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# Divergent Synthesis of Bipolar Membranes Combining Strong Interfacial Adhesion and High-Rate Capability

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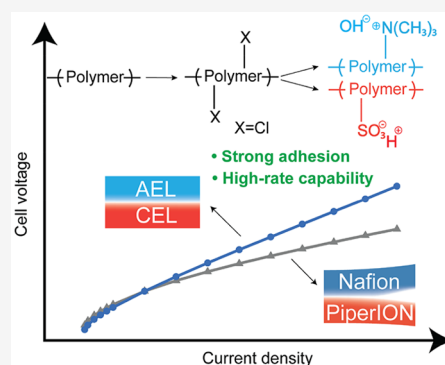


Article Recommendations



Supporting Information

**ABSTRACT:** Bipolar membranes are emerging as attractive solid electrolytes for water electrolysis, electrochemical CO<sub>2</sub> reduction, and CO<sub>2</sub> capture by base from electro dialysis. The development of these technologies is currently hampered by the resistance of current commercial materials under reversed bias, as well as interfacial incompatibility between the layers that can lead to delamination. This letter reports a divergent route to a nonfluorinated TiO<sub>2</sub>-catalyzed bipolar membrane, where the interfacial compatibility is governed by constructing the cation/anion exchange layers from the same backbone chemistry. We show that this BPM design concept has the potential to drastically enhance the adhesion strength at the interfacial junction, without compromising rate capability under bipolar membrane water electrolysis conditions.



A bipolar membrane (BPM) is a laminate of anion- and cation-exchange ionomer layers that can support water dissociation and ionic separation of H<sup>+</sup> and OH<sup>-</sup> ions under the influence of an applied voltage.<sup>1–3</sup> The result is the buildup of a pH gradient across the BPM, which can be used for pH adjustments in various industrial chemical and biochemical processes.<sup>4,5</sup> BPM electro dialysis can also be used for acid/base generation from aqueous salt solutions<sup>6</sup> and further in conjunction with CO<sub>2</sub> capture processes that use pH swings.<sup>7,8</sup> Furthermore, the use of a BPM in water and CO<sub>2</sub> electrolysis cells has been found to effectively mitigate unwanted reactant/product crossover<sup>9,10</sup> and to provide electrochemical environments that contribute to performance gains and to improved utilization of precious metals.<sup>11–15</sup>

One of the main hurdles in the development of electrochemical devices based on BPMs is the high resistance of commercial materials at practical current densities, which mainly originates from the slow water dissociation (WD) reaction at the interface between the anion and cation exchange layers.<sup>16</sup> This has triggered tremendous research efforts spanning from mapping and probing of phenomena that govern water dissociation and ionic separation<sup>17–19</sup> to the design of new BPMs with enhanced water dissociation activity<sup>20–23</sup> and mass transport characteristics.<sup>13,24</sup> The evaluation of different water dissociation catalysts currently points to graphene oxide,<sup>25–27</sup> TiO<sub>2</sub>,<sup>23</sup> and SnO<sub>2</sub><sup>28</sup> as good candidates that combine high activity, earth abundance, and good stability. Remarkably high-rate capability has recently

been reported for TiO<sub>2</sub>- and SnO<sub>2</sub>-catalyzed BPMs with cation exchange layers (CELs) and anion exchange layers (AELs) based on perfluorosulfonic acid (Nafion) and poly(arylene piperidinium) (PiperION), respectively.<sup>18,23,28</sup>

A large majority of the BPMs reported in the literature are based on individual CELs/AELs of vastly different backbone chemistry, which often result in low adhesion strength at the CEL/AEL interface and therefore blistering and delamination during operation.<sup>2</sup> Physical anchoring of the individual layers by entanglement of nanofibers at the interface<sup>20,22,29,30</sup> or covalent interlocking<sup>31,32</sup> has recently been explored to mitigate delamination. Furthermore, many of the reported BPMs are constructed based on perfluorinated CELs, which may be problematic from environmental and sustainability perspectives.<sup>33</sup>

This work addresses these challenges by constructing a BPM based on a single nonfluorinated polymer through divergent functionalization of poly(styrene-*b*-poly(ethylene-*ran*-butylene)-*b*-polystyrene) (SEBS). As shown in Scheme 1, the individual layers were obtained via chloromethylation, followed

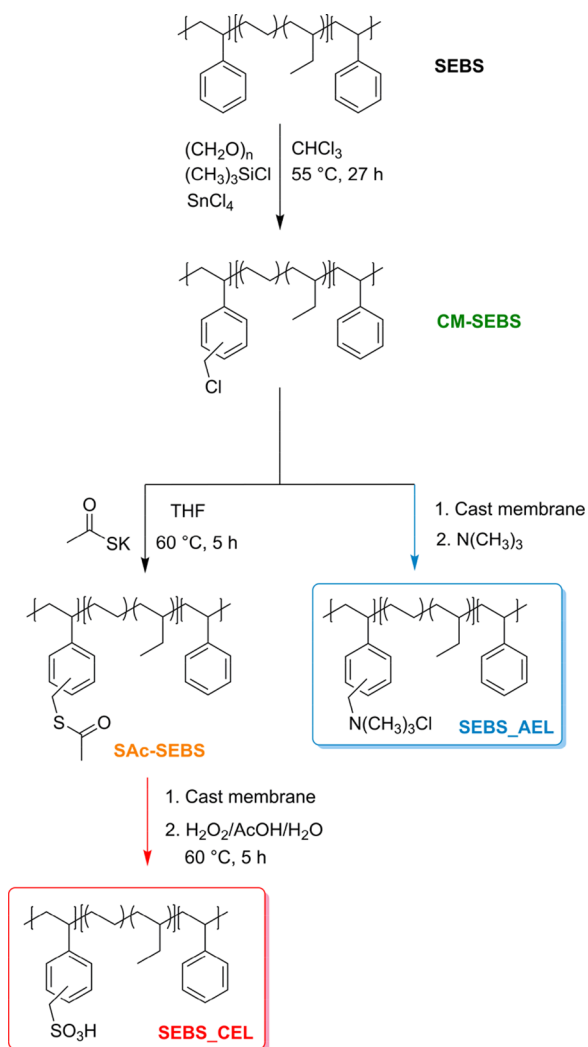
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**Scheme 1. Divergent Synthetic Route to the Individual Layers of the BPM<sup>a</sup>**


<sup>a</sup>The degree of chloromethylation, calculated from  $^1\text{H}$  NMR data, was 73% of the styrene unit in the parent SEBS. Chloromethylated SEBS (CM-SEBS) underwent the divergent route to form the quaternary ammonium SEBS as SEBS\_AEL and the sulfonated SEBS as SEBS\_CEL (see section S1.2 for details).

by a heterogeneous Menshutkin reaction for the AEL<sup>34</sup> or substitution with thioacetate followed by heterogeneous oxidation to the corresponding sulfonic acid for the CEL.<sup>35</sup> The precursor polymer films were cast to a thickness of 50–60  $\mu\text{m}$ , and the final synthetic steps were carried out heterogeneously due to the insolubility of the sulfonated

SEBS (SEBS\_CEL) and quaternary ammonium functionalized SEBS (SEBS\_AEL). The  $^1\text{H}$  NMR and FTIR spectra of the intermediates and products are shown in Figures S1 and S2, respectively. Table 1 summarizes the ion-exchange capacity (IEC), water uptake (WU), swelling in thickness ( $\text{SW}_T$ ), and in-plane ionic conductivity of the individual SEBS\_AEL and SEBS\_CEL. Both layers were derived from the same polymer precursor, and the IECs were therefore similar. However, the SEBS\_AEL showed a considerably higher WU than the SEBS\_CEL.

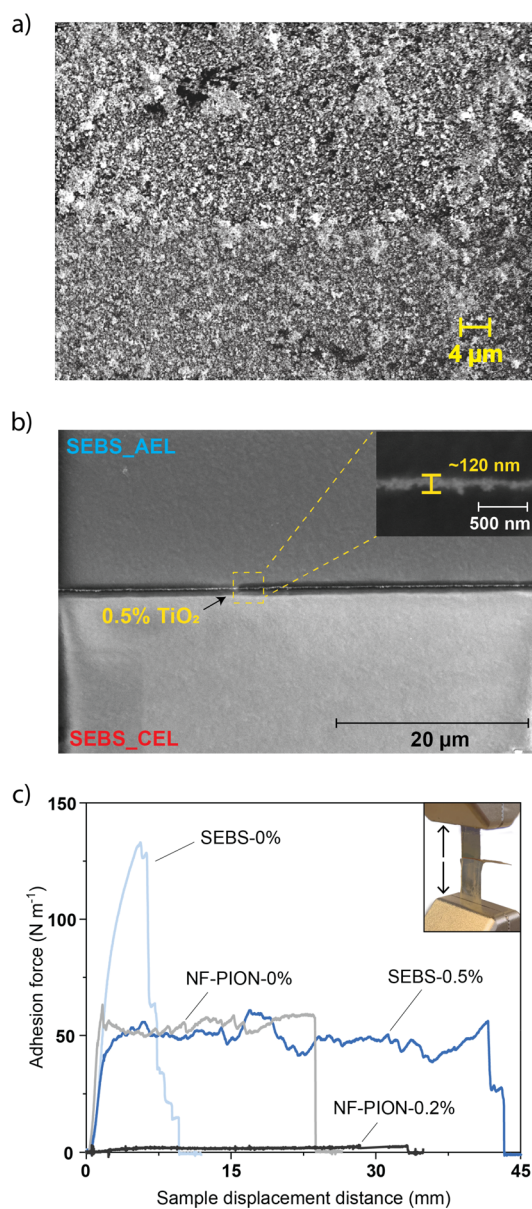
The SEBS-derived BPMs (SEBS\_BPM) were thereafter prepared by spin coating an ink of  $\text{TiO}_2$  dispersed in a  $\text{H}_2\text{O}/\text{IPA}$  mixture onto the SEBS\_CEL (in  $\text{H}^+$  form), followed by lamination of the SEBS\_AEL (in  $\text{OH}^-$  form) without pressing. Figure 1a,b shows SEM top-down and cross-section images of the SEBS\_BPM prepared from an ink containing 0.5%  $\text{TiO}_2$ , respectively. The thickness of the  $\text{TiO}_2$  interfacial layer was estimated to be 120 nm, and the top-down morphology image shows a nearly complete  $\text{TiO}_2$  coverage of the SEBS\_CEL surface. Different loadings of  $\text{TiO}_2$  were achieved by spin coating with an ink dispersion of different  $\text{TiO}_2$  concentrations in a 1:1 weight ratio of a  $\text{H}_2\text{O}/\text{IPA}$  mixture onto the SEBS\_CEL surface. The specific mass loading of  $\text{TiO}_2$  could not be determined reliably by conventional gravimetric methods due to the small masses and the response to humidity changes. Therefore, the obtained BPMs are denoted as SEBS-XX%, where XX is the  $\text{TiO}_2$  content of the spin coating ink, in line with procedures described in the literature.<sup>18</sup> An estimation of the corresponding  $\text{TiO}_2$  mass loadings based on SEM top-down images using *ImageJ* is shown in section S1.5 in the Supporting Information. Note that 0.2%, 0.5%, and 1% were used as the concentrations prepared, while samples with 2% and 4% were prepared by 1% ink spin coated two and four times, respectively. Thus, the notations 2% and 4% do not correspond to the specific ink concentrations but refer to the spin-coating of 2 and 4 layers of the 1% ink, respectively. The morphology of the  $\text{TiO}_2$ -coated SEBS\_CEL was examined via top-down SEM imaging, with 0.2% showing the lowest surface coverage of  $\text{TiO}_2$ , while 4% had the densest surface coverage (Figure S5).

In addition to having a straightforward synthetic route for the BPM development, our hypothesis was that the identical backbone chemistry would lead to improved junction adhesion, in particular for BPMs fabricated from direct lamination. To test this hypothesis, the interfacial layer compatibility of the SEBS\_BPM was assessed by recording the adhesion force between SEBS\_CEL and SEBS\_AEL with and without  $\text{TiO}_2$  at the interface via a T-peel strength test (Figure 1c). The junction adhesion force of SEBS\_BPM was compared with the baseline 2D junction BPMs derived from

**Table 1. Ion Exchange Capacity, Conductivity, Water Uptake, and Swelling of the Individual SEBS\_CEL and SEBS\_AEL with Thicknesses of  $86 \pm 3$  and  $66 \pm 4 \mu\text{m}$ , Respectively<sup>a</sup>**

	IEC (meq/g)	conductivity (mS/cm) <sup>b</sup>	WU (%)	$\text{SW}_T$ (%)	$\lambda$ ( $\text{H}_2\text{O}$ per $-\text{SO}_3^-$ or $-\text{N}(\text{CH}_3)_3^+$ )
SEBS_CEL	$1.51 \pm 0.09$	46 ( $25^\circ\text{C}$ )	$39.0 \pm 4$ ( $22^\circ\text{C}$ )	$22.1 \pm 7.2$ ( $22^\circ\text{C}$ )	$14.4 \pm 1.3$ ( $22^\circ\text{C}$ )
		71 ( $55^\circ\text{C}$ )	$48.1 \pm 2.4$ ( $55^\circ\text{C}$ )	$28.4 \pm 8.0$ ( $55^\circ\text{C}$ )	$17.8 \pm 1.5$ ( $55^\circ\text{C}$ )
SEBS_AEL	$1.46 \pm 0.07$	41 ( $25^\circ\text{C}$ )	$84.4 \pm 16$ ( $22^\circ\text{C}$ )	$8.0 \pm 2.0$ ( $22^\circ\text{C}$ )	$32.4 \pm 7.6$ ( $22^\circ\text{C}$ )
		65 ( $55^\circ\text{C}$ )	$100 \pm 10$ ( $55^\circ\text{C}$ )	$17.7 \pm 7.3$ ( $55^\circ\text{C}$ )	$38.3 \pm 5.5$ ( $55^\circ\text{C}$ )

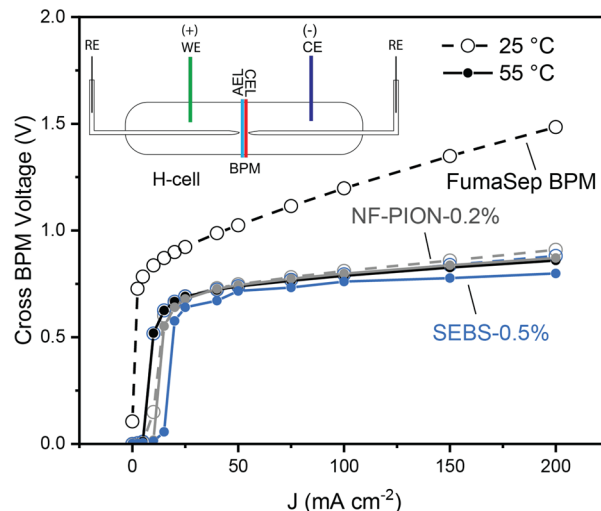
<sup>a</sup>The conductivity data are the average of two samples, while the other data represent the average and standard deviation for three samples. <sup>b</sup>CEL in  $\text{H}^+$  form and AEL in  $\text{OH}^-$  form. The true  $\text{OH}^-$  conductivity was determined as described in the literature;<sup>36</sup> see Figure S4. <sup>c</sup>Measured at room temperature:  $\sim 22 \pm 2^\circ\text{C}$ .



**Figure 1.** (a) Top-down SEM image of SEBS\_CEL spin coated with an ink containing 0.5% TiO<sub>2</sub>. (b) Cross-sectional SEM of SEBS-0.5% with a thickness of the interfacial layer of ca. 120 nm. (c) Adhesion force as a function of sample displacement from a 180° T-peel strength for SEBS and NF-PION with and without water dissociation catalyst. The inset shows a photograph of SEBS-0.5% during the T-peel test.

Nafion and PiperION (NF-PION).<sup>23</sup> For the pristine SEBS\_CEL and SEBS\_AEL laminate without TiO<sub>2</sub> between the layers, the test resulted in deformation of the bulk materials rather than delamination, indicating high interfacial compatibility and strong adhesion energy. A strong adhesion can be observed upon contact of SEBS\_CEL and SEBS\_AEL, as shown in a video in the Supporting Information. The adhesion force of a NF-PION laminate without water dissociation catalyst was 50 N m<sup>-1</sup>. After application of TiO<sub>2</sub> from an ink with a concentration of 0.2%, which has been identified as the optimal composition for the NF-PION system,<sup>23</sup> the adhesion force of the NF-PION laminate was only around 5 N m<sup>-1</sup>, while the adhesion force of the SEBS\_BPM was about 1 order of magnitude higher.

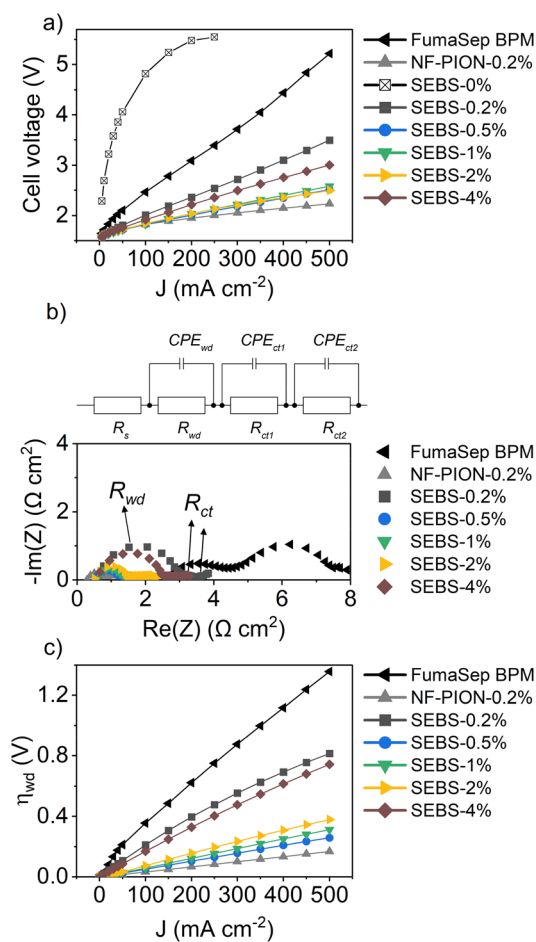
After comprehensive chemical and physical characterizations of the SEBS\_CEL and SEBS\_AEL, the BPM prepared from an ink containing 0.5% TiO<sub>2</sub> (i.e., SEBS-0.5%) was examined and compared with a commercial BPM (FumaSep FBM) in a four-electrode H-cell using neutral electrolyte of 0.5 M aqueous KNO<sub>3</sub>. The polarization curves (*j*-*V* curve) at 25 and 55 °C are shown in Figure 2. H-cell measurements have been



**Figure 2.** BPM polarization curves recorded in a four-electrode H-cell at 25 and 55 °C using 0.5 M aqueous KNO<sub>3</sub> as electrolyte. The voltage across the BPM was estimated from the voltage measured between two Ag/AgCl reference electrodes placed in Luggin capillaries near each side of the BPM as a function of applied current densities.  $V_{\text{onset}}$  values at 25 °C are 0.85, 0.69, and 0.68 V for FumaSep BPM, SEBS-0.5%, and NF-PION-0.2%, respectively.

extensively used as a first-line evaluation tool to assess the water dissociation performance before implementing the fabricated BPM in various applications.<sup>16,29,30,37,38</sup> The *j*-*V* curve of a BPM with neutral electrolyte in the H-cell characterizes the onset of the water dissociation reaction when the cross membrane voltage (not *iR* corrected) exceeds the thermodynamic potential of 0.83 V at standard conditions (protons in the CEL and hydroxide in the AEL are each at unit activity) across the BPM interface.<sup>3,5</sup> As shown in Figure S6, the onset potential ( $V_{\text{onset}}$ ) was determined by the intersection of two tangent lines of the polarization curve before and after the evident start of the water dissociation reaction.<sup>21,29</sup> The onset potential of 0.85 V determined for the commercial FumaSep BPM at 25 °C is in good agreement with previous studies under similar conditions (Table S2).<sup>21,27,29,30</sup>  $V_{\text{onset}} = 0.69$  V of SEBS-0.5% at 25 °C is close to those of various customized BPMs reported in the literature, as summarized in Table S2. The elevated temperature resulted in lowered cross-membrane voltages, with a more significant impact on the commercial FumaSep BPM. The temperature dependence of the SEBS-0.5% was similar to that of the NF-PION-0.2%, which is discussed in more detail elsewhere.<sup>18</sup> At low cross BPM voltages (before the  $V_{\text{onset}}$ ), 2D junction BPMs show slightly higher currents contributed from the co-ion crossover than the FumaSep BPM.

Following the initial H-cell tests of SEBS-0.5%, the impact of TiO<sub>2</sub> loading on polarization performance was thereafter characterized in a membrane electrode assembly (MEA) water electrolyzer fed by pure water at 55 °C (Figure 3a). The cell



**Figure 3.** (a) Water electrolysis  $j$ - $V$  curves in MEA at 55 °C fabricated with the SEBS-derived BPM with different  $\text{TiO}_2$  loadings, using  $\text{Co}_3\text{O}_4$  on stainless steel for the anode and Pt black on carbon for the cathode. (b) Nyquist plots of the SEBS-derived BPM with different  $\text{TiO}_2$  loadings at 100  $\text{mA cm}^{-2}$ . The semicircle at high frequency is related to  $R_{wd}$  while the semicircles at low frequency are associated to  $R_{ct}$ .  $R_{ct}$  is the sum of  $R_{ct1}$  +  $R_{ct2}$ . The equivalent circuit is used to fit the EIS data, and the fitting results are shown in Figure S9 (c)  $\eta_{wd}$  values of the SEBS\_BPM with different  $\text{TiO}_2$  loadings extracted from the EIS data.

voltages at 500  $\text{mA cm}^{-2}$  for SEBS-0.2%, SEBS-0.5%, SEBS-1%, SEBS-2%, and SEBS-4% were 3.5, 2.5, 2.6, 2.5, and 3.0 V, respectively. This trend is consistent with the loading dependence on BPM's performance previously reported for NF-PION,<sup>23</sup> but with an optimum at slightly higher  $\text{TiO}_2$  loading for the SEBS-derived analogue (SEBS-0.5%). As shown in Figure S5, SEBS-0.2% presented a relatively low  $\text{TiO}_2$  coverage, while the coverage of SEBS-0.5% was nearly complete. The lower performance of SEBS-1%, SEBS-2%, and SEBS-4% could likely be explained by a larger thickness of the junction, which lowers the electric field across the junction and results in increasing ionic resistance for  $\text{H}^+$  and  $\text{OH}^-$  ions migrating from the junction toward the SEBS\_CEL and SEBS\_AEL, respectively.<sup>39</sup>

In contrast to the cell equipped with the FumaSep membrane, the cells with the SEBS-derived BPM showed no apparent signs of mass transport limitations at  $>300 \text{ mA cm}^{-2}$ . Mass transport of water may become critical during operation at high current densities,<sup>13,24</sup> and the high WU of the

SEBS\_AEL could potentially play an important role in the water management of this electrolyte system.

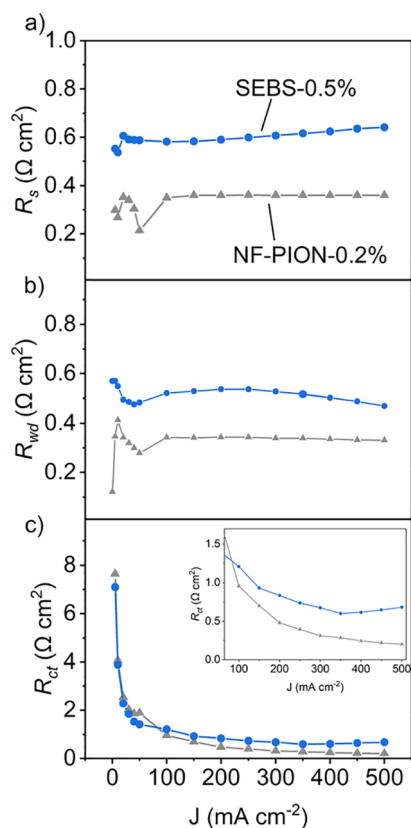
Since the MEA electrolyzer cell voltage contains contributions from the anode and cathode, the water dissociation overpotential ( $\eta_{wd}$ ) is a more appropriate performance indicator of the BPM alone. As previously reported,<sup>23</sup>  $\eta_{wd}$  can be isolated via electrochemical impedance spectroscopy (EIS) by identifying the water dissociation resistance ( $R_{wd}$ ) as associated with the high-frequency impedance arc from the total-cell impedance in a Nyquist plot (Figure 3b). The resistance contributions were acquired by fitting EIS results to the equivalent circuit shown in Figure 3b. The high-frequency semicircle represents  $R_{wd}$ , and the low-frequency semicircles represent the charge-transfer resistance ( $R_{ct}$ ), where  $R_{ct}$  is the sum of the charge transfer resistances of both electrodes ( $R_{ct1}$  and  $R_{ct2}$ ). According to eq 1, integrating  $R_{wd}$  as a function of current density allows us to extract  $\eta_{wd}$ , which is shown in Figure 3c.

$$\eta_{wd} = \int_0^j R_{wd}(j) dj \quad (1)$$

The trend of  $\eta_{wd}$  with different  $\text{TiO}_2$  loadings corresponds to the trend of the cell voltage, with 0.5%  $\text{TiO}_2$  possessing the lowest  $\eta_{wd}$  of 0.26 V at 500  $\text{mA cm}^{-2}$  among all loadings. The best-performing SEBS-0.5% not only outperformed the commercial BPM but also showed performance comparable to that of the NF-PION-derived BPM in an MEA water electrolyzer equipped with identical electrodes and operated under similar conditions. We note that the commercial FumaSep BPM includes an embedded reinforcement material in the membrane, which may contribute additional resistance, especially in the MEA measurements.

Figure 4 shows the  $R_s$ ,  $R_{wd}$ , and  $R_{ct}$  values of NF-PION and the SEBS-0.5% at various current densities. The EIS fitting results agree with results from Chen et al.,<sup>23</sup> where  $R_s$  and  $R_{wd}$  remain nearly constant and  $R_{ct}$  changes across current densities. Table 2 summarizes the resistance contributions in the MEA water electrolyzer at 30 and 450  $\text{mA cm}^{-2}$ , which indicate that the better cell performance of the cell equipped with NF-PION is due to lower Ohmic resistance ( $R_s$ ) and  $R_{wd}$ . Although electrode conditions for the redox reactions were kept identical, the different membrane-electrode interfaces may be the reason for unexpected deviations on  $R_{ct}$  of both BPMs. To keep the conditions consistent with previous work, Nafion and PiperION ionomer were used for the cathode and anode fabrication, respectively, which could contribute to incompatibility between electrodes and the BPM. To further analyze the performance difference, the expected area-specific resistances originating from the CEL and AEL was calculated from the specific conductivity data for the individual layers assuming isotropic conductivity behavior and were found to be 0.27 and 0.11  $\Omega \text{ cm}^2$  at 55 °C for the SEBS\_BPM and NF-PION, respectively. These values correspond to the higher  $R_s$  and  $R_{wd}$  of the SEBS\_BPM from the EIS analysis, indicating the overall performance difference is a result of the conductivity differences of the membrane constituents and not specific to the BPM junction where water dissociation occurs.

The stability of SEBS-0.5% was measured in a MEA electrolyzer operating with a pure-water feed at 500  $\text{mA cm}^{-2}$  at 55 °C. Polarization curves and impedance data at current densities of 500, 100, 50, and 30  $\text{mA cm}^{-2}$  were collected every 3 h at 500  $\text{mA cm}^{-2}$ . The polarization curves



**Figure 4.** Resistance contributions from  $R_s$  (a),  $R_{wd}$  (b), and  $R_{ct}$  (c) of the SEBS-0.5% and NF-PION-0.2% at various current densities extracted from EIS analysis of BPMs in an MEA water electrolyzer. The inset is a zoom-in at higher current densities.

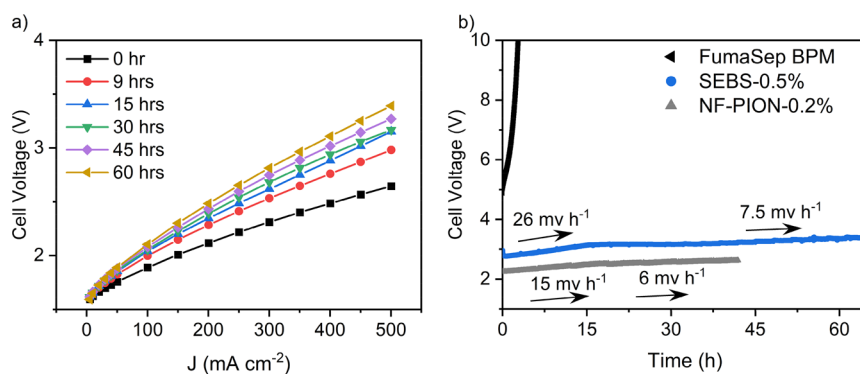
**Table 2.** Comparison of Resistance Contributions in the MEA Water Electrolyzer at 30/450 mA cm<sup>-2</sup>

BPM type	$R_s$ (Ω cm <sup>2</sup> )	$R_{wd}$ (Ω cm <sup>2</sup> )	$R_{ct}$ (Ω cm <sup>2</sup> )
NF-PION-0.2%	0.33/0.36	0.32/0.33	2.03/0.22
SEBS-0.5%	0.59/0.64	0.49/0.48	1.84/0.65

and time evolution of cell voltage are shown in Figure 5a,b, respectively. After the initial characterization cycle to collect the  $j$ - $V$  curve, the cell ran for 60 h with a degradation rate of 26 mV h<sup>-1</sup> in the first 15 h and 7.5 mV h<sup>-1</sup> after 36 h. After electrolysis testing, the GDEs were strongly adhering to SEBS-

0.5% and could not be delaminated. For comparison, the NF-PION-0.2% showed a voltage increase of 15 mV h<sup>-1</sup> during the first 18 h and 6 mV h<sup>-1</sup> during the following 18 h,<sup>23</sup> while a rapid degradation in voltage efficiency of the FumaSep BPM was observed within 3 h. The faster voltage increase of the SEBS-0.5% in the beginning of the test may be due to degradation of the AEL, which was equipped with cationic headgroups in benzylic positions that are known to be relatively unstable.<sup>40,41</sup> Ionomer oxidation within the anode may also contribute to the voltage increase,<sup>42</sup> as the cell is operated in pure water without supporting electrolyte to facilitate ionic contact at the BPM–electrode interface. The impedance data also show evidence of degradation over the 60 h test (Figure S10). The increasing  $R_{wd}$  values at both low and high current densities indicate degradation of the BPM junction, which confirms the aforementioned degradation of the SEBS\_AEL. Although  $R_{ct}$  remains stable at the low current densities, it is worth noting that the long-term operation can still suffer from oxidative instability of the anode ionomer.<sup>42</sup> It should be noted that the low-frequency EIS data at 500 mA cm<sup>-2</sup> is noisy, which results in unreliable fitting values of  $R_{ct}$  (Figure S10d). This may be related to degradation of the electrodes at high current densities. Although ex situ studies have shown that the SEBS\_AEL shows relatively good stability in 1 M KOH at 60 °C during 30 days,<sup>43</sup> substitution of the cationic head groups with more stable chemistries in combination with the introduction of alkyl spacers to circumvent common degradation pathways will in any case be expected to improve the operating lifetime, perhaps in combination with a protective barrier layer between catalysts and ionomer to mitigate anode degradation.<sup>44</sup>

In summary, this study presents a divergent synthesis route for preparing a BPM from the same polymer backbone structure. The identical polymer backbone matrix with different functional groups was prepared from the same precursor through one-step chloromethylation on the aromatic unit of the backbone structure. The CEL and AEL of a BPM derived from the same precursor ensures the identical backbone structure, which may provide an advantage toward compatibility of the two membrane layers. The elastomeric nature of SEBS and excellent adhesion enabled construction of simple 2D junction morphologies with high-rate capability through direct lamination of the two layers. In an MEA water electrolyzer, the SEBS-derived BPM not only outperformed the commercial FumaSep BPM but also showed performance



**Figure 5.** (a) Polarization curves of SEBS-0.5% at different points of operation. (b) Voltage evolution of a MEA water electrolyzer equipped with FumaSep BPM, SEBS-0.5%, and NF-PION-0.2%<sup>23</sup> at 500 mA cm<sup>-2</sup> at 55 °C (stability test started after the initial current cycle and EIS measurements).

comparable to the best-performing BPM reported in the literature so far. While there is room for improvement in terms of polarization behavior and performance stability through continued optimization of polymer chemistries and junction composition, this work describes a new BPM design concept with the potential to materialize into a new class of nonfluorinated and high-performing BPM for electrochemical devices.

## ■ ASSOCIATED CONTENT

### SI Supporting Information

The Supporting Information is available free of charge at <https://pubs.acs.org/doi/10.1021/acseenergylett.4c01178>.

Experimental details,  $^1\text{H}$  NMR and FTIR data of polymers, illustration showing BPM fabrication process and adhesion between the layers, conductivity data, top-down SEM micrographs after  $\text{TiO}_2$  coating, reverse/forward bias cycling, determination of water dissociation onset potential, and electrochemical data for the water electrolysis tests (PDF)

Video showing BPM fabrication process and adhesion between the layers (MP4)

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### Notes

The authors declare no competing financial interest.

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