

# Lawrence Berkeley National Laboratory

## LBL Publications

### Title

Vapor-Liquid Equilibria for Binary Solutions of Arborescent and Linear Polystyrenes

### Permalink

<https://escholarship.org/uc/item/5qk483n5>

### Authors

Lieu, John G

Prausnitz, J M

Gauthier, Mario

### Publication Date

1999-03-01

### Copyright Information

This work is made available under the terms of a Creative Commons Attribution License, available at <https://creativecommons.org/licenses/by/4.0/>



# ERNEST ORLANDO LAWRENCE BERKELEY NATIONAL LABORATORY

## Vapor-Liquid Equilibria for Binary Solutions of Arborescent and Linear Polystyrenes

John G. Lieu, J.M. Prausnitz, and Mario Gauthier  
Chemical Sciences Division

March 1999

Submitted to  
*Polymer*



REFERENCE COPY |  
Does Not |  
Circulate |  
Bldg. 50 Library - Ref.  
Lawrence Berkeley National Laboratory

## **DISCLAIMER**

This document was prepared as an account of work sponsored by the United States Government. While this document is believed to contain correct information, neither the United States Government nor any agency thereof, nor the Regents of the University of California, nor any of their employees, makes any warranty, express or implied, or assumes any legal responsibility for the accuracy, completeness, or usefulness of any information, apparatus, product, or process disclosed, or represents that its use would not infringe privately owned rights. Reference herein to any specific commercial product, process, or service by its trade name, trademark, manufacturer, or otherwise, does not necessarily constitute or imply its endorsement, recommendation, or favoring by the United States Government or any agency thereof, or the Regents of the University of California. The views and opinions of authors expressed herein do not necessarily state or reflect those of the United States Government or any agency thereof or the Regents of the University of California.

# Vapor-Liquid Equilibria for Binary Solutions of Arborescent and Linear Polystyrenes

John G. Lieu and J. M. Prausnitz

Department of Chemical Engineering

University of California

and

Chemical Sciences Division

Lawrence Berkeley National Laboratory

University of California

Berkeley, CA 94720, U.S.A.

and

Mario Gauthier

Department of Chemistry

University of Waterloo

Waterloo, Ontario N2L 3G1, Canada

March 1999

This work was supported by the Director, Office of Energy Research, Office of Basic Energy Sciences, Chemical Sciences Division of the U.S. Department of Energy under Contract Number DE-AC03-76SF00098.

# **Vapor-Liquid Equilibria for Binary Solutions of Arborescent and Linear Polystyrenes**

**John G. Lieu and John M. Prausnitz\***

Chemical Engineering Department  
University of California, Berkeley

and

Chemical Sciences Division  
Lawrence Berkeley National Laboratory  
Berkeley, CA 94720

and

**Mario Gauthier**  
Department of Chemistry  
University of Waterloo  
Waterloo, Ontario N2L 3G1, Canada

\* To whom correspondence should be addressed

## ABSTRACT

Vapor-liquid-equilibrium data are reported for binary mixtures of arborescent polystyrene or linear polystyrene dissolved in chloroform, toluene, or cyclohexane in the range 50-70°C. Using a classic gravimetric-sorption method, the amount of solvent absorbed by the polymer was measured as a function of solvent vapor pressure. Vapor-liquid-equilibrium data are compared to osmotic second-virial-coefficient data for similar arborescent and linear polystyrenes. Solvent activity depends on arborescent polystyrene generation number in cyclohexane solutions but similar dependence on arborescent polystyrene generation number is not observed for polymers dissolved in chloroform or toluene.

## INTRODUCTION

The synthesis and study of polymers with highly-branched, well-defined architectures have become topics of growing interest in recent years. Dendrimers are an important class of macromolecules; synthetic methods have become available to control precisely their structure, molecular weight, and surface chemistry. Dendrimers are characterized by a central core with multiple "arms" radiating outwards to form increasingly packed "shells" or "generations"<sup>1</sup>.

In general, dendrimer building blocks are low-molecular-weight molecules; many steps are required to produce a material of high molecular weight. To reduce the number of steps, Gauthier and Möller developed a synthetic "graft-on-graft" technique using polymers as building blocks<sup>2</sup>. Through this technique, arborescent polymers of high

molecular weight can be obtained in fewer steps than those required for traditional dendritic growth.

A promising application of these polymers is in the formation of ultrathin films. Sheiko et al.<sup>3</sup> demonstrated that monomolecular films of uniform thickness can be obtained from arborescent polystyrenes. The thickness of monolayer film depends on the molecular weight and branching density of the polymer.

This work reports binary vapor-liquid-equilibrium (VLE) data for arborescent or linear polystyrenes in chloroform at 50°C, toluene at 70°C, and cyclohexane at 70°C. Vapor-liquid-equilibrium data are compared to osmotic second virial coefficients reported by Gauthier et al.<sup>4</sup> for similar arborescent polystyrenes in toluene and cyclohexane.

## EXPERIMENTAL

### *Materials*

Solvents were degassed with a standard freeze-thaw procedure described by Panayiotou and Vera<sup>5</sup> and used without further purification. *Table 1* gives solvent properties.

The arborescent polymers used in the investigation were synthesized by repeatedly grafting a linear polystyrene core with polystyrene side chains. The initial grafting reactions yielded a comb polymer designated as generation zero (S05-0); the generation 1 polymer (S05-1) is twice grafted, and so on. The core polymer and the side chains grafted in each reaction had a molecular weight around 5,000 g/mol. Gauthier et al.<sup>2,6,7</sup> described the methods for synthesizing and characterizing these samples.

Two linear polystyrene samples of different molecular weights were also investigated. A sample with molecular weight  $1.75 \times 10^4$  g/mol was investigated in chloroform; a sample with molecular weight  $5.0 \times 10^4$  g/mol was investigated in toluene and in cyclohexane.

For subsequent calculations, all polymers are assumed to have a specific gravity of unity. *Tables 2 and 3* give the polymer properties.

### *Apparatus*

VLE data were collected using a gravimetric-sorption method previously described by several authors (see, for example, Gupta and Prausnitz<sup>8</sup>). *Figure 1* shows a schematic diagram of the apparatus. The entire system is submerged in an isothermal water or air bath maintained at  $\pm 0.3^\circ\text{C}$ .

Each glass chamber contains one aluminum pan suspended from a quartz spring (Ruska Instruments Corp., Houston, TX). The calibrated springs have a sensitivity of about 1 mg/mm and a maximum load of 250 mg. Within this range, the elongation of each spring is linear with respect to change in mass.

A cathetometer (Wild, Heerbrugg, Switzerland) is used to measure the extension of the springs and the mercury levels of the manometer.



### *Experimental Procedure*

Polymer samples of known mass (10–20 mg) are placed into previously weighed aluminum pans. The system is then vacuum-dried for 12 to 24 hours to remove residual moisture and solvent. After obtaining the mass of dry polymer, solvent is introduced by opening and then closing the valve between the solvent flask and the evacuated glass chambers.

The system is allowed to equilibrate anywhere from 12 hours to a few days after each solvent injection. Equilibrium is assumed when measurements in spring length do not change more than  $\pm 0.05$  mm over a 12-hour period.

Because the polymer is nonvolatile, the total pressure is equal to the vapor pressure of solvent above the polymer solution. Because experimental pressures are low (less than 0.7 bar), the solvent vapor is considered to be an ideal gas. Solvent activity  $a_1$  is given by the ratio of the measured pressure to the pure-solvent saturation pressure at system temperature.

The vernier scale on the cathetometer allows measurements to be made to the nearest 0.05 millimeter; therefore, pressure and mass readings have a precision of 0.1 torr and 0.1 mg, respectively. Uncertainty in solvent activity is 1–2% above  $a_1 = 0.1$  and 2–4% below  $a_1 = 0.1$ . Solvent weight fraction  $w_1$  uncertainty is 2–5% above  $w_1 = 0.5$  and 5–15% below  $w_1 = 0.5$ .

Reliability of the apparatus and experimental procedure were established by reproducing published experimental VLE data for polystyrene in chloroform<sup>9</sup>.

## RESULTS AND DISCUSSION

*Table 4* presents VLE data for S05-1, S05-3 and linear polystyrene. *Figures 2-4* show solvent activity  $a_1$  as a function of solvent segment fraction  $\Phi_1$ .

*Figure 2* shows solvent activities for solutions of S05-1, S05-3 and linear polystyrene in chloroform; there is no significant difference in solvent absorption among the polymers. *Figure 3* shows results for S05-1, S05-3 and linear polystyrene in toluene. Again, solvent-activity data for the polymers do not differ significantly. However, *Figure 4* shows considerable differences for solvent absorption in cyclohexane; S05-1 absorbs the most cyclohexane, followed by linear polystyrene and then by S05-3.

The data are fitted using the Flory-Huggins equation<sup>10</sup>. The activity of the solvent is given by

$$\ln a_1 = \ln \Phi_1 + \left(1 - \frac{r_1}{r_2}\right) \Phi_2 + \chi_{FH} \Phi_2^2. \quad (1)$$

Solvent and polymer segment fractions,  $\Phi_1$  and  $\Phi_2$ , are defined by

$$\Phi_2 = 1 - \Phi_1 = \frac{r_2 N_2}{r_1 N_1 + r_2 N_2} \quad (2)$$

where  $N_1$  and  $N_2$  are the number of molecules and  $r_1$  and  $r_2$  are the number of segments per molecule of solvent and polymer, respectively. We set  $r_1$  equal to unity and calculate  $r_2$  by

$$r_2 = \frac{M_2 \rho_1}{M_1 \rho_2} = \frac{\text{molar volume of polymer}}{\text{molar volume of solvent}} \quad (3)$$

where  $M_1$  and  $M_2$  are molecular weights and  $\rho_1$  and  $\rho_2$  are mass densities of solvent and polymer, respectively. The dimensionless Flory-Huggins parameter  $\chi_{FH}$  characterizes the solvent-polymer interaction energy; the lower this parameter, the

stronger the attraction between solvent and polymer. *Table 5* gives fitted  $\chi_{FH}$  values.

The Flory parameters in *Table 5* indicate that the polymers interact most favorably with chloroform (low  $\chi_{FH}$ ) and least favorably with cyclohexane (high  $\chi_{FH}$ ). *Figure 5* shows that our results are consistent with those in the literature for linear polystyrene in chloroform, toluene, and cyclohexane.

*Figures 2* and *3* show that the Flory-Huggins theory gives a good fit for the polymers in chloroform and toluene, respectively. *Figure 4*, however, shows that calculated VLE for the polymers in cyclohexane are not reproduced with the same accuracy.

With rising generation number, the branching density of arborescent polystyrene increases and the resulting molecular structure is expected to stiffen and approach that of a hard sphere in semi-dilute solution owing to steric crowding<sup>13</sup>. This stiffening suggests that solvent power may show a significant dependence on generation number.

From light-scattering measurements, Gauthier et al.<sup>4</sup> reported the dependence of osmotic second virial coefficients  $A_2$  on temperature for arborescent and linear polystyrenes in toluene and in cyclohexane in the range 25-65°C. Because the data cover a reasonable temperature range,  $A_2$  can be split into contributions from enthalpy ( $A_{2,H}$ ) and entropy ( $A_{2,S}$ ). For S05-0 and S05-1, Gauthier et al. report that  $A_{2,S}$  is positive and decreases with rising generation number when dissolved in toluene or cyclohexane;  $A_{2,H}$  is negative and changes insignificantly in toluene, but decreases in magnitude with rising generation number in cyclohexane. The variation of  $A_{2,H}$  and  $A_{2,S}$  supports our conjecture that a decrease in solvent power (lower  $A_2$ ) with rising generation number is

due to steric factors (lower  $A_{2,S}$ ); increased molecular stiffness inhibits penetration of solvent into the polymer.

To compare our Flory parameters with osmotic second virial coefficients, we use the relation<sup>14</sup>

$$\chi_{FH} = 0.5 - v_1 \rho_2^2 A_2 \quad (4)$$

where  $v_1$  is the molar volume of the solvent and  $\rho_2$  is the polymer mass density. The dependence of  $A_2$  on temperature is linear for S05-0, S05-1 and for linear polystyrene. *Table 6* shows  $A_2$  linearly extrapolated to 70°C and *Table 7* shows  $\chi_{FH}$  calculated by Equation (4).

As shown in *Tables 5* and *7*,  $\chi_{FH}$  obtained from VLE in toluene and cyclohexane do not agree well with  $\chi_{FH}$  calculated from  $A_2$ . Disagreement is probably due to very different concentration regimes used for data acquisition. Our Flory parameters are obtained from solvent-activity data for concentrated polymer solutions, whereas osmotic second virial coefficients are obtained from light-scattering data for highly dilute polymer solutions.

Qualitatively, our VLE data indicate that solvent absorption depends on polymer generation number in cyclohexane, but not in chloroform or toluene. A possible explanation is that for binary mixtures of arborescent polystyrenes, entropic contributions are of similar magnitude in the solvents used here. The quality of the solvents may then be primarily a function of the enthalpic contributions. For example, chloroform and toluene are good solvents for arborescent polystyrene and favorable polymer-solvent interactions may result from favorable enthalpic contributions with relatively small entropic contributions. Cyclohexane, however, is a poor solvent for arborescent

polystyrene, perhaps because the enthalpic contribution is low. Because the entropic contribution in cyclohexane may be significant, VLE results for polymers in cyclohexane depend on generation number.

## CONCLUSIONS

Osmotic second virial coefficients indicate that for arborescent polystyrene, solvent-polymer interaction depends on generation number. Vapor-liquid-equilibrium data for solutions of arborescent polystyrenes in cyclohexane also show dependence on generation number; however, similar dependence of solvent absorption on generation number is not observed when the solvent is chloroform or toluene. Conclusions from osmotic-second-virial-coefficient data are not necessarily inconsistent with those obtained from vapor-liquid-equilibrium data because the former pertain to very dilute solutions whereas the latter pertain to highly concentrated polymer solutions.

## ACKNOWLEDGMENTS

This work was supported by the Director, Office of Energy Research, Office of Basic Energy Sciences, Chemical Sciences Division of the U.S. Department of Energy under contract No. DE-AC03-76SF0098, and by the Donors of the Petroleum Research Fund administered by the American Chemical Society. The authors are grateful to John O. Tanbonliong and Cristina Mio for construction of experimental apparatus and helpful comments.

## REFERENCES

1. Newkome, G. R., Moorefield, C. N. and Vögtle, F., *Dendritic Molecules: Concepts, Syntheses, Perspectives*. VCH Publishers, Inc., New York, 1996.
2. Gauthier, M. and Möller, M., *Macromolecules*, 1991, **24**, 4548.
3. Sheiko, S. S., Gauthier, M. and Möller, M., *Macromolecules*, 1997, **30**, 2343.
4. Gauthier, M., Chung, J., Choi, L. and Nguyen, T. T., *J. Phys. Chem. B.*, 1998, **102**, 3138.
5. Panayiotou, C. and Vera, J. H., *Polym. J.*, 1984, **16**, 89.
6. Gauthier, M., Li, W. and Tichagwa, L., *Polymer*, 1997, **38**, 6363.
7. Gauthier, M., Tichagwa, L., Downey, J. S. and Gao, S., *Macromolecules*, 1996, **29**, 519.
8. Gupta, R. B. and Prausnitz, J. M., *J. Chem. Eng. Data.*, 1995, **40**, 784.
9. Bawn, C. E. H. and Wajid, M. A., *Trans. Faraday Soc.*, 1956, **52**, 1658.
10. Flory, P. J., *Principles of Polymer Chemistry*. Cornell University Press, New York, 1953.
11. Tait, P. J. T. and Abushihada, A. M., *Polymer*, 1977, **18**, 810.
12. Krigbaum, W. R. and Geymer, D. O., *J. Am. Chem. Soc.*, 1959, **81**, 1859.
13. Gauthier, M., Möller, M. and Burchard, W., *Macromol. Symp.*, 1994, **77**, 43.
14. Brandrup, J. and Immergut, E. H., *Polymer Handbook*, 3<sup>rd</sup> ed. John Wiley & Sons, New York, 1989.

15. Daubert, T. E. and Danner, R. P., *Physical and Thermodynamic Properties of Pure Chemicals: Data Compilation*. Hemisphere Pub. Corp, New York, 1989.

**Table 1** Solvent properties

Solvent	Supplier	Purity
chloroform	Fisher Scientific	99.9%
toluene	Fisher Scientific	99.9%
cyclohexane	Fisher Scientific	99.96%



**Table 2** Linear-polystyrene properties

Polymer	Supplier	$M_w$ (g/mol)	$M_w/M_n$
linear polystyrene <sup>a</sup>	Pressure Chemical Company	$1.75 \times 10^4$	< 1.06
linear polystyrene <sup>b</sup>	Pressure Chemical Company	$5.0 \times 10^4$	< 1.06

<sup>a</sup> vapor-liquid-equilibrium data obtained in chloroform

<sup>b</sup> vapor-liquid-equilibrium data obtained in toluene and cyclohexane

**Table 3** Arborescent-polystyrene properties

Polymer	Generation Number	$M_w^a$ (g/mol)	$M_w/M_n^b$
S05-0	0	$6.7 \times 10^4$	1.07
S05-1	1	$8.7 \times 10^5$	1.07
S05-3	3	$9.0 \times 10^7$	1.15

<sup>a</sup> absolute weight-average molecular weight from light-scattering measurements

<sup>b</sup> apparent polydispersity index from SEC analysis of the graft polymers

**Table 4** Vapor-liquid-equilibrium data for S05-1, S05-3 and linear polystyrene

$w_1$  (POLY) = solvent weight fraction in the liquid phase with polymer "POLY";  
 "linear" refers to linear polystyrene

$a_1 = P / P_1^{\text{sat}}$  = solvent activity

$P$  = vapor pressure in Torr

$P_1^{\text{sat}}$  = pure-solvent saturation pressure (calculated from equations suggested by Daubert and Danner<sup>15</sup>) in Torr

Solvent: Chloroform; T = 50°C; $P_1^{\text{sat}} = 526$ Torr				
$w_1$ (linear <sup>a</sup> )	$a_1$	$w_1$ (S05-1)	$w_1$ (S05-3)	$a_1$
0.043	0.088	0.138	0.139	0.279
0.160	0.327	0.190	0.184	0.369
0.288	0.541	0.351	0.349	0.627
0.378	0.673	0.453	0.449	0.760
0.468	0.782	0.541	0.538	0.855
0.544	0.859			
Solvent: Toluene; T = 70°C; $P_1^{\text{sat}} = 204$ Torr				
$w_1$ (linear <sup>b</sup> )	$w_1$ (S05-1)	$w_1$ (S05-3)	$a_1$	
0.020	0.020	0.027	0.066	
0.048	0.041	0.048	0.180	
0.082	0.078	0.076	0.294	
0.116	0.110	0.108	0.403	
0.155	0.142	0.146	0.506	
0.188	0.177	0.181	0.594	
0.244	0.232	0.235	0.691	
0.307	0.293	0.303	0.785	
0.404	0.379	0.398	0.855	
Solvent: Cyclohexane; T = 70°C; $P_1^{\text{sat}} = 544$ Torr				
$w_1$ (linear <sup>b</sup> )	$w_1$ (S05-1)	$w_1$ (S05-3)	$a_1$	
0.024	0.025	0.020	0.348	
0.046	0.052	0.036	0.468	
0.077	0.081	0.060	0.612	
0.099	0.106	0.078	0.724	
0.108	0.114	0.093	0.803	
0.115	0.129	0.100	0.852	

<sup>a</sup>  $M_w = 1.75 \times 10^4$  g/mol

<sup>b</sup>  $M_w = 5.0 \times 10^4$  g/mol

**Table 5** Flory-Huggins interaction parameters

Solvent	T (°C)	Linear Polystyrene	$\chi_{FH}$	
			S05-1	S05-3
chloroform	50	0.238 <sup>a</sup>	0.207	0.219
toluene	70	0.318 <sup>b</sup>	0.382	0.353
cyclohexane	70	1.187 <sup>b</sup>	1.123	1.337

<sup>a</sup>  $M_w = 1.75 \times 10^4$  g/mol

<sup>b</sup>  $M_w = 5.0 \times 10^4$  g/mol

**Table 6** Osmotic second virial coefficients for S05-1, S05-3 and linear polystyrene from Gauthier et al.<sup>4</sup>;  $A_2$  extrapolated to 70°C

Solvent	$A_2$ (cm <sup>3</sup> ·mol / g <sup>2</sup> )		
	Linear Polystyrene <sup>a</sup>	S05-0	S05-1
toluene	$7.78 \times 10^{-4}$	$3.14 \times 10^{-4}$	$3.48 \times 10^{-5}$
cyclohexane	$1.77 \times 10^{-4}$	$1.31 \times 10^{-4}$	$1.32 \times 10^{-5}$

<sup>a</sup>  $M_w = 7.3 \times 10^4$  g/mol

**Table 7** Flory parameters calculated from osmotic second virial coefficients for S05-1, S05-3 and linear polystyrene;  $A_2$  extrapolated to 70°C

$\chi_{FH} = 0.5 - v_1 \rho_2^2 A_2$			
Solvent	Linear Polystyrene <sup>a</sup>	S05-0	S05-1
toluene	0.413	0.465	0.496
cyclohexane	0.480	0.485	0.498

<sup>a</sup>  $M_w = 7.3 \times 10^4$  g/mol

## Figure Captions

**Figure 1** Experimental apparatus for vapor-liquid equilibrium measurements.

**Figure 2** Solvent activities for binary solutions of S05-1, S05-3 and linear polystyrene in chloroform at 50°C; fitted curves calculated with the Flory-Huggins equation; linear polystyrene with  $M_w = 17,500$  g/mol

**Figure 3** Solvent activities for binary solutions of S05-1, S05-3 and linear polystyrene in toluene at 70°C; fitted curves calculated with the Flory-Huggins equation; linear polystyrene with  $M_w = 50,000$  g/mol

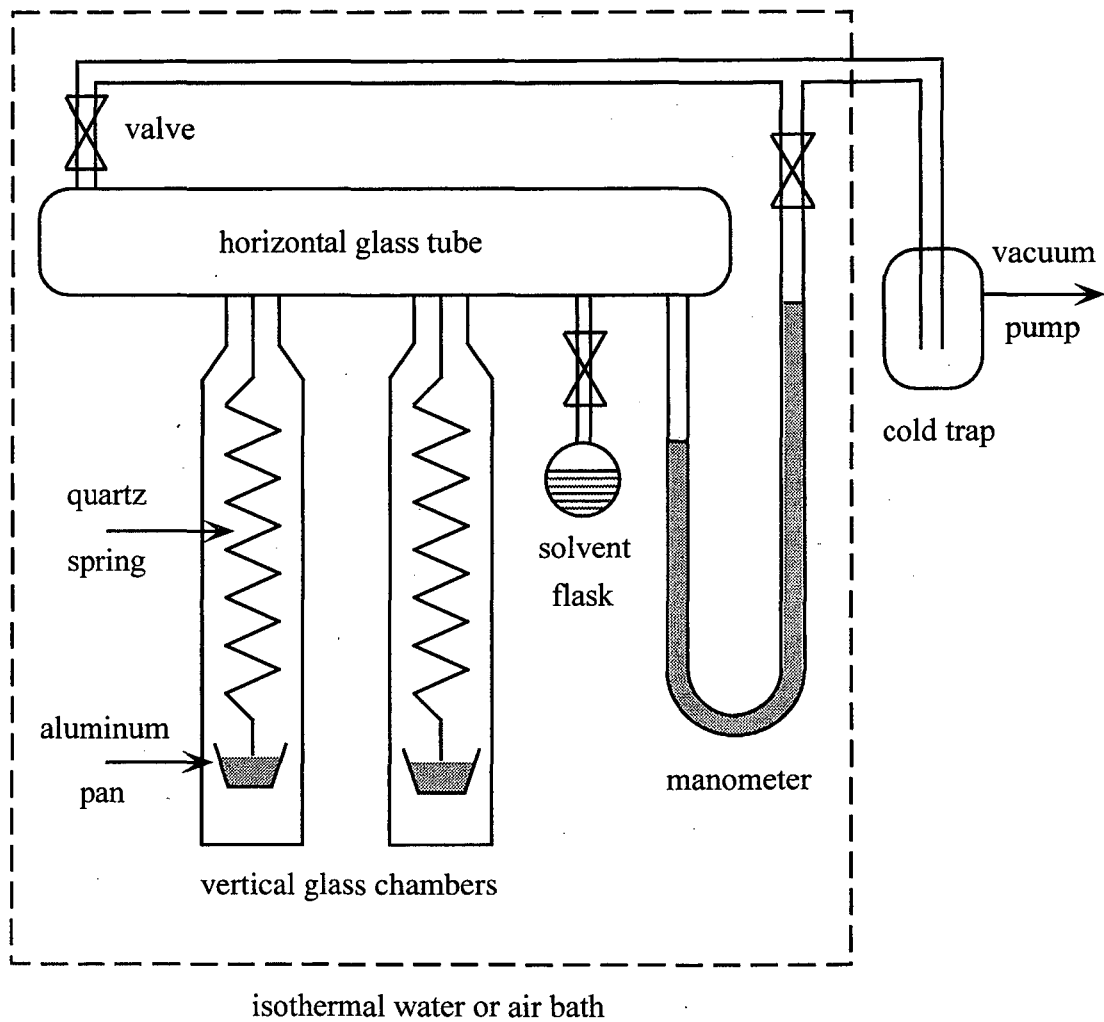
**Figure 4** Solvent activities for binary solutions of S05-1, S05-3 and linear polystyrene in cyclohexane at 70°C; fitted curves calculated with the Flory-Huggins equation; linear polystyrene with  $M_w = 50,000$  g/mol

**Figure 5** Solvent activity data for binary solutions of:

linear polystyrene with  $M_n = 290,000$  g/mol in chloroform;  $T = 50^\circ\text{C}$ ; Bawn et al.<sup>9</sup>

linear polystyrene with  $M_n = 10,300$  g/mol in toluene;  $T = 48.5^\circ\text{C}$ ; Tait et al.<sup>11</sup>

linear polystyrene with  $M_n = 25,100$  g/mol in cyclohexane;  $T = 44^\circ\text{C}$ ; Krigbaum et al.<sup>12</sup>



**Figure 1** Experimental apparatus for vapor-liquid-equilibrium measurements



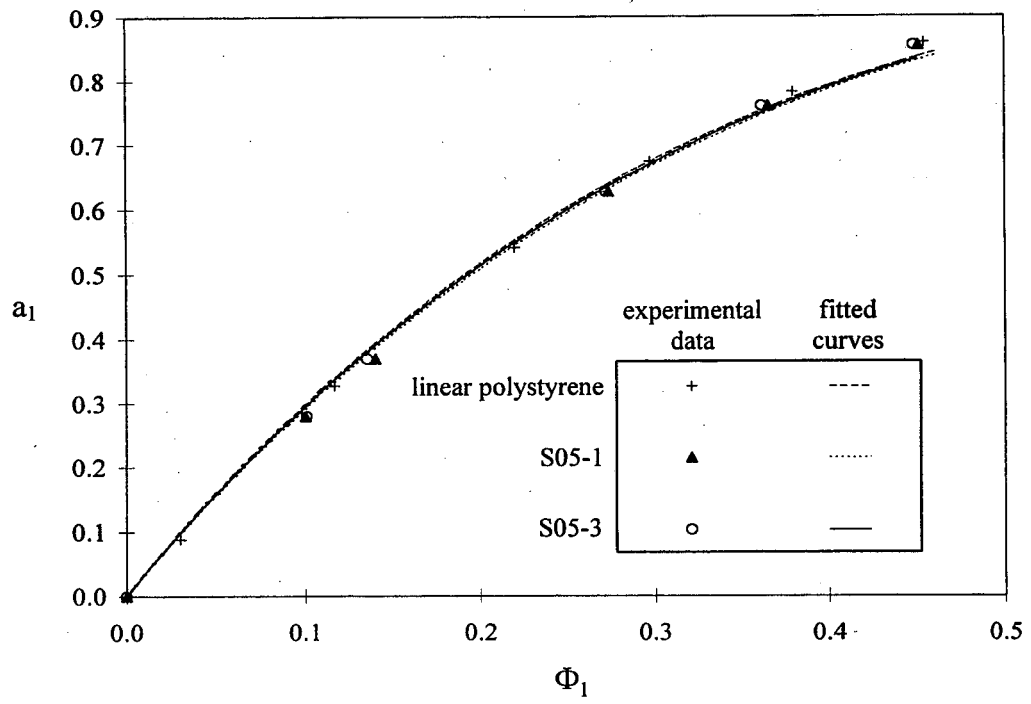


Figure 2

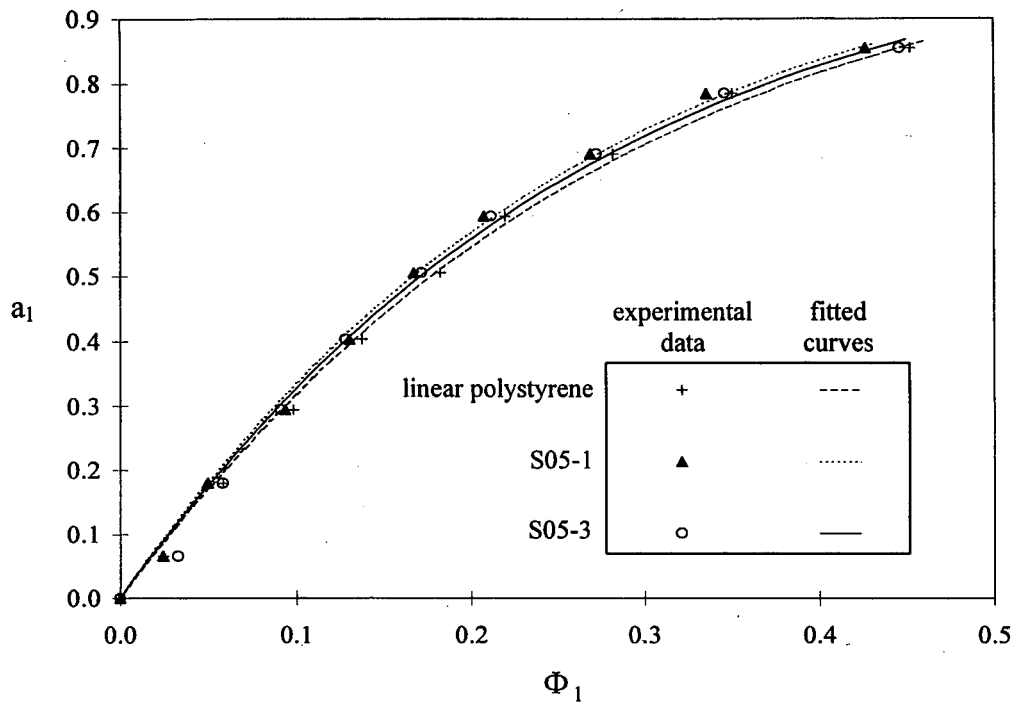


Figure 3

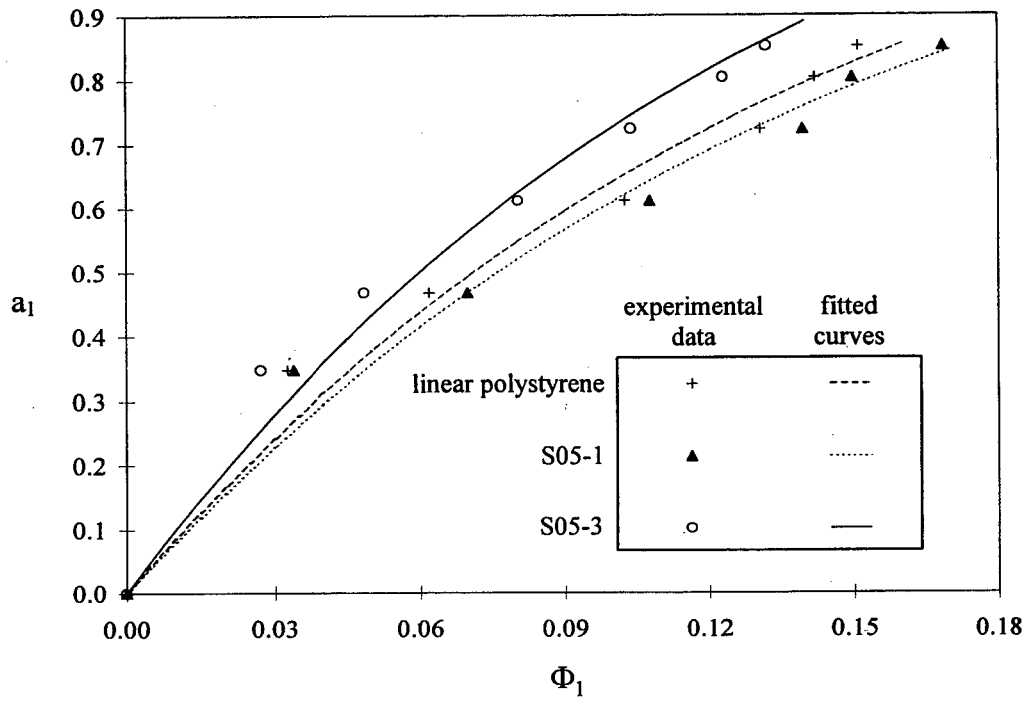


Figure 4

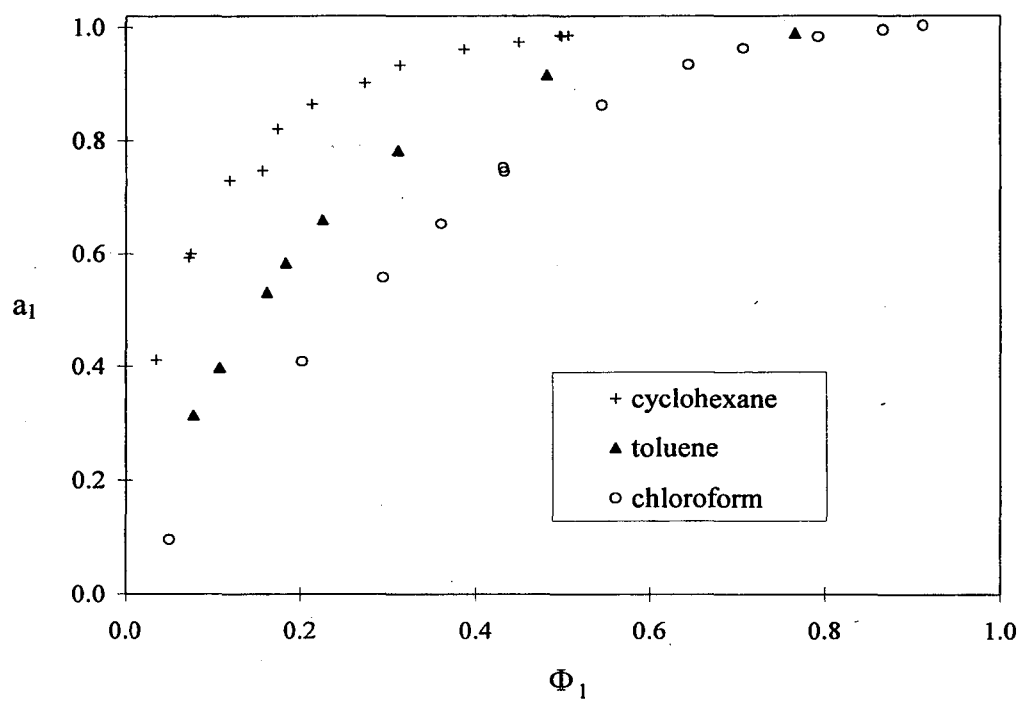


Figure 5

ERNEST ORLANDO LAWRENCE BERKELEY NATIONAL LABORATORY  
ONE CYCLOTRON ROAD BERKELEY, CALIFORNIA 94720