Journal of The Electrochemical Society, **162** (14) F1-F36 (2015) 0013-4651/2015/162(14)/F1/36/\$33.00 © The Electrochemical Society

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Review—Recent Progress in Electrocatalysts for Oxygen Reduction Suitable for Alkaline Anion Exchange Membrane Fuel Cells

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Alkaline fuel cell technology has been reinvigorated since the recent rapid development and deployment of anion exchange membranes. Without the "acid-stability" requirement in low pH environments such as that of proton exchange membrane fuel cells, a much wider range of materials including noble metals, non-noble transition metals, and even metal-free electrocatalysts for the oxygen reduction reaction (ORR) in alkaline media have been developed due to both thermodynamic and kinetic reasons. As compared to the rapidly increasing number of reports on the development of novel catalyst materials, the understanding of the reaction mechanisms of the various ORR electrocatalysts is quite insufficient, and the application and investigation in real alkaline anion exchange membrane fuel cells (AAEMFCs) is even scarcer. By reviewing the compositions, preparation methods, physiochemical properties and ORR performance of different categories of cathodic electrocatalysts that have emerged in the past few years, some common and intrinsic properties and factors that account for the superior activity of these materials may be extracted and summarized, which may further help to identify the reasons for the kinetic facility of the ORR in alkaline media. Some practical issues of utilization of the promising novel replacement materials for the state-of-the-art Pt-based cathodic electrocatalysts in AAEMFCs are pointed out. In addition to the progress on the development of novel materials with outstanding ORR activity, many and varied compositions and morphologies in one, two and three dimensions, scalable preparation technologies, low cost, and other unique properties, some feedback on the performance and especially the problems of their use as cathodes in AAEMFCs is urgently needed. Such feedback should provide guidelines for the design and manufacture of next-generation electrocatalysts and accelerate the application of AAEMFCs. © 2015 The Electrochemical Society. [DOI: 10.1149/2.0551514jes] All rights reserved.

Manuscript submitted August 5, 2015; revised manuscript received September 21, 2015. Published 00 0, 2015.

Although the alkaline fuel cell (AFC) was the first to be put into 27 practical use in the history of fuel cells, it has been largely ignored by 28 the electrochemical research community for decades due to technical 29 problems¹⁻³ and some other economic factors. A renaissance of AFC 30 technology was catalyzed by the replacement of the conventional liq-31 uid electrolyte by the alkaline anion exchange membrane.⁴⁻⁶ Some 32 long standing limitations such as electrolyte leakage and high purity 33 fuels with low CO₂ concentrations were overcome by the usage of a 34 solid state electrolyte. The development of alkaline anion exchange 35 membrane fuel cells (AAEMFCs) is further motivated by the intrinsic 36 advantages over their acidic analog proton exchange membrane fuel 37 cells (PEMFCs). The merits of an AAEMFC as shown in Figure 1 38 include the following: (i) The electrode kinetics of the cathodic re-39 duction reaction is more facile in a high pH environment; (ii) Many 40 non-noble-metal materials that are unstable in the PEMFC acidic en-41 vironment can be used as electrode components; (iii) Hydroxide anion 42 and electroosmotically driven water molecules generally migrate from 43 the cathode to the anode, suppressing the crossover of anodic fuels 44 in the opposite direction; (iv) Even with the exposure to air or in 45 the case of direct methanol fuel cells where CO₂ is inevitably pro-46 duced, the metal carbonate/bicarbonate formation and precipitation 47 problems no longer exist since anion exchange membranes are free 48 of metal ions.⁷ Although for the current AAEMFC technology there 49 still remain a number of major issues such as the low conductivity of 50 the membranes⁶ and unsatisfactory performance of membrane elec-51 trode assemblies,^{8,9} the successful application can be foreseen with 52 scientific and engineering improvement and continuous industrial and 53 policy support. 54

Among many factors controlling the AAEMFCs' performance, 55 electrocatalysis plays a central role in electrochemical reactions. There 56 are two distinct electrochemical processes for the reactants at the two 57 electrodes (i.e. electrooxidation on the anode and electroreduction on 58 the cathode). The oxygen reduction reaction (ORR) is notorious for 59 suffering from sluggish kinetics¹⁰⁻¹² that may be affected by elec-60 trolyte pH,¹³ the nature of the counter cation of the hydroxides,¹⁴ 61 temperature,¹⁵ etc. From Figure 2 the reaction scheme of the ORR 62 in alkaline media is similar to that in the acidic environment. In-63

*Electrochemical Society Active Member. ^zE-mail: <u>qghe@zju.edu.cn</u> stead of H₂O₂ and H₂O formation when protons are abundant, the ORR in alkaline media generates peroxide anion in the series path-65 way and hydroxide anion as the final product. However, the ORR 66 is generally more facile in alkaline media for both thermodynamic 67 and kinetic reasons.^{12,16–18} It has been commonly concluded that the 68 rate-controlling-step is the first electron transfer to the adsorbed O2.ad 69 (inner sphere reaction) or formation of the superoxide radical anion 70 $O_2^{\bullet-}$ (outer sphere reaction) during ORR in both acidic and alka-71 line media,^{12,19-22} although there is a controversial viewpoint that 72 dissociative chemisorption of molecular O₂ on the electrode surface







Figure 2. Reaction pathways for ORR in acidic and alkaline media (redrawn from Ref. 371).

determines the ORR rate according to Yeager.^{23–25} Figure 3a shows 74 the first electron transfer reactions and overall reduction reactions of 75 oxygen molecules in acidic and alkaline media. For the reaction 1a 76 77 (& 1b), it typically happens on some specific electrode surface on 78 which an exothermic process of O₂ adsorption is involved. For those electrode materials without strongly chemisorbed O₂ such as ideal 79 graphite, the reaction 1a' (& 1b') accompanied with an outer sphere 80 electron transfer process is dominant. Because there is no proton (or 81 hydroxide ion) involved, both reaction 1a (& 1b) and reaction 1a' (& 82 1b') are pH independent. However, the overpotential of the ORR is 83 actually correlated with the difference of equilibrium potential be-84 tween the first electron transfer reaction and the overall reaction (see 85 Figure 3a). Because protons (or hydroxide ions) are involved in both 86 the 2e⁻ transfer reaction (2a & 2b, or 2a' & 2b') and the 4e⁻ transfer 87 reaction (3a & 3b, or 3a' & 3b'), the overpotential of ORR is still pH 88 dependent considering the overall process. To clearly show the influ-89 ence of pH on the facility of the ORR, Blizanac et al.¹⁸ contributed 90 detailed theoretical calculations and constructed a modified form of 91 the Pourbaix diagram (Figure 3b) with the overpotential of the ORR 92 instead of the equilibrium potential as the y axis. 93

From Figure 3b, some very important information can be obtained. 94 (i) Without strong adsorption of O_2 on the electrode (see line 3), the 95 overpotential values to form H_2O_2 and HO_2^- are much less than those 96 to form H₂O (\sim 40% less at pH = 1 and \sim 70% less at pH = 13). That 97 means it is always more energetically favorable to go through the per-98 oxide intermediate species during ORR. In other words, a $2e^{-} + 2e^{-}$ 99 serial four-electron pathway is preferred on those electrodes without 100 specific adsorption ability for O_2 (outer sphere reaction). However, in 101 the case of line 3' with an inner sphere reaction, a cross-section can 102 be noticed at $\sim pH = 12$ for line 3' and line 2. This indicates that 103 a direct 4-electron transfer pathway can be realized on some specific 104 electrodes (e.g. Pt) but only in alkaline media. (ii) For simplicity, 105 considering the reaction 1 (line 3) only as the initial step of ORR 106 (instead of both line 3 and line 3'), the minimum overpotential to form 107 H₂O designated by the difference between line 3 and line 1 decreases 108 significantly from pH = 1 (\sim 1.5 V) to pH = 13(\sim 0.8 V). When the 109 incomplete reduction reaction to form H₂O₂ is considered, the min-110

imum overpotential between line 3 and line 2 is only \sim 0.3 V at pH 111 = 13. The dramatic decrease of the intrinsic overpotential of ORR 112 that is evaluated by the above difference of standard potential from 113 a low pH to a high pH environment was presumed as the primary 114 thermodynamic reason for a feasible ORR process on a large number 115 of electrode materials.^{18,26} Nevertheless, in fact, a smaller overpo-116 tential does not necessarily indicate "surface-independency" of the 117 rate-determining step of ORR in alkaline media. 118

This question was better explained by Nagappan et al.¹² with con-119 sideration of the double layer structure and outer-sphere electron trans-120 fer mechanisms (see Figure 3c). In the schematic illustration of the 121 double-layer structure during ORR in alkaline media (Figure 3c), Na-122 gappan et al. show a "universal" scenario with both chemisorbed O2 123 at the inner Helmholtz plane (IHP) and water solvated O₂ packed at 124 the outer Helmholtz plane (OHP). The inset (a) in Figure 3c depicts a 125 common inner-sphere electron transfer mechanism applicable for both 126 acidic and alkaline media. More interestingly, the inset (b) shows an 127 outer-sphere reaction that is unique to alkaline media. The uniqueness 128 is actually coming from the interaction between the H atom in OH_{ads} 129 and the O atom in the solvent water molecule via an H bond. Such "H 130 bond" interaction appears less likely in acidic media because the elec-131 trode will be mainly covered with anions (e.g. ClO_4^{-} , SO_4^{2-}) from 132 the supporting electrolyte. Though much lower than the chemisorp-133 tion energy associated with O_{2ads} , the hydrogen bond energies (<35 134 $kJ mol^{-1}$) are just enough to overcome the minimum overpotential be-135 tween line 3 and line 2 in high pH environment as shown in Figure 3b. 136 As a direct consequence, an outer-sphere electron transfer to form 137 the superoxide species can be promoted in alkaline media regardless 138 of the underlying electrode surface. As an important conclusion, the 139 promotion by the interaction between the $O_2 \cdot (H_2O)_n$ cluster and the 140 surface hydroxyl species was assigned as the fundamental reason for 141 the so-called "nonspecificity" of the rate-determining step of the ORR 142 in alkaline media, which creates the possibility to use a broad range 143 of conducting materials as ORR electrodes. 144

However, the above conclusion was built on some presumptions, 145 that for example the first reaction step involving the redox couple of 146 $O_{2,ad}/O_{2,ad}^{-}$ is a surface-independent outer-sphere electron transfer 147 process.²⁷ Under real conditions in which more complex multistep and 148 multielectron processes and different types of adsorbed intermediates 149 and surface modified electrodes are considered, a better understanding 150 of the generally more facile ORR in alkaline media has to be made 151 from the point of view of kinetics. It is only reasonable to compare 152 the kinetics of the ORR at extreme pH conditions (traversing from 0 153 to 14) on the same electrode surface because many factors (Eq. 1^{18}) 154 such as the order of activity of active sites and coverage of spectator 155 species vary with different electrodes. 156

$$i = nFkc_{O_2}(1 - y\Theta_{ad})^x \exp\left(\frac{-\beta FE}{RT}\right) \exp\left(\frac{-\gamma r\Theta_{ad}}{RT}\right)$$
[1]

First of all, for the benchmark catalyst material of Pt for ORR, the 157 kinetics is even inhibited to some extent in alkaline media.^{11,28,29} From 158 the work pioneered by Conway³⁰ and others, the surface of a polycrys-159 talline Pt electrode is covered by oxide species with an onset potential 160 of ca. 0.75 V (vs. RHE), either due to water activation in acid or OH⁻ 161 anion adsorption in alkaline media. However, as long as the strong Pt-162 O₂ interaction is not fully blocked typically below 1.15 V (vs. RHE),³¹ 163 the energy barrier of the first electron transfer for the redox couple of 164 $O_{2,ad}/O_{2,ad}^{-}$ can still be easily overcome due to the strong interaction 165 between Pt and molecular O₂ in both inner- and outer-sphere manners. 166 Consequently, some catalytically active sites for molecular O_2 may 167 be blocked by the overwhelming OH⁻ species in high pH environ-168 ment, and a 25 mV overpotential and nearly one order of magnitude 169 lower exchange current density were obtained when switching from a 170 0.1 M HClO₄ solution to a 0.1 M NaOH solution.¹¹ In contrast, on a 171 Ru electrode the ORR kinetics in alkaline media becomes much faster 172 than the acidic media.¹¹ The very oxophilic surface of Ru grants its 173 superior ability for water activation. As such it has been a good as-174 sistant to remove poisoning adsorbed species (e.g. CO) on adjacent 175



Figure 3. (a) The first electron transfer and overall oxygen reduction reactions in acidic and alkaline media considering two electron-transfer mechanisms of the inner-sphere reaction and the outer-sphere reaction. (b) Modified form of Pourbaix diagram. All potentials are expressed relative to the equilibrium potential for reaction $O_2 + 4H^+ + 4e^- = 2H_2O$. Line 1: pH dependence of equilibrium potential for reaction $O_2 + 4H^+ + 4e^- = 2H_2O$. Line 1: pH dependence of equilibrium potential for reaction $O_2 + 4H^+ + 4e^- = 2H_2O$ ($p_{O_2} = 1$ atm); line 2: pH dependence of equilibrium potential for reaction $O_2 + 2H^+ + 2e^- = H_2O_2$ ($log(p_{O_2} / (H_2O_2)) = 0$, $log(p_{O_2}/(HO_2^-)) = 0$); line 3: pH dependence of equilibrium potential for reaction $O_2 + e^- = O_2^-$ proceeding as a inner sphere reaction (ΔG_{ads} is adsorption free energy of $O_{2,ad}^-$; in this case, as illustration, ΔG_{ads} is ca. -30 kJ/mol). Reprinted with permission from Ref. 18 Copyright 2007 Elsevier. (c) Schematic illustration of the double-layer structure during ORR in alkaline media. Insets (a, b) illustrate the inner- and outer-sphere electron transfer processes. Reprinted with permission from Ref. 12 Copyright 2012 Hindawi Publishing Corporation. (d) ORR and H_2O_2 Reduction Reaction (HPRR) on a FeTPP/C catalyst (pyrolyzed at 800°C) in acidic and alkaline electrolytes. All measurements were performed at 900 rpm rotation rate and 20 mV/s scan rate. Reprinted with permission from Ref. 12 Copyright 2012 Hindawi Publishing Corporation.

¹⁷⁶ alloyed Pt sites during anodic electrooxidation of methanol through ¹⁷⁷ a bifunctional mechanism.³² However, the surface oxides may block ¹⁷⁸ efficient O_2 adsorption, resulting in large overpotentials.

Thanks to the nonspecificity of the underlying electrode for the 179 first electron transfer in alkaline media,¹¹ the ORR can still proceed 180 at relatively high potentials on Ru that may be covered with oxide 181 182 species already. This "nonspecificity" is originated from the interaction between the solvation shell of the $O_2 \cdot (H_2O)_n$ cluster and the 183 excessive OH⁻ species on the electrode surface through a H bond.¹¹ 184 In general, it is the easier outer-sphere electron transfer process in 185 alkaline medial that compensates the weak interaction between the 186 187 electrode and the O2 molecules. This compensation effect also works

on the non-noble-metal electrodes such as pyrolyzed metal macrocy-188 cle compounds and recently reported N or S doped two dimensional 189 carbon materials.^{33–35} For instance, a 200 mV positive shift of the half 190 wave potential for ORR has been seen on Fe or Co based metal-N 191 composite electrodes when they are transferred from acidic to alka-192 line media.^{36,37} The above mentioned "nonspecificity" and promotion 193 of outer-sphere electron transfer are certainly beneficial for ORR to 194 "occur" in alkaline media. However, on the other hand, it may be 195 considered as a disadvantage for "complete" oxygen reduction since 196 peroxide species are the main products of the outer-sphere reaction 197 mechanisms, given the fact that the 2-electron + 2-electron series 198 pathway is more likely according to direct evidence from rotating 199

ring disk electrode (RRDE) studies.^{11,38,39} As such, a more important 200 reason for the faster kinetics in alkaline media is the better stabiliza-201 tion of the peroxide intermediate and faster following reduction. It 202 has been known that the predominant ORR intermediate species stay 203 as the HO_2^- anion at pH>12,⁴⁰ which is different from the neutral 204 molecule of H_2O_2 at pH<12. Under the real fuel cell operating con-205 ditions where the potential on the cathode is typically much higher 206 than the potential of zero charge (pzc) value, the positive charge on 207 the electrode may provide an electrostatic attraction force toward the 208 negatively charged HO₂⁻ and the possibility of further reduction to 209 OH⁻ on the catalytically active sites. From Figure 3d, it can be seen 210 that a more positive onset potential and higher current density for the 211 hydrogen peroxide reduction reaction were obtained on a FeTPP/C 212 catalyst in 0.1 M NaOH than that in 0.1 M HClO₄, indicating that 213 peroxide reduction is more kinetically favored in alkaline media. In 214 summary, from the point of view of kinetics, the fundamental rea-215 son for more facile ORR in alkaline media than acidic media is the 216 stabilization effect of the peroxide intermediate of HO₂⁻ due to its 217 negative charge as opposed to the neutrality of H₂O₂ in the case of 218 acid solutions. 219

The thermodynamic and kinetic facility of the ORR stemming 220 from the electrode surface independency of the first electron transfer 221 and the stabilization effect on the peroxide intermediate in alkaline 222 media, has opened the gate for usage of a large variety of electrodes 223 224 including non-noble metal materials. On the other hand, the general 'nonspecificity" of the ORR in alkaline media does not mean that any 225 conductive material can be employed as a cathode electrocatalyst in 226 AAEMFCs. Some prerequisites and common requirements (adsorp-227 tion of O₂, metals that have multiple valence states, easy desorption 228 of products and electronic conductivity, etc.) have to be met to exhibit 229 230 good enough catalytic activity for the ORR. One aim of this review is to decipher the intrinsic properties of different types of catalysts 231 including modified Pt group metals, non-Pt-group metals (alloys), 232 non-noble-metal oxides with or without being imbedded in macro-233 cycles, and nanocarbon materials, etc. that have appeared during the 234 235 past three years.

236 This review may serve as the basis for designing the next generation of novel electrocatalysts with benefits gained from new materials 237 for further improvement of the ORR kinetics. Aside from the fun-238 damental standpoint, technologically speaking, the cornerstone and 239 success of any newly developed catalyst for replacement of the state-240 of-the-art Pt/C is to pass the critical judgement with employment in 241 a real alkaline fuel cell, in which the thickness of the electrode, volu-242 metric current density, durability, gas diffusion, membrane-electrode 243 interface, water management and so many other factors may play roles 244 individually or in combination. As such, the second aim of this review 245 to summarize the recent progress in terms of the practical applications 246 of replacement candidates for Pt/C and point out the deficiencies and 247 urgent needs of electrocatalysis research for acceleration of AAEM-248 FCs technologies. 249

Fundamental Contributions from Recent Innovations of Material Development

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Modification of traditional Pt based electrocatalysts.— Until now 252 Pt/C is still most commonly used and referenced for evaluation of 253 novel materials for ORR, indicating its unassailable role as the main-254 stay of electrocatalysts in AFCs. The somewhat inhibited catalytic 255 activity due to strong adsorption of abundant OH- species in alkaline 256 media and the aspect of small molecule alcohol tolerance during ORR 257 maintain it as an interesting topic for modifications on Pt based elec-258 trodes by alloying, changing its structure on the nanoscale, etc. Indeed, 259 in acidic media, it has been a routine strategy to improve the catalytic 260 activity of Pt for ORR by increasing the Pt d-band vacancies,⁴¹ the sac-261 rificial effect,⁴² modification of the nanostructure^{43–45} and other factors 262 via alloying with 3d transition metals (e.g. Fe, Co, Ni). However, the 263 number of reports about alloyed Pt electrocatalysts for ORR in alka-264 line media is much less, partially because these 3-d transition metals 265 usually remain as oxide or hydroxide forms with low conductivity



Figure 4. Synthesis and proposed general structure of platinous backbonepolymerized complexes-magnetite hybrid nanostructure (PtBPC–MHN) and platinum–magnetite hybrid nanostructure (Pt–MHN). Reprinted with permission from Ref. 56 Copyright 2013 Royal Society of Chemistry.

and stability at pH = 14.⁴⁶ Therefore, the pertinent work was more fo-267 cused on alloving Pt with other noble metals. Nanoporous PtPd alloys 268 with various ratios of Pt were fabricated using a "one-step" method 269 by dealloying PtPdAl precursors.⁴⁷ The superior activity of the PtPd 270 alloyed catalyst was ascribed to both shrinking of the Pt lattice and 271 stronger binding energies for OOH (beneficial for the first electron 272 transfer) but lower adsorption of OH (less blockage and inhibition 273 by oxide species) on PtPd alloys.^{48,49} Alloying Pt with In, Au, Ru 274 and Ag, and ORR testing were also demonstrated with a combination 275 of good activity and other gains such as tolerance for CO and alco-276 hols and long term stability. 50-54 Actually bimetallic Pt-3d transition 277 metal catalysts do not disappear from the scene completely, providing the possibility of fabrication of unique structures.^{55–57} For example, 279 as shown in Figure 4. Fe₃O₄ nanoparticles with epitaxial growth of 280 Pt show improved specific activity for ORR due to electron transfer 281 between the Fe₃O₄ core and the Pt shell, in which the underlying 282 Fe₃O₄ was fully protected from corrosion by the unique core-shell 283 structure.⁵⁶ Apart from the above-mentioned electronic effect, the 284 ORR kinetics on Pt can be improved by changing the crystal structure 285 in the microscopic range. Devivaraprasad et al.⁵⁸ correlated ORR ac-286 tivity with the crystal structure of Pt nanoparticles, and established the 287 order of Pt-tetrahedral ({111}-facet dominant) > Pt-polycrystalline \approx Pt-cubic({100}-facet dominant) > Pt-cuboctahedral ({100}-facet 289 dominant), which agrees with the single crystal studies in 0.1M KOH 290 or NaOH with the order of $\{111\} > \{110\} > \{100\}^{28,59}$ In contrast, 291 changing the morphology macroscopically only showed a marginal 292 effect on improvement of ORR activity of Pt.^{60,61} Neither does the 293 replacement of the porous carbon support (e.g. Vulcan Carbon) with 294 graphene^{51,60} or carbon xerogels⁶² exhibit noticeable kinetics benefits 295 since the nanoparticle dispersion and strong metal-support interaction 296 are well established on regular porous carbon, except that the stability 297 of the catalysts can be significantly improved by depositing Pt on some 298 new types of supports such as ITO,⁶³ carbides^{64,65} and nitrides.^{66,67} It 299 is worthwhile to mention a big advantage of the modification of Pt 300 with the above methodologies to reduce the sensitivity to the crossover 301 of anode fuels.^{51,52,68} Besides the studies focused on materials, new 302 inputs about the fundamental mechanisms of ORR in alkaline media 303 are highlighted and summarized in Table I. Although a progressive 304 understanding of ORR mechanisms on Pt-based electrocatalysts was 305 put forward, some important aspects are still puzzling and additional 306 investigation is needed from the following perspectives: 1 The in-307 teractional effects of blockage of active sites for O₂ adsorption and 308 the facilitating of electron transfer due to OH adsorption; (2) details of the effect of ion adsorption on ORR kinetics; (3) details of the

Material	Study tool/method	Main scope	New inputs for mechanisms of ORR	Ref
Pt/C	RRDE, Electrogenerated chemiluminescence	The influence of KOH concentration, oxygen partial pressure and temperature	 Solubility, diffusion coefficient, and limiting current all drop as the concentration of KOH increases. The averaged electron transfer number change from 3.81 (in 0.5M KOH) to 1.87 (in 8M KOH), indicating more HO₂⁻ formation. ORR intermediate species (HO₂⁻) can be detected by a fluorescent probe. "Salting-effect" makes O₂ pressure influence become weak in high concentration KOH. Temperature shows dual effects by mediating strong OH adsorption and decreasing O₂ solubility. 	383
Pt/C	RDE, SEM	The effect of temperature (over 100 °C) and pressure on ORR kinetics	 The transfer coefficient (α) of O₂ is constant in the Langmuir region (large current density), but is temperature dependent in the Temkin region (low current density). Diffusion coefficient (D₀) of O₂ is independent on pressure. Connection between O₂ concentration (C₀*) and pressure and temperature was established. ECSA of the Pt electrode increases largely at high temperatures. 	384
PtCu/C	RRDE	The effect of OH _{ads} coverage on Pt based electrodes	 The rate determine step of ORR is the same at extreme pH conditions. Basic kinetics current of ORR is inversely proportional to OH_{ads} coverage. Lower rate of increase of OH_{ads} coverage can be achieved on PtCu than Pt. At certain high potential (ca. 0.83 < E < 0.90 V), a universal rate of dθ/dE was found on any Pt based catalysts. 	385
Polycrystalline Pt nanoparticles	RRDE, TEM	The effect of the shape of Pt nanoparticles	 The order of ORR activity is Pt-TD > Pt-PC ≈ Pt-NC > Pt-CO (TD: tetrahedral, PC: polycrystalline, NC: cubic; CO: cuboctahedral). The order of peroxide formation is Pt-CO > Pt-PC > Pt-TD > Pt-NC. 	58
Pt single crystals	Hanging meniscus rotating disk electrode	The effect of surface structure of Pt single crystals on ORR kinetics	 Pt(111) is the most active surface for ORR in alkaline media. Introduction of step density (defects) on single crystal's (except (100)) surface diminish the ORR activity due to large OH adsorption energy on steps. OH adsorption strength depends on the surface structure of Pt instead of pH. Lower activity for ORR on Pt(100) is due to stronger OH adsorption 	59

The effect of

anion-exchange cationic

functionalities on Pt

activity for ORR

Table I. Recent discoveries about fundamental mechanisms of ORR on Pt based electrocatalysts in alkaline media

ORR pathway, intermediates, and mechanisms in highly concentrated
basic solutions (close to the real conditions of AAEMFCs cathode);
(4) reasons for the very slow kinetics of oxygen reduction.

Cyclic and

hydrodynamic

RDE-LSV

Polycrystalline Pt

Non-Pt noble metal electrocatalysts .-- Pd and Ag based 314 electrocatalysts.- The high cost and scarcity of Pt have always been 315 the major impediments for commercialization of fuel cells. Fortu-316 nately the more facile ORR process creates the possibility of replacing 317 Pt with less expensive and more abundant "noble-metals". Pd or Ag 318 based catalyst materials indeed have exhibited very promising ORR 319 performance comparable to that of Pt/C.⁶⁹⁻⁷¹ Among the major ef-320 forts for further improvement of ORR kinetics on Pd or Ag based 321 322 electrocatalysts, some progress has been realized in recent years. One

general and reasonable strategy is to make and disperse nanoparticles on functionalized carbon support for increasing the surface area of metal particles and accelerating electron transfer and other processes. Given enough consideration on the shape and size effects,^{72–79} Jeon et al.^{80,81} deposited Pd and Ag nanoparticles on linker grafted graphene support and achieved remarkable electrocatalytic activity. Figures 5a and 5b show the unique role of the linkers to facilitate intermolecular charge-transfer and dispersion and stability of metal nanoparticles.

The surface sites covered by OH also participate in

• Inhibition of ORR specific activity follows the order:

< KOH-BTMA < KOH-BAABCO < KOH-BMI.

blank KOH < KOH-KCl < KOH-TMA <KOH-BOTMHA

electron transfer.

In addition to sphere-shaped nanoparticles, some recent advances on preparing metallic Pd and Ag nanocrystals with special shapes and excellent ORR activity can be found. Various shaped Pd and Ag nanoparticles such as Pd nanocubes,⁸² Pd cubes and octahedra,⁸³ hollow Pd nanoshells,⁷⁵ Pd icosahedra,⁸⁴ Ag nanodecahedra

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Figure 5. Schematic diagram of synthesis of linkages Grafted Graphene supported palladium (a) (Reprinted with permission from Ref. 80 Copyright 2015 Elsevier.), and silver (b) nanoparticles Reprinted with permission from Ref. 81 Copyright 2015 The Electrochemical Society.

and nanocubes,⁷⁷ Ag nanoclusters,⁸⁵ worm like and angular Ag 336 nanoparticles,⁷⁶ all seem to be able to catalyze ORR in rather facile 337 ways, and further exploration is needed for better understanding of 338 the shape effects. Besides, it is a little counterintuitive to develop no-339 ble metal oxides as ORR electrocatalysts since they were expected 340 to block effective O₂ adsorption as in the case of PtO_x. Surprisingly, 341 PdO/C synthesized by heat treatment of Pd/C in air at 250°C showed 342 almost identical catalytic activity to that of Pd/C, and a PdO/C-4h 343 sample synthesized by the reaction of PdCl₂ with a Mn₃O₄/C sub-344 strate showed superior activity and kinetics as compared to Pd/C.86 345 Higher specific activity but a smaller number of electrons transferred 346 were also found on Ag particles with oxide surfaces.⁷⁶ Although the 347 ORR mechanism of outer-sphere electron transfer and more efficient 348 interaction between O2.ads and extra OH- species at the double layer 349 interface is still a hypothesis, it can be certainly inferred that ORR 350 351 processes are different on the above materials and highlight it as a very interesting topic for further investigation. 352

Similar to the surface modification of Pt by alloying with other metals, a number of novel Pd and Ag based alloy electrocatalysts including core-shell structured materials have been tested for ORR in alkaline media and reported in recent years. Some typical examples that can be used as references for further alloyed catalyst development 357 are listed in Table II. Generally, some more inert elements for ORR 358 such as Au have been added to improve the stability of the catalysts 359 as it functionalizes in acidic media.⁸⁷ It can be noticed that the choice 360 of alloying elements have been broadened very much because 3d 361 transition metals (e.g. Cu, Fe, Ni, Co) can be widely employed and 362 even enhanced stability of the catalysts can be obtained.^{88,89} Since 363 high temperature heat treatment is not always necessary for synthesis 364 of the above alloy catalysts, the enhanced activity may be attributed to 365 stronger synergistic and better ensemble or miscibility effects with Pd 366 or Ag although no detailed studies on this hypothesis are available yet. 367

Different from forming alloys or core-shell structures with other metals, some metal oxides were also added into Pd or Ag based catalysts and helped to improve the overall ORR performance. Slanac et al.⁹⁰ synthesized Ag-MnO_x/C composites with a new electroless co-deposition method. From the STEM imaging and EDS elemental mapping in Figure 6i Ag nanoparticles are interconnected with MnO_x nanodomains, providing a ligand effect and an ensemble effect on ORR activity of the composite catalyst approaching that of Pt in Figure 6ii. From others' reports, Pd or Ag-MnO_x/CoO_x composites were prepared using a solvothermal method,⁹¹ immersion-calcination 371

Table II. Novel Pd and Ag based alloy electrocatalysts for ORR in alkaline media.

Catalyst	Preparation method	Kinetics parameter	Highlights	Ref.
with Au Au ₁₀ Pd ₄₀ Co ₅₀ / C-core-shell, Au ₁₀ Pd ₄₀ Co ₅₀ / C-intermetallic	For the core-shell structure, Co/C was formed by reduction of CoCl ₂ , which is followed by coating of Au and Pd.	Mass activity at 0.9 V, Intermetallic: 0.13 (A/mg), Core-shell: 0.09 vs. Pt _{3.5nm} /C: 0.14	 Structurally ordered Au₁₀Pd₄₀Co₅₀ catalysts that exhibit comparable activity to conventional platinum catalysts Core-shell structure changed to intermetallic ordered structure with high temperature treatment Au atoms help to significantly improve the stability of the catalysts 	386
Pd–Au nanochain networks / reduced graphene oxide (rGO)	The core-shell catalyst subjects a structure change to intermetallic with heat treatment. Wet-chemical co-reduction method with the assistance of caffeine	Mass activity at −0.1V (vs. Ag/AgCl), ~ 14 mA/mg	• Better electrochemical performance than commercial Pd-black and Pd–C toward ORR	387

Table II.	(Continued)
Table II.	(Commuca.)

Catalyst	Preparation method	Kinetics parameter	Highlights	Ref.
AuPd Nanochain/carbon black	Two-step galvanic replace-ment reaction	Half wave potential $(E_{1/2})$ (vs. SCE), Au _{0.8} Pd _{0.2} NN _S /C: -0.097 V Pt/C: 0.02 V	• ORR activity of Au _{0.8} Pd _{0.2} NN ₅ /C surpasses Pt/C	388
Au@Pd core–shell nanothorns	Wet-chemical sequential reduction method with the assistance of L-ascorbic acid	Mass activity at 0.9 V, \sim 16 mA/mg	 Higher ORR activity and stability than both of commercial Pd black and Pt black Thorn like morphology and synergistic effects between the Au core and the Pd shell 	389
Au@Ag electrodes	Under potential deposition (UPD) of Pb on Au followed by surface replacement of Ag	Kinetics current, half an order of magnitude improvement vs. Ag	• Surface oxygen affinity of Ag is improved by electronic interaction with Au sublayer	390
With Cu PdCu/rGO	Homogeneous hydrothermal reduction	Mass activity at -0.26 V (vs. SCE), 38.4 mA/mg	• Improved electrocatalytic performance and high methanol-tolerance ability	391
PdCu/graphene	"Dispersing-mixing vaporizing solvent" method	Mass activity at -0.25 V (vs. SCE), G-Cu ₃ Pd: 45.4 mA/mg _{NCPs}	 G-Cu₃Pd NCPs exhibit the highest electrocatalytic activity compared with other G-Cu_xPd_y The durability of G-Cu₃Pd NCPs is superior to commercial Pt/C catalysts 	88
Ag/octopus-tentacle-like Cu nanowire	Epitaxial growth of Ag nanocrystals on Cu nanowire	-	• Efficient approach for synthesizing metal heterostructures with large lattice misfit (>5%)	89
With Fe FeCo@Fe@Pd	Microwave-induced top-down nanostructuring and decoration	Exchange current density (j _o) = $1.26^* \ 10^{-2} \ \text{mA cm}^{-2}$)	• High tolerance to methanol	392, 393
FeAgPc/C	Pyrolysis of iron(II) and silver(II) phthalocyanines (MPc)	$E_{1/2} = 0.931 V$	• Effective interaction between Fe and Ag and unique nanostructure were formed during heat treatment	394
With Ni Palladium-nickel (PdNi) hollow nanoparticles	Galvanic replacement method	Mass activity at -0.1 V (vs. Ag/AgCl), 588.97 mA/g _(Pd)	• Superior ORR performance was achieved as compared to commercial Pt/C or Pd/C	375
With Co AgCo/Ti	Electrodeposition of Co particles on the dendrite-Ag/Ti electrode and further modified by	\bigcirc	 ORR activity: PANI-Ag_xCo_y/Ti > Ag_xCo_y/Ti > PANI-Ag/Ti > Ag/Ti Methanol or ethanol tolerant 	101
AgCo	Polyani-line (PANI) Incipient-wetness followed by rapid heating reduction	Specific Activity at 0.85 V, $\sim 1.5 \text{ mA}/\text{cm}^2$ (Ag)	• Subsurface Co-ligand effects as the primary source of enhanced activity	395
With Sn Ag4Sn/C	A solution phase reduction method	Mass activity at 0.75 V, 15.68 mA /mg, Specific activity at 0.75 V, 1.05 mA /cm ² $_{(geo)}$	• High methanol tolerance and good long-term stability	396
With Mo AgMo hybrid	A hydrothermal method	Mass Activity at -0.1 V (vs. Hg/HgO), AgMo-22: 0.67 mA /mg	• Better stability than Pt/C	397
AgPd alloys with different ratios	Wet-chemical co-reduction	Mass activity at -0.05 V (vs. NHE), Ag ₉ Pd: 3778 mA/mg _(Pd) , Ag ₄ Pd: 3518, Ag ₂ Pd: 2057, AgPd ₂ : 2011, Pd: 799	• The activity of more active Pd was enhanced by less active Ag by tuning the heteroatomic interactions	398
Pd ₂ NiAg	Solid-liquid phase chemicalroute	$\begin{split} E_{1/2} &= -0.131 \text{ V} \text{ (vs.} \\ \text{Ag/AgCl)} \end{split}$	 Increased availability of surface Ni sites and the features of twinned structural defects Improved catalytic activity 	399
Comparison study MPd ₃ (M = Fe, Cu, Ag, Au, Cr, Mo, W) nanocrystals/graphene	Electrostatic assembly and hydrogen reduction	-	• G-FePd ₃ NCPs exhibit the highest catalytic activity	400

*ORR kinetics parameters were obtained at room T, 1 atmosphere. Potentials were referred to the reversible hydrogen electrode (RHE) unless they are addressed otherwise.



Figure 6. (i) STEM imaging and EDS elemental mapping of 20% Ag - 35% MnO_x on Vulcan carbon XC72 (VC) The (A) bright field image shows darker regions (silver) surrounded by lighter regions (MnOx and carbon). In (B) STEM-EDS mapping shows that the darker regions from the bright field images correspond to silver (green) nanoparticles, whereas the regions between the Ag are covered with MnOx (red). Carbon mapping is not shown here as the signal would show up everywhere due to both Ag and MnOx being supported on carbon. (Reprinted with permission from Ref. 90) Copyright 2012 American Chemical Society. (ii) RDE polarization curves (cathodic scans) for plain VC, VC loaded with MnO_x, and AgMnO_x with respect to commercial standards of Pt/VC and Pd/VC. Reprinted with permission from Ref. 90 Copyright 2012 American Chemical Society.

method,⁹² a carbon reduction-calcination method,⁹³ or a
hydrothermal-wet reduction method,⁹⁴ from which promising ORR
performance was achieved individually probably due to the presence
of a metal-oxides interface.⁹⁰

From the aforementioned reports on Pd and Ag based catalysts, 382 commercial porous carbon black supported Pt, Pd and Ag were typi-383 cally employed for comparison and evaluation of ORR performance 384 of various types of catalyst materials. However, it has been known that 385 the carbon black support may interfere with the ORR by promoting 386 the 2e⁻ outer-sphere electron transfer and incomplete reduction of 387 O2. Moreover, carbon may suffer from being used as nanoparticles 388 due to severe corrosion and oxidation under the real fuel cell oper-389 ating conditions, resulting in general degradation of the performance 390 of supported catalysts. Many research groups endeavored to disperse 391 Pd and Ag particles on other support materials to improve the long 392 term stability. For instance, Lu et al.95 developed a new class of Pd 393 tetrahedron-tungsten oxide nanosheet hybrids with an organopalla-394 dium complex precursor and in situ-synthesized W₁₈O₄₉ nanosheets. 395 396 From Figure 7, the binding energy of Pd 3d and the binding energy of W 4f for Pd/W₁₈O₄₉ move in opposite directions. This indicates 397

that partial electrons may transfer from Pd to W due to the strong in-398 teraction. A Similar phenomenon was found on a CuFe/C bimetallic 399 catalyst with soft X-ray absorption measurement.⁹⁶ The lowering of 400 electron density on Pd may significantly help to enhance the dissocia-401 tive adsorption of O₂ and the following 4-electron reduction.^{95,97–99} 402 In addition to the Pd-WO_x hybrids with both enhanced activity and 403 stability, some robust metals like Ti (or TiO_x)^{100,101} and Ni foam,¹⁰² 404 some 2-dimental carbon materials like carbon nanotubes (CNT)^{103,104} and graphene,¹⁰⁵⁻¹⁰⁷ and other carbon supports like B doped C,¹⁰⁸ car-406 bon nitride,¹⁰⁹ carbon nanofibers¹¹⁰ were also used to support Pd or 407 Ag nanoparicles and nanoalloys. 408

Other non-Pt noble metal electrocatalysts.—Other than Pd and Ag, 409 the number of reports of other non-Pt noble metal electrocatalysts is 410 rather limited. Among the research efforts on Au, 111-113 Ru, 114,115 Ir¹¹⁶ 411 and other precious metal catalysts for ORR in alkaline media, the main 412 motivations seem to be devoted to the understanding of ORR mecha-413 nisms on a broad scope or assist in the study of other materials such as 414 supports and mediators, rather than using them as replacement for Pt 415 based electrocatalysts. Rodriguez and Koper¹¹⁷ have made a thorough 416 review on electrocatalysis of gold, in which some basic conclusions 417 were drawn regarding topics such as the pH and crystallographic ori-418 entation effects on the kinetics of ORR, the distinct roles of the d 419 band of metal electrodes in extreme pH conditions, the shape sensi-420 tivity of Au nanoparticles for ORR, and the influence of the support 421 and the particle size on kinetic currents. Given the fact that the non-422 Pt precious metals except Pd and Ag can usually catalyze ORR in 423 a 2e⁻ pathway by themselves, it is a little surprising to see that a 424 AuCu₃ alloy catalyst can show 1.5 times mass current density of com-425 mercial Pt/C for the ORR in 0.1M KOH.¹¹⁸ It has been known that 426 neither Au nor Cu is suitable for catalysis of ORR due to the weak 427 affinity between Au and O2 or OH-118-120 and a too-strong binding 428 energy between Cu and oxygen.^{118,119,121} Figure 8a shows that Cu/C 429 and Au/C have very poor ORR kinetics. However, based on the DFT 430 calculation model in Figure 8b, the adsorption energy of the AuCu₃ alloy with oxygen (-1.04 eV) is very close to that of Pt (-1.06 eV). 432 In other words, the balance of oxygen adsorption and intermediate 433 desorption was perfectly reached by changing the atomic ratio of Au 434 and Cu, which opens a new gate for design of novel catalyst materi-435 als using a combination having elements of weak and strong oxygen 436 affinities. 437

Non-noble-metal electrocatalysts.—Carbon supported M- N_x matrix (M = 3d transition metals).—Fundamental overview.— Different from the noble metal electrocatlalysts discussed in the above sections, some earth-abundant 3d transition metals(e.g. Fe, Co, Ni) usually do not exhibit catalytic activity for ORR in their metallic forms such as metal crystals or nanoparticles simply due to their strong reactivity or affinities with oxygen.¹²² Instead, they are typically used to



Figure 7. (A) XPS patterns of Pd 3d in Pd/W₁₈O₄₉, Pd NPs, and commercial Pd/C. (B) XPS pattern of W 4f in Pd/W₁₈O₄₉ and W₁₈O₄₉. Reprinted with permission from Ref. 95 Copyright 2014 American Chemical Society.



Figure 8. (a) LSV curves (background corrected and IR-compensated) of a series of catalysts: carbon, Cu/C, Au/C, Pt/C, intermetallic AuCu/C and intermetallic AuCu₃/C, normalised by the geometric area of the working electrodes. RDE measurements were tested in O₂–saturated 0.1 M KOH, scan rate: 10 mV/s, RDE rotation rate: 1600 rpm. Reprinted with permission from Ref. 118 Copyright 2014 Wiley-VCH. (b) The most probable adsorption mode of oxygen on AuCu (111) (rotated bridge mode); Cu (blue), Au (yellow) and O (red). Reprinted with permission from Ref. 118 Copyright 2014 Wiley-VCH.

form alloys with noble metals to enhance ORR kinetics by chang-445 ing the crystal lattice structure, electron density, surface morphology, 446 ensemble effects, and synergetic effects, etc. Recently, some novel 447 carbon-supported (with or without doping elements of N, S, P and B) 448 first row transition metal and metal oxides, ^{123–126} chalcogenides, ^{127–129} 449 spinels,^{130–132} pyrochlores^{115,133,134} have been reported to show some 450 activity for ORR in alkaline media. Among them, similar and ever 451 faster ORR kinetics than Pt based electrocatalysts have been widely 452 seen on this class of materials by stabilizing the metal or metal oxides 453 with surface nitrogen (or other elements) functionalities on graphitic 454 surfaces, which are the main focus of this section due to their direct 455 applicability in AAEMFCs. 456

After the ground-breaking discovery of the metal macrocycle 457 compounds,¹³⁵ a consensus of the key role of the N-metal bond on 458 exhibiting ORR catalytic activity has generally formed.¹³⁶ It is ac-459 cepted that in the macrocycles the ORR electrocatalysis active cen-460 ter is located on the central metal ion with sufficient d-character to 461 coordinate O₂ molecules. And that is verified by the fact that the 462 ORR normally operates at the potential of reduction of the metal-463 O_2^- adduct^{137,138} and the onset potential of ORR is closely linked to 464 the redox potential of the central metal.^{137–139} However, the catalysts 465 would not be stable without the strong anchoring effect caused by the 466 large bonding energy between the central metal and the surrounding 467 N.¹⁴⁰⁻¹⁴³ More importantly, the metal-N bond serves as the bridge for 468 the π -conjugated ligands on the outer periphery to relocate its redox 469 potential by modifying the electronic structure.^{136,144} For Example, 470 cobalt porphyrins can be converted to a 4-electron transfer catalyst 471 for ORR by placing pendant electron-withdrawing groups on the pe-472 riphery of the macrocyclic ligands.¹⁴⁵ Indeed, electron-withdrawing 473 groups on the macrocycle ring may shift the energy of the d orbitals 474 away from the Fermi level, resulting in a higher ORR onset potential 475 and higher turnover numbers due to a more suitable binding energy 476 for ORR intermediates. In addition, it was found that adsorption of 477 metal porphyrins on a carbon black support can dramatically enhance 478 the ORR activity and shift the onset potential toward in the positive 479 direction.146 480

The effect of the carbon support was attributed to the strong π - π 481 interaction between the metal macrocycle ring and the carbon basal 482 plane, for which the delocalized π electrons on the metal macrocycles 483 could not exist without the metal-Nx matrix. And it was confirmed that 484 the axial coordination on the central metal ions themselves does not 485 contribute much to the strong binding.¹⁴⁶ At low pH, it is surprising 486 to see that a dramatic anodic shift for the ORR onset potential can be 487 achieved by pyrolysis of a mixture of metal macrocycles and carbon 488 black at certain high temperatures (e.g. 700–900°C) under inert Ar or N_2 atmosphere.^{33,147–149} Contrarily, the heat treatment effect on the 489 490

positive shift of the onset and half wave potentials of ORR is less 491 prominent in alkaline media than its counterpart in acidic media.^{11,12} 492 This difference has not been explained and needs due consideration 493 because an even larger positive shift of the redox potential of $Fe^{2+/3+}$ 494 was noticed in 0.1 M NaOH as compared to 0.1 M HClO₄ from a 495 square-wave voltammetry measurement.³³ Nevertheless, the stability 496 and selectivity of metal macrocycle catalysts for ORR can be largely 497 improved after pyrolysis.^{12,150–152} As a result, it is generally required 498 to conduct the step of heat treatment during synthesis of transition 499 metal macrocycle based electrocatalysts to achieve optimized ORR 500 performance, from which some alternative ways to form metal-N_x 501 composites were derived and developed (voyez-infra). Not the en-502 tire organic framework can survive after treatment under such harsh 503 conditions. However, at least partial metal- N_x moieties can remain in 504 light of recent evidence by HR-XPS.^{96,153} It is the expectation that the 505 metal-N bond still plays a key role in the catalytic properties of the 506 pyrolyzed macrocycles. However, this must not be the complete story 507 because the pristine compounds with more optimized d characters 508 should have higher activity otherwise. There have been continuous 509 efforts on the identification of the active-site structure of pyrolyzed 510 metal macrocycles (especially the ones supported on carbon). 511

Some representative theories such as van Veen et al.'s secondary structures containing $M-N_4/C$ moieties, ^{154–160} Yeager et al.'s $C-N_x$ -512 513 Me complex with reabsorption of metal species, $^{161-166}$ Wiesener's metal free C–N_x functional groups, 167,168 and Dodelet's metal ion-514 515 pyridinic nitrogen-edges of graphitic sheets,¹⁴⁹ were proposed and 516 may be true under their specific preparation conditions. This debat-517 able topic and the obscurity surrounding the nature of the active site 518 after pyrolysis of metal macrocycles have been given considerable 519 attention in recent years. Indeed some theoretical and experimental 520 works have advanced our understanding of the common nature and 521 original causes of activity of this class of electrocatalysts. Nagappan 522 et al.³³ combined electrochemical and spectroscopic studies to unravel 523 the nature of the active sites and ORR mechanisms on heat treated 524 porphyrin catalysts in both acidic and alkaline media. Although the 525 in situ XAS delta-mu ($\Delta\mu$) technique is literarily meant to remove 526 the background of the bulk electrode and obtain specific information 527 about surface adsorbates, 169-174 the nature of the sites where O₂ ad-528 sorbs can be still clarified with the assistance of theoretical simulations 529 since any adsorbates cannot stand alone with the direct effect of local 530 symmetrical and coordinating environments of the electrode surface. 531 By careful comparison of Figure 9a and Figure 9c, one may notice 532 that the active site for ORR has changed from a FeN₄C₁₂ cluster to 533 a FeN₄C_z cluster (z = 10 or 8), whereas the number z is correlated 534 to the degree of the destruction of the carbon methine bridges. The 535 simulated structures (Figures 9b and 9d) before and after pyrolysis 536



Figure 9. Active site structure identification. Experimental XANES and $\Delta\mu$ signatures of Fe–N_x/C catalyst pyrolyzed at (a) 300 and (c) 800°C. The $\Delta\mu$ signatures were obtained by subtracting the XANES signatures according to $\Delta\mu = \mu(0.90 \text{ (or) } 1.10 \text{ V}) - \mu(0.10 \text{ V})$. Experiments were conducted at Fe K-edge under in situ conditions in argon saturated 0.1 M NaOH electrolyte. Vertical dotted line indicates the pre-edge position at 7112.5 eV. Structural models shown in the insets of panels a and c were utilized for $\Delta\mu$ analysis using FEFF8 simulation. Also shown are the complete structural models of active site structures before (b) and after (d) pyrolysis at 800°C. Color codes in structural models: red, iron; blue, nitrogen; gray, carbon; white, oxygen. Reprinted with permission from Ref. 33 Copyright 2013 American Chemical Society.

are reminiscent of some crystallographic zones (e.g. divacancy) of 537 carbon supports, indicating that the Fe-N₄ active sites are covalently 538 integrated into the π -conjugated carbon basal plane. As a result, not 539 only the adsorption energy of O2 and intermediates on the catalytically 540 active sites can be modulated by the delocalized π -electron system of 541 the entire carbon basal plane, but also more efficient electron transfer 542 between the reactants (O_2 molecule) and the electrode can be realized. 543 This could be the fundamental reason for the dramatic shift of redox 544 potential of Fe^{2+}/Fe^{3+} and the corresponding onset potential of the 545 ORR 546

In spite of the fact that the desired coordination number of N sur-547 rounding the central metal ions is still unclear,^{175–177} the anchoring 548 of Metal-N_x (e.g. Fe-N₄³³ or Co-N₄¹⁷⁷ on some defects or inter-549 plane regions of the carbon support seems to be the original cause 550 of enhanced ORR activity. The active sites can be formed by other 551 methods in addition to pyrolysis of metal macrocycles. Xu et al.¹⁷⁸ 552 prepared different transition metal (Co, Fe, Cu, Mn, and Ni) incor-553 porated nitrogen-containing electrocatalysts by pyrolysis of inorganic 554 metal salts and aminopyrine (Apyr) as the nitrogen precursor. Be-555 sides the finding of significant enhancement by the pyrolysis due to 556 formation of surface carbon-bonded pyridinic-N and metal, different 557 metal elements exhibited discrepancy of ordering in terms of ORR 558 activity and selectivity. This might be attributed to a higher content 559

of sulfur in Mn- and Fe- incorporated catalysts, which is indicative of 560 the importance of the appropriate choice of metal salts for pyrolysis. 561 Asazawa et al.¹⁷⁹ synthesized Co-polypyrrole-based electrocatalysts 562 using Co(NO₃)₂ as the starting metal salt. Moreover, two kinds of ni-563 trogen structures (pyrrolic and pyridinic) were found to be coordinated 564 with Co to form active sites for ORR using Hard X-ray Photo Electron 565 Spectroscopy (HAXPES) analysis and DFT calculations. Consistent 566 with the deteriorated performance by treatment of the pristine CoP-567 PyC catalyst with sulfuric acid, Domínguez et al.¹⁸⁰ also found the 568 activity of Fe based electrocatalysts was decreased when subjected to 569 acid treatment, possibly due to removal of active sites and blockage 570 by adsorbed sulfates. 571

From Nagappan et al.'s study³³ it is the pyrolysis process that 572 integrates Fe-N4 active sites into defective pockets on the carbon sup-573 port that can be either induced by pre-pyrolysis¹⁸¹⁻¹⁸⁶ or during the 574 heat treatment by carbothermic reactions, ^{182,184} providing a large shift 575 of redox potential of the Fe^{2+}/Fe^{3+} couple and much lowered ORR 576 overpotential. Beyond that the pyrolyzing atmosphere was found to 577 be important to the catalytic activity, and the Co-based catalysts heat 578 treated in N₂ show better results than those in Ar or CO₂.¹⁸⁷ The py-579 rolysis temperature was also found to be important in maximizing the 580 ORR performance of cobalt-polypyrrole and cobalt-phthalocyanine 581 based catalysts, because metallic Co that is not ORR active may be 582



Figure 10. SEM images of the FePc/RGO (reduced graphene oxide) (A), FePc/MCV (mesoporous carbon vesicle) (B), and FePc/OMC (ordered mesoporous carbon) (C) with the mass ratio (FePc: carbon matrix) of 1:1. (D) SEM image of FePc/OMC with the mass ratio (FePc: OMC) of 3:1, inset is SEM image of FePc. Reprinted with permission from Ref. 189 Copyright 2014 Elsevier.

generated when the temperature is above a certain value.^{150,188} The 583 crucial role of pyrolysis on improvement of ORR activity of non-584 noble-metal catalysts did not seem to be debatable until a recent 585 report about the effect of carbon support with varying microporous 586 surface area on the catalytic activity of iron phthalocyanines (FePc) 587 came out. Li et al.¹⁸⁹ prepared FePc/MVC (mesoporous carbon vesi-588 cle), FePc/OMC (ordered mesoporous carbon) and FePc/rGO (re-589 duced graphene oxide) simply by mixing FePc and different carbon 590 matrixes at room temperature. The as-synthesized catalysts with the 591 SEM images shown in Figure 10, all display the 4-electron pathway 592 for ORR and FePc/OMC shows comparable catalytic activity and bet-593

ter stability than Pt/OMC. It will be very interesting to see if edge 594 plane-like defect sites on the OMC are truly the anchor zones for 595 Fe-N₄ active sites via non-covalent π - π interaction. If true, the lim-596 itation in the active site density and low effective metal loading (\leq 597 3 wt.%)^{33,190} on the current non-noble metal electrocatalysts can be 598 overcome. This can have a significant impact on the overall fuel cells' 599 performance by increasing the turnover number for the ORR while 600 keeping the thickness of the electrodes unchanged.¹⁹ 601

It has been demonstrated that the activation of solvated O₂ 602 molecules can be facilitated by OH- ions located at the electrode-603 electrolyte interface, leading to more facile ORR kinetics and 604 electrode-independent outer-sphere electron transfer.^{12,18} As the main 605 fundamental reason for a broad choice of electrode materials for ORR 606 electrocatalysts in high pH environment, however, it obviously cannot 607 explain the complete O₂ reduction results with 4-electron transfer on 608 numerous carbon supported non-noble-metal electrocatalysts.^{36,192–194} 609 In fact, as illustrated in Figure 11, the first 2-electron outer-sphere 610 transfer process has been suppressed by efficient displacement of 611 axial OH^- anions on the catalytically active site of Fe(II)-N₄ by 612 molecular O₂. This clearly indicates that the ORR has switched to 613 an inner-sphere electron transfer mechanism, in which the ferrous-614 hydroperoxyl adduct is stabilized and oxidized further to a ferric-615 hydoxyl species with the aid of a Frumkin-type double-layer effect.¹⁹⁵ 616 Consistent with this study, Robson et al.¹⁹⁶ performed ORR mecha-617 nistic research on Fe-aminoantipyrine pyrolyzed electrocatalysts. A 2 618 \times 2 pathway that mimics the direct 4-electron pathway was proposed 619 and deferred by the evidence of rapid reduction of H₂O₂ in both acidic 620 and alkaline media. 621

Novel synthesis methods for metal-Nx/C electrocatalysts.—Knowing 622 the original causes of activity, it becomes unnecessary to prepare 623 the catalysts by pyrolysis of organometallic compounds, which may 624 raise the cost significantly with expensive precursors in large scale 625 production. One feasible alternative way to prepare metal-Nx/C cat-626 alysts is to change the precursors or sources of nitrogen, metal ions 627 and carbon for ensuing high temperature pyrolysis. Recently evolved 628 heat-treatment precursors along with synthesis parameters and ORR 629 results are summarized in Table III. 630

Aside from thermal annealing, it is always more favorable to conduct the synthesis at relatively low temperatures. As shown in Figure 12, a poly(sodium-p-styrenesulfonate) modified reduced graphene oxide support (PSS-rGO) was first fabricated at 95°C with the assistance of hydrazine hydrate. Then metal 5,10,15,20-tetrakis(4hydroxyphenyl)porphyrin (M-THPP) was grown in situ on the PSSrGO hybrid using a solvothermal method at 150°C. The unique



Figure 11. Proposed ORR mechanism. Catalyst cycle showing the redox mechanism involved in ORR on pyrolyzed $Fe-N_x/C$ active sites in dilute alkaline medium. Reprinted with permission from Ref. 33 Copyright 2013 American Chemical Society.

Material	Precursors for pyrolysis	Synthesis parameters	ORR performance	Ref.
Fe-N _x /C	Prussian blue nanocubes on carbon	1 h, 3 h at the pyrolysis temperature (700°C) without gas	• 0.313 mA mg^{-1} @0.775 V (the best catalyst in Ref. 401)	401
Fe-N/C	Methylenediantipyrine mixed with $Fe(NO_3)_3 \cdot 9H_2O$	Pyrolyzed at 800, 900, 950°C with different time under N_2 , H_2	• j_d at 0.9 V: -2.15 mAcm ⁻² (the catalyst treated at 900°C in NH ₃)	374
Fe-N/C	2,2-Pyridylbenzimidazole mixed with ferrous sulfate	Pyrolysis at different temperatures in NH ₃	• E _{1/2} V (vs. SHE), HT-PBZ/Fe-700 : 0.058 V	402
Fe-N/C	11,11'-bis(dipyrido[3,2-a:2',3'-c] phenazinyl (bidppz) mixed with FeSO ₄ · 7H ₂ O	Heated to 700, 750, 800, 850 and 900°C for 1.5 h, HCl washing	 E_{1/2}, Fe-N/C-800 : 809 mV (Pt/C: 818 mV) Superior durability than Pt/C 	36
Fe-N/C	4,40,400-s-Triazine-1,3,5-triyltrip-aminobenzoic acid mixed with FeCl ₂ · 4H ₂ O and carbon black	Pyrolyzed at 800°C for 120 min at a rate of 3°C min ⁻¹ under a nitrogen atmosphere	 Kinetic current density: 4.1 mA cm⁻² at 0.6 V Comparable stability and tolerance to methanol with other Fe-N/C catalysts 	403
Fe-N/C	FeTEPA chelate mixed with pretreated BP 2000 powder	Pyrolyzed at 800°C for 90 min with a heating ramp of 5° C min ⁻¹ in N	• E @ -0.6 mA, 47 mV higher than that of Pt/C	404
Fe-N/C	Hemin	Pyrolyzed at 500–950°C in an argon atmosphere for 2 h	 Current density at -0.1 V (vs. Hg/HgO), Self-assembly-HM (950°C): 3.3 mA/cm² 	405
Fe-N/C	MIL-88B-NH3 (MOF)	Pyrolyzed at 900°C in an argon	• E _{1/2} , 0.92 V	406
Fe-N/C	CPM-99 (MOF)	Pyrolyzed at different	• E _{1/2} , 0.802 V for CPM-99(Fe)/C	407
Fe-N/C	Mixture of ferrocene and melamine	Pyrolyzed at 600°C for 10 h with a heating ramp of 10°C/min	 Kinetic current density (j_k) NC-600: 4.02 mA/cm² Better methanol tolerance than Pt/C 	408
Fe-N/graphene	Mixture of precipitates (ZnO/GO) , FeCl ₃ · 6H ₂ O and melamine	Pyrolyzed at 900° C for 2 h under Ar, H ₂ SO ₄ leaching	 Cathodic current, -1.80 mA /cm² for Fe/N/GR-50-(0.10) Better stability and methanol tolerance than Pt/C 	409
	Iron (II) 1-cyclopenta-2,4-dienyl reduced graphene oxide	Pyrolyzed at 800°C for 2 h under nitrogen flow followed by treatment at 800°C for 10 min under NH ₂	• Onset potential is 13 mV lower than that of Pt/C	410
	2,2-bipyridine and FeCl ₃ · 6H ₂ O encapsulated in SBA-15	Pyrolysis at the given temperature for 3 h in high pure N ₂ , a heating rate of 2° C min ⁻¹ HE etching	• E _{1/2} , Fe–N–GC-900: 0.86 V	411
Fe-N/CNTs	Mixture of FeCl ₃ , Polypyrrole and carbon nanotubes	Heat treated in N ₂ flow at different temperatures (700, 800, and 900°C) for 2 h, H ₂ SO ₄ leaching	 E_{onset} and E_h of NCNT-800 are comparable to Pt/C Tolerant to MeOH 	412
N-Fe CNT/CNP	Mixture of iron acetate, cyanamide and BP 2000	Pyrolyzed at 950°C in nitrogen for 1 h, H_2SO_4 leaching	• $E_{1/2}$, 0.87 \pm 0.01 V at the loading of 0.2 mg cm ⁻² , 0.93 V at the loading of 1.0 mg cm ⁻² • Superior stability than Pt/C	252
Co-N/C	Mixture of pyrrole, carbon dots and $Co(NO_3)_2 \cdot 6H_2O$	800°C for 2 h	 Onset potential: -0.005 V vs. Ag/AgCl) Number of Electron transfer: 3.8 High cycling stability and tolerance to MeOH 	413
Co-N/C	Mixture of ethylenediaminetetra acetic acid (EDTA), melamine, KOH and Co(NO2 - 6H2O)	$700^\circ C$ for 2 h with a heating rate of $10^\circ C\ min^{-1}$ under N_2	 E_{1/2}, NPC-Co₄₅: 0.79 V e⁻ selectivity 	414
Co-N/C	Mixture of N,N' - bis(salicylidene)ethylenediamine and CoSQ $_4$.7H2O	Heat treated at different temperature for 2 h under N_2	• j _k at -0.10 V (mA cm ⁻²), Co-N-S/C-700: 4.80	415
Co-N/C	Co-COF	Pyrolyzed for 2 h under N_2	• Number of Electron transfer: 3.86 for Co-COF-900	416

Table III. Novel Metal- N_x electrocatalysts synthesized by pyrolysis at high temperature.

Table III. (Con	ntinued.)			
Material	Precursors for pyrolysis	Synthesis parameters	ORR performance	Ref
Co-N/C	Vitamin B12 (VB12) and carbon quantum dots	Heat treated at 500, 700 or 900°C for 4 h under N_2 , at the rate of 5°C min ⁻¹	 Number of Electron transfer: 3.56 for Co_{1.12}/N_{2.92}/C-700 Onset potential: -0.1 V (vs. SCE) for Co_{1.12}/N_{2.92}/C-700 Outperformed methanol tolerance and stability 	417
	Vitamin B12 (VB12) and graphene	Heat treated at 600–800°C for 2 h under Ar, a heating rate of 5° C min ⁻¹	 E_{1/2}, 0.833 V for g-VB12 High stability 	418
	Vitamin B12 (VB12) and BP2000	Heated at different temperatures for 2 h under NH ₃	 E_{1/2} (vs. Hg/HgO), 0.072 V for g-VB12 n = 3.9 Superior methanol tolerance to Pt/C 	419
Co-N- graphene	Mixture of cobalt dichloride, GuHCl (guanidine hydrochloride) and GO (graphene oxide)	Heat treatment at 650, 750, 850 and 950°C for 1 h in an Ar atmosphere	• E _{1/2} (vs. SCE), Co-NG 850: -0.164 V (Pt/C: -0.181 V)	420
Co-N- graphene	Mixture of melamine, cobalt nitrate and GO	Heat treatment at 850°C for 30 min under Ar	 Number of electron transfer: 3.97 for Co–N-GX Onset potential: -0.05 V (vs. Ag/AgCl) for Co–N-GX 	421
Mg-Co-Al- N/C	Mg-Co-Al layered double hydroxides	Heat-treated at 600, 700 and 800°C for 3 h, in acetonitrile vapor	• 2-electron pathway	422
Metal-N-C	Poly(ethyleneimine) mixed with $Co(NO_3)_2 \cdot 6H_2O$, $Fe(NO_3)_3 \cdot 9H_2O$, $Ce(NO_3)_3 \cdot 6H_2O$, and $CoSO_4 \cdot 7H_2O$	Heat-treated at 800°C for 1 h under a nitrogen atmosphere	• E _{1/2} (vs. SHE), Co-PEI: 0 mV	423
Metal-N- graphene	Metal oxides-Polyaniline-Graphene	Heat-treated at 800°C under a nitrogen atmosphere	 E_{1/2} (vs. Ag/AgCl), Fe–NCG: -0.19 V, Co–NMCG: -0.18 V, FeCo–NMCG: -0.18 V Number of electron transfer: Fe–NCG: 3.9, Co–NMCG: 3.4, FeCo–NMCG: 3.8 	424

*ORR kinetics parameters were obtained at room T, 1 atmosphere. Potentials were referred to the reversible hydrogen electrode (RHE) unless they are addressed otherwise.



Figure 12. The synthesis routes to M-THPP/PSS-rGO composites Reprinted with permission from Ref. 488 Copyright 2014 Royal Society of Chemistry.

2-dimensional structure of rGO and the intact M-THPP moieties 638 may provide a stronger π - π interaction than that between Co por-639 phyrins and regular carbon black,¹⁴⁶ resulting in a $E_{1/2}$ of -0.22640 V (vs. SCE) for the CoTHPP/PSS-rGO close to Pt/C (-0.20 V vs. 641 SCE). In another work, Liu et al.¹⁹⁷ synthesized a FePc-graphene cat-642 alyst through an amidation reaction between carboxyl-functionalized 643 graphene oxide and iron(II) tetra-aminophthalocyanine at 90°C. Af-644 ter being covalently bonded onto the graphene surface, the catalyst 645 shows comparable catalytic activity with Pt/C as well as high stability 646 and tolerance to crossover of methanol. Within the same category, a 647 hybrid metal framework type of Fe porphyrin based catalyst ((G-dye-648 FeP)nMOF) was synthesized by the combination of (Fe-P)_n MOF 649 and G-dye (pyridine-functionalized graphene) that is terminated with 650 pyridinium moieties.¹⁹⁸ The catalyst synthesized at 150°C shows a 651 favored 4-electron ORR pathway with a n value of 3.82 and superior 652 durability to that of Pt/C. The strong π - π stacking interaction may 653 remain without any linker between the graphene sheets and the macro-654 cycles. Graphene nanosheets and chemically reduced graphene sup-655 656 ported iron phthalocyanine electrocatalysts were prepared by simple mixing under ultrasonication at room temperature.^{199,200} The resulting 657 catalyst exhibits excellent ORR activity and a long-term stability and 658 tolerance to CO in alkaline solution. 659

The special synergic effect has also been found on other 2-660 dimensional carbon materials such as carbon nanotubes.²⁰¹⁻²⁰⁴ For 661 662 example, after subjection of a mixture of nanoFeTSPc and MWCNTs to microwave irradiation, both hydroxyl/carboxyl (o) and sulfonate-663 functionalized (s) MWCNTs supported electrocatalysts were formed. 664 The nanoFeTSPc-o-MWCNT catalyst gives the best ORR perfor-665 mance in terms of the half wave potential and the catalytic rate 666 constant.²⁰¹ In another example,²⁰² FePc/SWCNTs composite synthe-667 sized by direct mixing of individual components shows high activity 668 and perfect selectivity for ORR as well as insensitivity to methanol. 669 Apart from the 2-dimensional carbon materials such as graphene and 670 carbon nanobutes with conjugated π electron character, it is intriguing 671 and surprising to see that some regular carbon supported organometal-672 lic complexes showing fast ORR kinetics were prepared at low tem-673 peratures. For example, Quernheim et al.²⁰⁵ used regular carbon black 674 to support a series of cobalt phenanthroline-indole macrocycles with-675 out any heat treatment and found that the catalysts show very close 676 $E_{1/2}$ values to Pt/C as well as long term stability and tolerance to 677 MeOH. 678

Metal-N_x/C electrocatalysts with novel compositions or shapes.— 679 It is more common to see Fe- or Co-N_x coordinates than other metal-680 N complexes as ORR electrocatalysts. However, recently, it has been 681 found that other third row transition metals can also be used to form 682 metal-N composite catalysts with outstanding ORR activity and stabil-683 ity. For example, Kang et al.²⁰⁶ prepared nitrogen-doped carbon from 684 glycine and performed heat treatment with a mixture of KMnO4 and 685 the N-carbon support. The obtained Mn-CN_x catalyst shows an ORR 686 $E_{1/2}$ potential that is only 12 mV lower than Pt/C. Ding et al.²⁰⁷ synthe-687 sized carbon-supported nickel phthalocyanine catalysts by a solvent-688 impregnation and milling procedure followed by heat treatment at 689 different temperatures. Although both metallic and N-coordinated Ni 690 were formed, only incomplete oxygen reduction was observed on 691 these catalysts. 692

In addition to single core metal-N_x complexes, bimetallic or 693 nitrogen-coordinated catalysts have drawn more and more attention 694 for further improvement of the catalytic activity and selectivity for 695 ORR. Fu et al.²⁰⁸ pyrolyzed a paste of a mixture of PANI modified 696 GO sheet, FeCl₃ and Co(NO₃)₂ and obtained the FeCo-N-rGO cat-697 alysts with a striking positive shift of $E_{1/2}$ of 46 mV as compared 698 to Pt/C. It was believed that the enhancement is from facilitation of 699 incorporation of Fe-N_x moieties into graphene sheets by the Co-N_x 700 moieties.²⁰⁸ In another work, an Fe co-added CoPc-/C catalyst ex-701 hibits more than 40 mV positive shift for the onset potential and the 702 half-wave potential as compared to the CoPc-/C pretreated under the 703 same conditions.²⁰⁹ The enhancement of performance was attributed 704 to generation of Fe-Nx moieties, indicating that the Co-Nx framework 705 may allow for rearrangement of N coordination during the pyrolysis 706

process. In addition to combination of intrinsically active elements 707 of Co and Fe, a bi-core CuFe-Nx/C composite electrocatalyst was synthesized by simple pyrolysis of FePc and CuPc precursors.^{96,153} 709 Although the Cu-Nx/C catalyst shows very limited ORR catalytic 710 activity, a synergistic interaction between Cu and Fe was confirmed 711 by high resolution X-ray photoelectron spectroscopy (HR-XPS) and 712 soft X-ray absorption spectroscopy (XAS) measurements, resulting 713 in enhancement of the ORR performance over that of the single core 714 Fe-N_x/C catalyst. 715

Although the metal-N_x catalysts typically are amorphous in the 716 tens of nanometer range, some pioneering work has been done to pre-717 pare ORR catalysts with special shapes at the submicrometer or mi-718 crometer range. Chao et al.²¹⁰ polymerized melamine with formalde-719 hyde and doped with Co. The hierarchical peanut-like catalyst (Fig-720 ure 13a) generated after hydrothermal reaction followed by heat treat-721 ment shows high catalytic activity (Figure 13b) for ORR in alkaline 722 media. By heat treatment of a mixture of melamine, polyacrylonitrile 723 (PA) and ferric chloride (FeCl₃), another fog-like fluffy structured Fe-724 N_x/C (Figure 13c) catalyst was prepared. The added melamine was 725 found to be responsible for an increase of the porosity and defects in 726 the carbon matrix and modification of the N content and distribution, 727 leading to high ORR performance (Figure 13d) and outstanding sta-728 bility for the catalysts. Furthermore, an ordered hierarchically porous 729 structure (Figure 13e) seems to be beneficial to achieve a higher onset potential and higher current density than Pt/C on a N and Fe codoped 731 catalyst(Figure 13f). Without any carbon support, a hollowed-out oc-732 tahedral Co(II)-N complex (Figure 13g) with comparable ORR activ-733 ity to that of Pt/C (Figure 13h) was formed by a two-step synthesis 734 process (self-assembly at room T and carbonization at 800°C). 735

Other types of non-noble-metal electrocatalysts.—Metal oxides.—It is 736 plausible that the ORR catalytic activity of the first row transition met-737 als relies on multiple and reversible oxidation states that operate near 738 the equilibrium potentials of ORR, providing that nitrogen coordinated 739 metal ions instead of metallic forms can be used as efficient catalyst 740 materials. Analogously, transition metal oxides that remain stable in 741 alkaline media are expected to show similar intrinsic properties for 742 ORR. Indeed, Chatenet et al. have studied a series of nanostructured 743 MnO_x compounds that not only exhibited excellent ORR activity in 744 alkaline media but also showed high tolerance to sodium borohydride 745 and ethanol that could be used as fuels for alkaline direct liquid fuel cells.^{211–213} In Su et al.'s DFT and electrochemical study,²¹⁴ a nanos-747 tructured a-Mn₂O₃ has been shown to be an excellent bi-functional 748 catalyst for both oxygen reduction and oxygen evolution reactions 749 (OER). Figure 14a depicts a general MnO_x Pourbaix diagram and 750 clearly shows that the MnO_x electrode exhibits different oxidation states with various surface adsorbates at various potentials and pH 752 values. From 0.69 V to 0.98 V, the onset potential region for ORR, 753 the MnO_x catalyst is oxidized into 1/2 ML HO^{*} covered Mn₂O₃(110) 754 that is indicative of an active surface. It is a reminiscent of the active 755 site of square-planar Fe^{2+} – N_4 with the axial adsorbate of labile OH⁻ anion for the Fe-N_x/C catalysts.³³ From Figure 14b, it is interesting 757 to observe that bulk $Mn_3O_4(001)$, $Mn_2O_3(110)$ and $MnO_2(110)$ show 758 only a marginal difference in terms of activity for ORR. That means, 759 unlike most of noble-metal and metal-Nx electrocatalysts, the ORR is 760 possibly much less sensitive to the starting oxidation states, which is 761 further evidenced by examples including metal oxides and hydroxides 762 shown in Table IV. 763

Nevertheless, it has been found that the ORR activity can be signif-764 icantly influenced by the nanostructure on metal oxide catalysts with 765 the same composition.²¹⁵ Meng et al.²¹⁵ synthesized α -, β -, δ - and 766 amorphous MnO_2 and found that only α - MnO_2 can catalyze ORR in a 4-electron transfer mechanism as opposed to 2 e⁻ transfer on other 768 MnO₂ samples. In another work, Selvakumar et al.²¹⁶ synthesized 769 different types of α -MnO₂ nanostructures by a hydrothermal method, 770 and found that ORR activity follows an order of nanowire > nanorod 771 > nanotube> nanoparticle > nanoflower. This is in line with the find-772 ing that a long belt-like a-MnO₂ catalyst shows doubled and 4 times 773 higher mass activity than a mixed tremella and short belt-like a-MnO₂ 774 catalyst and a Tremella-like d-MnO₂ catalyst respectively (Figure 15). 775



Figure 13. (a) A SEM image of the peanut-like Co/N-PC Reprinted with permission from Ref. 210 Copyright 2015 Elsevier. (b) ORR polarization curves of the N-C, peanut-like Co/N-PC and commercial Pt/C catalysts at a scan rate of 10 mVs⁻¹ at 1600 rpm. Reprinted with permission from Ref. 210 Copyright 2015 Elsevier. (c) A TEM image of Fog-like fluffy CPAM-50. Reprinted with permission from Ref4.89 Copyright 2015 Royal Society of Chemistry. (d) LSV curves of fog-like fluffy CPA, CPAM-30, and CPAM-50. Reprinted with permission from Ref. 489 Copyright 2015 Royal Society of Chemistry. e. A TEM image of ordered hierarchically porous Fe-NOHPC Reprinted with permission from Ref. 490 Copyright 2014 Wiley-VCH. f. ORR polarization curves for ordered hierarchically porous Fe-NOHPC, Fe-NPC, NOHPC, and Pt/C catalysts at a rotation rate of 1600 rpm in O2-saturated 1 M NaOH. Reprinted with permission from Ref. 490 Copyright 2014 Wiley-VCH. g. A FE-SEM image of hollowed-out octahedral Co/N-HCOs. Reprinted with permission from Ref4.91 Copyright 2015 Elsevier. h. Polarization curves of Co/N-HCOs and Pt/C at 1600 rpm in O2-saturated 0.1 M KOH solution. The polarization curveswere measured in O2-saturated 0.1 M KOH at a scan rate of 10 mVs⁻¹. Reprinted with permission from Ref. 491 Copyright 2015 Elsevier.

⁷⁷⁶ The models described in Su et al.'s work²¹⁴ may be applicable to other

Transition metal oxides with prevalent phase changes on the electrode surface and in the sub-surface region with examples summarized in

779 Table IV.

For noble-metal and metal-N_x types of ORR electrocatalysts, the 780 carbon support has been widely used to improve the dispersion of 781 metal nanoparticles and provide specific anchoring sites for metal-N_x 782 active centers or synergic interactions between catalysts and the sup-783 port. Although in some cases in Table IV, decent ORR kinetics can 784 also be achieved on the metal oxide catalysts themselves, this does 785 not mean that the carbon support is a reductant. Not only can the 786 conductivity be enhanced by mixing with carbon for electronic per-787 colation, but also some synergic effects might exist for achievement 788 of better ORR performance in terms of both activity and stability.²¹⁷ 789 It has been found that the MnOx nanoparticles shape/phase and activ-790 ity can be changed by using different carbon substrates.^{218–221} Many 791 ²²⁵ mesoporous types of carbon materials including carbon black,²² 792 carbon,^{226,227} carbon nanotubes^{228–230} have been employed as supports 793 for transition metal oxide composites. A recent review has also thor-794 oughly covered the "starred" graphene supported non-noble-metal 795 oxide electrocatalysts.231 796

Transition metal chalcogenides and sulfur doped non-noble-metal 797 catalysts.- Transition metal based chalcogenides are an important 798 class of alternative materials to Pt based electrocatalysts in acidic me-799 dia due to their promising ORR activity and tolerance to crossover 800 of methanol, and received continuous exploration in PEMFCs for 801 the past two decades.^{232–234} Nonetheless, the enthusiasm for utiliza-802 tion of transition metal chalcogenides in alkaline media seems to 803 be surpassed by other types of transition metal electrocatalysts (vide 804 ante), given the very few reports in the literature during the last three 805 years. All the same, some attempts to develop transition metal chalco-806 genides with novel compositions and structures have been put into 807 practice, which help to better understand some fundamental func-808 tions of this class of materials for ORR in alkaline media. Tetragonal 809 and cubic phase Cu₂Se nanowires (NWs) were synthesized using a 810 self-assembling method at 220°C and 280°C respectively.¹²⁷ From the 811 kinetics study, the ORR pathway is structure-dependent with a direct 812 4e⁻ mechanism on the tetragonal Cu₂Se NWs and a dual-path mode 813 that comprises both 2e⁻ and 4e⁻ mechanisms on the cubic Cu₂Se 814 NWs. However, no further investigation follows the hypothesis that 815 the spatial arrangement of Cu and Se atoms affects the adsorption and 816 activation of O₂ molecules and modulates the electrocatalytic ORR 817 performance of Cu₂Se NWs. Different from the synthesis route using 818 surfactants for phase structure control of Cu₂Se NWs, CoSe₂/C was 819 prepared via a two-step heating reaction method in p-xylene without 820 any surfactants.²³⁵ The as-synthesized cubic CoSe₂ catalyst shows a 821 four-electron transfer pathway for ORR in alkaline media and higher 822 tolerance to methanol than Pt/C. Analogous to selenium, transition 823 metal sulfur chalcogenides were also studied for the catalytic reduc-824 tion of oxygen in alkaline media. 825

With a general goal of improvement of conductivity and investi-826 gation of possible synergetic coupling effects between metal sulfides 827 and nitrogen doped graphene, aerogel-supported NiS₂ nanoparticles 828 were prepared by a one-pot hydrothermal method.²³⁶ Only nitrogen 829 was doped into the graphene support, and the existence of a synergetic 830 effect between NiS2 and NG was inferred according to the more pos-831 itive onset potential and higher current density of ORR on NiS₂/NG 832 as compared to stand-alone NiS₂ and NG. In another example, Peri-833 asamy et al.²³⁷ prepared Cu₉S₈/CNT nanocomposites by a one-step 834 wet chemical method. In spite of some catalytic activity for ORR 835 and good tolerance to MeOH and CO, a hypothesis of formation of 836 oxy-hydroxyl species of Cu(II) on the Cu₉S₈/CNT loaded electrode 837 surface requires further attention with regard to the stability of this 838 catalyst material. 839

From the above Carbon supported $M-N_x$ matrix (M = 3d transition 840 metals) and Metal oxides section, it can be seen that N-doped carbon 841 has been commonly used as a support material. For the purpose of 842 increasing new non-electroneutral sites on carbon backbones, some 843 recent works have focused on adding another doping heteroatom of 844 sulfur during the synthesis of non-noble-metal electrocatalysts. Xu 845 et al.¹⁹² found that a N and S co-doped Fe–N/C–TsOH catalyst using 846 TsOH (p-toluenesulfonic acid) as the S precursor shows better ORR 847 activity than the sulfur free catalyst. The enhancement was ascribed 848



Figure 14. (a) General surface Pourbaix diagram for MnO_x catalysts. The oxidation state of the surface and the ORR and OER potential are constant versus the reversible hydrogen electrode (RHE). Lines a and b represent the RHE line and the O_2/H_2O equilibrium line. Reprinted with permission from Ref. 214 Copyright 2012 Royal Society of Chemistry. (b) Calculated current density for Mn_3O_4 , Mn_2O_3 and MnO_2 . Reprinted with permission from Ref. 214 Copyright 2012 Royal Society of Chemistry.

Table IV	. Nove	l non-noble metal	oxides	electrocatal	vsts for	ORR in	alkaline me	dia
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Metal element	Electrocatalyst	Doping elements	Preparation method; Precursors	Catalyst morphology /shape	ORR kinetics parameters	Ref.
	Manganese oxide octahedral molecular sieve	-	One-pot wet synthesis, calcination at different temperatures for 8 h; KMnO ₄	Short nanorods (with CTAB), Nanofiber (without CTAB)	$E_{1/2}$ (vs. SCE) HT-OMS-2_{500} $^{\circ}\mathrm{C}$: $-0.2~\mathrm{V}$	425
	Cu-a-MnO ₂	Cu	A hydrothermal method; $KMnO_4$, $MnSO_4 \cdot H_2O$, $Cu(NO_3)_2 \cdot 3H_2O$	Nanowire	$\begin{array}{l} E_{1/2} \left(vs. \; Ag/AgCl \right) \left[Cu\% = 2.92 \right]: \\ -0.292 \pm 0.018 \; V \end{array}$	426
	Mn ₃ O ₄ /NrGO	Ν	Electrodeposition process; Mn(CH ₃ COO) ₂	Hierarchical nanoflakes network	E _{1/2} (vs. Ag/AgCl) Mn ₃ O ₄ /NrGO: -0.2 V	427
Mn	Mn ₃ O ₄ /NrGO	N	In situ reduction of both graphene oxide (GO) and Mn(VII)	Nanoparticles	Onset potential for ORR, -0.175 V (vs. SCE)	428
	MnO ₂	-	Using graphene oxide as the template	Layered nanosheets	The number of electrons transferred: 3.4	429
	Mn ₂ O ₃		Calcination; Shewanella loihica PV-4 in the presence of MnO ₄ ⁻	Micro-/nanocubes	$ E_{1/2} \mbox{ (vs. Ag/AgCl), } Mn_2O_3\mbox{-}500\mbox{:} \\ -0.24 \pm 0.003 \mbox{ V} $	430
Fe	FeO _{1.4} /N-C	N	Hydrothermal reaction at 180°C and a thermal treatment at 800°C for 2 h under nitrogen atmosphere; Fe(NO ₃) ₃ · 9H ₂ O	Wires with ultrafine particles	$ J_k = 0.9 \text{ mA mg}^{-1} _{Catalysts} @ \\ -0.1 V (vs. Ag/AgCl) $	431
	Fe ₃ O ₄ /N-C	N	Solvothermal carbonization process; Ferric chloride	Granular-like	E _{1/2} (vs. Ag/AgCl), Fe ₃ O ₄ /N–C-900: -0.184 V	432
	Fe ₃ O ₄ /N-C	Ν	Fe ³⁺ - mediated polymerization of dopamine on SiO ₂ nanospheres, carbonization and subsequent KOH etching of the SiO ₂ template	Hollow nano-spheres	The number of electrons transferred, 3.8	433
	$Fe_X @NOMC (X) = 25, 10, 5)$	Ν	Precursors (FcN][NTf ₂ and [MCNIm][N(CN) ₂]] filling in SBA-15, calcination and subsequent template removal	Semiexposure morphology	$J_k = 5.30 \text{ mA cm}^{-1} @ -0.5 \text{ V}$ (vs. MMO) for Fe ₁₀ @NOMC	434
	Fe ₃ O ₄ /N-GAs	Ν	Hydrothermally assembled at 180°C, iron acetate	Nanoparticles	Onset potential for ORR, -0.19 V (vs. Ag/AgCl)	435
Co	Fe-doped Co ₃ O ₄ nanofilms	Fe	Electrodeposition at -0.8 V for 600 s, annealing at 400°C for 4 h; Co(NO ₃) ₂ · 6H ₂ O, FeCl ₃ · 4H ₂ O, FTO conductive substrates	Flower-like architecture	Onset potential of -0.162 V (vs. Ag/AgCl)	436
	Co(OH) ₂ / graphene	-	Electrodeposition from Co(NO ₃) ₂	Interlaced nanowalls	$E_{1/2}$, positive shift of 190 mV compared to GC	437

Table IV. (Continued.)

Metal element	Electrocatalyst	Doping elements	Preparation method; Precursors	Catalyst morphology /shape	ORR kinetics parameters	Ref
	CoO/CNTs	Ν	Growing nanocrystals on oxidized multiwalled CNTs, annealing in NH ₂ : Co(OAc)	Cubic rock salt structure	-	230
	Co ₃ O ₄ /C	-	A solvent-mediated morphological control method, annealing at 330°C for 2 h; CoClo : 6H ₂ O	Nano-rods and spherical structures	J _{-50, -600 mV} / mA cm ⁻² Co ₃ O ₄ -11: 0.239, 3.54	438
	Co ₃ O ₄ /rGO	-	A one-pot hydrothermal $Procedure: Co(Ac)_2 \cdot 4H_2O$	Nanorods	The number of electrons	439
	Co ₃ O ₄ /N-MG	Ν	Hydrothermal reaction at 150° C for 3 h: Co(Ac) ₂	-	Onset potential, 0.93 V	440
	Co/Co ₃ O ₄ /C–N	Co, N	Sol-gel, annealed in N_2 at different temperatures; $Co(NO_3)_2 \cdot 6H_2O$	Nanoparticles	Onset potential, Co/Co ₃ O ₄ /C-N-750: -36.0 mV (vs. Hg/HgO)	441
	CoO@Co/N–C	Co, N	Reflux reaction at 90°C, annealed in Ar at 700°C; cobalt(II) chloride hexahydrate	Particles with diameter of about 30–50 nm	Onset potential, 0.99 V	442
	g-C ₃ N ₄ @CoO	C, N	Wet impregnation, 550°C under Ar; Co(OAc) ₂ , cyanamide	A core-shell structure	J_k , 16.78 mA cm ⁻² at -0.25 V (vs. Ag/AgCl)	443
	Co-gC ₃ N ₄ / graphene	C, N	Wet impregnation, 600°C under Ar; Dicyandiamide and Co(OAc) ₂ · 4H ₂ O	Uniform porous morphology	E _{1/2} (vs. Ag/AgCl), CCNG-600: -0.141 V	444
Ni	Ni(OH) ₂ /GO	-	A microwave irradiation approach; nickel(II) acetate	Platelets and rhombus particles	The number of electrons transferred, 3.5	445
Cu	Cu ₂ O	-	A reductive solution route; $Cu(Ac)_2$	Nanocubes	The number of electrons transferred, 3.7	446
	Cu/TiO ₂	-	A hydrothermal method; copper acetate	Nanoparticles	The number of electrons transferred, 3.74	447
Bimetallic	NiO/NiCo ₂ O ₄	-	Coaxial electrospinning, annealing treatment at 600°C in air; Co(Ac) ₂ · 6H ₂ O, Ni(Ac) ₂ · 6H ₂ O	Nanotubes	Onset potential for ORR, -0.05 V (vs. Ag/AgCl)	448
	MnO _x -Co ₃ O ₄ /C	-	Wet Chemistry; $Co(OAc)_2$, KMnO ₄	Nanoparticles on nanosheets	E _{1/2} , 814 mV	223
	Ni(OH) ₂ -MnO _x /C	-	Reducing the amorphous MnO ₂ /C suspension in the presence of Ni ²⁺ with NaBH4; Mn(CH ₃ COO) ₂ \cdot 4H ₂ O, KMnO ₄ , Ni(NO ₃) ₂	Floccule	$E_{1/2}$, positive shift of 0.05 V compared to MnO ₂ /C and MnO _x /C; Unchanged electron transfer number after AAT testing	224
	Co ₂ FeO ₄ /MWCNT	-	Wet chemistry, annealing at 350° C for 3 h under H ₂ atmosphere; CoCl ₂ · 6H ₂ O, FeCl ₂ · 4H ₂ O	Hollow structured	E _{1/2} , 0.73 V	449
	NiCo ₂ O ₄	-	A facile hydrothermal method at 180° C for 6 h; Ni(NO ₃) ₂ · 6H ₂ O, Co(NO ₃) ₂ · 6H ₂ O	Urchin-like sphere	Onset potential for ORR, 0.83 V	450
	NiCo ₂ O ₄	-	A hydrothermal method at 180° C for 12 h, annealed 400° C for 2 h; Ni(NO ₃) ₂ · 6H ₂ O, Co(NO ₃) · 6H ₂ O	Macroporous sheets	The number of electrons transferred, > 3.5	451
Spinel	ZnCo ₂ O ₄ /NCNT	Ν	Solvothermal preparation at 150°C for 10 h; Co(OAc) ₂ · 6H ₂ O, Zn(NO ₃) ₂ · 6H ₂ O	_	The number of electrons transferred, > 3.7	452
	CuCo ₂ O ₄ /N-rGO)	Ν	A simple solvothermal method at 160°C for 3 h; Co(OAc) ₂ , Cu(OAc) ₂	-	The number of electrons transferred, 3.8	453
	CoMn ₂ O ₄ / PDDA-CNTs	-	A solvothermal method at 180° C for 10 h, Co(OAc) ₂ · 6H ₂ O and Mn(OAc) ₂ · 6H ₂ O	_	$E(V) @ I = -3 mA cm^{-2},-0.133$	454
	CoMn ₂ O ₄ , MnCo ₂ O ₄	_	Thermal degradation at 400°C	-	The number of electrons transferred, CoMn ₂ O ₄ : 3.68, MnCo ₂ O ₄ : 3.51	455

*ORR kinetics parameters were obtained at room T, 1 atmosphere. Potentials were referred to the reversible hydrogen electrode (RHE) unless they are addressed otherwise.



Figure 15. SEM images of Tremella-like δ -MnO₂ (a and b), mixed tremella and short belt-like α -MnO₂ (c and d), and long belt like α -MnO₂ (e and f). Inset in b: photograph of dried Tremella fuciformis fungi forcomparison (http://tupian.baike.com). Reprinted with permission from Ref. 492 Copyright 2015 Elsevier.

to the altering of electroneutrality of the carbon backbone, increase of 849 support porosity, and assistance of trapping of Fe ions in a pyrole-type 850 N enriched environment caused by formation of C-S-C and oxidized 851 -SO_n-bonds. Qing et al.²³⁸ used copper phthalocyanine tetrasulfonic 852 acid tetrasodium salt as the single precursor for Cu, N, and S during a 853 pyrolysis reaction. In addition to the increased porosity of the carbon 854 support and C-S_n-C (n = 1,2) bonds formation, it was believed that the 855 inhibition of creation of copper carbide in the presence of sulfur is also 856 helpful in achieving the superior ORR performance. From the above 857 ^{39–243} there is no evidence yet studies and others in the literature, 37,128, 858 to show that there is any coordination between sulfur and metal that 859 is responsible or not for ORR catalytic activity as it does in the case 860 861 of N and metal.

Similar to Ni-Co based spinel in Table IV, some thiospinel 862 type NiCo₂S₄/rGO catalysts were prepared using a solvothermal 863 strategy with NaS or thiourea as the reducing agents and sulfur 864 precursors.^{244,245} With more octahedral catalytically active sites of 865 Co^{3+244} , the as-synthesized sulfur doped catalysts show similar ORR 866 activity to that of Pt/C and better durability and tolerance to MeOH 867 than the spinel NiCo₂O₄-rGO counterpart. In addition, the improved 868 ORR performance may be benefited by the enhanced conductivity re-869 sulting from doping S into graphene, as indicated by the XPS signals 870 of thiophenic-S (aromatic C-S-C). 871

Carbides & nitrides/oxynitrides.— As indicated in Table III, a 872 large number of active metal- N_x/C catalysts can be synthesized by 873 a high temperature pyrolysis process. Aside from the formation or 874 rearrangement of metal-N bonds and anchoring in some specific sites 875 on the carbon support, it is inevitable to encapsulate some metal-876 lic particles in graphitic carbon shells,²⁴⁶⁻²⁴⁹ which are thought to 877 be spectators for ORR.²⁴⁹ The important role of the metal carbide 878 phase in the ORR had not been paid much attention until some recent 879 studies on this specific topic came out. Hu et al.²⁴⁶ placed a mixture 880 of cyanamide and ferrocene in an autoclave and pyrolyzed the sealed 881 raw materials at 700°C-800°C. While the pressure inside the autoclave 882 reached 600 bar, Fe₃C nanoparticles encased by uniform graphitic lay-883 884 ers (Figure 16) instead of Fe-N moieties were formed unexpectedly.



Figure 16. Oxygen reduction process on Fe_3C/C -700 (scale bar = 5.00 nm). Reprinted with permission from Ref. 246 Copyright 2014 Wiley-VCH.

The "high- temperature, high-pressure" obtained Fe₃C/C catalysts 885 showed very similar ORR behavior to that of Pt/C in 0.1M KOH even after hot acid leaching, indicating that there remains a synergic in-887 teraction between the Fe₃C particles and the surrounding protective graphic layers. Yang et al. 250 added PEG-PPG-PEG Pluronic P123 888 889 into a mixture of melamine and $Fe(NO_3)_3$ (no carbon support) and 890 successfully prepared bamboo-like carbon nanotube/Fe₃C nanoparti-891 cle hybrids after pyrolysis at 800°C in N2 under normal pressure. The ORR half-wave potential on the PMF-800 catalyst showed a positive 893 shift of 49 mV compared to a 20 wt% Pt/C catalyst and much higher 894 stability and better methanol tolerance. In line with the Fe₃C/C cata-895 lysts in Hu et al.'s study,²⁴⁶ it was found that the Fe₃C nanoparticles 896 were encapsulated in b-CNTs, leading to a change of local work functions of CNT walls and strong stability in both acidic and alkaline 898 media.251 800

For electrocatalysis in fuel cells, group IVB to VIB transition metal 900 carbides such as TiC, ^{256–258} ZrC, ²⁵⁹ WC/W₂C^{260–262}, VC, ²⁶³ Mo₂C²⁶⁴ 901 have been typically used as support materials to improve the stability 902 of the electrocatalysts. Nevertheless, using a one-step hydrothermal 903 method, TiC nanowires were synthesized and exhibited doubled ex-904 change current density in comparison to the TiC powder sample.²⁵⁶ As 905 expected, the one dimensional TiC catalyst also showed very good sta-906 bility and tolerance to MeOH. In addition to the above monometallic 907 transition metal carbides, a bimetallic CoWC@C catalyst was synthesized by a reduction and carbonization method in a flow of H₂ and 909 Ar.²⁶⁵ The higher catalytic activity of the bimetallic CoWC@C cata-910 lyst as compared to WC@C and Co@C was attributed to the formation 911 of a Co₃W₃C phase as the active site for ORR. 912

In the large family of metal nitrides and oxynitrides, the composites 913 with metal elements from the groups from IVB to VIB have been widely used as ORR electrocatalysts in both acidic and basic media 915 due to their stability and the capability to push electron density towards 916 the Fermi level by contraction of d-bands.^{266,267} Using mpg-C₃N₄ 917 templates to control the particle size, TiN nanoparticles with particle 918 sizes in diameter of 7 nm, 12 nm and 23 nm were prepared with a 919 wet chemistry and a calcination step and tested for ORR in 0.1M 920 NaOH.²⁶⁸ The ORR current follows the order of 7 nm >12 nm >921 23 nm, which is consistent with the order of surface area on the 922 TiN nanoparticles. However, more than 50% of H₂O₂ content for the 923 ORR products on the best TiN-7 nm catalyst indicates that only a two-924 electron transfer process was taking place on the oxynitrided electrode 925 surface. Recently, it was found that the ORR selectivity of TiN can 926 be dramatically improved by formation of a hierarchical TiN/TiCN 927 structure using a chemical vapor deposition approach.²⁵⁸ The interface 928 between TiN and TiCN layers as shown in Figures 17a and 17b was 929 believed to be active for oxygen adsorption. The TiN/TiCN sample 930 (a)



Figure 17. (a) SEM images of the cross-view of titanium nitride/titanium carbonitride hierarchical structures (TNTCNHS-1 and TNTCNHS-2) before Ni template removed. (b) Schematic the active interfaces of TNTCNHS. Reprinted with permission from Ref. 258 Copyright 2014 Nature Publishing Group. (c) Single cell testing of the TNTCNHS-1 and commercial Pt/C as cathode catalysts with a loading of 4 mg cm⁻² and 2 mg cm⁻², respectively. Anode catalysts are both platinum on carbon ($m_{Pt} = \sim 0.4 \text{ mg cm}^{-2}$). Reprinted with permission from Ref. 258 Copyright 2014 Nature Publishing Group.

(TNTCNHS) with Ni template removed was employed and examined
as cathodic catalyst in a single cell. From Figure 17c, with a catalyst
loading of 0.1 mg cm⁻² it shows a higher open circuit potential and
comparable maximum power density to that of a Pt/C cathode.

Other than metals from groups IVB to VIB, recently, late transition 935 metals such as copper have been used to form nitrides for use as ORR 936 electrocatalysts in alkaline media. Wu et al.²⁶⁹ prepared copper nitride 937 nanocubes in a nonaqueous system with programmed increasing tem-938 perature up to 250°C. The Cu₃N nanocubes had an average size of 939 26.0 ± 5.6 nm and exhibited electrocatalytic activity for ORR in 0.1 M 940 KOH, though much lower than a Pd/C catalyst. Regarding the catalytic 941 activity of metal nitrides/oxynitrides, it may be further improved by 942 forming bimetallic composites to obtain multiple active species and 943 tuning of electronic states.^{267,270} A Co_{0.50}Mo_{1-x}Mo_{0.50}O_yN_z synthe-944 sized by an impregnation method followed by ammonolysis demon-945 strated an onset potential of 0.918 V for ORR in 0.1 M KOH. From 946 XPS and EXAFS measurements, it was concluded that the integra-947 tion of CoO into the rock-salt structure of Mo₂N correlates with the 948 enhanced activity. 949

Perovskites.— Although the perovskite materials were proposed
 as ORR electrocatalysts in fuel cells in the 1970s, their performance
 has been limited dramatically by their high ohmic losses, low specific

surface area and crystallite agglomeration.^{271–274} In pursuit of mini-953 mizing the size of crystallites and the degree of their agglomeration, 954 combinations with carbon based materials have been investigated. 955 Perovskite-carbon nanocomposites were prepared via an in situ auto-956 combustion route with Vulcan-XC72 carbon and La and Mn-glycine 957 complex as the precursors.²⁷⁴ By comparison of particle sizes in Fig-958 ures 18A, 18B and Figures 18C, 18D, smaller particles were formed 959 by the in situ autocombustion method than the sol-gel method. From 960 Figures 18E–18H, the degree of agglomeration of oxide perovskite 961 crystalline materials was significantly suppressed on the nanocom-962 posites, leading to a factor of 2.4 activity enhancement. Importantly, 963 a dual role of the carbon support to improve the electrical contact and 964 catalyze O_2 to H_2O_2 was also concluded from the study of LaCoO₃/C 965 and La_{0.8}Sr_{0.2}MnO₃/C composites.²⁷⁵ 966

Others have attempted to improve the intrinsic catalytic activity by modifying the compositions. Suntivich et al.²⁷⁶ correlated the ORR activity with e_g electron numbers of different transition metal oxide perovskites and obtained a volcano plot. It indicates that the B-O (B = Cr, Mn, Fe, Co, and Ni) bond strength that governs the rate-determining step of ORR has a maximum value. Notably different from this finding for oxide perovskites, it is worthwhile to recall that a downshift in energy level of e_g -orbitals generally 974



Figure 18. SEM Images recorded by: SEM (A) and TEM (B) for LaMn-AC; SEM (C) and TEM (D) for LaMn-SG; SEM (E) for LaMn-AC manually mixed with Vulcan–XC72 in 1:1 mass ratio; and SEM (F) and TEM (G, H) for 50-LaMn–ISAC–Vulcan. Reprinted with permission from Ref. 274 Copyright 2015 Elsevier.

leads to higher ORR onset potentials and higher turnover numbers in 975 the case of metal-N electrocatalysts.^{33,139,146,277} Practically, Sunarso 976 et al.²⁷⁸ synthesized LaMO₃ and LaNi_{0.5} $M_{0.5}O_3$ (M = Ni, Co, 977 Fe, Mn and Cr) perovskite oxide electrocatalysts via a combined 978 ethylenediaminetetraacetic acidcitrate complexation technique and 979 subsequent calcinations. Among them LaCoO₃ and LaNi_{0.5}Mn_{0.5}O₃ 980 showed the best ORR kinetics with a 4-electron transfer pathway 981 within each class of materials. 982

Metal-free electrocatalysts.— From the above sections, transition 983 metal based materials (noble-metal and non-noble metal) with charac-984 teristics such as partially filled d band orbitals, multiple and reversible 985 oxidation states, and suitable adsorption energy with O₂ and inter-986 mediates may serve as electrocatalyts for ORR in alkaline media. Of 987 all the non-metal elements in the periodic table, carbon is probably 988 the only element that can possibly be used as the main component 989 of a metal-free electrocatalyst for ORR, provided that some prereq-990 991 uisites such as sufficient conductivity, large surface area, and reasonable stability in extreme pH environments are met. However, a good 992 electrocatalyst for ORR needs to have much more special properties 993 than a simple conductor or current collector. Figure 3c illustrates the 994 double-layer structure at an ideal Pt polycrystalline (or single crystal) 995 electrode in alkaline media. However, in the case of an ideal graphite 996 electrode (with solely sp²-hybridized carbon) there is one electron 997 residing in the unhybridized p orbital that can pair up with one of 998 the O_2 electron pair in the π orbital. This means that O_2 will have 999 to approach the graphite surface horizontally to form an O-C bond 1000 via π - π interaction and rearrangement of electron density. It has been 1001

theoretically calculated and concluded that O_2 in its triplet state has 1002 weaker chemisorption compared to O_2 in its singlet state on graphite 1003 and the chemisorbed species are highly unstable.²⁷⁹ As a result, the 1004 amount of chemisorbed O_2 at the IHP near an ideal graphite electrode 1005 is negligible. 1006

Thanks to the dramatic decrease of overpotential (ca. 0.83 V) for 1007 the first electron transfer ($O_{2,aq} + e^- \rightarrow (O_2^{-})_{aq}$) during ORR with 1008 pH changed from 0 to 14, an outer-sphere electron transfer can still 1009 be facilely conducted with the rather small overpotential that can be 1010 overcome by noncovalent forces such as hydrogen bonding. The hy- 1011 drogen bond formation between non-specifically adsorbed OH⁻ and 1012 solvated O₂ molecules can be further promoted by modification of the 1013 carbon surface with quinone/hydroquinone functional groups.²⁸⁰⁻²⁸² 1014 Nevertheless, for the aforementioned carbon surface, the oxygen re- 1015 duction has to stop at the second electron transfer step with HO₂⁻ as 1016 the major product because there is a lack of proper adsorption sites for 1017 HO₂⁻ to continue the following electron transfer steps.²⁸³ It is there- 1018 fore necessary to modify the crystallographic structure of the graphite 1019 in order to pursue a fundamental change from an outer-sphere elec-1020 tron transfer path to a favored inner-sphere electron path for oxygen 1021 reduction. 1022

As it is generally known that transition metal- N_x moieties anchored 1023 at carbon crystallographic atomic defects such as the divacancy and 1024 armchair edges are key active sites for ORR after a pyrolysis process 1025 with a mixture of precursors of metal and nitrogen and carbon materials, tremendous efforts have been devoted to the investigation of ORR 1027 performance of all kinds of carbon materials with doped heteroatoms 1028 to create defects. Indeed, all metal-free carbon based electrocatalysts 1029



Figure 19. (a) Free energy diagram of different heteroatom-doped graphenes at the equilibrium potential U^0 . Reprinted with permission from Ref. 34 Copyright 2014 American Chemical Society. (b) Enlarged LSVs plots at the ORR initial region for different catalysts on RDE at 1600 rpm in an O₂-saturated 0.1 M solution of KOH. Inset illustrates the first electron transfer step that is O₂ to adsorbed OOH*. Reprinted with permission from Ref. 34 Copyright 2014 American Chemical Society. (c) Volcano plot between j₀ theory and ΔG_{OOH^*} with charge-transfer coefficient $\alpha = 0.5$ (red dashed line). Blue hollow squares are j₀^{expt} obtained from Tafel plots and DFT-derived ΔG_{OOH^*} for each doped graphene catalyst. Reprinted with permission from Ref. 34 Copyright 2014 American Chemical Society. (d) RRDE measured electron transfer numbers (black) and corresponding 2e⁻ pathway selectivity (blue) for N-graphene catalyst. Reprinted with permission from Ref. 34 Copyright 2014 American Chemical Society.

with promising ORR performance reported so far have doped ele-1030 ments such as N, O, B, S, and P (infra vide), whereas the graphene 1031 or reduced graphene oxide catalysts only show limited activity and 1032 selectivity for ORR.^{284,285} Though categorized by the type of carbon 1033 materials in morphology in this section, the importance of dopant for 1034 achievement of complete reduction of oxygen on metal free electro-1035 catalysts will be discussed in each subsection. A more detailed re-1036 view about the effect of different doping elements was also published 1037 recently.286 1038

Graphene based metal-free electrocatalysts.—As the most shining 1039 "star" in the carbon family in the last decade, graphene and func-1040 tionalized graphene materials have been widely used as supports for 1041 ORR electrocatalysts.¹⁰⁵ Only recently has the "secondary role" of 1042 graphene in a cathodic eletrocatlayst for ORR been reconsidered, and 1043 a large number of reports has appeared dealing with the identifica-1044 tion of the basic mechanism of ORR, new synthesis technologies, 1045 improvement of some features like easy stacking, effects of differ-1046 ent heteroatoms and other aspects. Jiao et al.³⁴ constructed models 1047 for 13 configurations of graphene clusters doped with 5 different 1048 heteroatoms (N, S, O, B, and P) and conducted both electrochemi-1049 cal measurements and density functional theory (DFT) calculations. 1050 From Figure 19a, all heteroatom-doped graphene electrodes have the 1051 same rate-determining step, i.e., the first electron transfer to form 1052 OOH*, which is consistent with that on other types of metal based 1053 electrocatalysts^{12,19-21} and dictates the order of onset potentials for 1054 ORR (see Figure 19b). However, due to weak adsorption of OOH* 1055 on these doped graphene surfaces, the theoretical exchange current 1056 density (j₀) values were all located on the right branch of a volcano 1057 plot as shown in Figure 19c. The weak adsorption of OOH* also leads 1058 to an exothermic desorption process, which is the fundamental reason 1059 for the lack of selectivity for ORR and a mixed 2e⁻ (33%) and 4e⁻ 1060 (67%) pathway on the gN-G model (Figure 19d). 1061

Although a molecular orbital origin involving hybridization of the 1062 valence band (v) of the active sites with the (σ) orbital of the adsorbed 1063 oxygen-containing species was proposed,34 the exact identification of 1064 the "active sites" is still quite elusive. It has been demonstrated that 1065 chemisorption of O₂ on N-functionalized carbon is more facilitated 1066 than for N-free carbon surfaces with a ketone formed on the carbon 1067 atoms next to the graphitic-N group.286,287 Raman and XPS are two 1068 major techniques for characterization of the basic structure of the 1069 graphene substrate and different types of doped N. For example, us-1070 ing the D/G band intensity ratio of a Raman spectrum as an index of 1071 the disorder degree and the average size of the sp² domains,^{217,288–290} 1072 Lu et al.²⁹⁰ studied the degree of structural defects and edge plane ex-1073 posure of N-doped reduced graphene oxides with various N contents. 1074 It was found that more defected N-RGO in few-layer flakes was pro-1075 duced after doping with N, which is responsible for the higher ORR 1076 activity on N-RGO than that on RGO. 1077

Lai el al.²⁹¹ prepared various N-graphene samples with different 1078 N precursors and pyrolysis at different temperatures. Pyrodinc N, 1079 pyrrolic N and quaternary N (graphitic N) were identified by their 1080 characteristic peaks corresponding to different binding energy val-1081 ues in XPS spectra. From the ORR results, it was concluded that the 1082 ORR limiting current can be enhanced by graphitic N and the ORR 1083 selectivity for 4e⁻ pathway can be improved by pyridinic N species. 1084 In spite of the controversial role of the type of N (with graphitic $N^{292-294}$, pyridinc $N^{295,\,296}$ and pyrolic $N^{297-300}$ as the dominating fac-1085 1086 tor for ORR), the overall ORR activity should positively rely on the 1087 N content in heterogeneous nanocarbon materials with the limit of 1088 conductivity and active sites considered, assuming the carbon atoms 1089 adjacent to doped N are the active site for O₂ interaction.^{301,302} Zhang 1090 et al.²⁸³ employed a two-step pyrolysis method to synthesize N-doped 1091 graphene with various N contents showing electrocatalytic activity 1092 and long-term stability for ORR in 0.1 M KOH. From both experi-1093 mental and theoretical studies, it was concluded that an optimized N 1094 content should be around 25% to achieve sufficient carbon active sites 1095 with high spin density and charge transfer^{283,298,303} as well as good 1096 conductivity. 1097

Of all heteroatom-doped graphene catalysts, the B-doped is the 1098 most competitive alternative to the N-doped.³⁴ Through a DFT calcu- 1099 lation on a model of graphic B-doped graphene, Fazio et al.³⁰⁴ inferred 1100 that the positively charged boron atom is the active center for ORR in 1101 the B-doped graphene catalysts. For both dissociative and associative 1102 mechanisms of ORR, they conceived that the very first step is the ad- 1103 sorption of molecular oxygen on B atoms with an end-on adsorption 1104 mode. In addition to single element doped graphene, there have ap- 1105 peared a number of studies of bi-element co-doped graphene catalysts 1106 for ORR and the enhanced ORR activity as compared to N-doped 1107 samples was usually attributed to a "synergic effect" between N and 1108 the other elements.^{296,305-308} Although it is probably true that the over- 1109 all ORR activity may be benefited from an increased number of active 1110 sites, improved surface area and conductivity, and other factors under 1111 their specific preparation and testing conditions, the essence and the 1112 actual effect of the so called "synergic interaction" between different 1113 doping atoms needs further investigation. 1114

Although the thorough understanding of adsorption and desorp- 1115 tion modes of O₂ and the reduction intermediates on heteroatom doped 1116 graphene is still pending, the synthesis and evaluation of ORR per- 1117 formance have continued. Table V shows the recent work on ORR in 1118 alkaline media using heteroatom-doped graphene-based electrocata- 1119 lysts without any metal salt added during preparation. It can be seen 1120 that the overall performance of the graphene metal-free catalysts is 1121 still quite far from the standard Pt/C catalyst except the ones with 1122 highly porous structure.³⁰⁹ It has been noticed that bulk graphene 1123 layers typically suffer from serious stacking due to strong π - π inter- 1124 actions, which may cause dramatically reduced specific surface area 1125 and reduced ORR performance.^{310,311} In order to increase the porosity 1126 of heteroatom doped graphene catalysts, a template adding-removal 1127 strategy was usually employed during the doping process prior to 1128 high temperature pyrolysis. For example, an aqueous dispersion of 1129 melamine and GO was dipped into liquid nitrogen to form ice crystal 1130 templates.³¹² After sublimation of the ice and heat treatment, an N- 1131 doped graphene sample with 30 times higher specific surface area than 1132 that without ice crystal templates was formed. The obtained catalyst 1133 showed a decrease of overpotential of 60 mV and produced an oxygen 1134 reduction intermediate of HO · radical. It is also very interesting to 1135 find that graphene like carbon nanosheets can be produced without the 1136 precursor of graphene oxide. As a typical example, Liu et al.³¹³ used 1137 chitosan and urea as the precursors and conducted pyrolysis with- 1138 out any other treatment. The TEM image in Figure 20a shows that 1139 a transparent texture and crumpled-sheet morphology were formed. 1140 Due to the large specific area of $\sim 1510 \text{ m}^2 \text{ g}^{-1}$ and high ratio of 1141 graphitic/pyridinic nitrogen structure, the carbon nanosheet catalyst 1142 showed ORR performance close to that of Pt/C (Figure 20b). 1143

Carbon nanotube based metal-free electrocatalysts.—In principle, the 1144 original cause of ORR activity from carbon nanotubes (CNTs) should 1145 be similar to that of graphene because the latter can be considered as 1146 the configuration of CNT unzipped longitudinally along its axis. As 1147 described in the above section, superior electrocatalytic activity for 1148 ORR on graphene may come from the defects and doping heteroatoms 1149 (for altering the charge density and increase of active sites), which 1150 leads to the major difference of preparation of these two types of 1151 electrocatalysts. From Table V, it can be seen that the synthesis of 1152 heteroatom doped graphene catalysts usually starts from the precursor 1153 of graphene oxide. It is not only because reduction of graphene oxide is 1154 a well-established protocol for preparation of graphene layers, but also 1155 because structure defects in bulk and facile replacement of oxygen by 1156 other heteroatoms can be realized, considering the fact that no report 1157 on the treatment of heteroatom sources (e.g. NH₃ or urea) with pristine 1158 graphene can be found.

In contrast, heteroatom-doped CNTs are commonly produced according to the following methods. (i) In situ CVD growth of N-CNTs. 1161 It has been widely employed to grow CNTs on transition metal particles (catalysts) using a chemical vapor deposition method and a precursor containing C such as acetylene, ethylene, and methane. As such an N-doped CNT catalyst can be easily produced with a precursor 1165

Table V. Novel net	eroatom-uopeu graphene base	u metal-mee electrocatalysis	IOI OKK III aikainie incula.		
Material	Content of doped elements	Preparation method	Morphology	Novelty/merits	Ref.
N-doped graphene	Typical atomic content, 3.5%	A silica templating approach, growing silica on GO, coating of polydopamine, pyrolysis and removal of template	Nanosheet	Uniform and tunable mesoporous structure; More positive onset potential and $E_{1/2}$ than Pt/C; Long term stability	309
N-doped rGO	At.% = 1.81 - 2.82%	A thermal annealing approach, pyrolysis of the mixture of GO and urea under N ₂	Crumpled sheets	A 2-electron transfer pathway is dominant	290
N-doped graphene	At. $\% = 8.59 - 20.59\%$	Pyrolysis of the mixture of GO and urea under Ar	Three-dimensional stacked structures	The NG700 showed better ORR performance than others treated at lower temperature	456
N-doped graphene	At.% = 6.8 - 6.9%	Hydrothermal reduction of GO and urea, annealing at 600°C	Graphene sheet structure	Selectivity for ORR was improved after annealing	293
N-doped graphene	3.27-15.28 wt.%	Wet-chemical approach with GO and 2,3-diaminopyridine	Nanoplatelets	Higher stability than Pt/C	457
	At. $\% = 4 - 12\%$	Thermal annealing with a mixture of cyanamide and GO	Crumpled slate-like	Stable methanol crossover effect, high current density and durability	458
N-doped graphene	At. $\% = 2 - 3\%$	One step pyrolysis method with a GO-ppy composite	3D porous structure	A predominant four-electron ORR; Superior stability and tolerance to crossover effect than Pt/C	292
	6.24 - 8.55%	One step pyrolysis method with a GO-melamine composite	Micron-sized flake	Optimized pyrolysis temperature is 900°C	294
N-doped carbon nanosheet	At.% = 2.91 - 3.89%	Pyrolysis of chitosan and urea	Crumpled-sheet	Large BET surface area of $\sim 1510 \text{ m}^2 \text{ g}^{-1}$; The onset potential is only 18 mV less positive than that of Pt/C; Higher stability and tolerance to MeOH than Pt/C	313
	At.% = 3.02 - 11.2%	Pyrolysis of crystal sugar and urea	Entangled and crumpled morphology	Large BET surface area of 565.1 m ² g ⁻¹ for NG1000; Higher kinetic current density than Pt/C	459
	1.55 wt. %	Pyrolysis of folic acid	Porous	BET surface area is 1358 m^2 g ⁻¹ ; Similar limiting current density with Pt/C; Higher stability and tolerance to MeOH than Pt/C	460
N-doped carbon nanoribbon	4.1–8.3 wt. %	Pyrolysis of graphene nanoribbons (GNR)/polyaniline (PANI) compo-Sites	Nanoribbon	Carbon nanoribbon was prepared from unzipping CNTs; Four-electron transfer process	461
N-Doped graphene quantum dots/graphene	At.% = 4.3%	An electrochemical method for preparation of N-GQDs, followed by a hydrothermal treatment for preparation of N-GODs/graphene	-	Comparable activity to Pt/C	462
N-doped graphene; N,S-codoped graphene	-	An organic condensation method using 1,2-diaminobenzene as the N source and 2-aminothiophenol as the source of N and S	Edge-rich	Lack of π-π stacking; SNG exhibits a higher catalytic activity than NG	463
B-doped graphene	At.% = 3.2%	Annealing of GO and B_2O_3	Flake-like structure	On-set potential is 100 mV	336
	At.% = $0.57 - 1.92\%$	Annealing of GO and boric acid	Lamella structure	The BG700 showed better ORR performance than others treated at lower temperature.	456
S-doped graphene	S level: 1.30%–1.53%	Annealing of GO and benzyl disulfide	Sheets with wrinkled and folded features	Catalytic activity of S-graphene-1050 is better than Pt/C; J_k value is 9.34 mA/ cm ⁻² at -0.30 V (vs.	464

Ag/AgCl)

able '	V.	Novel	hetero	atom-o	loped	graphene	based	"metal-free"	' electrocata	alysts for	: ORR i	n alkaline	media
						-							

Material	Content of doped elements	Preparation method	Morphology	Novelty/merits	Ref.
Carbon black/S-doped graphene	_	Annealing of GO, sodium polysulfide and carbon black	Highly developed porous structure	Higher exchange current density than Pt/C	465
I-doped graphene	-	Annealing of GO and iodine	A wrinkled and voile-like feature	Catalytic activity of I-graphene-900 w is better than Pt/C; J _k value is 9.21 mA/ cm ⁻² at -0.30 V (vs. Ag/AgCl)	466
N/B co-doped graphene	6.80% of N and $4.82%$ of S	Annealing the mixture of H ₃ BO ₃ and NG	Slice-like	Onset potential of BNG was -0.17 V (vs. Ag/AgCl)	467
N/B co-doped graphene	2.5 at.% of B; 3.4 at.% of N;	Doping B with BH ₃ and GO followed by doping N with hydrazine	Nano-platelets	No annealing process; The number of electrons transferred is 3.86	308
N/B co-doped graphene	5.4% B and 5.3% N	Annealing with a GO-CBP composite	2D morphology	$E_{1/2} = -0.27 V$ (vs. Ag/AgCl)	468
N/B co-doped carbon nanosheet	$\sim 5.64 - 13.07$ at.% N and 1.23 - 7.76 at.% B	Annealing with a mixture of urea-PEG-boric acid	A crumpled, cross-linked thin film	J_k value, BCN-2.5-1000: 26.62 mA cm ⁻²	469
N/B co-doped Graphene Quantum Dots / Graphene Hybrid	~18.3 at. % nitrogen and ~13.6 at. % boron	Annealing of GQD/GO and boric acid under NH ₃ /Ar	Flake-like	~15 mV more positive onset potential than Pt/C	470
N/S co-doped graphene	2.12% of N and 1.70% of S	Annealing with a Cys-PDA-rGO composite	Porous 3D network	No evident restacking of graphene sheets; higher ORR activity than NG	305
N/S co-doped graphene	0.89–1.25% of N, 0.17–0.34% of S	Pyrolyzing GO and poly[3-amino-5-mercapto- 1,2,4-triazole] composite (PAMTa)	Wrinkled structure	$E_{1/2}$ is comparable with Pt/C	306
SN-rGO	Atomic ratio: $N/C = 0.12$; S/C = 0.08	Reflux reaction with thiourea and GO	Wrinkled single sheet	No annealing treatment; onset potential on SN-rGO is very close to that of the Pt/C	296

Table V. Novel heteroatom-doped graphene based	l "metal-free"	' electrocatalysts for	ORR in alkaline media.
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containing both C and N. For example, Li et al.³¹⁴ prepared N-CNTs 1166 using ethanediamine as a precursor and conducted heat treatment 1167 at different temperatures. Interestingly, the N-CNTs sample (800°C) 1168 with the highest content of pyridinic N shows the best catalytic activ-1169 ity for ORR (approaching Pt/C). In sharp contrast, the N-CNTs sam-1170 ple (900°C) with the highest content of quaternary/graphitic N gives 1171 the worst performance. (ii) Post doping of N (or other elements) on 1172 CNTs. After pretreatment of CNTs with concentrated H₂SO₄/HNO₃, 1173 N-doped CNTs were prepared by heat treating oxidized CNTs and 1174 tripyrrolyl[1,3,5]triazine at different temperatures.³¹⁵ As opposed to 1175 the findings by Li et al.,³¹⁴ as-prepared NCNT-900 with the high-1176 est graphitic-N content exhibits the highest kinetic current density 1177 for ORR in 0.1 M KOH. In addition, the NCNT-1000 sample with 1178 a total N content of 0.70 at.% (vs. 2.40% for NCNT-900) shows 1179 a *n* value of 3.1 for ORR, indicating that the active sites for com-1180

plete oxygen reduction are not sufficient after annealing at 1000°C. ¹¹⁸¹ Other examples using alterative N precursors such as ammonia,³¹⁶ ¹¹⁸² polymers,³¹⁷ triazole and tetrazole derivatives,³¹⁸ cyanamide,³¹⁹ dual ¹¹⁸³ nitrogen sources,³²⁰ and other heteroatom resources for B³²¹ and S³²² ¹¹⁸⁴ can be found in the literature. (iii) Surface decoration of N. Giambastiani et al.^{323,324} functionalized MWCNTs with different N-containing ¹¹⁸⁶ heterocycles under mild conditions (see Figure 21a). Because the ¹¹⁸⁷ CNTs surface was solely functionalized by pyridinic moieties, it is ¹¹⁸⁸ possible to study the effect of electronic properties of the heterocycle ¹¹⁸⁹ on the kinetics of ORR. It was found that polarization values of the ¹¹⁹⁰ N-C_α bond shown in the Figure 21b must be located in a range of ¹¹⁹¹ 4.0–4.5 in order to trigger complete oxygen reduction paths. ¹¹⁹²

Aside from the existing recognition that the catalytic activity of 1193 ORR on CNTs can be enhanced by doping heteroatoms into the basal 1194 or edge plane, a recent work has shown that surface modification to 1195



Figure 20. (a) SEM images of Nitrogen-Doped Carbon Nanosheets (NCN). Reprinted with permission from Ref. 313 Copyright 2014 American Chemical Society. (b) LSV curves of carbonized chitosan (CC), NCN, and Pt/C electrodes in O_2 -saturated 0.1 M KOH at a scan rate of 5 mVs⁻¹ and a rotational rate of 1600 rpm. Reprinted with permission from Ref. 313 Copyright 2014 American Chemical Society.



Figure 21. (a) MWCNT N-Decoration via Aryldiazonium Salt (Tour) Protocol. Reprinted with permission from Ref. 323 Copyright 2014 American Chemical Society. (b) N-Containing Heterocycles Used for the MWCNT Decoration. Reprinted with permission from Ref. 323 Copyright 2014 American Chemical Society.

generate C-O groups may also help to improve the ORR performance 1197 significantly. Dumitru et al.³²⁵ treated CNTs with citric acid, diazo- 1198 nium salts and peroxymonosulfuric acid separately and conducted 1199 heat treatment at moderate temperature (up to 450°C) in some cases. 1200 Though not obvious from Figures 22a and 22b, an increase of the 1201 signal of COO on citric acid treated CNTs and C-O (or hydroxyl) 1202 on peroxymonosulfuric acid treated CNTs, and the presence of the 1203 4-nitrophenyl group on diazonium salts treated CNTs can be found 1204 based on deconvolution calculations (Figure 22c). From the K-L plots 1205 in Figure 22d, the C-O (or hydroxyl) enriched sample shows a four- 1206 electron pathway for ORR, whereas others show only a dominate 1207 two-electron pathway. It is very interesting to explore the special role 1208 of the surface C-O (or hydroxyl) function on the improvement of ORR 1209 selectivity and activity, given that non-specific adsorbed OH- on any 1210 electrode surface is quite abundant and responsible for promotion of 1211 mediated outer-sphere electron transfer for ORR.¹ 1212 Other types of carbon materials.—Apart from the heteroatom doped 1213 or surface functionalized graphene and carbon nanotubes as metal-free 1214 ORR electrocatalysts, numerous and miscellaneous carbon materials 1215 such as carbon fiber, mesoporous carbon, graphyne and graphdiyne, 1216 aerogels, nanoparticles, quantum dots, and others with special mor- 1217 phology or structure have been reported. Nevertheless, a general strat- 1218 egy to change the pristinely inefficient (2-electron transfer for ORR) 1219 into efficient (4-electron transfer) electrocatalysts for ORR is still fo- 1220 cused on doping heteroatoms, creating structural defects, and surface 1221 functionalization, given that there remain inconsistent results con- 1222 cerning the active sites, role of heteroatoms and their content under 1223 different preparation conditions.

Other than the typical examples about preparation methods, structure, ORR kinetics performance, etc. summarized in Table VI, some 1226



Figure 22. (a) C1s core level spectra of unmodified and modified CNTs. Reprinted with permission from Ref. 325 Copyright 2014 Elsevier. (b) O1s core level spectra of unmodified and modified CNTs. Reprinted with permission from Ref. 325 Copyright 2014 Elsevier. (c) Deconvolution of C1s core level spectra of CNT0. Reprinted with permission from Ref. 325 Copyright 2014 Elsevier. (d) K-L plot for unmodified and modified carbon nanotubes at -0.6 V. Reprinted with permission from Ref. 325 Copyright 2014 Elsevier.

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Material	Content of doped elements	Preparation method	Structure/Morphology	Surface area	Novelty/Merits	Ref.
N-doped carbon fiber	1.3%–3.4 at.% of N	Carbonizing the electronspun polyacrylonitrile carbon fiber at 1000°C, followed by acidification and NH ₃ etching	Fiber	-	Improvement of wettability, diameter reduction, highly porous structure, more exposed edge planes, and higher proportion of pyridinic-N by post origification and NH, atching	471
	31.6–44.1 at.% of pyrrolic-N content	Thermal treatment of electronspun polyacrylonitrile carbon fiber under NH ₃	Fiber	_	The NCNFs sample with the best catalytic activity for ORR has the highest content of pyrrolic-N	472
N-doped mesoporous carbons	_	Carbonizing a composite of honey- SBA-15 at different temperature	Mesopores with short rod-like microstructures	1059 – 1273 m²/g	The best catalyst of N-OMCs-800 has the highest pyridinic N and graphitic N content and the largest surface area.	473
N-doped mesoporous carbons	-	Pyrolyzing polymerized ethylenediamine nanocasted into a SBA-15 hard template	Mesoporous structure with a hexagonal porous network	473–517 m ² /g	Higher j_k value than Pt/C	474
B-doped mesoporous carbons	1.30 at.% of B	Carbonization of sucrose and 4-hydroxyphenylboronic acid into SBA-15 silica template	Rod-like morphology	778–1040 m ² /g	It needs to reach a balance between B content and surface area.	475
N-doped graphdiyne	3.04 – 3.35 at.% of N	Cross-coupling reaction, followed by heating under ammonia/Ar	Loose, spongy structure	-	N-doping leads to high positive charges on the carbon atoms	476
N/S codoped carbon aerogels	5 wt.% of N; 1 wt.% - 4 wt.% of S	Hydrothermal synthesis, followed by pyrolysis	Homogeneous interconnected particle matrix	224.5–266.7 m ² g ⁻¹	Synergistic effect of co-doped sulfur- and nitrogen	477
N doped graphene nanoribbons aerogel	2.8 at.% of N	Unzipping of CNTs, hydrothermal treatment, annealing	Interconnected, porous structure with hierarchical pores	$617 \text{ m}^2 \text{ g}^{-1}$	Superb electrocatalytic activity and better stability than commercial Pt/C	478
N doped carbon nanoparticle	0.39–0.58 at.% of N	A solution plasma process	Turbostratic structure	-	In situ nitrogen doping	479
N doped carbon nanoball	0.23–0.49 at.% of N	A solution plasma process, followed by annealing	Ball-shaped structure	-	ORR activity can be improved by thermal annealing	480
N/P doped carbon foams	-	Copyrolyzing of poly(vinyl alcohol)/polystyrene (PVA/PS) hydrogel composites	Hierarchical interconnected macroporous structure	$1083 \text{ m}^2 \text{ g}^{-1}$	First report on N and P dual-doped hierarchical porous carbon foams for ORR	339
N doped carbon spheres	0–1.58% of N	Pyrolysis of hollow poly(o-phenylenediamine) spheres	Hollow microspheres	_	Higher activity than MWCNTs or NCNTs	481
N doped carbon spheres	2.35 – 4.82 wt.% of N	Carbonizing a MV/HMS composite, following by removal of silica	Hierarchically micro-meso- macroporous structure	$1413 \text{ m}^2 \text{ g}^{-1}$	Higher J_k value than Pt/C	482
N/S doped carbon nanospheres	4.25–9.52 wt.% of S; Up to 74.7 at.% of N	Pyrolysis of a mixture of polyacrylonitrile nanospheres and S	Nanospheres	$653 \text{ m}^2 \text{ g}^{-1}$	Sulfur helps to improve the ORR activity	483
N-doped carbon hemispheres	10.9 wt.% of N	IL coating on silica, followed by removal of silica and annealing	Honeycomb-like	$65.1 \text{ m}^2 \text{ g}^{-1}$	Ionic liquids were used as the carbon source	484
Sulfur-containing	1.0-3.4 at % of S	Flame synthesis	Disordered,	_	The first report using flame	485
(N, P, and B)-codoped nanocarbons	-	Pyrolysis of a mixture of urea, phosphoric acid and boracic acid	Nanoporous morphology	$89.5 \text{ m}^2 \cdot \text{g}^{-1}$	ORR activity is higher than single- or dual-doped nanocarbons	486
N doped carbon	3.15 at.% of N	Polymerization of <i>o</i> PD using a hard template of silica colloid, followed by pyrolysis, removal of silica	Hierarchical porous structure	$1280 \text{ m}^2 \text{ g}^{-1}$	Highest ORR activity among metal-free catalysts	487

and activation by NH₃

Table VI. Recently developed metal-free carbon electrocatalysts other than graphene or carbon nanotubes for ORR in alkaline media.



Figure 23. a) Micro apparatus for the ORR electrochemical experiment. b) Optical photograph of the HOPG as the working electrode with the air-saturated droplet deposited on the edge of the HOPG. c) The air saturated droplet was deposited on the basal plane of the HOPG electrode. d) LSV curves of the ORR tested for a droplet located either on the edge (as shown in Figure 23b) or on the basal plane (as shown in Figure 23c) of the HOPG. Reprinted with permission from Ref. 341 Copyright 2014 Wiley-VCH

new fundamental findings need to be emphasized in the following. 1227 1228 It is generally accepted that the charge neutrality of pristine carbon materials can be changed by doping or surface modification with more 1229 electronegative elements like F^{330, 331}, N^{332, 333}, O^{286, 334}, electroneg-ativity similar elements like S^{123, 335} or less electronegative elements 1230 1231 like B^{336, 337}, P^{338, 339}, endowing a shift of the Fermi level, availability 1232 of active sites, and improvement of ORR towards the 4e⁻ pathway. 1233 In addition, ORR can be significantly benefited by an increase of 1234 surface area and porosity of carbonaceous electrocatalysts. For ex-1235 ample. P doped ordered mesoporous carbon with different lengths 1236 and thicknesses were prepared by pyrolyzing of triphenylphosphine 1237 (P source) and phenol (C source) using SBA-15 templates with dif-1238 ferent rod lengths. The POMC-3 sample with the shortest channel 1239 length exhibits the largest surface area of 1182 m² g⁻¹ and pore vol-1240 ume of $1.87 \text{ cm}^3 \text{ g}^{-1}$, leading to an increase in activity for ORR in 1241 0.1 M KOH.3 1242

In addition to the changes by dopants, the carbon materials them-1243 selves may exhibit structural effects on ORR activity. With an elec-1244 trochemical micromanipulator-microinjection system in Figure 23a, 1245 air-saturated 1 M KOH micro-droplets were deposited either on the 1246 edge (Figure 23b) or on the basal plane (Figure 23c) of HOPG. From 1247 the LSV curves in Figure 23d, the edge is more active than the basal 1248 plane for ORR, which is an important guideline for design of better 1249 metal-free carbon based ORR electrocatalysts. Indeed, the graphite 1250 sample prepared by ball-milling with more edges exposed shows 1251 much enhanced electrocatalytic activity and selectivity than the pris-1252 tine graphite.³⁴¹ It is true that carbon in its elementary substance form 1253 is the most attractive kind of material to be used as metal-free electro-1254 catalyst for ORR. Besides that, the development of conducting poly-1255 mer based electrocatalysts cannot be ignored due to their unique prop-1256 erties and promising performance for ORR in alkaline media.^{342,343} 1257 Kerr et al.³⁴³ prepared two poly(3,4-ethylenedioxythiophene) (PE-1258 DOT) samples using a vapor-phase polymerization and an electrode-1259 position method. Although the PEDOT samples prepared by both 1260

methods have similar structure, it is surprising to observe that ORR 1261 undergoes a transition from a 2-electron process to a 4-electron 'series' on vapor-phase polymerized PEDOT, whereas it proceeds via a 1263 2-electron pathway on electrodeposited PEDOT. 1264

Composites and natural resourced carbon materials.—Outstanding 1265 intrinsic ORR activity has been observed on the aforementioned 1266 carbon materials. However, some of them may suffer from practi-1267 cal problems when being used as electrodes for ORR. For instance, 1268 heteroatom-doped graphene materials showing high ORR catalytic 1269 activity have a common limitation of re-stacking of layers by $\pi - \pi$ 1270 interactions and vander Waals forces.^{231,344} The electrode surface area 1271 may drop dramatically when a high loading is needed, which will 1272 cause a significant decrease of current density for ORR. One strategy 1273 to overcome this problem is to incorporate carbon nanotubes as a 1274 spacer into graphene layers and form a composite so that restacking 1275 of graphene can be avoided. Ratso et al.³⁴⁴ pyrolyzed a mixture of GO 1276 and MWCNTs at 800°C for 2 h using urea or DCDA as the N source 1277 for doping. As-synthesized electrocatalysts showed remarkable elec- 1278 trocatalytic activity that is close to a commercial Pt/C as well as good 1279 long-term stability. 1280

In another example, Young et al.³⁴⁵ synthesized a core-sheath ¹²⁸¹ structured CNT/N-carbon composite by pyrolysis of a monolithic ¹²⁸² CNT-ionic liquid-silica composite and subsequent removal of silica ¹²⁸³ by HF. From RDE and alkaline fuel cell testing, the nanocomposite ¹²⁸⁴ catalyst displayed one of the best performances among metal-free ¹²⁸⁵ electrocatalysts for ORR. Unfortunately, the comparison of CNT/Ncarbon composite and N-carbon prepared under similar conditions ¹²⁸⁷ is missing, which makes the role of CNT in this composite sample ¹²⁸⁸ unclear. Additionally, (N and S) doped mesoporous carbon/graphene ¹²⁹⁹ composites were prepared by calcining mesoporous silica/graphene ¹²⁹⁰ composites in the presence of different types of amino acids as heteroatoms sources.³⁴⁶ In this case, mesoporous carbon was formed ¹²⁹² on graphene sheets as shown in Figure 24. As-prepared single ¹²⁹³ doped and dual doped composite catalysts exhibited similarly high ¹²⁹⁴



Figure 24. The synthesis procedure of Heteroatom doped mesoporous carbon/graphene nanosheets (HMCGs) (a) self-assembly of mesoporous TEOS on GO, (b) removal of CTAB and (c) nanocasting approach of each amino acid. Reprinted with permission from Ref. 346 Copyright 2014 Elsevier.

¹²⁹⁵ electrocatalytic activity and kinetics for ORR and superior durability ¹²⁹⁶ as compared to Pt/C.

From the perspective of environmental protection, it would be desirable to prepare metal-free carbon based electrocatalysts using some earth-abundant materials or even waste materials. Chen et al.³⁴⁷ prepared N doped carbon nanosheets by a two-step hydrothermal reaction and pyrolysis process (under NH_3) using typha orientalis as 1301 the only starting material. The sample heat treated at 800°C shows a 1302 3D interpenetrated network structure (see Figures 25a and 25b), and 1303 similar catalytic activity but higher durability than Pt/C (Figures 25c 1304 and 25d). Various carbon materials based electrocatalysts with different stuctures and dopants have been also prepared by pyrolysis of 1306 Escherichia coli,³⁴⁸ natural seaweed,³⁴⁹ water hyacinth,³⁵⁰ gelatin,³⁵¹ 1307 and protein-rich pulse flour,³⁵² etc. 1308

Practical Considerations

The transplantation speed for cathodic electrocatalysts into real 1310 AAEMFCs falls far behind that for development of novel materials, 1311 as evidenced by the extremely scarce reports about real alkaline fuel 1312 cell testing. This may be partially due to the unsatisfactory overall 1313 cell performance caused by the intrinsic limited properties of anion 1314 exchange membranes.^{353,354} On the other hand, more attention has to 1315 be paid to some remaining electrocatalysis issues. Rotating ring disk 1316 electrode (RRDE) measurements have become a routine way to eval- 1317 uate and compare the catalytic activity of ORR electrocatalysts along 1318 with their function as the tool to study ORR kinetics without the effect 1319 of solution diffusion limitations. However, a very important but of- 1320 ten omitted difference between RRDE measurement and AAEM fuel 1321 cell testing is the effective contact with the electrolyte. In the case of 1322 RRDE, an electrode covered or modified with anodic electrocatalysts 1323 is usually fully immersed in the alkaline electrolyte (typically 0.1 M 1324 KOH). This creates a big advantage of almost complete utilization of 1325 the active sites by wetting the electrode with liquid electrolyte solu- 1326 tion that is saturated by O₂. In a sharp contrast, a solid-phase anion 1327



Figure 25. (a) The SEM image of Nitrogen-doped nanoporous carbon nanosheets (NCS-800). Reprinted with permission from Ref. 347 Copyright 2014 Royal Society of Chemistry. (b) The STEM image of NCS-800. Reprinted with permission from Ref. 347 Copyright 2014 Royal Society of Chemistry. (c) RDE voltammograms in O₂-saturated 0.1 M KOH solution at room temperature (rotation speed 1600 rpm, sweep rate 20 mV s⁻¹) for NCS-800, CS-800 and Pt/C. Reprinted with permission from Ref. 347 Copyright 2014 Royal Society of Chemistry. (d) Current–time (i–t) chronoamperometric response of NCS-800 and Pt/C electrodes at 0.10 V (vs. RHE) in O₂-saturated 0.1 M KOH solution at a rotation rate of 800 rpm. Reprinted with permission from 347 Copyright 2014 Royal Society of Chemistry.

1309



Figure 26. Schematic illustration of (a) an AAEMFC, (b) the three phase boundary in the anode and (c) the three phase boundary in the cathode. Reprinted with permission from Ref. 361 Copyright 2014 Elsevier.

1328 exchange membrane is used as both OH⁻ conductor and electrode1329 separator in an AAEMFC.

1330 Current anion exchange membranes are typically composed of 1331 polymer backbones with hydrophobic side chains terminated with quaternary ammonium groups. Upon adsorption of water, ionic clus-1332 ters and ionic channels can be formed inside the bulk membrane and 1333 the surface by proper alignment of the hydrophilic quaternary am-1334 monium groups.^{355–357} It has been shown that good electrochemical 1335 performance of a composite electrode cannot be obtained unless there 1336 is direct contact between catalyst and ionic channels in the solid mem-1337 brane electrolyte for facile reactions and mass transport.^{354,358,359} It is 1338 not difficult to imagine that only the top surface of the catalyst layer 1339 with direct contract to ionic channels of the membrane can be utilized 1340 no matter whether the catalyst layer is prepared by depositing cata-1341 lyst materials on a gas diffusion layer (e.g. carbon cloth) or spraying 1342 them directly on the membrane. It is the blending of liquid ionomer 1343 in the catalyst layer with the membrane material that dramatically 1344 helps to extend the reaction zone deep into the catalyst layer.³⁶⁰ From 1345 Figure 26, a three-phase boundary can be formed inside the catalyst 1346 layer and the transport of electrons, hydroxide ions, and molecular 1347 oxygen can be significantly promoted, resulting in significant en-1348 hancement of the ORR kinetics. For example, the highest peak power 1349 density of 358 mW cm⁻² was achieved with a 20 wt.% ionomer con-1350 tent in the catalyst layers in AAEMFC tests by minimizing the active, 1351 ohmic and mass diffusion polarization losses.³⁶¹ In addition, the ORR 1352 pathway on silver nanowire catalysts may be shifted towards the 4e-1353 mechanism by increasing the ionomer content during preparation of 1354 the catalyst ink.³⁶² Even so, considering the very limited conductivity 1355 of current ionomers and electrode architectures, the thickness of the 1356 electrodes (especially the cathode) plays a critical role in the overall 1357 performance of an AAEMFC. 1358

During the operation of a real AAEMFC mass-transport limitations and cooperative issues inside the catalyst layer have to be addressed in order to increase the utilization rate of electrocatalysts. On this perspective some experimental and modeling work in acidic media can be used as reference for future investigation of similar problems in al-



Figure 27. GDE-example of an oxygen cathode in alkaline media. Reprinted with permission from Ref. 370 Copyright 2002 Elsevier.

kaline media.^{363–365} Durand et al.^{366,367} studied kinetic parameters and 1364 the mechanism of ORR inside Nafion using RDE and electrochemi- 1365 cal impedance spectroscopy (EIS). Not only the diffusion limitation 1366 in aqueous electrolyte but also the diffusion limitation in the active 1367 layer was fully considered to obtain the electrode kinetic parame- 1368 ters. In practice, the diffusion in aqueous electrolyte was corrected 1369 by RDE with a Levich plot.³⁶⁷ On the other hand a homogeneous 1370 flooded model³⁶⁷⁻³⁷⁰ was employed to correct for diffusion limita- 1371 tions in the active layer assuming that the mass transport in the gas 1372 layer is fast enough. From the dc and ac experiments it was found 1373 that an "ECE-Damjanovic" mechanism is valid on Pt nanoparticles 1374 inside the Nafion, and a direct four-electron transfer mechanism was 1375 confirmed. Durand et al.^{369,370} further studied the diffusion, ohmic, 1376 spatial discrete distribution drop and other effects in a gas diffusion 1377 electrode (GDE, illustrated in Figure 27) that is the most important 1378 component for catalysis in all kinds of fuel cells. From Figure 27, 1379 the catalyst active layer of a GDE is made of catalyst nanoparticles, 1380 PTFE binder and Nafion ionomer in the voids. It is reasonable to infer 1381 that the thinner active layer leads to better ORR performance because 1382 ORR takes place only on the catalytically active sites having contact 1383 with both the carbon and electrolyte phases, and the gas (oxygen) 1384 diffusion resistance and ohmic drop are smaller. Using a modified 1385 flooded homogeneous model and EIS analysis, it was concluded that 1386 the restricted diffusion behavior for a GDE is not completely induced 1387 by the concentration gradient within the active layer.³ 1388

For the state-of-the-art Pt/C catalysts, the catalyst laver thickness 1389 of a 30% Pt/C is about 10 µm with a loading of 0.5 mgPt/cm².³⁷¹ 1390 However, for the non-precious metal catalysts prepared by pyrolysis 1391 of metal macrocycle compounds, the "active" transition metal load- 1392 ing in the form of metal-N_x instead of metallic form is usually lower 1393 than 3%. In order to increase the number of active sites and abso-1394 lute current value, a strategy of increasing the catalyst loading is 1395 always pursued. 192,235,238,372 As a result, a catalyst layer thickness of 1396 \sim 50–100 μ m will easily be reached, which makes the volumetric current density 125–1000 times lower than that of a Pt/C electrode under 1398 the best scenario of equal current. Unfortunately, the absolute current 1399 will be decreased dramatically with significant mass transport issues 1400 within the catalyst layer even with the best ionomer and electrode ar- 1401 chitectures to date. 356 Consequently, in general, an electrocatalyst with 1402 excellent ORR performance during RRDE measurements is promising 1403 but may not be qualified to be used in AAEMFCs.³⁷³ New approaches 1404 are needed for changing the microstructure of electrodes that are made 1405 of electrocatalysts of lower active-site density than Pt. 1406

Recently, there have been some pioneering attempts to test and 1407 study the ORR performance of cathodic electrocatalysts in AAEM-FCs. He et al.²¹⁷ fabricated AAEMFCs with an A201 Tokuyama anion exchange membrane and either a commercial Pt/C catalyst or 1410 a high metal loading (24.7 wt.%) CoO/rGO(N) non-precious metal catalyst as the cathode. The large metal loading of CoO endows increased active sites of CoO strongly coupled with pyridinic nitrogens in rGO(N) and reduced thickness of the catalyst layer. The cell voltage-current polarization curves shown in Figure 28 were obtained with a CoO/rGO(N) cathode of 7.8 μ m and a Pt/C cathode of 6.0 μ m. With a comparable thickness of catalyst layer, the power density on CoO/rGO(N) catalyst is closely approaching that of the Pt catalysts at practical voltages (e.g. 0.6 V).



Figure 28. Performance of anion-exchange-membrane fuel cells using identical Pt/C anodes with Pt/C (square symbols) and CoO/rGO(N) cathodes (circle symbols) tested at $60^{\circ}C$ with H_2 (at 1 atm, 57% RH) feed at the anode and O_2 (at 1 atm, 100% RH) at the cathode. The cell voltage–current polarization curves (filled symbols) on the left axis and the power current curves (open symbols) on the right axis. Reprinted with permission from Ref. 217 Copyright 2013 American Chemical Society.

In line with the preparation of the cathode in He et al.'s report, an 1420 OH- type ionomer was added into the N-CNTs and Pt/C catalyst ink 1421 to make gas diffusion electrodes.³¹⁷ Without the reporting of catalyst 1422 layer thickness, the metal-free N-CNTs cathode shows a maximum 1423 power density of 37 mW/cm² as compared to that of 62 mW/cm² on 1424 Pt/C, and good stability over 30 h under fuel cell operating conditions. 1425 A better result that approaches the power density of transition metal 1426 based catalysts²¹⁷ was achieved by spraying CNTs/HDC catalysts with 1427 1428 ionomer directly onto pore-filling anion conducting membranes.34 1429 During the preparation of a cathode for an AAEM single cell, the catalyst powder is usually mixed with ionomer in a volatile organic solvent 1430 and sprayed or coated onto carbon paper/cloth or membranes.³⁷⁴ Al-1431 ternatively, in a recent work, the PdNi/C catalyst ink with the binder of 1432 PTFE was sprayed onto GDLs and post-treated with poly(vinybenzyl 1433 1434 chloride) which is the backbone of the anion exchange membrane.³ 1435 As-prepared gas diffusion electrodes were submerged in undiluted N,N,N',N'-tetramethylhexane-1,6-diamine for 24 h and KOH solu-1436 tion for 1h before fuel cell testing. With a catalyst loading of 0.4 mg 1437 cm⁻², the PdNi/C electrode showed a 1.7 times higher power den-1438 sity at 0.4 V than that of a commercial Pt/C electrode. For further 1439 improvement of the cell performance, a few constructive suggestions 1440 such as maximization of active sites of electrocatalysts, minimization 1441 of thickness of the AAEM, and optimization of fuel cell conditions 1442 were proposed.3 1443

It is beyond the scope of this paper to introduce the status of 1444 development of anion exchange membranes and some engineering 1445 issues about AAEMFCs, and readers are referred to some more rele-1446 vant reviews published recently.5,353 However, some forward-looking 1447 work has to be specially emphasized here for smoother and faster 1448 implementation of various promising electrocatalysts materials into 1449 real AAEMFC applications. It has been pointed out that the degra-1450 dation of head groups of AAEM in quaternary ammonium types or 1451 imidazolium-types can occur under strong basic conditions over a long 1452 period of time.^{4,376–379} To study the influence of these mobile cationic 1453 head groups on the ORR performance of electrocatalysts, Ong et al.³⁷⁹ 1454 added 1 mM of different quaternary ammonium-, imidazolium-, and 1455 DABCO-based cationic groups in 1 M KOH and measured cyclic 1456 voltammetry in the absence of O_2 and hydrodynamic voltammetry in 1457 the presence of O₂ on a Pt disk RDE. It was found that the hindrance 1458 of ORR activity by cationic groups follows the same order as for 1459 the suppression of hydrogen adsorption and electrochemical surface 1460 1461 area of the Pt electrode. Considering the largest impact on ORR ki-



Figure 29. IL-TEM images after 0 (A, C, E) and after 3600 (B, D, F) degradation cycles. Green circles indicate agglomeration, the red circle shows a detached platinum particle, blue arrows point at platinum particles that decrease in size due to dissolution, and orange arrows emphasize massive changes in the support structure. Reprinted with permission from Ref. 380 Copyright 2012 American Chemical Society.

netics by imidazolium-based functional groups, it was believed that 1462 AAEMs containing these moieties may not be suitable for fuel cell 1463 applications. 1464

Another crucial aspect that must be considered for fuel cell op- 1465 eration is the stability of the electrocatalysts especially under the 1466 drastic operating conditions such as sudden change of potentials on 1467 the cathode. Therefore, it is necessary to investigate the degradation 1468 mechanism of cathode electrocalysts over a long period of time un- 1469 der extreme pH environments. To save time for assembling polymer 1470 electrode assemblies and testing in fuel cell systems, Meier et al.³⁸⁰ 1471 developed an "accelerated aging tests" protocol with a combination 1472 of an electrochemical half-cell and a technology of identical location 1473 transmission electron microscopy (IL-TEM). By means of precise 1474 identification of a specific area of a TEM gold grid coated with Pt/C 1475 electrocatalyst pre- and post-test cycles in acidic solutions, the degra- 1476 dation processes were monitored in an ex-situ manner (see Figure 29) 1477 and several different degradation pathways were observed. By chang- 1478 ing the electrolyte from acid to base, this advanced technique is highly 1479 applicable for evaluation and study of the stability of noble-metal, 1480 transition metal, and metal-free electrocatlysts materials quickly and 1481 reliably, devoid of the use of anion exchange membranes. By means 1482 of the same technique of IL-TEM, Zadick et al.³⁸¹ found that cu- 1483 bic Pd nanoparticles (NPs) turned into coalesced and near-spherical 1484 NPs after a hundred scans of CVs due to the intensive hydrogen 1485

1492

1486 insertion/desinsertion process and further electrooxidation on the Pd 1487 surface. In another report of Pt/C degradation in alkaline medium, a 1488 three-times faster degradation rate was measured as compared to the 1489 same material in acidic medium.³⁸² This was ascribed to a modifica-1490 tion of the carbon surface chemistry anchoring sites of the particles 1491 on the support in alkaline media.

Conclusions and Perspectives

Among many constraints on the overall alkaline anion exchange 1493 membrane fuel cells (AAEMFCs) performance, electrocatalysis and 1494 the sluggish oxygen reduction reaction (ORR) are especially promi-1495 nent. In spite of the disadvantages of cost and scarcity and numerous 1496 studies of replacement candidates (for decades) of Pt/C electrocata-1497 lysts for ORR, Pt/C is still the state-of-the-art and most practically 1498 used ORR electrocatalyst in the fuel cell industry and serves as the 1499 benchmark for evaluation of novel catalysts in the scientific commu-1500 nity. The lack of sufficient understanding of the details of the ORR 1501 processes in alkaline media makes the investigations focused on fun-1502 damental mechanisms especially valuable. The new inputs on ORR 1503 mechanisms summarized in this review help to unravel the complex 1504 interconnections and effects of such variables as surface structure, the 1505 shape of nanoparticles, and other factors like temperature and pressure 1506 and adsorption of OH⁻ anion and quaternary ammonium cations. 1507

The endeavor of searching for alternative materials to Pt-based 1508 catalysts for ORR in alkaline media has never stopped. Among the 1509 non-Pt noble metals, Pd and Ag based catalysts are two promising 1510 groups, showing comparable ORR activity with commercial Pt/C cat-1511 alysts. Progressive achievements have been made in recent years on 1512 preparing Pd and Ag nanoparticles with different shapes, facets and 1513 1514 sizes using novel synthesis routes, enhancing the metal-support interactions, development of novel catalysts in oxide forms, alloying 1515 with a broad range of noble or non-noble metals, etc. Nevertheless, 1516 the detailed and solid information on the intrinsic origin of dramatic 1517 enchantment of ORR activity and stability on Pd and Ag based elec-1518 1519 trocatalysts as pH increases is unavailable, which makes it difficult 1520 to conduct a bottom-up strategy for the design of novel catalysts of these families. Some in situ electrochemical spectroscopy investiga-1521 tions and fuel cell testing are required to accelerate the process of 1522 utilizing these materials in practical applications. In contrast to the 1523 large number of reports of Pd and Ag based cathode catalysts, it is 1524 much less common to see studies on other non-Pt noble metals such 1525 Au, Ru and Ir. However, an important discovery of an AuCu₃ alloy¹¹⁸ 1526 showing higher mass activity than Pt has opened the gate of design-1527 ing novel active ORR electrocatalysts with combinations of elements 1528 having strong and weak affinity for oxygen. 1529

Inspired by the natural capability of organometallic compounds for 1530 ORR, tremendous efforts have been devoted to searching and studying 1531 an important class of non-precious metal electrocatalysts with central 1532 transition metal ions coordinated with nitrogen functionalities. Some 1533 general viewpoints, consensus and controversies are summarized here. 1534 First of all, for metal-N_x-C electrocatalysts prepared by pyrolysis of 1535 metal macrocycles or metal salts with N precursors and carbon sup-1536 ports, it is reasonable to assign the metal-Nx moieties anchored on 1537 some graphitic defects or inter-plane regions of the carbon support 1538 as the active sites for ORR. Secondly, it is generally assumed that 1539 an optimal pyrolysis temperature exists for achievement of covalent 1540 bonds and avoiding the formation of metallic particles. In addition, 1541 to obtain catalytically active and stable metal-N_x/C electrocatalysts, 1542 the heat treatment atmosphere, metal and N precursors and follow-1543 up acid leaching procedures all matter to some but less extent, given 1544 enough specific cavities on carbon. Thirdly, aside from high temper-1545 ature heat treatment, some intriguing work has been done to prepare 1546 functionalized mesoporous and two-dimensional carbon (e.g. CNTs 1547 and graphene) supported metal-Nx electrocatalysts via solvothemal or 1548 even reactions at room temperature. The obtained comparable ORR 1549 performance was attributed to the strong non-covalent π - π interaction 1550 between the active metal center and the carbon support, which is not 1551 1552 fully evidenced and deserve further attention and investigation.

Among other types of non-noble-metal electrocatlalysts for ORR 1553 in alkaline media, the first row transition metal oxides are the most 1554 important class of materials in view of their excellent activity, superior 1555 stability and feasibility of synthesis, etc. Unlike the confined coordi- 1556 nation in the metal-N_x/C, more freedom and merits can be given to 1557 form transition metal oxide catalysts. Firstly, the stoichiometric ratio 1558 of metal and oxygen can vary in a large range in that MO, MO2, 1559 M₂O₃, M₃O₄ and other compositions (or combination of different 1560 metal elements) can be seen in the literature. Secondly, by simple 1561 modification of precursor salts, concentration, pH, temperature of hy- 1562 drothermal and possible calcination reactions, etc. various designed 1563 shapes of metal oxides can be made, in which a prolonged morphol- 1564 ogy like nanowires or long belts generally shows better ORR kinetics. 1565 Thirdly, unlike most of the pyrolyzed metal-Nx/C electrocatlysts with 1566 very low effective metal loading limited by total defect sites of carbon 1567 supports, a much higher catalyst loading (up to ca. 20 wt.%) can be 1568 obtained for the carbon supported metal oxide catalysts, potentially 1569 leading to smaller ohmic resistance and facile mass transport and turn 1570 over frequency in a real AAEMFC.

Though less intensively reported, some transition metal chalcogenides, sulfur-doped non-noble-metal catalysts, transition metal carbides and nitrides/oxynitrides and perovskites have attracted more and more attentions due to promising ORR performance in alkaline media. From some recent reports on late transition metal chalcogenides composed of selenium and sulfur, variously structured nanoparticles or nanocomposites can be formed with a wet chemical method under mild temperatures. Only some hypothesis about structure-activity relation and possible synergetic effects between chalcogenides and carbon supports were proposed, which makes it urgently needed to do systematical studies on this class of materials with compositions, microstructures, surface chemistry, support, stability of electrode, intermediates of ORR and other variables fully considered.

In contrast to chalcogenides, better ORR kinetics was obtained on 1585 some sulfur-doped non-noble-metal catalysts. These materials were 1586 prepared by doping sulfur into carbon backbones with a pyrolysis 1587 process or forming thiospinels with a solvothermal method. The enhancement of ORR kinetics may be caused by improved porosity and conductivity by doping heteroatoms of sulfur into carbon backbones 1590 and altering of oxidation status of transition metals. However, there is some vague or missing information that needs clarification, including the coordination effect of metal and sulfur in the cases of doping sulfur into carbon support and the distinct roles of metal-S bonds in thiospinels as opposed to those in chalcogenides. 1590

Some transition metal carbides and nitride/oxynitride electrocatalysts have evolved recently with decent (comparable or even better than Pt/C) ORR performance and durability in the absence or presence of methanol in alkaline media. The catalysts of Fe_3C encapsulated in graphic layers or CNT walls have shown superior ORR kinetics to that of Pt/C and stability provided by the protective carbon layers, indicating that the metal carbide phases presumed as ORR inactive phases previously deserve urgent re-visit and thorough exploration. Transition metal carbides and nitrides/oxynitrides with metal elements from IVB to VIB groups have shown catalytic activity but incomplete oxygen reduction typically. For further improvement of the catalytic activity of the transition metal carbides and nitrides/oxynitrides, it may be beneficial to form bimetallic composites for obtaining multiple active species and tuning of electronic states.

Without the "acid-stability' requirement, some attempts have been 1610 made on the utilization of perovskite materials as electrocatalysts for 1611 ORR in alkaline media. Some disadvantages of perovskite materials such as high ohmic loss, low specific surface area and crystallite agglomeration have been alleviated by combination of carbon support, 1614 new synthesis technologies, etc. Although the intrinsic catalytic activity of transition metal oxide perovskites can be improved by adjusting 1616 the metallic compositions, these materials have lower activity than 1617 the state-of-the-art cathodic catalysts for ORR considering the best 1618 performing perovskite materials reported thus far.

For preparation of metal-free carbon material based electrocata- 1620 lysts for ORR in alkaline medial, it is generally required to modify 1621

the electron neutrality of the carbon plane with highly delocalized SP² 1622 electron properties by doping with heteroatoms such as N, O, P, B, S, I 1623 and so on. And it is quite interesting to notice that the electronegativity 1624 of the doping elements seems to be irrelevant for surface modification 1625 of electronic structures, since more electronegative elements like N, 1626 more electron-deficient elements like P and B, and electronegatively 1627 similar elements like S can all serve the purpose of changing the local 1628 electron density and Fermi level of the carbon substrate very well. 1629 Nevertheless, a theoretical and experimental study has proved that 1630 heteroatom doped graphene with five different commonly used atoms 1631 (N, S, O, B, and P) all exhibit inferior exchange current densities than 1632 an ideal X-graphene catalyst,³⁴ indicating that there is still opportunity 1633 for further improvement of the catalytic properties of doped carbon 1634 materials towards ORR. 1635

While urgent investigations of ORR mechanisms and precise iden-1636 tification of the nature of the active sites on metal-free electrocatalysts 1637 need to be conducted, some common properties can be obtained for 1638 the design of improved electrocatalysts for ORR in alkaline medial af-1639 ter reviewing a large variety of carbonaceous materials such as doped 1640 graphene, carbon nanotubes, carbon fibers, mesoporous carbons, and 1641 carbon aerogels (see Tables V and VI). First of all, there is no doubt 1642 that the active sites on carbon substrates for ORR are introduced by 1643 the heteroatoms (X) although some non-active X-C moieties may also 1644 be formed. Consequently, it is beneficial to increase the content of 1645 heteroatoms as long as the conductivity is sufficient and the max-1646 imum number of active sites is not reached. Secondly, outstanding 1647 ORR performance can be usually seen on those heteroatom- doped 1648 carbon materials with large surface area (typically > $600 \text{ m}^2/\text{g}$). For 1649 instance, low overpotentials, fast kinetics and 4e- pathway, and good 1650 long-term durability were found on many mesoporous carbon elec-1651 1652 trocatalysts prepared by pyrolysis of a mixture of precursors for C and heteroatoms and a silica substrate followed by removal of silica 1653 with HF or strong base. To overcome the problem of re-stacking of 1654 graphene layers due to strong π - π interactions, some composite mate-1655 rials like graphene/CNTs have shown much improved catalytic prop-1656 1657 erties. Last but not least, edges and topological defects have shown 1658 better catalytic activity than basal planes on carbon, which needs to be considered during design and preparation of novel metal-free 1659 electrocatalyst materials. 1660

To the end, from the point of view of practical applications, al-1661 though RRDE measurement is a fast and reliable method for screen-1662 1663 ing electrocatalysts for ORR, one must realize that the RRDE results 1664 may not necessarily be transferable to a real AAEMFC. By mixing the catalyst powder with hydroxide-conducting ionomer during the 1665 preparation of membrane electrode assemblies (MEAs), the reaction 1666 zone has been largely extended into the catalyst layer instead of being 1667 localized on the surface with direct contact to ionic clusters and ionic 1668 channels of the anion exchange membranes. However, the "higher 1669 catalyst loading - better ORR performance" phenomenon as seen dur-1670 ing RRDE measurements is no longer available in AAEM fuel cell 1671 testing, due to the significantly deteriorated performance with a large 1672 mass transport resistance and low conductivity ionomers. Therefore, 1673 from the point of view of electrocatalysis, the next step to advance the 1674 AAEMFC technology relies on the development of electrode archi-1675 tectures with significantly increased active site density and/or greatly 1676 improved ionomer conductivity. 1677

In addition to activity and kinetics for ORR, the stability of a 1678 cathode electrocatalyst is equally important in order to be employed 1679 in AAEMFCs. Similar to the situation in PEMFCs, the conventional 1680 Pt/C electrodes still suffer from aggregation of metal nanoparticles 1681 and degradation of the carbon support in AAEMFCs, and methanol 1682 crossover in the case when methanol is the fuel. From the literature, it 1683 is not unusual to see largely improved stability for alternative electro-1684 catalysts for Pt/C in diluted base (e.g. 0.1 M KOH). Nevertheless, real 1685 long-term alkaline fuel cell testing or accelerated aging tests under 1686 strongly basic conditions are desirable. For a better understanding of 1687 the degradation mechanism of ORR, some pioneering studies such 1688 as the impact of mobile ionomer head groups and some advanced 1689 1690 technologies like identical location- TEM are also highly needed.

Acknowledgment

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This work was supported by "The Recruitment Program of Global 1692 Youth Experts" from the Chinese government and the "Hundred Tal- 1693 ents Program" of Zhejiang University. We thank Dr. S. Khene and Dr. 1694 J.-P Dodelet for valuable discussions. 1695

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