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Authors

Deng, Shijie
Jolly, Brandon J
Wilkes, James R
[et al.](#)

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1 **Spatiotemporal control for integrated catalysis**

2 Shijie Deng,^{1,#} Brandon J. Jolly,^{1,#} James R. Wilkes,² Yu Mu,² Jeffery A. Byers,² Loi H. Do,³ Alexander J. M.
3 Miller,⁴ Dunwei Wang,² Chong Liu,¹ and Paula L. Diaconescu^{1*}

4 ¹Department of Chemistry and Biochemistry, University of California, Los Angeles, 607 Charles E. Young
5 Drive East, Los Angeles, California 90095, United States

6 ²Department of Chemistry, Eugene F. Merkert Chemistry Center, Boston College, 2609 Beacon Street,
7 Chestnut Hill, Massachusetts 02467, United States

8 ³Department of Chemistry, University of Houston, 4800 Calhoun Road, Houston, Texas 77004, United
9 States

10 ⁴Department of Chemistry, University of North Carolina at Chapel Hill, Chapel Hill, North Carolina 27599-
11 3290, United States

12 [#]These authors contributed equally.

13 ^{*}Corresponding author: pld@chem.ucla.edu

14 **Abstract**

15 Integrated catalysis is an emerging methodology that can streamline the multistep synthesis of
16 complicated products in a single reaction vessel, achieving a high degree of control and reducing the waste
17 and cost of an overall chemical process. Integrated catalysis can be defined by the use of spatial and
18 temporal control to couple different catalytic cycles in one pot. This primer discusses commonly employed
19 approaches and their underlying mechanisms, and elaborates on how the integration of spatially and
20 temporally controlled catalysis in one pot can deliver the synthesis of complex products with high
21 efficiency. We highlight recent advances, analyze current applications and limitations, and provide an
22 outlook for the future development of integrated catalysis.

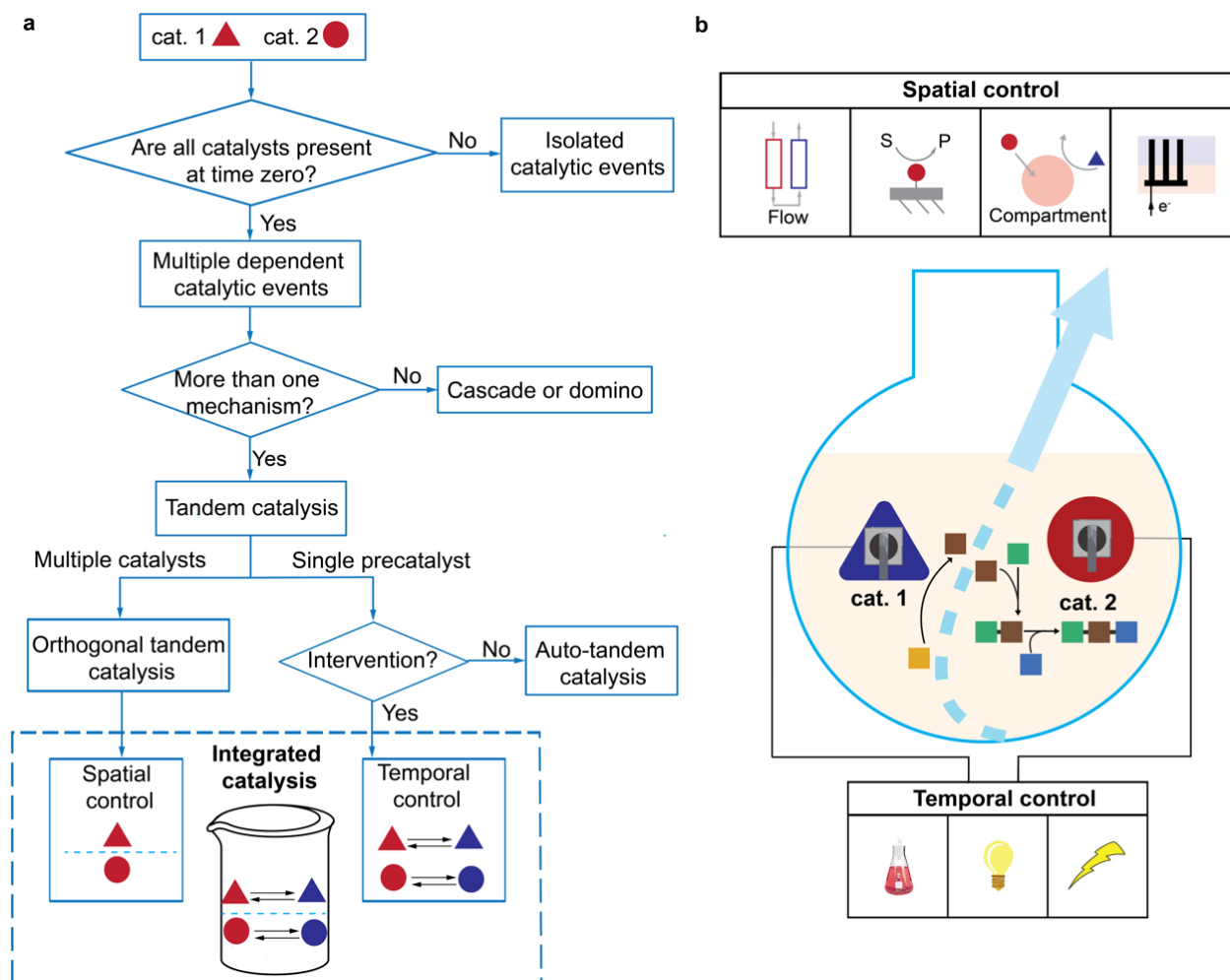
23 [H1] Introduction

24 Chemical synthesis plays a crucial role in modern technology and everyday life. From plastics to
25 pharmaceuticals, virtually every facet of society is impacted by our ability to construct small molecules
26 and macromolecules. A major focus in chemical research is the development of efficient methods for the
27 production of synthetic chemicals. In 2017, the chemical industry was responsible for 10% of the total
28 annual global energy consumption (and 28% of industrial energy consumption).^{1,2} Thus, alternative
29 approaches to chemical synthesis that minimize energy consumption and increase efficiency are needed.

30 The majority of commodity chemicals, pharmaceuticals and consumer materials are prepared in multistep
31 syntheses that require catalysts to achieve high yields with selectivity toward the desired products.³ A
32 drawback of such methods is that they require time, energy, and exhaustive effort between reaction steps
33 to separate and purify stable reaction intermediates. Alternative methods that enable multistep
34 sequences would remove the need to isolate such species. A particularly attractive approach for chemical
35 synthesis is integrated catalysis, in which multiple catalysts are carefully controlled and positioned to
36 allow efficient multistep reaction sequences, funneling products generated by one catalyst to the next.

37 A combination of catalytic processes, either involving one catalyst or multiple catalysts with orthogonal
38 reactivity, (FIG. 1a)⁴ may be classified as a **cascade or domino process [G]** if only one linear reaction
39 sequence occurs. If multiple reactions are proceeding simultaneously, then it is considered a **tandem**
40 **process [G]**. Examples of integrated catalysis are often special cases of tandem catalysis, in which multiple
41 catalysts operate through orthogonal mechanisms synergistically or can be switched on/off using external
42 triggers. The recent literature has many excellent examples of cascade or tandem processes,⁴⁻²⁰ but
43 integrated processes are rarely reported. Multiple catalytic processes operating together could be solely
44 chemo- or bio- based, or a combination of the two. In this primer, we will focus on chemocatalytic
45 systems.

46 Integrated reactions hold promise to be more efficient than an iterative process; combining spatial and
47 temporal control avoids the need for separation and purification of intermediate steps. Furthermore,
48 combining spatial and temporal control may also lead to the development of new chemistry and novel
49 products. For example, a hypothetical integrated catalytic system (FIG. 1b) with spatiotemporal control
50 can allow the efficient conversion of a starting material (gold square) to an intermediate (brown square).
51 This intermediate can diffuse to another part of the reactor where a second catalyst, spatially separated
52 so as not to interact with the first catalyst, reacts with and couples the intermediate with a second
53 reactant (green square). The second catalyst may also be temporally switched to a state where it is now
54 active for the incorporation of a third reactant (blue square). This approach could be a general strategy to
55 synthesize complex structures that are not accessible using conventional methods, as such methods do
56 not typically consider spatial and temporal control.



57

58 **Fig. 1 | Concept of integrated catalysis.** a | A flowchart guide to nomenclature of different multistep one-pot catalytic
 59 processes. b | Illustration of integrated catalysis. In a hypothetical integrated catalytic system with spatiotemporal
 60 control, the starting material (gold square) is efficiently converted to an intermediate (brown square). This
 61 intermediate could then react with another catalyst that would combine the synthesized intermediate with another
 62 reactant (green square). The second catalyst can also be switched on to incorporate a third reactant (blue square).
 63 This approach can be a general strategy for synthesizing complex structures that are not available by conventional
 64 methods. Temporal control methods include external stimuli, e.g., chemical reagents, light, electron transfer, etc.,
 65 whereas spatial control can be achieved by using flow chemistry, immobilization, compartmentalization, and
 66 microscopic concentration gradients.

67

68 To enable multiple catalysts to operate concurrently, issues relating to compatibility must be overcome.
 69 For example, potentially problematic catalyst-catalyst, catalyst-reactant, and catalyst-product
 70 interactions need to be addressed. To reconcile potential incompatibility, spatial and/or temporal control
 71 are required to manipulate where and when certain processes occur. Spatial control may be employed to
 72 localize and separate catalysts or entire catalytic systems from each other. This may be achieved in a
 73 number of approaches (vide infra), namely **compartmentalization** [G],^{8,21-27} immobilization onto a

74 surface,²⁸⁻³⁵ or by taking advantage of microscopic concentration gradients.^{18,20,36,37} By preventing
75 incompatible species from coming into contact with each other, efficient integrated processes may be
76 promoted. In addition to spatial control, introducing temporal control can also alleviate compatibility
77 concerns. If two processes compete with or hinder each other's activity, deactivating one while the other
78 is active can help avoid incompatibility. Temporal control may be achieved using a variety of external
79 stimuli³⁸⁻⁴¹ to switch between different states of a catalyst that have **orthogonal reactivity [G]** toward
80 certain substrates.

81 In this primer, approaches to achieve spatial and temporal control in catalysis to achieve integrated
82 catalysis are discussed. Seminal studies illustrating spatiotemporal control of catalysts will be presented
83 to showcase their impact on some of the most challenging problems in catalysis. The development of a
84 toolbox for integrated catalysis is also discussed, followed by limitations and suggested optimizations for
85 this nascent field of research. Lastly, the direction in which integrated catalysis is likely to make progress
86 in the next 5-10 years is discussed.

87

88 **[H1] Experimentation**

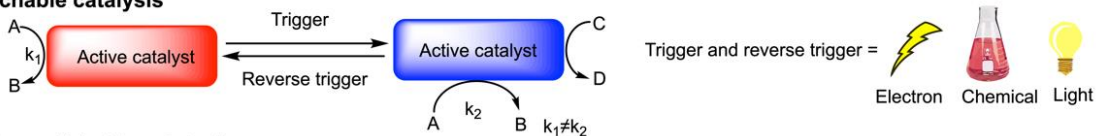
89 This section outlines considerations for the temporal and spatial control of a number of catalytic systems.
90 By the use of examples, reaction processes and mechanisms are discussed, as well as considerations for
91 each catalytic system. The typical setup for catalytic systems and design considerations for such systems
92 are described.

93 **[H2] Temporal control**

94 In nature, living organisms have the ability to respond to environmental factors, causing them to behave
95 differently or take on different forms. At the microscopic level, external stimuli regulate feedback loops
96 and modulate enzymatic reactions within cells to effect biological changes. Taking inspiration from nature,
97 scientists have been working on artificial catalytic systems that could be tuned reversibly by external
98 stimuli. In such switchable systems, a catalyst could be toggled on/off or may oscillate between different
99 catalytic states to achieve orthogonal reactivity. Depending on the application and reaction conditions,
100 different external stimuli can be used to implement a switchable behavior. In this section, redox, chemo-,
101 and photo-switching will be discussed, with a focus on the switching mechanisms and general catalyst
102 design concepts. Several comprehensive reviews have been published on temporally switchable
103 catalysis.^{38,40-43}

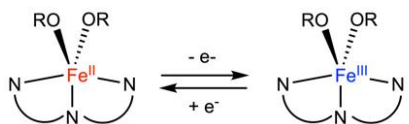
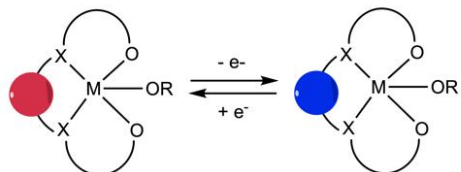
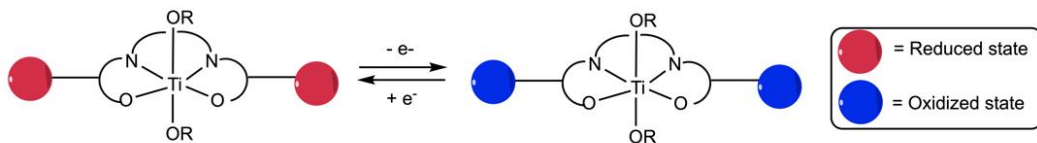
104

a Switchable catalysis

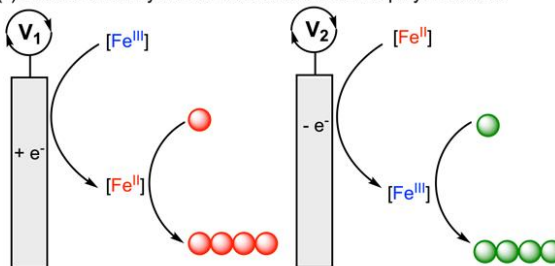


b Redox switchable catalysis

(i) Redox switchable metal catalyst

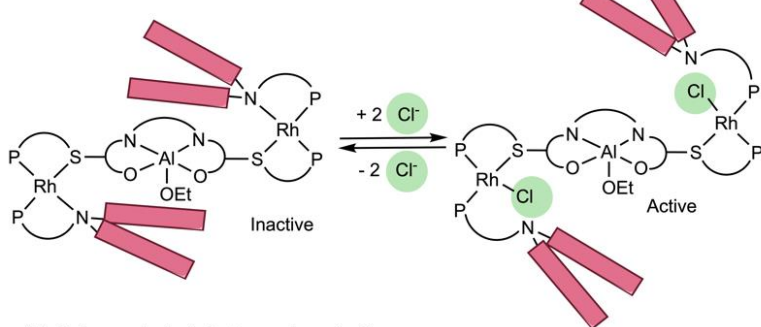


(ii) Electrochemically controlled redox switchable polymerization

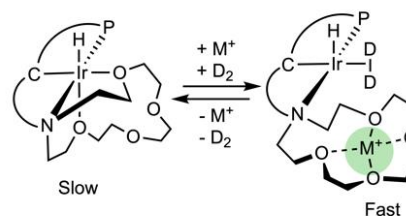


c Chemoswitchable catalysis

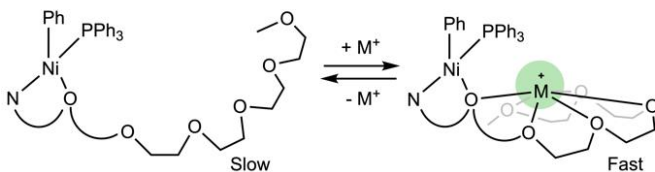
(i) Allosteric controlled lactone polymerization



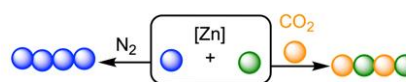
(ii) Cation controlled hydrogen activation



(iii) Cation controlled ethylene polymerization

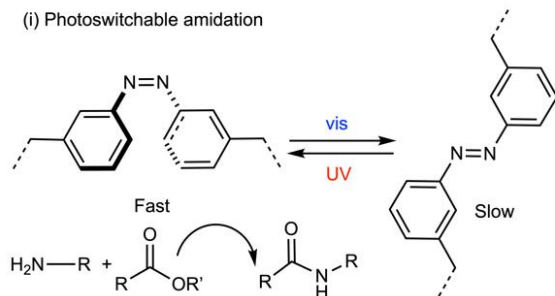


(iv) CO₂ controlled polymerization

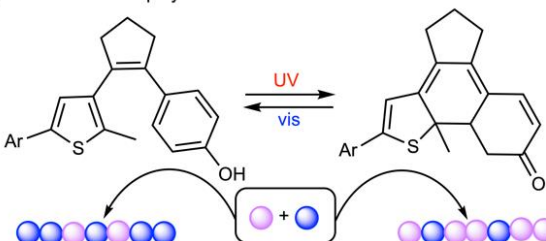


d Photoswitchable catalysis

(i) Photoswitchable amidation



(ii) Photoswitchable polymerization



106 **Fig. 2 | Different types of switchable catalysis as temporal control.** a | Switchable catalysis using different external
107 stimuli. b | Redox-switchable catalysis. (i) Design of a redox-switchable metal catalyst. (ii) Redox-switchable
108 polymerization using electrochemical setup. Fe(II) catalyst can polymerize lactide (red ball) while the Fe(III) catalyst
109 can polymerize cyclohexene oxide (green ball). c | Chemoswitchable catalysis. (i) Anion coordination leads to
110 allosteric change which unblocks the catalytic active center for the ring opening polymerization of ϵ -caprolactone.
111 The red block denotes a bulky aromatic group that results in steric hindrance. (ii) Metal cation coordination onto the
112 hemilabile crown ether moiety promotes the hydrogen activation reaction. (iii) Metal cation coordination to the
113 oligomeric ethylene glycol chain increases ethylene polymerization activity. (iv) Presence of CO₂ prevents the
114 polymerization of ϵ -caprolactone (blue ball) and initiates the ring opening copolymerization of CO₂ and cyclohexene
115 oxide (green ball). d | Photoswitchable catalysis. (i) The catalyst can bind to the substrates via hydrogen bonds; in
116 the E form the catalyst can bring the substrates closer and accelerate the amidation process, while the Z form
117 separates the substrates apart and thus slows down the amidation. (ii) The diarylethene-type catalyst with a phenol
118 moiety in the ring-opened phenol form incorporates more valerolactone (blue ball) while the ring-closed ketone
119 form incorporates more trimethylene carbonate (purple ball) in the copolymerization process. (iii) By using different
120 photocatalysts and changing the wavelength of light, the polymerization mechanism can switch between radical and
121 cationic polymerization.

122

123 [H3] Redox-switchable catalysis

124 A challenge associated with achieving switchable catalysis is designing a system that has two (or more)
125 different reactive states that can be accessed through application of external stimuli. Since redox reactions
126 change the electronic configuration of a compound, which is intimately associated with its reactivity, an
127 attractive option for switchable catalysts is through iterative addition of oxidants or reductants. A
128 common way to carry out **redox-switchable catalysis [G]** is to design redox-active ancillary ligands⁴⁴⁻⁴⁶ that
129 are coordinated to a redox-inactive metal, which serves as the site for catalysis. This strategy was
130 employed in the first example of redox-switchable catalysis,⁴⁷ when a rhodium complex supported by a
131 cobaltocene bis(phosphine) was used for the hydrogenation and isomerization of alkenes. Despite this
132 first example being applied to catalysis involving small molecules, the utility of redox-switchable catalysis
133 has been exploited with more success in polymerization. For example, a titanium complex containing two
134 redox-active ferrocene moieties appended to a salen (N,N'-bis(salicylidene)ethylenediamine) ancillary
135 ligand (FIG. 2bi)⁴⁸ demonstrated redox modulation when used for the polymerization of lactide, with the
136 reduced species being more active than the oxidized form of the catalyst. Since this report, several groups
137 have utilized the ferrocene moiety for redox-switchable polymerization.⁴⁹⁻⁵⁴ For example, using chelating
138 ligands to position the ferrocene moiety in close proximity to the redox-inactive site for catalysis results
139 in a greater difference in the reaction rate of the oxidized and reduced states of a catalyst (FIG. 2b). For
140 example, while both forms of the above titanium complex demonstrated some activity for lactide
141 polymerization, an yttrium complex showed complete on/off activity for lactide polymerization.⁵⁵

142 An alternative method for redox-switchable catalysis is to use redox-active metals that serve as the redox-
143 switching moiety and the site for catalysis (FIG 2bi). Catalysts based on several different redox-active
144 metals have been explored using this strategy, with the most notable examples being ring-opening
145 polymerization catalysts using cerium salen⁵⁶ and iron bis(imino)pyridine complexes.⁵⁷ These catalysts

146 show similar behavior as that of polymerization catalysts utilizing redox-active ancillary ligands,
147 demonstrating that it is not necessary to separate the redox-switching entity from the catalytically active
148 entity.

149 A challenge associated with redox-switchable catalysis is the need to add oxidants and reductants to the
150 reaction. When chemical redox reagents are used, purification of the product is required to remove the
151 byproducts from the redox-switch. Moreover, adding chemical redox reagents to reactions that require
152 gaseous reagents at elevated pressures requires specialized equipment. To address these limitations, an
153 electrochemical potential can be used instead of chemical redox reagents for redox switching (FIG. 2bii).
154 Such electrochemical potential can be achieved by employing bis(imino)pyridine iron complexes whose
155 redox-active site is also the site for catalysis,⁵⁸ or catalysts that contain redox-switchable moieties installed
156 in the ancillary ligand.⁵⁹

157 While there are now many redox-switchable catalysts, a mechanistic understanding of how these systems
158 perform redox switching is not well established. The oxidation state of the active catalyst and the
159 efficiency of the redox switch are dependent on many factors. In addition to the proximity of the redox-
160 switching moiety to the catalytically active site, another important factor is the identity of the metal center.
161 For example, while the yttrium complex is active for lactide polymerization in its reduced state, the indium
162 complex that contains the same ancillary ligand is active for lactide polymerization in its oxidized state.⁵⁵
163 The interaction between the metal center and the redox switchable moiety can be intricate; as revealed
164 by computational and experimental studies,^{60,61} the oxidation state of the redox active group can alter the
165 Lewis acidity of the metal center, as well as change the energetic profile of the catalyst-substrate
166 interaction.⁶² Another factor is the identity of the reactant; some reactants may display orthogonal
167 reactivity with respect to the oxidation state of the catalyst and some may not. For example, the iron
168 complex shown in FIG. 2bii,⁶³ as well as other redox switchable catalysts,^{51,53,55,60,64,65} is capable of
169 polymerizing lactide selectively in its reduced form and epoxide in its oxidized form, but less selectivity is
170 observed for lactones or cyclic carbonates.^{61,64,66-68} The selectivity shown by each state of the system, i.e.,
171 orthogonal reactivity, is important in being able to combine multiple catalytic cycles without interference
172 from the reaction that is turned off, for example. While more work is needed to understand these and
173 other effects, two related factors appear to be important in polymerization catalysis: the propensity of
174 the monomer to bind to the catalytically active site and the electrophilicity/nucleophilicity of reactive
175 intermediates.^{61,67,69} Both factors are altered by changing the oxidation state of the catalysts, and the
176 relative importance of each is related to the nature of each reaction, including the identity of the metal
177 centers and the monomers employed.

178

179 [H2] Chemoswitchable catalysis

180 Chemoswitchable catalysts are compounds that are responsive to the presence of external chemical
181 additives. Unlike redox-switchable catalysis, chemoswitchable catalysis [G] does not involve alterations to
182 the catalyst that leads to changes in their formal oxidation state. Because chemical reagents have a wide
183 range of properties, they can trigger molecular events via various modes of action. For example, cations

184 can bind Lewis basic sites, whereas anions can bind Lewis acidic sites. Such interactions could turn a
185 catalyst on or off, or modulate their reaction rates. Alternatively, chemical reagents could covalently
186 modify a catalyst to produce another active species capable of achieving orthogonal reactivity.

187 The key design challenge in chemoswitchable catalysis is to enable a catalyst to change its structure and
188 function by interacting with a chemical additive. One effective strategy for chemoswitchable reactivity
189 involves regulating catalysis using anion coordination/dissociation to alter the metal complex geometry
190 or block/unblock catalytically active sites. For instance, a supramolecular triple layer catalyst, comprising
191 an aluminum salen complex flanked by two rhodium nodes equipped with biaryl blocking groups, was
192 used for the chemoswitchable polymerization of lactones (FIG. 2ci). In the closed form, the rhodium
193 centers are ligated by the amino donor of the supporting ligand, which positions the biaryl units above
194 and below the aluminum active site.⁷⁰ Because aluminum is inaccessible due to the steric bulk of the
195 amino arms, the catalyst cannot react with substrates. In the open form, chloride anions are bound to
196 rhodium so that the amino groups are forced away from aluminum, opening up access to incoming
197 monomers. When chloride salts are added, the triple layer catalyst reaches an open state that is active
198 for the ring-opening polymerization of ϵ -caprolactone; when sodium salts are added, the chloride is
199 abstracted from the rhodium centers, re-forming the closed catalyst state and almost completely stopping
200 the polymerization. Remarkably, the molecular weight of the polymer increased linearly with conversion
201 even as the catalyst was activated, deactivated, and reactivated, indicating an excellent control over
202 catalysis.

203 Another strategy for chemoselective switching is to regulate catalysis using cations. By installing crown
204 ether moieties in ancillary ligands, alkali metal cations can interact with the crown ether moiety to tune
205 the electron density of the catalytically active site. This type of cation switching has been well-
206 demonstrated in small molecule activation (FIG. 2cii).⁷¹ For example, an iridium PCN-pincer complex was
207 prepared containing an aza-crown ether macrocycle, which serves as a hemilabile ligand and cation
208 receptor. When sodium or lithium tetraarylborate salts were added to a CD_2Cl_2/Et_2O solution of the
209 compound, the free energy of aza-crown ether dissociation from iridium is lowered due to the favorable
210 interaction of the alkali metal ion with the macrocycle. In the presence of these alkali metal cations,
211 binding of dihydrogen becomes possible, and the cation-activated iridium species catalyzed H/D exchange
212 with D_2 is significantly faster than the unactivated complex. This concept can be extended to a three-state
213 (off/slow/fast) catalyst system, such as the positional olefin isomerization.⁷² For example, iridium chloride
214 complex is inactive for isomerization of allylbenzene; removal of the chloride produces a cationic species
215 with hemilabile Ir–O interactions resulting in a slow catalyst. Addition of Li^+ salts to this cationic catalyst
216 enhances the isomerization rate over 1,000-fold. The rate enhancement is attributed to cation–crown
217 interactions making olefin binding more favorable, and increasing the amount of iridium that is actively
218 engaged in catalysis. Another example of a cation-switchable system was used to achieve regioselectivity
219 in positional isomerization: without salts added, alkenes were isomerized from the 1- to the 2-position;
220 under the same conditions but with added Na^+ salts, 3-alkenes were observed instead.⁷³

221 The cation coordination strategy of a catalyst can be used to tune not only the reaction rates but also the
222 architecture of a polymer product.⁷⁴ For example, a family of nickel phenoxyimine complexes bearing

223 polyethylene glycol (PEG) chains can coordinate secondary metals (FIG. 2ciii); the addition of M^+ (where
224 $M^+ = Li^+, Na^+, \text{ or } K^+$) can produce 1:1 and 2:1 nickel: alkali species. The association constants between Ni
225 and M^+ correlated with the size match between the ionic radius of M^+ and the chain length of the PEG
226 chelator (larger cations require longer PEG chains and vice versa). Combining Na^+ or K^+ with the nickel
227 catalysts featuring tri- or tetra-ethylene glycol chains increased the ethylene polymerization activity and
228 gave polymers with higher molecular weight and branching density than the nickel catalysts alone. Cation-
229 tuning was also applied to other olefin polymerization platforms and catalyst nuclearity was controlled
230 through suitable ligand design.⁷⁵⁻⁷⁸

231 Small gas molecules can also be utilized as chemoselective switches by serving either as a trigger or a
232 substrate for a reaction. For example, CO_2 can be used to oscillate a catalytic system between ring opening
233 polymerization [G] (ROP) of a lactone and ring opening copolymerization (ROCOP) of epoxides and CO_2
234 (FIG. 2civ).^{79,80} Another example of a small gas molecule switch is O_2 . Although more well-known as a
235 radical scavenger, O_2 can also be used in chemical transformations to generate radical species that can
236 initiate radical polymerization.^{81,82} Small gas molecules have the advantage of being easy to remove,
237 however, a pressure reactor might be needed for the reaction.

238 Such examples demonstrate that chemical switching can be a useful strategy for regulating many different
239 catalytic processes. Chemical switching can also take advantage of solution equilibria to tune reaction
240 rates in a dynamic fashion. In cation tuning, different amounts or types of metal salts can be used to
241 achieve different effects without requiring tedious synthetic modifications of the catalyst. Ideally, the
242 chemical switch is only needed in catalytic amounts relative to the substrate (for example, in cation
243 switching) or is incorporated into the reaction product (such as in CHO and CO_2 ROCOP). Some possible
244 disadvantages of chemical switching are that the chemical reagents used are not traceless so they may
245 need to be removed from the final product or they might not be compatible with subsequent steps in
246 one-pot tandem or cascade reactions. Another potential limitation in cation switching is that the catalyst
247 must be amenable to installation of secondary metal binding groups to achieve high cation responsiveness
248 since Lewis acid additives are relatively commonly used to enhance activity.⁸³

249

250 [H3] Photoswitchable catalysis

251 Photoresponsive processes are ubiquitous in nature and in artificial synthesis and catalysis.
252 Photoswitchable catalysis involves a catalytically active species that can undergo a reversible
253 photochemical transformation, which consequently changes its intrinsic catalytic properties.⁸⁴ In
254 photoswitchable catalysis, photochromic functionalities such as azobenzenes, which can undergo an E-Z
255 isomerization, and diarylethenes, which can undergo a photo-induced ring closing, are commonly
256 employed.

257 The photoinduced E-Z isomerization of diarylethenes and stilbenes can lead to a change in the steric
258 environment of the active site, which can block or unblock substrate access or bring substrates closer
259 together or further apart, thus changing the catalytic activity.⁸⁵ Such azobenzene photochromic
260 functionality has been used to control the rate of an amidation reaction (FIG. 2di).⁸⁶ For example, for the

261 amidation between aminoadenosine and adenosine-derived *p*-nitrophenol ester, a template molecule
262 that contains two adenine receptors linked by an azobenzene spacer was designed. When the template
263 molecule is in the E configuration, substrates bound to each receptor are far apart, resulting in a slow
264 coupling rate. Upon UV irradiation ($\lambda_{\text{ex}} = 366 \text{ nm}$), the template molecule undergoes a photo-induced
265 isomerization, resulting in a photostationary state ratio of E:Z = 1:1. The Z configuration brings the two
266 substrates in close proximity, thereby accelerating the reaction.

267 The photoinduced ring opening or ring closing of photochromic functionalities, such as spiropyran^{87,88}
268 and diarylethenes,⁸⁹ results in steric and electronic changes that have been used to alter rates of lactone
269 polymerization. For example, in a diarylethene-based system (FIG. 2dii),⁹⁰ the ring-opened phenol catalyst
270 uses the exposed -OH group to activate lactide, which leads to a high polymerization rate. Upon UV
271 irradiation ($\lambda_{\text{ex}} = 300 \text{ nm}$), a photostationary state is reached, leading to 98% of the ring-closed ketone
272 isomer, which shows a diminished polymerization rate. The system can be turned back on to the active
273 state by irradiation with visible light. The different rates of the opened and closed forms toward
274 valerolactone and trimethylenecarbonate (TMC) polymerization can also be harnessed to control the
275 microstructure of the polymers. The ring-opened phenol catalyst, incorporates more valerolactone than
276 TMC to synthesize copolymers with higher valerolactone content, while the ring-closed ketone isomer
277 leads to a polymer with higher TMC than valerolactone content.

278 Unlike most redox-switchable and chemoswitchable catalysts, photoswitchable catalysis provides a non-
279 invasive method to achieve temporal control since light is the only reagent required for switching.
280 Consequently, product purification does not require removing excess reagents. Additionally, switching
281 can be fast and not limited by mass transport.^{91,39,92} A combination of different polymerization
282 mechanisms can also be achieved by changing the wavelengths of light. For example, by using
283 photocatalysts and a thiocarbonate chain transfer agent, cationic polymerization could be initiated by
284 green light, while radical polymerization could be commenced by blue light (FIG. 2diii).⁹³ In terms of the
285 experimental setup, light-emitting diodes are typically used as a source of light with specific and narrow
286 wavelength. Although photoswitchable catalysis shows many advantages in temporal control, it also
287 needs to overcome several hurdles such as obtaining a high photostationary state isomer ratio with a
288 short irradiation time, finding isomers with orthogonal reactivity, and using UV light, which limits
289 compatibility with some organic substrates or metal catalysts.

290

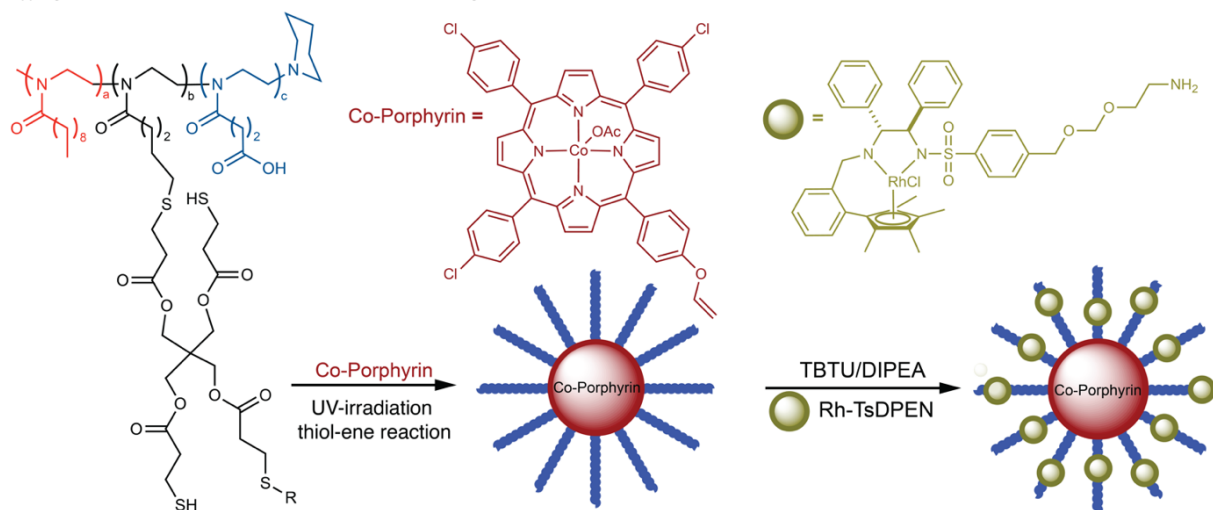
291 [H2] Spatial control

292 Spatial control in catalysis refers to the localization or separation of a catalyst from other species in
293 reaction media. There are many reasons why spatial control is desirable, ranging from mitigating
294 incompatibility between reagents/catalysts^{8,13,18,20,21,23-27,94-99} to simple heterogenization of a catalyst to
295 be recycled,^{23,100-107} and opportunities to capitalize on local concentrations of reagents and effects that
296 may occur from local magnetic or electric fields.^{20,37,108-110} Spatial control may be realized in numerous
297 ways, with the bulk of this work centered around confining catalysts within compartments,^{8,13,20,23,25-27}
298 using biphasic conditions,¹¹¹⁻¹¹⁴ and immobilizing catalysts onto supports.¹⁰⁰⁻¹⁰³ The last few decades have

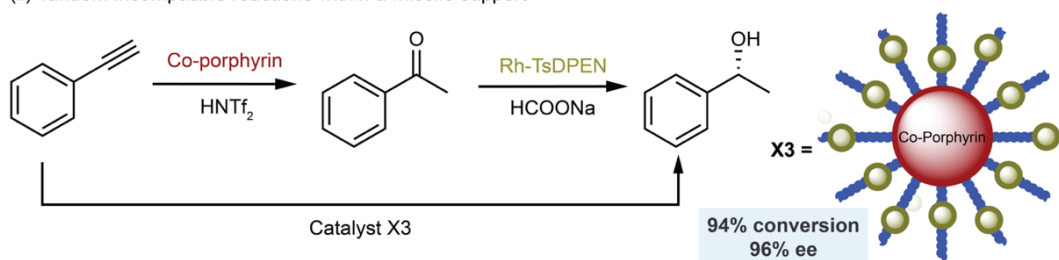
299 witnessed a steady growth in exploring the spatial control of molecular catalysts, with several reviews
 300 outlining the intricacies and caveats of localizing catalysts.^{23,26,97,100} Here, the motivations and working
 301 principles for spatial control are discussed, all within the context of ultimately utilizing spatial localization
 302 to control multiple catalysts in proximity and circumvent potential challenges in integrating catalysis to
 303 carry out catalytic transformations that are not trivial for homogeneous catalysts.

a Compartmentalization of two catalysts in micelles

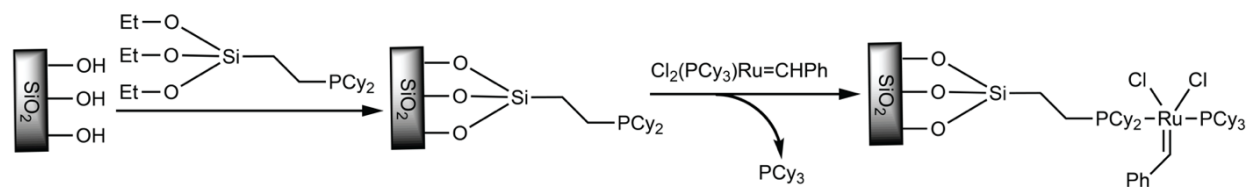
(i) Synthetic scheme for micelle formation and catalyst confinement



(ii) Tandem incompatible reactions within a micelle support



b Catalyst immobilization onto an oxide support



304
 305 **Fig. 3 | Approaches to spatial control via compartmentalization of catalysts in close proximity within confined**
 306 **spaces.** a | (i) Micelle support with the synthetic scheme for micelle formation. An amphiphilic ABC-triblock
 307 copolymer was used to form the micelle support. The cobalt catalyst was covalently attached to the hydrophobic
 308 core (red and black blocks) via the thio-ene reaction, while the rhodium catalyst was attached to the hydrophilic arm
 309 (blue block). (ii) Tandem alkyne hydration and hydrogenation. b | Immobilization of two species in close proximity
 310 onto an oxide surface for synergistic catalysis.

311

312 [H3] Compartmentalization

313 Two major forms of spatial control are compartmentalization and **surface immobilization [G]**. The key
314 challenge in compartmentalization is to design a system that keeps each catalyst inside a specific
315 compartment while allowing reactants, intermediates, and products to move between the compartments.
316 Compartmentalization has been reported in the biocatalytic literature as an approach for constructing
317 efficient tandem catalysis by separating enzymes in well-defined micro- and nano-structures.^{21,22,115-119} In
318 doing so, compartmentalization results in beneficial circumvention of deactivating or competing pathways,
319 retention of reactive or toxic intermediates, increases in reaction rates and high local substrate
320 concentration.^{21,22,115-119} Inspired by the mechanistic work on in vivo compartmentalization, spatial
321 organization at the nano- and microscopic levels has been implemented to construct in vitro biomimetic
322 cascades with augmented catalytic performance.^{22,26,95,99,117,120,121} For example, confining the β -galactose,
323 glucose oxidase, and horseradish peroxidase in metal-organic frameworks led to an enhancement of the
324 reaction yield in comparison to a freely diffusing enzyme.^{26,95} Additionally, encapsulation of a nickel-iron
325 hydrogenase in capsids enhanced the rate of H₂ production and improved the enzyme's thermal
326 stability.¹²¹

327 Following the wealth of literature in applications of bio-compartmentalization, the organometallic
328 community has subsequently made great strides in confining transition metal-based catalysts. Of
329 relevance to integrated catalysis, compartmentalization may be used to construct efficient tandem,
330 heterogeneous, organometallic systems that otherwise cannot be achieved with homogeneous
331 catalysts.^{8,13,18,20,27} The majority of prior confined organometallic catalysts focuses on employing
332 macromolecular structures to tune selectivity in a manner unachievable in a homogeneous setting.²³
333 Additionally, the confinement of such catalysts often results in an improved stability and heightened
334 activity over freely diffusing analogues.²³ Furthermore, compartmentalization has been applied to
335 organometallic-mediated catalytic chain transfer polymerization, from which insight into the relationship
336 between confinement and polymer modality has been extensively studied.¹²²⁻¹²⁴

337 Organometallic catalyst(s) can be compartmentalized by encapsulation in molecular cages to accelerate
338 reaction rates and alter selectivity.^{23,125-129} One example of compartmentalization is the selective
339 recognition and stabilization of imminium ions by a Ga(III) catecholate molecular cage.¹³⁰ The
340 compartmentalization of catalysts in molecular cages has been extensively applied in various reactions,
341 such as aza-Prins cyclizations,¹³¹ to promote kinetically disfavored pathways and thus steer selectivity.¹³¹
342 One way to do this is using a micelle to support two co-encapsulated catalysts for incompatible catalytic
343 reactions (FIG. 3a).⁸ For example, in the direct conversion of an alkyne to an enantioenriched secondary
344 alcohol, the Co-porphyrin catalyzed hydration of alkyne to ketone was not compatible with the Rh-TsDPEN
345 catalyzed asymmetric hydrogenation of ketone to secondary alcohol, and when the two catalytic reactions
346 were carried out in tandem, no product was detected. To bypass the issue, the cobalt catalyst was
347 immobilized in the hydrophobic core of the micelle and the rhodium catalyst in the hydrophilic shell thus
348 separating the two catalytic systems in two different domains to avoid interference. The intra-micellar
349 diffusion of the ketone intermediate was fast enough to render high efficiency to the overall reaction.

350 Changing the local environment of a catalyst may understandably alter its catalytic properties, such as
351 activity. Thus, in the realm of confinement via compartmentalization, a judicious design and choice of
352 compartments will be paramount.¹³² A likely pitfall of this approach may be a deleterious reduction in
353 activity. To circumvent this, we point out a recent report that modeled the effect of varying compartment
354 dimensions on catalytic activity for several common catalytic cycles.²⁷ Ultimately, a confinement must be
355 employed carefully so that entry and exit into the compartment via diffusion is as fast as or slower than
356 the kinetics of the catalytic cycle.

357

358 *[H3] Surface immobilization*

359 Another way to achieve spatial control over a reaction is by attaching a molecular catalyst onto a solid
360 support material, also known as **surface immobilization [G]**.^{28,30-35,133-135} A rich history of surface
361 attachment of catalysts has led to a diverse lexicon: a compound can be attached, anchored, or
362 immobilized to produce a surface-supported or surface-immobilized catalyst. Sometimes such systems
363 are referred to as single-site heterogeneous catalysts because, ideally, the molecular nature of the catalyst
364 leads to excellent homogeneity in catalyst activity and selectivity, while also boasting the benefits of a
365 heterogeneous catalyst (for example, easy separation from reactants/products, facile recycling). An
366 immobilized catalyst will only carry out the reaction where it is anchored to the surface, controlling the
367 location of product generation. Furthermore, two or more catalysts can each be attached to a surface in
368 order to prevent unwanted interactions and ensure catalyst compatibility, an invaluable aspect in
369 integrated catalysis. For example, a palladium catalyst and an organic base were co-immobilized in close
370 proximity onto a silica surface (FIG. 3b).¹³⁶⁻¹³⁸ Synergism was realized by a significant acceleration (3 times
371 higher conversion) of palladium catalyzed Tsuji–Trost allylic alkylation reactions with the co-immobilized
372 palladium catalyst and organic base material, in comparison to a palladium catalyst on the silica surface
373 without an organic base pair in close proximity.¹³⁶ In integrated catalysis, this approach may be adapted
374 to co-immobilize two incompatibly catalysts, such as a metal/enzyme system,^{139,140} to minimize transport
375 between catalyst sites, while preventing deleterious interactions between them.

376 Considering the breadth of methods for surface attachment, ranging from covalent bonding to a silica
377 surface or non-covalent interactions with modified surfaces,^{28-35,133-135,141-143} the following should be
378 considered when designing an anchored catalyst system. First, the application is important. Thermal
379 reactions require a support that is robust under the reaction conditions, whereas electrochemical
380 reactions require a conductive support and a linker that provides sufficient electronic coupling.
381 Photochemical reactions generally require a transparent support, and often materials with a high surface
382 area so that a sufficient amount of photocatalyst can absorb light. Second, the reaction mechanism is
383 relevant. If multiple catalysts are required, the anchoring group should be sufficiently long and flexible to
384 accommodate intermolecular interactions. If ligands dissociate, then the dissociating ligands should not
385 be chosen for the attachment group to avoid catalyst leaching. Third, the reaction solvent is also important.
386 Sequestration methods that rely on weak intermolecular forces, such as hydrophobic interactions, may
387 be appropriate for reactions in water but not reactions that require nonpolar solvents. Finally, in terms of

388 the synthetic strategy to be used, sometimes it is more effective to anchor an organic group with a key
389 functionality, and then use a different reaction to anchor the metal unit. For example, a silyl ether
390 containing an azide can be attached to a surface, and then an alkyne-containing metal complex can be
391 connected to the azide in a copper-catalyzed click reaction to form a robust linkage.³⁵

392

393 [H2] Biocatalysis

394 Biocatalysis has become a vital component in modern organic synthesis, spanning from academic research
395 to industrial chemical and pharmaceutical processes.¹⁴⁴ Natural enzymatic catalysis is remarkable in its
396 high activity and selectivity and mild working conditions. Although naturally evolved enzymes typically
397 have a limited substrate scope, their performance may be enhanced by artificial enzyme engineering or
398 integration with chemocatalysis for broader applications.¹⁴⁵ For instance, in dynamic kinetic resolution of
399 amines and alcohols, an enantioselective enzyme catalyst was coupled with a racemization catalyst to
400 maximize the reaction yield.¹⁰⁴ Furthermore, the spatial and temporal control methods developed for
401 synthetic catalysis could also be applied to biocatalysis, providing new strategies to manipulate enzymes.
402 For example, the integration of biocatalysis and photoredox catalysis has been developing rapidly in
403 recent decades enabling otherwise challenging chemical transformations.^{146,147} Spatial control approaches
404 such as immobilizing enzymes onto heterogeneous supports¹⁴⁸ and crosslinking enzymes to form
405 extended structures^{149,150} can simplify the workup process and facilitate enzyme recycling.

406 Biology has many exquisite examples of systems that can manage complex reaction networks and perform
407 efficient multistep reaction sequences.^{21,24-26,95,96,116,117,119,120,151,152} Compartmentalization is a key spatial
408 control feature that allows organelles to orchestrate how enzymes and substrates/intermediates interact,
409 while simultaneously blocking entry of unwanted species. Discussed previously, compartmentalization is
410 a major form of spatial control that biology also utilizes, wherein meticulously designed organelles localize
411 enzymes and key substrates in close proximity to allow efficient channeling of intermediates between
412 active sites, while simultaneously blocking entry of unwanted or exit of wanted intermediate species into
413 or out of the confinement.^{151,152}

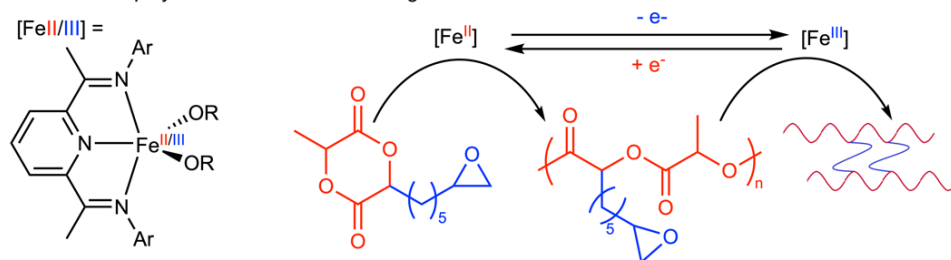
414 A representative example is the co-encapsulation of glucose oxidase and horse radish peroxidase within
415 macromolecular scaffolds such as MOFs or polymersomes.^{26,153} The cascade sequence between the two
416 enzymes that consumes glucose shows drastically improved yields when the enzymes are confined versus
417 the freely diffusing analogues. This method has been applied to many multi-enzyme systems,
418 demonstrating that it is a robust strategy for creating complex yet efficient catalytic processes. Temporal
419 control methods are also commonly used in biocatalysis, such as applying actuators or substrate gates to
420 direct when each step of multienzymatic processes occurs.^{154,155} The combination of enzymes with
421 synthetic catalysts offers the best of both worlds, providing new opportunities to streamline chemical
422 synthesis.¹⁵⁶

423

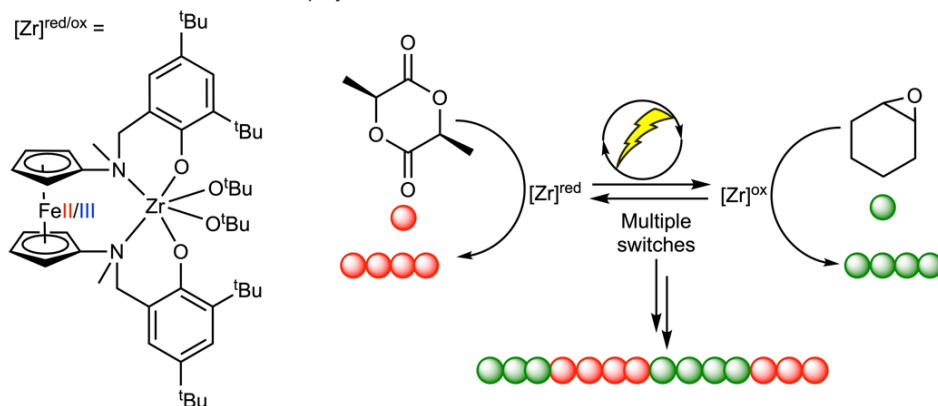
424

a Switchable catalysis in polymer microstructure control

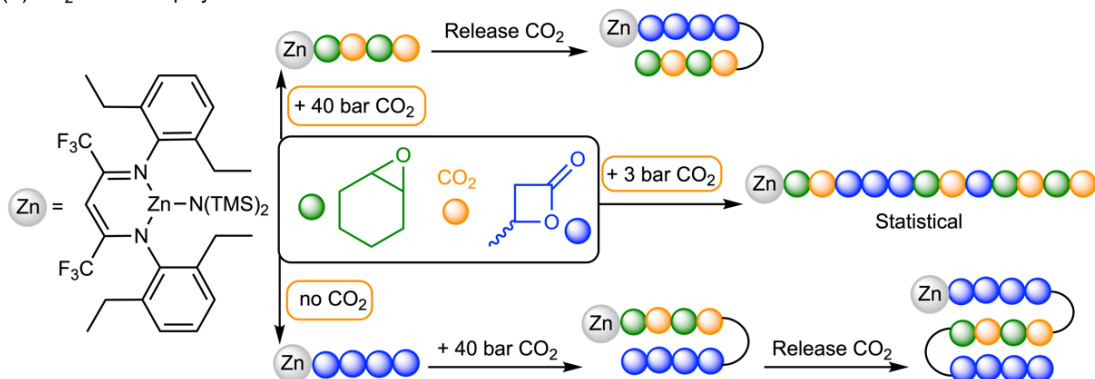
(i) Redox switchable polymerization and crosslinking



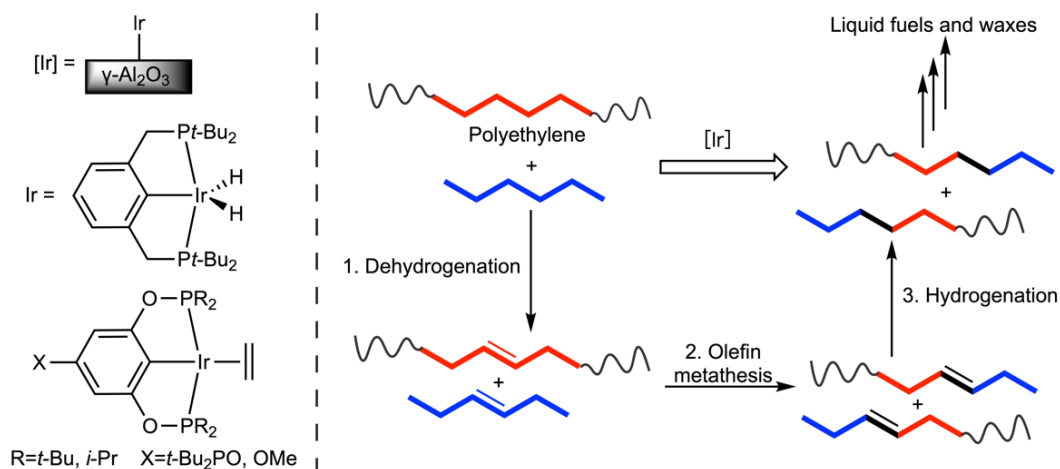
(ii) Electrochemical redox switchable polymerization



(iii) CO₂ controlled polymerization



b Polyethylene degradation by supported Ir catalyst



426 **Fig. 4 | Temporal and spatial control in integrating different catalytic cycles.** a| Harnessing activity of different
427 catalytic states to control the polymer sequence and microstructure. (i) Redox-switchable catalysis toward the
428 synthesis of a biodegradable crosslinked polymer network. (ii) Electrochemically controlled redox-switchable
429 polymerization to synthesize a tetrablock copolymer. b| Polyethylene degradation via tandem (de)hydrogenation
430 using γ -Al₂O₃ supported iridium complexes and alkane metathesis using Re₂O₇/Al₂O₃. The dehydrogenation/
431 hydrogenation process was catalyzed by the iridium compound while the olefin metathesis step was catalyzed by
432 Re₂O₇/Al₂O₃.

433

434 [H2] Addressing catalytic compatibility

435 Spatial and temporal control approaches provide the means for coupling multiple catalytic cycles in a
436 single reaction vessel. Spatiotemporal control may be utilized to couple different catalytic cycles by either
437 exploiting the switchable catalysis of a single precatalyst or by reconciling incompatibility among multiple
438 catalytic systems to generate products that would otherwise be difficult to synthesize. In this regard,
439 polymerization reactions are the best examples to showcase how complex products can be generated
440 from simple building blocks.

441 [H3] Cross-linking

442 Cross-linked polymer networks are valuable materials due to their high toughness and enhance thermal
443 properties.^{157,158} These materials are often synthesized using two-part resins or through the application of
444 heat or light as a trigger for cross-linking. Each of these methods have different limitations such as the
445 temperature required for heating and limited substrate penetration, respectively. The orthogonal activity
446 of redox-switchable catalysis can be applied in the realm of polymer crosslinking to address some of these
447 limitations (FIG. 4ai).¹⁵⁹ For example, when a bifunctional monomer that contained a cyclic diester and a
448 pendant epoxide was polymerized upon exposure to an iron(II) complex, an epoxide-functionalized
449 polyester was formed. By adding an external oxidizing agent, Fe(II) is oxidized to Fe(III), triggering the ring-
450 opening polymerization of the epoxide moiety, thereby forming a crosslinked polymer network.
451 Compared to linear poly(lactic acid), the cross-linked polymers show remarkably different thermal and
452 physical properties. Moreover, the crosslinking method that capitalizes on the switching capability of the
453 iron complex is beneficial because it does not require two-part resins, polymer creep is not an issue, and
454 there are no limitations with respect to the thickness of substrates.

455 [H3] Switchable polymerization

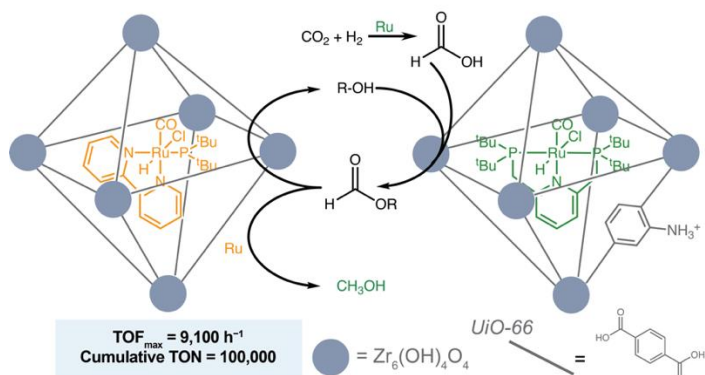
456 Other sophisticated macromolecules can be synthesized by taking advantage of switchable
457 polymerization reactions, such as block copolymers. Block copolymers demonstrate very useful properties
458 by melding the properties of two different polymer classes. However, some block copolymers cannot be
459 synthesized through sequential addition of monomers because the mechanisms for their polymerization
460 may be very different. Consequently, these block copolymers are usually synthesized through sequential
461 polymerization reactions that sometimes involve tedious and imperfect post-polymerization chain-end
462 modifications to accommodate subsequent reactions. When encountering this scenario, switchable
463 polymerization reactions are a good option to allow for the synthesis of block copolymers from pools of

464 monomers in a single reaction vessel. Electrochemistry has advanced redox-switchable catalysis by
465 obviating the need for chemical oxidants and reductants, thus bypassing the incompatibility issue
466 between substrates and redox reagents when the reaction is conducted in one pot. As such,
467 electrochemically controlled redox-switchable catalysis have been employed to synthesize block
468 copolymers in one pot.^{58,59} For example, a ferrocene-containing zirconium compound is active in its
469 reduced state for lactide polymerization, but inactive for epoxide polymerization (FIG. 4a_{ii}). When
470 oxidized, the activity is reversed toward these two types of monomers. To achieve the synthesis of a
471 multiblock copolymer, a one-pot setup was used with lactide and cyclohexene oxide monomers present
472 at the beginning of the reaction to simplify the overall process, and electrochemistry was used to eliminate
473 the need to add reagents during copolymerization. Using this strategy, a tetrablock copolymer was
474 synthesized through sequential application of oxidative and reductive potentials. In addition to simplifying
475 polymer purification, the electrochemical setup precludes possible side reactions, such as epoxide
476 polymerization initiated by oxidants.

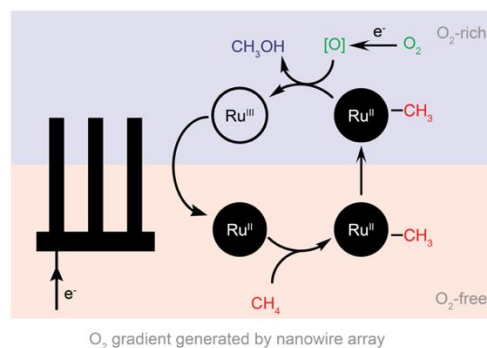
477 [H3] Solid supports

478 Spatially localizing a catalyst on the surface of a silica support is another important method that can be
479 used to address compatibility issues. Although the general perception is that immobilizing the catalyst
480 onto a surface reduces its activity due to hindered mass transport, the activity loss can be compensated
481 with appropriate system modifications and optimization. For example, when various γ -Al₂O₃ supported
482 iridium complexes (Ir@ γ -Al₂O₃) used for alkane dehydrogenation and alkene hydrogenation were
483 combined with a heterogeneous alkene metathesis catalyst (Re₂O₇/Al₂O₃), polyolefin degradation was
484 observed when the polymer was combined with a light alkane (FIG. 4b).¹⁶⁰ By carrying out the alkane
485 dehydrogenation in tandem with the olefin metathesis, alkanes are converted into substrates for alkene
486 metathesis, the products from which are substrates for hydrogenation, thereby resulting in new alkanes.
487 When the polymeric alkane polyethylene is combined with an excess of a light alkane, the result is smaller
488 alkanes. Importantly, the dual nature of the iridium complexes used for alkane dehydrogenation and
489 alkene hydrogenation enables the process, and requires that the supported iridium complex be used
490 concurrently with the heterogeneous metathesis catalyst. Moreover, separating the molecular iridium
491 complexes from the rhenium alkane metathesis catalyst circumvents any unwanted catalyst-catalyst
492 interactions, which plagued similar reactions involving entirely homogeneous catalysts.⁶ In addition, this
493 system proved effective even when commercial polyethylene products, such as plastic bottles and food
494 packaging were employed. This approach has also been employed in alkane upgrading by both homo- and
495 heterogeneous Ir species,¹⁶¹ the olefin degradation exemplified discussed shows spatial control of multiple
496 catalysts.

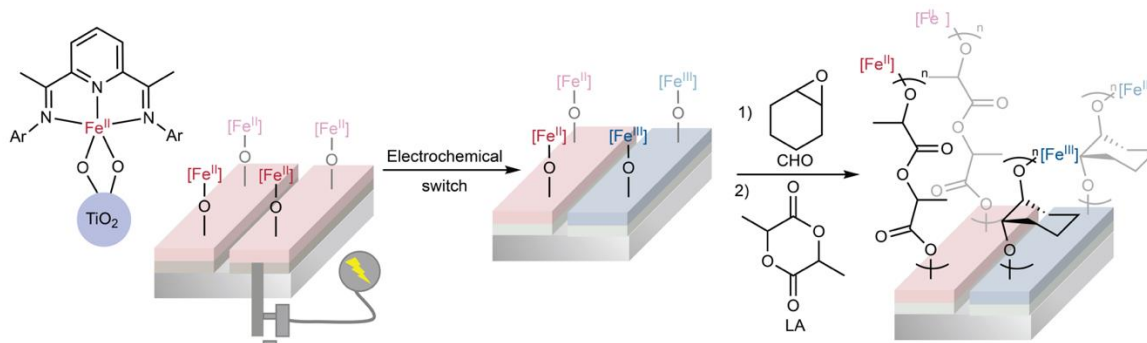
a Host-guest system for hydrogenation of CO₂ to CH₃OH



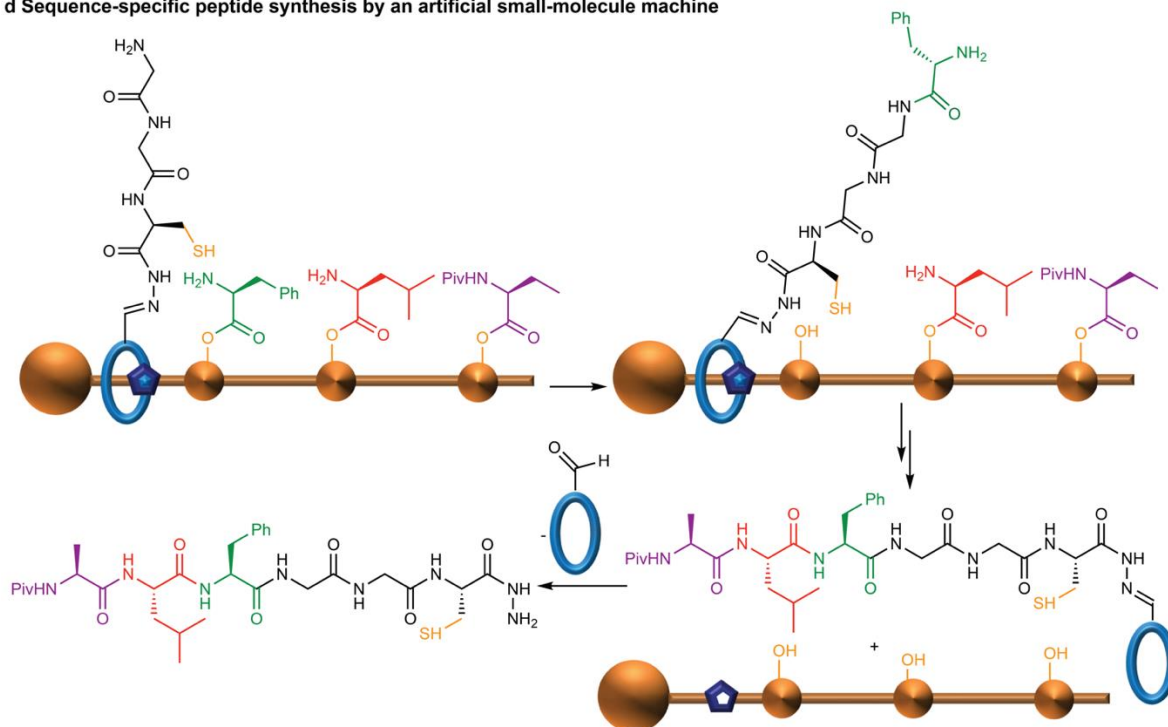
b Catalytic cycle of incompatible steps by an [O₂] gradient



c Patterning of surfaces using electrochemically switchable polymerization



d Sequence-specific peptide synthesis by an artificial small-molecule machine



497

498 **Fig. 5] Applications of integrated catalysis.** a) Metal-organic framework (MOF) host-guest system for tandem CO₂
 499 hydrogenation to CH₃OH via two separate ruthenium species encapsulated in a MOF (note: only one octahedral cage
 500 of the MOFs is shown for simplicity). b) O₂ mediated CH₄ oxidation to CH₃OH via an air sensitive Rh(II) intermediate

501 enabled in air by an electrochemically generated O₂ gradient. c| Integration of electrochemically catalyzed CO₂
502 reduction to CO and organometallic catalyzed ethylene/CO copolymerization for polyketone synthesis. d|
503 Electrochemical control of a redox-switchable iron compound supported on a TiO₂ surface with two electronically
504 isolated sections leading to different polymerization reactions. e| Sequence specific peptide synthesis by localizing
505 the amino acid building blocks on a rotaxane.

506

507 [H1] Results

508 For temporal control, prior to reporting any catalytic results, it is essential to characterize the activity of
509 the molecular catalyst in different states. NMR spectroscopy is the most commonly employed method for
510 diamagnetic compounds, while other approaches like UV-vis spectroscopy can be used for paramagnetic
511 compounds. When reporting the activity and selectivity of a catalyst in different states, vitality is
512 important to rule out the possible interference coming from the external stimulus. Thus, control
513 experiments should always be performed and reported. Furthermore, the addition and presence of a
514 substrate in the reaction medium, i.e., from an incomplete reaction, may alter the nature of the
515 catalytically active species and change its activity toward another substrate. Therefore, future research
516 would benefit substantially from detailed experiment procedures, e.g., the concentrations and order of
517 addition, when reactivity results are reported.

518 To confirm spatial control, one may employ a suite of characterization methods for heterogeneous
519 systems. For example, in immobilizing a catalyst onto a surface, solid state NMR spectroscopy can help
520 confirm and also determine the nature of a bound species.¹⁶² Other methods such as FTIR spectroscopy
521 can confirm the presence of key functional groups on the surface, while inductively coupled plasma -
522 optical emission spectrometry (ICP-OES) can assess catalyst loading on the solid support.³³

523 When combining two or more spatially controlled catalytic systems, mass transport between catalysts
524 may understandably cloud reporting of reaction rates. In order to assess the extent to which mass
525 transport alters observed reaction rates, the Φ criterion proves useful.^{163,164} Developed in the middle to
526 late 1900s, the Φ criterion can provide a qualitative assessment of mass transport. Derived from the
527 reaction rate, concentration, diffusion coefficient of the species to be transported, and diffusion path
528 length, if $\Phi < 1$, then one may ignore diffusional effects on reported reaction rates and kinetics. However,
529 if $\Phi > 1$, one cannot ignore the effect of mass transport. In addition to providing insight into the interplay
530 of mass transport and kinetics in integrated catalysis, the Φ criterion can also provide a justification for
531 exploring ways to alleviate mass transport (vide infra).

532

533 [H1] Applications

534 Integrated spatiotemporally controlled catalysis, although rare, has been employed to construct
535 sophisticated systems and solve compatibility problems between multiple catalytic cycles. Such
536 applications include small molecule activation, polymerization, and surface patterning. Although the
537 development of integrated catalysis is still in its infancy, and some examples are not strictly, by definition,

538 an integrated system, they demonstrate the potential of integrated catalysis and how it can be exploited
539 in synthesizing products with high complexity.

540 [H2] Confinement

541 Integrated catalysis can address thermodynamic constraints in sequences of chemical reactions. For
542 example, the power of encapsulating transition metal catalysts in metal organic frameworks (MOFs) for
543 integrated catalysis was recently demonstrated for the efficient hydrogenation of CO₂ to methanol.^{19,165}
544 In this example (FIG. 5a), two different ruthenium complexes were encapsulated in UiO-66, enabling a
545 tandem catalytic reaction in three steps: the thermodynamically unfavorable hydrogenation of CO₂ to
546 formic acid catalyzed by a PNP ruthenium complex; the near thermoneutral conversion of formic acid to
547 formate ester catalyzed by the zirconium oxide nodes of UiO-66; the thermodynamically favored
548 hydrogenation of formate ester to methanol catalyzed by a PNN ruthenium complex. This catalyst system
549 overcomes the thermodynamic limitations associated with the hydrogenation of CO₂ to formic acid by
550 coupling it with the thermodynamically favored hydrogenation of formate esters. If the first step was
551 separated from the second two in a sequential process, no formic acid would be obtained. Importantly,
552 no methanol was observed unless at least one of the two ruthenium-based complexes was encapsulated
553 in UiO-66, and catalyst recyclability was only possible if both ruthenium complexes were encapsulated in
554 UiO-66. These observations highlight the benefits of catalyst compartmentalization to prevent undesired
555 catalyst-catalyst interactions.

556 [H2] Concentration gradients

557 Another form of spatial control that has been beneficial for integrated catalysis is the generation of local
558 concentration gradients, which can be conveniently achieved electrochemically. Depending on the
559 steepness of the gradient, areas rich or void of certain species may be loosely defined as compartments.
560 For example, a nanowire-array electrode can be employed to reconcile incompatibility between CH₄
561 activation by an O₂-sensitive rhodium(II) metalloradical with O₂-based oxidation for CH₃OH formation (FIG.
562 5b).^{20,166} A reducing potential applied to the nanowire array electrode generated an O₂ gradient along the
563 wire, and an anoxic, essentially O₂ free zone was established at the bottom of the wires. As a result, an
564 efficient catalytic cycle was established in which the air-sensitive Rh(II) activated CH₄ in the anoxic region,
565 whereas CH₃OH synthesis proceeded in the aerobic region with O₂ as the terminal oxidant. When a planar
566 electrode was used, such a result was unattainable, showing that the O₂ gradient of the nanowire array
567 was responsible for reconciling incompatibility. The effective detainment of the ephemeral Rh(II)
568 intermediate by the nanowire electrode for catalytic CH₄-to-CH₃OH conversion^{20,166} encourages further
569 exploration in utilizing microscopic concentration gradients in catalysis to reconcile incompatibility.

570 A similar strategy using the electrochemical method to control the concentration of small molecules can
571 also be applied in generating CO from CO₂ then utilizing the produced CO as a building block in subsequent
572 reactions. Considering that CO₂ is abundant and is one of the culprits of climate change, deriving reactive
573 building blocks from it and converting them into value-added products would be ideal and could benefit
574 substantially from integrated catalysis. For example, CO produced from CO₂ was utilized as the carbon
575 feedstock in reactions such as Fischer–Tropsch, hydroformylation, and carbonylation.¹⁶⁷ Furthermore, in

576 reactions like CO and ethylene copolymerization, the pressure of CO was fine-tuned electrochemically,
577 and the amount of CO incorporated was modulated in an integrated catalytic system to control the
578 structure of the resulting polyketone (FIG. 5c).¹⁶⁸

579 [H2] Solid-state polymerization

580 Integrated catalysis can generate highly complex products, such as a precisely controlled macromolecular
581 structure,^{58,59,169,170} but the spatiotemporal control that is inherent to integrated catalysis has also been
582 exploited to synthesize patterned polymer-functionalized surfaces (FIG. 5d).¹⁷¹ By immobilizing redox-
583 switchable bis(imino)pyridine iron polymerization catalyst to semiconducting TiO₂ nanoparticles, redox-
584 switchable polymerization reactions can be carried out in the solid state. Suspending the iron(II)-
585 functionalized TiO₂ nanoparticles on conducting fluorine-doped tin oxide surfaces led to electroactive
586 surfaces whose chemoselectivity for polymerization can be altered through the application of an electrical
587 current: surfaces with the catalyst in the iron(II) oxidation state react with lactide to form polyesters while
588 surfaces that have been exposed to oxidizing potentials result in oxidation of the catalyst to the iron(III)
589 oxidation state, which reacts with epoxides to form polyethers. By using fluorine-doped tin oxide
590 substrates that contain electrically isolated zones of the functionalized TiO₂ nanoparticles, patterned
591 surfaces containing polyesters and polyethers can be synthesized by applying oxidizing potentials to zones
592 where polyethers are desired.

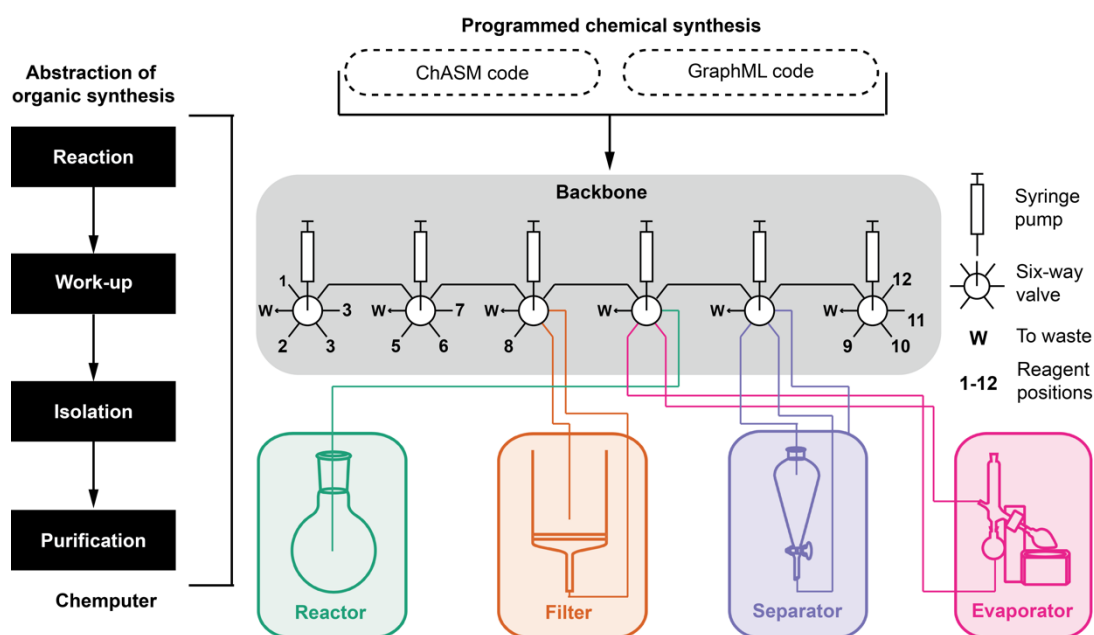
593 [H2] Molecular machines

594 Another example of synthesizing products of high complexity is the application of a molecular machine in
595 peptide synthesis. An artificial molecular machine was developed to mimic nature's ribosome and
596 synthesize oligopeptides with a predetermined sequence (FIG. 5e).¹⁷⁰ The system consists of a rotaxane,
597 an axle with protected amino acids immobilized to it, and a bulky end-stopper. The rotaxane has a
598 polypeptide arm that contains a cysteine moiety and a terminal glycyglycine amine group. The
599 oligopeptide synthesis is accomplished by a series of O-S and S-N acyl transfers as the rotaxane moves
600 along the axle. Though the system is only capable of incorporating up to 4 amino acids and is not catalytic,
601 it still represents a valuable proof of concept that demonstrates how artificial synthesis can mimic nature.
602 Furthermore, it illuminates an encouraging direction that, beyond stoichiometric templating, an
603 integrated system, showing spatial and temporal control, may be able to deliver the synthesis of highly
604 complex products.

605 [H2] Automation

606 Finally, the benefits of integrated catalysis are amenable to future automation strategies, such as the
607 Chemputer. Like in biocatalysis, where high-throughput screening can help identify the best protein from
608 the vast genome database among numerous candidates and myriad mutations, integrated catalysis could
609 also benefit from a highly automated synthesis-characterization-analysis system when devising a complex
610 system involving multiple catalytic cycles to optimize the working conditions, e.g., solvent, temperature,
611 concentrations, and cocatalyst. Other than the well-established peptide and nucleotide syntheses,
612 laboratory-scale synthesis of complicated products is still mainly performed manually. The Chemputer
613 demonstrates an efficient automation of multistep synthesis and purification processes (FIG. 6).¹⁷² By

614 using programming, various synthetic procedures can be abstracted from written protocols, translated
615 into machine language and implemented on synthetic modules to prepare pharmaceutical compounds.
616 The Chemputer may be as or more efficient than a traditional iterative lab approach, without any human
617 intervention. Furthermore, the Chemputer was specifically designed to be amenable to variations in the
618 sequence of steps performed, to allow adaptation to a wide array of chemical processes. In addition, such
619 a synthetic platform allows for the standardization of chemical synthesis, minimizing irreproducibility
620 caused by the synthetic nuances that are often omitted or assumed already known by the reader.^{172,173}



621
622 Fig. 6 | Organic synthesis in a robotic system enabled by the application of a chemical programming language to an
623 automated synthetic set up.

624 625 [H1] Reproducibility and data deposition

626 [H2] Reproducibility

627 The degradation of catalysts during a reaction is one of the main problems in catalysis. Degradation has
628 an even more profound impact on switchable catalysis, as the switching process introduces additional
629 possible degradation pathways. Therefore, a judicious choice of the most compatible external stimulus
630 may be the key to successful switchable catalysis. In addition, for catalysts confined onto surfaces, mass
631 transfer may slow down the overall reaction rate and is influenced by the distance and diffusivity between
632 the two catalysts. While this property can be exploited for integrated catalysis (for example, capitalizing
633 on local concentration gradients), if the physical location or diffusivity of the catalysts is not well controlled
634 (stirring, solvent, temperature), irreproducible results can be problematic.

635 In addition to the chemical and engineering complications that exist with integrated catalysis, there also
636 is an analytical challenge to address when catalysts are spatially confined. For homogeneous catalytic
637 systems, the characterization methods are diverse and often diagnostic, such as NMR spectroscopy and

638 X-ray crystallography. However, when the catalyst is compartmentalized or immobilized on a solid surface,
639 the system becomes complex, and characterization needs to involve relatively complicated techniques.
640 Some spectroscopic methods such as X-ray photoelectron spectroscopy, inductively coupled plasma mass
641 spectrometry (ICP-MS), and ICP-OES can be used to obtain elemental information either for the surface
642 or the bulk powder. Infrared, Raman, absorption, and solid state NMR spectroscopy can facilitate
643 understanding the nature of the active species. However, additional characterization methods are
644 necessary for a detailed and precise chemical structure of the catalytic system that would ensure
645 reproducibility. Especially in an integrated system, using operando techniques to understand the
646 mechanism of the reaction and the interactions between catalyst-catalyst, catalyst-substrate, and
647 substrate-substrate under working conditions will be extremely beneficial.^{174,175}

648 **[H2] Database**

649 The field would benefit from a database of coupled tandem to use as a reference when constructing
650 complicated integrated catalytic systems. When possible, the catalytic reactions involved, the
651 spatiotemporal control methods and reaction conditions employed, and how the activity and selectivity
652 of the overall reaction compared to the isolated stepwise reactions should be deposited. A database of
653 the resulting products would also be informative. In the case of polymerization reactions, for example,
654 many copolymers are synthesized using tandem polymerization reactions, and while there are databases
655 listing the structures and properties of polymers, such as [PolyInfo](#), [Polymer Property Predictor and
656 Database](#), and [CAMPUS](#), these databases are far from comprehensive in summarizing the structures and
657 corresponding properties of the various copolymers produced and reported. If this information could be
658 benchmarked and centralized, it could provide guidance for future polymer design and retrosynthesis.

659 **[H1] Limitations and optimizations**

660 A major limitation of the current state of iterative chemical synthesis is inefficiencies related to time and
661 material involved in workup steps, which may also lead to decreased yields.¹⁷⁶ An integrated catalytic
662 approach can alleviate this drawback, as well as pave the way to obtaining complex products from simple
663 feedstocks. As a field that continues to evolve, integrated catalysis still faces many challenges. First is the
664 issue of compatibility. Compatibility considerations in integrated systems is multifaceted and includes the
665 compatibility between catalysts, reagents, solvents and reaction conditions. When different reaction
666 cycles are carried out in one pot, the catalysts may undergo deactivation or decomposition caused by the
667 substrates or cocatalysts of another reaction. In principle, switchable catalysis circumvents the problem
668 by generating different catalytic species at different times, while spatial control can be used to separate
669 different precatalysts. Furthermore, when different reactions require different conditions, such as
670 temperature and pressure, reconciling such disparity is pivotal. Again, spatial control becomes important
671 by separating such reactions in different microenvironments (such as compartmentalization,
672 immobilization, or electrochemically generated concentration gradients).

673 Limitations and potential drawbacks may be related to the temporal control of a catalyst. For example,
674 the mode of temporal control (photochemical, electrochemical, or chemical) may not be compatible with
675 other reagents in the reaction medium. An applied potential or light source that switches a catalyst

676 between active states may have undesired consequences on other species in solution. One method to
677 circumvent this incompatibility would be to spatially separate the species of interest. For example, if a
678 catalyst is to be switched electrochemically, immobilizing it onto the electrode surface may help prevent
679 some unwanted redox reactions with other species. However, if the other species are free to diffuse, they
680 may still be decomposed by an applied potential. Further, compartmentalization of the incompatible
681 species could also help. Thus, great care must be taken to ensure other species in an integrated system
682 are compatible with the means of temporal control.

683 With respect to spatially localizing a catalyst, mass transport can become important. The heterogenization
684 of a previously homogeneous catalyst introduces transport from the bulk solution to the catalyst site as a
685 fundamental step for catalysis to proceed. Should this step prove limiting, it may be counterproductive to
686 spatially control a catalyst. Instead of relying solely on diffusion, the introduction of fluid transport may
687 help overcome mass transport limitations.¹⁷⁷⁻¹⁸¹ Further, conducting a reaction in flow provides numerous
688 additional parameters, such as flow rate and residence time, providing more opportunities for
689 optimization compared to a batch process. Mass transport limitations may also be exploited to avoid
690 unwanted background reactions. This would greatly depend on the pervasiveness of such mass transport
691 limitations, as well as the competition between diffusive and kinetic phenomena.¹⁶⁴

692 When employing spatiotemporal control to build an integrated catalytic system, one must take into
693 account some key considerations. The compatibility and practicality of all components of an integrated
694 system should be considered. First, all possible combinations of controls should be tested to assess
695 compatibility between catalysts, catalysts and reactants, and reactants. Simple outputs such as percent
696 conversion can be used to assess the effect of one reagent on another with respect to maintaining or
697 diminishing activity. In addition, assuming the separate catalyst systems have different optimal conditions
698 (such as temperature, solvent, pressure) compatible middle ground conditions must be determined. In
699 the event there is an incompatibility between some reagents in the two systems, spatial and/or temporal
700 control may be implemented to circumvent the mutual deactivation.

701 For spatial control, a key consideration is whether the catalyst/reagents need to be separated or can
702 feasibly be immobilized onto a surface or confined within an easily accessible compartment. For temporal
703 control, when incorporating switchable catalysis to either achieve on/off control or to open more avenues
704 for different reactions, electronic effect of a redox catalyst, the ring opening/closing of a photochromic
705 moiety, or the metal cation coordination onto a pendant ligand can be used, depending on the reaction
706 conditions. For example, if the reagents/substrates/products in the system are colored, then it might be
707 easier to add a redox-switchable or metal cation coordinating moiety to the ligand framework to realize
708 a switch in catalytic activity rather than employing light as the external stimulus. On the other hand, if
709 switchable catalysis requires intercepting short-lived reactive intermediates, then light may be the most
710 appropriate external stimulus to target. The next thing to consider is whether the exogenous trigger
711 interferes with the catalytic transformation itself. If the system is non-colored and remote control is
712 preferred, then a photoswitch or an electrochemical switch are the most viable options as neither
713 technique requires adding reagents to the reaction. Finally, practicality is as equal if not the most
714 important consideration. The most intricate spatial and temporal methods may be developed and applied

715 to address any conceivable compatibility issues. However, the time and effort spent should not be greater
716 than that of the combined systems treated independently. Thus, researchers must critically evaluate and
717 determine what compatibility issues need to be addressed before considering what spatial and/or
718 temporal methods to use and whether an integrated approach is superior to an approach involving
719 sequential catalytic reactions.

720 **[H1] Outlook**

721 In integrated catalysis, different reactions are coupled in a single vessel to generate products with high
722 complexity from a mixture of abundant starting materials. Inspired by macromolecule synthesis in living
723 cells, artificial catalysis for the synthesis of polymers with a well-defined sequence and microstructure has
724 been achieved in one pot with the proper utilization of integrated spatial and temporal control. Biological
725 macromolecules, such as proteins and DNA, encode information in their sequences and structures.
726 Likewise, the sequence and structure of synthetic macromolecules dictate their properties. We envisage
727 that integrated catalysis can become the machinery for synthesizing novel molecules and materials with
728 distinct properties. In addition to macromolecules, integrated catalysis can also be an effective tool for
729 multistep syntheses, and asymmetric syntheses of organic small molecules, such as pharmaceuticals.

730 Careful design of catalyst combinations in tandem catalytic cycles may enable reactions to proceed under
731 mild conditions and improve the selectivity and yield of the overall process. More importantly, integrated
732 catalysis can capture unstable, transient, and hazardous intermediates,¹⁸²⁻¹⁸⁴ and subsequently convert
733 them into stable and valuable products, thus expanding synthetic capabilities. For example, by coupling
734 an exothermic and endothermic reaction, thermodynamic leveraging in tandem reactions can drive the
735 formation of otherwise unviable products.^{19,165,185,186} Furthermore, breaking down a thermodynamically
736 favorable but high activation energy reaction into a series of steps that can be optimized individually, can
737 lower the overall energy barrier and allow the reaction to proceed through milder conditions.

738 To achieve precisely controlled and widely applicable integrated catalytic systems, it is imperative to
739 enrich and update the toolbox available by adding emerging methods for spatial and temporal control. As
740 a complement to artificial catalysis, biocatalysis is also indispensable, and often provides exquisite
741 selectivity. Thus, the construction of hybrid catalyst systems that involve biocatalysis and artificial spatial-
742 temporally controlled catalysis is an exciting new direction for integrated catalysis.¹⁴⁵ Finally, when
743 implementing integrated catalysis, engineering aspects such as reactor design are also crucial to ensure
744 that the anticipated results can be achieved.

745 Another way to facilitate the design of integrated catalytic systems is to use simulations and predictions
746 that evaluate structure-activity-selectivity relationships to identify the best catalyst in a timely manner.
747 Recent advances in quantum mechanical and finite element simulations now make possible an holistic
748 analysis of the entire integrated system that takes into account all contributing factors.¹⁸⁷ In this regard,
749 screening of catalysts for isolated reactions should be coupled with first-principles calculations and data
750 science to optimize the integrated system. Computer-assisted calculations can also be used in conjunction
751 with high-throughput automation¹⁸⁸ to further expedite screening and streamline the synthetic routes to
752 achieve high efficiency, low waste, and low cost.

753 **Glossary**

754 **Cascade / Domino process:** A transformation that installs two or more bonds under identical conditions
755 and with the same mechanism.

756
757 **Chemoswitchable catalysis:** A reaction in which the selectivity of a catalyst can be reversibly altered by
758 a chemical trigger.

759
760 **Compartmentalization:** Spatial localization of one or multiple species within a well-defined
761 encapsulation or confinement, where entry and exit within the compartment is dependent on the
762 chemical makeup of both the compartment and diffusing species.

763
764 **Orthogonal reactivity:** Reactivity of a multistate catalyst toward different substrates: catalyst is active in
765 one state for one type of reaction and inactive for another, and shows the opposite trend in the other
766 state.

767
768 **Redox-switchable catalysis:** The reactivity or selectivity of a catalyst that can be reversibly altered by
769 changing its oxidation state.

770
771 **Ring opening polymerization:** A chain growth polymerization reaction in which the polymer chain
772 propagation is achieved by the reactive terminus attacking and ring opening a cyclic monomer to
773 elongate the polymer chain and generate a new active terminus.

774
775 **Surface immobilization:** Spatial localization of a typically homogeneous species onto a heterogeneous
776 support.

777
778 **Tandem process:** Coupled catalytic processes in which substrates are converted sequentially by two or
779 more mechanistically distinct reactions.

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1298 **Competing interests**

1299 The authors declare no competing interests.

1300 **Related links**

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