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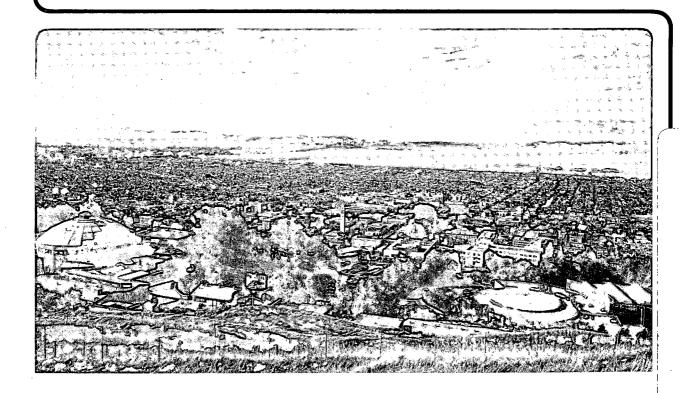
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# EARTH SCIENCES DIVISION

**Coupled Transport Processes in Semipermeable Media. Analytical Solutions of the Linearized Governing Equations** 

J.S. Jacobsen and C.L. Carnahan

March 1990



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# Coupled Transport Processes in Semipermeable Media. Analytical Solutions of the Linearized Governing Equations

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March 1990

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ABSTRACT — The thermodynamics of irreversible processes leads to nonlinear governing equations for direct and coupled mass transport processes. Analytical solutions of linearized versions of these equations can be used to verify numerical solutions of the nonlinear equations under conditions such that nonlinear terms are relatively small. This report presents derivations of the analytical solutions for one-dimensional and axisymmetric geometries.

#### GOVERNING EQUATIONS

Carnahan and Jacobsen (1990) have derived the governing equations for a saturated, porous or fractured system in which fluxes of heat, mass and electrical charge are driven by gradients of temperature, hydraulic potential, chemical potential and electrical potential. The derivations were based on the thermodynamics of irreversible processes.

Under the assumptions that gravitational and electrical forces are negligible, that no chemical reactions occur in the system, that the fluid phase is an ideal solution of a single solute, and that partial specific volumes and entropies of solute and solvent are constant, the balance equations are

$$\Gamma_1 \frac{\partial T}{\partial t} = -\nabla \cdot J_q - J_v \cdot \nabla P - \frac{\beta_f T}{\kappa_f} \nabla \cdot J_v - \frac{RT}{C_s M_s} J_s^{\circ} \cdot \nabla C_s, \tag{1}$$

$$\Lambda_1 \frac{\partial P}{\partial t} = -\nabla \cdot J_q - J_v \cdot \nabla P - \frac{c_{p,f} \rho_f}{\beta_f} \nabla \cdot J_v - \frac{RT}{C_s M_s} J_s^{\circ} \cdot \nabla C_s, \tag{2}$$

$$\epsilon_f \frac{\partial C_s}{\partial t} = -\nabla \cdot J_s,\tag{3}$$

where T is the temperature, P is the pressure,  $C_s$  is the concentration of the solute,  $J_q$  is the heat flux,  $J_v$  is the volume flux,  $J_s$  is the solute flux in the laboratory reference frame,  $J_s^o$  is the diffusional solute flux relative to motion of solvent, and  $\Gamma_1$  and  $\Lambda_1$  are shorthand notation for

$$\Gamma_1 = \epsilon_f \, \rho_f \, c_{v,f} + \epsilon_n \, \rho_n \, c_{v,n}, \tag{4a}$$

$$\Lambda_1 = \epsilon_f \, \rho_f \, c_{v,f} \, \frac{\kappa_f}{\beta_f} + \epsilon_n \, \rho_n \, c_{v,n} \, \frac{\kappa_n}{\beta_n}. \tag{4c}$$

All other symbols are defined in the Notation.

The fluxes to be used in (1)-(3) are given by the phenomenological equations

$$J_q = -L_{qq} \frac{\nabla T}{T} - L_{qv} \nabla P - L_{qs} \frac{RT}{C_s M_s} \nabla C_s, \tag{5}$$

$$J_v = -L_{vq} \frac{\nabla T}{T} - L_{vv} \nabla P - L_{vs} \frac{RT}{C_s M_s} \nabla C_s, \tag{6}$$

$$J_s^0 = -L_{sq} \frac{\nabla T}{T} - L_{sv} \nabla P - L_{ss} \frac{RT}{C_s M_s} \nabla C_s, \tag{7}$$

with the reciprocal relations

$$L_{qs} = L_{sq}, \quad L_{qv} = L_{vq}, \quad L_{vs} = L_{sv}. \tag{8}$$

The two solute fluxes,  $J_s$  and  $J_s^{\circ}$ , are related by

$$J_s = C_s J_v + (1 - C_s \overline{V}_s) J_s^{\circ}, \tag{9}$$

and therefore the solute flux in the laboratory frame of reference is given by

$$J_{s} = -\left[C_{s} L_{vq} + \left(1 - C_{s} \overline{V}_{s}\right) L_{sq}\right] \frac{\nabla T}{T}$$

$$-\left[C_{s} L_{vv} + \left(1 - C_{s} \overline{V}_{s}\right) L_{sv}\right] \nabla P$$

$$-\left[C_{s} L_{vs} + \left(1 - C_{s} \overline{V}_{s}\right) L_{ss}\right] \frac{RT}{C_{s} M_{s}} \nabla C_{s}.$$
(10)

When (5)–(7) and (10) are substituted into (1)–(3), a system of nonlinear governing equations is obtained. These equations were solved numerically by Jacobsen and Carnahan (1990). Under conditions such that the nonlinear terms are small relative to linear terms in the governing equations, the numerical results were verified by comparison with analytical solutions derived from linear versions of the governing equations. The analytical solutions were useful also in estimating contributions of nonlinear terms to magnitudes of the primary variables  $(T, P, C_s)$  and the fluxes.

#### DERIVATIONS OF ANALYTICAL SOLUTIONS

The phenomenological equations (5), (6) and (7) may be made linear by assuming constancy of the phenomenological coefficients and by replacing factors of temperature and solute concentration by average values, denoted below by  $T_m$  and  $C_{s,m}$ , respectively. The linear phenomenological equations are

$$J_q = -L_{qq} \frac{\nabla T}{T_m} - L_{qv} \nabla P - L_{qs} \frac{RT_m}{C_{s,m} M_s} \nabla C_s, \tag{11}$$

$$J_{v} = -L_{vq} \frac{\nabla T}{T_{m}} - L_{vv} \nabla P - L_{vs} \frac{RT_{m}}{C_{s,m} M_{s}} \nabla C_{s}, \tag{12}$$

$$J_{s} = -\left[C_{s,m} L_{vq} + \left(1 - C_{s,m} \overline{V}_{s}\right) L_{sq}\right] \frac{\nabla T}{T_{m}}$$

$$-\left[C_{s,m} L_{vv} + \left(1 - C_{s,m} \overline{V}_{s}\right) L_{sv}\right] \nabla P$$

$$-\left[C_{s,m} L_{vs} + \left(1 - C_{s,m} \overline{V}_{s}\right) L_{ss}\right] \frac{RT_{m}}{C_{s,m} M_{s}} \nabla C_{s},$$
(13)

The governing equations (1), (2) and (3) can be made linear by neglecting products of derivatives:

$$\Gamma_1 \frac{\partial T}{\partial t} = -\nabla \cdot J_q - \frac{\beta_f T_m}{\kappa_f} \nabla \cdot J_v, \tag{14}$$

$$\Lambda_1 \frac{\partial P}{\partial t} = -\nabla \cdot J_q - \frac{c_{p,f} \rho_f}{\beta_f} \nabla \cdot J_v, \tag{15}$$

$$\epsilon_f \frac{\partial C_s}{\partial t} = -\nabla \cdot J_s,\tag{16}$$

When the expressions for the fluxes from the phenomenological equations are substituted into the governing equations above, the only space derivative terms are second derivatives:

$$\frac{\partial T}{\partial t} = D_{TT} \nabla^2 T + D_{TP} \nabla^2 P + D_{TS} \nabla^2 C_s, \tag{17}$$

$$\frac{\partial P}{\partial t} = D_{PT} \nabla^2 T + D_{PP} \nabla^2 P + D_{PS} \nabla^2 C_s, \tag{18}$$

$$\frac{\partial C_s}{\partial t} = D_{ST} \nabla^2 T + D_{SP} \nabla^2 P + D_{SS} \nabla^2 C_s. \tag{19}$$

The  $D_{IJ}$  are functions of the material properties, phenomenological coefficients and the average values of temperature and solute concentration and are defined by

$$D_{TT} = \frac{1}{\Gamma_1} \left( \frac{L_{qq}}{T_m} + \frac{\beta_f}{\kappa_f} L_{vq} \right), \tag{20a}$$

$$D_{TP} = \frac{1}{\Gamma_1} \left( L_{qv} + \frac{\beta_f T_m}{\kappa_f} L_{vv} \right), \tag{20b}$$

$$D_{TS} = \frac{1}{\Gamma_1} \left( L_{qs} + \frac{\beta_f T_m}{\kappa_f} L_{vs} \right) \frac{RT_m}{C_{s,m} M_s}, \tag{20c}$$

$$D_{PT} = \frac{1}{\Lambda_1 T_m} \left[ L_{qq} + \left( \frac{c_{p,f} \rho_f}{\beta_f} \right) L_{qv} \right], \tag{20d}$$

$$D_{PP} = \frac{1}{\Lambda_1} \left[ L_{qv} + \left( \frac{c_{p,f} \, \rho_f}{\beta_f} \right) L_{vv} \right], \tag{20e}$$

$$D_{PS} = \frac{1}{\Lambda_1} \left[ L_{qs} + \left( \frac{c_{p,f} \rho_f}{\beta_f} \right) L_{vs} \right] \frac{RT_m}{C_{s,m} M_s}, \tag{20f}$$

$$D_{ST} = \frac{1}{\epsilon_f T_m} \left[ C_{s,m} L_{vq} + \left( 1 - C_{s,m} \overline{V}_s \right) L_{sq} \right], \tag{20g}$$

$$D_{SP} = \frac{1}{\epsilon_f} \left[ C_{s,m} L_{vv} + \left( 1 - C_{s,m} \overline{V}_s \right) L_{sv} \right], \tag{20h}$$

$$D_{SS} = \frac{1}{\epsilon_f} \left[ C_{s,m} L_{vs} + \left( 1 - C_{s,m} \overline{V}_s \right) L_{ss} \right] \frac{RT_m}{C_{s,m} M_s}, \tag{20i}$$

where  $\Gamma_1$  and  $\Lambda_1$  are defined by (4). To complete the mathematical formulation of the problem the initial and boundary conditions must be specified. Initially all variables are assigned constant values.

The boundary conditions for T, P and  $C_s$  at the inner boundary are derived from the constant heat, solute and solvent fluxes imposed there. In a one-dimensional coordinate system, the flux boundary is located at x = 0, and in radial coordinates, the flux boundary is located at r = a. At the outer boundary, located at infinity, T, P and  $C_s$  are held constant and equal to their initial values.

The analytical solution for the system of equations above is obtained using the Laplace transform method (Carslaw and Jaeger, 1959). The transformed system of equations is given by

$$s\overline{T} - T_i = D_{TT} \nabla^2 \overline{T} + D_{TP} \nabla^2 \overline{P} + D_{TS} \nabla^2 \overline{C}_s, \tag{21}$$

$$s\,\overline{P} - P_{i} = D_{PT}\,\nabla^{2}\overline{T} + D_{PP}\,\nabla^{2}\overline{P} + D_{PS}\,\nabla^{2}\overline{C}_{s},\tag{22}$$

$$s\,\overline{C}_{s} - C_{s,i} = D_{ST}\,\nabla^{2}\overline{T} + D_{SP}\,\nabla^{2}\overline{P} + D_{SS}\,\nabla^{2}\overline{C}_{s},\tag{23}$$

where  $T_i$ ,  $P_i$  and  $C_{s,i}$  are the initial values of temperature, pressure and solute concentration.

### Solutions for the Fully Coupled Case in a One-Dimensional Geometry

In a one-dimensional coordinate system,  $\nabla^2 = \partial^2/\partial x^2$ . Using this definition in (21), (22) and (23), the transformed equations in one-dimension are

$$s\overline{T} - T_i = D_{TT} \frac{\partial^2 \overline{T}}{\partial x^2} + D_{TP} \frac{\partial^2 \overline{P}}{\partial x^2} + D_{TS} \frac{\partial^2 \overline{C}_s}{\partial x^2}, \tag{24}$$

$$s\overline{P} - P_{i} = D_{PT} \frac{\partial^{2}\overline{T}}{\partial x^{2}} + D_{PP} \frac{\partial^{2}\overline{P}}{\partial x^{2}} + D_{PS} \frac{\partial^{2}\overline{C}_{s}}{\partial x^{2}}, \tag{25}$$

$$s\,\overline{C}_s - C_{s,i} = D_{ST}\,\frac{\partial^2 \overline{T}}{\partial x^2} + D_{SP}\,\frac{\partial^2 \overline{P}}{\partial x^2} + D_{SS}\,\frac{\partial^2 \overline{C}_s}{\partial x^2}.$$
 (26)

Noting that  $\exp(-\lambda x)$  and  $\exp(\lambda x)$  are solutions of

$$\frac{\partial^2 f}{\partial x^2} = \lambda^2 f,\tag{27}$$

for f, a function of x, and  $\lambda$ , a positive constant, it is reasonable to assume that solutions of the transformed equations above will involve exponential functions. Only exponential functions with negative arguments can satisfy the outer boundary condition, so the solutions for  $\overline{T}$ ,  $\overline{P}$  and  $\overline{C}_s$  will be assumed to be of the following form:

$$\overline{T} = \frac{T_i}{s} + A \exp(-\lambda x), \tag{28}$$

$$\overline{P} = \frac{P_i}{s} + B \exp(-\lambda x), \tag{29}$$

$$\overline{C}_s = \frac{C_{s,i}}{s} + E \exp(-\lambda x). \tag{30}$$

where, as above,  $\lambda$  is a positive constant to be determined and A, B and E are to be determined from the inner boundary conditions. Substituting the expressions for  $\overline{T}$ ,  $\overline{P}$  and  $\overline{C}_s$  above into the governing

equations (24), (25) and (26) yields the following matrix equation

$$\lambda^{2} \begin{pmatrix} D_{TT} & D_{TP} & D_{TS} \\ D_{PT} & D_{PP} & D_{PS} \\ D_{ST} & D_{SP} & D_{SS} \end{pmatrix} \begin{pmatrix} A \\ B \\ E \end{pmatrix} = s \begin{pmatrix} A \\ B \\ E \end{pmatrix}, \tag{31}$$

which will have a nonzero solution if and only if  $\lambda$  is chosen such that

$$\det(\lambda^2 \mathbf{D} - s \mathbf{I}) = 0 \tag{32}$$

(Boyce and DiPrima, 1969). **D** is the matrix of coefficients in (31), and **I** is the identity matrix. The equation defined by (32) is a cubic in  $\lambda^2/s$ :

$$d_1 \left(\frac{\lambda^2}{s}\right)^3 - d_2 \left(\frac{\lambda^2}{s}\right)^2 + d_3 \left(\frac{\lambda^2}{s}\right) - 1 = 0, \tag{33}$$

where

$$d_1 = D_{TT}D_{PP}D_{SS} + D_{TP}D_{PS}D_{ST} + D_{TS}D_{PT}D_{SP}$$

$$-D_{TT}(D_{PS}D_{SP}) - D_{PP}(D_{TS}D_{ST}) - D_{SS}(D_{TP}D_{PT}), \qquad (34a)$$

$$d_2 = D_{TP}D_{PT} + D_{TS}D_{ST} + D_{PS}D_{SP}$$

$$-D_{TT}D_{PP} - D_{TT}D_{SS} - D_{PP}D_{SS}, (34b)$$

$$d_3 = D_{TT} + D_{PP} + D_{SS}. (34c)$$

For a cubic of the form

$$y^3 + py^2 + qy + r = 0, (35)$$

Burington (1949) gives the following expression for the roots,

$$y_i = 2\sqrt{-\alpha}\cos\left[\frac{\theta}{3} + \frac{2\pi}{3}(i-1)\right] - \frac{p}{3}, \quad i = 1, 2, 3.$$
 (36)

The intermediate variables,  $\alpha$  and  $\theta$ , are defined by

$$\alpha = \frac{1}{9} \left( 3q - p^2 \right), \tag{37}$$

$$\cos \theta = \begin{cases} -\sqrt{\eta^2/\alpha^3}, & \text{if } \eta > 0, \\ +\sqrt{\eta^2/\alpha^3}, & \text{if } \eta \le 0, \end{cases}$$
 (38)

where

$$\eta = \frac{1}{54} \left( 2p^3 - 9pq + 27r \right). \tag{39}$$

The expression in (36) assumes that all of the roots are real. The sign of  $\alpha^3 + \eta^2$  indicates whether the roots of the cubic are real or imaginary. If  $\alpha^3 + \eta^2 > 0$ , then two of the roots are imaginary; if

 $\alpha^3 + \eta^2 \le 0$ , then all of the roots are real. It is difficult to check this condition a priori for  $\alpha$  and  $\eta$  defined in terms of the  $d_i$ ,

$$\alpha = \frac{1}{3d_1} \left( d_3 - \frac{d_2^2}{3d_1} \right),\tag{40}$$

$$\eta = \frac{1}{2d_1} \left( \frac{d_2 d_3}{3d_1} - \frac{2d_2^3}{27d_1^2} - 1 \right). \tag{41}$$

In this derivation, it has been assumed that  $\alpha^3 + \eta^2 \le 0$ . When the analytical solution is calculated for given values of the material properties, phenomenological coefficients and other input parameters, this condition is checked by calculating  $\alpha + (\eta/\alpha)^2$ . This alternate, but equivalent, form is used because, in practice, the magnitudes of  $\alpha$  and  $\eta$  are quite large.

As noted before, solutions involving exponential functions with positive arguments cannot satisfy the boundary conditions at infinity. Therefore, the  $\lambda_i$  are defined by

$$\lambda_i = \mu_i \sqrt{s}, \quad i = 1, 2, 3, \tag{42}$$

where

$$\mu_{i} = \left\{ \frac{d_{2}}{3d_{1}} + 2\sqrt{-\alpha}\cos\left[\frac{\theta}{3} + \frac{2\pi}{3}(i-1)\right] \right\}^{\frac{1}{2}}, \quad i = 1, 2, 3.$$
 (43)

The solutions to the transformed equations can be written as

$$\overline{T} = \frac{T_i}{s} + \sum_{i=1}^{3} A_i \exp\left(-\mu_i \sqrt{s} x\right), \qquad (44)$$

$$\overline{P} = \frac{P_i}{s} + \sum_{i=1}^{3} B_i \exp\left(-\mu_i \sqrt{s} x\right), \tag{45}$$

$$\overline{C}_s = \frac{C_{s,i}}{s} + \sum_{i=1}^3 E_i \exp\left(-\mu_i \sqrt{s} x\right), \tag{46}$$

assuming that  $\mu_i \geq 0$  for i = 1, 2, 3.

Equation (31) holds for all values of i, so it can be used to express the  $B_i$  and  $E_i$  coefficients in terms of the  $A_i$ :

$$B_i = b_i A_i, (47)$$

where

$$b_{i} = \frac{\mu_{i}^{2} \left( D_{TT} D_{PS} - D_{TS} D_{PT} \right) - D_{PS}}{\mu_{i}^{2} \left( D_{TS} D_{PP} - D_{TP} D_{PS} \right) - D_{TS}},\tag{48}$$

and

$$E_i = e_i A_i, \tag{49}$$

for

$$e_{i} = \frac{\mu_{i}^{2} (D_{TT} D_{SP} - D_{TP} D_{ST}) - D_{SP}}{\mu_{i}^{2} (D_{TP} D_{SS} - D_{TS} D_{SP}) - D_{TP}}.$$
(50)

The  $A_i$  can then be determined from the inner boundary conditions,

$$J_{q,inc} = -\frac{L_{qq}}{T_m} \left. \frac{\partial T}{\partial x} \right|_{x=0} -L_{qv} \left. \frac{\partial P}{\partial x} \right|_{x=0} -L_{qs} \left. \frac{RT_m}{C_{s,m} M_s} \left. \frac{\partial C_s}{\partial x} \right|_{x=0}, \tag{51}$$

$$J_{v,inc} = -\frac{L_{vq}}{T_m} \frac{\partial T}{\partial x} \bigg|_{x=0} -L_{vv} \frac{\partial P}{\partial x} \bigg|_{x=0} -L_{vs} \frac{RT_m}{C_{s,m} M_s} \frac{\partial C_s}{\partial x} \bigg|_{x=0},$$
 (52)

$$J_{s,inc}^{\circ} = -\frac{L_{sq}}{T_m} \left. \frac{\partial T}{\partial x} \right|_{x=0} -L_{sv} \left. \frac{\partial P}{\partial x} \right|_{x=0} -L_{ss} \left. \frac{RT_m}{C_{s,m} M_s} \left. \frac{\partial C_s}{\partial x} \right|_{x=0}, \tag{53}$$

and.

$$J_{s,inc} = C_{s,m} J_{v,inc} + (1 - C_{s,m} \overline{V}_s) J_{s,inc}^{o}.$$
 (54)

Transforming the boundary conditions and solving (54) for  $J_{s,inc}^{o}$  yield

$$\frac{J_{q,inc}}{s} = -\frac{L_{qq}}{T_m} \frac{\partial \overline{T}}{\partial x} \bigg|_{x=0} - L_{qv} \frac{\partial \overline{P}}{\partial x} \bigg|_{x=0} - L_{qs} \frac{RT_m}{C_{s,m} M_s} \frac{\partial \overline{C}_s}{\partial x} \bigg|_{x=0}, \tag{55}$$

$$\frac{J_{v,inc}}{s} = -\frac{L_{vq}}{T_m} \frac{\partial \overline{T}}{\partial x} \bigg|_{x=0} -L_{vv} \frac{\partial \overline{P}}{\partial x} \bigg|_{x=0} -L_{vs} \frac{RT_m}{C_{s,m}M_s} \frac{\partial \overline{C}_s}{\partial x} \bigg|_{x=0}, \tag{56}$$

$$\frac{J_{s,inc} - C_{s,m} J_{v,inc}}{s(1 - C_{s,m} \overline{V}_s)} = -\frac{L_{sq}}{T_m} \frac{\partial \overline{T}}{\partial x} \bigg|_{x=0} - L_{sv} \frac{\partial \overline{P}}{\partial x} \bigg|_{x=0} - L_{ss} \frac{RT_m}{C_{s,m} M_s} \frac{\partial \overline{C}_s}{\partial x} \bigg|_{x=0}.$$
 (57)

Substituting the expressions for  $\overline{T}$ ,  $\overline{P}$  and  $\overline{C}_s$  from (44), (45) and (46) into the transformed boundary conditions above and multiplying through by  $1/\sqrt{s}$  yield

$$\frac{J_{q,inc}}{s\sqrt{s}} = \sum_{i=1}^{3} l_{qi} \mu_i A_i, \qquad (58)$$

$$\frac{J_{v,inc}}{s\sqrt{s}} = \sum_{i=1}^{3} l_{vi} \,\mu_i \,A_i, \tag{59}$$

$$\frac{J_{s,inc} - C_{s,m} J_{v,inc}}{s\sqrt{s}(1 - C_{s,m} \overline{V}_s)} = \sum_{i=1}^{3} l_{si} \mu_i A_i,$$
 (60)

where

$$l_{qi} = \frac{L_{qq}}{T_m} + L_{qv}b_i + L_{qs}\frac{RT_m}{C_{s,m}M_s}e_i,$$
 (61)

$$l_{vi} = \frac{L_{vq}}{T_m} + L_{vv}b_i + L_{vs}\frac{RT_m}{C_{s,m}M_s}e_i,$$
 (62)

$$l_{si} = \frac{L_{sq}}{T_m} + L_{sv}b_i + L_{ss}\frac{RT_m}{C_{s,m}M_s}e_i.$$
 (63)

Equations (58), (59) and (60) can be solved for the  $A_i$ . The result is

$$A_{i} = \frac{1}{s\sqrt{s}} G_{i} = \frac{1}{s\sqrt{s}} \frac{g_{i}}{\Delta \mu_{i}}, i = 1, 2, 3,$$
 (64)

where

$$g_1 = (l_{v2}l_{s3} - l_{v3}l_{s2})J_{q,inc} + (l_{q3}l_{s2} - l_{q2}l_{s3})J_{v,inc}$$

$$+ (l_{q2}l_{v3} - l_{q3}l_{v2}) \left( \frac{J_{s,inc} - C_{s,m}J_{v,inc}}{1 - C_{s,m}\overline{V}_s} \right), \tag{65a}$$

$$g_2 = (l_{v3}l_{s1} - l_{v1}l_{s3})J_{q,inc} + (l_{q1}l_{s3} - l_{q3}l_{s1})J_{v,inc}$$

$$+ (l_{q3}l_{v1} - l_{q1}l_{v3}) \left( \frac{J_{s,inc} - C_{s,m}J_{v,inc}}{1 - C_{s,m}\overline{V}_s} \right), \tag{65b}$$

$$g_3 = (l_{v1}l_{s2} - l_{v2}l_{s1}) J_{q,inc} + (l_{q2}l_{s1} - l_{q1}l_{s2}) J_{v,inc}$$

$$+ (l_{q1}l_{v2} - l_{q2}l_{v1}) \left( \frac{J_{s,inc} - C_{s,m}J_{v,inc}}{1 - C_{s,m}\overline{V}_s} \right), \tag{65c}$$

 $\mathbf{and}$ 

$$\Delta = l_{q1} \left( l_{v2} l_{s3} - l_{v3} l_{s2} \right) + l_{q2} \left( l_{v3} l_{s1} - l_{v1} l_{s3} \right) + l_{q3} \left( l_{v1} l_{s2} - l_{v2} l_{s1} \right). \tag{66}$$

The final forms for the solutions in the transform space are

$$\overline{T} = \frac{T_i}{s} + \frac{1}{s\sqrt{s}} \sum_{i=1}^{3} G_i \exp\left(-\mu_i \sqrt{s} x\right), \tag{67}$$

$$\overline{P} = \frac{P_i}{s} + \frac{1}{s\sqrt{s}} \sum_{i=1}^{3} b_i G_i \exp\left(-\mu_i \sqrt{s} x\right), \qquad (68)$$

$$\overline{C}_s = \frac{C_{s,i}}{s} + \frac{1}{s\sqrt{s}} \sum_{i=1}^3 e_i G_i \exp\left(-\mu_i \sqrt{s} x\right), \tag{69}$$

where the  $G_i$  are defined implicitly in (64), the  $\mu_i$  are defined by (43), the  $b_i$  by (48) and the  $e_i$  by (50). All of these variables are free of the transform variable s. The solutions above can be inverted

using the two inversion formulas:

$$\mathcal{L}^{-1}\left\{\frac{k}{s}\right\} = k,\tag{70}$$

$$\mathcal{L}^{-1}\left\{\frac{k}{s\sqrt{s}}\exp\left(-\nu\sqrt{s}\right)\right\} = k\left[2\sqrt{\frac{t}{\pi}}\exp\left(-\frac{\nu^2}{4t}\right) - \operatorname{erfc}\left(\frac{\nu}{2\sqrt{t}}\right)\right],\tag{71}$$

where k is a constant independent of s, and erfc is the complementary error function. In the second inversion formula,  $\nu = \mu_i x$ , and letting

$$\xi_i = \frac{\mu_i \, x}{2\sqrt{t}},\tag{72}$$

the inverted solutions for the fully coupled case can be written

$$T = T_i + \sum_{i=1}^{3} G_i \left[ 2\sqrt{\frac{t}{\pi}} \exp\left(-\xi_i^2\right) - \mu_i x \operatorname{erfc}(\xi_i) \right], \tag{73}$$

$$P = P_i + \sum_{i=1}^{3} b_i G_i \left[ 2\sqrt{\frac{t}{\pi}} \exp\left(-\xi_i^2\right) - \mu_i x \operatorname{erfc}(\xi_i) \right], \tag{74}$$

$$C_s = C_{s,i} + \sum_{i=1}^{3} e_i G_i \left[ 2\sqrt{\frac{t}{\pi}} \exp\left(-\xi_i^2\right) - \mu_i x \operatorname{erfc}(\xi_i) \right], \tag{75}$$

where  $G_i = g_i/(\Delta \mu_i)$  and  $g_i$  is defined by (65),  $\Delta$  by (66) and  $\mu_i$  by (43). The procedure for calculating T, P and  $C_s$  from the equations above is given in the third section.

In the uncoupled case and when thermal osmosis and thermal filtration are included,  $D_{TS}$  and  $D_{PS}$  are zero. In these two cases, the definition of the  $b_i$  in (48) is indeterminant. There are two approaches to obtaining the solutions in these cases: the  $b_i$  may be redefined by

$$b_i = \frac{1 - \mu_i^2 D_{TT}}{\mu_i^2 D_{TP}}, (76)$$

or the solution may be rederived starting with a simplified version of the system of governing equations. The second approach is presented in the fourth section.

### Solutions for the Fully Coupled Case in a Radial Geometry

In this case, the system of transformed equations is given by (21), (22) and (23) with  $\nabla^2 = \frac{\partial^2}{\partial r^2} + (1/r)\frac{\partial}{\partial r}$ . The modified Bessel functions of order zero,  $I_0$  and  $K_0$ , are solutions of the differential equation,

$$\frac{\partial^2 \mathcal{F}}{\partial r^2} + \frac{1}{r} \frac{\partial \mathcal{F}}{\partial r} = \lambda^2 \mathcal{F},\tag{77}$$

for  $\lambda$  a constant. It is therefore reasonable to assume that solutions of the transformed equations can be written in terms of  $I_0$  and  $K_0$ . For large arguments, however,  $I_0$  increases exponentially, so

solutions involving  $I_0$  cannot satisfy the outer boundary conditions, which are that the solutions tend to their initial values as r increases. Therefore,  $I_0$  is discarded as a possibility, and solutions of the following form are assumed:

$$\overline{T} = \frac{T_i}{s} + A K_0 (\lambda r), \qquad (78)$$

$$\overline{P} = \frac{P_i}{s} + B K_0 (\lambda r), \qquad (79)$$

$$\overline{C}_s = \frac{C_{s,i}}{s} + E K_0(\lambda r). \tag{80}$$

Substituting these expressions into (21), (22) and (23) leads to the same matrix equation (30) as that derived when a one-dimensional coordinate system was used, and consequently many of the intermediate steps are the same for the one-dimensional and radial coordinate systems. Using the results from the previous section, the solutions in the transform space can be written

$$\overline{T} = \frac{T_i}{s} + \sum_{i=1}^3 A_i K_0 \left( \mu_i \sqrt{s} r \right), \tag{81}$$

$$\overline{P} = \frac{P_i}{s} + \sum_{i=1}^3 b_i A_i K_0 \left( \mu_i \sqrt{s} \, r \right), \tag{82}$$

$$\overline{C}_s = \frac{C_{s,i}}{s} + \sum_{i=1}^3 e_i A_i K_0 \left( \mu_i \sqrt{s} r \right). \tag{83}$$

where the  $b_i$  are given by (48) or (76) depending on the coupling, the  $e_i$  are given by (50) and the  $\mu_i$  are given by (43). As with the one-dimensional solution, the  $A_i$  can be determined using the transformed inner boundary conditions and (53):

$$\frac{J_{q,inc}}{s} = -\frac{L_{qq}}{T_m} \frac{\partial \overline{T}}{\partial r} \bigg|_{r=a} - L_{qv} \frac{\partial \overline{P}}{\partial r} \bigg|_{r=a} - L_{qs} \frac{RT_m}{C_{s,m} M_s} \frac{\partial \overline{C}_s}{\partial r} \bigg|_{r=a}, \tag{84}$$

$$\frac{J_{v,inc}}{s} = -\frac{L_{vq}}{T_m} \frac{\partial \overline{T}}{\partial r} \bigg|_{r=0} -L_{vv} \frac{\partial \overline{P}}{\partial r} \bigg|_{r=0} -L_{vs} \frac{RT_m}{C_{s,m}M_s} \frac{\partial \overline{C}_s}{\partial r} \bigg|_{r=0}, \tag{85}$$

$$\frac{J_{s,inc} - C_{s,m} J_{v,inc}}{s \left(1 - C_{s,m} \overline{V}_{s}\right)} = -\frac{L_{sq}}{T_{m}} \left. \frac{\partial \overline{T}}{\partial r} \right|_{r=a} - L_{sv} \left. \frac{\partial \overline{P}}{\partial r} \right|_{r=a} - L_{ss} \left. \frac{RT_{m}}{C_{s,m} M_{s}} \left. \frac{\partial \overline{C}_{s}}{\partial r} \right|_{r=a} \right.$$
(86)

Substituting the expressions for  $\overline{T}$ ,  $\overline{P}$  and  $\overline{C}_s$  from (81), (82) and (83) into the equations above and multiplying through by  $1/\sqrt{s}$  result in three equations for the  $A_i$ ,

$$\frac{J_{q,inc}}{s\sqrt{s}} = \sum_{i=1}^{3} l_{qi} \mu_i A_i K_1 \left(\mu_i \sqrt{s} a\right), \tag{87}$$

$$\frac{J_{v,inc}}{s\sqrt{s}} = \sum_{i=1}^{3} l_{vi} \mu_i A_i K_1 \left(\mu_i \sqrt{s} a\right), \tag{88}$$

$$\frac{J_{s,inc} - C_{s,m} J_{v,inc}}{s\sqrt{s} \left(1 - C_{s,m} \overline{V}_{s}\right)} = \sum_{i=1}^{3} l_{si} \mu_{i} A_{i} K_{1} \left(\mu_{i} \sqrt{s} a\right), \tag{89}$$

where the  $l_{qi}$ ,  $l_{vi}$  and  $l_{si}$  are defined by (61), (62) and (63). Solving these yields the same results as in the one-dimensional case: the  $A_i$  are defined by equations (64) through (66).

The final expressions for the solutions in the transform space for the fully coupled case are

$$\overline{T} = \frac{T_i}{s} + \frac{1}{s\sqrt{s}} \sum_{i=1}^{3} G_i \frac{K_0 \left(\mu_i \sqrt{s} r\right)}{K_1 \left(\mu_i \sqrt{s} a\right)},\tag{90}$$

$$\overline{P} = \frac{P_i}{s} + \frac{1}{s\sqrt{s}} \sum_{i=1}^{3} b_i G_i \frac{K_0 (\mu_i \sqrt{s} r)}{K_1 (\mu_i \sqrt{s} a)},$$
(91)

$$\overline{C}_{s} = \frac{C_{s,i}}{s} + \frac{1}{s\sqrt{s}} \sum_{i=1}^{3} e_{i} G_{i} \frac{K_{0} (\mu_{i} \sqrt{s} r)}{K_{1} (\mu_{i} \sqrt{s} a)}, \tag{92}$$

where the  $b_i$ ,  $e_i$ ,  $G_i$  and  $\mu_i$  are defined by equations (48), (50), (63) and (43), respectively, and all are free of the transform variable s. These solutions can be inverted using the inversion formula (70) and

$$\mathcal{L}^{-1}\left\{\frac{1}{s\sqrt{s}}\frac{K_0\left(\mu_i\sqrt{s}\,r\right)}{K_1\left(\mu_i\sqrt{s}\,a\right)}\right\} =$$

$$\frac{2 a \mu_i}{\pi} \int_0^\infty \left[ 1 - \exp\left( -\frac{t u^2}{a^2 \mu_i^2} \right) \right] \frac{Y_0(ru/a) J_1(u) - J_0(ru/a) Y_1(u)}{J_1^2(u) + Y_1^2(u)} \frac{du}{u^2}$$
(93)

(Carslaw and Jaeger, 1959). Because of the difficulty in calculating the integral in (93), it is computationally more efficient to numerically invert the solutions in the transform space using an algorithm by Stehfest (1970). A procedure for calculating  $\overline{T}$ ,  $\overline{P}$  and  $\overline{C}_s$  from equations (90) through (92) is outlined below.

### Computational Procedure for the Fully Coupled Case

The analytical solutions for the one-dimensional and radial coordinate systems for the uncoupled and all of the coupled cases, including the fully coupled case, can be computed as follows:

- 1. calculate the  $D_{IJ}$  from (20),
- 2. calculate the  $d_i$ , for j = 1, 2, 3, 4, from (34),
- 3. calculate  $\alpha$  and  $\eta$  from (40) and (41),
- 4. calculate  $\theta$  from (38),
- 5. calculate the  $\mu_i$  from (43),

- 6. calculate the  $b_i$  from (76) in the uncoupled case and when thermal osmosis and thermal filtration are included or from (48) in all other cases,
- 7. calculate the  $e_i$  from (50),
- 8. calculate the  $l_{qi}$ ,  $l_{vi}$  and  $l_{si}$  from (61), (62) and (63),
- 9. calculate  $J_{v,inc}$  from the incoming solvent and solute fluxes,  $J_{0,inc}$  and  $J_{s,inc}$ , using  $J_{v,inc} = J_{0,inc} \overline{V}_0 + J_{s,inc} \overline{V}_s$ ,
- 10. calculate the  $g_i$  from (65) and  $\Delta$  from (66),
- 11. calculate the  $G_i$  from  $G_i = g_i/(\Delta \mu_i)$ ,
  - 12. in the one-dimensional case, calculate T, P and  $C_s$  from (73), (74) and (75) using  $\xi_i = \mu_i x/2\sqrt{t}$  and in the radial case, calculate  $\overline{T}$ ,  $\overline{P}$  and  $\overline{C}_s$  from (90), (91) and (92) and numerically invert them to obtain T, P and  $C_s$ .

In steps 5 through 12 above, i = 1, 2, 3.

## Solutions for the Uncoupled and Thermal Osmosis Cases in One Dimension

In the thermal osmosis case, that is, when thermal osmosis and thermal filtration are included, all of the phenomenological coefficients corresponding to the indirect processes are zero except for the coefficients of thermal filtration and thermal osmosis,  $L_{qv}$  and  $L_{vq}$ . In the uncoupled case, both of these coefficients are zero as well. In both cases,  $D_{TS}$  and  $D_{PS}$  defined by (20), are zero, which simplifies the system of transformed equations:

$$s\overline{T} - T_{i} = D_{TT} \nabla^{2}\overline{T} + D_{TP} \nabla^{2}\overline{P}, \tag{94}$$

$$s\overline{P} - P_{i} = D_{PT} \nabla^{2}\overline{T} + D_{PP} \nabla^{2}\overline{P}, \tag{95}$$

$$s\overline{C}_{s} - C_{s,i} = D_{ST} \nabla^{2}\overline{T} + D_{SP} \nabla^{2}\overline{P} + D_{SS} \nabla^{2}\overline{C}_{s}. \tag{96}$$

In the system above, solutions for  $\overline{T}$  and  $\overline{P}$  may be obtained independently of that for  $\overline{C}_s$ , and once they have,  $\overline{C}_s$  may be determined from (96).

Assuming solutions for  $\overline{T}$  and  $\overline{P}$  of the same form as those in (28) and (29) yields the following matrix equation:

$$\lambda^{2} \begin{pmatrix} D_{TT} & D_{TP} \\ D_{PT} & D_{PP} \end{pmatrix} \begin{pmatrix} A \\ B \end{pmatrix} = s \begin{pmatrix} A \\ B \end{pmatrix}, \tag{97}$$

Equation (97) will have a nonzero solution only if the determinant of the coefficient matrix for the corresponding homogeneous matrix equation is zero:

$$(D_{PP}D_{TT} - D_{PT}D_{TP})\lambda^4 - (D_{PP} + D_{TT})s\lambda^2 + s^2 = 0.$$
(98)

The roots of (98) are

$$\lambda^2 = s \frac{(D_{PP} + D_{TT}) \pm \sqrt{(D_{TT} - D_{PP})^2 + 4D_{PT}D_{TP}}}{2(D_{TT}D_{PP} - D_{PT}D_{TP})},$$
(99)

and therefore,

$$\lambda = \pm \sqrt{s \frac{(D_{PP} + D_{TT}) \pm \sqrt{(D_{TT} - D_{PP})^2 + 4D_{PT}D_{TP}}}{2(D_{TT}D_{PP} - D_{PT}D_{TP})}}.$$
 (100)

It is necessary to determine which combination of signs in (100) yields positive values of  $\lambda$  because only positive values, and hence negative arguments in the exponential functions in (28) and (29), will give solutions that satisfy the boundary conditions at infinity.  $D_{TT}$ ,  $D_{PP}$ ,  $D_{TP}$  and  $D_{PT}$  are all positive, because the material properties and phenomenological coefficients in the definitions are all positive. Substituting the expressions for  $D_{TT}$ ,  $D_{PP}$ ,  $D_{TP}$  and  $D_{PT}$  from (20) yields the following expression for the denominator in (100):

$$D_{TT}D_{PP} - D_{PT}D_{TP} = \frac{1}{\Gamma_1 \Lambda_1} \left( \frac{c_{p,f} \rho_f}{T_m \beta_f} - \frac{\beta_f}{\kappa_f} \right) \left( L_{qq} L_{vv} - L_{qv} L_{vq} \right). \tag{101}$$

On the right-hand side of (101), the first two factors are positive because each individual term in them is positive. The third factor is positive because the phenomenological coefficients are constrained by  $(L_{qq}L_{vv}-L_{qv}L_{vq})>0$  (Katchalsky and Curran, 1967). Therefore, the denominator in (100) is positive. The second term in the numerator of (100) is positive and can be rewritten as

$$(D_{PP} - D_{TT})^2 + 4D_{PT}D_{TP} = (D_{PP} + D_{TT})^2 - 4(D_{PP}D_{TT} - D_{PT}D_{TP}).$$
(102)

By (101), the second term in parentheses on the right-hand side of (102) is positive, so

$$D_{PP} + D_{TT} > \sqrt{(D_{PP} + D_{TT})^2 - 4(D_{PP}D_{TT} - D_{PT}D_{TP})},$$
(103)

and therefore, the numerator of (100) is always positive. Letting

$$\lambda_i = \mu_i \sqrt{s}, \ i = 1, 2, \tag{104}$$

 $\lambda_1$  and  $\lambda_2$  are real and positive for  $\mu_1$  and  $\mu_2$  defined by

$$\mu_1 = \sqrt{\frac{(D_{PP} + D_{TT}) - \sqrt{(D_{TT} - D_{PP})^2 + 4D_{PT}D_{TP}}}{2(D_{TT}D_{PP} - D_{PT}D_{TP})}},$$
(105a)

$$\mu_2 = \sqrt{\frac{(D_{PP} + D_{TT}) + \sqrt{(D_{TT} - D_{PP})^2 + 4D_{PT}D_{TP}}}{2(D_{TT}D_{PP} - D_{PT}D_{TP})}}.$$
 (105b)

The solutions for the transformed variables  $\overline{T}$  and  $\overline{P}$  can now be written as

$$\overline{T} = \frac{T_i}{s} + \sum_{i=1}^{2} A_i \exp\left(-\mu_i \sqrt{s} x\right), \qquad (106)$$

$$\overline{P} = \frac{P_i}{s} + \sum_{i=1}^{2} B_i \exp\left(-\mu_i \sqrt{s} x\right), \qquad (107)$$

where the  $\mu_i$  are defined by (105).

Using (97), the  $B_i$  can be expressed in terms of the  $A_i$  by  $B_i = b_i A_i$ , where the  $b_i$  are given by (76). The transformed inner boundary conditions can be used to determine the  $A_i$ . In the uncoupled case, they are

$$\frac{J_{q,inc}}{s} = -\frac{L_{qq}}{T_m} \frac{\partial \overline{T}}{\partial x} \bigg|_{x=0}, \tag{108}$$

$$\frac{J_{v,inc}}{s} = -L_{vv} \frac{\partial \overline{P}}{\partial x} \bigg|_{x=0}, \tag{109}$$

and in the thermal osmosis case, they are

$$\frac{J_{q,inc}}{s} = -\frac{L_{qq}}{T_m} \left. \frac{\partial \overline{T}}{\partial x} \right|_{x=0} - L_{qv} \left. \frac{\partial \overline{P}}{\partial x} \right|_{x=0}, \tag{110}$$

$$\frac{J_{v,inc}}{s} = -\frac{L_{vq}}{T_m} \frac{\partial \overline{T}}{\partial x} \bigg|_{x=0} - L_{vv} \frac{\partial \overline{P}}{\partial x} \bigg|_{x=0}. \tag{111}$$

Substituting the solutions for  $\overline{T}$  and  $\overline{P}$  from (106) and (107) into the transformed boundary conditions above yields the following equations for the  $A_i$ :

$$\frac{J_{q,inc}}{s\sqrt{s}} = \sum_{i=1}^{2} l_{qi} \,\mu_i \,A_i, \tag{112}$$

$$\frac{J_{v,inc}}{s\sqrt{s}} = \sum_{i=1}^{2} l_{vi} \,\mu_i \,A_i, \tag{113}$$

where in the uncoupled case, the  $l_{qi}$  and  $l_{vi}$  are defined by

$$l_{qi} = \frac{L_{qq}}{T_m},\tag{114}$$

$$l_{vi} = b_i L_{vv}, \tag{115}$$

and in the thermal osmosis case, they are defined by

$$l_{qi} = \frac{L_{qq}}{T_m} + b_i L_{qv}, (116)$$

$$l_{vi} = \frac{L_{vq}}{T_m} + b_i L_{vv}. {117}$$

Solving (112) and (113) for the  $A_1$  and  $A_2$  and substituting these results into (106) and (107) give the final forms for the solutions in the transform space:

$$\overline{T} = \frac{T_i}{s} + \frac{1}{\Delta s \sqrt{s}} \sum_{i=1}^{2} \frac{g_i}{\mu_i} \exp\left(-\mu_i \sqrt{s} \, x\right), \tag{118}$$

$$\overline{P} = \frac{P_i}{s} + \frac{1}{\Delta s \sqrt{s}} \sum_{i=1}^{2} \frac{b_i g_i}{\mu_i} \exp\left(-\mu_i \sqrt{s} x\right), \qquad (119)$$

where

$$g_1 = l_{v2} J_{q,inc} - l_{q2} J_{v,inc}, (120a)$$

$$g_2 = l_{q1} J_{v,inc} - l_{v1} J_{q,inc}, (120b)$$

and

$$\Delta = l_{q1}l_{v2} - l_{q2}l_{v1}. \tag{121}$$

In (118) and (119) the  $b_i$  are defined by (76), the  $\mu_i$  by (105), and the  $l_{qi}$  and  $l_{vi}$  are defined by (114) and (115) in the uncoupled case and by (116) and (117) when thermal osmosis and thermal filtration are included.

Using the inversion formulas (70) and (71), the inverted solutions for the uncoupled and thermal osmosis cases are

$$T = T_i + \sum_{i=1}^{2} G_i \left[ 2\sqrt{\frac{t}{\pi}} \exp\left(-\xi_i^2\right) - \mu_i x \operatorname{erfc}(\xi_i) \right], \tag{122}$$

$$P = P_i + \sum_{i=1}^{2} b_i G_i \left[ 2\sqrt{\frac{t}{\pi}} \exp\left(-\xi_i^2\right) - \mu_i x \operatorname{erfc}(\xi_i) \right], \tag{123}$$

where the  $b_i$  are defined by (76) and the  $\mu_i$  by (105) and as in the first section,  $G_i = g_i/(\Delta \mu_i)$  and  $\xi_i = \mu_i x/(2\sqrt{t})$ , where  $\Delta$  is defined by (121) and the  $g_i$  by (120).

The solution for  $C_s$  remains to be determined. Substituting the expressions for  $\overline{T}$  and  $\overline{P}$  from (118) and (119) into (96), the governing equation for  $\overline{C}_s$ , yields

$$D_{SS} \nabla^2 \overline{C}_s - s \overline{C}_s = -\frac{1}{\sqrt{s}} \sum_{i=1}^2 \left( D_{ST} + b_i D_{SP} \right) G_i \mu_i^2 \exp\left( -\mu_i \sqrt{s} x \right) - C_{s,i}, \tag{124}$$

which may be solved using the method of undetermined coefficients (Boyce and DiPrima, 1969). The first step is to find the general solution to the homogeneous equation, and the second is to look for a particular solution to the nonhomogeneous equation. Combining the results from the two steps gives the final solution.

The homogeneous equation is

$$D_{SS} \nabla^2 \overline{C}_s - s \overline{C}_s = 0, \tag{125}$$

which has as its general solution

$$\overline{C}_{s,H} = E_1 \exp\left(-x\sqrt{\frac{s}{D_{SS}}}\right) + E_2 \exp\left(x\sqrt{\frac{s}{D_{SS}}}\right),\tag{126}$$

where the  $E_i$  are constants. A particular solution to the nonhomogeneous equation is

$$\overline{C}_{s,N} = \frac{C_{s,i}}{s} + \sum_{i=1}^{2} F_i \exp\left(-\mu_i \sqrt{s} x\right), \qquad (127)$$

where  $F_1$  and  $F_2$  are constants. Substituting this expression into (124) and solving for the  $F_i$  yield

$$F_i = \frac{f_i G_i}{s\sqrt{s}},\tag{128}$$

where

$$f_i = \frac{(D_{ST} + b_i D_{SP}) \mu_i^2}{1 - D_{SS} \mu_i^2}.$$
 (129)

The general solution to (124) is the sum of  $\overline{C}_{s,H}$  and  $\overline{C}_{s,N}$ . The constant  $E_2$  in  $\overline{C}_{s,H}$  must, however, be zero in order for the boundary condition at infinity to be satisfied. The solution for  $\overline{C}_s$  can now be written as

$$\overline{C}_s = \frac{C_{s,i}}{s} + E_1 \exp\left(-x\sqrt{\frac{s}{D_{SS}}}\right) + \sum_{i=1}^2 F_i \exp\left(-\mu_i \sqrt{s} x\right), \tag{130}$$

where the  $F_i$  are given by (128) and  $E_1$  is to be determined from the transformed inner boundary condition, which for both the uncoupled and thermal osmosis cases is

$$\frac{J_{s,inc} - C_{s,m} J_{v,inc}}{s \left(1 - C_{s,m} \overline{V}_{s}\right)} = -L_{ss} \frac{RT_{m}}{C_{s,m} M_{s}} \frac{\partial \overline{C}_{s}}{\partial x} \bigg|_{x=0}.$$
(131)

Substituting the expression for  $\overline{C}_s$  from (130) in the equation above and solving for  $E_1$  yield

$$E_1 = \frac{e_1}{s\sqrt{s}},\tag{132}$$

where

$$e_1 = \frac{\sqrt{D_{SS}} C_{s,m} M_s}{L_{ss} R T_m} \left( \frac{J_{s,inc} - C_{s,m} J_{v,inc}}{1 - C_{s,m} \overline{V}_s} \right) - \sqrt{D_{SS}} \sum_{i=1}^{2} \mu_i f_i G_i.$$
 (133)

The final form for  $\overline{C}_s$  is

$$\overline{C}_s = \frac{C_{s,i}}{s} + \frac{e_1}{s\sqrt{s}} \exp\left(-x\sqrt{\frac{s}{D_{SS}}}\right) + \frac{1}{s\sqrt{s}} \sum_{i=1}^2 f_i G_i \exp\left(-\mu_i \sqrt{s} x\right). \tag{134}$$

Using (70) and (71) to invert  $\overline{C}_s$  gives

$$C_s = C_{s,i} + e_1 \left[ 2\sqrt{rac{t}{\pi}} \exp\left(-\zeta^2
ight) - x \operatorname{erfc}(\zeta) 
ight]$$

$$+\sum_{i=1}^{2} f_{i} G_{i} \left[ 2 \sqrt{\frac{t}{\pi}} \exp\left(-\xi_{i}^{2}\right) - \mu_{i} x \operatorname{erfc}(\xi_{i}) \right], \tag{135}$$

where

$$\zeta = \frac{x}{2\sqrt{t\,D_{SS}}},\tag{136}$$

 $D_{SS}$  is defined by (10),  $e_1$  by (133), the  $f_i$  by (129),  $G_i = g_i/(\Delta \mu_i)$ , the  $g_i$  by (120),  $\Delta$  by (121), the  $\mu_i$  by (105) and  $\xi_i = \mu_i x/(2\sqrt{t})$ .

Because of the complicated form of the solutions, it is exceedingly difficult to algebraically prove that the solutions for T, P and  $C_s$  in (73) through (75) reduce to those in (122), (123) and (135) in the uncoupled case and when thermal osmosis and thermal filtration are included. The equivalence of the solutions has been verified numerically by calculating the solutions for the uncoupled and thermal osmosis cases from the first section and comparing the results to those obtained by calculating the solutions derived in this section. The procedure used to calculate the latter is outlined in the last section.

# Solutions for the Uncoupled and Thermal Osmosis Cases in a Radial Geometry

For the uncoupled and thermal osmosis cases, the simplified system of transformed equations is given by (94) to (96) with  $\nabla^2 = \frac{\partial^2}{\partial r^2} + (1/r)\frac{\partial}{\partial r}$ . Assuming solutions of the form of (78) and (79) for  $\overline{T}$  and  $\overline{P}$  and following the procedure used in the previous section lead to the following expressions:

$$s\overline{T} - T_i = \sum_{i=1}^2 A_i K_0 \left( \mu_i \sqrt{s} \, r \right), \tag{137}$$

$$s\overline{P} - P_i = \sum_{i=1}^2 b_i A_i K_0 \left( \mu_i \sqrt{s} r \right), \qquad (138)$$

where the  $b_i$  are given by (76), the  $\mu_i$  by (105), and the  $A_i$  are to be determined from the inner boundary conditions. In the uncoupled case, the boundary conditions are

$$\frac{J_{q,inc}}{s} = -\frac{L_{qq}}{T_m} \frac{\partial \overline{T}}{\partial r} \bigg|_{r=a},\tag{139}$$

$$\frac{J_{v,inc}}{s} = -L_{vv} \frac{\partial \overline{P}}{\partial r} \bigg|_{r=a}, \tag{140}$$

and in the thermal osmosis case, they are

$$\frac{J_{q,inc}}{s} = -\frac{L_{qq}}{T_m} \frac{\partial \overline{T}}{\partial r} \bigg|_{r=a} -L_{qv} \frac{\partial \overline{P}}{\partial r} \bigg|_{r=a}, \tag{141}$$

$$\frac{J_{v,inc}}{s} = -\frac{L_{vq}}{T_m} \frac{\partial \overline{T}}{\partial r} \bigg|_{r=a} -L_{vv} \frac{\partial \overline{P}}{\partial r} \bigg|_{r=a}. \tag{142}$$

Substituting the solutions for  $\overline{T}$  and  $\overline{P}$  from (137) and (138) into the equations above yields the following equations for the  $A_i$ :

$$\frac{J_{q,inc}}{s\sqrt{s}} = \sum_{i=1}^{2} l_{qi} \,\mu_i \,A_i \,K_1 \,(\mu_i \,\sqrt{s} \,a) \,, \tag{143}$$

$$\frac{J_{v,inc}}{s\sqrt{s}} = \sum_{i=1}^{2} l_{vi} \, \mu_i \, A_i \, K_1 \, (\mu_i \, \sqrt{s} \, a) \,, \tag{144}$$

where in the uncoupled case, the  $l_{qi}$  and  $l_{vi}$  are given by (114) and (115) and when thermal osmosis and thermal filtration are included by (116) and (117). Solving (143) and (144) for the  $A_i$  and substituting the results into (137) and (138) give the final expressions for  $\overline{T}$  and  $\overline{P}$ :

$$\overline{T} = \frac{T_i}{s} + \frac{1}{s\sqrt{s}} \sum_{i=1}^{2} G_i \frac{K_0(\mu_i \sqrt{s} r)}{K_1(\mu_i \sqrt{s} a)},$$
(145)

$$\overline{P} = \frac{P_i}{s} + \frac{1}{s\sqrt{s}} \sum_{i=1}^{2} b_i G_i \frac{K_0(\mu_i \sqrt{s} r)}{K_1(\mu_i \sqrt{s} a)},$$
(146)

where the  $b_i$  are defined by (76),  $G_i = g_i/(\Delta \mu_i)$ , the  $g_i$  are defined by (120),  $\Delta$  by (121) and the  $\mu_i$  by (105).

The solution for  $\overline{C}_s$  is obtained by substituting  $\overline{P}$  from (138) into (96) and following the steps given in the fourth section. The general solution to the homogeneous equation (125) is

$$\overline{C}_{s,H} = E_1 K_0 \left( r \sqrt{s/D_{SS}} \right) + E_2 I_0 \left( r \sqrt{s/D_{SS}} \right), \tag{147}$$

where the  $E_i$  are constants. The nonhomogeneous equation is

$$D_{SS} \nabla^{2} \overline{C}_{s} - s \overline{C}_{s} = -\frac{1}{\Delta \sqrt{s}} \sum_{i=1}^{2} (D_{ST} + b_{i} D_{SP}) g_{i} \mu_{i} \frac{K_{0} (\mu_{i} \sqrt{s} r)}{K_{1} (\mu_{i} \sqrt{s} a)} - C_{s,i},$$
 (148)

a particular solution of which is

$$\overline{C}_{s,N} = \frac{C_{s,i}}{s} + \sum_{i=1}^{2} F_{i} \frac{K_{0} (\mu_{i} \sqrt{s} r)}{K_{1} (\mu_{i} \sqrt{s} a)}, \tag{149}$$

where the  $F_i$  are defined by (128). The general solution to (148) is the sum of  $\overline{C}_{s,H}$  and  $\overline{C}_{s,N}$ . Because  $I_0(\mu_i\sqrt{s}r)$  increases exponentially as r increases, the constant  $E_2$  in  $\overline{C}_{s,H}$  must be zero in order for

the boundary condition at infinity to be satisfied. Combining the expressions from (147) and (149), the solution for  $\overline{C}_s$  can be written

$$\overline{C}_{s} = \frac{C_{s,i}}{s} + E_{1} K_{0} \left( r \sqrt{s/D_{SS}} \right) + \sum_{i=1}^{2} F_{i} \frac{K_{0} \left( \mu_{i} \sqrt{s} r \right)}{K_{1} \left( \mu_{i} \sqrt{s} a \right)}, \tag{150}$$

where the only remaining unknown,  $E_1$ , can be determined using the inner boundary condition for  $\overline{C}_3$ . For both the uncoupled and thermal osmosis cases, the boundary condition is

$$\frac{J_{s,inc} - C_{s,m} J_{v,inc}}{s \left(1 - C_{s,m} \overline{V}_{s}\right)} = -L_{ss} \frac{RT_{m}}{C_{s,m} M_{s}} \frac{\partial \overline{C}_{s}}{\partial r} \bigg|_{r=a}.$$
(151)

Substituting the expression for  $\overline{C}_s$  from (150) in the equation above and solving for  $E_1$  yield

$$E_1 = \frac{e_1}{s\sqrt{s}\,K_1\left(a\sqrt{s/D_{SS}}\right)},\tag{152}$$

where  $e_1$  is defined by (133). The final expression for  $\overline{C}_s$  is

$$\overline{C}_{s} = \frac{C_{s,i}}{s} + \frac{e_{1}}{s\sqrt{s}} \frac{K_{0}\left(r\sqrt{s/D_{SS}}\right)}{K_{1}\left(a\sqrt{s/D_{SS}}\right)} + \frac{1}{s\sqrt{s}} \sum_{i=1}^{2} f_{i} G_{i} \frac{K_{0}\left(\mu_{i}\sqrt{s}r\right)}{K_{1}\left(\mu_{i}\sqrt{s}a\right)}.$$
(153)

where  $D_{SS}$  is defined by (10),  $e_1$  by (133), the  $f_i$  by (129),  $G_i = g_i/(\Delta\mu_i)$ , the  $g_i$  by (120),  $\Delta$  by (121), and the  $\mu_i$  by (105). As noted in the second section, the solutions in (145), (146) and (153) may be analytically inverted using (70) and (93) or numerically inverted using the Stehfest (1970) algorithm. The procedure for calculating  $\overline{T}$ ,  $\overline{P}$  and  $\overline{C}_s$  is outlined in the next section.

#### Computational Procedure for the Uncoupled and Thermal Osmosis Cases

For completeness, the procedure for calculating the analytical solutions for the uncoupled and thermal osmosis cases for the one-dimensional and radial geometries, derived in the fourth and fifth section, respectively, is outlined in this section. The computational procedure outlined in the third section could also be used.

- 1. calculate the  $D_{IJ}$  from (20),
- 2. calculate the  $\mu_i$  from (105),
- 3. calculate the  $b_i$  from (76),
- 4. calculate the  $l_{qi}$  and  $l_{vi}$  for the uncoupled case from (114) and (115), and calculate the  $l_{qi}$  and  $l_{vi}$  when thermal osmosis and thermal filtration are included from (116) and (117),
- 5. calculate  $J_{v,inc}$  from the incoming solvent and solute fluxes,  $J_{0,inc}$  and  $J_{s,inc}$ , using  $J_{v,inc} = J_{0,inc} \overline{V}_0 + J_{s,inc} \overline{V}_s$ ,
- 6. calculate the  $g_i$  from (120) and  $\Delta$  from (121),
- 7. calculate the  $G_i$  from  $G_i = g_i/(\Delta \mu_i)$ ,

- 8. calculate the  $f_i$  from (129),
- 9. calculate  $e_1$  from (133),
- 10. in the one-dimensional case, calculate T, P and  $C_s$  from (122), (123) and (135) using  $\xi_i = \mu_i \, x/2 \, \sqrt{t}$  and  $\zeta = x/2 \, \sqrt{t \, D_{SS}}$ , and in the radial case, calculate  $\overline{T}$ ,  $\overline{P}$  and  $\overline{C}_s$  from (145), (146) and (153) and numerically invert them to obtain T, P and  $C_s$ .

In steps 5 through 10 above, i = 1, 2.

#### NOTATION

a	location of inner boundary in axisymmetric case	m
$C_s$	concentration of solute	kg/m³
$\overline{C}_s$	Laplace transform of solute concentration	${ m kg\cdot s/m^3}$
$C_{s,i}$	initial value of solute concentration	kg/m <sup>3</sup>
$C_{s,m}$	average concentration of solute	kg/m³
$C_0$	concentration of solvent	kg/m <sup>3</sup>
$c_{p,f}$	specific heat capacity of fluid phase at constant pressure	$J/(K \cdot kg)$
$c_{p,n}$	specific heat capacity of solid phase at constant pressure	$J/(K \cdot kg)$
$c_{v,f}$	specific heat capacity of fluid phase at constant volume	$J/(K \cdot kg)$
$c_{v,n}$	specific heat capacity of solid phase at constant volume	$J/(K \cdot kg)$
$J_{q}$	heat flux	$W/m^2$
$J_{q,inc}$	incoming heat flux at inner boundary	$W/m^2$
$J_s$	solute flux (laboratory frame of reference)	$kg/m^2 \cdot s$
$J_{s,inc}$	incoming solute flux (laboratory frame of reference) at inner boundary	kg/m²⋅s
$J_s^{o}$	solute flux (defined relative to motion of solvent)	kg/m²⋅s
$J_{s,inc}^{o}$	incoming solute flux (defined relative to motion of solvent) at inner	<u>.</u>
	boundary	kg/m²⋅s
$J_{m{v}}$	volume flux	m/s
$J_{v,inc}$	incoming volume flux at inner boundary	m/s
$J_0$	solvent flux (laboratory frame of reference)	kg/m²⋅s
$J_{0,inc}$	incoming solvent flux (laboratory frame of reference) at inner boundary	$ m kg/m^2 \cdot s$
$L_{qs}$	coefficient of Dufour effect	$ m kg/m\cdot s$
$L_{sq}$	coefficient of thermal diffusion	kg/m·s
$L_{ss}$	coefficient of mass diffusion (Fick's law)	$ m kg^2/J \cdot m \cdot s$
$L_{sv}$	coefficient of ultrafiltration	${ m kg\cdot m^2/J\cdot s}$
$L_{vq}$	coefficient of thermal osmosis	$m^2/s$
$L_{vs}$	coefficient of chemical osmosis	${ m kg\cdot m^2/J\cdot s}$
$L_{oldsymbol{v}oldsymbol{v}}$	coefficient of advection (Darcy's Law)	$\mathrm{m}^5/\mathrm{J}{\cdot}\mathrm{s}$
$M_s$	molecular weight of solute	kg/mole
P	pressure	Pa
$\overline{P}$	Laplace transform of pressure	$\mathbf{Pa} \cdot \mathbf{s}$
$P_{i}$	initial value of pressure	Pa
r	radial distance	m
R	universal gas constant	J/K·mole
s	Laplace transform variable	$s^{-1}$
t	time	s

T	temperature	K
$\overline{T}$	Laplace transform of temperature	K⋅s
$T_{m i}$	initial value of temperature	K
$T_{m}$	average temperature	K
$\overline{V}_s$	partial specific volume of solute	$m^3/kg$
$\boldsymbol{x}$	distance	m
$oldsymbol{eta_f}$	coefficient of thermal expansion of fluid phase	$K^{-1}$
$eta_n$	coefficient of thermal expansion of solid phase	$K^{-1}$
$\epsilon_f$	volume fraction of fluid phase	
$\epsilon_n$	volume fraction of solid phase	
$\kappa_f$	coefficient of isothermal compressibility of fluid phase	$m^2/N$
$\kappa_n$	coefficient of isothermal compressibility of solid phase	$m^2/N$
$ ho_f$	density of fluid phase	$kg/m^3$
$\rho_n$	density of solid phase	$kg/m^3$

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#### REFERENCES

- Boyce, W. E., and DiPrima, R. C., 1969. Elementary Differential Equations and Boundary Value Problems. John Wiley & Sons, New York.
- Burrington, R. S., 1949. Handbook of Mathematical Tables and Formulas. Handbook Publishers, Sandusky, Ohio.
- Carnahan, C. L., and Jacobsen, J. S., 1990. Simulation of Coupled Processes in Semipermeable Media: Part I. Theoretical Basis. Lawrence Berkeley Laboratory Report LBL-25618.
- Carslaw, H. S., and Jaeger, J. C., 1959. Conduction of Heat in Solids, 2nd edition. Oxford University Press, London.
- Jacobsen, J. S., and Carnahan, C. L., 1990. Simulation of Coupled Processes in Semipermeable Media: Part II. Numerical Methods and Results. Lawrence Berkeley Laboratory Report LBL-25619.
- Katchalsky, A., and Curran, P. F., 1967. Nonequilibrium Thermodynamics in Biophysics. Harvard University Press, Cambridge, Massachusetts.
- Stehfest, H., 1970. Algorithm 368. Numerical inversion of Laplace transforms. ACM Comm., 13, 47-49.

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