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Publication Date

2024-04-25

DOI

10.1017/jfm.2024.297

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Effects of buoyancy on the dispersion of drugs released intrathecally in the spinal canal

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(Received xx; revised xx; accepted xx)

This paper investigates the transport of drugs delivered by direct injection into the cerebrospinal fluid (CSF) that fills the intrathecal space surrounding the spinal cord. Because of the small drug diffusivity, the dispersion of neutrally buoyant drugs has been shown in previous work to rely mainly on the mean Lagrangian flow associated with the CSF oscillatory motion. Attention is given here to effects of buoyancy, arising when the drug density differs from the CSF density. For the typical density differences found in applications, the associated Richardson number is shown to be of order unity, so that the Lagrangian drift includes a buoyancy-induced component that depends on the spatial distribution of the drug, resulting in a slowly evolving cycle-averaged flow problem that can be analyzed with two-time scale methods. The asymptotic analysis leads to a nonlinear integro-differential equation for the spatiotemporal solute evolution that describes accurately drug dispersion at a fraction of the cost involved in direct numerical simulations of the oscillatory flow. The model equation is used to predict drug dispersion of positively and negatively buoyant drugs in an anatomically correct spinal canal, with separate attention given to drug delivery via bolus injection and constant infusion.

Key words:

1. Introduction

The subarachnoid space (SAS) surrounding the spinal cord is filled with cerebrospinal fluid (CSF), a colorless Newtonian fluid whose density ρ and kinematic viscosity ν are very similar to those of water. The CSF moves in response to the cyclic pressure variations induced by the blood pulsations in the cranial cavity and to the abdominal pressure variations associated with the respiratory cycle (Linninger *et al.* 2016; Kelley & Thomas 2023). CSF motion plays a fundamental role in the physiological function of CSF as a vehicle for the transport of hormones, nutrients, and neuroendocrine substances (Greitz *et al.* 1993; Greitz & Hannerz 1996; Pollay 2010) and also facilitates the dispersion of

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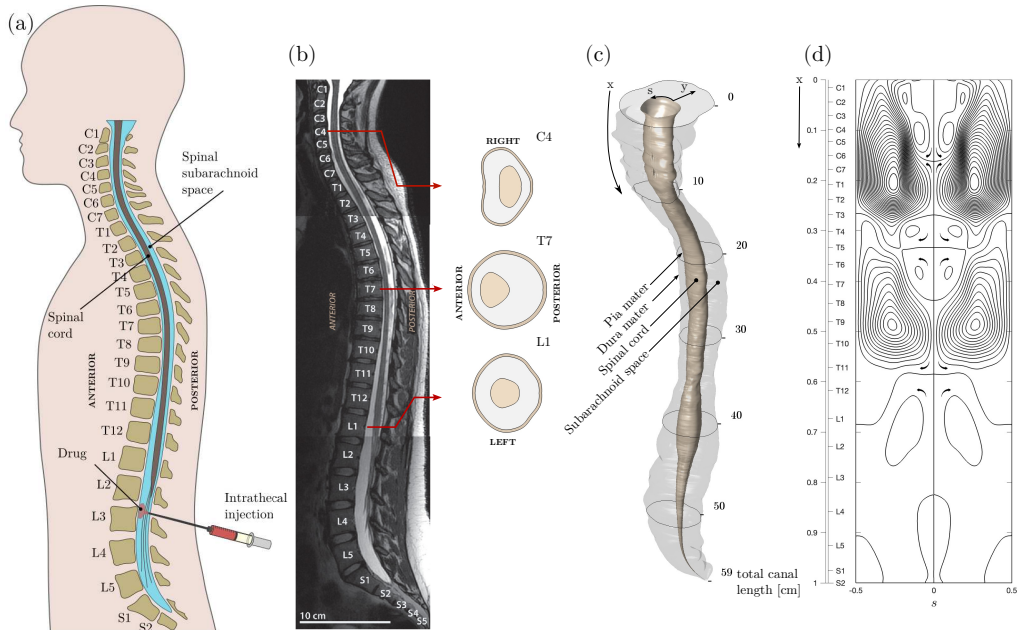


FIGURE 1. The spinal canal, including (a) a schematic showing the typical intrathecal injection location, (b) sagittal T2-weighted MR image of the spine in a subject in the supine position, including cross-sectional views at three different locations, (c) transversely stretched three-dimensional view of the spinal canal obtained after Gaussian smoothing the MR images, with an indication of the bounding surfaces and the dimensionless coordinate system used in the model derivation, and (d) streamlines of the Lagrangian flow projected onto the dimensionless plane $x - s$ (see § 6).

38 drugs delivered by direct injection into the SAS (Hettiarachchi *et al.* 2011a). This medical
 39 procedure, known as intrathecal drug delivery (ITDD), has been used since the early
 40 1980s to bypass the blood-brain barrier, facilitating the administration of analgesics,
 41 chemotherapy and enzymes to the central nervous system (Onofrio *et al.* 1981; Greene
 42 1985; Patel *et al.* 2012; Calias *et al.* 2012; Lynch 2014; Lee *et al.* 2017; Remes *et al.* 2013;
 43 Bottros & Christo 2014; Tangen *et al.* 2019; Fowler *et al.* 2020; De Andres *et al.* 2022).
 44 Standard ITDD protocols involve either the continuous pumping of the drug through a
 45 small catheter or the administration of a finite dose at selected times (Bottros & Christo
 46 2014; Fowler *et al.* 2020; De Andres *et al.* 2022), with drug delivery commonly taking
 47 place in the lumbar region, as shown in the schematic of figure 1(a). Analgesic delivery
 48 via ITDD usually targets sites along the spinal cord close to the injection location, so
 49 that reduced drug dispersion is desired, while for other patients there is interest in rapid
 50 dispersion towards the cranial cavity, that being the case of intrathecal chemotherapy
 51 for brain tumors.

52 Although ITDD is used with satisfactory results, efforts to optimize the delivery
 53 protocol are hindered by the lack of an accurate methodology for predicting drug-
 54 delivery rates to targeted locations, which sometimes results in unexpected over-dosing
 55 and under-dosing complications (Buchser *et al.* 2004; Wallace & Yaksh 2012) that cannot
 56 be explained by existing pharmacokinetics knowledge (Kamran & Wright 2001; Pardridge
 57 2011). The development of predictive models necessitates improved understanding of the
 58 interacting convective and diffusive mechanisms controlling the transport of the drug.
 59 The present paper, complementing previous computational (Myers 1996; Kuttler *et al.*

2010; Hsu *et al.* 2012; Tangen *et al.* 2015; Haga *et al.* 2017; Tangen *et al.* 2017; Khani *et al.* 2018; Gutiérrez-Montes *et al.* 2021; Khani *et al.* 2022), experimental (Hettiarachchi *et al.* 2011*b*; Khani *et al.* 2022; Seiner *et al.* 2022; Moral-Pulido *et al.* 2023; Ayansiji *et al.* 2023), and theoretical (Sánchez *et al.* 2018; Lawrence *et al.* 2019) efforts, seeks to contribute to the needed understanding by analyzing effects of buoyancy, which are known by clinicians to play an important role in the dispersion rate of ITDD drugs for patients in an upright or sitting position (Wildsmith *et al.* 1981; Chambers *et al.* 1981; Greene 1985; Hocking & Wildsmith 2004; De Andres *et al.* 2022). Asymptotic methods based on the disparity of length and time scales present in the problem will be used to derive a reduced transport equation for the drug, enabling accurate predictions of drug dispersion at a fraction of the computational cost associated with direct numerical simulations.

The rest of the paper is organized as follows. After reviewing in § 2 the main features of the flow in the spinal canal, the problem of solute dispersion in the presence of buoyancy forces will be formulated in § 3. The asymptotic development leading to the reduced transport equation describing drug dispersion is presented next in § 4. The simplified model will be used in § 5 to compute dispersion of positively and negatively buoyant solutes in geometrically simple models of the spinal canal. The results will be validated by comparisons with direct numerical simulations, similar to those performed earlier in connection with neutrally buoyant solutes (Gutiérrez-Montes *et al.* 2021). Computations accounting for anatomically correct spinal canals are presented next, with separate consideration given to drug delivery via bolus injection (§ 6) and constant infusion (§ 7), the latter analysis involving a localized solute source with a rescaled effective Richardson number. Finally, concluding remarks are given in § 8.

2. Flow and transport in the spinal canal

The SAS surrounding the spinal chord can be described in the first approximation as a thin annular channel of characteristic width $h_c \sim 0.1 - 0.4$ cm much smaller than the characteristic spinal-chord perimeter $\ell_c \sim 2 - 3$ cm, which in turn is much smaller than the spine length $L \sim 60$ cm, so that the canal dimensions satisfy the inequalities $L \gg \ell_c \gg h_c$. The CSF moves along the canal with an oscillatory velocity that is synchronized with the cardiac and respiratory cycles. The CSF oscillatory flow is more pronounced near the canal entrance, where the characteristic velocities u_c are on the order of a few cm s^{-1} , but become progressively smaller on approaching the closed end of the canal, as revealed by in vivo magnetic-resonance measurements (Haughton & Mardal 2014; Coenen *et al.* 2019; Aktas *et al.* 2019; Sincomb *et al.* 2022). The following analysis specifically focuses on the flow induced by the cardiac cycle, corresponding to angular frequencies $\omega \simeq 2\pi \text{ s}^{-1}$ and characteristic stroke lengths $L_s = u_c/\omega \sim 1$ cm much smaller than the canal length L .

The motion in the spinal canal is viscous, in that the characteristic viscous time across the canal h_c^2/ν based on the CSF kinematic viscosity $\nu \simeq 0.7 \times 10^{-3} \text{ cm}^2/\text{s}$ is comparable to—although somewhat larger than—the characteristic flow-oscillation time ω^{-1} , resulting in order-unity values $3 \lesssim \alpha \lesssim 12$ of the Womersley number $\alpha = (h_c^2\omega/\nu)^{1/2}$. By way of contrast, effects of inertia associated with convective acceleration are very limited, as measured by the relevant Strouhal number $\omega L/u_c = L/L_s \gg 1$, the inverse of which defines an asymptotically small parameter $\varepsilon \sim L_s/L \simeq 0.02 - 0.04$. Thus, in the first approximation the motion in the slender spinal canal is given by a balance between the pressure gradient, the local acceleration and the viscous forces. The resulting linear unsteady lubrication problem can be solved to give closed-form expressions for the leading-order oscillatory velocity (Sánchez *et al.* 2018; Lawrence *et al.* 2019), whose

time-averaged value is identically zero. Corrections to this solution can be obtained by extending the asymptotic analysis to higher orders in $\varepsilon \ll 1$ (Sánchez *et al.* 2018; Lawrence *et al.* 2019). The first-order velocity corrections, of order εu_c , exhibit non-zero time-averaged values. This *steady-streaming* velocity, first identified in the seminal computational work of Kuttler *et al.* (2010), is partly due to the effect of convective acceleration and partly due to the canal compliance (see, e.g. Bhosale *et al.* 2022a,b; Cui *et al.* 2024, for recent analyses of steady-streaming flows stemming from boundary compliance). The associated residence times for the bulk flow in the canal $L/(\varepsilon u_c) = \varepsilon^{-2}\omega^{-1} \sim 30$ min are of the order of those observed in *in vivo* experiments employing radioactive tracers to mark the displacement of the CSF particles (Di Chiro 1964; Greitz & Hannerz 1996).

As shown by Lawrence *et al.* (2019), the disparity between the short time ω^{-1} characterizing the oscillatory velocity fluctuations and the residence time $\varepsilon^{-2}\omega^{-1}$ associated with the bulk motion can be used in deriving a simplified transport equation for the drug. The analysis revealed that shear-enhanced diffusion (Watson 1983), which is potentially important for solutes with order-unity values of the Schmidt number $S = \nu/\kappa$, is entirely negligible for the large Schmidt numbers $S \gg 1$ corresponding to the small molecular diffusivities κ of typical ITDD drugs (e.g. for methotrexate $\kappa = 5.26 \times 10^{-10}$ m²/s, yielding $S \simeq 1330$ for $\nu = 0.7 \times 10^{-6}$ m²/s). The evolution of the drug concentration in the long time scale $\varepsilon^{-2}\omega^{-1}$ was found to be governed by a transport equation involving molecular diffusion across the width of the canal and convective transport driven by the time-averaged Lagrangian motion resulting from the combined effects of steady streaming and Stokes drift. The use of this simplified equation effectively circumvents the need to describe the small concentration fluctuations occurring in the short time scale ω^{-1} , thereby drastically reducing computational times. The accuracy and limitations of this time-averaged description have been recently tested by means of comparisons with results of direct numerical simulations spanning hundreds of oscillation cycles (Gutiérrez-Montes *et al.* 2021), as needed to generate significant dispersion of the solute. The comparisons clearly demonstrate the accuracy of the time-averaged description, which is seen to provide excellent fidelity at a fraction of the computational cost involved in the direct numerical simulations. The present investigation extends our previous analyses of flow and transport in the spinal canal by accounting for the effects of the small density differences between the drug and the CSF. The mathematical development parallels that employed recently in our analysis of buoyant Lagrangian drift in a vertical wavy-walled channel (Alaminos-Quesada *et al.* 2022).

3. Problem description

3.1. The Richardson number

As can be seen in Table 1, the drug density ρ_d of common intrathecal drug solutions is very close to that of the CSF ($\rho = 1.00059$ g/cm³ at 37° C) (Lui *et al.* 1998; Nicol & Holdcroft 1992; Hejtmanek *et al.* 2011; Lynch 2014; McLeod 2004). The drug density can be modified by adding different diluents such as saline, glucose and dextrose. Even though the resulting relative differences are very small (i.e. $10^{-4} \lesssim |\rho - \rho_d|/\rho \lesssim 10^{-2}$), the associated buoyancy forces affect in a fundamental way the dispersion of the drug. Thus, it has been seen that for hyperbaric (i.e. dense) drugs, the transport of the drug is restricted when the patient is seated for some time before moving to a supine position (Mitchell *et al.* 1988; Povey *et al.* 1989; Veering *et al.* 2001; Loubert *et al.* 2011). Conversely, when a hypobaric (light) drug is injected, faster cephalic dispersion occurs in

Drug	ρ_d (g/cm ³)	$\frac{\rho - \rho_d}{\rho}$	$Ri_{\varepsilon=0.04}$	$Ri_{\varepsilon=0.02}$
Fentanyl (50 μ g/mL)	0.99320	7.386×10^{-3}	1.963	7.765
Droperidol (2.5 mg/mL)	0.99440	6.186×10^{-3}	1.601	6.405
Midazolam (1 mg/mL)	0.99970	0.889×10^{-3}	0.230	0.921
Lidocaine (20 mg/mL)	0.99990	0.690×10^{-3}	0.178	0.714
Epinephrine (1 mg/mL)	1.00050	0.090×10^{-3}	0.0236	0.093
Bupivacaine (10 mg/mL)	1.00072	-0.130×10^{-3}	-0.033	-0.135
Lidocaine CO ₂ (20 mg/mL)	1.00100	-0.410×10^{-3}	-0.106	-0.424
Morphine (10 mg/mL)	1.00157	-0.979×10^{-3}	-0.254	-1.014
Meperidine (100 mg/mL)	1.00830	-7.206×10^{-3}	-1.994	-7.98

TABLE 1. A few common intrathecal drugs, their densities (Lui *et al.* 1998; Nicol & Holdcroft 1992; Hejtmanek *et al.* 2011), and associated Richardson numbers $Ri = [g(\rho - \rho_d)]/(\rho\varepsilon^2\omega^2L)$, the latter evaluated with $g = 9.81$ m/s², $L = 0.6$ m and $\rho = 1.00059$ g/cm³ for two different values of the reduced stroke length ε .

155 a seated injection position than in a lateral injection position (Richardson *et al.* 1996).
 156 As expected, the density of the drug is inconsequential when injection occurs in the
 157 lateral position (Hallworth *et al.* 2005) or when the solution density matches that of CSF
 158 (Wildsmith *et al.* 1981).

159 To anticipate how the presence of buoyancy forces modifies drug dispersion for patients
 160 in sitting or upright position, it is useful to compare the characteristic value of the
 161 buoyancy-induced acceleration $g(\rho - \rho_d)/\rho$ with the characteristic value of the convective
 162 acceleration along the canal u_c^2/L , their ratio defining the relevant Richardson number

$$163 \quad Ri = \frac{g(\rho - \rho_d)/\rho}{u_c^2/L} = \frac{g(\rho - \rho_d)/\rho}{\varepsilon^2\omega^2L}. \quad (3.1)$$

164 Typical values of this number are evaluated in Table 1 for a few common intrathecal drugs
 165 and two different values of the reduced stroke length ε . As can be seen, values of Ri of
 166 order unity characterize most situations of practical interest, so that in ITDD processes
 167 buoyancy acceleration can be anticipated to be comparable to convective acceleration.
 168 As previously discussed, the motion of CSF at leading order is given by an unsteady
 169 lubrication balance involving the local acceleration and the viscous and pressure forces,
 170 with convective acceleration introducing small corrections of order ε , responsible for the
 171 steady-streaming motion. This leading-order balance is not altered in the relevant limit
 172 $Ri \sim 1$ that applies to intrathecal drugs, in which the associated buoyancy-induced
 173 velocities are comparable to the steady-streaming velocities (and therefore a factor ε
 smaller than the pulsating velocities).

174 3.2. The model problem

175 The problem is formulated in dimensionless form using the scales and notation em-
 176 ployed in the previous buoyancy-free analysis of Lawrence *et al.* (2019), which can be
 177 consulted for details of the derivation. Attention is focused on the motion driven by the
 178 periodic intracranial pressure fluctuations associated with the arterial blood flow, to be
 179 described for simplicity with the simple sinusoidal function $(\Delta p)_c \cos(\omega t')$, where $(\Delta p)_c$
 180 is the fluctuation amplitude and $\omega \simeq 2\pi$ s⁻¹ is the angular frequency of the cardiac cycle,
 181 with t' representing the time. The spinal SAS is modelled as an annular canal bounded
 182 internally by the pia mater, surrounding the spinal chord, and externally by the dura

183 membrane. The canal is compliant because of the presence of fatty tissue and venous
 184 blood. The displacement of the dura membrane at a given location is assumed to be
 185 equal to the product of the local pressure fluctuation and a compliance factor γ' that
 186 may vary along the canal. Its mean value γ'_c can be used to estimate the characteristic
 187 value of the dura displacement $\gamma'_c(\Delta p)_c$, which is much smaller than the canal width,
 188 with the ratio

$$\varepsilon = \frac{\gamma'_c(\Delta p)_c}{h_c} \sim \frac{L_s}{L} \quad (3.2)$$

189 defining the small asymptotic parameter representing the dimensionless stroke length.

190 As indicated in figure 1(c), the problem is described in terms of curvilinear coordinates,
 191 including the longitudinal distance to the canal entrance x (scaled with L), the transverse
 192 distance from the spinal chord y (scaled with the characteristic canal width h_c), and the
 193 azimuthal distance s (scaled with the local spinal-chord perimeter, so that $0 \leq s \leq 1$).
 194 The corresponding streamwise, transverse, and azimuthal velocity components (u, v, w)
 195 are scaled with their characteristic values $u_c = \varepsilon\omega L$, $v_c = \varepsilon\omega h_c$, and $w_c = \varepsilon\omega\ell_c$, the
 196 last two of which follow from continuity. The geometry of the canal is defined by the
 197 dimensionless unperturbed canal width $\bar{h}(x, s)$ (scaled with h_c) and spinal-cord perimeter
 198 $\ell(x)$ (scaled with ℓ_c). The linear elastic equation for the canal takes the form

$$h' = \gamma(\cos t + k^2 p'), \quad (3.3)$$

199 where h' is the dura-membrane displacement (scaled with εh_c), $t = \omega t'$ is the di-
 200 mensionless time, $p'(x, t)$ is the streamwise pressure variation (scaled with $\rho u_c \omega L$),
 201 $k = L\omega / [(h_c/\gamma'_c)/\rho]^{1/2}$ is a dimensionless elastic wavenumber, and $\gamma(x) = \gamma'/\gamma'_c$ is a
 202 dimensionless function describing the streamwise variation of the canal compliance.

203 3.3. Dimensionless formulation

204 In the thin-film approximation that applies in the limit $L \gg \ell_c \gg h_c$, the continuity,
 205 momentum, and solute conservation equations take the simplified form

$$\frac{1}{\ell} \frac{\partial}{\partial x}(\ell u) + \frac{\partial v}{\partial y} + \frac{1}{\ell} \frac{\partial w}{\partial s} = 0, \quad (3.4)$$

$$\frac{\partial u}{\partial t} + \varepsilon \left[u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} + \frac{w}{\ell} \frac{\partial u}{\partial s} \right] = -\frac{\partial p'}{\partial x} + \frac{1}{\alpha^2} \frac{\partial^2 u}{\partial y^2} - \varepsilon Ri c, \quad (3.5)$$

$$\frac{\partial w}{\partial t} + \varepsilon \left[\frac{u}{\ell} \frac{\partial}{\partial x}(\ell w) + v \frac{\partial w}{\partial y} + \frac{w}{\ell} \frac{\partial w}{\partial s} \right] = -\frac{1}{\ell} \frac{\partial \hat{p}}{\partial s} + \frac{1}{\alpha^2} \frac{\partial^2 w}{\partial y^2}, \quad (3.6)$$

$$\frac{\partial c}{\partial t} + \varepsilon \left(u \frac{\partial c}{\partial x} + v \frac{\partial c}{\partial y} + \frac{w}{\ell} \frac{\partial c}{\partial s} \right) = \frac{\varepsilon^2}{\alpha^2 \sigma} \frac{\partial^2 c}{\partial y^2}, \quad (3.7)$$

206 where c is the drug concentration and \hat{p} is an auxiliary function describing the azimuthal
 207 pressure variations. The problem has been formulated using the Boussinesq approxima-
 208 tion, as is appropriate for $|\rho - \rho_d| \ll \rho$. Since the spinal curvature is relatively small, for the
 209 case of a sitting patient considered here the streamwise coordinate x is practically aligned
 210 with the vertical direction, so that the component of the buoyancy force acting in the az-
 211 imuthal direction is small, and has been correspondingly neglected in writing (3.6). With
 212 the definition (3.1), the Richardson number Ri measuring the buoyancy force in (3.5)
 213 is positive/negative when the drug is lighter/heavier than the CSF, buoyancy driving
 214 the drug upwards/downwards, in the negative/positive x direction. Following Lawrence
 215 et al. (2019), the diffusion term in (3.7) has been written in terms of the reduced Schmidt
 216 number $\sigma = \varepsilon^2 S$, assumed to be of order unity, as is consistent with the values $S \sim 2000$
 217 and $\varepsilon \sim 0.02 - 0.04$ that characterize drug dispersion in the spinal canal.

218 The velocity satisfies the non-slip condition $u = v = w = 0$ at $y = 0$ and $u =$
 219 $v - \partial h'/\partial t = w = 0$ at $y = h$. Although drug uptake by the spinal nerve as well as
 220 through the dura membrane could be incorporated in the model by accounting for nonzero
 221 diffusive fluxes at the boundary, for simplicity the following analysis is restricted to non-
 222 permeable bounding surfaces, for which the boundary condition for the concentration
 223 reduces to $\partial c/\partial \eta = 0$ at $y = 0, h$. The pressure drop is negligible at the entrance of the
 224 canal, resulting in the condition $p' = 0$ at $x = 0$. The requirement that the axial volume
 225 flux $\int_0^1 \left(\int_0^h u dy \right) ds$ must vanish at the closed end $x = 1$ completes the set of boundary
 226 conditions needed to determine the flow in the canal.

227 Besides the Richardson number Ri defined in (3.1) and the compliance parameter
 228 $\varepsilon \ll 1$ defined in (3.2), the set of governing parameters includes the Womersley number
 229 $\alpha = h_c/(\nu/\omega)^{1/2}$, the dimensionless elastic wavenumber $k = L\omega/[(h_c/\gamma'_c)/\rho]^{1/2}$, and the
 230 rescaled Schmidt number $\sigma = S\varepsilon^2$. The problem is to be solved in the limit $\varepsilon \ll 1$ with
 231 $\alpha \sim 1$ and $k \sim 1$, as is appropriate for describing CSF flow in the spinal canal, for solutes
 232 with $\sigma = S\varepsilon^2 \sim 1$ and $Ri \sim 1$, the distinguished limit of interest in intrathecal drug
 233 dispersion.

234 4. Solute transport in the presence of buoyancy

235 Following our previous analyses (Sánchez *et al.* 2018; Lawrence *et al.* 2019; Alaminos-
 236 Quesada *et al.* 2022), the problem defined above is solved by expressing the different
 237 variables as expansions in powers of ε (e.g. $u = u_0 + \varepsilon u_1 + \dots$) and solving sequentially the
 238 equations that arise when collecting terms at different orders in ε . In the development,
 239 it is convenient to replace the transverse coordinate y by its normalized counterpart
 240 $\eta = y/h$, with $0 \leq \eta \leq 1$. The velocity field depends on the solute concentration through
 241 the buoyancy term appearing in (3.5), although the dependence is weak, since $\varepsilon \ll 1$. The
 242 distribution of c can be anticipated to vary over times of the order of the residence time
 243 associated with the bulk motion $\varepsilon^{-2}\omega^{-1}$, inducing slow changes in the velocity, to be
 244 described below by introducing the long time scale $\tau = \varepsilon^2 t$ as an additional independent
 245 variable. In this two-time scale formalism, all variables are assumed to be 2π periodic
 246 in the short time scale t , slow changes in time being described by the additional time
 247 variable τ , which is formally introduced in the equations by replacing the original time
 248 derivatives by $\partial/\partial t + \varepsilon^2 \partial/\partial \tau$.

249 4.1. Leading-order solution

250 At leading order in the limit $\varepsilon \ll 1$ the problem reduces to the integration of

$$\frac{1}{\ell} \frac{\partial}{\partial x} (\ell u_0) - \frac{\eta}{h} \frac{\partial \bar{h}}{\partial x} \frac{\partial u_0}{\partial \eta} + \frac{1}{h} \frac{\partial v_0}{\partial \eta} + \frac{1}{\ell} \frac{\partial w_0}{\partial s} - \frac{\eta}{h} \frac{1}{\ell} \frac{\partial \bar{h}}{\partial s} \frac{\partial w_0}{\partial \eta} = 0, \quad (4.1)$$

$$\frac{\partial u_0}{\partial t} = -\frac{\partial p'_0}{\partial x} + \frac{1}{\alpha^2 \bar{h}^2} \frac{\partial^2 u_0}{\partial \eta^2}, \quad (4.2)$$

$$\frac{\partial w_0}{\partial t} = -\frac{1}{\ell} \frac{\partial \hat{p}_0}{\partial s} + \frac{1}{\alpha^2 \bar{h}^2} \frac{\partial^2 w_0}{\partial \eta^2}, \quad (4.3)$$

$$\frac{\partial c_0}{\partial t} = 0 \quad (4.4)$$

251 supplemented with $h'_0 = \gamma(\cos t + k^2 p'_0)$, the leading-order form of (3.3), with boundary
 252 conditions $u_0 = v_0 = w_0 = \partial c_0/\partial \eta = 0$ at $\eta = 0$ and $u_0 = v_0 - \partial h'_0/\partial t = w_0 = \partial c_0/\partial \eta = 0$
 253 at $\eta = 1$, $p'_0 = 0$ at $x = 0$, and $\int_0^1 \left(\bar{h} \int_0^1 u_0 d\eta \right) ds = 0$ at $x = 1$. As indicated by (4.4),

at leading order the solute concentration varies only in the long time scale τ , variations with the short time scale t affecting only higher-order corrections of relative order ε and smaller. As shown previously (Sánchez *et al.* 2018), the solution to the periodic linear lubrication problem (4.1)–(4.3) can be written as

$$u_0 = \text{Re} (ie^{it}U), v_0 = \text{Re} (ie^{it}V), w_0 = \text{Re} (ie^{it}W), \quad (4.5)$$

$$p'_0 = \text{Re} (e^{it}P'), \hat{p}_0 = \text{Re} (e^{it}\hat{P}), h'_0 = \text{Re} (e^{it}H'),$$

where the complex functions $U(x, \eta, s)$, $V(x, \eta, s)$, $W(x, \eta, s)$, $P'(x)$, $\hat{P}(x, s)$, and $H'(x, s)$ are given in an Appendix for completeness. The leading-order solution (4.5), identical to that found in our earlier analyses (Sánchez *et al.* 2018; Lawrence *et al.* 2019), is buoyancy-free, and therefore independent of the long-time scale τ . Buoyancy will be seen to enter at the following order to modify the bulk motion.

4.2. Time-averaged Eulerian velocity

While the above harmonic functions (4.5) have zero mean values over an oscillation period, i.e. $\langle u_0 \rangle = 0$ with $\langle \cdot \rangle = \int_t^{t+2\pi} \cdot dt / (2\pi)$, the velocity corrections (u_1, v_1, w_1) contain nonzero cycle-averaged components $(\langle u_1 \rangle, \langle v_1 \rangle, \langle w_1 \rangle)$ that satisfy the quasi-steady conservation equations

$$\mathcal{F} = \frac{1}{\ell} \frac{\partial}{\partial x} (\ell \bar{h} \langle u_1 \rangle) + \frac{1}{\ell} \frac{\partial}{\partial s} (\bar{h} \langle w_1 \rangle) - \frac{\partial}{\partial \eta} \left(\eta \frac{\partial \bar{h}}{\partial x} \langle u_1 \rangle + \frac{\eta}{\ell} \frac{\partial \bar{h}}{\partial s} \langle w_1 \rangle \right) + \frac{\partial \langle v_1 \rangle}{\partial \eta}, \quad (4.6)$$

$$\mathcal{F}_x = -\frac{\partial \langle p'_1 \rangle}{\partial x} + \frac{1}{\bar{h}^2 \alpha^2} \frac{\partial^2 \langle u_1 \rangle}{\partial \eta^2} - Ri c_0, \quad (4.7)$$

$$\mathcal{F}_s = -\frac{1}{\ell} \frac{\partial \langle \hat{p}_1 \rangle}{\partial s} + \frac{1}{\bar{h}^2 \alpha^2} \frac{\partial^2 \langle w_1 \rangle}{\partial \eta^2}, \quad (4.8)$$

obtained by taking the time average of the equations that emerge when collecting terms of order ε in (3.4)–(3.6). The functions \mathcal{F} , \mathcal{F}_x , and \mathcal{F}_s appearing on the left-hand side of the above equations carry the combined effects of convective acceleration and canal deformation on the mean Eulerian motion. These functions involve time averages of products of the harmonic functions (4.5), with expressions given in the appendix.

The velocity must satisfy the homogeneous boundary conditions $\langle u_1 \rangle = \langle v_1 \rangle = \langle w_1 \rangle = 0$ at $\eta = (0, 1)$ and $\int_0^1 (\bar{h} \int_0^1 \langle u_1 \rangle d\eta) ds = 0$ at $x = 1$. Note that the condition $\langle v_1 \rangle = 0$ at $\eta = 1$ follows at this order from the general condition $v = \partial h' / \partial t$ written in the two-time-scale formalism in the form $v = \partial h' / \partial t + \varepsilon^2 \partial h' / \partial \tau$, so that $\langle v \rangle = \varepsilon^2 \partial \langle h' \rangle / \partial \tau$.

Observation of (4.6)–(4.8) reveals that the mean Eulerian motion has two different driving mechanisms, namely, the buoyancy force $-Ri c_0$ appearing on the right-hand-side of (4.7), which varies slowly in the long-time scale τ , and the steady functions \mathcal{F} , \mathcal{F}_x , and \mathcal{F}_s , associated with convective acceleration and canal deformation. Since the problem is linear, the two distinct driving mechanisms can be quantified separately by expressing the mean Eulerian velocity $(\langle u_1 \rangle, \langle v_1 \rangle, \langle w_1 \rangle) = (u_{\text{SS}} + u_{\text{B}}, v_{\text{SS}} + v_{\text{B}}, w_{\text{SS}} + w_{\text{B}})$ as the sum of the steady-streaming velocity $(u_{\text{SS}}, v_{\text{SS}}, w_{\text{SS}})$ and the buoyancy-induced drift $(u_{\text{B}}, v_{\text{B}}, w_{\text{B}})$. The former was obtained in our previous analyses (Sánchez *et al.* 2018; Lawrence *et al.* 2019) by integration of the problem arising with $Ri = 0$, yielding the solution given in the appendix, while the latter, the new contribution arising when the drug density differs from the CSF density (i.e. when $Ri \neq 0$), can be obtained by integration of the reduced problem corresponding to $\mathcal{F} = \mathcal{F}_x = \mathcal{F}_s = 0$. The resulting solution, involving integrals

of the leading-order solute concentration c_0 , can be cast in the form

$$\frac{u_B}{\alpha^2 Ri \bar{h}^2} = 3\eta(1-\eta) \frac{\int_0^1 \bar{h}^3 \mathcal{C} ds}{\int_0^1 \bar{h}^3 ds} + \eta \int_0^\eta c_0 d\tilde{\eta} - \int_0^\eta c_0 \tilde{\eta} d\tilde{\eta} - \eta \int_0^1 c_0(1-\eta) d\eta, \quad (4.9)$$

$$\frac{w_B}{\alpha^2 Ri \bar{h}^2} = \frac{3\eta(1-\eta)}{\bar{h}^3} \frac{\partial}{\partial x} \left[\ell \left(\int_0^s \bar{h}^3 \mathcal{C} d\tilde{s} - \frac{\int_0^1 \bar{h}^3 \mathcal{C} ds}{\int_0^1 \bar{h}^3 ds} \int_0^s \bar{h}^3 d\tilde{s} \right) \right], \quad (4.10)$$

$$\frac{v_B}{\alpha^2 Ri} = \frac{\eta^2}{\ell} \left(\eta - \frac{3}{2} \right) \frac{\partial}{\partial x} (\ell \bar{h}^3 \mathcal{C}) - \frac{1}{\ell} \frac{\partial}{\partial x} (\ell \bar{h}^3 f_B) + \eta \frac{\partial \bar{h}}{\partial x} \frac{u_B}{\alpha^2 Ri} + \frac{\eta}{\ell} \frac{\partial \bar{h}}{\partial s} \frac{w_B}{\alpha^2 Ri}, \quad (4.11)$$

where

$$\mathcal{C} = \int_0^1 c_0 \eta(1-\eta) d\eta \quad (4.12)$$

and

$$f_B = \frac{1}{2} \int_0^\eta c_0 \tilde{\eta}^2 d\tilde{\eta} + \left(\frac{\eta^2}{2} - \eta \right) \int_0^\eta c_0 \tilde{\eta} d\tilde{\eta} - \frac{\eta^2}{2} \int_\eta^1 c_0(1-\tilde{\eta}) d\tilde{\eta}, \quad (4.13)$$

with tildes used to denote dummy integration variables.

4.3. The integro-differential transport equation

As shown by Lawrence *et al.* (2019), the transport equation that determines the slow spatiotemporal evolution of $c_0(x, \eta, s, \tau)$, given by

$$\frac{\partial c_0}{\partial \tau} + u_L \frac{\partial c_0}{\partial x} + \left[\frac{v_L}{\bar{h}} - \frac{\eta}{\bar{h}} \left(u_L \frac{\partial \bar{h}}{\partial x} + \frac{w_L}{\ell} \frac{\partial \bar{h}}{\partial s} \right) \right] \frac{\partial c_0}{\partial \eta} + \frac{w_L}{\ell} \frac{\partial c_0}{\partial s} = \frac{1}{\alpha^2 \sigma \bar{h}^2} \frac{\partial^2 c_0}{\partial \eta^2}, \quad (4.14)$$

can be obtained by analyzing terms of order ε^2 in (3.7). The convective transport in the long time scale is found to be driven by the mean Lagrangian velocity

$$\begin{cases} u_L = u_{SS} + u_B + u_{SD} \\ v_L = v_{SS} + v_B + v_{SD} \\ w_L = w_{SS} + w_B + w_{SD} \end{cases} \quad (4.15)$$

given by the sum of the cycle-averaged Eulerian velocity ($\langle u_1 \rangle, \langle v_1 \rangle, \langle w_1 \rangle$) = $(u_{SS} + u_B, v_{SS} + v_B, w_{SS} + w_B)$ and the Stokes drift (u_{SD}, v_{SD}, w_{SD}) , the latter being a purely kinematic contribution resulting from the spatial non-uniformity of the pulsatile flow (Lawrence *et al.* 2019). The steady-streaming and Stokes-drift contributions to the time-averaged Lagrangian motion, constant and independent of the drug concentration, were identified in our previous analysis (Lawrence *et al.* 2019), with corresponding expressions given in an appendix. The slowly varying buoyancy-induced velocity (u_B, v_B, w_B) is a new contribution coupling the bulk motion with the drug concentration. Since the expressions for (u_B, v_B, w_B) , given in (4.9)–(4.11), contain spatial integrals of the solute concentration c_0 , the transport equation (4.14), which is a linear partial differential equation in the buoyancy-free case $Ri = 0$ analyzed earlier (Lawrence *et al.* 2019), adopts for $Ri \neq 0$ a nonlinear integro-differential character that complicates the description.

The transport equation (4.14), supplemented with (4.9)–(4.11) for the evaluation of the slowly varying buoyancy-induced velocity (u_B, v_B, w_B) and with the expressions given in the appendix for the time-independent velocity components (u_{SS}, v_{SS}, w_{SS}) and (u_{SD}, v_{SD}, w_{SD}) , can be integrated with boundary conditions $\partial c_0 / \partial \eta = 0$ at $\eta = (0, 1)$ to determine the evolution of the solute. An additional condition must be prescribed at points across the entrance section $x = 0$ where there exists inflow (i.e. positive

values of u_L). In the following integrations, it is assumed that the drug concentration of the incoming fluid particles is identically zero, as is consistent with drug delivery in the lumbar region. Bolus injection can be described by using as initial condition the solute distribution $c_0 = c_i(x, \eta, s)$ existing at the end of the short injection phase. The description of continuous drug infusion is somewhat more complicated, in that it requires consideration of a localized solute source at the delivery location, a case to be addressed separately in § 7.

Although the reduced Schmidt number $\sigma = S\varepsilon^2$ can be expected to take order-unity values for the drugs typically used in applications (e.g. $\sigma = 0.532 - 2.128$ when evaluated with $\varepsilon = 0.02 - 0.04$ for methotrexate), it is instructive to investigate simplifications arising for extreme values of this parameter. For example, for $\sigma \gg 1$ the transverse-diffusion term in (4.14) becomes negligible, with the result that the solute particles are transported by the mean Lagrangian velocity while maintaining its initial concentration. Numerical methods specifically tailored to describe Lagrangian-particle dispersion can be instrumental to speed up the associated computations (Guan *et al.* 2023). In the opposite limit $\sigma \ll 1$, diffusion rapidly uniformizes the composition in the transverse direction, so that the concentration becomes independent of η . The simplified equation applying in this limit can be derived by integrating (4.14) in η with boundary conditions $\partial c_0 / \partial \eta = 0$ at $\eta = (0, 1)$ to yield

$$\frac{\partial c_0}{\partial \tau} + \bar{u}_L \frac{\partial c_0}{\partial x} + \frac{\bar{w}_L}{\ell} \frac{\partial c_0}{\partial s} = 0, \quad (4.16)$$

where $\bar{u}_L = \int_0^1 u_L d\eta$ and $\bar{w}_L = \int_0^1 w_L d\eta$ are the width-averaged values of the longitudinal and azimuthal components of the mean Lagrangian velocity. It will be of interest in future work to assess the predictive capability of the above simple equation.

It is worth noting that, unlike direct numerical simulations (DNS) of drug delivery, which need to account for the small cumulative concentration changes that occur over subsequent cardiac cycles, the reduced description (4.14) targets directly the solute evolution in the long time scale $\varepsilon^{-2}\omega^{-1}$ that characterizes drug dispersion along the canal. Since the number of cardiac cycles required to achieve significant drug dispersion scales with ε^{-2} , DNS computations accounting for realistic values of $\varepsilon \sim 0.02 - 0.04$ must in general consider hundreds of cycles, resulting in computational times that are orders of magnitude larger than those involved in integrating (4.14).

5. Validation of the reduced model

For buoyancy-free systems (i.e. $Ri = 0$) the mean Lagrangian velocity reduces to $(u_L, v_L, w_L) = (u_{SS} + u_{SD}, v_{SS} + v_{SD}, w_{SS} + w_{SD})$, independent of the solute concentration, with the result that the associated transport equation (4.14) becomes a linear partial differential equation with time-independent coefficients. The accuracy of the resulting simplified description was tested previously (Gutiérrez-Montes *et al.* 2021) by comparing the model predictions with results of DNS computations involving integrations of the complete Navier-Stokes equations. The previous comparisons are extended here to cases with $Ri \neq 0$, for which (4.14) displays its complicated nonlinear integro-differential character. As in the previous paper, results are given below for two different geometrical configurations with constant perimeter $\ell = 1$, namely, a constant-eccentricity annular canal bounded by parallel cylindrical surfaces, yielding a canal width $\bar{h}(s) = 1 - 0.5 \cos(2\pi s)$, and a variable-eccentricity configuration with canal width $\bar{h}(x, s) = 1 - 0.5 \cos(2\pi s) \cos(2\pi x)$. The latter geometry is selected as a simplified model to mimic changes in the position of the spinal cord relative to the dura mater existing along the

human spinal canal, which are depicted in figure 1(b) and 1(c). As one traverses the spine caudally, the spinal cord, which is closer to the posterior side of the canal in the cervical region, moves closer to the anterior side in the thoracic region, eventually returning to the posterior side in the lumbar region. These changes in the spinal canal eccentricity are known to produce changes in the direction of the longitudinal mean Lagrangian velocity (Coenen *et al.* 2019), leading to the recirculating pattern of bulk CSF flow shown in figure 1(d).

The validation addresses the temporal evolution of the solute following the release of a finite dose, with the initial solute concentration described by the truncated Gaussian distribution

$$c_i = \min \left\{ 1, \frac{3}{2} \exp \left[-16 \left(\frac{x - x_0}{\delta} \right)^2 \right] \right\}, \quad (5.1)$$

which represents a band of solute with characteristic width δ centered at x_0 and having a saturated core flanked by thin layers across which the concentration decays to zero. The values $\delta = 0.2$ and $x_0 = 0.65$ are selected in the sample computations shown below.

The numerical scheme for the integration of (4.14) utilizes a second-order centered finite-difference approximation for the spatial discretization of the viscous terms and an upwind scheme for the nonlinear terms. A second-order explicit Runge-Kutta scheme is used for time marching, with the integral expressions (4.9)–(4.11) evaluated with a simple trapezoidal rule. A detailed account of the numerical scheme employed in the accompanying DNS computations can be found in Gutiérrez-Montes *et al.* (2021). The DNS computations were performed for a dimensionless stroke length $\varepsilon = 0.02$, so that every unit in the long-time scale τ corresponds to $(2\pi\varepsilon)^{-2} \simeq 400$ oscillatory cycles in the DNS computations. The resulting concentration, which includes short-time fluctuations associated with the oscillatory flow, is cycled-averaged to give $\langle c \rangle = \int_t^{t+2\pi} c dt / (2\pi)$, to be compared with the associated model prediction c_0 .

Results are shown in figures 2 (constant eccentricity) and 3 (variable eccentricity) for a canal with $\alpha = 3$, $k = 0.5$, $\gamma = 1$, and $\sigma = 0.4$. To illustrate effects of buoyancy on drug dispersion, in addition to the buoyancy-neutral case $Ri = 0$ the computations consider both a heavy solute with $\rho_d > \rho$ ($Ri = -1$) and a light solute $\rho_d < \rho$ ($Ri = 1$). The figures display three-dimensional views of the entire canal showing isosurfaces of solute concentration c_0 for several values of τ . The quantitative comparisons between the model and the DNS include distributions of width-averaged concentrations $\int_0^1 c_0 d\eta$ and $\int_0^1 \langle c \rangle d\eta$ as well as corresponding axial distributions of concentration per unit length of canal, computed according to $C_0 = \int_0^1 \bar{h} \int_0^1 c_0 d\eta ds$ and $\langle C \rangle = \int_0^1 \bar{h} \int_0^1 \langle c \rangle d\eta ds$, with the dotted curves representing the initial distribution $C_i = \int_0^1 \bar{h} \int_0^1 c_i d\eta ds$. For reference, the left-side contour panels showing $\int_0^1 c_0 d\eta$ include the streamlines corresponding to the width-averaged Lagrangian drift velocity $(\int_0^1 u_L d\eta, \int_0^1 w_L d\eta)$, which evolve in time under the action of buoyancy when $Ri \neq 1$. The upper panel in each figure represents the fraction of the drug bolus that remains in the canal at time τ , as computed with the reduced-transport model according to $\chi = \int_0^1 C_0 dx / \int_0^1 C_i dx$.

Observation of the panels displaying streamlines reveals that the solute moves predominantly following the width-averaged flow, thereby highlighting the important role of the Lagrangian drift in the dispersion of the drug. For a non-buoyant solute in a constant-eccentricity canal, investigated in figure 2(c), the mean Lagrangian flow exhibits a simple circulating pattern, in which the fluid enters along the wide part of the canal ($s = 0.5$) and leaves along the narrow part ($s = 0$), the motion being slower near the closed end

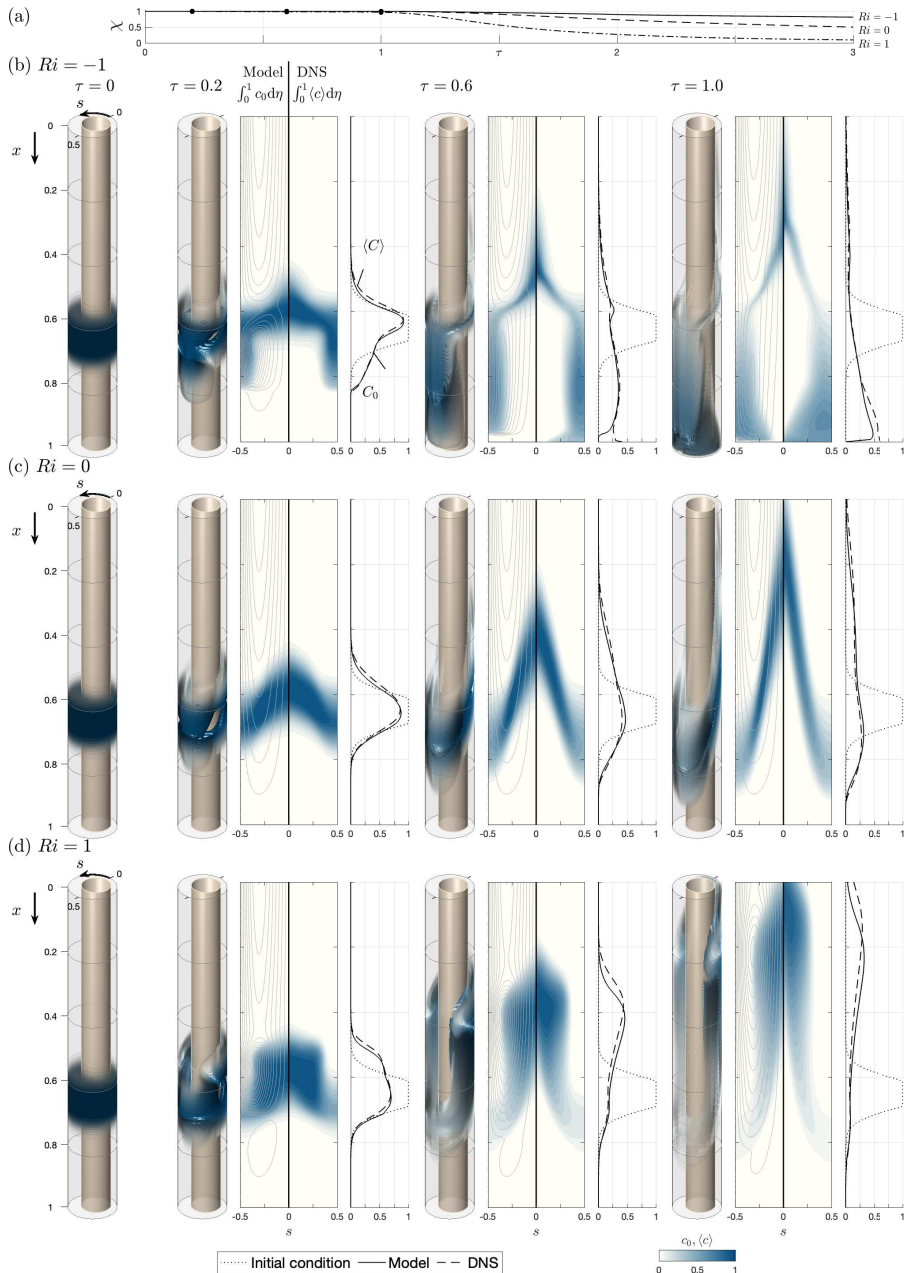


FIGURE 2. The temporal evolution of the solute concentration in a constant-eccentricity canal with $\ell = 1$, $\bar{h}(s) = 1 - 0.5 \cos(2\pi s)$, $\alpha = 3$, $k = 0.5$, $\gamma = 1$, and $\sigma = 0.4$ as obtained from the reduced transport equation (4.14) and from DNS computations for three different values of $Ri = -1$ (b), $Ri = 0$ (c) and $Ri = 1$ (d), with the upper panel (a) showing the temporal evolution of the total amount of solute contained in the canal (normalized with its initial value) predicted with the reduced model, as computed from $\chi = \int_0^1 C_0 dx / \int_0^1 C_i dx$. The plots include three-dimensional isosurfaces of solute concentration c_0 , distributions of width-averaged concentrations $\int_0^1 c_0 d\eta$ and $\int_0^1 \langle c \rangle d\eta$ and corresponding axial distributions of concentration per unit length of canal $C_0 = \int_0^1 \bar{h} \int_0^1 c_0 d\eta ds$ (solid curves) and $\langle C \rangle = \int_0^1 \bar{h} \int_0^1 \langle c \rangle d\eta ds$ (dashed curves), with the dotted curves representing the initial distribution $C_i = \int_0^1 \bar{h} \int_0^1 c_i d\eta ds$. The streamlines shown in the plots of $\int_0^1 c_0 d\eta$, corresponding to the width-averaged Lagrangian drift velocity ($\int_0^1 u_L d\eta$, $\int_0^1 w_L d\eta$), are plotted using a constant spacing equal to 0.01 for the associated width-averaged stream function.

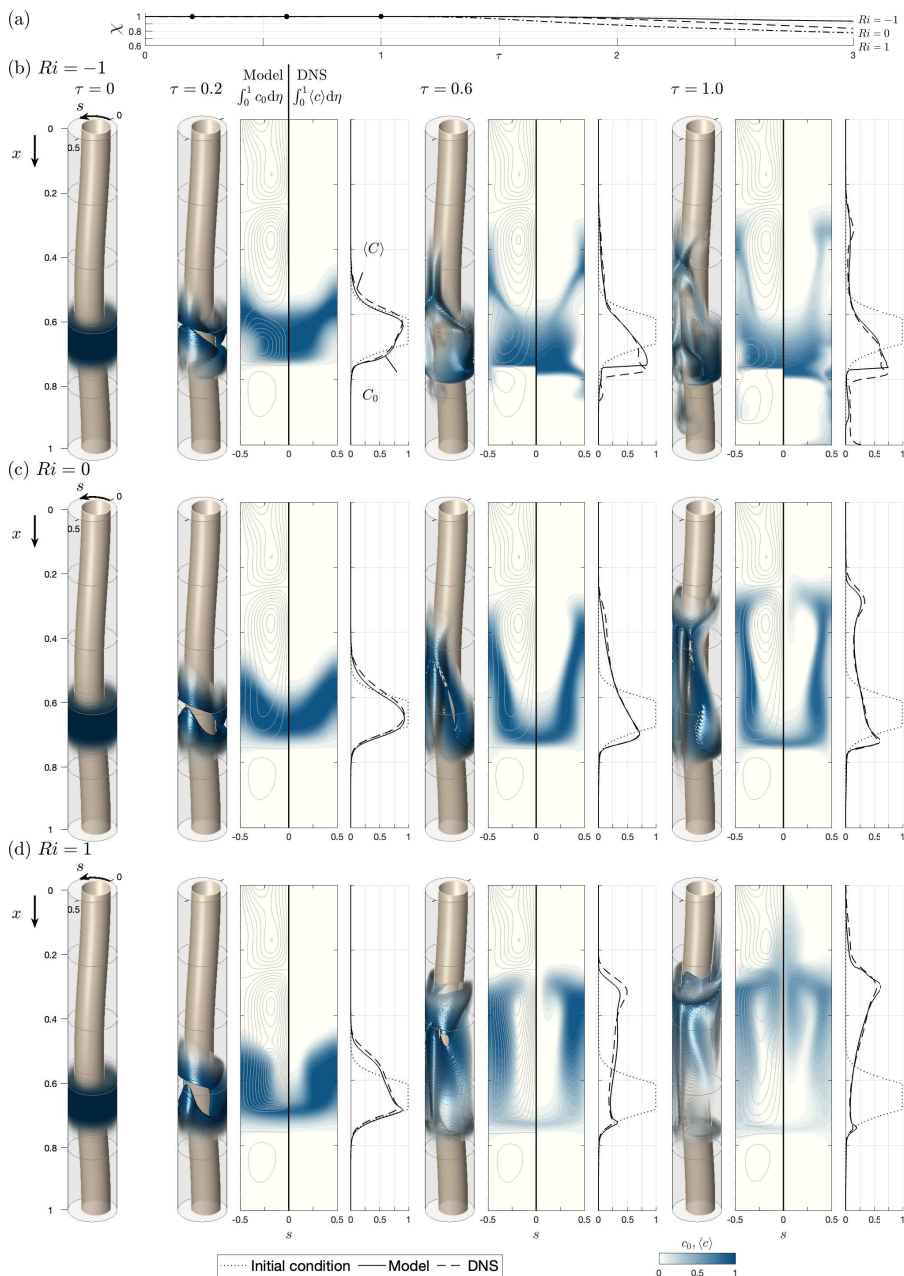


FIGURE 3. Same as figure 2 but for a variable eccentricity canal with $\bar{h}(x, s) = 1 - 0.5 \cos(2\pi s) \cos(2\pi x)$.

407 $x = 1$. As seen in figures 2(b) and 2(d) the presence of buoyancy alters the flow, with
 408 associated streamlines evolving in time as the spatial distribution of the solute changes.
 409 Buoyancy promotes rapid ascension of the light solute along the narrow part of the canal,
 410 that being the behavior displayed in figure 2(d). Conversely, heavy solutes tend to sink
 411 to the bottom, progression towards the canal entrance being limited to a thin solute
 412 filament stretching along the narrow section $s = 0$, as seen in figure 2(b). While the

overall agreement between the model and the DNS is generally satisfactory, a notable deviation arises at $x = 1$ in the heavy-solute results. Here, the model predicts a zero concentration for all times, whereas the DNS yields a concentration that increases over time. These disparities stem from the effect of axial diffusion (not present in the model), which, though negligible elsewhere, becomes significant in this terminal region as the velocity diminishes to zero.

Buoyancy effects are clearly visible in the axial distributions of concentration per unit length of canal C_0 and $\langle C \rangle$ and also in the curves representing in figure 2(a) the fraction χ of the initial bolus that remains inside the canal at time τ . The results indicate that at the longest time computed ($\tau = 3$) most of the light solute (91%) has abandoned the canal, while about 82% of the heavy solute remains inside. This behavior is consistent with previous clinical observations pertaining to hyperbaric and hypobaric drugs (Mitchell *et al.* 1988; Povey *et al.* 1989; Richardson *et al.* 1996; Veering *et al.* 2001; Loubert *et al.* 2011).

For the variable-eccentricity canal shown in figure 3, the streamline patterns of the mean Lagrangian motion feature multiple recirculating regions. The flow direction is reversed between contiguous recirculating cells, as can be inferred by the maps of solute concentration. The solute, carried by the fluid particles, encircles the recirculating regions, thereby hindering the solute progression towards the canal entrance. The plots at $\tau = 1$ show most of the light solute accumulating at the interface separating near $x = 0.25$ the two top recirculating regions (see figure 3(d)), while the heavy solute accumulates around $x = 0.75$, above the nearly stagnant bottom recirculating region, as shown in figure 3(b). As indicated by the comparison of figures 2(a) and 3(a) the rate at which the solute reaches the canal entrance is significantly lower for canals with variable eccentricity, in accordance with previous results (Coenen *et al.* 2019; Gutiérrez-Montes *et al.* 2021).

The agreement between the model and the DNS results is very satisfactory, quantitative departures remaining consistently small regardless of the value of Ri . The degree of agreement is particularly remarkable in connection with the dashed and solid curves representing the longitudinal distribution of the solute at different instants of time. In view of the comparisons shown in figures 2 and 3, it can be concluded that the reduced model provides a sufficiently accurate description for most purposes while requiring computational times that are a fraction of those involved in the DNS computations. For instance, to generate the results corresponding to each value of Ri in figures 2 and 3, the computations using the reduced model were completed in about 10 minutes using a laptop computer, whereas the DNS computations took about a week on a 24-core cluster.

6. Dispersion of a drug bolus

The reduced transport equation (4.14) can be used to generate predictions of drug dispersion based on subject-specific canal boundaries and dimensions, with the model parameters determined using magnetic resonance imaging (MRI) measurements, as explained in Coenen *et al.* (2019). The sample computations shown below use measurements corresponding to a 25-year old woman (subject 1 in Coenen *et al.* (2019)), with relevant anatomical and Lagrangian-flow details shown in figure 1(b–d). High-resolution images of the entire spine were segmented to extract the 3D position of the pia and dura mater, with the cauda equina (the group of roots branching off at the end of the spinal cord in the lumbar region) represented as an extension of the spinal cord with cross-sectional area tapering down to the end of spinal canal. The resulting canal anatomy is shown in figure 1(c), with the transverse dimension scaled by a factor three to facilitate

461 visualization. A Gaussian filter was used to generate smooth distributions of perimeter
 462 and canal width, their mean values $\ell_c = 21.8$ mm and $h_c = 3.6$ mm employed to
 463 scale the geometrical functions $\ell(x)$ and $\bar{h}(x, s)$ used in the model, with the longitudinal
 464 distance x being scaled with the total canal length $L = 59$ cm. As explained in Coenen
 465 *et al.* (2019), the compliance of the canal was determined by comparing predictions
 466 of oscillatory flow rate with phase-contrast MRI measurements, yielding the function
 467 $\gamma'(x) = 14.3[0.8 + 0.3 \tanh(4x - 0.2)]$ m/MPa with mean value $\gamma'_c = 14.107$ m/MPa. For
 468 this subject, the associated values of the Womersley number and elastic wave number
 469 were found to be $\alpha = h_c/(\nu/\omega)^{1/2} = 10.8$ and $k = L\omega/[(h_c/\gamma'_c)/\rho]^{1/2} = 0.73$, respectively.

470 As discussed earlier in connection with figures 2 and 3, the solute moves predominantly
 471 following the Lagrangian drift. Before computing drug dispersion, it is therefore of interest
 472 to investigate the structure of the mean Lagrangian flow in the absence of buoyancy
 473 forces for the anatomically correct canal shown in figure 1(c). To that end, streamlines
 474 corresponding to the width-averaged velocity $(\int_0^1 u_L d\eta, \int_0^1 w_L d\eta)$ with $(u_L, w_L) = (u_{SS} +$
 475 $u_{SD}, w_{SS} + w_{SD})$ are plotted in figure 1(d). The resulting flow pattern comprises three main
 476 recirculating regions that occupy approximately the cervical, thoracic and lumbar regions
 477 along with smaller recirculating regions distributed along the posterior midline ($s = 0$).
 478 The streamlines plotted correspond to evenly spaced values of the associated stream
 479 function, so that the physical distance between contiguous streamlines is a measure of
 480 the local flow velocity. As is clear from the plot, the fluid is nearly stagnant in the lumbar
 481 region, where drug delivery usually takes place, suggesting that neutrally buoyant or
 482 heavy drugs will tend to remain near the injection site. The extent to which buoyancy
 483 promotes the dispersion of light drugs is to be evaluated in figure 4(c).

484 To mimic an intrathecal injection via the L3/L4 posterior intervertebral space, the
 485 description of drug dispersion utilizes as initial condition the Gaussian solute distribution

$$c_i = \exp \left\{ - \left[\left(\frac{x - x_0}{\delta_x} \right)^2 + \left(\frac{\eta - \eta_0}{\delta_\eta} \right)^2 + \left(\frac{s - s_0}{\delta_s} \right)^2 \right] \right\} \quad (6.1)$$

486 with $(x_0, \eta_0, s_0) = (0.8, 0.5, 0)$ and $(\delta_x, \delta_\eta, \delta_s) = (1/16, 500, 2/7)$. The reduced Schmidt
 487 number is selected to be $\sigma = \varepsilon^2 S = 1$, corresponding to a drug Schmidt number in the
 488 range $625 < S < 2500$ for $\varepsilon = 0.02 - 0.04$. Buoyancy effects are investigated for $Ri = 1$
 489 and $Ri = -1$, taken as representative of Midazolam and Morphine. Their temporal
 490 evolution is compared in figure 4 with results corresponding to a neutrally buoyant drug.
 491 To facilitate visualization, besides three-dimensional distributions of drug concentration
 492 c_0 , the figure shows two-dimensional maps of width-averaged concentration $\int_0^1 c_0 d\eta$ at
 493 selected times, with particular attention given to the short-time evolution. For the three
 494 cases considered, corresponding videos are available as supplementary material, showing
 495 the evolution of the drug up to $\tau = 5$.

496 The plots in figure 4(b) reveal that, since the mean Lagrangian motion exhibits low
 497 velocities in the lumbar region, in the absence of buoyancy the initial drug evolution
 498 is very slow, with changes in the solute-concentration distribution remaining virtually
 499 inappreciable for $\tau \leq 0.1$. For longer times, the drug spreads following the lumbar
 500 recirculating vortices, with the result that the drug concentrates in an elongated region
 501 about the $s = 0$ axis. For the longest time shown in the figure ($\tau = 3$) only a small
 502 amount of drug has moved into the thoracic region.

503 Buoyancy fundamentally alters this dispersion pattern, as seen in figure 4(a) and 4(c).
 504 For the localized drug distribution considered in the computations, a fast buoyancy-driven
 505 vortex is formed upon injection, as revealed by the closely spaced streamlines shown in the
 506 two-dimensional plots for $\tau = 0.01$ and $\tau = 0.04$, rapidly spreading the drug around the

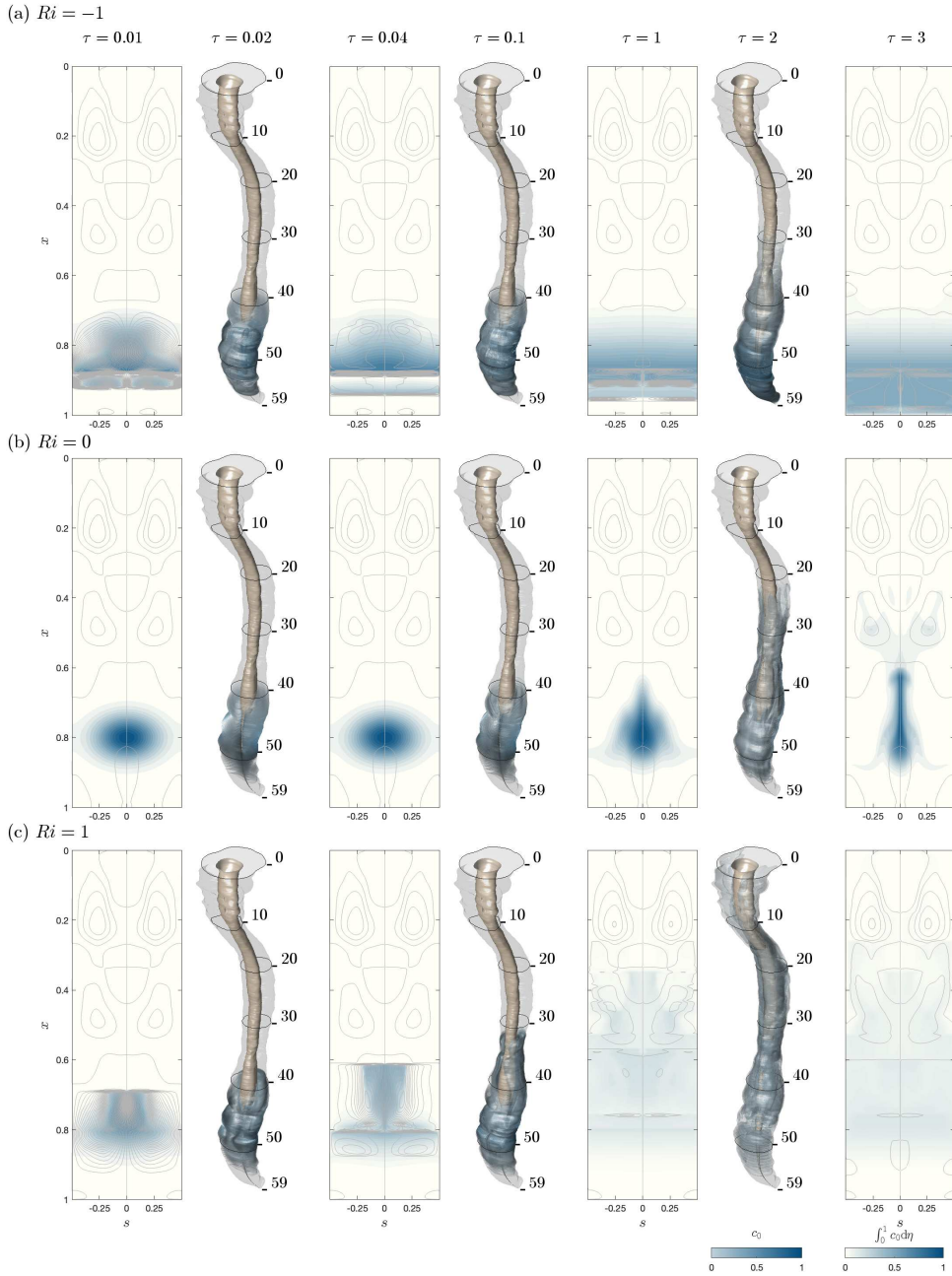


FIGURE 4. Drug dispersion following delivery of a finite dose via the L3-L4 intervertebral space as predicted for $\sigma = 1$ and three different values of the Richardson number $Ri = -1$ (a), $Ri = 0$ (b), and $Ri = 1$ (c) by integration of the reduced transport equation (4.14) subject to the initial condition (6.1). The plots include distributions of width-averaged concentrations $\int_0^1 c_0 d\eta$ at $\tau = (0.01, 0.04, 1, 3)$ along with three-dimensional isosurfaces of solute concentration c_0 at intermediate times $\tau = (0.02, 0.1, 2)$.

507 spinal cord from the initial injection site. The associated recirculatory motion is directed
 508 upwards/downwards along the $s = 0$ axis for a light/heavy drug, thereby promoting drug
 509 dispersion towards the cranial cavity/sacrum region. The progression rate, very rapid for
 510 short times, when the buoyancy-induced velocities are larger as a result of the existing
 511 high solute concentrations, slows down for longer times, with the heavy drug adopting
 512 a stratified distribution that slowly sinks towards the bottom end of the canal, while
 513 the light drug continues to evolve upwards, spreading through the thoracic and cervical
 514 region and eventually reaching the cranial cavity. The behavior revealed in the figure is
 515 therefore consistent with clinical observations regarding intrathecal injections in a seated
 516 position (Wildsmith *et al.* 1981; Mitchell *et al.* 1988; Povey *et al.* 1989; Richardson *et al.*
 517 1996; Veering *et al.* 2001).

518 7. The description of continuous drug infusion

519 ITDD medication is often released by continuous infusion with use of a percutaneous
 520 catheter connected to an external pump or a totally implanted system. The delivery
 521 rates are usually small, with maximum values $\dot{Q} \lesssim 1$ mL/h (De Andres *et al.* 2022).
 522 Since drug dispersion is driven by the mean Lagrangian motion, it can be anticipated
 523 that the total volume of drug released in times of order of the characteristic bulk-flow
 524 residence time $\varepsilon^{-2}\omega^{-1}$, given by $\dot{Q}\varepsilon^{-2}\omega^{-1}$ will be spread over the entire volume of the
 525 canal $L\ell_ch_c \sim 40 - 60$ mL, resulting in characteristic drug concentrations of order

$$c_c = \frac{\dot{Q}\varepsilon^{-2}\omega^{-1}}{L\ell_ch_c} \quad (7.1)$$

526 with $c_c \lesssim 0.01$. As a result, in describing continuous drug infusion it is appropriate to
 527 use an order-unity rescaled concentration $\varphi = c/c_c$. Also, since the density differences
 528 associated with the presence of the drug can be expected to be of order $c_c(\rho - \rho_d)$, the
 529 Richardson number (3.1), which was defined assuming solute concentrations of order
 530 unity, must be replaced with

$$Ri^* = \frac{g(\rho - \rho_d)c_c/\rho}{\varepsilon^2\omega^2L}, \quad (7.2)$$

531 so that the buoyancy acceleration term $-\varepsilon Ri c$ in (3.5) becomes $-\varepsilon Ri^* \varphi$.

532 Drug injection will be modeled using a localized volume source. To evaluate the
 533 contribution of the source to the mass and momentum balance, we must compare the
 534 characteristic value of the velocity induced by the source $\dot{Q}/(\ell_ch_c)$, obtained by dividing
 535 the volumetric injection rate \dot{Q} by the characteristic canal cross section ℓ_ch_c , with the
 536 characteristic bulk-flow velocity $\varepsilon^2\omega L$, the ratio of both quantities reducing simply to
 537 $[\dot{Q}/(\ell_ch_c)]/(\varepsilon^2\omega L) = c_c \ll 1$, as can be seen from (7.1). Since drug infusion induces
 538 negligibly small velocities, the presence of the localized source can be neglected in the
 539 first approximation when writing the continuity and momentum balance equations (3.4)–
 540 (3.6), but not in the solute conservation equation (3.7), which takes the form

$$\frac{\partial \varphi}{\partial t} + \varepsilon \left(u \frac{\partial \varphi}{\partial x} + v \frac{\partial \varphi}{\partial y} + \frac{w}{\ell} \frac{\partial \varphi}{\partial s} \right) = \frac{\varepsilon^2}{\alpha^2 \sigma} \frac{\partial^2 \varphi}{\partial y^2} + \varepsilon^2 q, \quad (7.3)$$

541 where the dimensionless function $q(x, \eta, s)$ represents the delivery rate per unit volume,
 542 scaled with $\dot{Q}/(L\ell_ch_c)$, so that $\int_0^1 \ell \int_0^1 \bar{h} \int_0^1 q d\eta ds dx = 1$. The asymptotic analysis, which
 543 parallels that leading to (4.14), provides in this case the reduced transport equation

$$\frac{\partial \varphi_0}{\partial \tau} + u_L \frac{\partial \varphi_0}{\partial x} + \left[\frac{v_L}{\bar{h}} - \frac{\eta}{\bar{h}} \left(u_L \frac{\partial \bar{h}}{\partial x} + \frac{w_L}{\ell} \frac{\partial \bar{h}}{\partial s} \right) \right] \frac{\partial \varphi_0}{\partial \eta} + \frac{w_L}{\ell} \frac{\partial \varphi_0}{\partial s} = \frac{1}{\alpha^2 \sigma \bar{h}^2} \frac{\partial^2 \varphi_0}{\partial \eta^2} + q \quad (7.4)$$

544 for the leading-order representation φ_0 of the reduced solute concentration $\varphi = \varphi_0 + \varepsilon\varphi_1 +$
 545 \dots , with the buoyancy-driven component (u_B, v_B, w_B) of the Lagrangian drift velocity
 546 (u_L, v_L, w_L) evaluated from (4.9)–(4.11) with Ri and c_0 replaced by Ri^* and φ_0 .

547 To represent injection in the posterior intrathecal region through the L3-L4 interver-
 548 tebral space, the sample computations shown in figure 5 consider a localized source with
 549 a normalized Gaussian distribution $q(x, \eta, s) = q_o / (\int_0^1 \ell \int_0^1 \bar{h} \int_0^1 q_o d\eta ds dx)$ centered at
 550 $(x_0, \eta_0, s_0) = (0.8, 0.5, 0)$, where the function q_o is the exponential distribution found
 551 on the right hand side of (6.1) with $(\delta_x, \delta_\eta, \delta_s) = (1/18, 1/5, 1/13)$. For the three
 552 cases considered, corresponding videos are available as supplementary material. The
 553 integrations, initiated with a zero drug concentration everywhere in the canal, describe
 554 transient drug infusion for three different reduced Richardson numbers $Ri^* = c_c Ri$,
 555 with the values $Ri^* = -0.1$ and $Ri^* = 0.1$ being comparable to, although somewhat
 556 larger than, those expected in connection with the dispersion of Meperidine and Fentanyl
 557 (see table 1). As in figure 4, figure 5 shows three-dimensional distributions of drug
 558 concentration φ_0 along with two-dimensional maps of width-averaged concentration
 559 $\int_0^1 \varphi_0 d\eta$. Note that, for each plot, the scale of the colour contours has been adjusted
 560 to accommodate the increasing concentration, which is found to be significantly larger
 561 for non-buoyant drugs.

562 As can be seen in the plots of figure 5(b), the neutrally buoyant drug accumulates near
 563 the injection location while spreading longitudinally along the posterior axis $s = 0$ at a
 564 small rate determined by the existing mean Lagrangian velocity. In contrast, the heavy
 565 drug with $Ri^* = -0.1$, shown in figure 5(a), immediately begins to sink upon injection,
 566 driving a recirculatory motion that promotes simultaneous azimuthal spreading. At $\tau =$
 567 0.2 the drug has already reached the sacral end of the canal, where it accumulates, forming
 568 a stratified distribution that is continuously stirred by the persistent buoyancy-driven
 569 recirculatory flow. Up to the longest time considered ($\tau = 2$), the heavy drug is confined
 570 to the lumbar region, with the result that the mean Lagrangian motion remains virtually
 571 unperturbed in the thoracic and cervical regions. On the other hand, infusion of light
 572 drugs, considered in figure 5(c), leads to the development of a plume. The light fluid rises
 573 until it reaches the boundary separating the lumbar and thoracic recirculating regions,
 574 forming a front at $x \simeq 0.6$, corresponding approximately to the T11-T12 intervertebral
 575 space. At that level, the drug spreads azimuthally to reach the anterior side, where it
 576 continues to flow upwards into the thoracic region, thereby resuming its progression
 577 towards the cranial cavity.

578 In analyzing the transient results of figure 5 one should bear in mind that, while
 579 the present computation assumes impermeable surfaces, leading to continuous drug
 580 accumulation, in ITDD processes drug uptake by the spinal nerve as well as through
 581 the dura membrane would eventually balance the infusion rate, leading to a steady drug
 582 distribution along the spine. For heavy drugs, the results shown in 5(a) suggest that
 583 the combined effects of buoyancy forces and drug uptake may limit drug dispersion to
 584 the lumbar and sacral regions. On the other hand, the results in figure 5(c) indicate
 585 that the ability of light drugs to reach the cranial cavity will depend on the competi-
 586 tion of buoyancy-enhanced drug dispersion and drug absorption, whose quantification
 587 necessitates of an extended reduced model accounting for pharmacokinetic effects.

588 8. Conclusions

589 Asymptotic and numerical methods have been used to quantify, for the first time,
 590 effects of buoyancy on the dispersion of drugs delivered in the spinal intrathecal space.

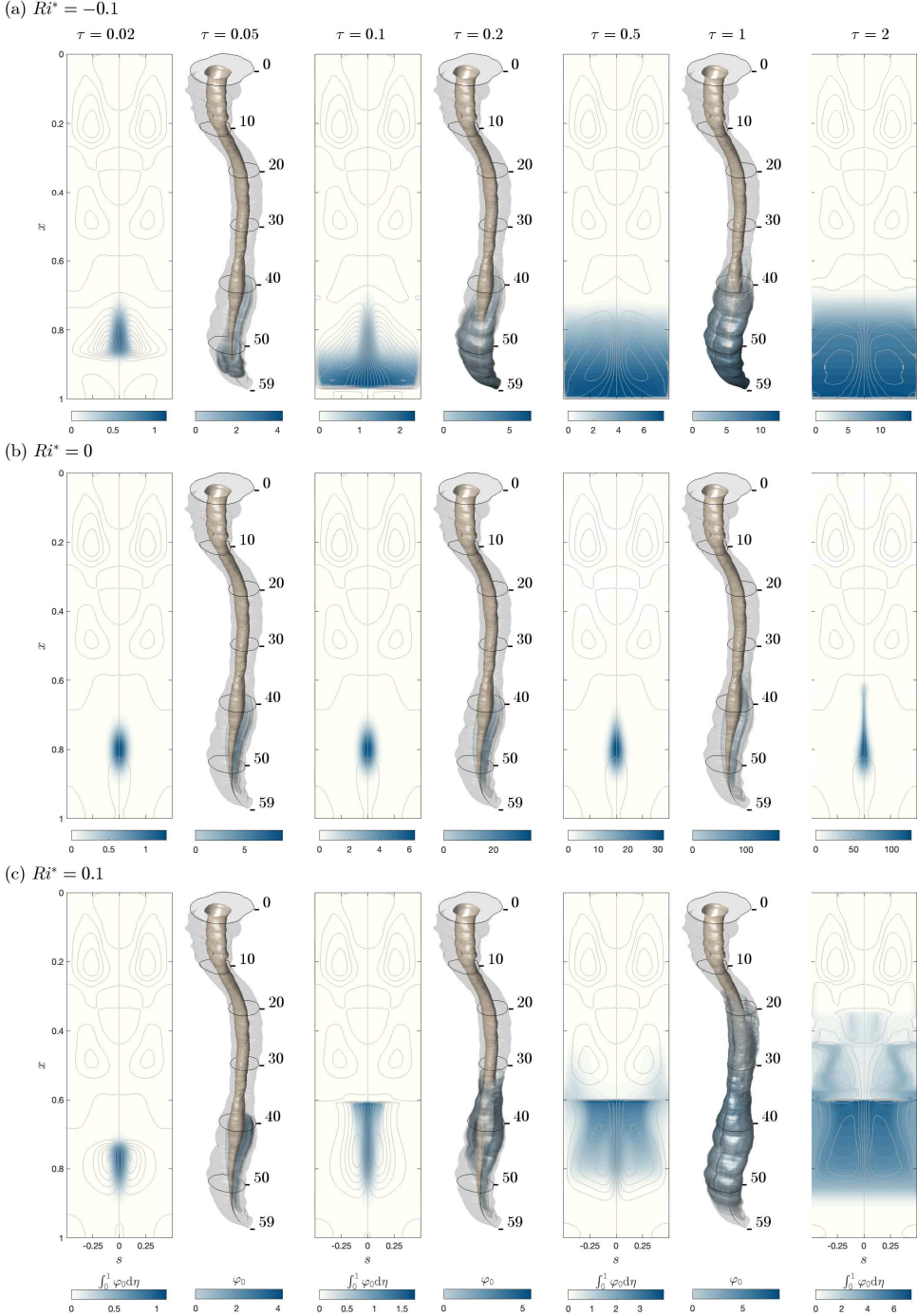


FIGURE 5. Drug dispersion corresponding to continuous drug infusion via the L3-L4 intervertebral space as predicted for $\sigma = 1$ and three different values of the rescaled Richardson number $Ri^* = -0.1$ (a), $Ri^* = 0$ (b), and $Ri^* = 0.1$ (c) by integration of the reduced transport equation (7.4) with a localized solute source centered at $(x_0, \eta_0, s_0) = (0.8, 0.5, 0)$. The plots include distributions of width-averaged concentrations $\int_0^1 \varphi_0 d\eta$ at $\tau = (0.02, 0.1, 0.5, 2)$ along with three-dimensional isosurfaces of solute concentration φ_0 at intermediate times $\tau = (0.05, 0.2, 1)$.

A two-time scale asymptotic analysis, similar to that employed in a recent investigation pertaining to a wavy-walled planar channel (Alaminos-Quesada *et al.* 2022), leads to a simplified transport description targeting the relevant long time scale characterizing drug dispersion.

Since the buoyancy-driven component of the mean Lagrangian velocity driving the convective transport depends on spatial integrals of the solute concentration, as described in (4.9)–(4.11), the resulting solute transport equation, given in (4.14), displays an integro-differential character. The accuracy of the model is tested in computations of buoyancy-modulated solute dispersion in constant-eccentricity and variable-eccentricity annular canals. The model predictions are shown in figures 2 and 3 to be in excellent quantitative agreement with DNS results for positively, neutrally and negatively buoyant solutes, with the computational cost associated with integrations of the reduced transport equation typically being three to four orders of magnitude smaller than those involved in the DNS computations. It is worth mentioning that the two-time scale methodology developed here can find application in analyzing buoyancy-modulated secondary motion in other applications involving small density differences, including those related to active particles (Guan *et al.* 2023).

The reduced model can be combined with MRI anatomical measurements to derive subject-specific predictions of drug dispersion, following the methodology outlined by Coenen *et al.* (2019). Sample computations are given for the transient solute evolution associated with the release of a finite dose and with the continuous infusion of a small constant rate. Buoyancy forces alter the mean Lagrangian motion, promoting upward (cranial)/downward (caudal) transport of light/heavy solutes. The comparisons presented in figures 4 and 5 clearly underline the important role of the small drug-to-CSF density differences $10^{-4} \lesssim |\rho - \rho_d|/\rho \lesssim 10^{-2}$, confirming previous clinical observations (Mitchell *et al.* 1988; Povey *et al.* 1989; Richardson *et al.* 1996; Veering *et al.* 2001; Loubert *et al.* 2011).

Future refinements of the transport description should account for additional effects, including respiration-induced flow, which is known to prevail in the lumbar region (Aktas *et al.* 2019; Gutiérrez-Montes *et al.* 2022), thereby possibly promoting drug dispersion near the injection site. Also important is the effect of the different microanatomical features that populate the spinal canal, such as denticulate ligaments, nerve roots and trabeculae (Stockman 2006; Gupta *et al.* 2008; Pahlavian *et al.* 2014; Tangen *et al.* 2015; Haga *et al.* 2017; Khani *et al.* 2018; Ayansiji *et al.* 2023). For instance, the recent experiments of Ayansiji *et al.* (2023) have shown that the presence of nerve roots significantly promotes tracer dispersion. The effect of trabeculae, which form a continuous weblike structure stretching across the spinal canal (Mortazavi *et al.* 2018), can be modeled by adding a distributed Brinkman flow-resistance term to the momentum equation, as done earlier (Gupta *et al.* 2008; Tangen *et al.* 2015; Sincomb *et al.* 2022). Nerve roots and ligaments, on the other hand, are arranged in quasi-periodic rows aligned along the canal. Their discrete nature may potentially hinder their integration in models based on a slowly varying geometry. Fundamental understanding acquired in connection with oscillatory flows in wavy channels (Guibert *et al.* 2010; Alaminos-Quesada *et al.* 2022, 2023a) and obstacle arrays (House *et al.* 2014; Bhosale *et al.* 2020; Alaminos-Quesada *et al.* 2023b) can be instrumental to aid these future modelling efforts. In this connection, it is worth mentioning the approximate transport equation recently proposed by Linninger *et al.* (2023), which incorporates a longitudinal diffusion term with an experimentally fitted diffusivity as a computationally inexpensive means to provide quantification of drug dispersion in the presence of nerve roots.

Additional *in vitro* experiments, similar to those carried out recently (Moral-Pulido

641 *et al.* 2023; Ayansiji *et al.* 2023), could be useful in guiding further model refinements.
 642 Besides consideration of effects of nerve roots, addressed in the recent work of Ayan-
 643 siji *et al.* (2023), these future efforts should specifically consider the quantification of
 644 buoyancy-induced flow, with the densities of the working fluids representing the drug and
 645 the CSF selected to match the Richardson numbers found in ITDD applications. These
 646 experiments will be challenging, because the required density differences are extremely
 647 small, so that additional care will be needed to avoid density departures stemming from
 648 temperature differences.

649 Incorporation of pharmacokinetic effects, such as tissue uptake and drug clearance by
 650 the blood, which are central to ITDD (Segal & Brunnemann 1989; Sarntinoranont *et al.*
 651 2003; Kuttler *et al.* 2010; Linninger *et al.* 2023), will be necessary to improve the
 652 predictive capability of the model in connection with clinical applications. Many drugs
 653 have characteristic absorption times on the order of the spinal residence time, so that a
 654 non-negligible fraction of the solute deposited in the lumbar region is absorbed along the
 655 canal before reaching the cranial cavity. For heavy drugs delivered in an upright position,
 656 the case depicted in figures 4(a) and 5(a), the combined effects of buoyancy forces and
 657 tissue uptake can be expected to result in drug confinement in the lumbar region, which
 658 can be beneficial for analgesic administration. In contrast, buoyancy can promote the
 659 dispersion of light drugs towards the cranial cavity, as seen in 4(c) and 5(c), thereby
 660 limiting uptake rates along the spine and enabling drug delivery to distant intracranial
 661 locations.

662 **Acknowledgement.** We thank Dr Jenna Lawrence for insightful discussions.

663 **Funding.** This work was supported by the National Institute of Neurological Disorders
 664 and Stroke through contract No. 1R01NS120343-01. The work of WC and CGM was
 665 supported by the Spanish MCIN/AEI/10.13039/501100011033 through the coordinated
 666 projects PID2020-115961RB-C31, PID2020-115961RB-C32, and PID2020-115961RA-
 667 C33.

668 **Declaration of Interests.** The authors report no conflict of interest.

669 Appendix A. Buoyancy-free velocity description

670 The solution for the velocity field in the spinal canal in the absence of buoyancy forces
 671 was given in our previous publications (Sánchez *et al.* 2018; Lawrence *et al.* 2019). A
 672 summary of the relevant formulae, needed to quantify the steady-streaming and Stokes-
 673 drift velocities appearing in the convective terms in (4.14), is given in this appendix.

674 The solution to the leading-order problem (4.1)–(4.4) is given by the harmonic func-
 675 tions (4.5), which are repeated here for convenience

$$\begin{aligned}
 u_0 &= \operatorname{Re}(ie^{it}U), v_0 = \operatorname{Re}(ie^{it}V), w_0 = \operatorname{Re}(ie^{it}W), \\
 p'_0 &= \operatorname{Re}(e^{it}P'), \hat{p}_0 = \operatorname{Re}(e^{it}\hat{P}), h'_0 = \operatorname{Re}(e^{it}H').
 \end{aligned}
 \tag{A 1}$$

The complex functions describing the spatial variations of the velocity components can

be written as

$$U = \frac{dP'}{dx}G, \quad (\text{A } 2)$$

$$W = \frac{1}{\ell} \frac{\partial \hat{P}}{\partial s} G, \quad (\text{A } 3)$$

$$V = -\frac{1}{\ell} \frac{\partial}{\partial x} \left(\ell \frac{dP'}{dx} \bar{h} \int_0^\eta G d\eta \right) - \frac{1}{\ell} \frac{\partial}{\partial s} \left(\frac{1}{\ell} \frac{\partial \hat{P}}{\partial s} \bar{h} \int_0^\eta G d\eta \right) + \left[\frac{\partial \bar{h}}{\partial x} \frac{dP'}{dx} + \frac{1}{\ell^2} \frac{\partial \bar{h}}{\partial s} \frac{\partial \hat{P}}{\partial s} \right] \eta G, \quad (\text{A } 4)$$

in terms of the auxiliary functions

$$G = 1 - \frac{\cosh[\Lambda(2\eta - 1)]}{\cosh \Lambda} \quad \text{and} \quad \int_0^\eta G d\eta = \eta - \frac{\sinh[\Lambda(2\eta - 1)] + \sinh \Lambda}{2\Lambda \cosh \Lambda}, \quad (\text{A } 5)$$

where

$$\Lambda(x, s) = \frac{\alpha \bar{h} (1 + i)}{2 \sqrt{2}}. \quad (\text{A } 6)$$

As in the main text, tildes are used throughout the appendix to denote dummy integration variables. The axial pressure variation is obtained from the boundary-value problem

$$\frac{1}{\ell} \frac{d}{dx} \left[\ell \left(\int_0^1 q ds \right) \frac{dP'}{dx} \right] + (k^2 P' + 1) \int_0^1 \gamma ds = 0; \quad \left\{ \begin{array}{ll} P' = 0 & \text{at } x = 0 \\ \frac{dP'}{dx} = 0 & \text{at } x = 1 \end{array} \right. , \quad (\text{A } 7)$$

involving the volume-flux function $\int_0^1 q ds$, with

$$q(x, s) = \bar{h} \int_0^1 G d\eta = \bar{h} \left(1 - \frac{\tanh \Lambda}{\Lambda} \right). \quad (\text{A } 8)$$

The function $P'(x)$ can be used in

$$H' = \gamma(1 + k^2 P') \quad (\text{A } 9)$$

to evaluate the canal deformation and in

$$\frac{1}{\ell} \frac{\partial \hat{P}}{\partial s} = -\frac{1}{q} \left[\frac{\partial}{\partial x} \left(\ell \int_0^s q d\bar{s} \frac{dP'}{dx} \right) + \ell(k^2 P' + 1) \int_0^s \gamma ds \right] \quad (\text{A } 10)$$

to evaluate the azimuthal pressure gradient, thereby completing the solution at leading order.

The steady streaming velocity components (u_{ss}, v_{ss}, w_{ss}) are obtained by integration of (4.6)–(4.8) with $Ri = 0$. The functions

$$\mathcal{F} = -\frac{1}{\ell} \frac{\partial}{\partial x} (\ell \langle h'_0 u_0 \rangle) + \frac{\partial}{\partial \eta} \left(\eta \langle u_0 \frac{\partial h'_0}{\partial x} \rangle \right) - \frac{1}{\ell} \frac{\partial}{\partial s} (\langle h'_0 w_0 \rangle), \quad (\text{A } 11)$$

687

$$\mathcal{F}_x = \frac{1}{\ell} \frac{\partial}{\partial x} (\ell \langle u_0^2 \rangle) + \frac{1}{h} \frac{\partial}{\partial \eta} \langle u_0 v_0 \rangle + \frac{1}{\ell} \frac{\partial}{\partial s} \langle u_0 w_0 \rangle - \frac{\eta}{h} \frac{\partial}{\partial \eta} \langle \frac{\partial h'_0}{\partial t} u_0 \rangle - \frac{\partial \bar{h}}{\partial x} \frac{\eta}{h} \frac{\partial}{\partial \eta} \langle u_0^2 \rangle - \frac{1}{\ell} \frac{\partial \bar{h}}{\partial s} \frac{\eta}{h} \frac{\partial}{\partial \eta} \langle u_0 w_0 \rangle + \frac{2}{h^3 \alpha^2} \frac{\partial^2}{\partial \eta^2} \langle h'_0 u_0 \rangle, \quad (\text{A } 12)$$

688 and

$$\begin{aligned} \mathcal{F}_s = & \frac{\partial}{\partial x} \langle u_0 w_0 \rangle + 2 \frac{\langle u_0 w_0 \rangle}{\ell} \frac{\partial \ell}{\partial x} + \frac{1}{\bar{h}} \frac{\partial}{\partial \eta} \langle v_0 w_0 \rangle + \frac{1}{\ell} \frac{\partial}{\partial s} \langle w_0^2 \rangle - \frac{\eta}{\bar{h}} \frac{\partial}{\partial \eta} \left\langle \frac{\partial h'_0}{\partial t} w_0 \right\rangle \\ & - \frac{\partial \bar{h}}{\partial x} \frac{\eta}{\bar{h}} \frac{\partial}{\partial \eta} \langle u_0 w_0 \rangle - \frac{1}{\ell} \frac{\partial \bar{h}}{\partial s} \frac{\eta}{\bar{h}} \frac{\partial}{\partial \eta} \langle w_0^2 \rangle + \frac{2}{\bar{h}^3 \alpha^2} \frac{\partial^2}{\partial \eta^2} \langle h'_0 w_0 \rangle. \end{aligned} \quad (\text{A } 13)$$

appearing on the left-hand side of (4.6)–(4.8) involve time averages of products of the leading-order functions (A 1) that can be evaluated with use of the identity $\langle \text{Re}(e^{i\tau} f_1) \text{Re}(e^{i\tau} f_2) \rangle = \text{Re}(f_1 f_2^*)/2$, which applies to any pair of time-independent complex functions f_1 and f_2 , with the asterisk $*$ denoting complex conjugates. The solution for the steady-streaming velocity can be expressed in the form

$$\frac{u_{ss}}{\bar{h}^2 \alpha^2} = -\frac{dp'_{ss}}{dx} \frac{(1-\eta)\eta}{2} + \eta \int_0^\eta \mathcal{F}_x d\tilde{\eta} - \int_0^\eta \mathcal{F}_x \tilde{\eta} d\tilde{\eta} - \eta \int_0^1 \mathcal{F}_x (1-\eta) d\eta \quad (\text{A } 14)$$

$$\frac{w_{ss}}{\bar{h}^2 \alpha^2} = -\frac{1}{\ell} \frac{\partial \hat{p}_{ss}}{\partial s} \frac{(1-\eta)\eta}{2} + \eta \int_0^\eta \mathcal{F}_s d\tilde{\eta} - \int_0^\eta \mathcal{F}_s \tilde{\eta} d\tilde{\eta} - \eta \int_0^1 \mathcal{F}_s (1-\eta) d\eta, \quad (\text{A } 15)$$

$$\begin{aligned} v_{ss} = & -\frac{1}{\ell} \frac{\partial}{\partial x} \left(\bar{\ell} \bar{h} \int_0^\eta u_{ss} d\tilde{\eta} \right) - \frac{1}{\ell} \frac{\partial}{\partial s} \left(\bar{h} \int_0^\eta w_{ss} d\tilde{\eta} \right) + \eta \left[\frac{\partial \bar{h}}{\partial x} u_{ss} + \frac{1}{\ell} \frac{\partial \bar{h}}{\partial s} w_{ss} \right] \\ & + \eta \langle u_0 \frac{\partial h'_0}{\partial x} \rangle - \frac{1}{\ell} \int_0^\eta \left[\frac{\partial}{\partial x} (\ell \langle h'_0 u_0 \rangle) + \frac{\partial}{\partial s} \langle h'_0 w_0 \rangle \right] d\tilde{\eta} \end{aligned} \quad (\text{A } 16)$$

689 in terms of the axial and azimuthal pressure gradients

$$\frac{dp'_{ss}}{dx} = \frac{12}{\int_0^1 \bar{h}^3 ds} \int_0^1 \left(\frac{1}{\alpha^2} \int_0^1 \langle h'_0 u_0 \rangle d\eta - \frac{\bar{h}^3}{2} \int_0^1 \mathcal{F}_x \eta (1-\eta) d\eta \right) ds \quad (\text{A } 17)$$

690

$$\begin{aligned} \frac{1}{\ell} \frac{\partial \hat{p}_{ss}}{\partial s} = & \frac{12}{\bar{h}^3} \frac{\partial}{\partial x} \left[\bar{\ell} \int_0^s \left(\frac{1}{\alpha^2} \int_0^1 \langle h'_0 u_0 \rangle d\eta - \frac{\bar{h}^3}{2} \int_0^1 \mathcal{F}_x \eta (1-\eta) d\eta - \frac{\bar{h}^3}{12} \frac{dp'_{ss}}{dx} \right) d\bar{s} \right] \\ & + \frac{12}{\bar{h}^3} \left(\frac{1}{\alpha^2} \int_0^1 \langle h'_0 w_0 \rangle d\eta - \frac{\bar{h}^3}{2} \int_0^1 \mathcal{F}_s \eta (1-\eta) d\eta \right), \end{aligned} \quad (\text{A } 18)$$

691 which complete the determination of the steady-streaming velocity. On the other hand,
692 the Stokes-drift velocity components, which provide an additional contribution to the
693 time-averaged Lagrangian drift driving convective transport in the slow time scale, can
694 be expressed in the form

$$\begin{aligned} u_{SD} = & \frac{1}{\bar{h}} \left\{ \langle u_0 h'_0 \rangle + \frac{1}{\ell} \frac{\partial}{\partial s} \left(\bar{h} \left\langle u_0 \int w_0 dt \right\rangle \right) \right\} \\ & + \frac{1}{\bar{h}} \frac{\partial}{\partial \eta} \left\langle u_0 \left[\int v_0 dt - \eta \left(h'_0 + \frac{1}{\ell} \frac{\partial \bar{h}}{\partial s} \int w_0 dt \right) \right] \right\rangle, \end{aligned} \quad (\text{A } 19)$$

$$\begin{aligned} v_{SD} = & \frac{1}{\ell} \frac{\partial}{\partial x} \left(\bar{\ell} \left\langle v_0 \int u_0 dt \right\rangle \right) + \frac{1}{\ell} \frac{\partial}{\partial s} \left\langle v_0 \int w_0 dt \right\rangle \\ & - \frac{\eta}{\bar{h}} \frac{\partial}{\partial \eta} \left\langle v_0 \left(h'_0 + \frac{\partial \bar{h}}{\partial x} \int u_0 dt + \frac{1}{\ell} \frac{\partial \bar{h}}{\partial s} \int w_0 dt \right) \right\rangle, \end{aligned} \quad (\text{A } 20)$$

$$\begin{aligned} w_{SD} = & \frac{1}{\bar{h}} \left[\langle w_0 h'_0 \rangle + \frac{\partial}{\partial x} \left(\bar{h} \left\langle w_0 \int u_0 dt \right\rangle \right) \right] \\ & + \frac{1}{\bar{h}} \frac{\partial}{\partial \eta} \left\langle w_0 \left[\int v_0 dt - \eta \left(h'_0 + \frac{\partial \bar{h}}{\partial x} \int u_0 dt \right) \right] \right\rangle, \end{aligned} \quad (\text{A } 21)$$

695 where the different time averages can be evaluated with use of the expressions (A 1)
 696 and associated antiderivatives $\int u_0 dt = \text{Re}(e^{it}U)$, $\int v_0 dt = \text{Re}(e^{it}V)$, and $\int w_0 dt =$
 697 $\text{Re}(e^{it}W)$.

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