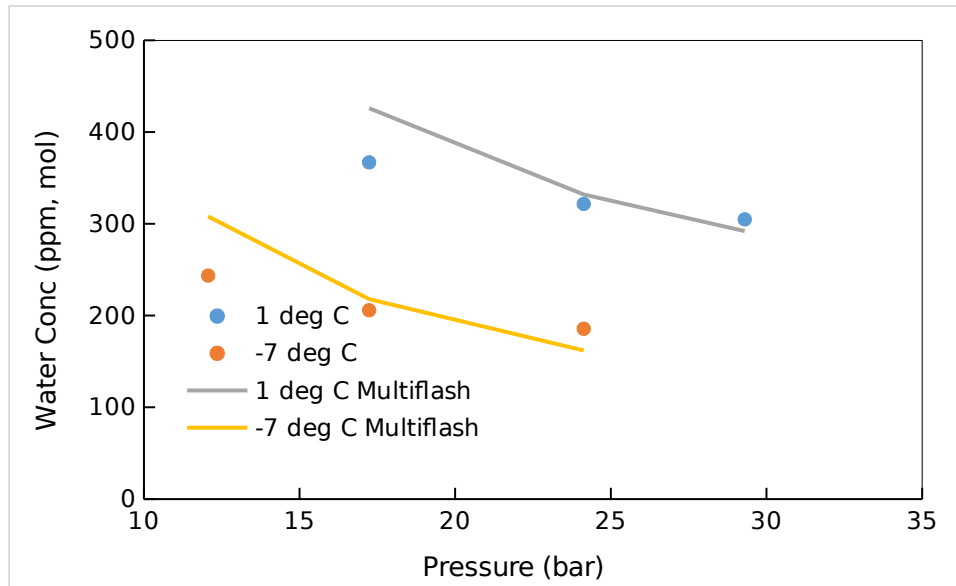
### 217 **3. Results and Discussion**

#### 218 3.1 Water Content Measurements

219 Carbon dioxide hydrate was first formed with the greatest driving force  
220 (highest pressure on a given isotherm), and then the pressure was  
221 isothermally lowered in order to collect water content data on water content  
222 of the CO<sub>2</sub> gas and hydrate formation data as a function of time and  
223 pressure. X-ray CT scans were taken approximately every 2 hours during the  
224 day and water content was measured immediately after each scan. Once  
225 the X-ray CT scans showed no further carbon dioxide hydrate formation and

226 the water content measurements remained constant, that water content was  
227 reported as the final equilibrium concentration.

228         Since the gas - hydrate region of the carbon dioxide and water phase  
229 diagram is not very large, only 2 isotherms were acquired to represent the  
230 region: one at 1°C and another at -7°C. Carbon dioxide hydrate was  
231 nucleated and annealed at 1°C before moving to the experimental  
232 temperature for both isotherms. This temperature gives the largest driving  
233 force for carbon dioxide hydrate formation, while remaining above the ice  
234 point. It was desirable to stay above the ice point as hydrate formation  
235 kinetics are much faster when forming from liquid water compared to ice.  
236 The results for both isotherms and corresponding Multiflash 6.2 Cubic Plus  
237 Association (CPA) predictions are shown in Figure 3- Equilibrium water  
238 content of gaseous carbon dioxide at hydrate conditions collected along 2  
239 different isotherms (1 (orange) and -7°C (blue)) compared with predicted  
240 values from Multiflash CPA model. Figure 3.[41] The Multiflash CPA model  
241 combines the Soave Redlich Kwong equation of state with further terms for  
242 hydrogen bonding, making it a preferred model for gas hydrate equilibrium  
243 predictions.[42]



244

245 *Figure 3- Equilibrium water content of gaseous carbon dioxide at hydrate conditions collected along 2*  
 246 *different isotherms (1 (orange) and -7°C (blue)) compared with predicted values from Multiflash CPA*  
 247 *model with hydrate phase. Error bars represent one standard deviation from 5 replicate experiments.*

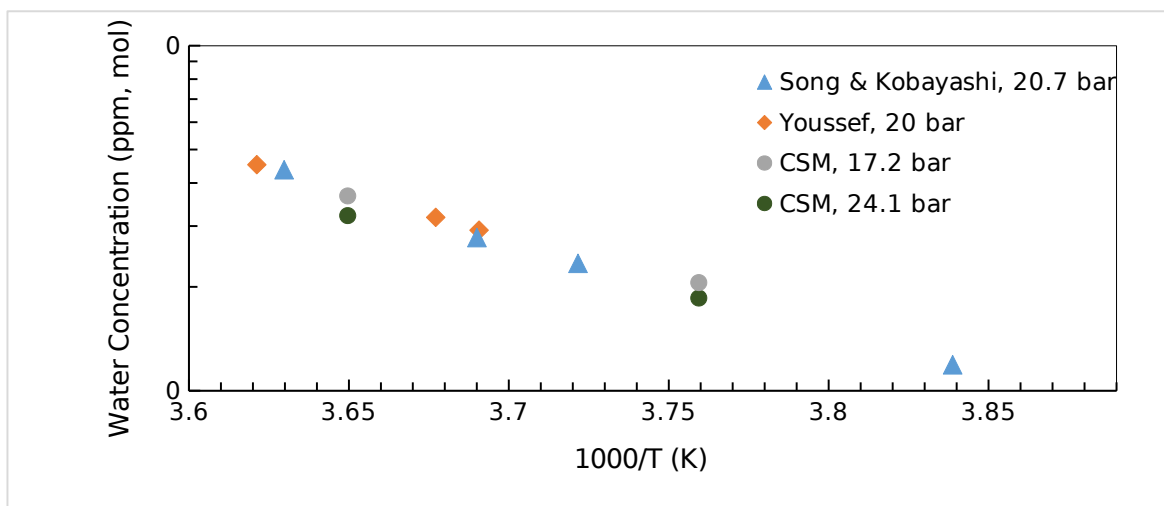
248 Both measured isotherms show a small decrease in water  
 249 concentration with pressure. The higher temperature, 1°C, shows higher  
 250 water contents in the gas phase compared to the lower temperature, as  
 251 expected. Vapor pressure over solids increases with increasing temperature  
 252 as molecules have more kinetic energy to escape into the gas phase.  
 253 Measured values are close to predicted values from Multiflash CPA and even  
 254 within error (one standard deviation of 5 replicate experiments) for most  
 255 points. Other phase equilibrium software designed for forecasting hydrate  
 256 formation and phase properties, like in-house software CSMGEM[43] (stands  
 257 for Colorado School of Mines, Gibbs Energy Minimization), was evaluated and  
 258 found to match Multiflash predictions almost exactly. To verify that the tube  
 259 had sufficient residence time to reach equilibrium at 0.1 mL/min, the flow

260 rate was doubled (to 0.2 mL/min) and CO<sub>2</sub> water contents were measured.

261 Water content values at the higher flowrate were within error of those

262 measured at the original flowrate (0.1 mL/min).

263 Figure 4 compares the data collected in this work to previously  
264 measured values for gaseous carbon dioxide water content. Note the limited  
265 amount of data for this system; far more data is available at conditions  
266 where carbon dioxide exists as a liquid.



267

268 *Figure 4- Comparison of measured water content (labeled CSM) in gaseous carbon dioxide (grey and*  
269 *green circles) to previous data collected by Youssef (orange diamonds) and Song et al (blue triangles)*  
270 *plotted on a log-inverse scale. Error bars on CSM data represent one standard deviation from 5*  
271 *replicates and are almost smaller than the points.*

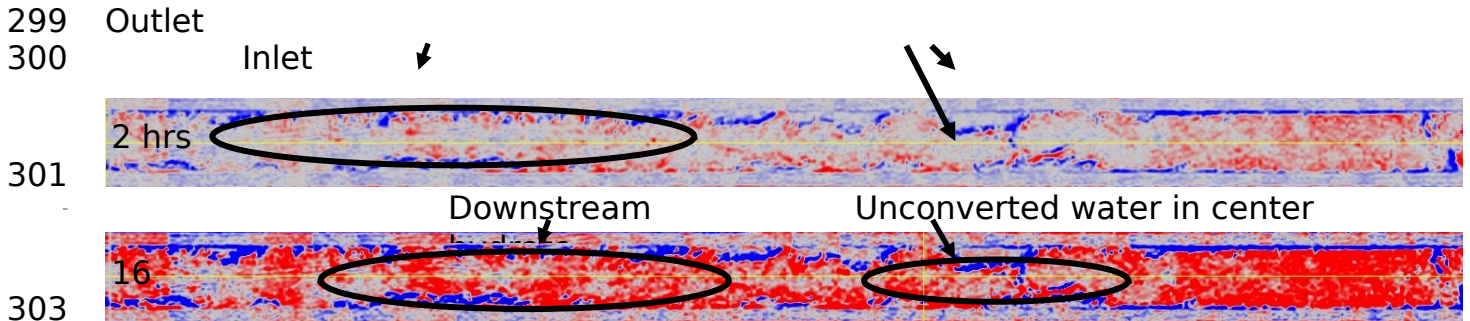
272 The data collected in this work (error bars are one standard deviation  
273 from 5 replicates) are in agreement with water contents measured  
274 previously in other labs for similar pressures. On a plot of natural logarithm  
275 of concentration of water versus inverse absolute temperature plot, the data  
276 are all linear, as predicted by the Clausius-Clapeyron equation for a

277 univariant system.[44] Note that the Clausius-Clapeyron equation, normally  
278 applied to a pure component, applies equally well to this binary, but  
279 univariant system.

280         The data do indicate a weak function of pressure, as may be expected  
281 with a highly compressible gas phase. The highest pressure data (at CSM  
282 24.1 bar) falls at the lowest water content compared to the other lower  
283 pressure at the corresponding temperature. While collecting the equilibrium  
284 values, X-ray CT was utilized to ensure that all liquid water had converted to  
285 carbon dioxide hydrate.

### 286 3.2 Effect of bulk water phase

287         While measuring the water content of carbon dioxide, CT scans were  
288 being taken at the same times. CT scanners work by measuring densities  
289 inside of each voxel in the system. Liquid water, ice, and carbon dioxide  
290 hydrate densities differ enough for them to be detected in the scanner. In  
291 this analysis, changes in density from initial conditions (liquid water and  
292 carbon dioxide gas) were evaluated. At the beginning of the experiment, a  
293 scan of the packing saturated with water was taken at ambient conditions.  
294 Then, after cooling and pressurization, further scans were taken and  
295 differences between each condition and the initial water system were taken.  
296 Colors have been assigned to the values for density differences to make  
297 viewing easier in ImageJ.[45,46] A sample of this can be seen with the CT  
298 scan in Figure 5.



304 *Figure 5- (top) X-ray CT scan taken 2 hours after hydrate nucleation and (bottom) X-ray CT scan taken*  
 305 *16 hours after hydrate nucleation at 1°C and 29.3 bar. Red represents a density increase (carbon*  
 306 *dioxide hydrate), white is no change, and blue is a density decrease, all relative to the starting liquid*  
 307 *water conditions (1.27 cm ID x 45.72 cm long).*

308 This scan was taken two hours after carbon dioxide hydrate nucleation  
 309 occurred and is a cross section down the center of the pipe. These scans are  
 310 only differences in density between the scan taken at each time and the  
 311 initial scan with liquid water. CO<sub>2</sub> entered the tube on the right had side,  
 312 flowing to the outlet at the left at 0.1 mL/min. The tube walls can be seen at  
 313 both the top and bottom of each image. Red represents an increase in  
 314 density, blue represents a decrease, and white is no change. Increases in  
 315 density indicate hydrate formation since carbon dioxide hydrate is denser  
 316 than the original liquid water. Density decreases are due to liquid water  
 317 vacating its position to move towards the carbon dioxide hydrate and being  
 318 replaced by gas. Ice would be shown in Figure 5 by a lighter blue color  
 319 compared to the deep blue of a liquid moving away and being replaced by a  
 320 gas (larger density change). Since the differences are being taken from  
 321 liquid water, white represents positions where density has not changed and  
 322 liquid water still exists. It can be seen in the scan at two hours (Figure 5 top)

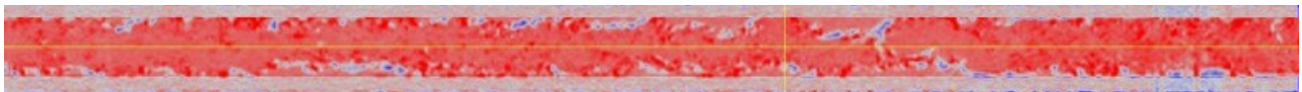


323 that there is some carbon dioxide hydrate formation on the right side, which  
324 is where carbon dioxide flowed into the system. There is still a significant  
325 amount of unconverted water (white) further downstream.

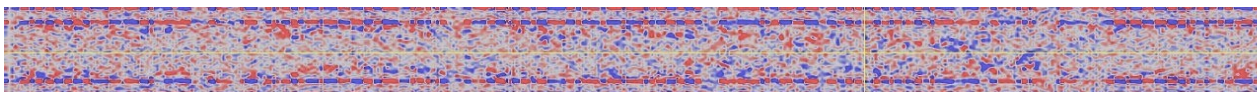
326 At longer times, like 16 hours after nucleation, further carbon dioxide  
327 hydrate formation has occurred. The area of red (carbon dioxide hydrate)  
328 has spread much further downstream (to the left) and less liquid water  
329 (white) remains, as seen in the bottom portion of Figure 5. There are still  
330 some white regions which contain liquid water that may be converted to  
331 carbon dioxide hydrate.

332 Finally, after 46 hours, the tube has become nearly all red due to  
333 carbon dioxide hydrate formation (Figure 6, top). There is almost no liquid  
334 water remaining. This can be confirmed by changing the point of reference  
335 to a later scan, at 42 hours. Because the subtraction is done at a new  
336 reference point, it is nearly all white, indicating no changes in density have  
337 occurred in those additional 4 hours. The constant density over this new  
338 time frame indicates no more carbon dioxide hydrate has formed. Both of  
339 these images can be seen in Figure 6.

340

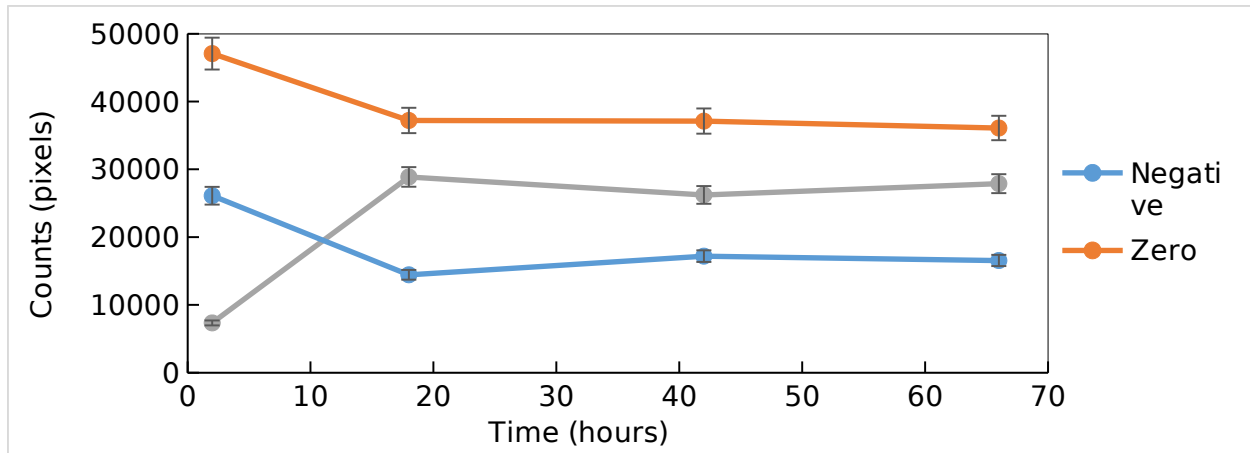


341



342 *Figure 6- Top: carbon dioxide hydrate formation (in red) 46 hours after nucleation at 1°C and 29.3 bar.*  
343 *Bottom: Additional carbon dioxide hydrate formation from 42 to 46 hours after nucleation at 1°C and*  
344 *29.3 bar. White indicates no further hydrate formation.*

345 Further, the number of red/blue/white voxels can be quantified to be  
346 sure that nothing is changing between these two times. In Figure 7, the  
347 numbers of positive, negative, and zero valued pixels along the slice down  
348 the center of the tube were quantified for select times after nucleation with  
349 error from the standard deviation of 10 different axial slices of CT images.  
350 The plots in Figure 7 agree with what was seen in Figures 5-6, where major  
351 conversion occurs early (first 24 hrs) in the experiment, as can be seen by  
352 the sharp increase in positive density changes initially. For carbon dioxide  
353 hydrate to form, water must be consumed, as indicated by the decreasing  
354 number of zero value pixels. All of these values are constant by 42 hours  
355 after nucleation, which is consistent with the visual analysis shown in prior  
356 Figures 5-6.

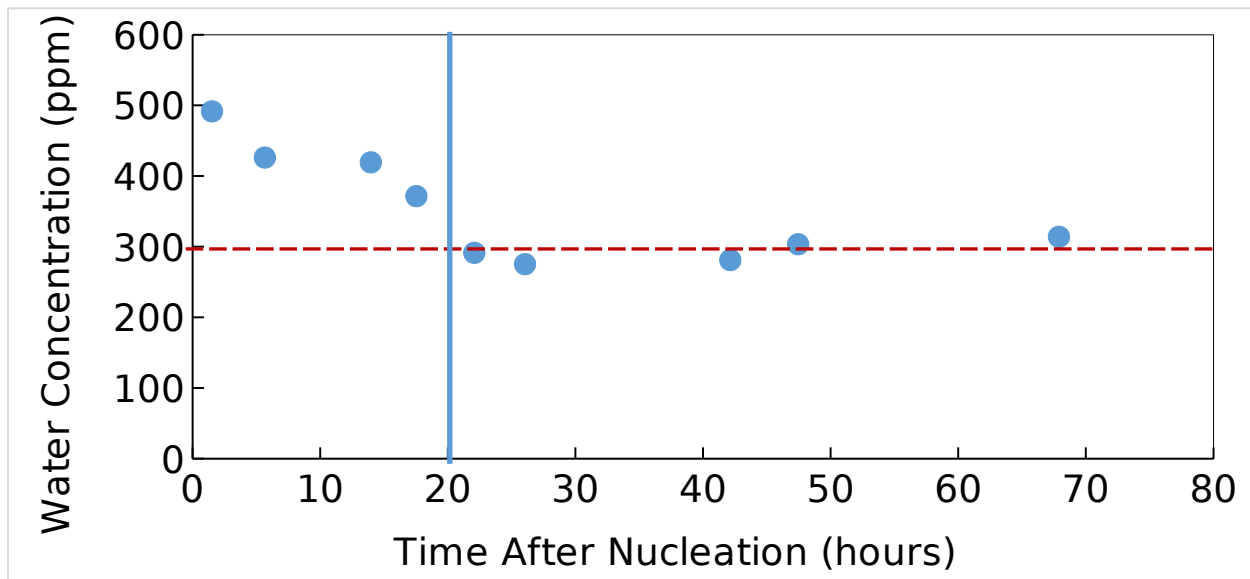


357

358 *Figure 7- Changes of X-ray CT density of pixels along centerline of tube at various times after*  
 359 *nucleation. Error bars represent one standard deviation from 10 different axial slices of the CT*  
 360 *images.*

361 When each X-ray CT scan was acquired, the water content in the CO<sub>2</sub>  
 362 gas effluent was also measured. In this way, the effect of carbon dioxide  
 363 hydrate versus liquid water was evaluated. The water content of carbon  
 364 dioxide decreased over time as liquid water converted to carbon dioxide  
 365 hydrate, as seen in Figure 8. Error bars on this plot represent one standard  
 366 deviation of 5 replicate experiments. The first point is likely high due to a  
 367 higher measured temperature in the cell from the exothermic hydrate  
 368 reaction. This temporary increased temperature from hydrate formation  
 369 would also increase the measured water content. However, the temperature  
 370 returns to the setpoint value (1°C) within 2 hours and any increased water  
 371 content values after that are unlikely to be due to temperature effects. While  
 372 the water content slowly decreased over the first 24 hours as liquid water  
 373 converted to carbon dioxide hydrate, it finally reached a constant value once  
 374 carbon dioxide hydrate conversion had completed. The phase of the water

375 in contact with the CO<sub>2</sub> is very important for these measurements, as it can  
376 change the water content by nearly 50%. For this reason, the solid phase  
377 must be evaluated when making hydrate equilibrium measurements.



378

379 *Figure 8- Water content of carbon dioxide over water (left side) and hydrate (right side) as liquid water*  
380 *converts to hydrate over time at 1°C and 29.3 bar. X-ray CT scans confirmed maximum carbon*  
381 *dioxide hydrate conversion after 40 hours. Dashed line represents Multiflash 6.2 CPA prediction (292*  
382 *ppm,mol). Error bars represent one standard deviation of 5 replicate experiments.*

### 383 3.3 Carbon dioxide hydrate metastability

384 In addition to the X-ray CT, HP-DSC was performed to confirm water  
385 metastability in the carbon dioxide hydrate forming region. Procedures for  
386 these experiments were similar to those done previously at CSM, with the  
387 exception that chenille fabric was added to the cell in order to increase  
388 surface area to improve hydrate conversion and mimic the experimental  
389 conditions in the X-ray CT. Conversion can be calculated based on the area

390 under the curve of the hydrate dissociation peak and knowledge of initial  
391 water amounts.[47]

392 Using this technique, conversion was calculated after various  
393 annealing times, which are summarized in Table 1 below. Additionally,  
394 conversion in the X-ray CT apparatus was estimated from the CT density  
395 values, like previously presented by Seol et al.[48] To calculate the  
396 conversion, the average change in density for every slice was calculated  
397 using ImageJ.[46] Next, the density change for each slice was converted to a  
398 mass with knowledge of the voxel size. The total mass increase was then  
399 summed, and with knowledge of the initial mass of water loaded into the  
400 tube and ratio of water to carbon dioxide in hydrates, the conversion can be  
401 calculated.

402 *Table 1- Calculated carbon dioxide hydrate conversion from differential scanning calorimetry*  
403 *experiments and estimated conversion from X-ray CT data.*

Time after Nucleation (hrs)	HP-DSC actual conversion ( $\pm 5\%$ )	X-ray CT estimated conversion ( $\pm 5\%$ )
4	No formation	23%
16	47%	39%
24	55%	64%
42	54%	65%

404

405 Similar duration experiments were necessary to achieve maximum  
406 conversion in both methods. Just like X-ray CT results, no further conversion

407 was seen after 24 hours in the HP-DSC. It was expected that hydrate  
408 formation in both of these apparatuses would match well, as both utilized the  
409 same packing materials and thermodynamic conditions. While the HP-DSC is  
410 a quiescent system, the flow through the tube in the X-ray CT was low  
411 enough that it was similar to the HP-DSC in terms of conversion timescales.  
412 The actual conversion is slightly higher in the X-ray CT due to the increased  
413 mass transfer from the flowing system. Due to the flowing nature of the X-  
414 ray CT experiments, the conversion can never reach 100% since some water  
415 (~300ppm level) is constantly flowing out of the system in the effluent  
416 carbon dioxide stream during experiments.

417 Both the X-ray CT and HP-DSC experiments eventually became mass  
418 transfer limited. There is no flow or mixing in the HP-DSC so once the water  
419 at the interface converts to carbon dioxide hydrate, the remaining liquid  
420 water inside the carbon dioxide hydrate shell will take much longer to  
421 convert to hydrate because mass transfer through the hydrate shell is slow.  
422 Similarly, the X-ray CT indicates a carbon dioxide hydrate shell forming even  
423 with a low flow rate. The carbon dioxide hydrate forms at the edge of the  
424 packing as seen in the area marked "Unconverted water in center) in Figure  
425 5. The red (hydrate) at the edge of the fabric surrounds white (unconverted  
426 water) as a carbon dioxide hydrate shell forms around the unconverted  
427 water, slowing mass transfer and stopping any further hydrate formation.  
428 Once this shell is thick enough that it prevents any further water conversion  
429 to carbon dioxide hydrate, the gas outside the shell in the vapor phase is in

430 equilibrium with the carbon dioxide hydrate shell as seen by the constant  
431 water content.

#### 432 **4. Conclusions**

433         When measuring water content of gases at hydrate forming conditions,  
434 it is important to not just characterize the phase in equilibrium with hydrates;  
435 the solid phase (hydrate and metastable phases) must be also considered.  
436 For the first time, water contents of gases at hydrate forming conditions  
437 were measured while simultaneously the state of the water phase present in  
438 the equilibrium. Specifically, two isotherms (1°C and -7°C) were collected  
439 between 12.06 and 29.30 bar for gaseous carbon dioxide water content in  
440 equilibrium with carbon dioxide hydrate. In order to verify values were  
441 collected in equilibrium with carbon dioxide hydrate, X-ray CT was used to  
442 simultaneously evaluate the state of the water phase. Initially, when liquid  
443 water still persisted in the system and carbon dioxide hydrate conversion  
444 was low, measured water content values were up to 50% higher than final  
445 equilibrium values. As time moved forward and further liquid water was  
446 converted to carbon dioxide hydrate, the water content of the CO<sub>2</sub> decreased  
447 asymptotically until reaching equilibrium values as the gas came into  
448 equilibrium with only a hydrate shell.

449         Water metastability within the carbon dioxide hydrate forming region  
450 was also evaluated. X-ray CT indicated that carbon dioxide hydrate took  
451 over 42 hours to achieve maximum conversion from liquid water at 29.3 bar

452 and 1°C. HP-DSC confirmed metastability results in the X-ray CT, as  
453 conversion in two independent apparatuses took place over similar  
454 timescales (>24 hours). Carbon dioxide hydrate conversion took so long  
455 (>24 hours) in both systems due to the large amounts of water and mass  
456 transfer limitations after maximum conversion. Water metastability is an  
457 important parameter that must be considered when making hydrate phase  
458 equilibrium measurements, as different water phases may lead to  
459 significantly different measured water content in the equilibrated fluid phase.

## 460 **5. Conflicts of Interest**

461 There are no conflicts of interest to declare.

## 462 **6. Acknowledgements**

463 The authors would like to acknowledge the GPA Midstream Association  
464 for funding this work, especially Dr. Håvard Lidal from Equinor and the GPA  
465 Midstream Research Committee for their guidance. Additionally, Mike  
466 Stadick and Mike Klasner were essential for getting the systems at CSM  
467 working properly.

## 468 **References**

- 469 [1] L. Hughes, Biological consequences of global warming: is the signal  
470 already apparent?, Trends Ecol. Evol. 15 (2000) 56-61.
- 471 [2] T.A. Boden, G. Marland, R.J. Andres, Global, Regional, and National  
472 Fossil-Fuel CO<sub>2</sub> Emissions, Oak Ridge, Tenn., USA, 2017.



- 473 [3] R.S. Haszeldine, Carbon Capture and Storage: How Green Can Black  
474 Be?, *Science* (80-. ). 325 (2009) 1647–1653.
- 475 [4] K.S. Lackner, S. Brennan, J.M. Matter, A.H.A. Park, A. Wright, B. Van Der  
476 Zwaan, The urgency of the development of CO<sub>2</sub> capture from ambient  
477 air, *PNAS*. 109 (2012) 13156–13162.  
478 <https://doi.org/10.1073/pnas.1108765109>.
- 479 [5] J. Gibbins, H. Chalmers, Carbon capture and storage, *Energy Policy*. 36  
480 (2008) 4317–4322. <https://doi.org/10.1016/j.enpol.2008.09.058>.
- 481 [6] D. Figueroa, T. Fout, S. Plasynski, H. Mcilvried, R.D. Srivastava,  
482 Advances in CO<sub>2</sub> capture technology — The U. S. Department of  
483 Energy’s Carbon Sequestration Program, *Int. J. Greenh. Gas Control*.  
484 (2008) 9–20. [https://doi.org/10.1016/S1750-5836\(07\)00094-1](https://doi.org/10.1016/S1750-5836(07)00094-1).
- 485 [7] M.E. Boot-Hanford, J.C. Abanades, E.J. Anthony, M.J. Blunt, S. Brandani,  
486 Carbon Capture and Storage Update, *Energy Environ. Sci.* 7 (2014) 130–  
487 189. <https://doi.org/10.1039/c3ee42350f>.
- 488 [8] R. Svensson, M. Odenberger, F. Johnsson, L. Stromberg, Transportation  
489 systems for CO<sub>2</sub> -- application to carbon capture and storage, *Energy*  
490 *Convers. Manag.* 45 (2004) 2343–2353.  
491 <https://doi.org/10.1016/j.enconman.2003.11.022>.
- 492 [9] M.D. Aminu, S.A. Nabavi, C.A. Rochelle, V. Manovic, A review of  
493 developments in carbon dioxide storage, *Appl. Energy*. 208 (2017)

- 494 1389-1419. <https://doi.org/10.1016/j.apenergy.2017.09.015>.
- 495 [10] M. Peter, N.P. Fofonoff, Conversion of pressure to depth in the ocean,  
496 Deep Sea Res. 23 (1976) 109-111.
- 497 [11] E.D. Sloan, C. Koh, A.K. Sum, Natural Gas Hydrates in Flow Assurance,  
498 First, Elsevier, 2011.
- 499 [12] E.D. Sloan, C.A. Koh, Clathrate Hydrates of Natural Gases, 3rd ed., CRC  
500 Press, 2008.
- 501 [13] M.N. Lingelem, A.I. Majeed, E. Stange, Industrial Experience in  
502 Evaluation of Hydrate Formation, Inhibition, and Dissociation in Pipeline  
503 Design and Operation, Ann. N. Y. Acad. Sci. 715 (1994) 75-93.
- 504 [14] J.J. Xiao, G. Shoup, G. Hatton, V. Kruka, OTC 8728 Predicting Hydrate  
505 Plug Movement During Subsea Flowline Depressurization Operations,  
506 Offshore Technol. Conf. (1998) 161-170.
- 507 [15] A. Witkowski, A. Rusin, M. Majkut, S. Rulik, K. Stolecka, Comprehensive  
508 analysis of pipeline transportation systems for CO<sub>2</sub> sequestration .  
509 Thermodynamics and safety problems, Energy Convers. Manag. 76  
510 (2013) 665-673. <https://doi.org/10.1016/j.enconman.2013.07.087>.
- 511 [16] M. Naseer, W. Brandstatter, Hydrate formation in natural gas pipelines,  
512 Comput. Methods Multiph. Flow VI. 70 (2011) 261-270.  
513 <https://doi.org/10.2495/MPF110221>.
- 514 [17] H.G. Donnelly, D.L. Katz, Phase Equilibria in the Dioxide-Methane

- 515 System, Ind. Eng. Chem. Res. 46 (1954) 511-517.  
516 <https://doi.org/10.1021/ie50531a036>.
- 517 [18] S.D. Larson, Phase studies of the two component carbon dioxide-water  
518 system involving the carbon dioxide hydrate, U. of Illinois, 1955.
- 519 [19] M. Wendland, H. Hasse, G. Maurer, Experimental Pressure -  
520 Temperature Data on Three- and Four-Phase Equilibria of Fluid ,  
521 Hydrate , and Ice Phases in the System Carbon Dioxide - Water, J.  
522 Chem. Eng. Data. 44 (1999) 901-906.  
523 <https://doi.org/10.1021/je980208o>.
- 524 [20] S.O. Yang, I.M. Yang, Y.S. Kim, C.S. Lee, Measurement and prediction of  
525 phase equilibria for water+CO<sub>2</sub> in hydrate forming conditions, Fluid  
526 Phase Equilib. 175 (2000) 75-89. [https://doi.org/10.1016/S0378-](https://doi.org/10.1016/S0378-3812(00)00467-2)  
527 [3812\(00\)00467-2](https://doi.org/10.1016/S0378-3812(00)00467-2).
- 528 [21] S. Adisasmito, R.J. Frank, E.D. Sloan, Hydrates of Carbon Dioxide and  
529 Methane Mixtures, J. Chem. Eng. Data. 36 (1991) 68-71. [https://doi.org/](https://doi.org/10.1021/je00001a020)  
530 [10.1021/je00001a020](https://doi.org/10.1021/je00001a020).
- 531 [22] P. Babu, P. Linga, R. Kumar, P. Englezos, A review of the hydrate based  
532 gas separation (HBGS) process for carbon dioxide pre-combustion  
533 capture, Energy. 85 (2015) 261-279.  
534 <https://doi.org/10.1016/j.energy.2015.03.103>.
- 535 [23] K.Y. Song, R. Kobayashi, The Water Content of CO<sub>2</sub>-rich Fluids in

- 536 Equilibrium with Liquid Water and/or Hydrates, 1986.
- 537 [24] K.Y. Song, K.R. Cox, W.G. Chapman, Water Content in Gaseous and  
538 Liquid Carbon Dioxide and its Mixtures with Methane in Equilibrium with  
539 Hydrate, GPA Midstream Tech. Publ. (2019).
- 540 [25] A. Chapoy, R. Burgass, B. Tohidi, J.M. Austell, C. Eickhoff, Effect of  
541 Common Impurities on the Phase Behavior of Carbon-Dioxide-Rich  
542 Systems : Minimizing the Risk of Hydrate Formation and Two-Phase  
543 Flow, SPE J. 16 (2011) 921-930.
- 544 [26] R. Burgass, A. Chapoy, P. Duchet-Suchaux, B. Tohidi, Experimental  
545 water content measurements of carbon dioxide in equilibrium with  
546 hydrates at (223.15 to 263.15) K and (1.0 to 10.0) MPa, J. Chem.  
547 Thermodyn. 69 (2014) 1-5. <https://doi.org/10.1016/j.jct.2013.09.033>.
- 548 [27] M. Do Seo, J.W. Kang, C.S. Lee, Water Solubility Measurements of the  
549 CO<sub>2</sub> -Rich Liquid Phase in Equilibrium with Gas Hydrates Using an  
550 Indirect Method, J. Chem. Eng. Data. 56 (2011) 2626-2629.  
551 <https://doi.org/10.1021/je2001232>.
- 552 [28] Z. Youssef, A. Barreau, P. Mougín, J. Jose, I. Mokbel, C.B.L. I,  
553 Measurements of Hydrate Dissociation Temperature of Methane ,  
554 Ethane , and CO<sub>2</sub> in the Absence of Any Aqueous Phase and Prediction  
555 with the Cubic Plus Association Equation of State, Ind. Eng. Chem. Res.  
556 48 (2009) 4045-4050.

- 557 [29] L. V Jaspersen, J.W. Kang, C.S. Lee, D. Macklin, P.M. Mathias, R.J.  
558 McDougal, W.G. Rho, D. VonNiederhausern, Experimental  
559 Determination of the Equilibrium Water Content of CO<sub>2</sub> at High  
560 Pressure and Low Temperature, *J. Chem. Eng. Data.* 60 (2015) 2674-  
561 2683. <https://doi.org/10.1021/acs.jced.5b00320>.
- 562 [30] E.D. Sloan, F. Fleyfel, Molecular Mechanism for Gas Hydrate Nucleation  
563 from Ice, *AIChE J.* 37 (1991).
- 564 [31] V. Natarajan, P.R. Bishnoi, N. Kalogerakis, Induction Phenomena In Gas  
565 Hydrate Nucleation, *Chem. Eng. Sci.* 49 (1994) 2075-2087.
- 566 [32] L.A. Stern, S. Circone, S.H. Kirby, W.B. Durham, Anomalous Preservation  
567 of Pure Methane Hydrate at 1 atm, *J. Phys. Chem. B.* 105 (2001) 1756-  
568 1762. <https://doi.org/10.1021/jp003061s>.
- 569 [33] V.P. Melnikov, A.N. Nesterov, A.M. Reshetnikov, V.A. Istomin, V.G. Kwon,  
570 Stability and growth of gas hydrates below the ice - hydrate - gas  
571 equilibrium line on the P - T phase diagram, *Chem. Eng. Sci.* 65 (2010)  
572 906-914. <https://doi.org/10.1016/j.ces.2009.09.041>.
- 573 [34] I.L. Moudrakovski, G.E. McLaurin, C.I. Ratcliffe, J.A. Ripmeester, Methane  
574 and Carbon Dioxide Hydrate Formation in Water Droplets: Spatially  
575 Resolved Measurements from Magnetic Resonance Microimaging, *J.*  
576 *Phys. Chem. B.* 108 (2004) 17591-17595.  
577 <https://doi.org/10.1021/jp0473220>.

- 578 [35] H. Ohno, T.A. Strobel, S.F. Dec, E.D. Sloan, C.A. Koh, Raman Studies of  
579 Methane - Ethane Hydrate Metastability, *J. Phys. Chem. A.* 113 (2009)  
580 1711-1716.
- 581 [36] J. Wang, J. Zhao, M. Yang, Y. Li, W. Liu, Y. Song, Permeability of  
582 laboratory-formed porous media containing methane hydrate :  
583 Observations using X-ray computed tomography and simulations with  
584 pore network models, *Fuel.* 145 (2015) 170-179.  
585 <https://doi.org/10.1016/j.fuel.2014.12.079>.
- 586 [37] T.J. Kneafsey, Y. Seol, A. Gupta, L. Tomutsa, Permeability of Laboratory-  
587 Formed Methane-Hydrate-Bearing Sand : Measurements and  
588 Observations Using X-Ray Computed Tomography, *SPE J.* (2011) 78-94.
- 589 [38] A.T. Bozzo, H.-S. Chen, J.R. Kass, A.J. Barduhn, The Properties of the  
590 Hydrates of Chlorine and Carbon Dioxide, *Deslination.* 16 (1975) 303-  
591 320.
- 592 [39] V. Cnudde, M.N. Boone, High-resolution X-ray computed tomography in  
593 geosciences : A review of the current technology and applications, *Earth*  
594 *Sci. Rev.* 123 (2013) 1-17.  
595 <https://doi.org/10.1016/j.earscirev.2013.04.003>.
- 596 [40] T.J. Kneafsey, G.J. Moridis, X-Ray computed tomography examination  
597 and comparison of gas hydrate dissociation in NGHP-01 expedition  
598 ( India ) and Mount Elbert ( Alaska ) sediment cores : Experimental  
599 observations and numerical modeling, *Mar. Pet. Geol.* 58 (2014) 526-

600 539. <https://doi.org/10.1016/j.marpetgeo.2014.06.016>.

601 [41] KBC, Multiflash- PVT Modelling and Flow Assurance Software.

602 [42] G. M. Kontogeorgis, M. L. Michelsen, G. K. Folas, S. Derawi, N. von  
603 Solms, E. H. Stenby, Ten Years with the CPA (Cubic-Plus-Association)  
604 Equation of State. Part 1. Pure Compounds and Self-Associating  
605 Systems, *Ind. Eng. Chem. Res.* 45 (2006) 4855–4868.  
606 <https://doi.org/10.1021/ie051305v>.

607 [43] CHR, CSMGem.

608 [44] T.Y. Makogon, E.D. Sloan, Phase Equilibrium for Methane Hydrate from  
609 190 to 262 K, *J. Chem. Eng. Data.* 39 (1994) 351–353.  
610 <https://doi.org/10.1021/je00014a035>.

611 [45] P. Thevenaz, U.E. Ruttimann, M. Unser, A Pyramid Approach to Subpixel  
612 Registration Based on Intensity, *IEEE Trans. Image Process.* 7 (1998)  
613 27–41.

614 [46] C.A. Schneider, W.S. Rasband, K.W. Eliceiri, NIH Image to ImageJ : 25  
615 years of Image Analysis, *Nat. Methods.* 9 (2012) 671–675.

616 [47] J.W. Lachance, Investigation of Gas Hydrates Using Differential  
617 Scanning Calorimetry with Water-In-Oil Emulsion, Colorado School of  
618 Mines, 2008.

619 [48] Y. Seol, T.J. Kneafsey, Methane hydrate induced permeability  
620 modification for multiphase flow in unsaturated porous media, 116

621 (2011) 1-15. <https://doi.org/10.1029/2010JB008040>.

622