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**STRUCTURAL ENGINEERING AND  
STRUCTURAL MECHANICS**

**DOT/DETECT  
FINITE ELEMENT ANALYSIS  
OF NONLINEAR  
HEAT TRANSFER PROBLEMS**

by  
**RONALD M. POLIVKA  
AND  
EDWARD L. WILSON**

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FINITE ELEMENT ANALYSIS OF  
NONLINEAR HEAT TRANSFER PROBLEMS

by

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June, 1976

Structural Engineering and Structural Mechanics  
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## 1. INTRODUCTION

The finite element method has gained widespread use for the stress analysis of complex structural systems. In previous applications of the method, the complete thermal stress analysis of most structures involved two separate phases. First, the heat transfer problem alone is solved based on certain idealizations, and then the resulting temperature distribution is used in connection with certain structural idealizations to determine the thermal stresses within a structure. Because different idealizations are used for both the heat conduction and thermal stress analyses, a separate computer input must be prepared for each phase. It is desirable, therefore, to develop compatible heat transfer and stress analysis programs in order to minimize the preparation of data required for the thermal stress problem.

In the past decade, several approximate solution techniques for heat conduction problems have been developed based on the finite element method. The method was first applied by Zienkiewicz and Cheung [1] and Wilson [2] for the solution of steady state conduction problems and extended by Wilson and Nickell [3] to include linear transient problems. In Ref. [3], the method was developed in detail for two dimensional planar bodies idealized by a system of triangular finite elements.

It is widely known that the thermal conductivity and specific heat capacity of many materials can vary with temperature. Few attempts have been made, however, to assess the importance of this temperature-dependence because it leads to considerable nonlinearities in the governing equations for heat flow equilibrium.

This dissertation is concerned with the development of procedures for the solution of nonlinear transient heat conduction problems by the finite element method. Although the method has been developed for two-dimensional structures, it can be readily extended to the heat conduction analysis of three dimensional systems. A variable 4- to 8-node isoparametric element is used in the analysis. This was done to provide compatibility with some of the more recently developed stress analysis programs.

The finite element method is completely general with respect to geometry, material properties and boundary conditions. Complex bodies composed of several different anisotropic materials can be easily represented. Temperature or heat flux boundary conditions may be specified at any point within the finite element system. Additionally, the finite element approach generates a heat flow equilibrium equation for the system which contains a symmetric positive-definite matrix. This matrix is banded, and the equilibrium equations can therefore be solved with a minimum of computer storage and time.

The following sections contain the theoretical basis for the solution of nonlinear transient heat conduction problems. Based on this theory, two finite element analysis programs have been developed. The program DOT ("Determination Of Temperatures") is a general purpose heat transfer analysis program for both linear and nonlinear conduction problems, and the program DETECT ("Determination of Temperatures in Construction") is a linear heat transfer program for the analysis of structures constructed incrementally. A description of the required input data for these programs is given in Appendices A and B, respectively, along with the Fortran listings.

## 2. HEAT TRANSFER ANALYSIS

### 2.1 EQUATIONS FOR EQUILIBRIUM

For the purpose of illustration, the heat transfer equations will be presented for a two-dimensional problem. The analysis can, however, easily be extended to three dimensions. The nonlinear two-dimensional equation for transient heat conduction in an anisotropic and inhomogeneous material is given by:

$$\rho c \frac{\partial T}{\partial t} = \frac{\partial}{\partial x} \left( k_x \frac{\partial T}{\partial x} \right) + \frac{\partial}{\partial y} \left( k_y \frac{\partial T}{\partial y} \right) + Q \quad (2.1)$$

where

$T$  = unknown temperature

$Q$  = heat generation rate

$\left. \begin{matrix} k_x \\ k_y \end{matrix} \right\} =$  anisotropic conductivity coefficients  
(temperature and space dependent)

$\rho$  = mass density (space dependent)

$c$  = specific heat capacity (temperature and space dependent)

$x, y$  = rectangular cartesian coordinates

$t$  = time

If the thermal conductivity is constant and the material is isotropic, then  $k_x = k_y = k$  and Eq. (2.1) reduces to the more familiar form:

$$\nabla^2 T + \frac{Q}{k} = \frac{1}{\alpha} \frac{\partial T}{\partial t} \quad (2.2)$$

where the thermal diffusivity  $\alpha = k/\rho c$  and  $\nabla$  is the gradient operator.

In order to determine a unique solution to Eq. (2.1), proper initial and boundary conditions must be specified which are compatible with the physical conditions of the particular problem.

## 2.2 INITIAL CONDITION

The initial condition must be defined by prescribing the temperature distribution throughout the body at time zero as a known function of  $x$  and  $y$ :

$$T(x,y,0) = f(x,y) \quad @ \quad t = 0 \quad (2.3)$$

## 2.3 BOUNDARY CONDITIONS

Boundary conditions may be defined by specifying either the prescribed surface temperature or heat flow on the boundary of the body. In many problems, heat may also be transferred by convection or radiation across a boundary layer and these boundary conditions must also be specified.

### 2.3.1 Prescribed Surface Temperature

A surface temperature existing on a portion of the boundary of the body  $\Gamma_T$  must be specified as:

$$T(x,y,t) = T_1(x,y,t) \quad ; \quad x,y \text{ on } \Gamma_T \quad (2.4)$$

This is the easiest boundary condition to work with and the temperature may be either constant or a function of time.

### 2.3.2 Prescribed Heat Flow at the Surface

A prescribed heat flow boundary condition can be expressed as:

$$k \frac{\partial T}{\partial n}(x,y,t) = q_n(x,y,t) \quad ; \quad x,y \text{ on } \Gamma_q \quad (2.5)$$

where  $q_n$  is the specified amount of heat flow at point  $(x,y)$  on that portion  $\Gamma_q$  of the boundary of the body where the normal derivative of temperature is prescribed,  $n$  is the outward normal to this surface and  $k$  is the thermal conductivity.

### 2.3.3 Convection Boundary Condition

For the case of free convection, the rate of heat transfer across a boundary layer is given by:

$$k \frac{\partial T}{\partial n}(x,y,t) = h(T_e - T_s)^N ; \quad x,y \text{ on } \Gamma_h \quad (2.6)$$

where  $h$  is the surface heat transfer coefficient,  $T_e$  is the known temperature of the external environment,  $T_s$  is the surface temperature of the solid and  $\Gamma_h$  is that portion of the boundary surface undergoing convective heat transfer.

The convection boundary condition is linear and can be specified exactly if  $N = 1$  and  $h$  is not a function of temperature. If, in addition, there is a prescribed flux  $q_n(x,y,t)$  at the surface, Eq. (2.6) is replaced by:

$$k \frac{\partial T}{\partial n}(x,y,t) = q_n(x,y,t) + h(T_e - T_s) \quad (2.7)$$

### 2.3.4 Radiation Boundary Condition

Heat transfer by radiation between a boundary surface  $\Gamma_r$  and its surroundings can be expressed by:

$$q_r(x,y,t) = V\sigma \left[ \frac{1}{\frac{1}{\epsilon_r} + \frac{1}{\epsilon_s} - 1} \right] [\bar{T}_r^4 - \bar{T}_s^4] ; \quad x,y \text{ on } \Gamma_r \quad (2.8)$$

where  $V$  is the radiation view factor,  $\sigma$  the Stefan-Boltzmann constant,  $\epsilon_r$  is the emissivity of the external radiation source,  $\epsilon_s$  is the emissivity of the surface, and  $\bar{T}_r$  and  $\bar{T}_s$  are the absolute temperatures of the radiation source and the surface, respectively.

## 2.4 SOLUTION OF THE HEAT FLOW EQUILIBRIUM EQUATION

Three types of methods are available for solving the general heat transfer equation (Eq. (2.1)) for the temperature distribution within a body: exact methods, approximate analytical methods and approximate numerical methods.

### 2.4.1 Exact Solutions

The standard classical reference on heat transfer analysis is the book by Carslaw and Jaeger [ 4 ], in which a number of exact solutions are given for rectangular regions, infinite and semi-infinite solids bounded by two parallel planes, cylinders and spheres that are subjected to a variety of initial and boundary conditions. The methods used for these exact solutions range from simple techniques such as separation of variables to complex ones involving the use of Green's functions, Laplace transforms, integral transforms or Fourier transforms.

In almost all of the problems for which an exact solution is possible, the thermal properties  $k$ ,  $\rho$  and  $c$  are taken to be constants, independent of both temperature and position. If the thermal properties depend on temperature, the solution to Eq. (2.1) is much more complicated since the equation becomes nonlinear. In the majority of these cases, no exact solution exists, and the temperature field must be determined by numerical methods.

### 2.4.2 Analytical Solutions

This approximate method of solution requires that an initial temperature profile be assumed before the solution can be carried out. Two of the more commonly used techniques are the Laplace-variational method [ 5 ] and the integral method [ 6 ].

Analytical methods of solution are capable of solving a wider variety of heat conduction problems than can be solved by exact methods; e.g. a one dimensional problem with temperature-dependent thermal conductivity.

#### 2.4.3 Numerical Methods

The most commonly used numerical method for solving the heat equation (Eq. (2.1)) is the finite difference method [7]. In this implicit method, a truncated Taylor series expansion is used to approximate the derivatives in the governing differential equation and the space and time derivatives are then replaced by a finite difference representation. The resulting temperature distribution can then be obtained by solving a set of simultaneous algebraic equations at each level of time.

In recent years, the finite element method has gained widespread use in the stress analysis of complex structural problems. For the evaluation of thermal stresses, the finite element technique is desirable for solving the heat flow problem because the same model can be used for both the stress and heat transfer analyses, thus reducing the required amount of input data.

It is customarily assumed that the state of deformation in a body does not affect the temperature field. Therefore, a heat transfer analysis can be conducted initially using a finite element idealization and then a second pass can be made through the same program to determine the thermal stresses. If the initial heat transfer analysis had been performed using some other numerical technique, a special thermal analyzer would have been required to determine the temperature input compatible with the finite element stress program.

### 3. FINITE ELEMENT FORMULATION

In the finite element method of analysis, a solid continuum is idealized by an assemblage of discrete elements or subregions. These elements may be of variable size and shape, and are interconnected by a finite number of nodal points. The element boundaries are generally linear, although recent development of the 4- to 8-node isoparametric element has permitted the use of curved boundaries.

For the case of heat conduction, the temperature field within each element is approximated by a set of interpolation functions  $h_i$ , chosen in such a way so as to define the temperature uniquely within each finite element in terms of its nodal temperatures. The matrix equations for heat flow equilibrium can then be derived for the discrete number of nodal points within the finite element system.

The finite element method has several advantages over other solution procedures. The method is completely general with respect to geometry, material properties and arbitrary boundary conditions. Complex bodies of arbitrary shape composed of several different anisotropic materials can easily be represented. A mixture of temperature-dependent material properties and nonlinear boundary conditions can also be handled quite readily. The governing heat flow equilibrium equations for the response of the discrete system produce a symmetric, positive-definite matrix which may be placed in a band form. Efficient solution techniques can therefore be applied which require a minimum amount of computer time and storage.

Initially, the basic element types used to represent a two-dimensional body were triangular and rectangular elements containing straight-line boundaries. However, the recent development of the



variable 4- to 8-node isoparametric element has given the method much more flexibility [8]. This element is very useful for representing complex bodies with curved boundaries and it readily allows for varying the mesh size within a model.

A variable 4- to 8-node two-dimensional isoparametric element lying in the global X-Y plane is shown in Fig. 3.1(b). This element may be used to model either planar or axisymmetric solids. The planar element is assumed to have a unit thickness, whereas in the axisymmetric representation a unit radian segment ( $\theta = 1$ ) is considered, with the global Y-axis as the axis of revolution.

This curvilinear 4- to 8-node element can be obtained by means of an isoparametric mapping from a bi-unit square contained in a local r-s coordinate system. The local node numbering system for this bi-unit square, shown in Fig. 3.1(a), has nodes 1 through 4 located at the four corners and nodes 5 through 8 located at the mid-sides of the square.

Isoparametric mapping provides a one-to-one correspondence between the local (r,s) and global (x,y) coordinates. The coordinate transformation between the bi-unit square and the curvilinear element is given by:

$$x_m(r,s) = \sum_{i=1}^8 h_{im}(r,s) x_{im} \quad (3.1)$$

$$y_m(r,s) = \sum_{i=1}^8 h_{im}(r,s) y_{im} \quad (3.2)$$

where  $(x_{im}, y_{im})$  are the global coordinates of node i in element m and  $h_{im}$  is the interpolation function corresponding to node i of element m. The interpolation functions are defined as follows:

$$\begin{aligned}
h_1 &= \frac{1}{4} (1 + r)(1 + s) - \frac{1}{2} h_5 - \frac{1}{2} h_8 \\
h_2 &= \frac{1}{4} (1 - r)(1 + s) - \frac{1}{2} h_5 - \frac{1}{2} h_6 \\
h_3 &= \frac{1}{4} (1 - r)(1 - s) - \frac{1}{2} h_6 - \frac{1}{2} h_7 \\
h_4 &= \frac{1}{4} (1 + r)(1 - s) - \frac{1}{2} h_7 - \frac{1}{2} h_8 \\
h_5 &= \frac{1}{2} (1 - r^2)(1 + s) \\
h_6 &= \frac{1}{2} (1 - r)(1 - s^2) \\
h_7 &= \frac{1}{2} (1 - r^2)(1 - s) \\
h_8 &= \frac{1}{2} (1 + r)(1 - s^2)
\end{aligned} \tag{3.3}$$

where the local coordinates  $(r,s)$  vary on the interval  $(-1,1)$ .

If the curvilinear element has one or more straight sides, the midside node numbers 5, 6, 7 or 8 corresponding to the straight sides can be omitted by setting the corresponding interpolation functions equal to zero.

The same interpolation functions are used to approximate the temperature field within the element in terms of the temperatures at nodes 1 to 8:

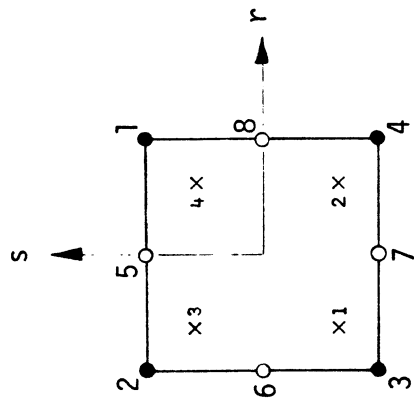
$$T_m(r,s,t) = \sum_{i=1}^8 h_{im}(r,s) T_{im}(t) \tag{3.4}$$

where  $T_{im}$  is the temperature of the  $i^{\text{th}}$  nodal point of element  $m$ .

Writing in matrix notation we have:

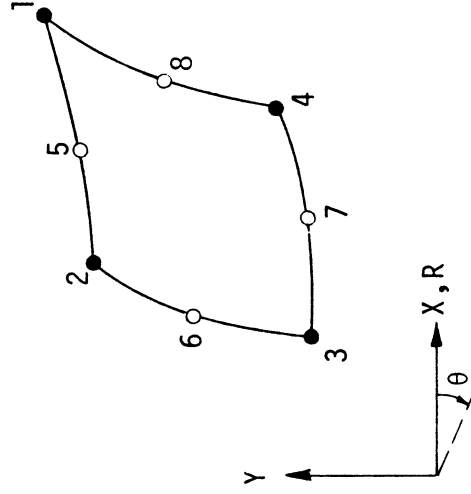
$$T_m(r,s,t) = \underset{1 \times 8}{\underline{b}_m(r,s)} \underset{8 \times 1}{\underline{T}_m(t)} \tag{3.5}$$

where  $\underline{b}_m(r,s)$  is the transformation matrix between the nodal point temperatures  $\underline{T}_m(t)$  and the temperature  $\underline{T}_m(r,s,t)$  at any point  $(r,s)$  within element  $m$ .



x Gauss Point Locations for 2x2 Integration Order

(a) Bi-unit Square in Local r-s System



(b) Curvilinear Two-Dimensional Element in Global X-Y System

FIG. 3.1 TWO-DIMENSIONAL MAPPING OF 4- TO 8-NODE ISOPARAMETRIC ELEMENT

In the evaluation of the element conductivity matrix  $\underline{K}_m$ , defined in the following section, it is required to know the transformation between the nodal temperatures and the global derivatives of the element temperature. This transformation is analogous to the strain-displacement transformation required in a stress analysis problem.

The transformation between the nodal temperatures and the local derivatives of the element temperature can be found by direct differentiation of Eq. (3.5):

$$\frac{\partial}{\partial r} T_m(r,s,t) = \sum_{i=1}^8 \frac{\partial}{\partial r} h_{im}(r,s) T_{im}(t) \quad (3.6)$$

$$\frac{\partial}{\partial s} T_m(r,s,t) = \sum_{i=1}^8 \frac{\partial}{\partial s} h_{im}(r,s) T_{im}(t) \quad (3.7)$$

Combining the above two equations and writing in matrix form we have:

$$\begin{bmatrix} \frac{\partial T}{\partial r} \\ \frac{\partial T}{\partial s} \end{bmatrix}_m = \underset{2 \times 8}{\underline{P}_m(r,s)} \underset{8 \times 1}{\underline{T}_m(t)} \quad (3.8)$$

where  $\underline{P}_m(r,s)$  contains the derivatives of the interpolation functions for element  $m$  with respect to the local  $(r,s)$  coordinates. The chain rule can now be applied to obtain these derivatives with respect to the global  $(x,y)$  coordinates. The chain rule may be written in matrix form as:

$$\begin{bmatrix} \frac{\partial T}{\partial r} \\ \frac{\partial T}{\partial s} \end{bmatrix}_m = \begin{bmatrix} \frac{\partial x}{\partial r} & \frac{\partial y}{\partial r} \\ \frac{\partial x}{\partial s} & \frac{\partial y}{\partial s} \end{bmatrix} \begin{bmatrix} \frac{\partial T}{\partial x} \\ \frac{\partial T}{\partial y} \end{bmatrix}_m \quad (3.9)$$

and inverted as

$$\begin{bmatrix} \frac{\partial T}{\partial x} \\ \frac{\partial T}{\partial y} \end{bmatrix}_m = \underline{J}_m^* \begin{bmatrix} \frac{\partial T}{\partial r} \\ \frac{\partial T}{\partial s} \end{bmatrix}_m \quad (3.10)$$

where

$$\underline{J}_m^* = \frac{1}{|\underline{J}|_m} \begin{bmatrix} \frac{\partial y}{\partial s} & -\frac{\partial y}{\partial r} \\ -\frac{\partial x}{\partial s} & \frac{\partial x}{\partial r} \end{bmatrix} \quad (3.11)$$

in which the determinant of the Jacobian transformation is

$$|\underline{J}|_m = \frac{\partial x}{\partial r} \frac{\partial y}{\partial s} - \frac{\partial y}{\partial r} \frac{\partial x}{\partial s} \quad (3.12)$$

The transformation between the nodal temperatures and the global derivatives of the element temperature can now be found by substituting Eq. (3.8) into the inverted chain rule Eq. (3.10):

$$\begin{bmatrix} \frac{\partial T}{\partial x} \\ \frac{\partial T}{\partial y} \end{bmatrix}_m = \underline{J}_m^* \underline{P}_m \underline{T}_m(t) \quad (3.13)$$

or

$$\underline{T}_{,i}(r,s,t) = \underset{2 \times 8}{\underline{a}_m}(r,s) \underset{8 \times 1}{\underline{T}_m}(t) \quad (3.14)$$

### 3.1 MATRIX EQUILIBRIUM EQUATIONS FOR TRANSIENT HEAT CONDUCTION

The governing equations for transient heat conduction in a solid idealized by a system of finite elements may be derived in a number of ways. In one approach, a functional is defined by some integral over the entire domain and its boundary, in which the unknown temperature field or its derivatives appear. The temperature field providing the correct solution to the problem is the one that causes the functional to be minimized. From this minimization of the functional results the governing partial differential equations.

This class of solution techniques, often referred to as variational methods [1,3], [9-19] is the most widely accepted technique for arriving at a finite element representation of the equilibrium equations.

A second approach requires prior knowledge of the differential equations governing the problem. The finite element approximation can then be directly derived mathematically from the differential equations by the method of weighted residuals [20,21]. Depending upon the choice of the weighting function, different techniques can be used such as the collocation method or the Galerkin method. The finite element derivation using the variational formulation is a special case of the method of weighted residuals using the Galerkin method for the weighting function.

A third method involves a purely physical interpretation of the equations for heat flow equilibrium [22-25]. This method has the advantage of providing insight to the solution of nonlinear analysis problems and is the one that will be used in this presentation.

### 3.1.1 Physical Statement of Heat Flow Equilibrium

The heat transfer equations for a solid idealized by a system of finite elements can be physically interpreted by a statement of the heat flow equilibrium at the nodes of the system at any time:

$$Q^s + Q^i = Q^e + Q^q \quad (3.15)$$

where

$Q^s$  = rate at which heat is stored within the elements adjacent to a node

$Q^i$  = rate of heat flow from the elements adjacent to a node by means of internal heat conduction

$Q^e$  = rate at which heat enters a node from an external source

$Q^q$  = rate at which heat is generated within the elements adjacent to a node

This heat balance equation is valid for all interior nodal points, but must be modified for nodes on the boundary surfaces in order to account for a variety of boundary conditions which will be described later.

Using the thermal properties of the finite elements, the heat transfer rates in Eq. (3.15) can be expressed in terms of the temperatures at the element nodes.

The instantaneous rate at which heat is stored within the material at any time  $t$  is:

$$q^s = \rho c(T)V \frac{\partial T}{\partial t} = C(T) \frac{\partial T}{\partial t} \quad (3.16)$$

where the thermal heat capacity  $C$  of the material is a function of the density  $\rho$ , the volume  $V$  and the temperature-dependent specific heat capacity  $c$  of the material.

If the heat flow is defined as positive for a positive temperature gradient, the rate of heat conduction per unit area along direction  $j$  within the material can be expressed as:

$$q_j^i = \sum_n k_{jn}(T) \frac{\partial T}{\partial n} \quad (3.17)$$

where  $k_{jn}$  is a symmetric positive-definite thermal conductivity tensor for the material which may vary with temperature, and  $n$  indicates the direction of the temperature gradient.

For a two-dimensional problem with coordinates  $x$  and  $y$ , Eq. (3.17) can be expressed in matrix form as:

$$\begin{bmatrix} q_x^i \\ q_y^i \end{bmatrix} = \begin{bmatrix} k_{xx} & k_{xy} \\ k_{xy} & k_{yy} \end{bmatrix} \begin{bmatrix} \frac{\partial T}{\partial x} \\ \frac{\partial T}{\partial y} \end{bmatrix} \quad (3.18)$$

where the three constants  $k_{xx}$ ,  $k_{xy}$  and  $k_{yy}$  which characterize the tensor must satisfy the conditions:

$$\begin{aligned} (a) \quad & k_{xx}, k_{yy} > 0 \\ (b) \quad & k_{xx}k_{yy} - k_{xy}^2 > 0 \end{aligned} \quad (3.19)$$

For an isotropic material,  $k_{xx} = k_{yy} = k$  and  $k_{xy} = 0$ .

Using the thermal properties defined in Eqs. (3.16) and (3.17) along with the interpolation functions for the element temperature given in Eqs. (3.5) and (3.14), the method of virtual work can be applied in order to express the heat balance rates in Eq. (3.15) in terms of the nodal point temperatures [26].



The resulting matrix differential equation governing heat flow equilibrium in a finite element system containing  $n$  nodes is:

$$\underset{n \times n}{\underline{C}}(T) \underset{n \times 1}{\dot{\underline{I}}}(t) + \underset{n \times n}{\underline{K}}(T) \underset{n \times 1}{\underline{I}}(t) = \underset{n \times 1}{\underline{Q}}(t) \quad (3.20)$$

where

$\underline{C}(T)$  = system heat capacity matrix which is dependent on the density  $\rho$  and the temperature-dependent specific heat capacity  $c$  of the material

$\underline{K}(T)$  = system thermal conductivity matrix which is dependent on the temperature  $T$  of the body

$\underline{I}(t)$  = vector of nodal point temperatures at time  $t$

$\dot{\underline{I}}(t)$  = vector of the time rate-of-change of the nodal point temperatures at time  $t$

$\underline{Q}(t)$  = vector of the externally supplied nodal heat fluxes at time  $t$  (heat which is generated within the elements can be considered in this vector)

Equation (3.20) represents a set of nonlinear equations to be solved for the nodal point temperatures of the finite element representation as a function of time. The matrices  $\underline{C}$ ,  $\underline{K}$  and  $\underline{Q}$  are known at any instant in time and Eq. (3.20) can therefore be solved using numerical integration.

In the following sections, the matrices  $\underline{K}$ ,  $\underline{C}$  and  $\underline{Q}$  are formulated and the numerical integration algorithm used to solve Eq. (3.20) will be described in Section 5.

## 3.2 SYSTEM MATRICES

### 3.2.1 Conductivity Matrix

The complete conductivity matrix for the system is formed by direct summation of the element conductivity matrices for all of the element types. This assembly operation is analogous to the direct stiffness assembly procedure and is indicated symbolically by means of the following equation:

$$\underline{K} = \sum_{m=1}^M \underline{K}_m \quad (3.21)$$

where  $M$  is the total number of elements in the finite element model.

The matrix  $\underline{K}_m$  is the conductivity matrix of element  $m$  and is defined as:

$$\underline{K}_m = \int_{V_m} \underline{a}_m^T \underline{k}_m \underline{a}_m dV_m \quad (3.22)$$

where

$\underline{k}_m$  = thermal conductivity tensor for the material  
(from Eq. (3.18))

$\underline{a}_m$  = transformation between the nodal temperatures  
and the global derivatives of the element  
temperature given by Eq. (3.14)

$V_m$  = volume of element  $m$

Since the transformation matrix  $\underline{a}_m$  is expressed in terms of the natural coordinates  $r$  and  $s$ , it is necessary to carry out the above integration in natural coordinates.

(a) Planar Solid

For a planar solid of constant thickness  $t^*$ , Eq. (3.22) can be expressed as:

$$\underline{k}_m = t^* \int_{A_m} \underline{a}_m^T \underline{k}_m \underline{a}_m dA_m \quad (3.23)$$

In the natural coordinate system the differential area is:

$$dA_m = dx dy = |\underline{J}| ds dt \quad (3.24)$$

where  $|\underline{J}|$  is the determinant of the Jacobian matrix from Eq. (3.12).

Substituting Eq. (3.24) into (3.23) and assuming a unit thickness we have:

$$\underline{k}_m = \int_{-1}^1 \int_{-1}^1 \underline{a}_m^T \underline{k}_m \underline{a}_m |\underline{J}| dr ds \quad (3.25)$$

This is of the general form:

$$\underline{k}_m = \int_{-1}^1 \int_{-1}^1 f(r,s) dr ds \quad (3.26)$$

and the integral Eq. (3.25) can now be evaluated numerically using Gaussian quadrature:

$$\underline{k}_m = \sum_{j=1}^N \sum_{i=1}^N H_i H_j \underline{a}_m^T(r_i, s_j) \underline{k}_m \underline{a}_m(r_i, s_j) |\underline{J}(r_i, s_j)| \quad (3.27)$$

where

$H_i, H_j$  = weighting coefficients for Gaussian integration

$r_i, s_j$  = abscissae of the integration points

$N$  = integration order

The weight coefficients and abscissae for the Gaussian quadrature formula may be found in Ref. [26]. Integration point locations for an integration order of 2 are shown in Fig. 3.1(a). For the DOT and DETECT computer programs described in Appendices A and B, respectively, integration orders of either 2 or 3 may be used. It is recommended, however, to use a 2x2 quadrature integration scheme for most cases.

(b) Axisymmetric Solid

For an axisymmetric solid, the volume integral for the element conductivity can be converted to an area integral since  $dV = R d\theta dA$ , where the radius  $R$  and the angle  $\theta$  are defined in Fig. 3.1(b). For a one radian segment of the solid:

$$\underline{K}_m = \int_{A_m} R \underline{a}_m^T \underline{k}_m \underline{a}_m dA_m \quad (3.28)$$

In the natural coordinate system  $dA_m = |\underline{J}| ds dt$ , therefore:

$$\underline{K}_m = \int_{-1}^1 \int_{-1}^1 R \underline{a}_m^T \underline{k}_m \underline{a}_m |\underline{J}| ds dt \quad (3.29)$$

The integral Eq. (3.29) can now be evaluated numerically using Gaussian quadrature as:

$$\underline{K}_m = \sum_{j=1}^N \sum_{i=1}^N H_i H_j \underline{f}(r_i, s_j) \quad (3.30)$$

where

$$\underline{f}(r_i, s_j) = \underline{a}_m^T(r_i, s_j) \underline{k}_m \underline{a}_m(r_i, s_j) R(r_i, s_j) |\underline{J}(r_i, s_j)| \quad (3.31)$$

### 3.2.2 Heat Capacity Matrix

The complete heat capacity matrix for the system is also formed by direct summation of the individual element heat capacity matrices:

$$\underline{C} = \sum_{m=1}^M \underline{C}_m \quad (3.32)$$

where  $M$  is the total number of finite elements in the model.

The heat capacity matrix  $\underline{C}_m$  of element  $m$  is defined as:

$$\underline{C}_m = \int_{V_m} \rho_m c_m \underline{b}_m^T \underline{b}_m dV_m \quad (3.33)$$

where

$c_m$  = specific heat capacity

$\rho_m$  = mass density

$\underline{b}_m$  = temperature interpolation vector given by Eq. (3.5)

$V_m$  = volume of element  $m$

The computation of  $\underline{C}_m$  in Eq. (3.33) results in a fully populated matrix identical in form to the thermal conductivity matrix  $\underline{K}_m$ . The assembled heat capacity matrix  $\underline{C}$  is symmetric, positive-definite, and exhibits the same coupling as the system conductivity matrix  $\underline{K}$ . This coupled  $\underline{C}$  matrix increases significantly the computational effort required to solve the heat flow equilibrium equation (3.20). It has been shown, however, that the element heat capacity matrix  $\underline{C}_m$  can be approximated by a lumped diagonal matrix with only a small loss of accuracy [3,22]. This approximation reduces by almost 50% the computer storage and computational steps required in the solution of Eq. (3.20).

The concept of lumping the heat capacity of an element at the nodes used to describe the element is equivalent to the lumped mass idealization in dynamic analysis. This lumping eliminates any coupling between the time rate-of-change of temperature at adjacent nodes and results in a diagonal heat capacity matrix  $\underline{C}_m$ . The accuracy of the lumping technique used depends on the number of nodes used to describe the element and the element shape.

(a) 4-Node Elements

For a regular finite element grid comprised of either 3- or 4-node elements, the lumped heat capacity matrix can be formed as:

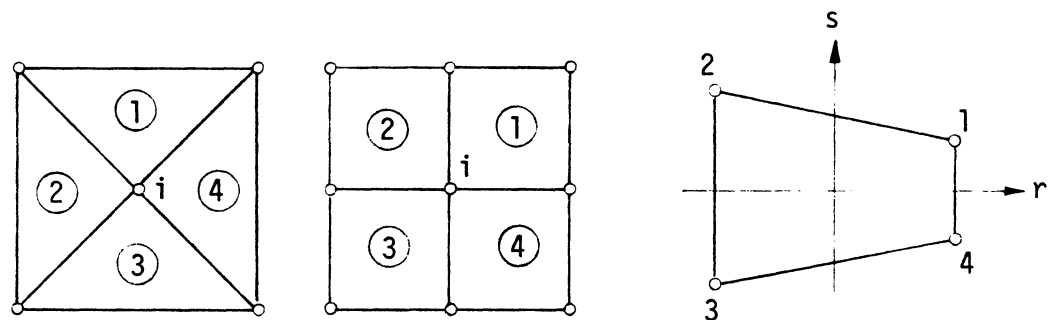
$$C_{ii} = \sum_m \frac{1}{M} \rho_m c_m V_m \quad (3.34)$$

where the summation is carried out over all  $m$  elements attached to nodal point  $i$ . The parameter  $M$  is the number of nodes describing each element, and the density  $\rho_m$ , specific heat  $c_m$  and volume  $V_m$  are those values associated with each element  $m$  (See Fig. 3.2(a)). This lumping procedure has been used in several earlier heat transfer programs [3,22] and stress analysis programs [27,28] involving 3- to 4-node elements. Inaccuracies can arise, however, if the grid has distorted elements. For the 4-node element shown in Fig. 3.2(b), the heat capacity would be lumped evenly to all nodes even though nodes 2 and 3 should be weighed heavier since they have a larger tributary volume.

For a distorted finite element grid, therefore, a more accurate formula to use in lumping the system heat capacity matrix is:

$$C_{ii} = \sum_m \sum_{j=1}^N \int_{V_m} \rho_m c_m h_{jm} dV_m \quad (3.35)$$

where  $m$  is the number of elements attached to node  $i$ ,  $N$  is the number of nodes in each element and  $h_{jm}$  is the interpolation function corresponding to node  $j$  of element  $m$ . For any element  $m$ , the integral in Eq. (3.35) is exactly equal to  $\rho_m c_m V_m$  for the element. Equation (3.35) is not applicable, however, to higher order elements because negative values of  $C_{ij}$  will result if the midside nodes are close to the corner nodes.



(a) Regular Grids

(b) Distorted Element

FIG. 3.2 HEAT CAPACITY IDEALIZATION FOR 4-NODE ELEMENTS

(b) Higher Order Elements

The DOT and DETECT finite element programs described in Appendices A and B employ a higher order 4- to 8-node element. For these programs, it was necessary to use a lumped heat capacity approximation for the consistent element heat capacity matrix, defined as:

$$(C_{ij})_m = \int_{V_m} \rho_m c_m h_{im} h_{jm} dV_m \quad (3.36)$$

The steps used for lumping the element heat capacity matrix for higher order elements are:

- (1) Calculate diagonal terms from consistent heat capacity equation (3.36):

$$(C_{ii})_m = \int_{V_m} \rho_m c_m h_{im}^2 dV_m \quad (3.37)$$

- (2) Compute the total heat capacity of element m:

$$(C_T)_m = \int_{V_m} \rho_m c_m dV_m \quad (3.38)$$

- (3) Compute sum of diagonal terms:

$$S_m = \sum_{i=1}^N (C_{ii})_m \cong (C_T)_m \quad (3.39)$$

where  $N$  = number of nodes in element  $m$ .

The sum  $S_m$  is approximately equal to  $(C_T)_m$ .

- (4) Apply corrections to the diagonal terms  $(C_{ii})_m$  so that  $S_m \equiv (C_T)_m$ :

$$(C_{ii}^*)_m = R_m (C_{ii})_m \quad (3.40)$$

where

$$R_m = \frac{(C_T)_m}{S_m} ; \text{ correction factor}$$

$$(C_{ii}^*)_m = \text{lumped diagonal heat capacity terms for element } m.$$

All of the integrations in the above steps are computed using Gaussian quadrature, and the lumped element heat capacity matrices resulting from Eq. (3.40) are assembled into the system heat capacity matrix  $\underline{C}$  by the direct summation shown in Eq. (3.32).



### 3.2.3 Heat Flux Vector

The system heat flux vector  $\underline{Q}(t)$  at time  $t$  is made up of the contributions from four separate sources:

$$\underline{Q}(t) = \underline{Q}^1(t) + \underline{Q}^2(t) + \underline{Q}^3(t) + \underline{Q}^4(t) \quad (3.41)$$

- where
- $\underline{Q}^1(t)$  = externally supplied nodal heat flux (time dependent)
  - $\underline{Q}^2(t)$  = convective heat transfer at the surface (time and temperature dependent)
  - $\underline{Q}^3(t)$  = radiative heat transfer at the surface (time and temperature dependent)
  - $\underline{Q}^4(t)$  = internal heat generation (time dependent)

#### A. Nodal Heat Fluxes

In the finite element solution of heat conduction problems, either a temperature or an externally supplied heat flux must be associated with each node. The external heat flow  $Q_i$  supplied to node  $i$  can either be constant or a prescribed function of time, and the system heat flux vector  $\underline{Q}^1(t)$  is formed by direct assembly of these  $Q_i$  contributions.

#### B. Convective Heat Transfer

In the case of linear free convection, the rate of heat flux across a boundary layer at the surface of a body per unit area is:

$$q^2 = h^C [T_e - T_s] \quad (3.42)$$

- where
- $h^C$  = heat transfer coefficient for the boundary layer which may be time dependent.
  - $T_e$  = temperature of the external environment which is a known function of time.
  - $T_s$  = unknown surface temperature of the body.

Assume that a boundary element  $m$  lies between nodes  $i$  and  $j$  and is subjected to surface heat transfer of the form described by Eq. (3.42). The surface temperature field for the boundary element can be expressed in terms of the nodal temperatures by the approximate relationship:

$$T_m(\bar{x}, t) = \underset{1 \times 2}{\phi_m(\bar{x})} \underset{2 \times 1}{T_m(t)} \quad (3.43)$$

where

$\phi_m(\bar{x})$  = interpolation vector describing the variation of temperature along boundary element  $m$ .

$T_m(t)$  = nodal point temperature vector for boundary element  $m$ .

$\bar{x}$  = spatial coordinate

The contribution to the surface heat flux vector  $\underline{Q}^2(t)$  at any time  $t$  is given by the surface integral [3,26]:

$$\underset{2 \times 1}{\underline{q}_m^2} = \int_{S_m} h_m^c T_e \underset{2 \times 1}{\phi_m^T} dS_m \quad (3.44)$$

where

$h_m^c$  = heat transfer coefficient for boundary element  $m$ .

$S_m$  = surface area of boundary element  $m$ .

$\phi_m$  = temperature interpolation vector given by Eq. (3.43).

The heat flux components in  $\underline{q}_m^2$  are added directly into the heat flux vector  $\underline{Q}^2(t)$ .

For convective heat transfer, the appropriate terms of the system conductivity matrix  $\underline{K}$  must be modified by the coefficients of the following matrix:

$$\underset{2 \times 2}{\underline{K}_m^2} = \int_{S_m} h_m^c \phi_m^T \phi_m dS_m \quad (3.45)$$

The matrix  $\underline{K}_m^2$  is directly assembled into  $\underline{K}$  for nodes  $i$  and  $j$  which define the boundary element  $m$ .

The matrices  $\underline{q}_m^2$  from Eq. (3.44) and  $\underline{K}_m^2$  from Eq. (3.45) will now be derived for both planar and axisymmetric solids.

(a) Planar Solid

Consider the convection boundary element  $m$  in Fig. 3.3(a) which lies between nodes  $i$  and  $j$  on the surface of a planar solid. The temperature interpolation vector  $\underline{\phi}_m$  which was defined in Eq. (3.43) can be constructed as:

$$T_m(r,t) = \underbrace{\underline{\phi}_m(r)}_{1 \times 2} \underbrace{T_m(t)}_{2 \times 1} = \left[ \left(1 - \frac{r}{L}\right) \left(\frac{r}{L}\right) \right] \begin{Bmatrix} T_i \\ T_j \end{Bmatrix} \quad (3.46)$$

where

$T_i, T_j$  = temperatures of nodes  $i$  and  $j$ .

$r$  = local coordinate measured along surface of element from node  $i$  to node  $j$ .

$L$  = length of boundary surface:

$$\left[ (x_i - x_j)^2 + (y_i - y_j)^2 \right]^{1/2}$$

$\left. \begin{matrix} x_i, x_j \\ y_i, y_j \end{matrix} \right\}$  = global coordinates of nodes  $i$  and  $j$ .

Assuming the planar boundary element to have unit width, the heat flux vector  $\underline{q}_m^2$  from Eq. (3.44) can now be determined:

$$\underline{q}_m^2 = \int_0^1 \int_0^L h_m^c T_e \begin{bmatrix} 1 - \frac{r}{L} \\ \frac{r}{L} \end{bmatrix} dr dt$$

and solving we have:

$$(q_i^2)_m = \frac{h_m^c L}{2} T_e$$

$$(q_j^2)_m = \frac{h_m^c L}{2} T_e$$

(3.47)

The element conductivity matrix  $K_m^2$  for a planar boundary surface  $m$  can be similarly found from Eq. (3.45) as:

$$K_m^2 = \int_0^1 \int_0^L h_m^c \begin{bmatrix} 1 - \frac{r}{L} \\ \frac{r}{L} \end{bmatrix} \begin{bmatrix} (1 - \frac{r}{L}) & (\frac{r}{L}) \end{bmatrix} dr dt$$

and solving we have:

$$\begin{aligned} (K_{ii}^2)_m &= \frac{h_m^c L}{3} \\ (K_{jj}^2)_m &= \frac{h_m^c L}{3} \\ (K_{ij}^2)_m &= \frac{h_m^c L}{6} \end{aligned} \quad (3.48)$$

(b) Axisymmetric Solid

Consider the axisymmetric convection boundary element in Fig. 3.3(b) which lies between nodes  $i$  and  $j$ . The temperature interpolation vector  $\phi_m$  which describes the variation of temperature along this element is identical to the one constructed for the planar solid in Eq. (3.46).

The differential surface area  $dS_m$  for a segment of angle  $\theta$  can be computed as:

$$dS_m = dr \cdot X_1(r) d\theta \quad (3.49)$$

where

$r$  = local coordinate for boundary element surface measured from node  $i$  to node  $j$ .

$X_1(r)$  = radius to any point  $r$  between nodes  $i$  and  $j$ .

From Eq. (3.1) we have:

$$x_1(r) = \phi_m x_m = \begin{bmatrix} (1 - \frac{r}{L}) & (\frac{r}{L}) \end{bmatrix} \begin{Bmatrix} x_i \\ x_j \end{Bmatrix} \quad (3.50)$$

Substituting Eq. (3.50) into (3.49) and assuming a unit radian segment ( $d\theta = 1$ ), the heat flux vector  $q_m^2$  for the axisymmetric boundary element  $m$  may now be found from Eq. (3.44):

$$q_m^2 = \int_0^1 \int_0^L h_m^c T_e \begin{bmatrix} 1 - \frac{r}{L} \\ \frac{r}{L} \end{bmatrix} \begin{bmatrix} (1 - \frac{r}{L}) & (\frac{r}{L}) \end{bmatrix} \begin{Bmatrix} x_i \\ x_j \end{Bmatrix} dr d\theta$$

and solving we have:

$$\begin{aligned} (q_i^2)_m &= \frac{h_m^c L}{6} T_e [2x_i + x_j] \\ (q_j^2)_m &= \frac{h_m^c L}{6} T_e [x_i + 2x_j] \end{aligned} \quad (3.51)$$

Similarly, the element conductivity matrix  $K_m^2$  for an axisymmetric boundary element may be determined from Eq. (3.45):

$$K_m^2 = \int_0^1 \int_0^L h_m^c \begin{bmatrix} 1 - \frac{r}{L} \\ \frac{r}{L} \end{bmatrix} \begin{bmatrix} (1 - \frac{r}{L}) & (\frac{r}{L}) \end{bmatrix} \begin{bmatrix} (1 - \frac{r}{L}) & (\frac{r}{L}) \end{bmatrix} \begin{Bmatrix} x_i \\ x_j \end{Bmatrix} dr d\theta$$

and solving we have:

$$\begin{aligned} (K_{ii}^2)_m &= \frac{h_m^c L}{4} [x_i + \frac{1}{3} x_j] \\ (K_{jj}^2)_m &= \frac{h_m^c L}{4} [\frac{1}{3} x_i + x_j] \\ (K_{ij}^2)_m &= \frac{h_m^c L}{12} [x_i + x_j] \end{aligned} \quad (3.52)$$

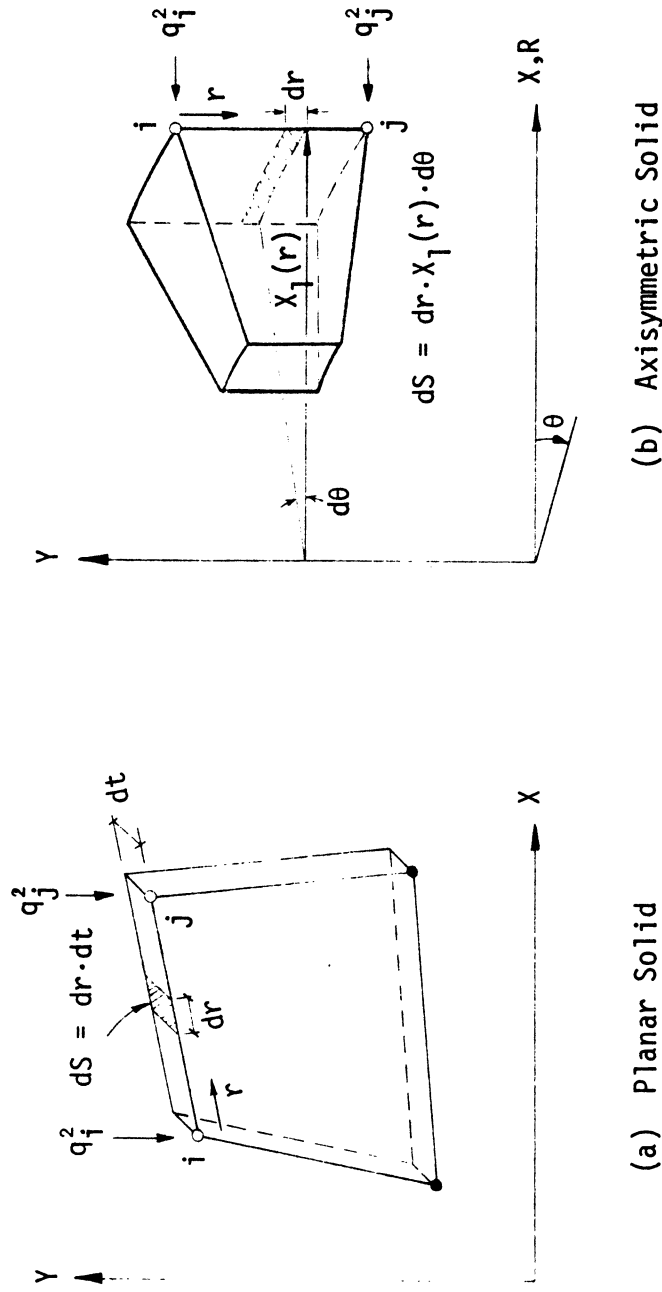


FIG. 3.3 CONVECTION BOUNDARY ELEMENTS FOR PLANAR AND AXISYMMETRIC SOLIDS

### C. Radiation Heat Transfer

The rate of heat transfer by radiation between two surfaces can be found by considering both surfaces to be gray and idealizing them as two infinitely large parallel plates. The net rate of radiative heat transfer per unit area between the surfaces can then be expressed as [29]:

$$q^3 = V\sigma \left[ \frac{1}{\frac{1}{\epsilon_r} + \frac{1}{\epsilon_s} - 1} \right] [\bar{T}_r^4 - \bar{T}_s^4] = h^r \cdot [\bar{T}_r^4 - \bar{T}_s^4] \quad (3.53)$$

where

- $V$  = radiation view factor.
- $\sigma$  = Stefan-Boltzmann constant.
- $\epsilon_r$  = emissivity of the radiation source.
- $\epsilon_s$  = emissivity of the boundary surface.
- $\bar{T}_r$  = absolute temperature of the radiation source.
- $\bar{T}_s$  = absolute temperature of the boundary surface.

If we consider a radiation boundary element  $m$  of unit thickness which lies between nodes  $i$  and  $j$ , the rate at which heat is transferred to the nodes will be approximately:

$$(Q_i^3)_m = \frac{1}{2} h_m^r L_m [(\bar{T}_r^4)_m - (\bar{T}_s^4)_m]$$

$$(Q_j^3)_m = \frac{1}{2} h_m^r L_m [(\bar{T}_r^4)_m - (\bar{T}_s^4)_m] \quad (3.54)$$

where

- $h_m^r$  = radiation heat transfer coefficient defined in Eq. (3.53).
- $L_m$  = length of boundary surface between nodes  $i$  and  $j$ :  

$$\left[ (x_i^2 - x_j^2) + (y_i^2 - y_j^2) \right]^{1/2}$$
- $\left. \begin{matrix} x_i, x_j \\ y_i, y_j \end{matrix} \right\}$  = global coordinates of nodes  $i$  and  $j$ .

$(\bar{T}_r)_m$  = absolute temperature of radiation source  
for boundary element m.

$(\bar{T}_s)_m$  = average value of absolute surface temperature:  

$$\left(\frac{1}{2} [\bar{T}_i + \bar{T}_j]\right)$$

The temperature of the radiation source  $\bar{T}_r$  must be given as a prescribed function of time, and the value of the average absolute surface temperature  $\bar{T}_s$  will depend on the unknown nodal temperatures  $\bar{T}_i$  and  $\bar{T}_j$ . For the finite element program DOT which is described in Appendix A, the value of  $\bar{T}_s$  was determined at the midpoint of a particular time step by assuming a linear variation of nodal temperatures over the previous time step.

#### D. Internal Heat Generation

The rate of internal heat generation  $p_m$  within any element m is assumed to initiate at some starting time  $t_0$  and thereafter can vary with time. Thus

$$\begin{aligned} p_m &= 0 & ; & t < t_0 \\ p_m &= f(t) & ; & t > t_0 \end{aligned} \quad (3.55)$$

where  $f(t)$  is a prescribed function of time.

The vector of nodal fluxes for element m at any time  $t > t_0$  can then be computed as:

$$q_m^k = \int_{V_m} \rho_m p_m \underline{b}_m^T dV_m \quad (3.56)$$

where

$\rho_m$  = mass density.

$p_m$  = rate of internal heat generation at time t.

$\underline{b}_m$  = temperature interpolation vector (Eq. (3.5)).

$V_m$  = volume of element.



The integration in Eq. (3.56) is evaluated numerically using Gaussian quadrature and the heat flux components in  $\underline{q}_m^h$  are assembled directly into the heat flux vector  $\underline{Q}^h(t)$ .

The basic equations for the formulation of the finite element equilibrium equation (3.20) are summarized in Table 3.1.

TABLE 3.1	
<u>MATRIX EQUILIBRIUM EQUATIONS FOR HEAT TRANSFER ANALYSIS</u>	
	$\underline{C}(T) \dot{\underline{I}}(t) + \underline{K}(T) \underline{I}(t) = \underline{Q}(t) \quad (3.20)$
where	$\underline{C}(T) = \sum_{m=1}^M \underline{C}_m(T) \quad (3.32)$
	$\underline{K}(T) = \sum_{m=1}^M \underline{K}_m(T) \quad (3.21)$
	$\underline{Q}(t) = \sum_{m=1}^M \underline{Q}_m(t) \quad (3.41)$
and	$\underline{C}_m(T) = \int_{V_m} \rho_m c_m(T) \underline{b}_m^T \underline{b}_m dV_m \quad (3.33)$
	$\underline{K}_m(T) = \int_{V_m} \underline{a}_m^T k_m(T) \underline{a}_m dV_m \quad (3.22)$
	$+ \int_{S_m} h_m^c(T) \underline{\phi}_m^T \underline{\phi}_m dS_m \quad (3.45)$
	$\underline{Q}_m(t) = \underline{Q}_m^1(t) + \int_{S_m} h_m^c T_e(t) \underline{\phi}_m^T dS_m \quad (3.41)$
	$+ \underline{Q}_m^3(t) + \int_{V_m} \rho_m p_m(t) \underline{b}_m^T dV_m \quad (3.44)$
	$(3.54)$
	$(3.56)$

## 4. BOUNDARY CONDITIONS

### 4.1 NODAL TEMPERATURE AND HEAT FLUX BOUNDARY CONDITIONS

If a surface element between nodes  $i$  and  $j$  is exposed to a known heat flux, the heat flow can be lumped at nodes  $i$  and  $j$  by using a method based on the tributary surface area. These lumped heat flow quantities can then be directly assembled into the system heat flux vector  $\underline{Q}^1(t)$ . For nodes on insulated surfaces, the external heat flow is zero.

At certain points in the system, the temperatures may be specified as a function of time. These temperature boundary conditions are similar to the displacement boundary conditions in structural analysis. A commonly used procedure which accounts for these boundary conditions is to partition the matrix equilibrium equation (3.20) in terms of the unknown and specified temperatures [22].

An alternative and very effective computational approach for treating specified nodal temperatures is outlined as follows. Consider node  $i$  in the finite element system shown in Fig. 4.1 where the temperature has a known value  $T_i(t)$ . Assume that an imaginary element which has a large volume and a high thermal conductivity is connected to node  $i$  only. Then the diagonal coefficient term in the system conductivity matrix  $\underline{K}$  for nodal point  $i$  is:

$$K_{ii} = K_{ii}' + k \quad (4.1)$$

where  $k \gg K_{ii}'$ . For the DOT and DETECT computer programs described in Appendices A and B, the value of  $k$  used is  $10^{10}$ .

In a structural analysis problem, this approach is equivalent to adding an imaginary spring to degree of freedom  $i$  which has a very large stiffness  $k_s$  and then specifying a load equal to  $k_s u_i$  at this degree of freedom which produces the specified displacement  $u_i$ .

Note that the system conductivity matrix  $\underline{K}$  does not become ill-conditioned by adding a large number  $k$  to the existing diagonal coefficient  $K_{ii}$ . Only the addition of large numbers to the off-diagonal terms can result in numerical instability of the  $\underline{K}$  matrix.

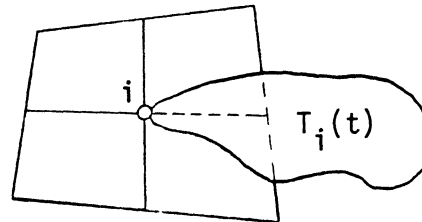


FIG. 4.1 TEMPERATURE BOUNDARY CONDITION IDEALIZATION

#### 4.2 CONVECTION BOUNDARY CONDITION

For linear free convection, the rate of heat flow across a given boundary layer is proportional to the difference in temperature between the surface of the solid  $T_s$  and the external environment  $T_e$ . The necessary modifications to the equilibrium as a result of surface heat transfer have been previously described in Eqs. (3.44) and (3.45). It is of interest to note that the surface temperature of a solid subjected to convection heat transfer closely follows the temperature variation of the external environment. The amount by which the surface temperature lags behind the

environmental temperature is controlled by the magnitude of the surface heat transfer coefficient  $h^c$  in Eq. (3.42). By using a sufficiently large  $h^c$  ( $\approx 10^{10}$ ), the surface temperature will follow the environmental temperature variation exactly.

### 4.3 RADIATION BOUNDARY CONDITION

The net rate of radiant heat transfer between a blackbody surface and an enclosure which completely surrounds it whose surface is also black, i.e. absorbs all the radiant energy incident upon it, is given by:

$$q_r = \sigma A_s [\bar{T}_r^4 - \bar{T}_s^4] \quad (4.2)$$

The heat flow rate  $q_r$  will be in BTU/hr if the surface area  $A_s$  is in sq. ft., the surface and radiation source temperatures  $\bar{T}_s$  and  $\bar{T}_r$  are in degrees Rankine ( $^{\circ}R$ ) and the Stefan-Boltzmann constant  $\sigma$  has the value of  $0.1714 \times 10^{-8}$  BTU/hr-ft $^2$ - $^{\circ}R$ .

Most surfaces encountered in engineering applications do not behave like blackbodies. If neither of the two bodies is a perfect radiator, i.e. if they emit radiation at a lower rate than blackbodies, they are called "gray" bodies.

For the DOT program described in Appendix A, the rate of radiation heat transfer between two gray surfaces is found by considering both the surface and the radiation source to be two infinitely large parallel plates. The required modifications to the system heat flux vector  $\underline{Q}^3(t)$  as a result of radiation heat transfer have been described previously in Eq. (3.54).

#### 4.4 COOLING PIPES

In the construction of mass concrete structures, the heat given off by the hydrating cement becomes entrapped in the mass under nearly adiabatic conditions and results in the concrete temperature increasing rapidly above the placement temperature. The subsequent decrease in temperature to a level corresponding to the ambient air temperature causes the concrete to contract and may result in random structural cracking if the magnitude of the temperature drop is not controlled. This temperature drop can be minimized by placing the concrete at a low initial temperature and by artificially cooling the concrete by means of embedded pipes.

The previously developed matrix equation governing heat flow equilibrium (Eq. (3.20)) must be modified in order to account for the heat transferred out of the solid by a cooling pipe. Consider a cooling pipe located at node  $i$  in a finite element system. Assuming that the cooling pipe is thin-walled, the temperature on the outer surface of the pipe is approximately equal to the temperature of the water  $T_w$  in the pipe. Having made this assumption, the exact temperature distribution between a cooling pipe located at node  $i$  of element  $m$  and an adjacent nodal point a distance "a" away from the pipe is shown in Fig. 4.1.

The rate at which heat flows out of the solid and into the cooling pipe is given by [22]:

$$q = -kA \cdot \frac{\partial T}{\partial r} = -k \cdot 2\pi r t \cdot \frac{\partial T}{\partial r} \quad (4.3)$$

where  $k$  = average thermal conductivity of the finite elements surrounding the cooling pipe.  
 $r$  = distance from the center of the pipe.  
 $T$  = temperature field.  
 $t$  = thickness of element.

By separating the variables in Eq. (4.3) and integrating between  $T_w$  at  $R$  and  $T_a$  at "a" we find:

$$q = \frac{2\pi kt}{\ln\left[\frac{a}{R}\right]} (T_w - T_a) \quad (4.4)$$

where  $T_a$  = temperature at the node point a distance "a" from the pipe.  
 $T_w$  = temperature of the cooling water.  
 $R$  = radius of the cooling pipe.

In the finite element solution, the temperature distribution within the elements adjacent to the cooling pipe is assumed to be linear. If we associate an effective tributary area having a radius of  $a/2$  with each cooling pipe in the system, then the rate at which heat flows into the pipe from this area can be found from Eq. (4.3) as:

$$q = -2\pi kt \left[\frac{a}{2}\right] \left(\frac{T_a - T_i}{a}\right) = \pi kt \cdot (T_i - T_a) \quad (4.5)$$

where  $T_i$  = apparent temperature at node  $i$  in the finite element system.

Combining Eqs. (4.4) and (4.5) and eliminating  $T_a$  we can obtain the rate at which heat is removed from the system by a cooling pipe:

$$q = H \cdot (T_w - T_i) \quad (4.6)$$

where

$$H = \frac{2\pi kt}{\ln\left[\frac{a}{R}\right] - 2}$$

It is of interest to note that for an element size "a" equal to 7.4 times the radius R of the pipe,  $\ln\left[\frac{a}{R}\right] = 2$  and the value of H is infinite. For this element size, therefore, the apparent nodal temperature  $T_i$  is equal to the cooling water temperature  $T_w$ . For other mesh spacings the correct value of H can be computed from Eq. (4.6). In case the elements surrounding the cooling pipe are not all the same size, a weighted value of "a" should be used in Eq. (4.6) representing the average distance to the adjacent nodes.

The cooling pipe boundary condition equation (4.6) is recognized to be of the same form as the convection boundary condition equation (3.42). Similar modifications, therefore, can be made to the system conductivity matrix  $\underline{K}$  and heat flux vector  $\underline{Q}$  as were made in Eqs. (3.47) and (3.48).

For a cooling pipe located at a typical nodal point i in a finite element system, the following modifications must be made to the system conductivity and heat flux matrices:

$$\begin{aligned} K_{ii} &= K'_{ii} + H \\ Q_i &= Q'_i + HT_w \end{aligned} \quad (4.7)$$

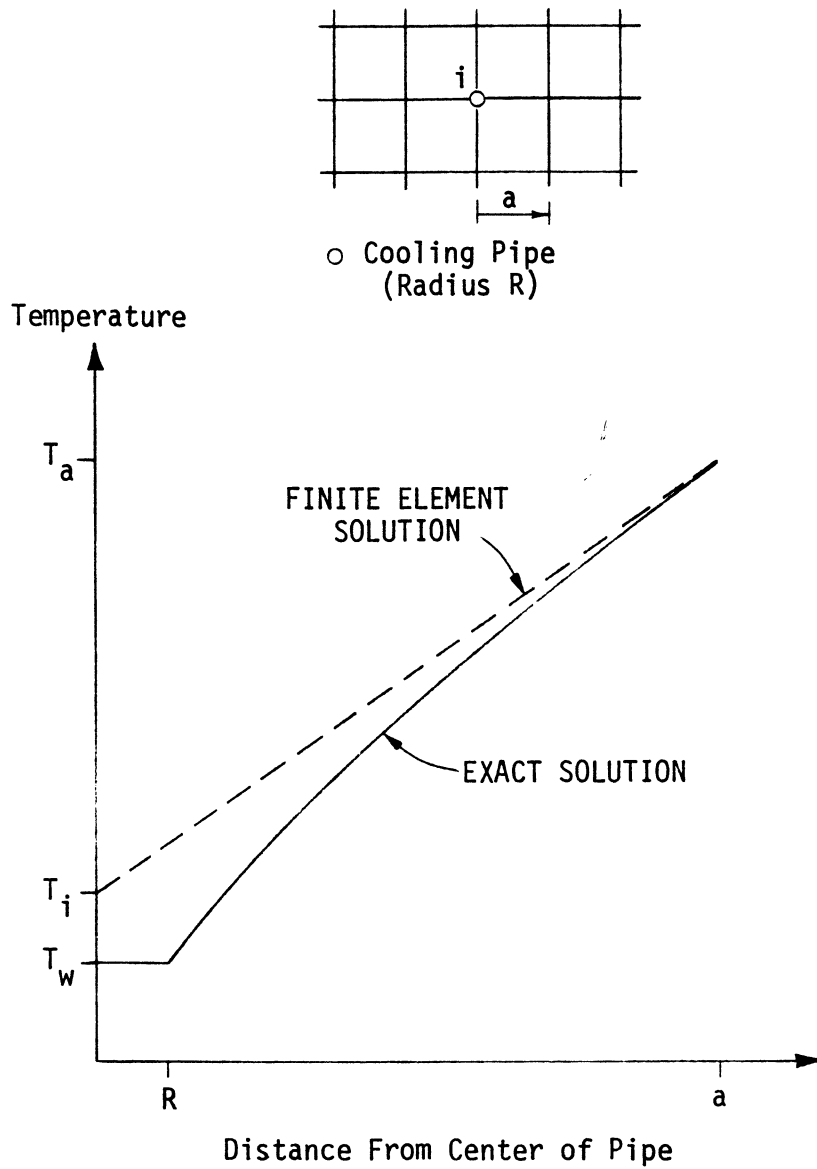


FIG. 4.1 TEMPERATURE DISTRIBUTION NEAR A COOLING PIPE



## 5. NUMERICAL SOLUTION OF THE HEAT FLOW EQUILIBRIUM EQUATION

The heat flow equilibrium equation (3.20) represents a set of first order nonlinear differential equations. Numerical integration schemes for solving this equation will be discussed for both linear systems having constant thermal properties and nonlinear systems in which the thermal properties are temperature dependent.

### 5.1 LINEAR SYSTEMS

At any instant "t" in time, the linear heat conduction equilibrium equation for a finite element system given by Eq. (3.20) can be expressed as:

$$\underline{C} \dot{\underline{T}}_t + \underline{K} \underline{T}_t = \underline{Q}_t \quad (5.1)$$

Similarly, at time  $t + \Delta t$  we have:

$$\underline{C}_{t+\Delta t} \dot{\underline{T}}_{t+\Delta t} + \underline{K}_{t+\Delta t} \underline{T}_{t+\Delta t} = \underline{Q}_{t+\Delta t} \quad (5.2)$$

The solution to this set of first order differential equations can be obtained by using a step-by-step integration (or time marching) procedure which assumes a linear variation of temperature over the time step  $\Delta t$  (Fig. 5.1). This is a simple method which has proven to be both efficient and accurate [ 3,24 ].

Using the assumption of linear temperature variation over the time step  $\Delta t$ , the time rate-of-change in temperature  $\dot{\underline{T}}$  at any time  $\xi$  in the interval  $\{t, t+\Delta t\}$  is:

$$\dot{\underline{T}}(\xi) = \frac{1}{\Delta t} (\underline{T}_{t+\Delta t} - \underline{T}_t) \quad (5.3)$$

Hence, at time  $t = t + \Delta t$  we have:

$$\dot{\underline{T}}_{t+\Delta t} = \frac{1}{\Delta t} (\underline{T}_{t+\Delta t} - \underline{T}_t) \quad (5.4)$$

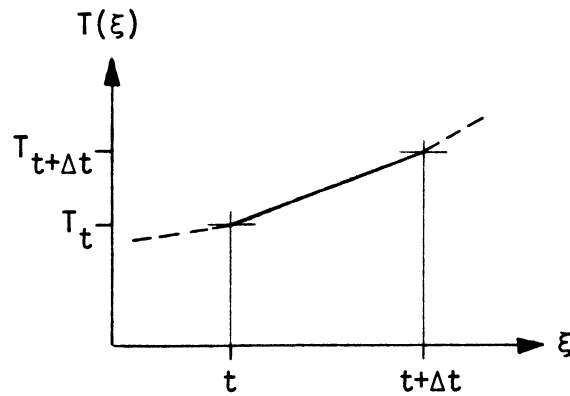


FIG. 5.1 TIME VARIATION OF NODAL TEMPERATURES  $T$   
OVER A SHORT TIME PERIOD  $\Delta t$

The matrix equation for heat flow equilibrium at time  $t+\Delta t$  can now be found by substituting Eq. (5.4) into Eq. (5.2). The resulting equation is:

$$\left[ \frac{1}{\Delta t} \underline{C} + \underline{K} \right] \underline{T}_{t+\Delta t} = \underline{Q}_{t+\Delta t} + \frac{1}{\Delta t} \underline{C} \underline{T}_t \quad (5.5)$$

Defining,

$$\underline{K}^* = \frac{1}{\Delta t} \underline{C} + \underline{K} \quad (5.6)$$

$$\underline{Q}_{t+\Delta t}^* = \underline{Q}_{t+\Delta t} + \frac{1}{\Delta t} \underline{C} \underline{T}_t \quad (5.7)$$

Then Eq. (5.5) simplifies to:

$$\underline{K}^* \underline{T}_{t+\Delta t} = \underline{Q}_{t+\Delta t}^* \quad (5.8)$$

Since the matrices  $\underline{C}$ ,  $\underline{K}$ ,  $\underline{Q}_{t+\Delta t}$  and  $\underline{T}_t$  are known at the start of the time interval  $\{t, t+\Delta t\}$ , Eq. (5.8) can therefore be solved directly for the nodal temperatures  $\underline{T}_{t+\Delta t}$  at the end of the time interval. The step-by-step solution procedure for solving Eq. (5.8) is summarized in Table 5.1.

Since the "effective" conductivity matrix  $\underline{K}^*$  is not a function of time, it can be formed once for a given geometry and triangularized. In each subsequent time step, therefore, it is only necessary to define the thermal load vector  $\underline{Q}_{t+\Delta t}$  and then solve by simple back-substitution for the system temperatures  $\underline{T}_{t+\Delta t}$ . The matrix  $\underline{K}^*$  is normally banded and its triangularized form is banded as well, so a large amount of computer storage is usually not required for placing  $\underline{K}^*$  in core.

It should be noted that at time zero, an initial distribution of nodal temperatures  $\underline{T}_0$  may exist. For this case, the "effective" heat flux vector  $\underline{Q}_{\Delta t}^*$  at the end of the first time interval is given by:

$$\begin{aligned}\underline{Q}_{\Delta t}^* &= \underline{Q}_{\Delta t} + \frac{1}{\Delta t} \underline{C} \underline{T}_0 \\ &= \underline{Q}_{\Delta t} + \underline{E}_0\end{aligned}\tag{5.9}$$

where  $\underline{E}_0$  is called the initial resistance vector. In general:

$$\underline{Q}_{t+\Delta t}^* = \underline{Q}_{t+\Delta t} + \underline{E}_t\tag{5.10}$$

where

$$\underline{E}_t = \frac{1}{\Delta t} \underline{C} \underline{T}_t$$

TABLE 5.1

SUMMARY OF THE STEP-BY-STEP SOLUTION METHOD  
FOR LINEAR HEAT TRANSFER

## INITIAL CALCULATIONS

1. Form  $\underline{K}$  and  $\underline{C}$ ; initialize  $\underline{T}_0$ .
2. Modify  $\underline{K}$  for convection and cooling pipe boundary conditions.
3. Modify  $\underline{K}$  for temperature boundary conditions.
4. Compute the effective system matrices:

$$\underline{C}^* = \frac{1}{\Delta t} \underline{C}$$

$$\underline{K}^* = \underline{K} + \underline{C}^*$$

5. Compute the initial resistance vector:

$$\underline{E}_0 = \underline{C}^* \underline{T}_0$$

6. Triangularize  $\underline{K}^*$ .

## FOR EACH SOLUTION TIME STEP

1. Define the heat flow vector  $\underline{Q}_{t+\Delta t}$  at time  $t+\Delta t$ .
2. Compute the effective heat flow vector:

$$\underline{Q}_{t+\Delta t}^* = \underline{Q}_{t+\Delta t} + \underline{E}_t$$

3. Solve the effective heat flow equilibrium equation for the nodal temperatures  $\underline{T}_{t+\Delta t}$  at time  $t+\Delta t$ .

$$\underline{K}^* \underline{T}_{t+\Delta t} = \underline{Q}_{t+\Delta t}^*$$

4. Compute the resistance vector for the next time step:

$$\underline{E}_{t+\Delta t} = \underline{C}^* \underline{T}_{t+\Delta t}$$

5. Repeat for the next time step.

## 5.2 STABILITY OF THE NUMERICAL INTEGRATION SCHEME

The step-by-step integration procedure described in the previous section assumed a linear variation of temperature over the time step  $\Delta t$ . This algorithm is unconditionally stable for a heat conduction problem if the solution of the initial value problem is bounded (i.e. no error growth) for any time step  $\Delta t$ . This is to say that any round-off error in the predicted temperatures does not grow with time as the solution proceeds.

### 5.2.1 Modal Heat Flow Equations

Consider the heat flow equilibrium equation:

$$\underline{C} \dot{\underline{T}}(t) + \underline{K} \underline{T}(t) = \underline{Q}(t) \quad (5.11)$$

For a solution to the homogeneous part of this equation, assume:

$$\underline{T}(t) = e^{-\lambda t} \underline{\phi} \quad (5.12)$$

Thus,

$$\underline{C} [-\lambda e^{-\lambda t} \underline{\phi}] + \underline{K} [e^{-\lambda t} \underline{\phi}] = \underline{0}$$

Because the value of  $e^{-\lambda t}$  can never equal zero, we therefore obtain a statement of the generalized eigenvalue problem:

$$\underline{K} \underline{\phi} = \lambda \underline{C} \underline{\phi} \quad (5.13)$$

Equation (5.13) is an  $n$ th order equation where  $n$  is the number of temperature degrees of freedom in the system. The  $n$  solutions to Eq. (5.13) can be stated as:

$$\underline{K} \underline{\Phi} = \underline{C} \underline{\Phi} \underline{\Lambda} \quad (5.14)$$

where the columns in  $\underline{\Phi}$  are the  $\underline{C}$ -orthonormalized (i.e.  $\underline{\Phi}^T \underline{C} \underline{\Phi} = \underline{I}$ ) eigenvectors (thermal modes)  $\underline{\phi}_1, \dots, \underline{\phi}_n$ , and  $\underline{\Lambda}$  is a diagonal matrix containing the eigenvalues (thermal frequencies)  $\lambda_1, \dots, \lambda_n$ .

By using the transformation  $\underline{T} = \underline{\Phi} \underline{X}$  (and  $\dot{\underline{T}} = \underline{\Phi} \dot{\underline{X}}$ ), the heat flow equilibrium Eq. (5.11) can be written in the eigenvector basis as:

$$\underline{C} \underline{\Phi} \dot{\underline{X}} + \underline{K} \underline{\Phi} \underline{X} = \underline{Q} \quad (5.15)$$

Substituting Eq. (5.14) into (5.15):

$$\underline{C} \underline{\Phi} \dot{\underline{X}} + \underline{C} \underline{\Phi} \underline{\Lambda} \underline{X} = \underline{Q} \quad (5.16)$$

Pre-multiplying Eq. (5.16) by  $\underline{\Phi}^T$ :

$$\underline{\Phi}^T \underline{C} \underline{\Phi} \dot{\underline{X}} + \underline{\Phi}^T \underline{C} \underline{\Phi} \underline{\Lambda} \underline{X} = \underline{\Phi}^T \underline{Q} \quad (5.17)$$

Because the eigenvectors  $\underline{\Phi}$  are  $\underline{C}$ -orthonormalized, Eq. (5.17) reduces to the form:

$$\dot{\underline{X}} + \underline{\Lambda} \underline{X} = \underline{\Phi}^T \underline{Q} \quad (5.18)$$

These equations are uncoupled and can readily be solved by a number of numerical procedures.

To study the stability and accuracy of the iteration scheme, it is noted that the integration of the heat flow equilibrium equation (5.11) in the original finite element coordinate basis is equivalent to the integration of the  $n$  uncoupled first order differential equations (5.18) in the thermal mode basis. Therefore, for the purpose of a stability analysis, we only need to study the integration algorithm as applied to a typical equation "i" in Eq. (5.18):

$$\dot{x} + \lambda_i x = q \quad (5.19)$$

where

$$q = \underline{\Phi}_i^T \underline{Q}$$

### 5.2.2 Step-By-Step Integration Procedure

In order to express Eq. (5.19) in a difference form, let the temperature  $x_t$  and the time rate-of-change of temperature  $\dot{x}_t$  be known at time  $t$ . By assuming that the temperature varies linearly in the time interval  $\{t, t+\Delta t\}$ , the temperature gradient  $\dot{x}_{t+\Delta t}$  at time  $t+\Delta t$  is:

$$\dot{x}_{t+\Delta t} = \frac{1}{\Delta t} (x_{t+\Delta t} - x_t) \quad (5.20)$$

Substituting Eq. (5.20) into (5.19), the resulting heat flow equilibrium equation to be satisfied in the  $i$ th mode at time  $t+\Delta t$  is:

$$\frac{1}{\Delta t} (x_{t+\Delta t} - x_t) + \lambda_i x_{t+\Delta t} = q_{t+\Delta t}$$

or

$$x_{t+\Delta t} = Ax_t + Lq_{t+\Delta t} \quad (5.21)$$

where

$$A = \frac{1}{1 + \lambda_i \Delta t} \quad (5.22)$$

$$L = \frac{\Delta t}{1 + \lambda_i \Delta t} \quad (5.23)$$

The quantity  $A$  is the difference approximation operator and  $L$  is the heat flux operator as applied to the  $i$ th uncoupled modal heat flow equation.

The recursion relation in Eq. (5.21) can be used to study the stability and accuracy of the integration scheme. In general, the solution at any time  $t + m\Delta t$  (where  $m$  is a positive integer) is given by:

$$x_{t+m\Delta t} = A^m x_t + A^{m-1} L q_{t+\Delta t} + \dots + L q_{t+m\Delta t} \quad (5.24)$$

### 5.2.3 Stability

Consider Eq. (5.24) with  $q$  equal to zero:

$$x_{t+m\Delta t} = A^m x_t \quad (5.25)$$

The integration method is unconditionally stable if  $A^m$  is bounded for large values of  $m$  (i.e. as  $m \rightarrow \infty$ ) and for any time step  $\Delta t$ .

This stability condition may be stated as:

$$A \leq 1 \quad (5.26)$$

It is noted that if  $A < 1$ , then  $A^m \rightarrow 0$  as  $m \rightarrow \infty$ , and the smaller the value of  $A$  the more rapid the convergence. Recalling Eq. (5.22), the stability condition requires that:

$$A = \frac{1}{1 + \lambda_i \Delta t} \leq 1$$

or

$$1 + \lambda_i \Delta t \geq 1 \quad (5.27)$$

Since the thermal frequency  $\lambda_i$  for the  $i$ th mode must satisfy the relation  $\lambda_i \geq 0$ , the integration algorithm is unconditionally stable for all positive values of the selected time step ( $\Delta t > 0$ ). The accuracy of the integration scheme clearly depends on the magnitude of  $\lambda_i \Delta t$ .



### 5.3 NONLINEAR SYSTEMS

In the analysis of nonlinear systems, direct integration must be used. At time  $t + \Delta t$ , the exact equation of heat flow equilibrium is:

$$\underline{C}_{t+\Delta t} \dot{\underline{T}}_{t+\Delta t} + \underline{K}_{t+\Delta t} \underline{T}_{t+\Delta t} = \underline{Q}_{t+\Delta t} \quad (5.28)$$

where

$\underline{C}_{t+\Delta t}$  = system heat capacity matrix at time  $t + \Delta t$ .

$\underline{K}_{t+\Delta t}$  = system thermal conductivity matrix at  $t + \Delta t$ .

$\underline{T}_{t+\Delta t}$  = vector of nodal point temperatures at  $t + \Delta t$ .

$\dot{\underline{T}}_{t+\Delta t}$  = vector of the time rate-of-change of the nodal point temperatures at time  $t + \Delta t$ .

$\underline{Q}_{t+\Delta t}$  = vector of the externally supplied nodal heat fluxes at time  $t + \Delta t$ .

In order to solve Eq. (5.28), we make the approximation that:

$$\begin{aligned} \underline{C}_{t+\Delta t} &\cong \underline{C}_t \\ \underline{K}_{t+\Delta t} &\cong \underline{K}_t \end{aligned} \quad (5.29)$$

Equation (5.28) now becomes:

$$\underline{C}_t \dot{\underline{T}}_{t+\Delta t} + \underline{K}_t \underline{T}_{t+\Delta t} = \underline{Q}_{t+\Delta t} \quad (5.30)$$

Using the assumption in Eq. (5.4) that the temperature variation over the time step  $\Delta t$  is linear, we can substitute Eq. (5.4) into Eq. (5.30) to obtain the following approximation:

$$\underline{C}_t \frac{1}{\Delta t} (\underline{T}_{t+\Delta t} - \underline{T}_t) + \underline{K}_t \underline{T}_{t+\Delta t} = \underline{Q}_{t+\Delta t} \quad (5.31)$$

Subtracting  $\underline{K}_t \underline{T}_t$  from both sides of Eq. (5.31) we have:

$$\frac{1}{\Delta t} \underline{C}_t \Delta \underline{T}_t + \underline{K}_t \Delta \underline{T}_t \doteq \underline{Q}_{t+\Delta t} - \underline{K}_t \underline{T}_t \quad (5.32)$$

where

$$\Delta \underline{T}_t = \underline{T}_{t+\Delta t} - \underline{T}_t \quad (5.33)$$

Equation (5.32) can be rewritten as:

$$\left[ \frac{1}{\Delta t} \underline{C}_t + \underline{K}_t \right] \Delta \underline{T}_t \doteq \underline{Q}_{t+\Delta t} - \underline{K}_t \underline{T}_t$$

or

$$\underline{K}_t^* \Delta \underline{T}_t \doteq \underline{Q}_{t+\Delta t} - \underline{F}_t^k \quad (5.34)$$

where

$$\underline{K}_t^* = \frac{1}{\Delta t} \underline{C}_t + \underline{K}_t$$

$$\underline{F}_t^k = \underline{K}_t \underline{T}_t$$

The incremental equation for heat flow equilibrium given in Eq. (5.34) is equivalent to applying Eq. (5.8) in which  $\underline{K}$  is updated in each time step. The solution for the nodal temperatures at time  $t + \Delta t$  is given by:

$$\underline{T}_{t+\Delta t} = \underline{T}_t + \Delta \underline{T}_t \quad (5.35)$$

Because of errors introduced by the linearization of Eq. (5.31), the temperatures  $\underline{T}_{t+\Delta t}$  resulting from Eqs. (5.34) and (5.35) are only an approximation to the actual nodal temperatures at time  $t + \Delta t$ . These errors may be corrected by using an iterative technique for heat flow equilibrium. An efficient step-by-step solution procedure for nonlinear heat conduction problems is summarized in Table 5.2 which includes the option of heat flow equilibrium iteration.

TABLE 5.2

SUMMARY OF THE STEP-BY-STEP SOLUTION METHOD  
FOR NONLINEAR HEAT TRANSFER

## INITIAL CALCULATIONS

1. Define all input, including initial temperatures  $\underline{T}_0$ .
2. Form  $\underline{K}$  and  $\underline{C}$  based on properties at  $\underline{T}_0$ .
3. Modify  $\underline{K}$  for convection and cooling pipe boundary conditions.
4. Modify  $\underline{K}$  for temperature boundary conditions.
5. Compute the internal heat flow due to conduction at time zero:

$$\underline{F}_0^k = \underline{K}_0 \underline{T}_0$$

6. Compute the effective system matrices:

$$\underline{C}^* = \frac{1}{\Delta t} \underline{C}$$

$$\underline{K}^* = \underline{K} + \underline{C}^*$$

7. Triangularize  $\underline{K}^*$ .
8. Initialize:
  - a. Time step counter:  $i = 0$ ,  $t = t_{\text{START}}$
  - b. Convergence tolerance: TOL
  - c. Maximum number of iterations: NITER

## FOR EACH TIME STEP

1. Increment time step counter:  $i = i + 1$  and  $t = t + \Delta t$
2. Test for equation reformation:
  - NO : Advance to Step 9
  - YES : Continue
3. Form new system matrices  $\underline{K}_t$  and  $\underline{C}_t$  based on properties  $\underline{T}_t$ .
4. Modify  $\underline{K}_t$  for convection and cooling pipe boundaries.
5. Modify  $\underline{K}_t$  for temperature boundary conditions.

TABLE 5.2 (CON'T)

6. Compute internal heat flow due to conduction:

$$\underline{F}_t^k = \underline{K}_t \underline{T}_t$$

7. Compute the new effective system matrices:

$$\underline{C}_t^* = \frac{1}{\Delta t} \underline{C}_t$$

$$\underline{K}_t^* = \underline{K}_t + \underline{C}_t^*$$

8. Triangularize  $\underline{K}_t^*$ .

9. Define the heat flow vector  $\underline{Q}_{t+\Delta t}$  at time  $t + \Delta t$ .

10. Compute the effective heat flow vector:

$$\underline{Q}_{t+\Delta t}^* = \underline{Q}_{t+\Delta t} - \underline{F}_t^k$$

11. Solve for increments in nodal point temperatures  $\Delta \underline{T}_{t+\Delta t}$  using the latest  $\underline{K}_t^*$  matrix:

$$\underline{K}_t^* \Delta \underline{T}_{t+\Delta t} = \underline{Q}_{t+\Delta t}^*$$

12. Check if iteration required for heat flow equilibrium:

NO : Advance to Step 21

YES : Continue

13. Initialize:

a. Iteration counter:  $j = 0$

b. First approximation:  $\underline{T}_{t+\Delta t}^{(1)}$

14. Increment iteration counter:  $j = j + 1$

15. Calculate  $j$ th approximation to nodal point temperatures and time derivatives of nodal point temperatures:

$$\underline{T}_{t+\Delta t}^{(j)} = \underline{T}_t + \Delta \underline{T}_{t+\Delta t}^{(j)}$$

$$\dot{\underline{T}}_{t+\Delta t}^{(j)} = \frac{1}{\Delta t} (\underline{T}_{t+\Delta t}^{(j)} - \underline{T}_t)$$

TABLE 5.2 (CON'T)

16. Compute the internal heat flow due to conduction at time  $t + \Delta t$ :

$$F_{-t+\Delta t}^{k(j)} = K_{-t} T_{-t+\Delta t}^{(j)}$$

17. Calculate  $j$ th out-of-balance heat flow rates:

$$Q_{-t+\Delta t}^{r(j)} = Q_{-t+\Delta t} - C_{-t} \dot{T}_{-t+\Delta t}^{(j)} - F_{-t+\Delta t}^{k(j)}$$

18. Solve for  $j$ th correction to temperature increments using the latest  $K^*$  matrix:

$$K^* \Delta \Delta T_{-t+\Delta t}^{(j)} = Q_{-t+\Delta t}^{r(j)}$$

19. Calculate new temperature increments:

$$\Delta T_{-t+\Delta t}^{(j+1)} = \Delta T_{-t+\Delta t}^{(j)} + \Delta \Delta T_{-t+\Delta t}^{(j)}$$

20. Check for convergence:

$$\frac{\|\Delta \Delta T_{-t+\Delta t}^{(j)}\|_2}{\|\Delta T_{-t+\Delta t}^{(j+1)} - T_{-t}\|_2} < \text{TOL}$$

where the Euclidean norm  $\|z\|_2 = \sqrt{\sum_{i=1}^n |z_i|^2}$ .

If convergence :  $\Delta T_{-t+\Delta t} = \Delta T_{-t+\Delta t}^{(j+1)}$  : Advance to Step 21.

If no convergence and  $j < \text{NITER}$  : Advance to Step 14.  
Otherwise, restart using a smaller time step.

21. Calculate new nodal point temperatures:

$$T_{-t+\Delta t} = T_{-t} + \Delta T_{-t+\Delta t}$$

22. Repeat for the next time step : Advance to Step 1.

## 6. COMPUTER PROGRAMS

Two finite element analysis programs have been developed for this study. The program DOT ("Determination Of Temperatures") is a general purpose computer program for both linear and nonlinear analysis of transient heat conduction problems and the program DETECT ("DEtermination of Temperatures in ConsTruCtion") is a linear heat transfer program for the analysis of structures constructed incrementally (e.g. dams, bridge piers and large foundations). Both of these programs have been developed based on the theory presented in the previous sections of this dissertation and are coded in the standard Fortran IV language. A description of the required input data for the DOT and DETECT programs can be found in Appendices A and B, respectively, along with the Fortran listings.

In order to minimize the storage requirements and optimize efficiency, a compacted storage scheme is used in the DOT and DETECT programs to store the effective system conductivity matrix  $\underline{K}^*$ . This matrix is stored as a one-dimensional array in which only those elements below the "skyline" of  $\underline{K}^*$  are processed. This technique is similar to the one used in the nonlinear structural analysis program NONSAP [30].

The equilibrium equations are solved using the linear equation solver COLSOL [31]. This subroutine uses Gauss elimination on the positive-definite symmetrical system of equations, and requires a minimum number of operations since only those elements within the skyline of the  $\underline{K}^*$  matrix are processed.

In order to obtain maximum program capacity, the finite element groups are processed in blocks according to their type (e.g. planar or axisymmetric, convection, radiation or cooling pipes). Secondary or disc storage is then used to store each block of these finite elements. Using this element group data, the effective system thermal conductivity matrix  $\underline{K}^*$  is assembled and stored in primary storage (blank common).

The lowest primary storage locations are reserved throughout the solution for the storage of each block of element group data which is read in from secondary storage. The user must supply the maximum estimated number of storage locations (NUMEST) required to store any individual element group in primary storage. During the input phase, the program calculates the exact number of primary storage locations (MAXEST) required for each element group and NUMEST is reset to MAXEST.

To further improve the primary storage requirements, variable dimensioning is used to dynamically allocate the required core storage remaining into a single array A in blank common.

The program DOT has the option of punching the nodal point temperatures onto data cards after every n time steps as specified by the user. This punched temperature history can then be used as input to a thermal stress analysis program which uses the same finite element model as the heat transfer program.

## 7. SAMPLE ANALYSES

The results of a number of heat transfer problems are presented in this chapter. These analyses were selected to test all major features of the programs DOT and DETECT such as time-dependent boundary conditions, temperature or heat flux constraints, nonzero initial conditions, internal heat generation, surface convection and radiation, nonlinear material properties and incremental construction. Problems involving both steady state and transient response are included, and whenever possible the results have been compared with either analytical results or numerical solutions obtained by other investigators.

### 7.1 STEADY STATE HEAT CONDUCTION IN A SQUARE PLATE

A 4 by 4-in. square plate, as shown in Fig. 7.1, has one edge maintained at  $100^{\circ}\text{F}$  and the other edges held at  $0^{\circ}\text{F}$ . The steady state temperature distribution obtained used the program DOT and a constant value for thermal conductivity.

The temperature distribution was first obtained using a coarse 4 x 4 finite element grid connected by 25 nodal points. The analysis was then repeated using a finer 8 x 8 grid containing 81 nodes. In the second solution, it was only necessary to use a 4 x 8 grid with 45 nodes to represent the half-width of the plate since the global plane ( $Y = 2$  in.) is a plane of conduction symmetry.



The exact solution for the temperature at any point  $(x,y)$  within the plate is given by Carslaw and Jaeger [ 4 ] as the series solution:

$$T(x,y) = \frac{4T_0}{\pi} \sum_{n=0}^{\infty} \frac{1}{(2n+1)} \sin(2n+1)\frac{\pi x}{a} \sinh(2n+1)\frac{(a-y)\pi}{a} \operatorname{cosech}(2n+1)\pi$$

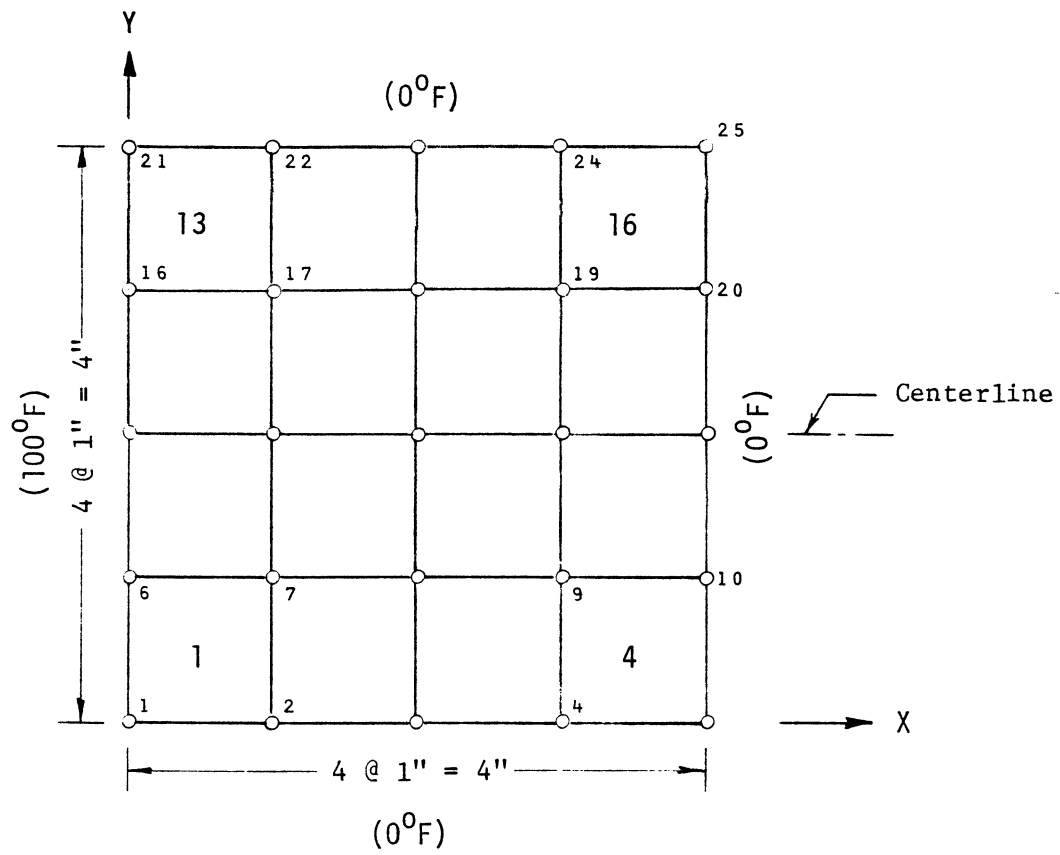
where

$a$  = length of one side of the plate (4 inches)

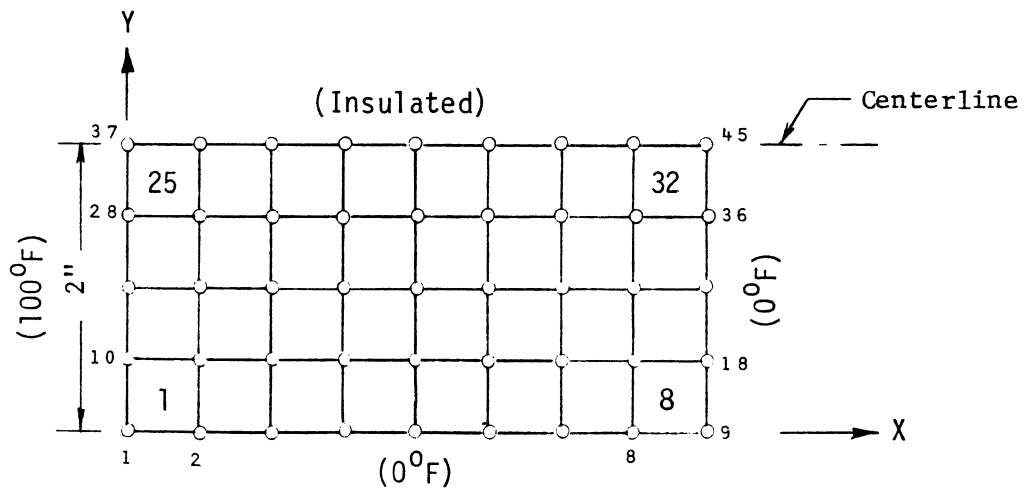
$T_0$  = temperature of side  $Y = 0$  ( $100^{\circ}\text{F}$ )

$x,y$  = coordinate system defined in Fig.

The analytical solution for the temperature distribution along the centerline ( $Y = 2$  in.) of the plate is compared in Fig. 7.2 with the DOT solution. As can be seen, the agreement is excellent and the solution improved when the finer 8 x 8 mesh was used. The results of the numerical solution also matched those obtained numerically by Peterson [25].



(a) 4 x 4 Finite Element Grid



(b) 4 x 8 Finite Element Grid

FIG. 7.1 FINITE ELEMENT MODELS OF 4 BY 4-IN. SQUARE PLATE

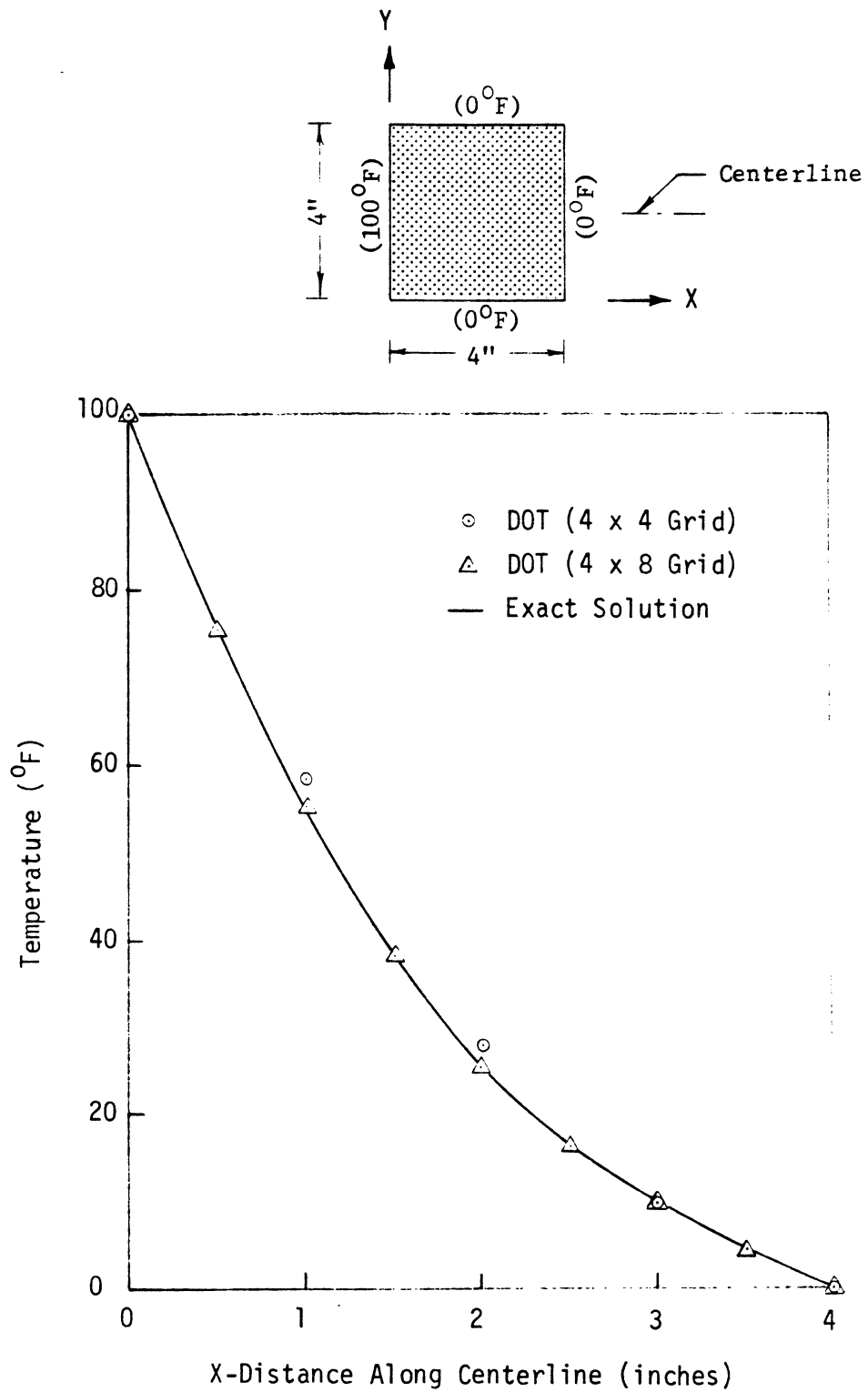


FIG. 7.2 TEMPERATURE DISTRIBUTION ALONG CENTERLINE OF THE 4 BY 4-INCH SQUARE PLATE

## 7.2 STEADY STATE HEAT CONDUCTION IN A LONG HOLLOW CYLINDER

A long hollow cylinder is subjected to an inside temperature of 100°F and an outer surface temperature of 0°F. The cylinder is insulated to prevent axial heat flow and has an inside radius of one inch and an outer radius of two inches. The program DOT was used to obtain the steady state temperature distribution in the radial direction, assuming a constant value of thermal conductivity throughout the cylinder.

For the finite element model, a 1-in. length of the cylinder is represented using ten equally spaced 4-node elements with 22 nodal points through the 1-in. thickness of the cylinder wall. This model is shown in Fig. 7.3(a).

The temperature at any arbitrary radius  $r$  within the curved cylinder wall is given by Kreith [29] as:

$$T(r) = T_i - \frac{T_i - T_o}{\ln(r_o/r_i)} \ln\left(\frac{r}{r_i}\right)$$

where

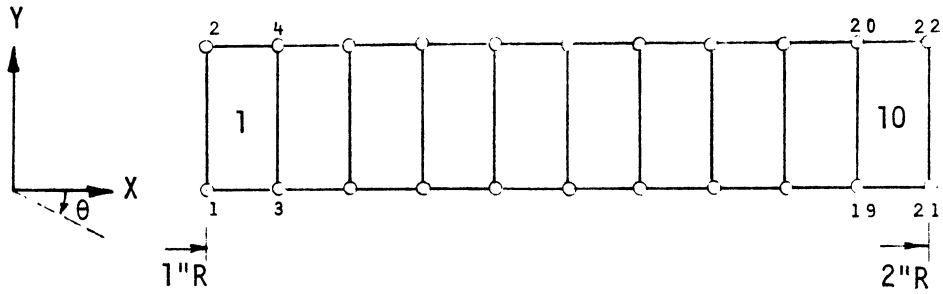
$T_i$  = inner surface temperature

$T_o$  = outer surface temperature

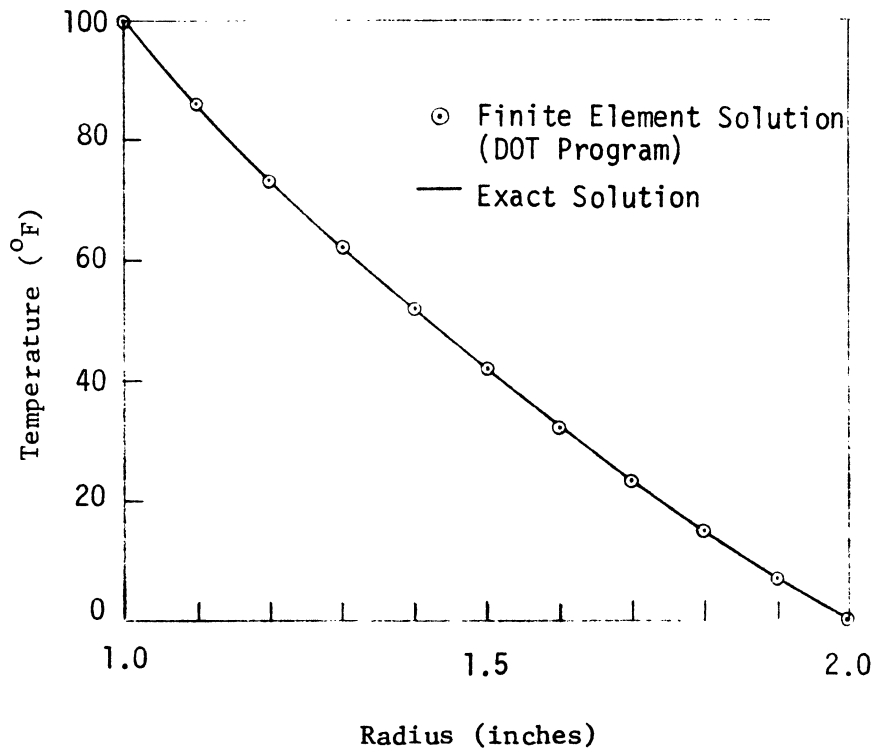
$r_i$  = inside radius

$r_o$  = outside radius

The steady state temperature profile through the cylinder wall obtained using DOT was found to closely match the exact solution given above, as shown in Fig. 7.3(b).



(a) Finite Element Model



(b) Temperature Distribution In Radial Direction

FIG. 7.3 STEADY STATE HEAT CONDUCTION IN A LONG HOLLOW CYLINDER

### 7.3 STEADY STATE HEAT CONDUCTION IN A RECTANGULAR CONCRETE COLUMN EXPOSED TO CONVECTION BOUNDARY CONDITIONS

An exposed 14 by 36-inch rectangular concrete column is subjected to an outside weather temperature of  $100^{\circ}\text{F}$  and an inside environment temperature of  $0^{\circ}\text{F}$ . The inside and outside surfaces of the column are separated by an 8-inch thick wall.

The convection coefficient for the  $100^{\circ}\text{F}$  environment is  $0.5 \text{ BTU/hr-ft}^2\text{-}^{\circ}\text{F}$  and for the  $0^{\circ}\text{F}$  environment is  $6.0 \text{ BTU/hr-ft}^2\text{-}^{\circ}\text{F}$ . Both coefficients decrease linearly to zero from the surface to the center of the abutting wall, as indicated in Fig. 7.4. The thermal conductivity of the concrete is assumed to have a uniform value of  $K = 1.0 \text{ BTU/hr-ft-}^{\circ}\text{F}$ .

In constructing a finite element model, it is only necessary to consider one-half of the column cross-section ( $Y \leq 7 \text{ in.}$ ) since the column centerline at  $Y = 7 \text{ in.}$  is a plane of conduction symmetry.

Ninety-six 4-node planar elements containing 125 nodes are used to represent a one inch deep transverse section of the column, as shown in Fig. 7.4. Nodes lying in the  $Y = 7 \text{ in.}$  plane are taken to be insulated, and the element surfaces in the  $X = 0$ ,  $Y = 0$  and  $X = 36 \text{ in.}$  planes are exposed to convective surface heat transfer.

The program DOT was used to obtain two steady state temperature distributions, one along the column face ( $Y = 0$ ) and the other along the column centerline ( $Y = 7 \text{ in.}$ ). The results are compared in Fig. 7.5 with a Fourier analysis solution performed by Peavy [32]. It can be seen that the temperature distributions obtained using the DOT program closely straddle Peavy's solution, which predicted the mean temperature over the entire 14-in. width of the cross-section.

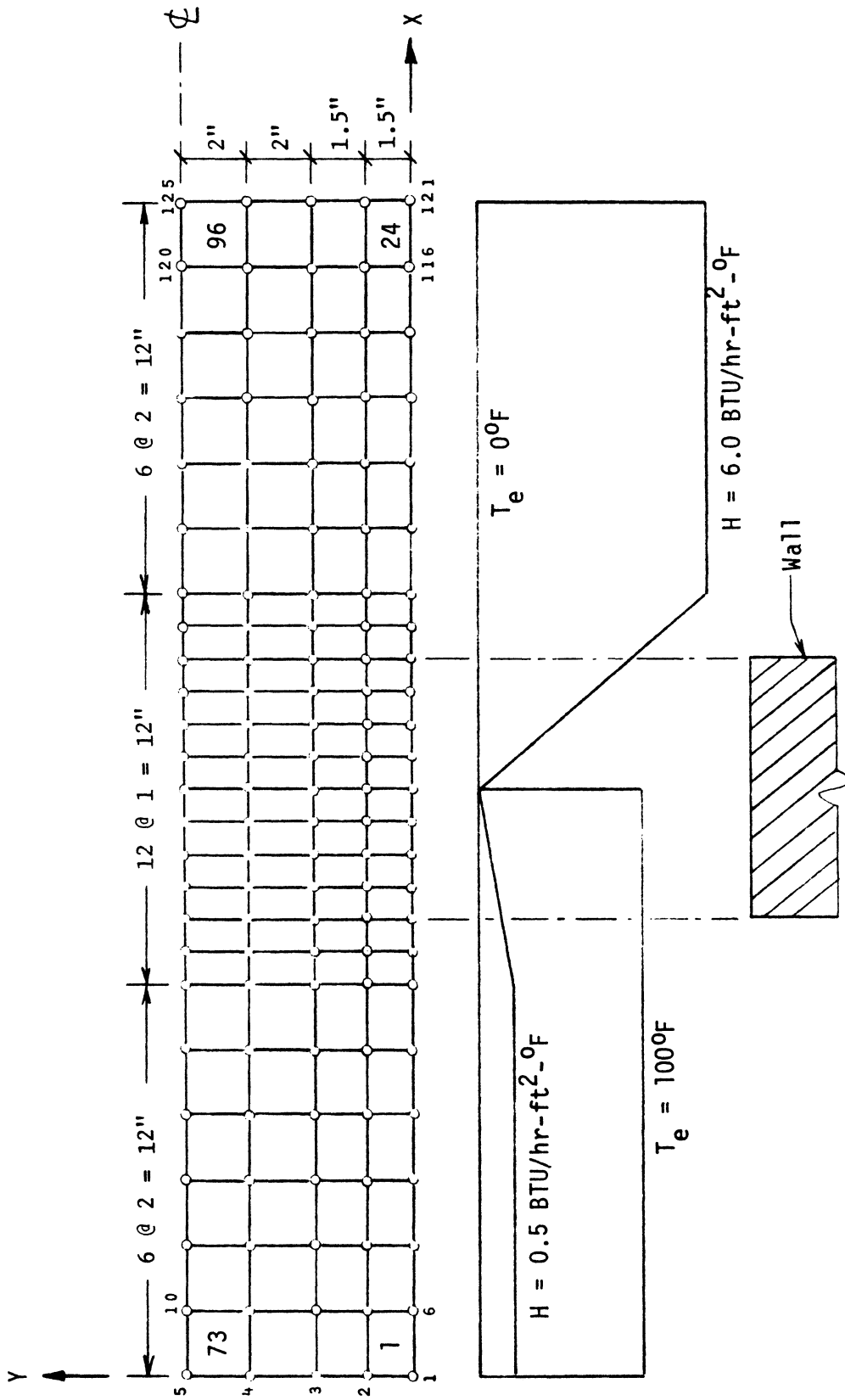


FIG. 7.4 FINITE ELEMENT MODEL OF THE 14 BY 36-IN. RECTANGULAR CONCRETE COLUMN

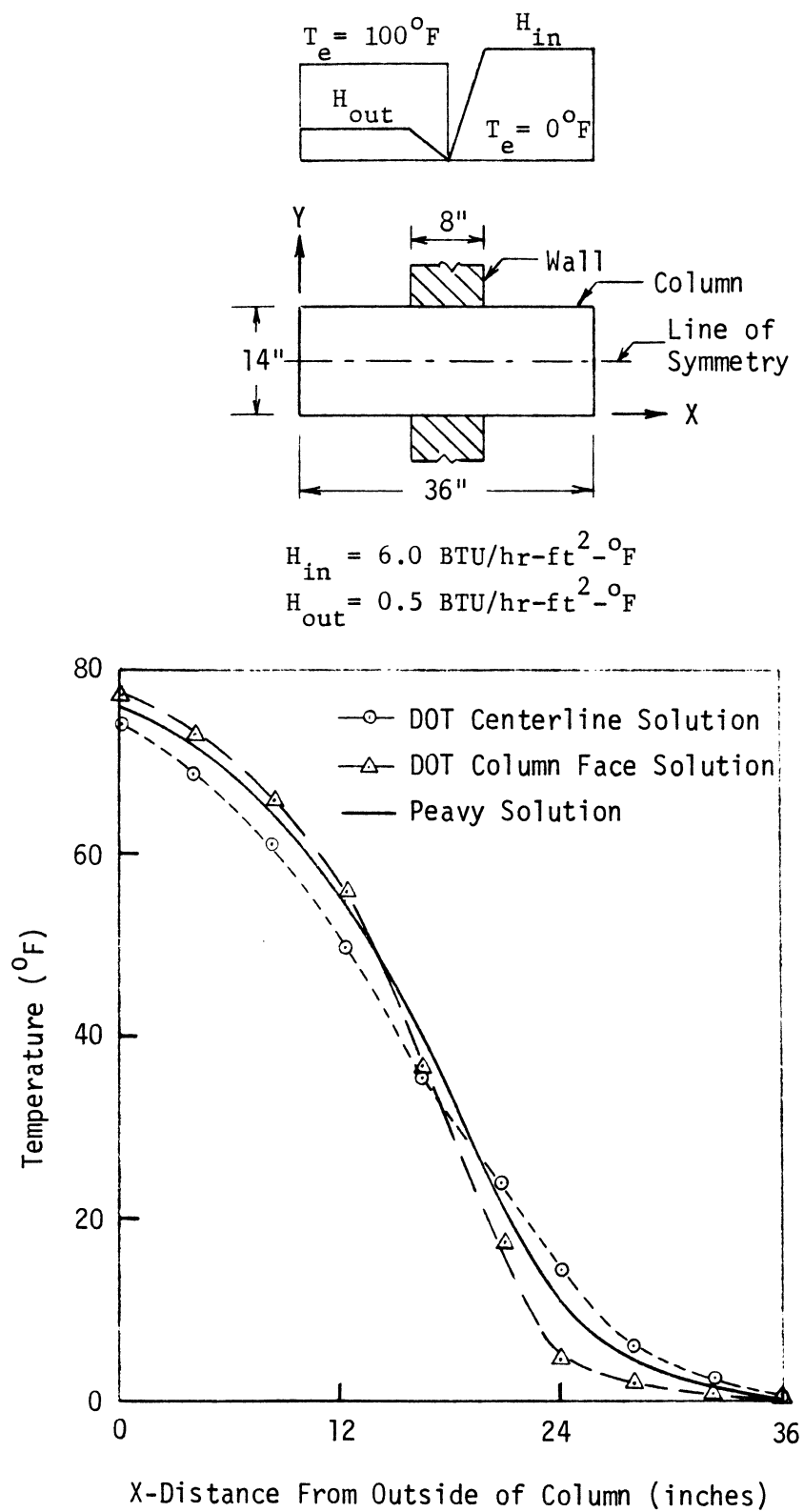


FIG. 7.5 TEMPERATURE DISTRIBUTIONS OVER THE 36-IN. WIDTH OF THE COLUMN



#### 7.4 INTERNAL HEAT GENERATION IN A PARALLEL-SIDED SLAB

An 8-inch thick slab, infinite in extent, is initially at  $0^{\circ}\text{F}$ . At time  $t = 0^+$ , heat is generated internally in the slab at a uniformly distributed rate  $\dot{q} = 2000 \text{ BTU/sec-in}^3$ . The external surfaces of the slab are maintained at  $0^{\circ}\text{F}$  for all time.

The material parameters chosen for this study are:

$$\text{Thermal Diffusivity } \kappa = 16 \text{ in}^2/\text{sec}$$

$$\text{Specific Heat } c = 1.0 \text{ BTU-in/sec}^2\text{-lb-}^{\circ}\text{F}$$

$$\text{Mass Density } \rho = 1.0 \text{ sec}^2\text{-lb/in}^4$$

which are equivalent to a thermal conductivity value of  $K$  equal to  $16.0 \text{ BTU/sec-in-}^{\circ}\text{F}$  ( $\kappa = K/\rho c$ ).

In developing a finite element model for the slab, the slab centerline is recognized as a plane of conduction symmetry. Ten equally spaced 4-node elements are used to represent a one square inch section through the 4-in. half-depth of the slab, as shown in Fig. 7.6(a). Nodes 21 and 22 at the surface ( $X = 4 \text{ in.}$ ) have a prescribed temperature boundary condition of  $0^{\circ}\text{F}$  and the nodes 1 and 2 at the slab mid-depth ( $X = 0$ ) are assumed to be insulated for all values of time.

The exact solution for the temperature at time  $t$  at any depth  $x$  within a slab subjected to internal heat generation is given by Carslaw and Jaeger [ 4 ] as:

$$T(x,t) = \frac{\dot{q}L^2}{2K} \left\{ 1 - \left(\frac{x}{L}\right)^2 - \frac{32}{\pi^3} \sum_{n=0}^{\infty} \frac{(-1)^n}{(2n+1)^3} \cos\left[\frac{(2n+1)\pi x}{2L}\right] e^{-\kappa \left[\frac{(2n+1)\pi}{2L}\right]^2 t} \right\}$$

where

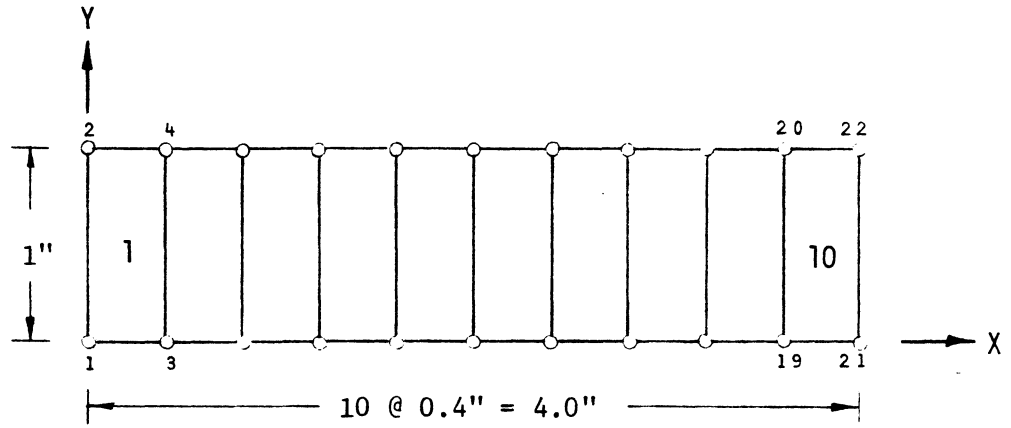
$\dot{q}$  = rate of internal heat generation (2000 BTU/sec-in<sup>3</sup>)

L = half-depth of slab (4.0 in.)

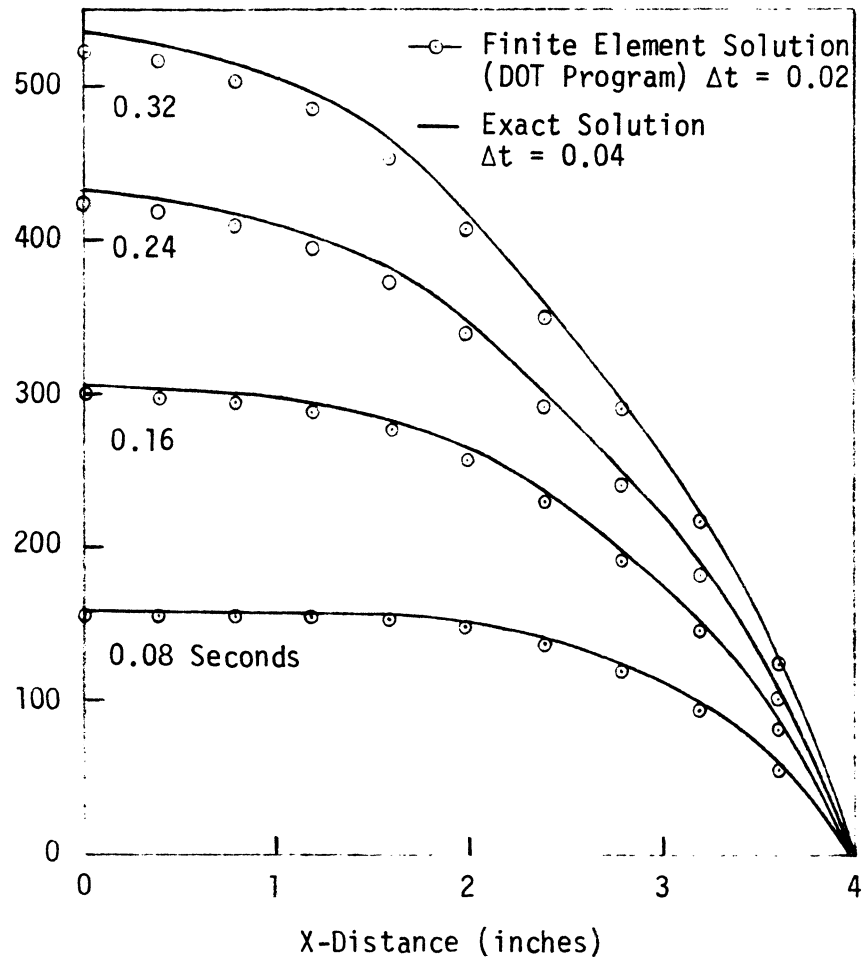
K = thermal conductivity (16.0 BTU/sec-in-<sup>0</sup>F)

$\kappa$  = thermal diffusivity (16.0 in<sup>2</sup>/sec)

Figure 7.6(b) shows the temperature profiles across the half-thickness of the slab. The four curves represent the series solution for the temperature distribution at times of 0.08, 0.16, 0.24 and 0.32 seconds and the plotted points are the nodal temperatures predicted by the DOT program for these respective times, using a solution time step  $\Delta t = 0.02$  seconds. It is noted that the finite element solution accurately predicts the temperatures resulting from internal heat generation in the slab.



(a) Finite Element Model



(b) Temperature Distribution

FIG. 7.6 INTERNAL HEAT GENERATION IN A PARALLEL-SIDED SLAB

7.5 TRANSIENT HEAT CONDUCTION IN A SEMI-INFINITE SOLID SUBJECTED TO A UNIT SURFACE HEAT FLUX

A semi-infinite solid initially at zero temperature is exposed to a constant surface heat flux of unit intensity at time  $t = 0^+$ , i.e.  $Q(0,t) = 1.0$ ,  $t > 0$ . The material properties are all assumed to be linear (temperature independent) and are assigned unit values:

$$\text{Conductivity } K = 1.0 \text{ BTU/sec-in-}^{\circ}\text{F}$$

$$\text{Specific Heat } c = 1.0 \text{ BTU-in/sec}^2\text{-lb-}^{\circ}\text{F}$$

$$\text{Mass Density } \rho = 1.0 \text{ sec}^2\text{-lb/in}^4$$

which are equivalent to a value of thermal diffusivity  $\kappa$  equal to  $1.0 \text{ in}^2/\text{sec}$  ( $\kappa = K/\rho c$ ).

Fifteen equally spaced 4-node planar elements are used in the analysis to represent a 3 inch depth of the solid, as shown in Fig. 7.7(a). The surface of the solid coincides with the global Y-Z plane. Nodes 31 and 32 on the interior plane ( $X = 3 \text{ in.}$ ) are assumed to be insulated and nodes 1 and 2 on the surface of the solid ( $X = 0$ ) are subjected to the unit value of heat flux. Temperatures were computed using the DOT program with two different time steps, namely  $\Delta t_1 = 0.025$  and  $\Delta t_2 = 0.05$  seconds.

The exact solution for the temperature at time  $t$  and at any depth  $x$  within the solid subjected to a unit surface heat flux is given by Carslaw and Jaeger [4] as:

$$T(x,t) = \frac{2}{K} \left\{ \left( \frac{\kappa t}{\pi} \right)^{1/2} e^{-x^2/4\kappa t} - \frac{x}{2} \text{erfc}(x/2\sqrt{\kappa t}) \right\}$$

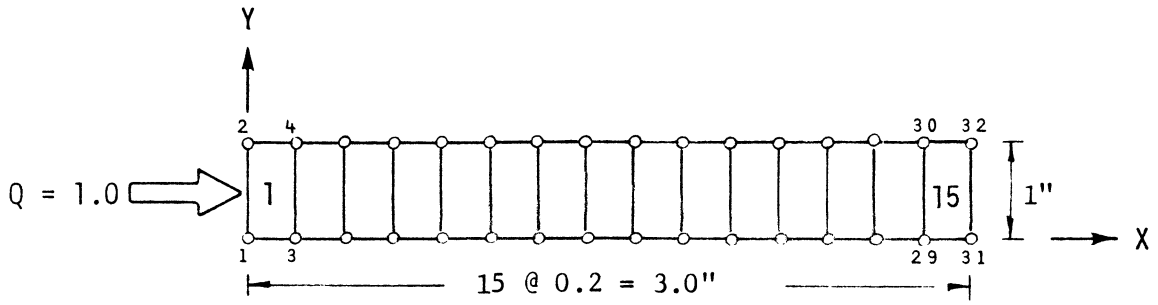
where

$K$  = thermal conductivity (1.0 BTU/sec-in- $^{\circ}$ F)

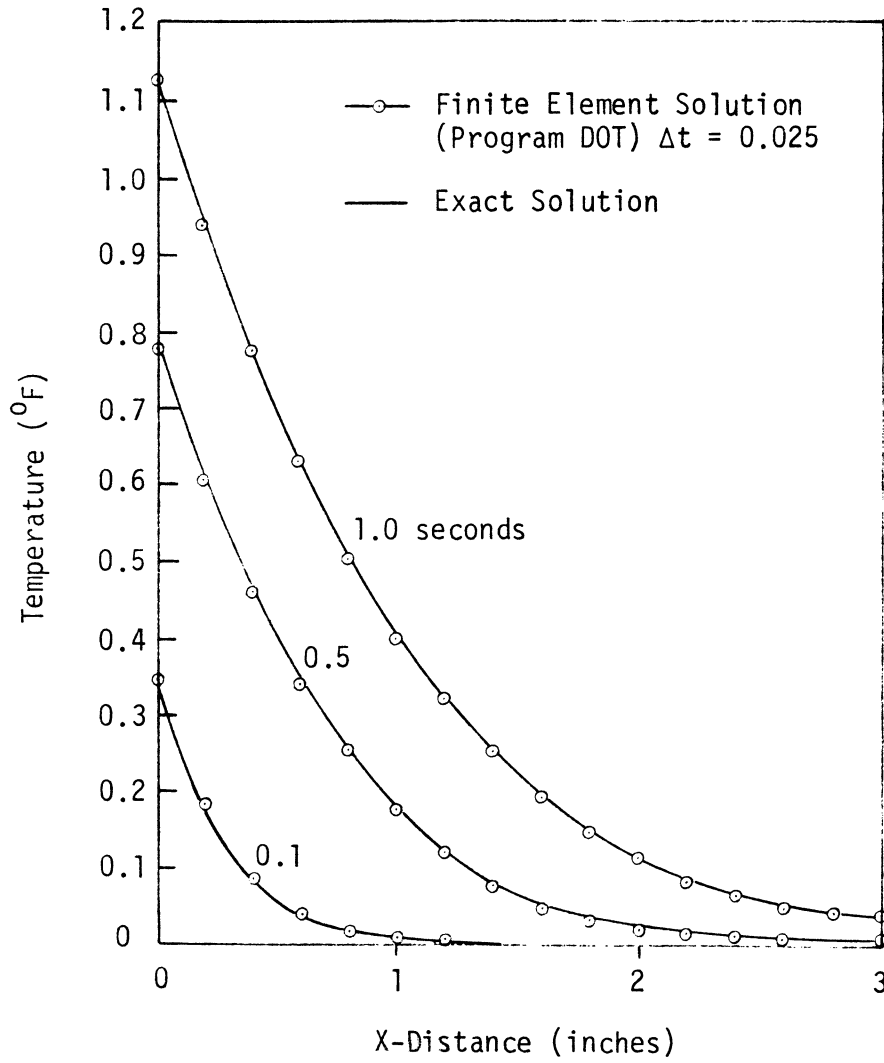
$\kappa$  = thermal diffusivity (1.0 in<sup>2</sup>/sec)

The temperature distributions into the depth of the solid are shown in Fig. 7.7(b) for time values of 0.1, 0.5 and 1.0 seconds. The solid curves represent the exact solution and the symbol points are the nodal temperatures obtained with the DOT program and the first solution time step  $\Delta t_1 = 0.025$  seconds. As can be seen, the agreement is very close.

Fig. 7.8 is a plot of the surface temperature of the solid versus time from the start of heating. The symbol points represent the finite element solution for the two different time steps. Both solutions are seen to accurately predict the temperature response of the solid.



(a) Finite Element Model



(b) Temperature Distribution

FIG. 7.7 SEMI-INFINITE SOLID SUBJECTED TO A UNIT SURFACE HEAT FLUX

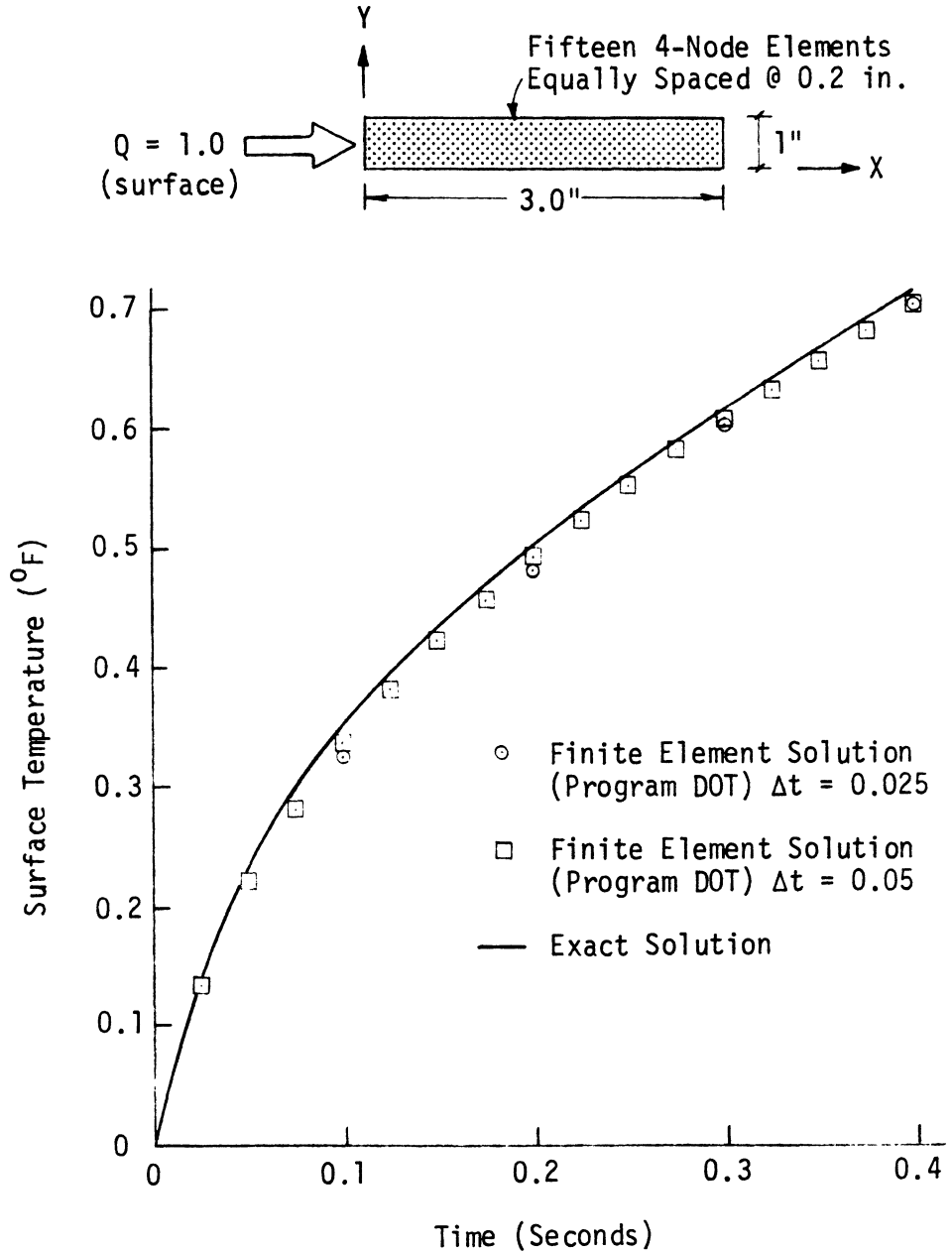


FIG. 7.8 SURFACE TEMPERATURE OF A SEMI-INFINITE SOLID VS. TIME FROM START OF HEATING

### 7.6 TRANSIENT HEAT CONDUCTION IN A FINITE LENGTH ROD

A 0.5-inch long rod with a cross-sectional area of one square inch has an initial temperature distribution which varies linearly with distance ( $x$ ) along its length:

$$T(x,0) = T_0(x/L)$$

where

$$T_0 = 100^\circ\text{F}$$

$$L = 0.5 \text{ inches}$$

At time  $t = 0^+$ , the end  $x = 0.0$  is maintained at  $0^\circ\text{F}$  and the end  $x = 0.5 \text{ in.}$  is insulated ( $Q = 0$ ).

The material parameters chosen for this study are:

$$\text{Conductivity } K = 6.0 \text{ BTU/sec-in-}^\circ\text{F}$$

$$\text{Specific Heat } c = 3.0 \text{ BTU-in/sec}^2\text{-lb-}^\circ\text{F}$$

$$\text{Mass Density } \rho = 2.0 \text{ sec}^2\text{-lb/in}^4$$

which are equivalent to a thermal diffusivity value  $\kappa$  equal to  $1.0 \text{ in}^2/\text{sec}$  ( $\kappa = K/\rho c$ ).

For the finite element model shown in Fig. 7.9(a), ten 4-node planar elements are used along the length of the rod. Nodes 1 and 2 are maintained at  $0^\circ\text{F}$  for all values of time and nodes 21 and 22 are insulated (zero external heat flow). Temperatures were obtained using the DOT program with a time step  $\Delta t = 0.001$  seconds.

The exact solution for the temperature at any distance  $x$  along the rod at time  $t$  is given by the series solution [33]:

$$T(x,t) = \frac{8T_0}{\pi^2} \sum \frac{(-1)^n}{(2n+1)^2} \sin\left[\frac{(2n+1)\pi x}{2L}\right] e^{-\kappa \left[\frac{(2n+1)\pi}{2L}\right]^2 t}$$



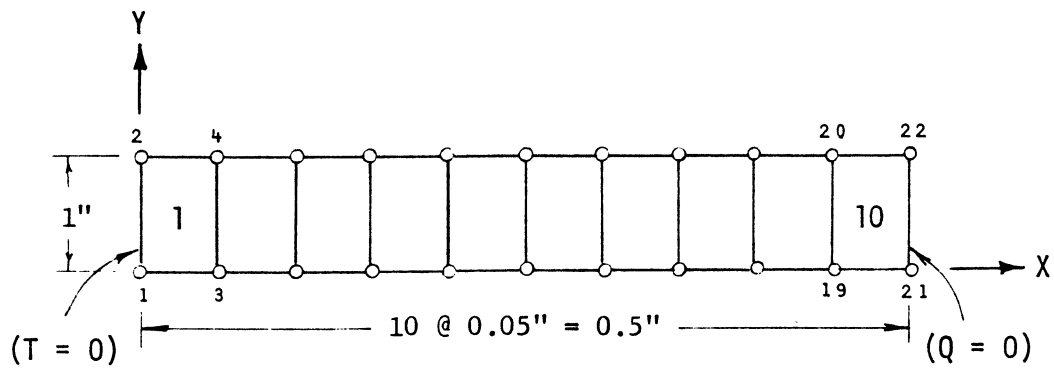
where

$T_0$  = temperature at end  $x = 0.0$  ( $100^{\circ}\text{F}$ )

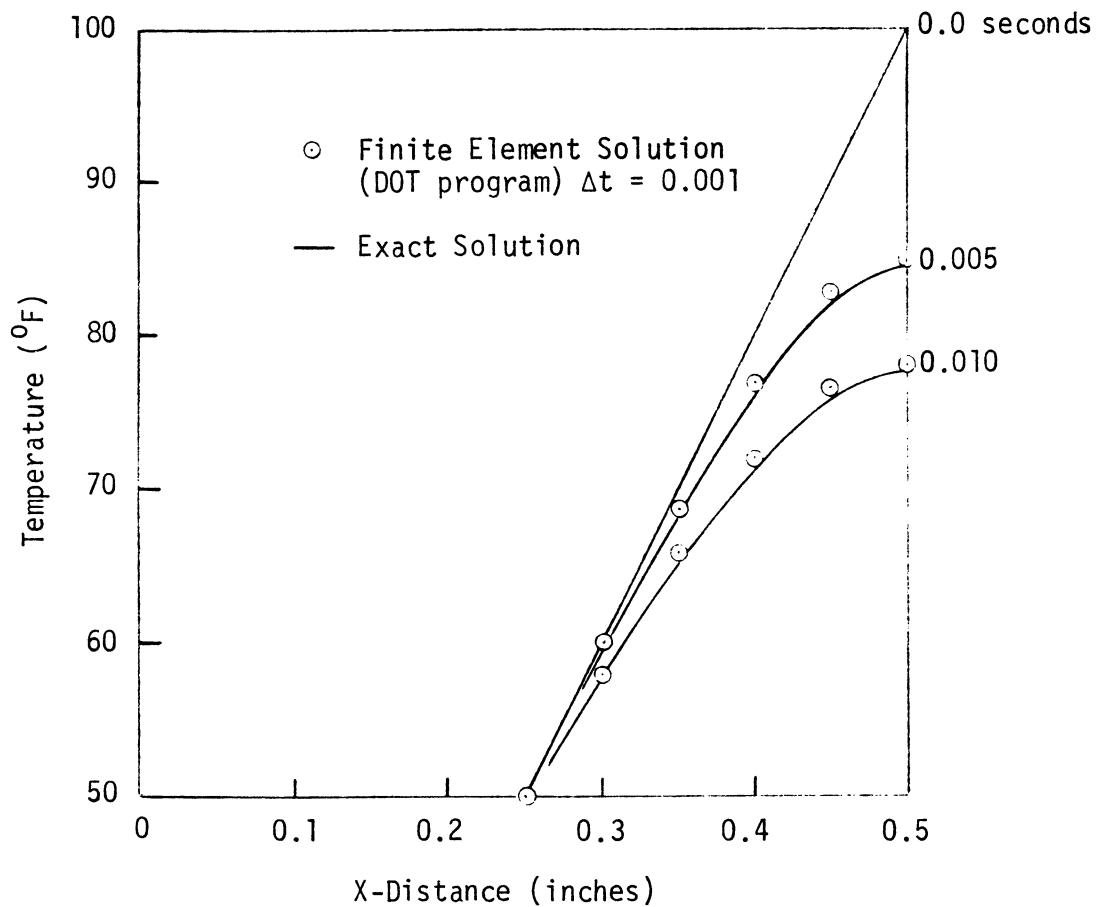
$L$  = length of rod (0.5 in.)

$\kappa$  = thermal diffusivity ( $1.0 \text{ in}^2/\text{sec}$ )

A comparison between the finite element and exact solution results is shown in Fig. 7.9(b). The solid curves represent the series solution for the temperature distribution along the rod at times of 0.005 and 0.010 seconds and the plotted points are the nodal temperatures predicted by the DOT program for these respective times. It can be seen that the numerical finite element results are in close agreement with the exact solution.



(a) Finite Element Model



(b) Temperature Distributions

FIG. 7.9 TRANSIENT HEAT CONDUCTION IN A FINITE LENGTH ROD

### 7.7 TRANSIENT HEAT CONDUCTION IN AN INFINITE PARALLEL-SIDED SLAB

A one-inch thick slab, infinite in extent, is initially at  $0^{\circ}\text{F}$ . At time  $t = 0^+$ , both faces of the slab are raised to  $100^{\circ}\text{F}$  and held constant for all time.

The material parameters chosen for the slab are:

$$\text{Conductivity } K = 6.0 \text{ BTU/sec-in-}^{\circ}\text{F}$$

$$\text{Specific Heat } c = 2.0 \text{ BTU-in/sec}^2\text{-lb-}^{\circ}\text{F}$$

$$\text{Mass Density } \rho = 3.0 \text{ sec}^2\text{-lb/in}^4$$

For the finite element model, ten equally spaced 4-node planar elements are used to represent a one square inch section through the 0.5-in. half-depth of the slab as shown in Fig. 7.10(a). Nodes 1 and 2 on the surface of the slab are maintained at  $100^{\circ}\text{F}$  for time  $t > 0$  and nodes 21 and 22 at the slab mid-depth lie in a plane of conduction symmetry and are treated as insulated nodes.

Figure 7.10(b) compares the temperature distributions across the half-thickness of the slab at times of 0.025, 0.050 and 0.075 seconds. The finite element solution was obtained using the program DOT with a time step  $\Delta t = 0.0025$  seconds. The finite difference solution points are from Carnahan, Luther and Wilkes [34], and the exact solution is an infinite series expansion given by Olson and Schultz [35]. All three solutions are seen to provide very close agreement in predicting the temperatures through the slab.

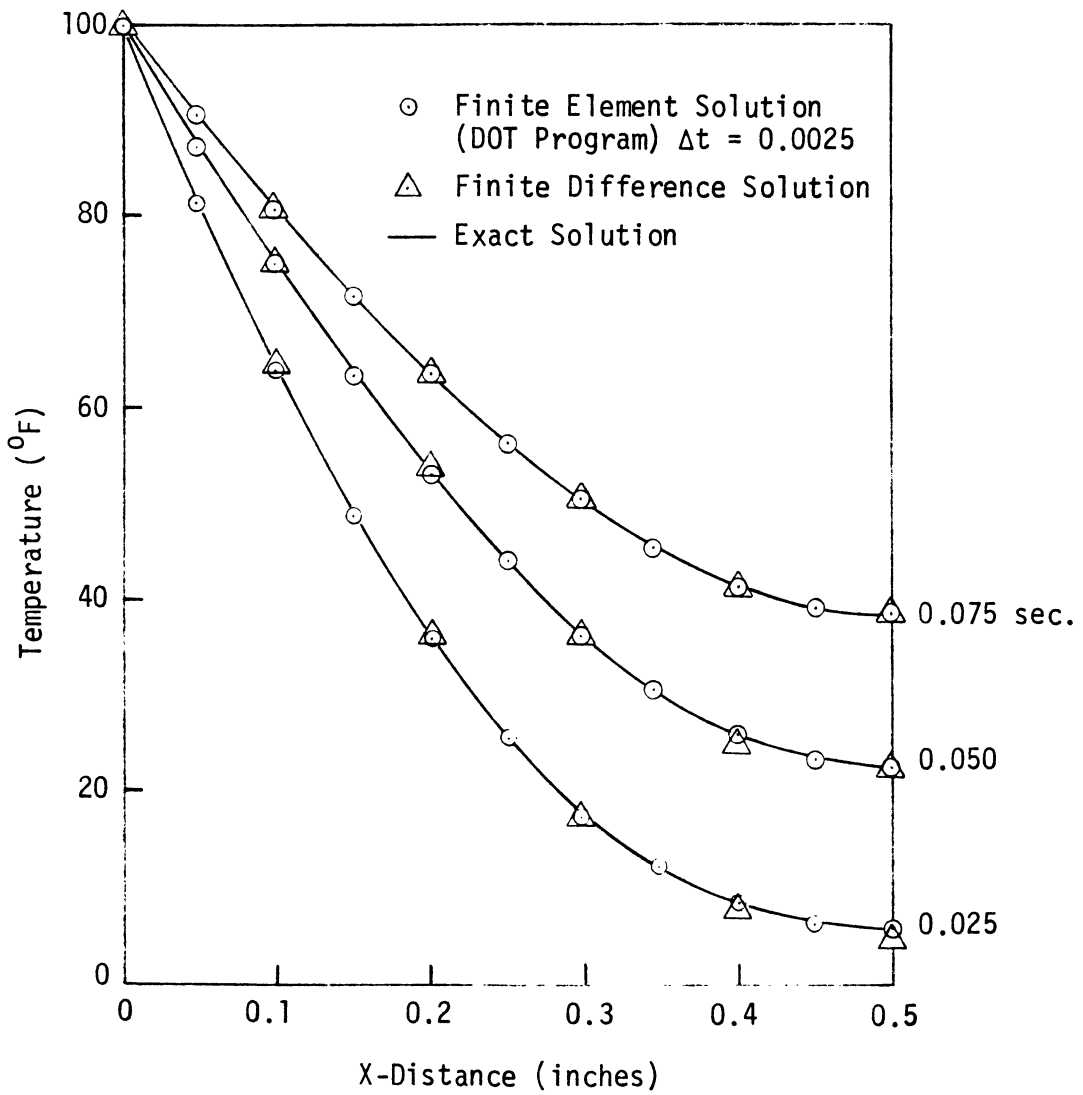
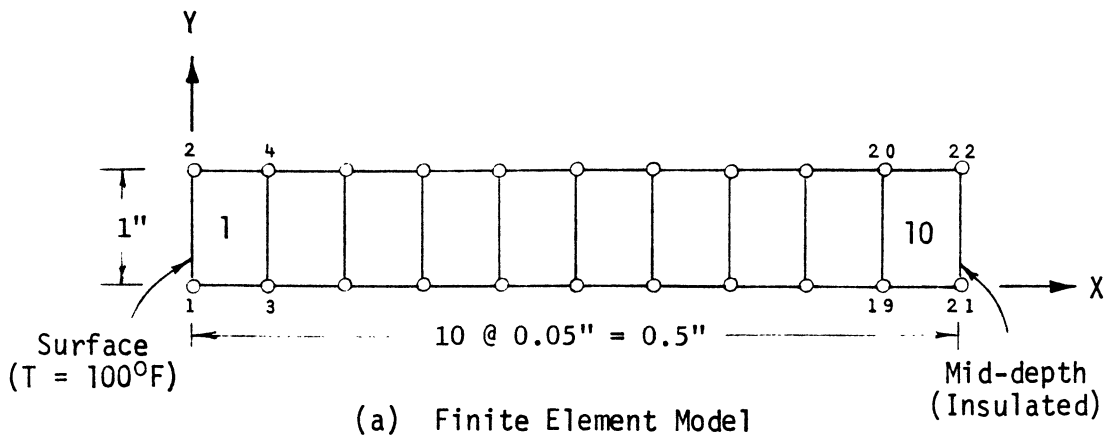


FIG. 7.10 TRANSIENT HEAT CONDUCTION IN A PARALLEL-SIDED SLAB

## 7.8 NONLINEAR TRANSIENT HEAT CONDUCTION THROUGH AN INFINITE PARALLEL-SIDED SLAB

A 20-inch thick slab, infinite in extent, is initially at a reference temperature of 100<sup>0</sup>F as shown in Fig. 7.11. At time  $t = 0^+$ , the temperature on the left face of the slab ( $X = 0$ ) is raised to 200<sup>0</sup>F and maintained at this level until time  $t = 10$  seconds when it drops back to 100<sup>0</sup>F. The thermal conductivity  $K$  is assumed to vary linearly with temperature and the specific heat  $c$  is taken to be constant. The material parameters chosen for this study are:

$$\text{Conductivity } K = 2 + (0.01)T \text{ BTU/sec-in-}^{\circ}\text{F}$$

$$\text{Specific Heat } c = 8 \text{ BTU-in/sec}^2\text{-lb-}^{\circ}\text{F}$$

$$\text{Mass Density } \rho = 0.25 \text{ sec}^2\text{-lb/in}^4$$

For the finite element model, twenty equally spaced 4-node planar elements are used to represent a one square inch section through the 20-in. thickness of the slab. The transient temperature distributions were obtained using the program DOT with a time step  $\Delta t = 1$  second and reforming the system equations every time step.

This same problem was also solved numerically by Aguirre-Ramirez and Oden [16] and by Wilson, Bathe and Peterson [24]. Wilson et al. used an algorithm involving heat flow equilibrium iteration and performed three analyses in which new conductivity matrices were formed and triangularized (1) in each time step, (2) every 5<sup>th</sup> time step and (3) only once at the start of solution when  $T = 100^{\circ}\text{F}$ . The temperatures calculated in these three analyses were found to be the same within 5 digits of accuracy, and the

average number of iterations required in the analyses were 2, 3 and 5 respectively.

Table 7.1 compares the results obtained from the DOT analysis with those obtained by Wilson et al. for the temperature at a distance  $x$  from the left face of the slab at times  $t = 10$  and  $11$  seconds. The two solutions are seen to be in close agreement. Additionally, both sets of results in Table 7.1 compare favorably with the predicted temperature variation given in a small figure in Ref. [16].

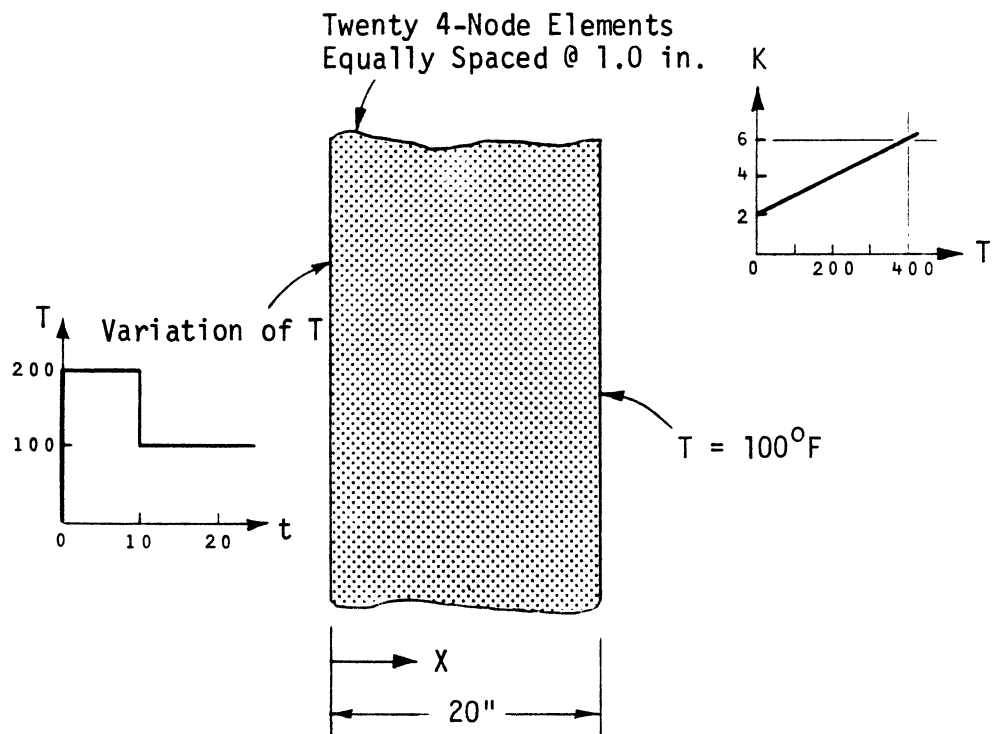


FIG. 7.11 NONLINEAR TRANSIENT HEAT CONDUCTION THROUGH  
AN INFINITE PARALLEL-SIDED SLAB

TABLE 7.1: TEMPERATURES AT A DISTANCE X FROM THE LEFT FACE OF THE SLAB AT TIMES  $t = 10$  AND  $t = 11$  SECONDS

Distance x	T @ t = 10		T @ t = 11	
	DOT Solution	Wilson Solution	DOT Solution	Wilson Solution
0	200.00	200.00	100.00	100.00
1	187.23	187.35	137.80	141.52
2	174.41	174.68	150.89	153.46
3	161.95	162.38	151.65	153.19
4	150.27	150.83	146.67	147.68
5	139.71	140.38	139.42	140.23
6	130.55	131.26	131.80	132.52
7	122.90	123.59	124.74	125.41

Note: All temperature values are in  $^{\circ}\text{F}$



## 7.9 TRANSIENT TEMPERATURE ANALYSIS OF A MASS CONCRETE STRUCTURE CONSTRUCTED INCREMENTALLY

This example was selected to illustrate the capability of the finite element program DETECT to predict the temperature distribution in a mass concrete structure constructed incrementally. The structure chosen for this study is the Norfolk dam, a concrete gravity dam [36]. The basic geometry of the section of dam analyzed is shown in Fig. 7.12. The finite element representation of the dam cross-section is shown in Fig. 7.13. This model includes a 40-ft. portion of the foundation rock, and the element boundaries in the concrete mass coincide with the theoretical lift placement boundaries used in this study.

The concrete temperature in the dam will increase rapidly above the placement temperature due to the heat given off by the hydrating cement. The degree of temperature rise will depend on the type of cement used, the quantity of cement in the mixture, the diffusivity of the aggregate used and the construction scheme. Most dams are typically constructed in 5 to 7-1/2 ft. high lifts placed at 5 to 7 days apart, but for the purposes of this example, the dam is idealized as being constructed in twelve 20-ft. high lifts placed at 30 day intervals, for a total construction time of 360 days. The placement temperature of the concrete was taken to be 45<sup>0</sup>F.

The hypothetical rate of internal heat generation for the Norfolk dam concrete shown in Fig. 7.14 was taken from the adiabatic temperature rise data determined for the Oroville dam mass concrete mix no. 3-B(II) containing 4 sacks of cement per cubic yard [37].

The boundary conditions assumed in the analysis are as follows:

- (1) At any level of construction, all existing concrete surfaces are exposed to linear, free convection. The convection coefficient selected was  $140 \text{ BTU/hr-ft}^2\text{-}^\circ\text{F}$  and the hypothetical 360-day air temperature cycle used in the analysis is shown in Fig. 7.15.
- (2) The base of the foundation rock, nodes 1 to 13 in Fig. 7.13, is insulated and maintained as a temperature boundary condition of  $55^\circ\text{F}$  for all time.

The material properties for the concrete and foundation rock were taken to be the same, and the following values were selected for this analysis:

$$\text{Conductivity } K = 1.2 \text{ BTU/hr-ft-}^\circ\text{F}$$

$$\text{Specific Heat } c = 0.22 \text{ BTU/lb-}^\circ\text{F}$$

$$\text{Mass Density } \rho = 155 \text{ lb/ft}^3$$

Fig. 7.16 is a plot of isothermal contours in the dam at the completion of construction ( $t = 360$  days). A similar set of contours is plotted in Fig. 7.17 showing the temperature distribution in the dam one year after the end of construction ( $t = 720$  days). The temperatures in the central core of the dam are observed to be significant ( $>100^\circ\text{F}$ ) at the end of construction (Fig. 7.16) and can be seen to have decreased in magnitude one year later (Fig. 7.17).

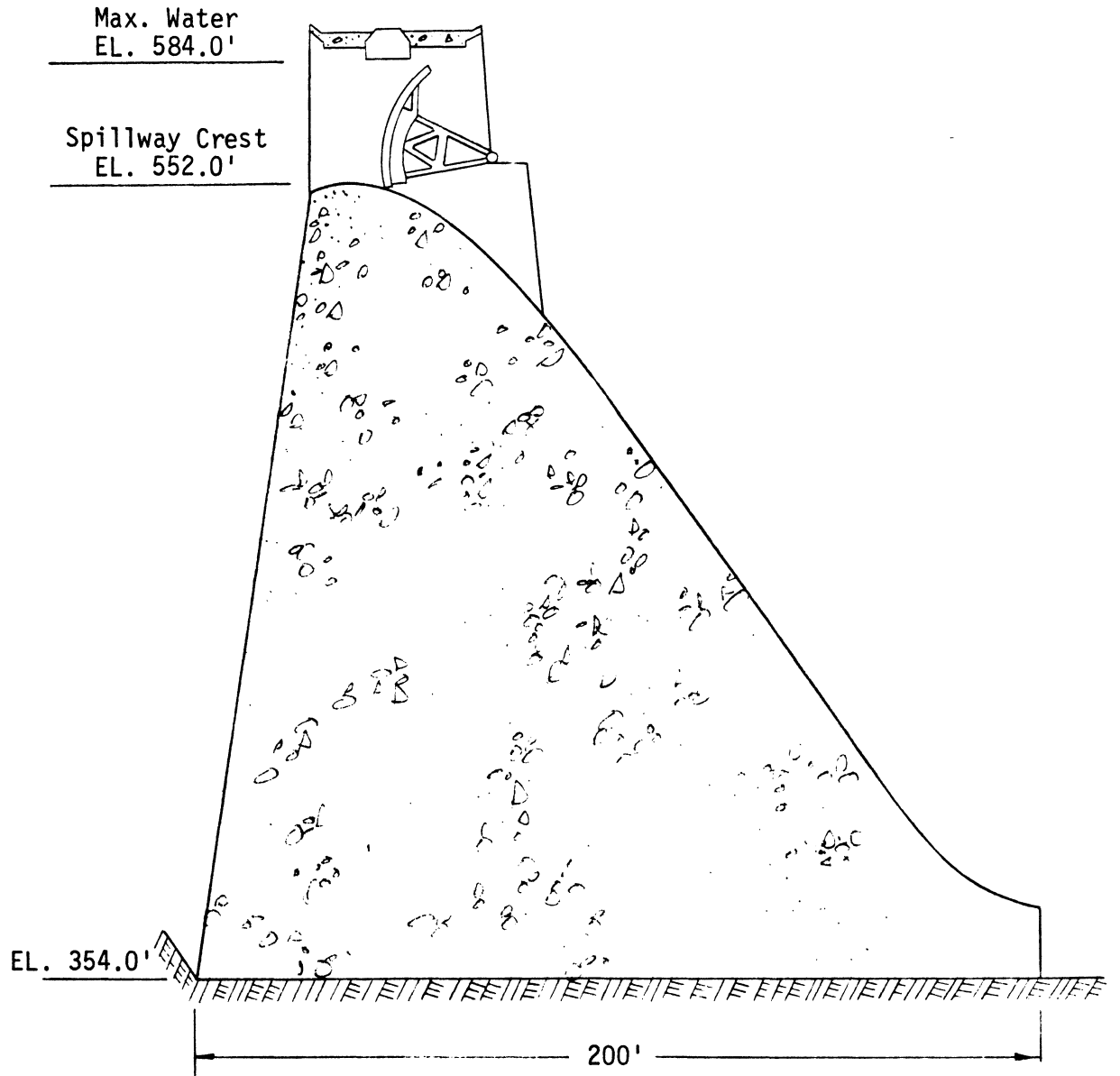


FIG. 7.12 CROSS SECTION OF NORFORK DAM

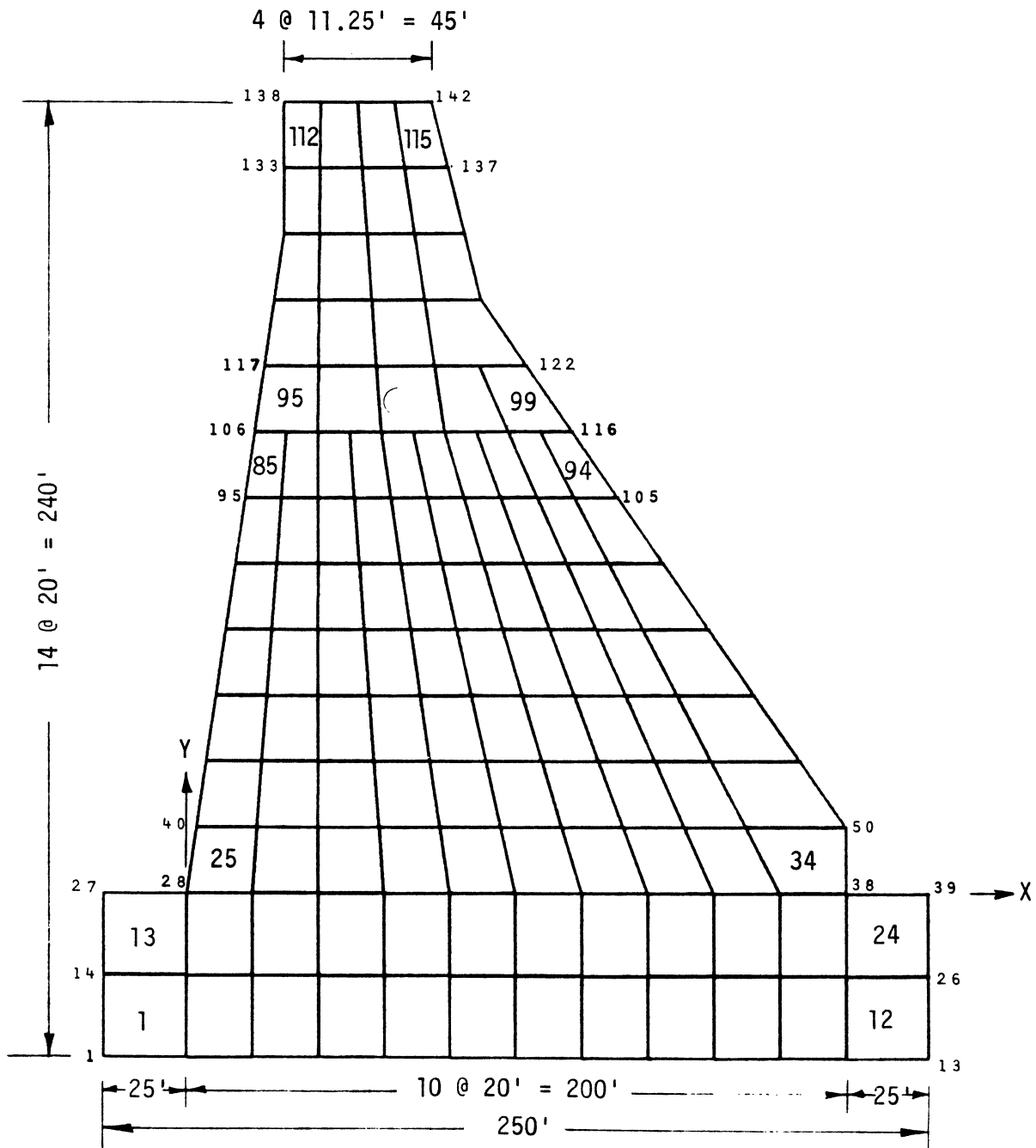


FIG. 7.13 FINITE ELEMENT MESH OF NORFORK DAM

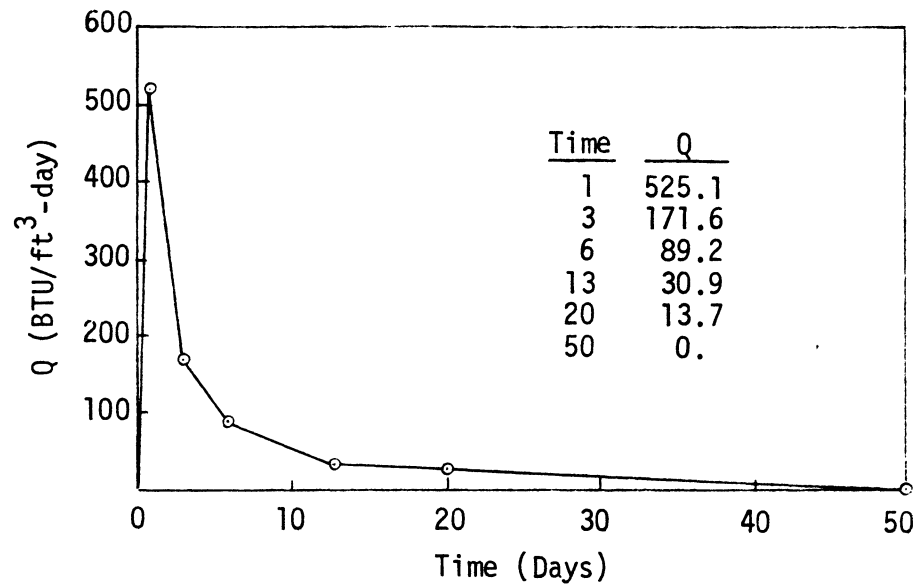


FIG. 7.14 HYPOTHETICAL RATE OF INTERNAL HEAT GENERATION FOR THE NORFORK DAM CONCRETE

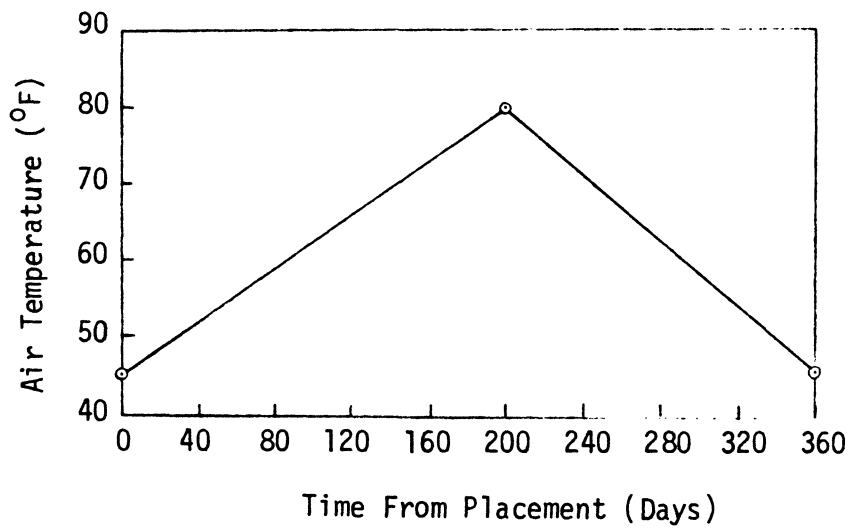


FIG. 7.15 360-DAY HYPOTHETICAL AIR TEMPERATURE CYCLE FOR NORFORK DAM

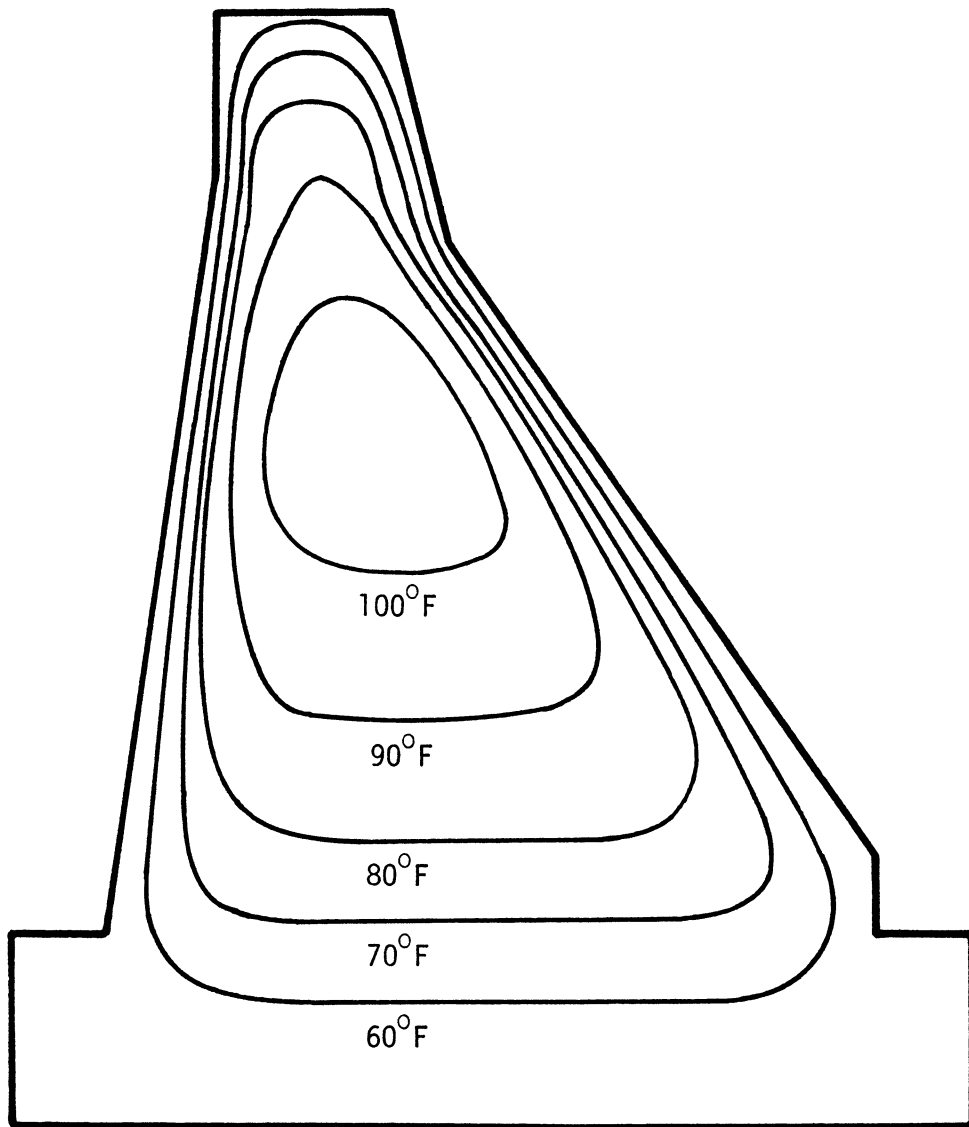


FIG. 7.16 TEMPERATURE CONTOURS IN DAM AT THE  
END OF CONSTRUCTION (360 DAYS)

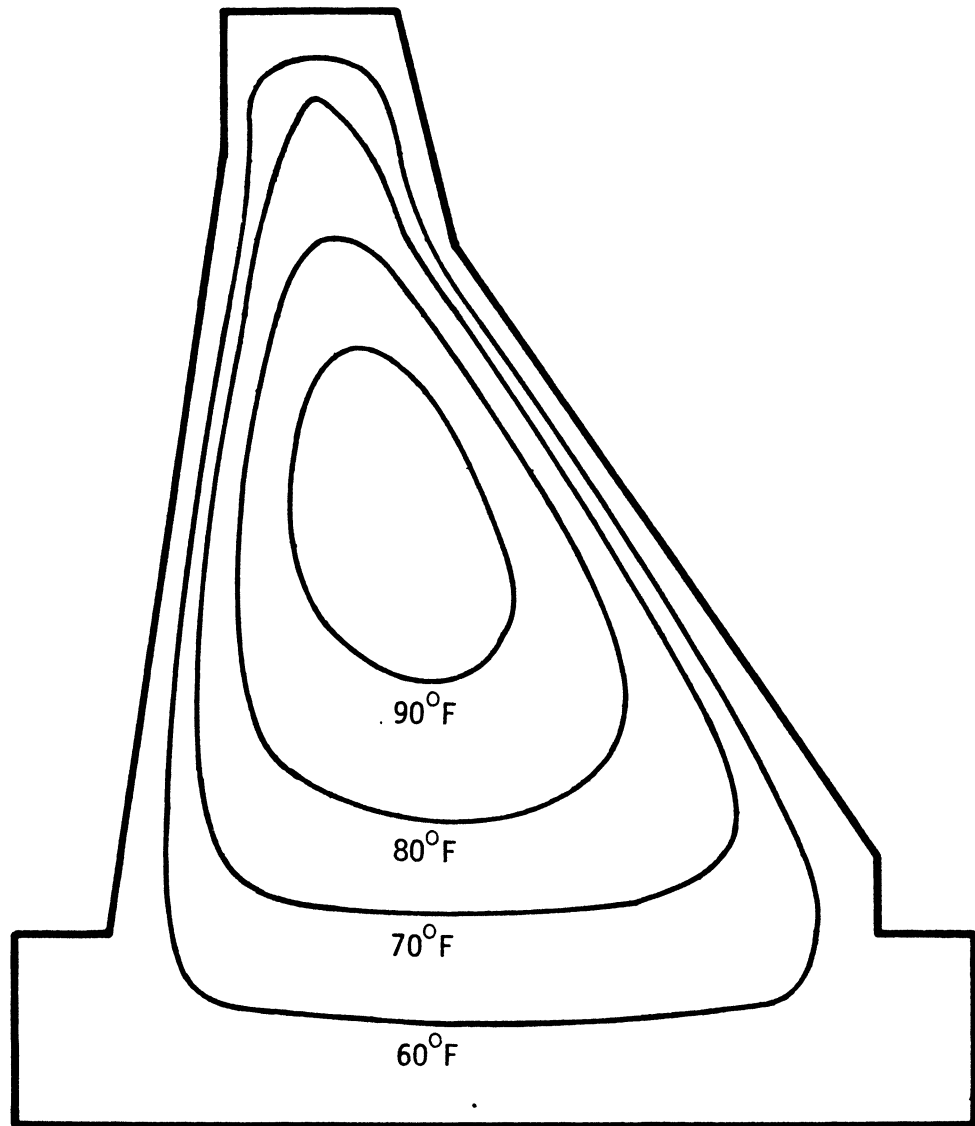


FIG. 7.17 TEMPERATURE CONTOURS IN DAM ONE YEAR  
FROM THE END OF CONSTRUCTION (720 DAYS)

### 7.10 NONLINEAR HEAT CONDUCTION IN A SQUARE CONCRETE COLUMN UNIFORMLY EXPOSED TO ASTM FIRE

A 20 x 20-in. plain concrete column, shown in Fig. 7.18(a), is at an initial room temperature of 68°F. At time  $t = 0^+$ , the column is exposed to a long duration moderately intense fire as defined by ASTM Standard E-119 [38]. The temperature variation of this pseudo-fire with time is given in Table 7.2.

The fire boundary condition on the external column surface is treated as a combination of a linear convection and a nonlinear radiation boundary condition. The convection coefficient (H) chosen for this study is 0.27 BTU/hr-ft<sup>2</sup>-°F, the view factor (V) is 1.0, the concrete surface emissivity ( $\epsilon_s$ ) is 0.9 and the fire emissivity ( $\epsilon_f$ ) is 0.6.

The thermal conductivity K is assumed to vary with temperature and the specific heat c is taken to be constant. The material properties chosen for this study are those given by Bizri [39]:

(a) Conductivity

$$68^{\circ}\text{F} < T < 390^{\circ}\text{F} \quad K = 1.01 \text{ BTU/hr-ft-}^{\circ}\text{F}$$

$$390^{\circ}\text{F} < T < 1650^{\circ}\text{F} \quad K = [1.01 - 0.0004(T-390)] \\ \text{BTU/hr-ft-}^{\circ}\text{F}$$

$$1650^{\circ}\text{F} < T \quad K = 0.506 \text{ BTU/hr-ft-}^{\circ}\text{F}$$

(b) Specific Heat  $c = 0.272 \text{ BTU/lb-}^{\circ}\text{F}$

(c) Density  $\rho = 150 \text{ lb/ft}^3$

In developing a finite element model, it is only necessary to consider one quadrant of the column in the analysis because the column is symmetrical and is exposed uniformly on all sides to the fire. The finite element mesh used for the column quadrant is shown



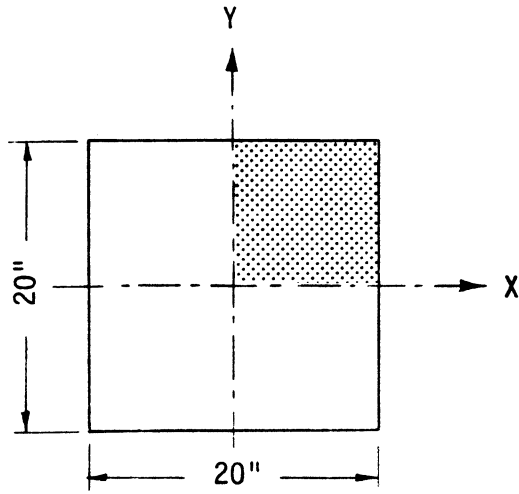
in Fig. 7.18(b). The planes of conduction symmetry are modeled as insulated surfaces ( $Q = 0$ ). Because a steep temperature gradient is expected to exist near the column surface, a finer mesh size is used in this region.

The transient temperature distributions in the column were calculated using the program DOT with a time step of 0.025 hours and reforming the system equations every 4<sup>th</sup> time step. The same problem was also solved using the finite element program FIRES-T, which uses an algorithm involving heat flow equilibrium iteration [40].

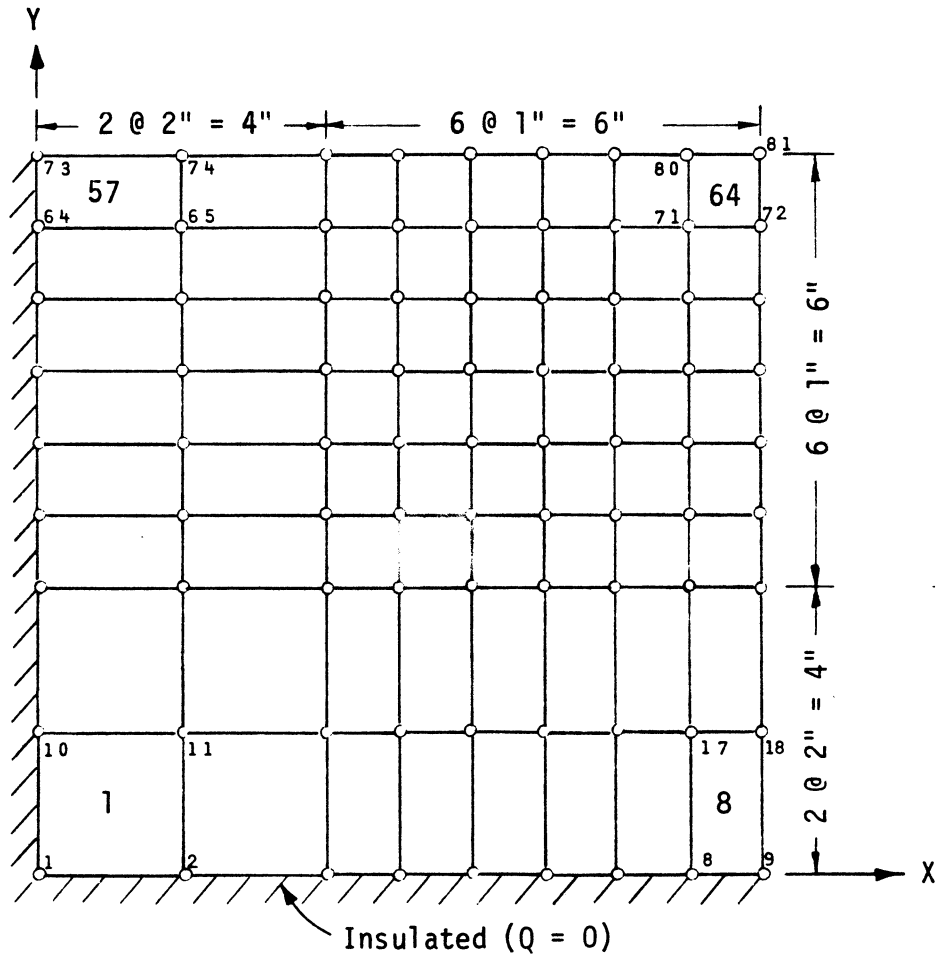
Figure 7.19 compares the predicted temperature histories obtained from the DOT and FIRES-T analyses for certain reference elements: the corner element (64), the midside element (8) and the center element (1). The results of the two analyses are seen to be in close agreement for elements 1 and 8, but differ slightly for the corner element 64. The reason for this discrepancy between the two analyses for element 64 is not altogether clear. The major portion of the difference occurred in the corner node 81 (Fig. 7.18(b)) with nodes 71, 72 and 80 being much closer in agreement. Part of the difference may be due to the type of element used on the respective programs; DOT uses a variable 4- to 8-node isoparametric element with 2x2 Gauss point integration, whereas FIRES-T uses a quadrilateral element constructed from four linear triangles with static condensation of the central node assuming that no external heat flow occurs at that point. Additionally, the linear convection boundary condition is solved exactly in the DOT program by making modifications to both the appropriate conductivity matrix terms and heat flux vector terms whereas FIRES-T uses an approximate solution technique where the heat flux vector alone is modified.

TABLE 7.2: ASTM STANDARD E-119 FIRE CURVE DATA FOR  
A LONG DURATION MODERATELY INTENSE FIRE

Time, min.	Temperature, °F
0	68
5	1000
10	1300
15	1399
20	1462
25	1510
30	1550
35	1584
40	1613
45	1638
50	1661
55	1681
60	1700



(a) Column Cross-Section



(b) Finite Element Mesh of Column Quadrant

FIG. 7.18 NONLINEAR HEAT CONDUCTION IN A SQUARE COLUMN UNIFORMLY EXPOSED TO ASTM FIRE

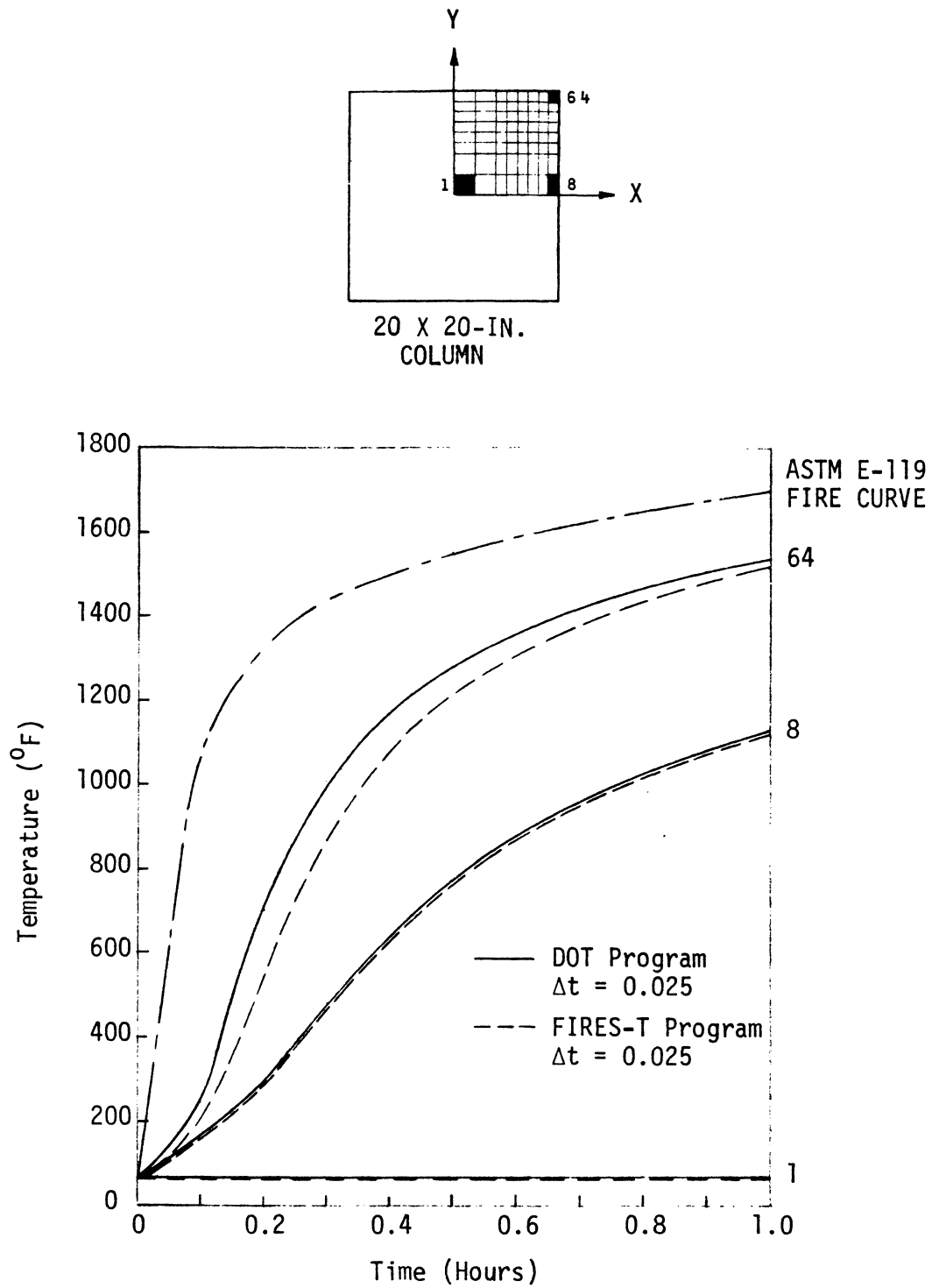


FIG. 7.19 COMPARISON OF PREDICTED ELEMENT TEMPERATURE HISTORIES FOR A SQUARE COLUMN UNIFORMLY EXPOSED TO ASTM E-119 FIRE

## 8. SUMMARY AND CONCLUSIONS

A finite element analysis technique for the solution of nonlinear transient heat conduction problems has been presented. Based on this theory, two finite element heat transfer programs have been developed. The program DOT ("Determination Of Temperatures") is capable of solving both linear and nonlinear heat transfer problems. Nonlinearities may be due to temperature-dependent material properties and, in particular, may be caused by nonlinear radiation boundary conditions. The program DETECT ("DEtermination of Temperatures in Construction") is a linear heat transfer analysis program developed with particular reference to mass concrete structures of arbitrary geometry constructed incrementally. Both programs can handle time-dependent boundary conditions and internal heat generation. A description of the required input data for the DOT and DETECT programs along with the Fortran IV listings is given in the Appendices of this dissertation.

A step-by-step solution technique has been described which is unconditionally stable for linear conduction problems and provides an efficient numerical solution of the heat flow equilibrium equations. The sample analyses presented in Section 7 show some applications of the method to different types of steady state and transient conduction problems and illustrate the major features of the programs.

For the solution of nonlinear heat transfer problems, it should be noted that the computational algorithm contained in the program DOT does not include an iterative scheme for heat flow equilibrium. Instead, a step-by-step solution procedure is used similar to the one outlined in Table 5.1 in which the effective thermal conductivity matrix  $\underline{K}^*$  is reformed after every  $n$  user-specified time steps. For a particular time interval  $\{t, t+\Delta t\}$ , the nodal temperatures are estimated at the midpoint of this time step as  $T_t + \frac{1}{2}(T_t - T_{t-\Delta t})$ . Temperature-dependent thermal properties are then computed based on this estimated midpoint temperature and the effective conductivity matrix  $\underline{K}^*$  is updated. Because the thermal properties of most engineering materials vary gradually with temperature, this approximate procedure for treating the material nonlinearities was judged to be sufficiently accurate for a large class of problems and an iterative heat flow equilibrium scheme was not deemed necessary.

The capabilities of the DOT and DETECT programs may be expanded by including new finite element groups such as one dimensional beam elements and three dimensional isoparametric solid elements. Because the programs have been developed in a modular fashion, these new element groups can be added by developing a few new subroutines with only minor changes to the existing programs.

## REFERENCES

1. Zienkiewicz, O. C. and Cheung, Y. K., "Finite Elements in the Solution of Field Problems," *The Engineer*, September 24, 1964.
2. Wilson, E. L., "A Digital Computer Program for the Steady-State Temperature Analysis of Plane or Axisymmetric Bodies," Aerojet-General Corporation, Sacramento, California, Report No. TD-44, March 1965.
3. Wilson, E. L. and Nickell, R. E., "Application of the Finite Element Method to Heat Conduction Analysis," *Nuclear Engineering and Design (Holland)*, Vol. 4, pp. 276-286, October 1966.
4. Carslaw, H. S. and Jaeger, J. C., "Conduction of Heat in Solids," 2nd ed., Oxford University Press, 1969.
5. Loretan, P. A., "Laplace Variational Method for Transient Multidimensional Temperature Distributions," *Nuclear Engineering and Design*, No. 11, pp. 27-40, 1970.
6. Goodman, T., "Application of Integral Methods to Transient Nonlinear Heat Transfer," Vol. 1, Academic Press, New York, pp. 51-122, 1964.
7. Trent, D. S. and Welty, J. R., "A Summary of Numerical Methods for Solving Transient Heat Conduction Problems," *Bulletin No. 49, Engineering Experiment Station, Oregon State University, Corvallis*, October 1974.
8. Ergatoudis, I., Irons, B. M. and Zienkiewicz, O. C., "Curved Isoparametric Quadrilateral Elements for Finite Element Analysis," *International Journal of Solids and Structures*, Vol. 4, pp. 31-42, 1968.
9. Biot, M. A., "Thermo-Elasticity and Irreversible Thermodynamics," *J. Appl. Phys.*, Vol. 27, No. 3, pp. 240-253, March 1956.
10. Biot, M. A., "New Methods in Heat Flow Analysis with Applications to Flight Structures," *Journal of the Aeronautical Sciences*, Vol. 24, No. 12, pp. 857-873, December 1957.
11. Biot, M. A., "Further Developments of New Methods in Heat-Flow Analysis," *Journal of the Aero/Space Sciences*, Vol. 26, No. 6, pp. 367-381, June 1959.
12. Lardner, T. J., "Biot's Variational Principle in Heat Conduction," *AIAA Journal*, Vol. 1, No. 1, pp. 196-206, January 1963.
13. Gurtin, M. E., "Variational Principles for Linear Initial-Value Problems," *Quarterly of Applied Mechanics*, Vol. 22, No. 3, pp. 252-256, 1964.

## REFERENCES (CON'T)

14. Gallagher, R. H. and Mallet, R., "Efficient Solution Processes for Finite Element Analysis of Transient Heat Conduction," ASME Paper No. 69-WA/HT-32, November 1969.
15. Rybicki, E. F. and Hopper, A. T., "Higher Order Finite Element Method for Transient Temperature Analysis of Inhomogenous Materials," ASME Paper No. 69-WA/HT-33, November 1969.
16. Aguirre-Ramirez, G. and Oden, J. T., "Finite-Element Technique Applied to Heat Conduction in Solids with Temperature Dependent Thermal Conductivity," ASME Paper No. 69-WA/HT-34, November 1969.
17. Richardson, P. D. and Shum, Y. M., "Use of Finite Element Methods in Solution of Transient Heat Conduction Problems," ASME Paper No. 69-WA/HT-36, November 1969.
18. Brocci, R. A., "Analysis of Axisymmetric Linear Heat Conduction Problems by Finite Element Method," ASME Paper No. 69-WA/HT-37, November 1969.
19. Emery, A. F. and Carson, W. W., "An Evaluation of the Use of the Finite Element Method in the Computation of Temperature," ASME Paper No. 69-WA/HT-37, November 1969.
20. Taylor, R. L., "\*HEAT\*, A Finite Element Computer Program for Heat Conduction Analysis" (Unpublished), University of California, Berkeley, May 1975.
21. Finlayson, B. A. and Scriven, L. E., "The Method of Weighted Residuals and its Relation to Certain Variational Principles for the Analysis of Transport Processes," Chemical Engineering Science, Vol. 20, pp. 395-404, 1965.
22. Wilson, E. L., "The Determination of Temperatures Within Mass Concrete Structures," Structural Engineering Laboratory Report No. 68-17, University of California, Berkeley, December 1968.
23. Farhoomand, I. and Wilson, E. L., "Non-Linear Heat Transfer Analysis of Axisymmetric Solids," SESM Report No. 71-6, University of California, Berkeley, April 1971.
24. Wilson, E. L., Bathe, K. J. and Peterson, F. E., "Finite Element Analysis of Linear and Nonlinear Heat Transfer," 2nd International Conference on Structural Mechanics in Reactor Technology, Berlin, Germany, Vol. V - Part L, September 1973.
25. Peterson, F. E. and Hui, H., "Sample Solutions and Theoretical Basis for 3D Transient Heat Transfer by Finite Element Procedure," Engineering/Analysis Corporation, Report No. 4.1.4.1, Berkeley, California, August 1971.



## REFERENCES (CON'T)

26. Zienkiewicz, O. C., "The Finite Element Method in Engineering Science," McGraw-Hill, London, 1971.
27. Wilson, E. L., "SAP, A General Structural Analysis Program," University of California Structural Engineering Laboratory Report No. UC SESM 70-20, September 1970.
28. Wilson, E. L., "SOLID SAP, A Static Analysis Program for Three Dimensional Structures," University of California Structural Engineering Laboratory Report No. UC SESM 71-19, Sept. 1971.
29. Kreith, F., "Principles of Heat Transfer," Intext Press Inc., New York, 1973.
30. Bathe, K. J., Wilson, E. L. and Iding, R. H., "NONSAP, A Structural Analysis Program for Static and Dynamic Response of Nonlinear Systems," University of California Structural Engineering Laboratory Report No. UC SESM 74-3, February 1974.
31. Wilson, E. L., Bathe, K. J. and Doherty, W. P., "Direct Solution of Large Systems of Linear Equations," Computers and Structures, Vol. 4, No. 2, pp. 363-372, March 1974.
32. Peavy, B. A., "Steady-State Heat Conduction in an Exposed Exterior Column of Rectangular Cross Section," J. Res. National Bureau of Standards, 69c, p. 145, 1965.
33. Irving and Mullineax, "Mathematics in Physics and Engineering," Academic Press Inc., New York, 1969.
34. Carnahan, Luther and Wilkes, "Applied Numerical Methods," John Wiley and Sons, New York, 1969.
35. Olson and Schultz, "Temperatures in Solids During Heating or Cooling," Ind. Eng. Chem., pp. 874-877, 1942.
36. Clough, R. W., "The Stress Distribution of Norfolk Dam," Institute of Engineering Research Report Series 100, Issue 19, University of California, Berkeley, August 1962.
37. Pirtz, D., Klein, A. and Trescony, L. J., "Thermal Properties of Lean Mass Concretes for Oroville Dam," Structural Engineering Laboratory Report No. 63-3, University of California, Berkeley, June 1963.
38. American Society for Testing and Materials, "Standard Methods of Fire Tests of Building Construction and Materials E119-73," Book of ASTM Standards, Part 14, Philadelphia, p. 462, November 1970.

## REFERENCES (CON'T)

39. Bizri, H., "Structural Capacity of Reinforced Concrete Columns Subjected to Fire Induced Thermal Gradients", Report No. UC SESM 73-1, Department of Civil Engineering, University of California, Berkeley, 1973.
40. Becker, J., Bizri, H. and Bresler, B., "FIRES-T - A Computer Program for the Fire Response of Structures - Thermal", Report No. UCB FRG 74-1, Fire Research Group, Department of Civil Engineering, University of California, Berkeley, 1974.

APPENDIX A1  
DOT USER'S MANUAL

PROGRAM IDENTIFICATION

DOT: A Nonlinear Determination of Temperatures Program  
for Analysis of Two Dimensional Planar or Axisymmetric  
Structures. Version I, February 1976.

Developed by: R. M. Polivka and E. L. Wilson  
University of California, Berkeley

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- A1.2 Program Capacity
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  - V. Boundary Condition Functions
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  - VII. Initial Conditions
  - VIII. Element Specification
    - Type 1: Two Dimensional Finite Elements
    - Type 2: Convection and Radiation Surface Elements
    - Type 3: Cooling Pipe Elements
  - IX. New Problem Data
  - X. Termination Card

### A1.1 PROGRAM DESCRIPTION

The computer program DOT performs the steady state or transient heat transfer analysis of two dimensional planar or axisymmetric structures subjected to surface heat flux, convective and radiative heat transfer, internal heat generation, temperature boundary conditions or artificial cooling by means of embedded pipes. The program is capable of solving both linear and nonlinear analysis problems. The nonlinearities may be due to either temperature dependent material properties or nonlinear boundary conditions.

The program is completely general, and is applicable to structures of arbitrary geometry composed of several different materials. The present version contains the following element types:

1. Two dimensional 4- to 8-node planar or axisymmetric solid elements.
2. Convection and radiation 2-node boundary elements.
3. Cooling pipe elements.

### A.1.2 PROGRAM CAPACITY

The computer program DOT uses variable dimensioning in order to make optimum use of the available high speed storage. The element data for each group of elements is stored in a block and transferred to disc storage. The required core storage remaining is dynamically allocated into a single array A in blank common.

The program capacity can be controlled by the user through the two fortran statements in the main program of DOT:

COMMON (n)

MTOT = n

The total memory n required can be changed depending on the size of the problem to be solved. The minimum value of n needed is given by

$$n = M_{\max} + 2*NPTM*NBCF + NBCF + 4*NNBC + 6*NUMNP + NWK + 1$$

where

$M_{\max}$  = Maximum storage required for element group data

NPTM = Maximum number of time points used to describe any of the boundary condition functions

NBCF = Number of boundary condition functions

NNBC = Number of nodal point boundary conditions

NUMNP = Number of nodes

NWK = Working storage required for conductivity matrix. Approximate by  $MB*NUMNP$  where  $MB$  = maximum bandwidth.

$M_{\max}$  is the maximum value of M for each of the three element types used in the analysis:

(a) Type 1 - Planar or axisymmetric elements

$$M_1 = NEL1*(4*MXNODS - 2) + NUMAT*(5*MAXTP + 4)$$

NEL1 = Number of elements in group 1

NUMAT = Number of material types

MXNODS = Maximum number of nodes defining any element

MAXTP = Maximum number of temperatures defining a given material

(b) Type 2 - Convection and radiation surface elements

$$M_2 = 6*NEL2 + 7*NUMAT + 2$$

NEL2 = Number of elements in group 2

NUMAT = Number of material types

(c) Type 3 - Cooling pipe elements

$$M_3 = 6*NEL3$$

NEL3 = Number of elements in group 3

If the value of n is set too small, an error message is printed which gives the amount by which the storage was exceeded and the program execution is terminated.

### A1.3 PROGRAM INPUT DATA

The following sections describe the necessary sequence of cards which define a given structure to be analyzed.

#### I. PROBLEM INITIATION AND TITLE (A5,3X,18A4) - One card

Columns	Variable	Description
1 - 5	MODE	Problem initiation flag. Punch the word START.
6 - 8	--	Blank
9 - 80	HED	Problem title for labeling output.

#### II. MASTER CONTROL CARD (4I5) - One card

Columns	Variable	Description
1 - 5	NUMNP	Total number of nodal points in structure.
6 - 10	NEG	Number of element groups. See Note 1.
11 - 15	NUMEST	Estimated maximum number of high speed storage locations $M_{\max}$ required to store each set of element group data. Specify (a) Zero or blank: defaults to 4000.
16 - 20	MODEX	Execution mode. Specify (a) Zero or blank: data check only. (b) 1: execution.

#### NOTE

- (1) An element group is a series of elements of a particular type (e.g. 2/D axisymmetric, 2/D planar, convection elements etc.). Elements of the same type may also be split into more than one group.

### III. NODAL POINT COORDINATES (I5,5X,2F10.0,I5,I1)

As many cards as needed to generate NUMNP nodal points.

Columns	Variable	Description
1 - 5	N	Node Number. See Note 1.
6 - 10	--	Blank
11 - 20	X(N)	X coordinate.
21 - 30	Y(N)	Y coordinate.
31 - 35	KN	Node number difference between successive generated nodes (given on first card in a sequence). Specify (a) Zero or blank: No generation. See Note 2.
36	JPR	Print suppression flag (on card for node 1 only). Specify (a) Zero or blank: No suppression. (b) 1: Suppress ordered list of node coordinates. See Note 3.

#### NOTE

- (1) Node cards need not be in numerical order. Eventually, however, all nodes from 1 to the total number of nodes (NUMNP) must be identified.
- (2) The mesh generation parameter KN must appear on the first card of a series of nodal points to be generated. The intermediate nodes to be generated between nodes N1 and N2 will be located at equal intervals along the straight line joining the two nodes. KN is the increment to be added to the previous node number. The node difference N2-N1 must be evenly divisible by KN.
- (3) JPR is used to eliminate the second printing of the ordered node coordinates. The JPR character is entered on the card for node 1 only.



IV. SOLUTION TIME AND TEMPERATURE CONTROL CARD (2I5,3F10.0,3I5)

Columns	Variable	Description
1 - 5	KST	Code for steady state or transient analysis. (a) -1: Steady state analysis. (b) Zero or blank: Transient analysis.
6 - 10	NDT	Number of solution time steps. Specify (a) Zero or blank: defaults to 1.
11 - 20	DT	Time step increment.
21 - 30	TSTART	Time at solution start. See Note 1.
31 - 40	TAMB	Ambient temperature. See Note 2.
41 - 45	NPRINT	Time interval for printout of nodal temperatures, expressed as a multiple of the integration time step. Specify (a) Zero or blank: defaults to 1.
46 - 50	NTSREF	Number of time steps between reforming effective conductivity matrix. Specify (a) Zero or blank: Conductivity matrix never reformed. (b) n: Conductivity matrix reformed every n steps.
51 - 55	KP	Time interval for punched output of nodal temperatures, expressed as a multiple of the integration time step. Specify (a) Zero or blank: No punched output. (b) n: Punched output every n steps. See Note 3.

NOTE

- (1) The time at solution start (TSTART) is an input convenience for restart jobs. In a restart job, TSTART is the final time to which a previous job was run and the nodal temperatures saved for use in supplying initial conditions for a new job. The time counter is incremented from TSTART, so none of the boundary condition functions in Section V need be revised.
- (2) The body is assumed to be at uniform ambient temperature (TAMB) prior to the application of any heat flow boundary conditions; i.e. at  $t = 0$  all nodes are at temperature (TAMB).

- (3) The punched output time interval KP controls punching of nodal temperatures. For  $KP = n$ , the temperatures at the end of every  $n$  steps are punched in exactly the same format as the initial conditions in Section VII. In addition, the nodal point coordinate data is also punched for possible use with a mesh plotting program.

For the case of  $KP = NDT$ , the nodal temperatures at the end of the analysis will be saved on punched cards, which in turn can be read in as initial conditions in a restart job. By setting  $TSTART = NDT*DT$ , a new analysis run can now be made.

V. BOUNDARY CONDITION FUNCTIONS

A. CONTROL INFORMATION (3I5) - One card

Columns	Variable	Description
1 - 5	NBCF	Number of boundary condition functions. See Note 1.
6 - 10	NPTM	Maximum number of points used to describe any one of the functions. See Note 2.
11 - 15	NNBC	Number of nodal point heat flow or temperature boundary conditions. See Note 3.

NOTE

- (1) NBCF determines the number of card sets to be read in Section V.B.
- (2) NPTM is the maximum number of  $[f(t),t]$  pairs used to define any one of the NBCF functions. At least two points are required to input any one function, and no function may be input with more than NPTM points.
- (3) NNBC determines the number of cards to be read or generated in Section VI.

B. TIME FUNCTION DATA - NBCF sets of cards

Each set consists of a control card followed by as many cards as needed to define the function.

1. CONTROL CARD (2I5) - First card of set.

Columns	Variable	Description
1 - 5	NC	Function number. (GE.1 and LE.NBCF) See Note 1.
6 - 10	NPTS(NC)	Number of time points used to describe this function. (GE.2 and LE.NPTM)

2. [f(t),t] DATA (8F10.0) - Remaining card(s) of set.

As many cards as needed to define NPTS(NC) pairs of points [TFN(NC,I),FN(NC,I)], four pairs per card. See Note 2.

Columns	Variable	Description
1 - 10	TFN(NC,1)	Time at point 1 : $t_1$
11 - 20	FN (NC,1)	Function value at point 1 : $f(t_1)$
21 - 30	TFN(NC,2)	Time at point 2 : $t_2$
31 - 40	FN (NC,2)	Function value at point 2 : $f(t_2)$
41 - 50	TFN(NC,3)	} Point 3
51 - 60	FN (NC,3)	
61 - 70	TFN(NC,4)	} Point 4
71 - 80	FN (NC,4)	

NEXT CARD(S) - If required

1 - 10	TFN(NC,5)	Time at point 5 : $t_5$
11 - 20	FN (NC,5)	Function value at point 5 : $f(t_5)$
...	...	...

NOTE

- (1) Time functions need not be input in order of increasing function number NC.

- (2) The function tables input in this section are used to prescribe time dependent boundary conditions such as environmental or nodal point temperatures and nodal point heat flows. The functions may also be used to describe the rate of internal heat generation and the variation of convection coefficient  $H$  with temperature.

Time values at successive points must increase in magnitude. Values of the functions at times (temperatures) other than  $TFN(NC,I)$  are calculated within the program using linear interpolation.

The first time point  $TFN(NC,1)$  must be less than or equal to the time at solution start  $TSTART$  and the final time point  $TFN(NC,NPTS(NC))$  must be greater than or equal to the time at the end of solution  $NDT*DT$ .

VI. NODAL POINT BOUNDARY CONDITIONS (4I5,F10.0,I5) - NNBC cards

Columns	Variable	Description
1 - 5	N	Boundary condition number. See Note 1.
6 - 10	NOD(N)	Global node number. (GE.1 and LE.NUMNP)
11 - 15	KODE(N)	Boundary condition type. Specify (a) Zero or blank : Externally supplied heat flux Q. (b) 1: Prescribed temperature T.
16 - 20	NFN(N)	Function number. (GE.0 and LE.NBCF) See Note 2.
21 - 30	TQ(N)	Boundary value amplitude. Specify (a) Heat flux (KODE(N) = 0). (b) Temperature (KODE(N) = 1). See Note 3.
31 - 35	KN	Node number difference between successive generated nodes (on first card in sequence). See Note 4.

NOTE

- (1) All nodal points not specified in this section are assumed to have externally supplied heat flux of zero for all values of time.
- (2) A function number equal to zero or blank means that the prescribed boundary condition is applied at time zero and remains constant for all time greater than zero (step function). The functions assigned in this section must have been defined previously in Section V. A given function can be used to describe any number of boundary conditions.
- (3) (a) For the case of flux or temperature boundary conditions which are not step functions, TQ(N) represents a function multiplier used to scale NFN(N) values for all time t.  
(b) For the case of flux or temperature boundary conditions applied as a step function from time zero, TQ(N) represents the actual value of prescribed flux or temperature.
- (4) In the printout of nodal point boundary conditions, all generated node data are prefixed by an asterisk. For use of the generation parameter KN, see Note 2, Section III.

VII. INITIAL CONDITIONS

This set of cards consists of a control card followed by as many cards as needed to define the initial nodal temperatures not equal to the specified ambient temperature (TAMB).

A. CONTROL CARD (I5) - One card

Columns	Variable	Description
1 - 5	ICON	Initial condition flag. Specify (a) Zero or blank: Temperatures of all nodes set automatically to the specified ambient temperature. (b) $n > 0$ : Nodes having user supplied initial conditions are read from data cards in Section VII.B. See Note 1.

B. INITIAL TEMPERATURES (4(I5,5X,E10.0)) - n temperatures

As many cards as needed to specify n nodal temperatures (four values per card) which are not equal to the ambient temperature. Omit if the initial condition flag ICON equals zero or blank. See Note 2.

Columns	Variable	Description
1 - 5	ND	Node number.
11 - 20	T(ND)	Temperature.
...	...	...

NOTE

- (1) The initial condition flag ICON is used to control card reading in Section VII.B. For ICON equal to zero, the initial temperatures are set equal to the specified ambient temperature TAMB and input should then resume beginning in Section VIII.
- (2) For a restart job where the initial conditions are supplied from a previous heat transfer solution performed using DOT, the variable ICON must equal NUMNP and the initial temperatures then read in Section VII.B will be the punched deck obtained from the first run using KP equal to NDT in Section IV.

### VIII. ELEMENT SPECIFICATION

Elements must be divided into "groups". Input as many blocks of data in the following sections as there are element groups (NEG). An element group is a series of elements of a particular type, and elements of the same type may also be divided into more than one group.

Element groups may be input in any order. The elements in any group must be numbered sequentially starting from the number of the first element as specified on the element group control card.

The following types of element groups may be used:

#### Type 1 - Two Dimensional Finite Elements

These are 4- to 8-node isoparametric elements which must be input in the global X-Y plane. When the element is used to represent an axisymmetric solid, the global Y-axis is the axis of revolution.

#### Type 2 - Convection and Radiation Surface Elements

These are 2-node planar or axisymmetric solid boundary elements which must be input in the global X-Y plane.

#### Type 3 - Cooling Pipe Elements

These are 1-node elements which are placed at existing nodal points in the finite element mesh. The axis of the cooling pipe is the Z-axis.



TYPE 1 - TWO DIMENSIONAL FINITE ELEMENTS

A. CONTROL INFORMATION (9I5) - One card

Columns	Variable	Description
1 - 5	NGR	Element group indicator. Punch the number "1".
6 - 10	NEL1	Number of elements in this group.
11 - 15	MFST	Element number of first element in group. (a) Zero or blank: defaults to 1. See Note 1.
16 - 20	ITYP2D	Element type code. Specify (a) Zero or blank: axisymmetric (b) 1: planar
21 - 25	MXNODS	Maximum number of nodes used to describe any one element. Specify (a) Zero or blank: defaults to 4. (GE.4 and LE.8)
26 - 30	NINT	Numerical integration order to be used in Gaussian quadrature. Specify (a) Zero or blank: defaults to 2. (GE.2 and LE.4) See Note 2.
31 - 35	NUMAT	Number of material property sets. Specify (a) Zero or blank: defaults to 1.
36 - 40	MAXTP	Maximum number of temperature points in material table. Specify (a) Zero or blank: defaults to 1. (GT.0)
41 - 45	IHFLG	Internal heat generation flag. Specify (a) Zero or blank: No internal heat generation. (b) 1: Internal heat generation exists.

NOTE

- (1) Element numbers need not begin with number 1 if MFST is specified.
- (2) For rectangular elements, an integration order of 2 is sufficient. If the element is distorted, a higher integration order need be used.

B. MATERIAL PROPERTY INFORMATION - NUMAT sets of cards.1. MATERIAL IDENTIFICATION CARD (I5,5X,F10.0,2I5,F10.0) - One card

Columns	Variable	Description
1 - 5	M	Material identification number. (GE.1 and LE.NUMAT)
6 - 10	--	Blank
11 - 20	DENS(M)	Density of material. Leave blank for steady-state problems.
21 - 25	NTC(M)	Number of temperature points describing the material. Specify (a) Zero or blank: defaults to 1.
26 - 30	NFHG(M)	Function number describing the rate of internal heat generation. See Note 1.
31 - 40	HGSC(M)	Internal heat generation function multiplier. See Note 1.

2. MATERIAL PROPERTY CARD(S) (5F10.0) - Remaining NTC(M) cards of set.  
See Note 2.

Columns	Variable	Description
1 - 10	TPROP(1)	Temperature $T_1$ .
11 - 20	TPROP(2)	Conductivity $k_{11}$ at temperature $T_1$ .
21 - 30	TPROP(3)	Conductivity $k_{22}$ at temperature $T_1$ .
31 - 40	TPROP(4)	Conductivity $k_{12}$ at temperature $T_1$ .
41 - 50	TPROP(5)	Specific heat $c$ at temperature $T_1$ .

NOTE

- (1) If no internal heat generation exists, i.e. if IHFLG equals zero, leave columns 26-40 blank. For the case where internal heat generation is considered, the functions NFHG assigned in this section must have been defined previously in Section V. See Note 2, Section VI.
- (2) Consistent units must be used for specification of material properties.

C. ELEMENT DATA (12I5)

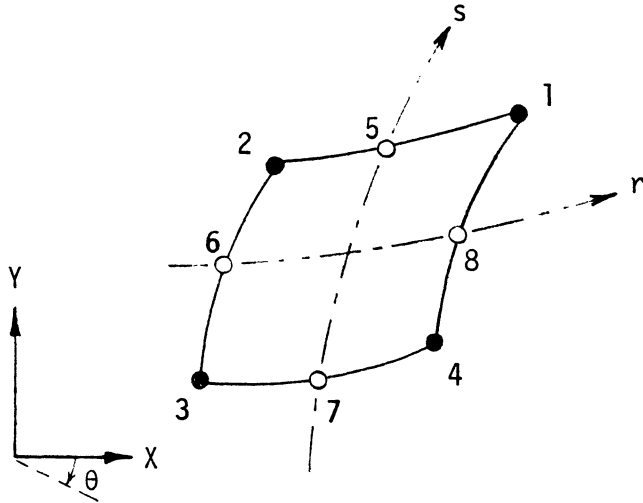
As many cards as needed to generate NELL elements.

Columns	Variable	Description
1 - 5	M	Element number. See Note 1.
6 - 10	NOD(1)	Global node number of element node 1.
11 - 15	NOD(2)	Global node number of element node 2.
16 - 20	NOD(3)	Global node number of element node 3.
21 - 25	NOD(4)	Global node number of element node 4.
26 - 30	NOD(5)	Global node number of element node 5.
31 - 35	NOD(6)	Global node number of element node 6.
36 - 40	NOD(7)	Global node number of element node 7.
41 - 45	NOD(8)	Global node number of element node 8. See Note 2.
46 - 50	MTYP	Material identification number. Specify (a) Zero or blank: defaults to 1. (GE.1 and LE.NUMAT)
51 - 55	IEL	Number of nodes used to describe element. (a) Zero or blank: defaults to MXNODS.
56 - 60	KG	Node number increment for element generation (given on first card in a sequence). (a) Zero or blank: defaults to 1. See Note 3.

NOTE

- (1) All elements must be input in increasing numerical order, starting with element number MFST. Cards for the first and last element must be included.
- (2) The number of nodes in element M is defined by IEL. For elements containing less than eight nodes (IEL.LT.8), input a zero or blank in NOD(I) for the particular node locations not used. As an example, for a 6-node element (IEL.EQ.6) with nodes 5 and 7 not used, the element node number array would be NOD(I) = [X X X X 0 X 0 X] where the nonzero entries (X) are the global node numbers of the 6 nodes.

Figure VIII-1 defines the mapping between the node numbering in the local r-s coordinate system and the global X-Y coordinate system. Nodes 1 through 4 are located at the four corners in a counterclockwise sense, and nodes 5 through 8 are located at the midsides of the element.



Node	r	s
1	+1	+1
2	-1	+1
3	-1	-1
4	+1	-1
5	0	+1
6	-1	0
7	0	-1
8	+1	0

FIG. VIII-1 TWO DIMENSIONAL FINITE ELEMENT NODE NUMBER INPUT SEQUENCE

- (3) The node generation parameter KG must appear on the first element card of a sequence, and is used to compute the node numbers for a group of missing elements.

If data for elements [M+1,M+2,... M+J] are omitted, these "J" missing elements are generated using the same values for material number (MTYP) and number of nodes (IEL) as given on the preceding card for element M, and the node numbers for the successive "J" elements are incremented by the value KG given on the M-th element card. Only the nonzero node numbers appearing on the M-th element card are incremented when generating missing element data.

In the printout of the element data, generated elements are prefixed by an asterisk.



C. MATERIAL PROPERTY INFORMATION - NUMAT sets of cards1. MATERIAL IDENTIFICATION CARD (3I5) - First card of set.

Columns	Variable	Description
1 - 5	M	Material identification number. (GE.1 and LE.NUMAT)
6 - 10	NFH	Function number describing the variation of convection coefficient H with temperature. See Note 1.
11 - 15	NFTE	Function number describing the environmental temperature variation with time. See Note 2.

2. MATERIAL PROPERTY CARD(S) (5F10.0) - Second card of set.

Columns	Variable	Description
1 - 10	PROP(1)	Convection coefficient function multiplier. See Note 1.
11 - 20	PROP(2)	Environmental temperature function multiplier. See Note 2.
21 - 30	PROP(3)	Radiation shape factor (view factor). (a) Zero or blank: radiation effects are ignored.
31 - 40	PROP(4)	Surface emissivity.
41 - 50	PROP(5)	Environment emissivity.

NOTE

- (1) The variation of convection coefficient H with temperature is computed using  $H(T) = \text{PROP}(1) * \text{NFH}$  where the function number NFH has been defined previously in Section V. A function number equal to zero or blank will be assumed to have the temperature independent value of unity.
- (2) The variation of environmental temperature with time is computed using  $T_e(t) = \text{PROP}(2) * \text{NFTE}$  where the function number NFTE has been defined previously in Section V. If the environmental temperature does not change with time, input NFTE equal to zero or blank and  $\text{PROP}(2) = T_0$ , constant for all time greater than zero (step function).

D. ELEMENT DATA (5I5)

As many cards as needed to generate NEL2 elements.

Columns	Variable	Description
1 - 5	M	Surface number. See Note 1.
6 - 10	NOD(1)	Global node number of element node I.
11 - 15	NOD(2)	Global node number of element node J. See Note 2.
16 - 20	MTYP	Material identification number. Specify (a) Zero or blank: defaults to 1. (GE.1 and LE.NUMAT)
21 - 25	KG	Node number increment for element generation (given on first card in a sequence). (a) Zero or blank: defaults to 1. See Note 3.

NOTE

- (1) All elements must be input in ascending numerical order, starting with element number MFST. Cards for the first and last element must be included.
- (2) Convection and radiation boundary elements are 2-node elements on the surface of a planar or axisymmetric solid, as shown in Figure VIII-2.

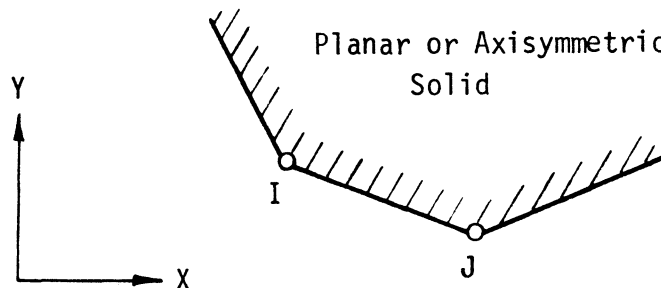


FIG. VIII-2 CONVECTION AND RADIATION SURFACE ELEMENTS

- (3) The node generation parameter KG must be given on the first element card prior to a group of missing elements. All generated elements will have the same material identification number (MTYP) as that given on the first element card in the sequence. In the printout of the element data, generated elements are prefixed by an asterisk.

TYPE 3 - COOLING PIPE ELEMENTSA. CONTROL INFORMATION (3I5) - One card

Columns	Variable	Description
1 - 5	NGR	Element group indicator. Punch the number "3".
6 - 10	NEL3	Number of elements in this group.
11 - 15	MFST	Element number of first element in group. (a) Zero or blank: defaults to 1. See Note 1.

B. ELEMENT DATA (2I5,F10.0,2I5,3F10.0)

As many cards as needed to generate NEL3 elements.

Columns	Variable	Description
1 - 5	M	Element number. See Note 1.
6 - 10	NOD	Global node number of cooling pipe location.
11 - 20	HP	Empirical constant. See Note 2.
21 - 25	NFC	Function number describing the cooling water temperature variation with time. See Note 3.
26 - 30	KG	Node number increment for element gener- ation (given on first card in a sequence). See Note 4.
31 - 40	TWTR	Cooling water temperature function multiplier. See Note 3.
41 - 50	TBTH	Time at initiation of cooling.
51 - 60	TDTH	Time when cooling is to be stopped.

NOTE

- (1) Element numbers need not begin with number 1 if MFST is specified. All elements must be input in increasing numerical order starting with element MFST. The first and last element cards must be included.



- (2) The rate at which heat is removed from the solid by a cooling pipe is given by:

$$q = HP(T_w - T_o)$$

where

$T_w$  = temperature of the cooling water.

$T_o$  = apparent temperature on the outer surface of the pipe at node NOD in the finite element solution.

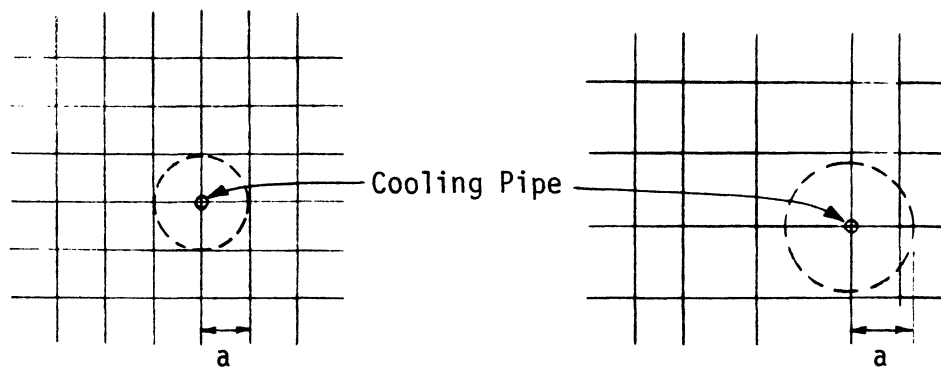
$$HP = \frac{2\pi k}{\ln\left(\frac{a}{R}\right) - 2}, \text{ an empirical constant.}$$

where

$k$  = average conductivity of finite elements adjacent to the cooling pipe.

$R$  = radius of cooling pipe.

$a$  = weighted distance to adjacent node.  
(See Fig. VIII-3)



(i) Regular Mesh

(ii) Irregular Mesh

FIG. VIII-3 DETERMINATION OF 'a' IN EQUATION FOR HP

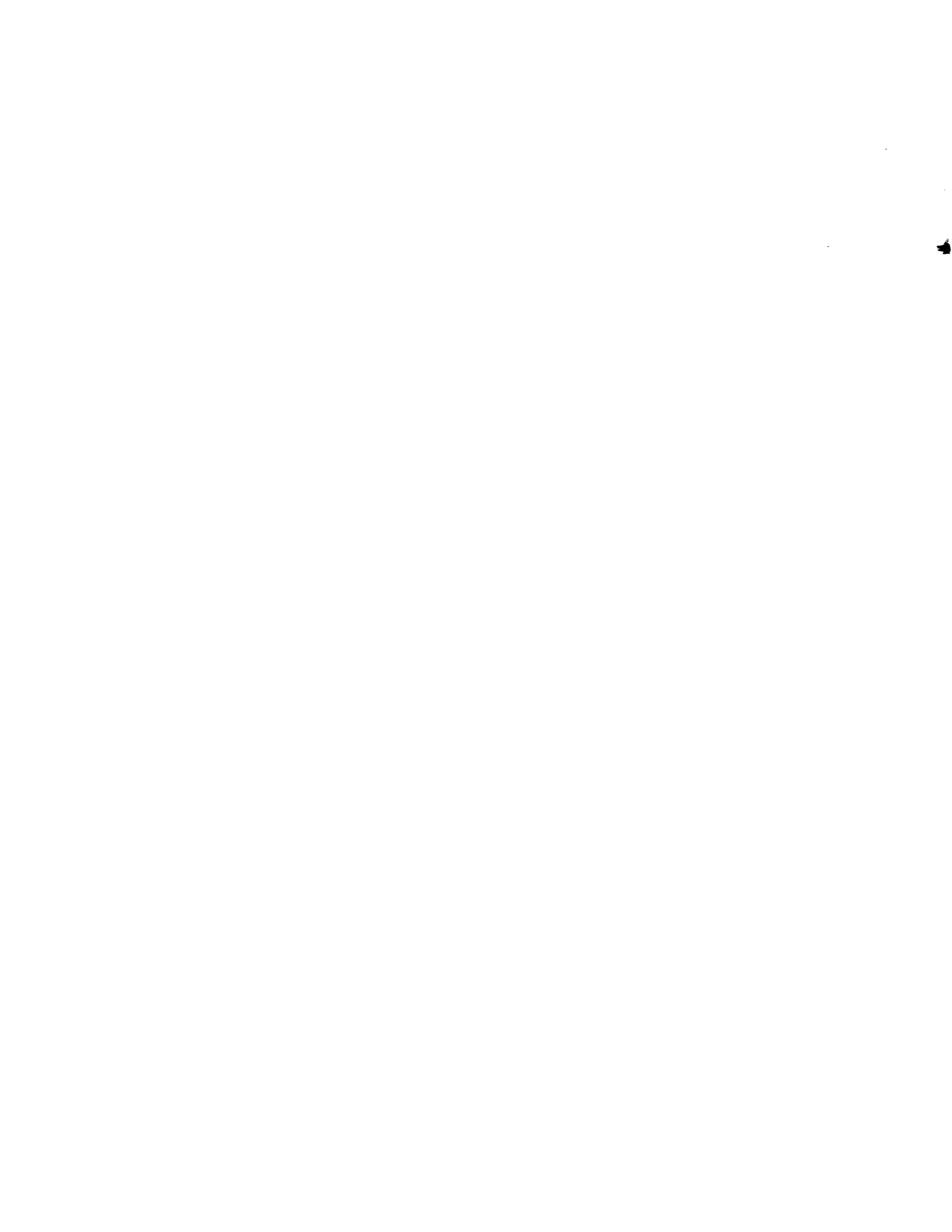
- (3) If the cooling water temperature  $T_w$  is time-dependent, then a nonzero function number NFC must be specified. If the cooling water temperature  $T_w$  does not change with time, then input NFC equal to zero or blank and TWTR =  $T_0$ , constant for all time greater than zero (step function).
- (4) The node generation parameter KG must appear on the first element card of a sequence, and is used to compute node numbers for missing elements. All data for generated elements is taken to be the same as that given on the first element card in the sequence. In the printout of the element data, all generated elements are prefixed by an asterisk.

IX. NEW PROBLEM DATA

A completely new problem may now be solved by starting with Section I. Any number of heat transfer problems may be solved within a single computer run.

X. TERMINATION CARD (A4) - One card

Columns	Variable	Description
1 - 4	MODE	Problem(s) termination flag. Punch the word STOP.



APPENDIX A2

DOT FORTRAN IV LISTING



```

001 1 PROGRAM DOT (INPUT,OUTPUT,PUNCH,TAPES=INPUT,TAPE6=OUTPUT,
002 2 TAPE1,TAPE2,TAPE3=PUNCH)
003 3
004 4
005 5 *****
006 6
007 7 DOT - A NONLINEAR DETERMINATION OF TEMPERATURES PROGRAM FOR
008 8 TWO DIMENSIONAL PLATE OR AXISYMMETRIC STRUCTURES
009 9
010 10 DEVELOPED BY - R.M. POLIVKA AND E.L. WILSON, FEBRUARY, 1976
011 11 *****
012 12
013 13 C
014 14
015 15 COMMON /CNTRL/ NUNNP,NEG,MODEX,NBAR(10),NG,KBC
016 16 COMMON /CNTRLE/ KST,NDT,TT,START,TAMB,NPRINT,NTSREF,TIME,KP
017 17 COMMON /DIR / N1,N2,N3,N4,N5,N6,N7,N8,N9,N10,N11,N12,N13,N14,N15
018 18 COMMON /JUNK / MBD10,MTOT,MLINE
019 19 COMMON /NBC / NBC,NBC,NPTN
020 20 COMMON /WORK / WORK(200)
021 21
022 22 COMMON A(10000)
023 23
024 24 MTOT = 10000
025 25 200 MAXEST = 0
026 26 *****
027 27
028 28 INPUT PHASE
029 29 *****
030 30
031 31 C
032 32 C
033 33 C
034 34 C
035 35 C
036 36 C
037 37 C
038 38 C
039 39 C
040 40 C
041 41 C
042 42 C
043 43 C
044 44 C
045 45 C
046 46 C
047 47 C
048 48 C
049 49 C
050 50 C
051 51 C
052 52 C
053 53 C
054 54 C
055 55 C
056 56 C
057 57 C
058 58 C
059 59 C
060 60 C
061 61 C
062 62 C
063 63 C
064 64 C
065 65 C
066 66 C
067 67 C
068 68 C
069 69 C
070 70

```

SHIFT STORAGE TO ELIMINATE NODAL COORDINATE DATA

```

5 I = 1 + MAXEST
N12M = N12 - 1
DO 10 J=N3,N12M
A(I) = A(J)
10 I = I + 1

```

```

N1 = 1 + MAXEST
N2 = N1 + NDT*NBCF
N3 = N2 + NDT*NBCF
N4 = N3 + NBCF
N5 = N4 + NBCF
N6 = N5 + NBCF
N7 = N6 + NBCF
N8 = N7 + NBCF
N9 = N8 + NUNNP + 1
N10 = N9 + NUNNP
N11 = N10 + NUNNP
N12 = N11 + NUNNP
N13 = N12 + NUNNP
N14 = N13 + NUNNP
N15 = N14 + NUNNP
IF(KST.EQ.1) N14 = N12
IF(KBC.EQ.0) N14 = N15
IF(N15.GT.MTOT) CALL ERROR (N15-MTOT)
IF(MODEX.EQ.0) GO TO 200

```

```

INITIALIZE CONDUCTIVITY MATRIX (KK) AND HEAT FLOW VECTOR (Q)
N12M = N12 - 1
DO 15 I=N10,N12M
A(I) = 0.0
15 A(I) = 0.0

```

```

INITIALIZE TEMPERATURE VECTOR TT(0) = T(0)
IF(KBC.EQ.0) GO TO 22
DO 20 I=1,NUNNP
TT = N8 + I - 1
TT = N14 + I - 1
20 A(ITT) = A(IT)

```

```

INITIALIZE THE TIME STEP COUNTER
KSTEP = 0
TIME = TSTART

```

```

INITIALIZE EFFECTIVE HEAT CAPACITY VECTOR (C)
IF(KST.EQ.-1) GO TO 30
N13M = N13 - 1
DO 25 I=N12,N13M
A(I) = 0.0
25 A(I) = 0.0

```

```

ASSEMBLE THE EFFECTIVE SYSTEM CONDUCTIVITY MATRIX (KK)
BASED ON MATERIAL PROPERTIES AT TEMPERATURE T(0), AND
MODIFY FOR LINEAR CONVECTION AND COOLING PIPE BC
30 CALL ASSENK

```

```

IF(NNBC.EQ.0) GO TO 15
MODIFY CONDUCTIVITY MATRIX F(J) TEMPERATURE BOUNDARY CONDITIONS
CALL MODKTP (A(N4),A(N5),A(N9),A(N10),A(N13),A(N15))
CALL MODKTP (A(N4),A(N5),A(N9),A(N10),A(N13),A(N15))
35 I = KST.EQ.-1) GO TO 40

```

BLANK COMMON STORAGE ALLOCATION

```

ARRAY -----DESCRIPTION-----
FN TIME VALUES AT POINTS
N1 NPTMNBCF
N2 NPTMNBCF
N3 FUNCTION VALUES AT POINTS
N4 NBCF
N5 NUMBER OF FUNCTION INPUT POINTS
N6 NBCF
N7 NODES HAVING PRESCRIBED BC
N8 NBCF
N9 BOUNDARY CONDITION TYPES
N10 NBCF
N11 BC FUNCTION NUMBERS
N12 NBCF
N13 T
N14 T
N15 T
N16 T
N17 T
N18 T
N19 T
N20 T
N21 T
N22 T
N23 T
N24 T
N25 T
N26 T
N27 T
N28 T
N29 T
N30 T
N31 T
N32 T
N33 T
N34 T
N35 T
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N42 T
N43 T
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N45 T
N46 T
N47 T
N48 T
N49 T
N50 T
N51 T
N52 T
N53 T
N54 T
N55 T
N56 T
N57 T
N58 T
N59 T
N60 T
N61 T
N62 T
N63 T
N64 T
N65 T
N66 T
N67 T
N68 T
N69 T
N70 T

```

PUNCH NODAL POINT COORDINATE DATA

```

IF(KP.EQ.0) GO TO 5
CALL FNDDE (A(N1),A(N2),NUNNP,NK,N8)

```

```

DOT 141 C      FORM THE INITIAL RESISTANCE VECTOR AT TIME ZERO, E(0)
DOT 142 C      E(0) = (C*(T(0)))
DOT 143 C
DOT 144 C      CALL FORME (A(N8),A(N13),A(N12),NUMNP)
DOT 145 C
DOT 146 C      TRIANGULARIZE THE EFFECTIVE CONDUCTIVITY MATRIX, (K*)
DOT 147 C
DOT 148 C      40 KTR = 0
DOT 149 C      CALL COLSOL (A(N10),A(N11),A(N9),NUMNP,N8,NWK,KTR)
DOT 150 C
DOT 151 C      *****
DOT 152 C      TIME MARCHING LOOP
DOT 153 C      *****
DOT 154 C
DOT 155 C      10C KSTEP = KSTEP + 1
DOT 156 C      TIME = TIME + DT
DOT 157 C
DOT 158 C      CHECK TO SEE IF SYSTEM EQUATIONS TO BE REFORMED THIS TIME STEP
DOT 159 C
DOT 160 C      IF(KSTEP.EQ.1) GO TO 70
DOT 161 C      K = MOD(KSTEP,NPRINT)
DOT 162 C      IF(K.NE.0) GO TO 70
DOT 163 C
DOT 164 C      REFORM THE SYSTEM EQUATIONS
DOT 165 C
DOT 166 C      DO 43 I=N10,N12M
DOT 167 C      45 A(I) = 0.0
DOT 168 C      IF(KST.EQ.-1) GO TO 55
DOT 169 C      DO 50 I=N12,N13M
DOT 170 C      50 A(I) = 0.0
DOT 171 C
DOT 172 C      55 CALL ASSEK
DOT 173 C
DOT 174 C      IF(NB.C.EQ.0) GO TO 60
DOT 175 C
DOT 176 C      CALL MODKTB (A(N4),A(N5),A(N9),A(N10),NNBC)
DOT 177 C
DOT 178 C      60 IF(KST.EQ.-1) GO TO 65
DOT 179 C
DOT 180 C      CALL FORME (A(N8),A(N13),A(N12),NUMNP)
DOT 181 C
DOT 182 C      65 KTR = 0
DOT 183 C      CALL COLSOL (A(N10),A(N11),A(N9),NUMNP,N8,NWK,KTR)
DOT 184 C
DOT 185 C      DEFINE EXTERNALLY SUPPLIED HEAT FLUX VECTOR (Q) FOR THIS TIME STEP
DOT 186 C
DOT 187 C      70 IF(NB.C.EQ.0) GO TO 75
DOT 188 C
DOT 189 C      PRESCRIBED (Q)
DOT 190 C
DOT 191 C      CALL FORMQP (A(N1),A(N2),A(N3),A(N4),A(N5),A(N6),A(N7),
DOT 192 C      1 A(N11),NPTM)
DOT 193 C
DOT 194 C      CONVECTION, RADIATION AND INTERNAL HEAT GENERATION (Q)
DOT 195 C
DOT 196 C      75 CALL FORMOC
DOT 197 C
DOT 198 C      IF(KST.EQ.-1) GO TO 80
DOT 199 C
DOT 200 C      COMPUTE EFFECTIVE HEAT FLUX VECTOR
DOT 201 C      Q*(TIME) = Q(TIME) + E(TIME-1)
DOT 202 C
DOT 203 C      CALL DEFF (A(N11),A(N13),NUMNP)
DOT 204 C
DOT 205 C      UPDATE (TT) VECTOR
DOT 206 C
DOT 207 C      80 IF(KBC.EQ.0) GO TO 84
DOT 208 C      DO 82 I=1,NUMNP
DOT 209 C      IT = N8 + I - 1
DOT 210 C      ITT = N14 + I - 1

```

```

DOT 211 C      82 A(ITT) = A(IT)
DOT 212 C
DOT 213 C      SOLVE THE HEAT EQUILIBRIUM EQUATIONS FOR THE SYSTEM TEMPERATURES
DOT 214 C      T(TIME) = (K*(TRI))Q*(TIME)
DOT 215 C
DOT 216 C      84 KTR = 2
DOT 217 C      CALL COLSOL (A(N10),A(N11),A(N9),NUMNP,N8,NWK,KTR)
DOT 218 C
DOT 219 C      0-VECTOR IS NOW T-VECTOR. SET T(I)=Q(I) AND Q(I)=0.
DOT 220 C
DOT 221 C      DO 85 I=1,NUMNP
DOT 222 C      IT = N8 + I - 1
DOT 223 C      IO = N11 + I - 1
DOT 224 C      A(IT) = A(IO)
DOT 225 C
DOT 226 C      85 A(IO) = 0.0
DOT 227 C
DOT 228 C      PRINT AND/OR PUNCH THE MODAL TEMPERATURE DISTRIBUTION,
DOT 229 C      IF REQUESTED, AT THIS TIME STEP
DOT 230 C
DOT 231 C      K = MOD(KSTEP,NPRINT)
DOT 232 C      IF(K.NE.0) GO TO 90
DOT 233 C      CALL OUT (A(N8),NUMNP,TIME,KSTEP)
DOT 234 C      90 IF(KP.EQ.0) GO TO 92
DOT 235 C      L = MOD(KSTEP,KP)
DOT 236 C      IF(L.NE.0) GO TO 92
DOT 237 C      CALL PTEMP (A(N8),TIME,NUMNP)
DOT 238 C
DOT 239 C      COMPUTE THE NEW THERMAL RESISTIVITY VECTOR (E)
DOT 240 C      92 IF(KST.EQ.-1) GO TO 95
DOT 241 C
DOT 242 C      CALL FORME (A(N8),A(N13),A(N12),NUMNP)
DOT 243 C
DOT 244 C      CHECK FOR FINAL TIME STEP
DOT 245 C
DOT 246 C      95 IF(KSTEP.LT.NDT) GO TO 100
DOT 247 C
DOT 248 C      GO TO 200
DOT 249 C
DOT 250 C      END

```

```

SUBROUTINE DOTT
DOT 1  C
DOT 2  C
DOT 3  C      COMMON /CNTRL1/ NUMNP,NEG,MODEX,NPAR(10),NG,KBC
DOT 4  C      COMMON /CNTRL2/ KST,NDT,DT,START,TAMB,NPRINT,NISREF,TIME,KP
DOT 5  C      COMMON /DIM / N1,N2,N3,N4,N5,N6,N7,N8,N9,N10,N11,N12,N13,N14,N15
DOT 6  C      COMMON /ELSTOR/ NIMEST,M1OEST,M1KEST
DOT 7  C      COMMON /JUNK / HED(18),MYDT,MLINE
DOT 8  C      COMMON /NBK / NNBC,NBCF,NPTM
DOT 9  C      COMMON A(1)
DOT 10 C      DIMENSION MOD(2)
DOT 11 C      DATA MOD/5HSTART,5HSTOP /
DOT 12 C
DOT 13 C      *****
DOT 14 C      READ CONTROL INFORMATION
DOT 15 C      *****
DOT 16 C
DOT 17 C      10 READ (5,1000) MODE,HED
DOT 18 C      IF(MODE.EQ.MOD(2)) STOP
DOT 19 C      IF(MODE.EQ.MOD(1)) GO TO 20
DOT 20 C      WRITE(6,3000)
DOT 21 C      GO TO 1C
DOT 22 C
DOT 23 C      20 READ (5,1001) NUMNP,NEG,NUMEST,MODEX

```









```

INIT 12 DO 100 I=1,NUMNP
INIT 13 100 T(1) = TAMB
INIT 14 C
INIT 15 IF(ICON.NE.0) GO TO 200
INIT 16 WRITE(6,2001) TAMB
INIT 17 GO TO 300
INIT 18 C
INIT 19 200 WRITE(6,2002)
INIT 20 READ(5,1001) (ND,T(ND),J=1,ICON)
INIT 21 WRITE(6,2003) (N,T(N),N=1,NUMNP)
INIT 22 C
INIT 23 C FORMAT STATEMENTS
INIT 24 C
INIT 25 1000 FORMAT(15)
INIT 26 1001 FORMAT(115,5X,F10.0)
INIT 27 2000 FORMAT(//19(1H)/19H INITIAL CONDITIONS/19(1H)//
INIT 28 1 51H INITIAL CONDITION CODE (ICON) ***** = 15//
INIT 29 2 49H EO, 0, ALL NODES SET TO AMBIENT TEMPERATURE/
INIT 30 3 51H EO, 1, INITIAL CONDITIONS ARE READ FROM CARDS, 3//
INIT 31 2001 FORMAT(4X,A7HALL NODES AT UNIFORM INITIAL TEMPERATURE ***** = F10.3)
INIT 32 2002 FORMAT(13(1H)/36H A, INITIAL TEMPERATURE DISTRIBUTION/36(1H)//)
INIT 33 2003 FORMAT(6(16,E14.6))
INIT 34 C
INIT 35 300 RETURN
INIT 36 END

ELCL 39 C
ELCL 40 C EO,0, AXISYMMETRIC SOLID CONVECTION BC
ELCL 41 C EO,1, PLANAR SOLID CONVECTION BC
ELCL 42 C NPAR(5) = NUMBER OF DIFFERENT MATERIALS (NUMAT)
ELCL 43 C *****
ELCL 44 C COOLING PIPE ELEMENTS
ELCL 45 C
ELCL 46 C NPAR(1) = 3
ELCL 47 C NPAR(2) = NUMBER OF COOLING PIPE ELEMENTS (NEL3)
ELCL 48 C NPAR(3) = NUMBER OF FIRST ELEMENT IN THIS GROUP (MFST)
ELCL 49 C *****
ELCL 50 C ZERO ACTIVE COLUMN WEIGHT ARRAY (NMT)
ELCL 51 C
ELCL 52 N12 = N11 + NUMNP + 1
ELCL 53 N13 = N12 + NUMNP
ELCL 54 IF(N13.GT.MTOT) CALL ERROR (N13-MTOT)
ELCL 55 C
ELCL 56 DO 5 I=N12,N13
ELCL 57 5 A(I) = 0.0
ELCL 58 C
ELCL 59 C REWIND 1
ELCL 60 C
ELCL 61 C LOOP OVER ALL ELEMENT GROUPS
ELCL 62 C
ELCL 63 DO 100 NG=1,NEG
ELCL 64 CALL TITLE (HED)
ELCL 65 WRITE(6,2000) NG
ELCL 66 MLINE = 7
ELCL 67 C
ELCL 68 READ (5,1000) NPAR
ELCL 69 C
ELCL 70 NGR = NPAR(1)
ELCL 71 C
ELCL 72 GO TO (1,2,3) NGR
ELCL 73 C
ELCL 74 C -----
ELCL 75 C ELEMENT GROUP 1
ELCL 76 C -----
ELCL 77 C
ELCL 78 1 IF(NPAR(2).GT.0) GO TO 10
ELCL 79 WRITE(6,3000)
ELCL 80 STOP
ELCL 81 10 IF(NPAR(6).LE.4) GO TO 20
ELCL 82 WRITE(6,3001)
ELCL 83 STOP
ELCL 84 20 IF(NPAR(3).EQ.0) NPAR(3) = 1
ELCL 85 IF(NPAR(5).EQ.0) NPAR(5) = 4
ELCL 86 IF(NPAR(6).EQ.0) NPAR(6) = 2
ELCL 87 IF(NPAR(7).EQ.0) NPAR(7) = 4
ELCL 88 IF(NPAR(8).EQ.0) NPAR(8) = 1
ELCL 89 IT = NPAR(4) + 1
ELCL 90 C
ELCL 91 WRITE(6,2001) NGR, (LABEL(I,IT), I=1,2), NPAR(2), NPAR(3), NPAR(5),
ELCL 92 1 CALL ADRES1 NPAR(6), NPAR(7), NPAR(8), NPAR(9)
ELCL 93 GO TO 50
ELCL 94 C
ELCL 95 C -----
ELCL 96 C ELEMENT GROUP 2
ELCL 97 C -----
ELCL 98 C
ELCL 99 C
ELCL 100 2 IF(NPAR(2).GT.0) GO TO 30
ELCL 101 STOP
ELCL 102 WRITE(6,3000)
ELCL 103 30 IF(NPAR(3).EQ.0) NPAR(3) = 1
ELCL 104 IF(NPAR(5).EQ.0) NPAR(5) = 1
ELCL 105 IT = NPAR(4) + 1
ELCL 106 WRITE(6,2002) NGR, (LABEL(I,IT), I=1,2), NPAR(2), NPAR(3), NPAR(5),
ELCL 107 CALL ADRES2
ELCL 108 C

```

```

SUBROUTINE ELCAL
COMMON /CNTRL/ NUMNP, NEG, MODEX, NPAR(10), NG, KBC
COMMON /DIM / N1, N2, N3, NA, NS, NG, NT, NB, NP, N10, N11, N12, N13, N14, N15
COMMON /ELSTOR/ NUNEST, MIDEST, MAXEST
COMMON /JUNK / HED(18), MLOT, NLINE
COMMON /WORK / NST(10), WORK(190)
COMMON /MOR/ A(1)
DIMENSION LABEL(2,2)
DATA LABEL/6HAXISYM,6HMETRIC,6HP L A ,6HN A R /
*****
THIS ROUTINE CALLS THE APPROPRIATE ELEMENT ROUTINES FOR READING,
GENERATING AND STORING THE ELEMENT DATA
TAPE 1 - STORES ELEMENT GROUP DATA
*****
TWO DIMENSIONAL FINITE ELEMENTS
NPAR(1) = 1
NPAR(2) = NUMBER OF TWO DIMENSIONAL ELEMENTS (NEL1)
NPAR(3) = NUMBER OF FIRST ELEMENT IN THIS GROUP (MFST)
NPAR(4) = ELEMENT TYPE CODE (ITYP2D)
EO,1, PLANAR
EO,1, AXISYMMETRIC
NPAR(5) = MAXIMUM NUMBER OF NODES (MXNODS)
NPAR(6) = NUMERICAL INTEGRATION ORDER (NINT)
NPAR(7) = NUMBER OF DIFFERENT MATERIALS (NUMAT)
NPAR(8) = MAX. NO. TEMPERATURE POINTS IN MATERIAL TABLE (MAXTP)
NPAR(9) = INTERNAL HEAT GENERATION FLAG (IHFLG)
*****
CONVECTION AND RADIATION ELEMENTS
NPAR(1) = 2
NPAR(2) = NUMBER OF CONVECTION BOUNDARY ELEMENTS (NEL2)
NPAR(3) = NUMBER OF FIRST ELEMENT IN THIS GROUP (MFST)
NPAR(4) = ELEMENT TYPE CODE (ITYP)

```



```

ELG1 1  SUBROUTINE ELG1 (X,Y,MHT,L,M,XY,IELT,NODS,MATP,NTC,TPROP,DENS,
ELG1 2  MFHG,HGSC,MXNODS,NDM,NODSI,M,MAXTP,NUMAT)
ELG1 3  C
ELG1 4  C
ELG1 5  C
ELG1 6  C
ELG1 7  C
ELG1 8  C
ELG1 9  C
ELG1 10 C
ELG1 11 C
ELG1 12 C
ELG1 13 C
ELG1 14 C
ELG1 15 C
ELG1 16 C
ELG1 17 C
ELG1 18 C
ELG1 19 C
ELG1 20 C
ELG1 21 C
ELG1 22 C
ELG1 23 C
ELG1 24 C
ELG1 25 C
ELG1 26 C
ELG1 27 C
ELG1 28 C
ELG1 29 C
ELG1 30 C
ELG1 31 C
ELG1 32 C
ELG1 33 C
ELG1 34 C
ELG1 35 C
ELG1 36 C
ELG1 37 C
ELG1 38 C
ELG1 39 C
ELG1 40 C
ELG1 41 C
ELG1 42 C
ELG1 43 C
ELG1 44 C
ELG1 45 C
ELG1 46 C
ELG1 47 C
ELG1 48 C
ELG1 49 C
ELG1 50 C
ELG1 51 C
ELG1 52 C
ELG1 53 C
ELG1 54 C
ELG1 55 C
ELG1 56 C
ELG1 57 C
ELG1 58 C
ELG1 59 C
ELG1 60 C
ELG1 61 C
ELG1 62 C
ELG1 63 C
ELG1 64 C
ELG1 65 C
ELG1 66 C
ELG1 67 C
ELG1 68 C
ELG1 69 C
ELG1 70 C

1 SUBROUTINE ELG1 (X,Y,MHT,L,M,XY,IELT,NODS,MATP,NTC,TPROP,DENS,
MFHG,HGSC,MXNODS,NDM,NODSI,M,MAXTP,NUMAT)
*****
INPUT INFORMATION FOR 4- TO 9-NODE ISOPARAMETRIC ELEMENTS
*****
DIMENSION X(11),Y(11),MHT(1),L(M,MXNODS,1),XY(NDM,1),IELT(1),
NODS(NDSIM,1),MATP(1),NTC(1),TPROP(MAXTP,5),NUMAT),
COMMON /CNTRL1/ NUMNP,NEG,MODEX,NPAR(10),NG,KBC
COMMON /JUNK / HED(18),MTOY,NLINE
COMMON /WORK / DUM(10),NOD(B),NODM(8),NODSM(8),WORK(166)
DIMENSION AST(2)
DATA AST/2H *2H */

NEL1 = NPAR(2)
MFST = NPAR(3)

*****
READ AND PRINT MATERIAL PROPERTY TABLE
*****

CALL TITLE (HED)
WRITE(6,2000) NG

DO 50 N=1,NUMAT
NTP = NTC(M)
IF(NTP.EQ.0) NTC(M) = 1
WRITE(6,2001) M,DENS(M),NTC(M),MFHG(M),HGSC(M)
IF(NTP.LE.MAXTP) GO TO 10
WRITE(6,3000)
STOP

READ TEMPERATURE DEPENDENT PROPERTIES
10 TOLD = -1.E+6
DO 20 K=1,NTP
READ (5,1001) (TPROP(K,J,M),J=1,5)
WRITE(6,2002) K,(TPROP(K,J,M),J=1,5)

TEMPERATURES MUST BE IN ASCENDING ORDER

IF(TPROP(K,1,M).GT.TOLD) GO TO 20
WRITE(6,3001)
STOP
20 CONTINUE

*****
READ AND GENERATE ELEMENT INFORMATION
*****

CALL TITLE (HED)
WRITE(6,2003) NG
WRITE(6,2004) (I,I=1,8)
NLINE = 10
N = N + J
IMEN = MFST
NLAST = MFST + NEL1 - 1
100 READ (5,1002) M,NOD,MTYP,IEL,KG
IF(MTYP.EQ.0) MTYP = 1
IF(IEL.EQ.0) IEL = MXNODS
IF(KG.EQ.0) KG = 1
IF(MXNODS.GE.IEL) GO TO 110
WRITE(6,3002) M
STOP

SUBROUTINE ELG1 (X,Y,MHT,L,M,XY,IELT,NODS,MATP,NTC,TPROP,DENS,
MFHG,HGSC,MXNODS,NDM,NODSI,M,MAXTP,NUMAT)
*****
INPUT INFORMATION FOR 4- TO 9-NODE ISOPARAMETRIC ELEMENTS
*****
DIMENSION X(11),Y(11),MHT(1),L(M,MXNODS,1),XY(NDM,1),IELT(1),
NODS(NDSIM,1),MATP(1),NTC(1),TPROP(MAXTP,5),NUMAT),
COMMON /CNTRL1/ NUMNP,NEG,MODEX,NPAR(10),NG,KBC
COMMON /JUNK / HED(18),MTOY,NLINE
COMMON /WORK / DUM(10),NOD(B),NODM(8),NODSM(8),WORK(166)
DIMENSION AST(2)
DATA AST/2H *2H */

NEL1 = NPAR(2)
MFST = NPAR(3)

*****
READ AND PRINT MATERIAL PROPERTY TABLE
*****

CALL TITLE (HED)
WRITE(6,2000) NG

DO 50 N=1,NUMAT
NTP = NTC(M)
IF(NTP.EQ.0) NTC(M) = 1
WRITE(6,2001) M,DENS(M),NTC(M),MFHG(M),HGSC(M)
IF(NTP.LE.MAXTP) GO TO 10
WRITE(6,3000)
STOP

READ TEMPERATURE DEPENDENT PROPERTIES
10 TOLD = -1.E+6
DO 20 K=1,NTP
READ (5,1001) (TPROP(K,J,M),J=1,5)
WRITE(6,2002) K,(TPROP(K,J,M),J=1,5)

TEMPERATURES MUST BE IN ASCENDING ORDER

IF(TPROP(K,1,M).GT.TOLD) GO TO 20
WRITE(6,3001)
STOP
20 CONTINUE

*****
READ AND GENERATE ELEMENT INFORMATION
*****

CALL TITLE (HED)
WRITE(6,2003) NG
WRITE(6,2004) (I,I=1,8)
NLINE = 10
N = N + J
IMEN = MFST
NLAST = MFST + NEL1 - 1
100 READ (5,1002) M,NOD,MTYP,IEL,KG
IF(MTYP.EQ.0) MTYP = 1
IF(IEL.EQ.0) IEL = MXNODS
IF(KG.EQ.0) KG = 1
IF(MXNODS.GE.IEL) GO TO 110
WRITE(6,3002) M
STOP

```

```

ELG1 71 C
ELG1 72 C
ELG1 73 C
ELG1 74 C
ELG1 75 C
ELG1 76 C
ELG1 77 C
ELG1 78 C
ELG1 79 C
ELG1 80 C
ELG1 81 C
ELG1 82 C
ELG1 83 C
ELG1 84 C
ELG1 85 C
ELG1 86 C
ELG1 87 C
ELG1 88 C
ELG1 89 C
ELG1 90 C
ELG1 91 C
ELG1 92 C
ELG1 93 C
ELG1 94 C
ELG1 95 C
ELG1 96 C
ELG1 97 C
ELG1 98 C
ELG1 99 C
ELG1 100 C
ELG1 101 C
ELG1 102 C
ELG1 103 C
ELG1 104 C
ELG1 105 C
ELG1 106 C
ELG1 107 C
ELG1 108 C
ELG1 109 C
ELG1 110 C
ELG1 111 C
ELG1 112 C
ELG1 113 C
ELG1 114 C
ELG1 115 C
ELG1 116 C
ELG1 117 C
ELG1 118 C
ELG1 119 C
ELG1 120 C
ELG1 121 C
ELG1 122 C
ELG1 123 C
ELG1 124 C
ELG1 125 C
ELG1 126 C
ELG1 127 C
ELG1 128 C
ELG1 129 C
ELG1 130 C
ELG1 131 C
ELG1 132 C
ELG1 133 C
ELG1 134 C
ELG1 135 C
ELG1 136 C
ELG1 137 C
ELG1 138 C
ELG1 139 C
ELG1 140 C

110 IF(M-IMEN) 290,120,200
SAVE ELEMENT INFORMATION FOR GENERATION OF ADDITIONAL ELEMENTS
120 DO 130 I=1,8
IF(IEL.EQ.0) GO TO 150
130 NODM(I)=NOD(I)
IF(I.EQ.0)
DO 140 I=5,8
NN=NOD(I)
IF(NN.EQ.0) GO TO 140
II=II + 1
NODSM(II)=I
140 CONTINUE
150 MTYP = MTYP
IELM = IEL
KAK = KG
ASTT = AST(1)
STORE PERMANENT ELEMENT INFORMATION
200 IZ = 0
DO 230 I=1,IELM
IF(I.LE.4) GO TO 210
JJ = NODSM(I-4)
II = NODM(JJ)
GO TO 220
210 II = NODM(I)
220 LM(I,N) = II
IZ = IZ + 2
XY(IZ-1,N) = X(II)
XY(IZ,N) = Y(II)
230 XY(IZ,N) = Y(II)
IELTN) = IELM
MATPN) = MTYP
IF(IELM.EQ.4) GO TO 250
NN=IELM - 4
DO 240 I=1,NN
240 NODSI(I,N)=NODSM(I)
UPDATE COLUMN HEIGHTS AND BANDWIDTH
250 CALL COLHT (MHT,IELM,L,M,N)
IF(NLINE.LT.55) GO TO 260
CALL TITLE (HED)
WRITE(6,2003) NG
WRITE(6,2004) (I,I=1,8)
NLINE = 10
260 WRITE(6,2005) ASTT,IMEN,NODM,MTYP,IELM
NLINE = NLINE + 1
IF(IMEN.EQ.NLAST) GO TO 300
N = N + J
IMEN = IMEN + 1
CHECK IF ELEMENT DATA IS TO BE STORED FOR CURRENT ELEMENT
IF(IMEN.EQ.N) GO TO 120
GENERATE NODE NUMBERS FOR NEXT ELEMENT
DO 270 I=1,8
IF(NODM(I).EQ.0) GO TO 270
NODM(I)=NODM(I)+KAK
270 CONTINUE

```









```

ADSK 21 10 MAXA(I+1) = MAXA(I) + MHT(I) + 1
ADSK 22 100 MA = MA + 1
ADSK 23 NWK = MAXA(NUMNP+1) - 1
ADSK 24 C RETURN
ADSK 25 END
ADSK 26

```

```

CLHT 12 100 CONTINUE
CLHT 13 C
CLHT 14 C COMPUTE COLUMN HEIGHT ABOVE DIAGONAL (ME) AND CHECK IF MAXIMUM
CLHT 15 C
CLHT 16 C
CLHT 17 C
CLHT 18 C
CLHT 19 C
CLHT 20 C
CLHT 21 C
CLHT 22 C
CLHT 23 C
CLHT 24 C

```

```

SUBROUTINE ASSEMK
*****
***** ASSEMBLE THE EFFECTIVE SYSTEM CONDUCTIVITY MATRIX (K*)
*****
COMMON /CNTRL1/ NUMNP, NEG, MODEX, NPAR(10), VG, KBC
COMMON /DIM / N1, N2, N3, N4, N5, N6, N7, N8, N9, N10, N11, N12, N13, N14, N15
COMMON /WORK / M1, M2, M3, M4, M5, M6, M7, M8, M9, M10, MDRK(110)
DIMENSION NST(110)
EQUIVALENCE (NST(1),M1)
REWIND 1
REWIND 2
LOOP OVER ALL ELEMENT GROUPS
DO 100 NG=1,NEG
READ (1) MIDEST,NPAR,NST,(A(1),I=1,MIDEST)
NGR = NPAR(1)
GO TO (1,2,3) NGR
-----
ELEMENT GROUP 1
-----
1 MKNODS = NPAR(5)
NUMAT = NPAR(7)
MAXTP = NPAR(8)
NDM = 2*MKNODS
NDSDIM = MKNODS-4
IF(NDSDIM.EQ.0) NDSDIM = 1
CALL COND1 (AIM1),A(M2),A(M3),A(M4),A(M5),A(M6),A(M7),A(M8),A(M9),
1 GO TO 100
MKNODS,NDM,NDSDIM,MAXTP,NUMAT)
-----
ELEMENT GROUP 2
-----
2 NPAR(5) = NUMAT
CALL COND2 (AIM1),A(M2),A(M3),A(M4),A(M5),A(M6),A(M7),A(M8),A(M9),NUMAT)
GO TO 100
-----
ELEMENT GROUP 3
-----
3 CALL COND3 (AIM1),A(M2),A(M5),A(M6))
100 CONTINUE
ASMK 57 C

```

```

ERR 1 C SUBROUTINE ERROR (N)
ERR 2 C
ERR 3 C WRITE(6,2000) N
ERR 4 C
ERR 5 C 2000 FORMAT(/'31H **ERROR** STORAGE EXCEEDED BY 16)
ERR 6 C STOP
END

```

```

TITL 1 SUBROUTINE TITLE (HED)
TITL 2 C
TITL 3 C DIMENSION HED(18)
TITL 4 C
TITL 5 C THIS ROUTINE PRINTS THE TITLE CARD AT TOP OF OUTPUT PAGE
TITL 6 C
TITL 7 C WRITE(6,2000) HED
TITL 8 C 2000 FORMAT('18H18A4,75X,8000 1976/')
TITL 9 C RETURN
TITL 10 C END

```

```

ADSK 1 SUBROUTINE ADRSK (MAXA,MHT,NUMNP,NWK,MA)
ADSK 2 C
ADSK 3 C *****
ADSK 4 C TO CALCULATE ADDRESSES OF DIAGONAL ELEMENTS IN A
ADSK 5 C Banded matrix whose column heights are known.
ADSK 6 C
ADSK 7 C MA = MAXIMUM BAND WIDTH
ADSK 8 C MHT = ACTIVE COLUMN HEIGHTS ABOVE DIAGONAL
ADSK 9 C MAXA = ADDRESSES OF DIAGONAL ELEMENTS
ADSK 10 C NWK = MAXIMUM STORAGE REQUIRED
ADSK 11 C *****
ADSK 12 C DIMENSION MAXA(1),MHT(1)
ADSK 13 C
ADSK 14 C MAXA(1) = 1
ADSK 15 C MAXA(2) = 2
ADSK 16 C MA = 0
ADSK 17 C IF (NUMNP.EQ.1) GO TO 100
ADSK 18 C DO 10 I=2,NUMNP
ADSK 19 C IF (MHT(I).GT.MA) MA = MHT(I)
ADSK 20 C

```

```

ADSK 21 10 MAXA(I+1) = MAXA(I) + MHT(I) + 1
ADSK 22 100 MA = MA + 1
ADSK 23 NWK = MAXA(NUMNP+1) - 1
ADSK 24 C RETURN
ADSK 25 END
ADSK 26

```

```

ERR 1 C SUBROUTINE ERROR (N)
ERR 2 C
ERR 3 C WRITE(6,2000) N
ERR 4 C
ERR 5 C 2000 FORMAT(/'31H **ERROR** STORAGE EXCEEDED BY 16)
ERR 6 C STOP
END

```

```

TITL 1 SUBROUTINE TITLE (HED)
TITL 2 C
TITL 3 C DIMENSION HED(18)
TITL 4 C
TITL 5 C THIS ROUTINE PRINTS THE TITLE CARD AT TOP OF OUTPUT PAGE
TITL 6 C
TITL 7 C WRITE(6,2000) HED
TITL 8 C 2000 FORMAT('18H18A4,75X,8000 1976/')
TITL 9 C RETURN
TITL 10 C END

```

```

ADSK 1 SUBROUTINE ADRSK (MAXA,MHT,NUMNP,NWK,MA)
ADSK 2 C
ADSK 3 C *****
ADSK 4 C TO CALCULATE ADDRESSES OF DIAGONAL ELEMENTS IN A
ADSK 5 C Banded matrix whose column heights are known.
ADSK 6 C
ADSK 7 C MA = MAXIMUM BAND WIDTH
ADSK 8 C MHT = ACTIVE COLUMN HEIGHTS ABOVE DIAGONAL
ADSK 9 C MAXA = ADDRESSES OF DIAGONAL ELEMENTS
ADSK 10 C NWK = MAXIMUM STORAGE REQUIRED
ADSK 11 C *****
ADSK 12 C DIMENSION MAXA(1),MHT(1)
ADSK 13 C
ADSK 14 C MAXA(1) = 1
ADSK 15 C MAXA(2) = 2
ADSK 16 C MA = 0
ADSK 17 C IF (NUMNP.EQ.1) GO TO 100
ADSK 18 C DO 10 I=2,NUMNP
ADSK 19 C IF (MHT(I).GT.MA) MA = MHT(I)
ADSK 20 C

```





```

SHP1 62 C INTERPOLATION FUNCTIONS AND LOCAL DERIVATIVES FOR MIDSIDE NODES
SHP1 63 C IF(NNDS.EQ.4) GO TO 50
SHP1 64 C
SHP1 65 C
SHP1 66 C
SHP1 67 C
SHP1 68 C
SHP1 69 C
SHP1 70 C
SHP1 71 C
SHP1 72 C
SHP1 73 C
SHP1 74 C
SHP1 75 C
SHP1 76 C
SHP1 77 C
SHP1 78 C
SHP1 79 C
SHP1 80 C
SHP1 81 C
SHP1 82 C
SHP1 83 C
SHP1 84 C
SHP1 85 C
SHP1 86 C
SHP1 87 C
SHP1 88 C
SHP1 89 C
SHP1 90 C
SHP1 91 C
SHP1 92 C
SHP1 93 C
SHP1 94 C
SHP1 95 C
SHP1 96 C
SHP1 97 C
SHP1 98 C
SHP1 99 C
SHP1 100 C
SHP1 101 C
SHP1 102 C
SHP1 103 C
SHP1 104 C
SHP1 105 C
SHP1 106 C
SHP1 107 C
SHP1 108 C
SHP1 109 C
SHP1 110 C
SHP1 111 C
SHP1 112 C
SHP1 113 C
SHP1 114 C
SHP1 115 C
SHP1 116 C
SHP1 117 C
SHP1 118 C
SHP1 119 C
SHP1 120 C
SHP1 121 C
SHP1 122 C
SHP1 123 C
SHP1 124 C
SHP1 125 C
SHP1 126 C
SHP1 127 C

2 I = I + 1
IF (I.GT.NNDS) GO TO 40
NN = NNDS(I) - 4
GO TO (5,6,7,8) NN

5 H(5) = 0.50*R2*SP
P(1,5) = -R*SP
P(2,5) = 0.50*R2
GO TO 2
6 H(6) = 0.50*R*M*S2
P(1,6) = -0.50*S2
P(2,6) = -R*M*S
GO TO 2
7 H(7) = 0.50*R2*SM
P(1,7) = -R*SM
P(2,7) = -0.50*R2
GO TO 2
8 H(8) = 0.50*R*P*S2
P(1,8) = 0.50*S2
P(2,8) = -R*P*S
GO TO 2

40 IM = 0
41 IM = IM + 1
IF(IM.GT.NNDS) GO TO 50
IN = NNDS(IM)
I1 = IM - 4
I2 = IPERM(I1)
H(I1) = H(I1) - 0.5*H(IM)
H(I2) = H(I2) - 0.5*H(IM)
H(IM+4) = H(IM)
DO 43 J=1,2
P(J,I1) = P(J,I1) - 0.5*P(J,IM)
P(J,I2) = P(J,I2) - 0.5*P(J,IM)
45 P(J,IM+4) = P(J,IM)
GO TO 41

C EVALUATE THE JACOBIAN MATRIX AT POINT (R,S)
50 DO 100 I=1,2
DO 100 J=1,2
SUM = 0.0
DO 90 K=1,NNDS
SUM = SUM + P(I,K)*XY(J,K)
90 SUM = SUM + P(I,K)*XY(J,K)
100 XJ(I,J) = SUM
C COMPUTE THE DETERMINANT OF THE JACOBIAN MATRIX AT POINT (R,S)
DETA = XJ(1,1)*XJ(2,2) - XJ(1,2)*XJ(2,1)
DUM = ABS(DETA)
IF(DUM.GT.1E-8) GO TO 500
WRITE (6,3000) NEL
STOP

3000 FORMAT('4SH **ERROR** ZERO JACOBIAN DETERMINANT FOR ELEMENT',I5)
500 RETURN
END

SUBROUTINE DERIV1 (XY,H,P,B,XJ,DETJ,RAD,ITYP2D)
*****
EVALUATION OF THE GLOBAL DERIVATIVE OPERATOR (B) AT A POINT (R,S)
FOR A QUADRILATERAL ELEMENT HAVING PLANAR OR AXISYMMETRIC GEOMETRY
*****
DIMENSION XY(2,1),H(1),P(2,1),B(2,1),XJ(2,2)
COMMON /TODIM / NEL,NNDS,MTYPE,NNDS
COMMON /WORK / DUM(145),XJ(2,2),WORK(51)
C COMPUTE INVERSE OF THE JACOBIAN MATRIX
DETJ = 1.0/DETJ
XJ(1,1) = XJ(2,2)*DETJ
XJ(1,2) = -XJ(1,2)*DETJ
XJ(2,1) = -XJ(2,1)*DETJ
XJ(2,2) = XJ(1,1)*DETJ
C EVALUATE GLOBAL DERIVATIVE OPERATOR ( B-MATRIX )
DO 10 K=1,NNDS
B(1,K) = XJ(1,1)*P(1,K) + XJ(1,2)*P(2,K)
10 B(2,K) = XJ(2,1)*P(1,K) + XJ(2,2)*P(2,K)
RAD = 1.0
IF(ITYP2D.NE.0) GO TO 500
C COMPUTE THE RADIUS AT POINT (R,S) FOR AXISYMMETRIC SOLID
RAD = 0.0
DO 50 K=1,NNDS
50 RAD = RAD + H(K)*XY(1,K)
IF(RAD.GT.1E-8) GO TO 500
WRITE (6,3000) NEL
STOP
3000 FORMAT('//50M **ERROR** ZERO RADIUS ENCOUNTERED IN ELEMENT NO.,I5)
500 RETURN
END

SUBROUTINE MATPR (TEM,EK,SP,T,PROP,NTP,MAXTP,KST)
*****
C COMPUTE THE TEMPERATURE DEPENDENT PROPERTIES AS A FUNCTION
OF THE KNOWN TEMPERATURE (TEM) AND MATERIAL TYPE, ASSUMING A
LINEAR VARIATION BETWEEN TEMPERATURES (T) LISTED IN THE TABLE
AND THE CORRESPONDING PROPERTIES (PROP) FOR EACH MATERIAL
*****
KST = -1 : K11(T),K22(T),K12(T)
KST = 0 : K11(T),K22(T),K12(T),C(T)
*****
DIMENSION EK(3),T(MAXTP),PPROP(MAXTP,4)
10 EK(1) = PROP(1,1)
EK(2) = PROP(1,2)
EK(3) = PROP(1,3)

```

```

MATP 22 IF(KST.EQ.-1) GO TO 100
MATP 23 SP = PROP(1,4)
MATP 24 GO TO 100
MATP 25 C
MATP 26 C CHECK TEMPERATURE BOUNDS
MATP 27 C
MATP 28 C 20 IF(ITEM.GE.T(1)) GO TO 30
MATP 29 WRITE(6,3000) TEM
MATP 30 STOP
MATP 31 30 IF(TEM.LE.T(NTP)) GO TO 40
MATP 32 WRITE(6,3000) TEM
MATP 33 STOP
MATP 34 40 IF(ITEM.EQ.T(1)) GO TO 10
MATP 35 C
MATP 36 DO 50 J=2,NTP
MATP 37 N = J - 1
MATP 38 IF(ITEM.GT.(NM).AND.TEM.LE.T(N)) GO TO 60
MATP 39 50 CONTINUE
MATP 40 C
MATP 41 C 60 DTEMP = T(N) - T(NM)
MATP 42 RATIO = (TEM-T(NM))/DTEMP
MATP 43 C
MATP 44 DO 70 I=1,3
MATP 45 70 EK(I) = PROP(NM,I) + RATIO*(PROP(N,I)-PROP(NM,I))
MATP 46 IF(KST.EQ.-1) GO TO 100
MATP 47 SP = PROP(NM,4) + RATIO*(PROP(N,4)-PROP(NM,4))
MATP 48 C
MATP 49 3000 FORMAT(/50H **ERROR** COMPUTED TEMPERATURE OUT OF RANGE FOR,
MATP 50 I 40H VALUES GIVEN IN MATERIAL TABLE .... T =,E10.3)
MATP 51 C
MATP 52 C 100 RETURN
MATP 53 END
MATP 54

```

```

CONZ 1 SUBROUTINE ADDC (A,SC,L,M,IEL)
CONZ 2 *****
CONZ 3 ADD ELEMENT HEAT CAPACITY TO GLOBAL LUMPED HEAT CAPACITY VECTOR
CONZ 4 *****
CONZ 5 C
CONZ 6 C DIMENSION A(1),SC(1),LM(1)
CONZ 7 C
CONZ 8 DO 100 I=1,IEL
CONZ 9 I=LM(I)
CONZ 10 100 A(I) = A(I) + SC(I)
CONZ 11 RETURN
CONZ 12 END
CONZ 13
CONZ 14

```

```

CONZ 1 SUBROUTINE COND2 (LM,XX,CL,MATP,NFH,PROP,NUMAT)
CONZ 2 *****
CONZ 3 MODIFY SYSTEM CONDUCTIVITY MATRIX (K*) FOR LINEAR CONVECTION BC
CONZ 4 *****
CONZ 5 C
CONZ 6 C DIMENSION LM(2,1),XX(2,1),CL(1),MATP(1),NFH(1),PROP(5,NUMAT)
CONZ 7 COMMON /CTRL1 / NUMNP,NEG,MODEX,NPAR(10),NC,KBC
CONZ 8 COMMON /CTRL2 / KST,ND,DT,START,TAMB,NPRINT,NTSREF,TIME,KP
CONZ 9 COMMON /DIM / N1,N2,N3,N4,N5,N6,N7,N8,N9,N10,N11,N12,N13,N14,N15
CONZ 10 COMMON /WORK / DUM(10),HK(2,2),WORK(100)
CONZ 11 COMMON A(1)
CONZ 12 NEL2 = NPAR(2)
CONZ 13 ITP = NPAR(4)
CONZ 14 DO 100 N=1,NEL2
CONZ 15 MT = MATP(N)
CONZ 16 NF = NFH(MT)
CONZ 17 IF(NF.NE.0) GO TO 100
CONZ 18 M = PROP(1,MT)
CONZ 19 HL = H*CL(N)
CONZ 20 FORM HK(2,2) FOR EACH LINEAR CONVECTION SURFACE ELEMENT
CONZ 21 IF(ITP.EQ.0) GO TO 30
CONZ 22 PLANAR SOLID CONVECTION BOUNDARY ELEMENTS
CONZ 23 HK(1,1) = HL/3.
CONZ 24 HK(1,2) = HL/6.
CONZ 25 GO TO 50
CONZ 26 C
CONZ 27 C AXISYMMETRIC SOLID CONVECTION BOUNDARY ELEMENTS
CONZ 28 C
CONZ 29 C 30 XI = XX(1,N)
CONZ 30 XJ = XX(2,N)
CONZ 31 HK(1,1) = XL*(XI + XJ)/4.
CONZ 32 HK(1,2) = HL*(XI + XJ)/12.
CONZ 33 C
CONZ 34 C 50 HK(2,2) = HK(1,1)
CONZ 35 HK(2,1) = HK(1,2)
CONZ 36 C
CONZ 37 C ASSEMBLE ELEMENT CONDUCTIVITY MATRIX INTO STRUCTURAL CCNDUCTIVITY
CONZ 38 CALL ADDBAN (A(N10),A(N9),HK,L,M(1,N),2)
CONZ 39 C
CONZ 40 C 100 CONTINUE
CONZ 41 C
CONZ 42 C
CONZ 43 C
CONZ 44 C
CONZ 45 C
CONZ 46 C
CONZ 47 C
CONZ 48 C
CONZ 49 C

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ADBN 1 SUBROUTINE ADDBAN (A,MAXA,S,LM,NDOF)
ADBN 2 *****
ADBN 3 ASSEMBLES ELEMENT CONDUCTIVITY INTO COMPACTED GLOBAL CONDUCTIVITY
ADBN 4 *****
ADBN 5 C
ADBN 6 C DIMENSION A(1),MAXA(1),S(1),LM(1)
ADBN 7 C
ADBN 8 DO 200 J=1,NDOF
ADBN 9 JJ = LM(J)
ADBN 10 MJ = MAXA(JJ)
ADBN 11 DO 200 I=1,NDOF
ADBN 12 II = LM(II)
ADBN 13 IJ = JJ - II
ADBN 14 IF(IJ) 200,100,100
ADBN 15 100 KK = MJ + IJ
ADBN 16 LS = (J-1)*NDOF + I
ADBN 17 AIKK = AIKK + S(LS)
ADBN 18 200 CONTINUE
ADBN 19 RETURN
ADBN 20 END
ADBN 21
ADBN 22

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CON2 50 RETURN
CON2 51 END

SUBROUTINE COND3 (LM,M,T3,TD)
*****
MODIFY SYSTEM CONDUCTIVITY MATRIX (K*) FOR COOLING PIPE EFFECTS
*****
DIMENSION LM(1),H(1),TB(1),TD(1)
COMMON /CNTRL1/ NUMNP,NEG,MODEX,NPAR(10),NG,KBC
COMMON /CNTRL2/ KST,NDT,DT,START,TAMB,NPRINT,NISREF,TIME,KP
COMMON /DIM / N1,N2,N3,N4,N5,N6,N7,N8,N9,N10,N11,N12,N13,N14,N15
COMMON A(1)
NEL3 = NPAR(2)
DO 100 N=1,NEL3
IF(TB(N).GT.TIME) GO TO 100
IF(TD(N).LE.TIME) GO TO 100
CALL ADDBAN (A(N10),A(N9),H(N),L(MN),1)
100 CONTINUE
RETURN
END

SUBROUTINE MODKTB (NOD,KODE,MAXA,XK,NNBC)
*****
MODIFY CONDUCTIVITY MATRIX FOR TEMPERATURE BOUNDARY CONDITIONS
*****
DIMENSION NOD(1),KODE(1),MAXA(1),XK(1)
DO 100 N=1,NNBC
IF(KODE(N).EQ.0) GO TO 100
NND=MOD(N)
NOI=MAXA(NND)
XK(NDI) = XK(NDI) + 1.0E+10
100 CONTINUE
RETURN
END

SUBROUTINE FOPWME (T,E,C,NUMNP)
*****
FORM THE THERMAL RESISTANCE VECTOR (E)
*****

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```

FRAME 7 C DIMENSION T(1),E(1),C(1)
FRAME 8 C
FRAME 9 C DO 10 I=1,NUMNP
FRAME 10 C 10 E(I) = C(I)*T(I)
FRAME 11 C
FRAME 12 C RETURN
FRAME 13 C END

SUBROUTINE COLSOL (A,V,MAXA,NN,MA,NWA,KKK)
*****
TO SOLVE SIMULTANEOUS EQUATIONS AX=V IN CORE, USING
COMPACTED STORAGE AND COLUMN REDUCTION SCHEME.
*****
A = MATRIX STORED IN COMPACTED FORM
V = VECTOR TO BE REDUCED
MAXA = VECTOR CONTAINING ADDRESSES OF DIAGONAL ELEMENTS OF A
FLAG FOR TRIANGULARIZATION (A=LU) AND/OR SIMPLE FORWARD
REDUCTION (LY=V) AND BACKSUBSTITUTION (UX=Y):
*****
DIMENSION A(NWA),V(1),MAXA(1)
MA1=MA - 1
IF (KKK-2) 100,700,800
*****
TRIANGULARIZATION
*****
100 IF(NN.EQ.1) GO TO 800
N=1
IF (A(1)) 80,85,110
80 WRITE (6,3000) N
STOP
85 WRITE (6,3001) N
STOP
110 DO 200 N=2,NN
KL=MAXA(N) + 1
KU=MAXA(N+1) - 1
IF (KU-KL) 200,210,210
210 B=0.
KN=MAXA(N)
K=N
DO 220 KK=KL,KU
K=K - 1
KI=MAXA(K)
C=A(KK)/A(KI)
B=B + C*A(KK)
220 A(KK)=C
A(KN)=A(KN) - R
IF (A(KN)) 222,224,226
222 WRITE (6,3000) N
STOP
224 WRITE (6,3001) N

```

COLS 1 C  
COLS 2 C  
COLS 3 C  
COLS 4 C  
COLS 5 C  
COLS 6 C  
COLS 7 C  
COLS 8 C  
COLS 9 C  
COLS 10 C  
COLS 11 C  
COLS 12 C  
COLS 13 C  
COLS 14 C  
COLS 15 C  
COLS 16 C  
COLS 17 C  
COLS 18 C  
COLS 19 C  
COLS 20 C  
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COLS 47 C  
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COLS 49 C  
COLS 50 C  
COLS 51 C  
COLS 52 C  
COLS 53 C  
COLS 54 C  
COLS 55 C  
COLS 56 C

```

COLS 57          STOP
COLS 58          M=MINO(MA1,NN-NJ)
COLS 59          IF (MR) 200,200I,228
COLS 60          MN=KU - AL * I
COLS 61          C
COLS 62          DO 240 J=1,MR
COLS 63          NJ=MAXA(NPJ,J)
COLS 64          IF (NJ) 240I,240I,230
COLS 65          NP=MINO(MN,NPJ)
COLS 66          C=0
COLS 67          K=KN + ND
COLS 68          IC=MJ - KN
COLS 69          DO 300 KK=KL,KU
COLS 70          C=C + A(KK)*K(K+IC)
COLS 71          A(KN+IC)=A(KN+IC) - C
COLS 72          CONTINUE
COLS 73          240
COLS 74          C
COLS 75          200 CONTINUE
COLS 76          IF (KK.EQ.0) RETURN
COLS 77          C
COLS 78          C
COLS 79          C
COLS 80          C
COLS 81          C
COLS 82          DO 400 N=2,NN
COLS 83          KL=MAXA(NJ) - 1
COLS 84          KU=MAXA(N+1) - 1
COLS 85          IF (KU-KL) 400,410,410
COLS 86          K=N
COLS 87          C=0
COLS 88          DO 420 KK=KL,KU
COLS 89          K=K - 1
COLS 90          C=C + A(KK)*V(K)
COLS 91          V(N)=V(N) - C
COLS 92          CONTINUE
COLS 93          GO TO 800
COLS 94          C
COLS 95          C
COLS 96          C
COLS 97          C
COLS 98          C
COLS 99          DO 480 N=1,NN
COLS 100          K=MAXA(N)
COLS 101          V(N)=V(N)/A(K)
COLS 102          IF (NN.EQ.1) RETURN
COLS 103          N=NN
COLS 104          DO 500 L=2,NN
COLS 105          KL=MAXA(N) + 1
COLS 106          KU=MAXA(N+1) - 1
COLS 107          IF (KU-KL) 500,510,510
COLS 108          K=N
COLS 109          DO 520 KK=KL,KU
COLS 110          K=K - 1
COLS 111          520 V(K)=V(K) - A(KK)*V(N)
COLS 112          N=N - 1
COLS 113          C
COLS 114          C
COLS 115          C
COLS 116          C
COLS 117          3000 FORMAT(//45H **STOP** STIFFNESS NOT POSITIVE DEFINITE.../)
COLS 118          1
COLS 119          3001 FORMAT(//733H **STOP** ZERO PIVOT IN POSITION I=)
COLS 120          RETURN
COLS 121          END

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FMQP 1           SUBROUTINE FORMQP (TFN, FN, NPTS, NDB, KODE, NFN, TO, O, NPTM1)
FMQP 2           C
FMQP 3           *****
FMQP 4           THIS ROUTINE FORMS THE PRESCRIBED FLUX VECTOR (Q) AT TIME (TIME)
FMQP 5           *****
FMQP 6           C
FMQP 7           DIMENSION TFN(NPTM1,1),FN(NPTM1,1),NPTS(1),NDB(1),KODE(1),
FMQP 8           NFN(1),TO(1),O(1)
FMQP 9           COMMON /CNTRL1/ NUMNP,NEG,MODEX,NPAR(10),NG,KBC
FMQP 10          COMMON /CNTRL2/ KST,NDT,DT,TSTART,TAMB,NPRINT,NTSREF,TIME,KP
FMQP 11          COMMON /NBC / NBC,NBCF,NPTM
FMQP 12          C
FMQP 13          INITIALIZE FLUX VECTOR (Q)
FMQP 14          DO 10 I=1,NUMNP
FMQP 15          Q(I) = 0.0
FMQP 16          C
FMQP 17          DO 50 N=1,NBC
FMQP 18          IF = MOD(N)
FMQP 19          NF = NFN(N)
FMQP 20          IF (NF.EQ.0) GO TO 20
FMQP 21          NPT = NPTS(NF)
FMQP 22          CALL INTERP (TFN(1,NF),FN(1,NF),NPT,TIME,VAL)
FMQP 23          20 IF (KODE(N).EQ.0) GO TO 40
FMQP 24          C
FMQP 25          C
FMQP 26          C
FMQP 27          C
FMQP 28          IF (NF.EQ.0) GO TO 30
FMQP 29          Q(I) = Q(I) + (1.0E+10)*TO(N)
FMQP 30          GO TO 50
FMQP 31          30 Q(I) = Q(I) + (1.0E+10)*TO(N)*VAL
FMQP 32          GO TO 50
FMQP 33          C
FMQP 34          C
FMQP 35          C
FMQP 36          C
FMQP 37          C
FMQP 38          C
FMQP 39          C
FMQP 40          C
FMQP 41          C
FMQP 42          C

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FMQC 1           SUBROUTINE FORMQC
FMQC 2           C
FMQC 3           *****
FMQC 4           THIS ROUTINE MODIFIES THE FLUX VECTOR (Q) FOR HEAT GENERATION,
FMQC 5           CONVECTION AND RADIATION BOUNDARIES AND COOLING PIPES
FMQC 6           *****
FMQC 7           C
FMQC 8           COMMON /CNTRL1/ NUMNP,NEG,MODEX,NPAR(10),NG,KBC
FMQC 9           COMMON /CNTRL2/ KST,NDT,DT,TSTART,TAMB,NPRINT,NTSREF,TIME,KP
FMQC 10          COMMON /DIM / N1,N2,N3,N4,N5,N6,N7,N8,N9,N10,N11,N12,N13,N14,N15
FMQC 11          COMMON /NBC / NBC,NBCF,NPTM
FMQC 12          COMMON /WORK / M1,M2,M3,M4,M5,M6,M7,M8,M9,M10,WORK(100)
FMQC 13          COMMON /A(1)
FMQC 14          DIMENSION NST(10)
FMQC 15          EQUIVALENCE (NST(1),M1)
FMQC 16          C
FMQC 17          REMIND 1
FMQC 18          REMIND 2
FMQC 19          C
FMQC 20          C
FMQC 21          C

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FQOC 22 C
FQOC 23 C
FQOC 24 C
FQOC 25 C
FQOC 26 C
FQOC 27 C
FQOC 28 C
FQOC 29 C
FQOC 30 C
FQOC 31 C
FQOC 32 C
FQOC 33 C
FQOC 34 C
FQOC 35 C
FQOC 36 C
FQOC 37 C
FQOC 38 C
FQOC 39 C
FQOC 40 C
FQOC 41 C
FQOC 42 C
FQOC 43 C
FQOC 44 C
FQOC 45 C
FQOC 46 C
FQOC 47 C
FQOC 48 C

DO 100 NGR=1,NEG
READ (1) MIDEST,NPAR,NST,(A(1),I=1,MIDEST)
NGR = NPAR(1)
GO TO (1,2,3) NGR
1 IFLAG = NPAR(9)
IF (IFLAG.EQ.0) GO TO 100
MKNODS = NPAR(5)
CALL FLUX1 (A(N1),A(N3),A(N5),A(N9),A(N10),A(N11),A(N12),A(N3),
A(N11),MKNODS,NPTM)
GO TO 100
2 NUMAT = NPAR(5)
CALL FLUX2 (A(N1),A(N2),A(N3),A(N4),A(N5),A(N6),A(N7),A(N8),A(N9),
A(N1),A(N2),A(N3),A(N4),A(N5),A(N6),A(N7),A(N8),A(N9),A(N10),
A(N11),A(N12),A(N13),A(N14),A(N15),A(N16),A(N17),A(N18),A(N19),
A(N20),A(N21),A(N22),A(N23),A(N24),A(N25),A(N26),A(N27),A(N28),
A(N29),A(N30),A(N31),A(N32),A(N33),A(N34),A(N35),A(N36),A(N37),
A(N38),A(N39),A(N40),A(N41),A(N42),A(N43),A(N44),A(N45),A(N46),
A(N47),A(N48),A(N49),A(N50),A(N51),A(N52),A(N53),A(N54),A(N55),
A(N56),A(N57),A(N58),A(N59),A(N60),A(N61),A(N62),A(N63),A(N64),
A(N65),A(N66),A(N67),A(N68),A(N69),A(N70),A(N71),A(N72),A(N73),
A(N74),A(N75),A(N76),A(N77),A(N78),A(N79),A(N80),A(N81),A(N82),
A(N83),A(N84),A(N85),A(N86),A(N87),A(N88),A(N89),A(N90),A(N91),
A(N92),A(N93),A(N94),A(N95),A(N96),A(N97),A(N98),A(N99),A(N100),
A(N101),A(N102),A(N103),A(N104),A(N105),A(N106),A(N107),A(N108),
A(N109),A(N110),A(N111),A(N112),A(N113),A(N114),A(N115),A(N116),
A(N117),A(N118),A(N119),A(N120),A(N121),A(N122),A(N123),A(N124),
A(N125),A(N126),A(N127),A(N128),A(N129),A(N130),A(N131),A(N132),
A(N133),A(N134),A(N135),A(N136),A(N137),A(N138),A(N139),A(N140),
A(N141),A(N142),A(N143),A(N144),A(N145),A(N146),A(N147),A(N148),
A(N149),A(N150),A(N151),A(N152),A(N153),A(N154),A(N155),A(N156),
A(N157),A(N158),A(N159),A(N160),A(N161),A(N162),A(N163),A(N164),
A(N165),A(N166),A(N167),A(N168),A(N169),A(N170),A(N171),A(N172),
A(N173),A(N174),A(N175),A(N176),A(N177),A(N178),A(N179),A(N180),
A(N181),A(N182),A(N183),A(N184),A(N185),A(N186),A(N187),A(N188),
A(N189),A(N190),A(N191),A(N192),A(N193),A(N194),A(N195),A(N196),
A(N197),A(N198),A(N199),A(N200),A(N201),A(N202),A(N203),A(N204),
A(N205),A(N206),A(N207),A(N208),A(N209),A(N210),A(N211),A(N212),
A(N213),A(N214),A(N215),A(N216),A(N217),A(N218),A(N219),A(N220),
A(N221),A(N222),A(N223),A(N224),A(N225),A(N226),A(N227),A(N228),
A(N229),A(N230),A(N231),A(N232),A(N233),A(N234),A(N235),A(N236),
A(N237),A(N238),A(N239),A(N240),A(N241),A(N242),A(N243),A(N244),
A(N245),A(N246),A(N247),A(N248),A(N249),A(N250),A(N251),A(N252),
A(N253),A(N254),A(N255),A(N256),A(N257),A(N258),A(N259),A(N260),
A(N261),A(N262),A(N263),A(N264),A(N265),A(N266),A(N267),A(N268),
A(N269),A(N270),A(N271),A(N272),A(N273),A(N274),A(N275),A(N276),
A(N277),A(N278),A(N279),A(N280),A(N281),A(N282),A(N283),A(N284),
A(N285),A(N286),A(N287),A(N288),A(N289),A(N290),A(N291),A(N292),
A(N293),A(N294),A(N295),A(N296),A(N297),A(N298),A(N299),A(N300),
A(N301),A(N302),A(N303),A(N304),A(N305),A(N306),A(N307),A(N308),
A(N309),A(N310),A(N311),A(N312),A(N313),A(N314),A(N315),A(N316),
A(N317),A(N318),A(N319),A(N320),A(N321),A(N322),A(N323),A(N324),
A(N325),A(N326),A(N327),A(N328),A(N329),A(N330),A(N331),A(N332),
A(N333),A(N334),A(N335),A(N336),A(N337),A(N338),A(N339),A(N340),
A(N341),A(N342),A(N343),A(N344),A(N345),A(N346),A(N347),A(N348),
A(N349),A(N350),A(N351),A(N352),A(N353),A(N354),A(N355),A(N356),
A(N357),A(N358),A(N359),A(N360),A(N361),A(N362),A(N363),A(N364),
A(N365),A(N366),A(N367),A(N368),A(N369),A(N370),A(N371),A(N372),
A(N373),A(N374),A(N375),A(N376),A(N377),A(N378),A(N379),A(N380),
A(N381),A(N382),A(N383),A(N384),A(N385),A(N386),A(N387),A(N388),
A(N389),A(N390),A(N391),A(N392),A(N393),A(N394),A(N395),A(N396),
A(N397),A(N398),A(N399),A(N400),A(N401),A(N402),A(N403),A(N404),
A(N405),A(N406),A(N407),A(N408),A(N409),A(N410),A(N411),A(N412),
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A(N1781),A(N1782),A(N1783),A(N1784),A(N1785),A(N1786),A(N1787),
A(N1788),A(N1789),A(N1790),A(N1791),A(N1792),A(N1793),A(N1794),
A(N1795),A(N1796),A(N1797),A(N1798),A(N1799),A(N1800),A(N1801),
A(N1802),A(N1803),A(N1804),A(N1805),A(N1806),A(N1807),A(N1808),
A(N1809),A(N1810),A(N1811),A(N1812),A(N1813),A(N1814),A(N1815),
A(N1816),A(N1817),A(N1818),A(N1819),A(N1820),A(N1821),A(N182
```

```

FLX2 57      Q(JJJ) = Q(JJJ) + QC
FLX2 58      GO TO 35
FLX2 59      C
FLX2 60      C
FLX2 61      C
FLX2 62      C
FLX2 63      C
FLX2 64      C
FLX2 65      C
FLX2 66      C
FLX2 67      C
FLX2 68      C
FLX2 69      C
FLX2 70      C
FLX2 71      C
FLX2 72      C
FLX2 73      C
FLX2 74      C
FLX2 75      C
FLX2 76      C
FLX2 77      C
FLX2 78      C
FLX2 79      C
FLX2 80      C
FLX2 81      C
FLX2 82      C
FLX2 83      C
FLX2 84      C
FLX2 85      C
FLX2 86      C
FLX2 87      C
FLX2 88      C
FLX2 89      C
FLX2 90      C
FLX2 91      C
FLX2 92      C
FLX2 93      C
FLX2 94      C
FLX2 95      C
FLX2 96      C
FLX2 97      C
FLX2 98      C
FLX2 99      C
FLX2 100     C
FLX2 101     C
FLX2 102     C

```

```

20 IF(TAVE,NE,T(1)) GO TO 30
H = HT(1)
GO TO 100
30 DO 50 J=2,NTP
N = J
NM = J - 1
IF(TAVE,GT,T(NM).AND.TAVE,LE,T(N)) GO TO 60
50 CONTINUE
60 DTEMP = T(N) - T(NM)
RATIO = (TAVE-T(NM))/DTEMP
H = HT(NM) + RATIO*(HT(N)-HT(NM))
3000 FORMAT(/,50H **ERROR** COMPUTED TEMPERATURE OUT OF RANGE FOR,
1 42H VALUES GIVEN IN CONVECTION TABLE .... T = E10.3)
100 RETURN
END

```

```

HPRP 18
HPRP 19
HPRP 20
HPRP 21 C
HPRP 22 C
HPRP 23 C
HPRP 24 C
HPRP 25 C
HPRP 26 C
HPRP 27 C
HPRP 28 C
HPRP 29 C
HPRP 30 C
HPRP 31 C
HPRP 32 C
HPRP 33 C
HPRP 34 C
HPRP 35 C
HPRP 36 C

```

```

AXISYMMETRIC SOLID CONVECTION BOUNDARY ELEMENTS
25 XI = XX(1,N)
AJ = XX(2,N)
OC = H*REF/6.
Q(11) = Q(11) + OC*(2.*XJ + XJ)
Q(22) = Q(22) + OC*(2.*XJ + XJ)
GO TO 35
30 TS = 0.5*(T(11) + T(JJJ))
TAVE = 0.5*(TE + TS)
COMPUTE TEMPERATURE DEPENDENT CONVECTION COEFFICIENT
NTP = NPTS(NFS)
CALL HPRP (TAVE,H,TFN(1,NFS),FM(1,NFS),NTP)
OC = 0.5*H*AH*KL*(TE - TS)
Q(11) = Q(11) + OC
Q(22) = Q(22) + OC
*****
RADIATION BOUNDARY CONDITIONS
*****
35 IF(V,GO,0.) GO TO 100
TS = 0.5*(T(11) + T(JJJ)) + TSHIFT
TS = TS*TS
TE = TE + TSHIFT
TE = TE*TE
TE = PROP(4,MTYP)
EF = PROP(5,MTYP)
OR = 0.5*SB*V*XL*(1./(1./EF + 1./ES - 1.))*(TE - TS)
Q(11) = Q(11) + OR
Q(22) = Q(22) + OR
100 CONTINUE
RETURN
END

```

```

SUBROUTINE HPROD (TAVE,M,T,HT,NTP)
*****
COMPUTE TEMPERATURE DEPENDENT CONVECTION COEFFICIENTS H(T)
*****
DIMENSION T(NTP),HT(NTP)
CHECK TEMPERATURE BOUNDS
IF(TAVE,GE,T(1)) GO TO 10
WRITE(6,3000) TAVE
STOP
10 IF(TAVE,LE,T(NTP)) GO TO 20
WRITE(6,3000) TAVE
STOP

```

```

HPRP 1
HPRP 2 C
HPRP 3 C
HPRP 4 C
HPRP 5 C
HPRP 6 C
HPRP 7 C
HPRP 8 C
HPRP 9 C
HPRP 10 C
HPRP 11 C
HPRP 12 C
HPRP 13 C
HPRP 14 C
HPRP 15 C
HPRP 16 C
HPRP 17 C

```

```

SUBROUTINE FLUX3 (LM,H,NFCP,TW,TB,TO,TFN,FM,NPTS,Q,NPTM)
*****
THIS ROUTINE MODIFIES FLUX VECTOR (Q) FOR COOLING PIPES
*****
DIMENSION LM(1),H(1),NFCP(1),TW(1),TB(1),TO(1),TFN(NPTM,1),
1 FM(NPTM,1),NPTS(1),Q(1)
COMMON /CNTRL/ NUMPD,NEG,MODEX,NPAR(10),NG,KSC
COMMON /CNTRL2/ KST,NDT,DT,TSTART,TAMB,NPRINT,NYSREF,TIME,KP
MEL3 = NPAR(2)
DO 100 N=1,NEL3
IF(TB(N),GT,TIME) GO TO 100
IF(YD(N),LE,TIME) GO TO 100
II = LM(N)
NF = NFCP(N)
IF(NF,EQ,0) GO TO 20
NPT = NPTS(NF)
CALL INTERP (TFN(1,NF),FM(1,NF),NPT,TIME,VAL)
20 IF(NF,EQ,0) VAL = 1.0
Q(II) = Q(II) + H(N)*T(N)*VAL
100 CONTINUE
RETURN
END

```

```

SUBROUTINE INTERP (TFN,FM,NPT,TIME,VAL)
*****
THIS ROUTINE INTERPOLATES A GIVEN TIME-DEPENDENT FUNCTION TO FIND
THE VALUE OF THE FUNCTION (VAL) AT A PARTICULAR TIME POINT (TIME)
*****
INTP 1 C
INTP 2 C
INTP 3 C
INTP 4 C
INTP 5 C
INTP 6 C
INTP 7 C
INTP 8 C

```

```

FLX3 1 C
FLX3 2 C
FLX3 3 C
FLX3 4 C
FLX3 5 C
FLX3 6 C
FLX3 7 C
FLX3 8 C
FLX3 9 C
FLX3 10 C
FLX3 11 C
FLX3 12 C
FLX3 13 C
FLX3 14 C
FLX3 15 C
FLX3 16 C
FLX3 17 C
FLX3 18 C
FLX3 19 C
FLX3 20 C
FLX3 21 C
FLX3 22 C
FLX3 23 C
FLX3 24 C
FLX3 25 C
FLX3 26 C
FLX3 27 C
FLX3 28 C
FLX3 29 C
FLX3 30 C

```

```

ITEM 1 C SUBROUTINE PTEMP (T,TIME,NUMNP)
ITEM 2 C *****
ITEM 3 C PUNCH THE NODAL POINT TEMPERATURES *****
ITEM 4 C *****
ITEM 5 C *****
ITEM 6 C *****
ITEM 7 C DIMENSION T(1)
ITEM 8 C
ITEM 9 C WRITE(3,2000) TIME
ITEM 10 C NCARD = NUMNP/4 + 1
ITEM 11 C NC = 0
ITEM 12 C
ITEM 13 C DO 100 I=1,NUMNP,4
ITEM 14 C NC = NC + 1
ITEM 15 C IP = I + 3
ITEM 16 C IF(NC.EQ.NCARD) IP = NUMNP
ITEM 17 C 100 WRITE(3,2001) (N,T(N),N=1,IP)
ITEM 18 C
ITEM 19 C 2000 FORMAT(35H NODAL POINT TEMPERATURES AT TIME = F11.4)
ITEM 20 C 2001 FORMAT(115,5X,F10.3)
ITEM 21 C
ITEM 22 C RETURN
ITEM 23 C END

```

```

INTP 8 C DIMENSION TFN(1),FN(1)
INTP 9 C
INTP 10 C DO 10 N=1,NPT
INTP 11 C DTIME = TFN(N) - TIME
INTP 12 C IF(DTIME.GT.0.) GO TO 15
INTP 13 C 10 CONTINUE
INTP 14 C
INTP 15 C 15 DIFF = TFN(N) - TFN(N-1)
INTP 16 C VAL = FN(N) - (FN(N) - FN(N-1))*DTIME/DIFF
INTP 17 C
INTP 18 C RETURN
INTP 19 C END

QEFF 1 C SUBROUTINE QEFF (J,E,NUMNP)
QEFF 2 C *****
QEFF 3 C FORM EFFECTIVE HEAT FLUX VECTOR (Q*) *****
QEFF 4 C *****
QEFF 5 C *****
QEFF 6 C *****
QEFF 7 C DIMENSION Q(1),E(1)
QEFF 8 C
QEFF 9 C DO 10 I=1,NUMNP
QEFF 10 C 10 Q(I) = 0.11 + E(I)
QEFF 11 C
QEFF 12 C RETURN
QEFF 13 C END

```

```

OUT 1 C SUBROUTINE OUT (T,NUMNP,TIME,KSTEP)
OUT 2 C *****
OUT 3 C PRINT NODAL TEMPERATURES FOR *TIME* *****
OUT 4 C *****
OUT 5 C *****
OUT 6 C *****
OUT 7 C DIMENSION T(1)
OUT 8 C
OUT 9 C WRITE(6,2000) KSTEP,TIME
OUT 10 C WRITE(6,2001) (N,T(N),N=1,NUMNP)
OUT 11 C
OUT 12 C FORMAT STATEMENTS
OUT 13 C
OUT 14 C 2000 FORMAT(320H TEMPERATURES AT TIME STEP =I5,ZX,7H TIME =E11.4,1H)/
OUT 15 C 2001 FORMAT(16,E11.6)
OUT 16 C
OUT 17 C RETURN
OUT 18 C END

```

```

PNOD 1 C SUBROUTINE PNODE (X,Y,NUMNP)
PNOD 2 C *****
PNOD 3 C PUNCH THE NODAL POINT COORDINATE DATA *****
PNOD 4 C *****
PNOD 5 C *****
PNOD 6 C *****
PNOD 7 C DIMENSION X(1),Y(1)
PNOD 8 C
PNOD 9 C WRITE(3,2000)
PNOD 10 C NCARD = NUMNP/3 + 1
PNOD 11 C NC = 0
PNOD 12 C
PNOD 13 C DO 100 I=1,NUMNP,3
PNOD 14 C NC = NC + 1
PNOD 15 C IP = I + 2
PNOD 16 C IF(NC.EQ.NCARD) IP = NUMNP
PNOD 17 C 100 WRITE(3,2001) (N,X(N),Y(N),N=1,IP)
PNOD 18 C
PNOD 19 C 2000 FORMAT(24H NODAL POINT COORDINATES)
PNOD 20 C 2001 FORMAT(3I5,2F10.3)
PNOD 21 C
PNOD 22 C RETURN
PNOD 23 C END

```



APPENDIX B1  
DETECT USER'S MANUAL

PROGRAM IDENTIFICATION

DETECT: Determination of Temperatures in Construction.  
A Two Dimensional Heat Transfer Program for  
Structures of Arbitrary Geometry Constructed  
Incrementally. Version I, February 1976.

Developed by: R. M. Polivka and E. L. Wilson  
University of California, Berkeley

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  - III. Nodal Point Coordinates
  - IV. Boundary Condition Functions
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  - VI. Element Specification
    - Type 1: Two Dimensional Finite Elements
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    - A. Lift Data Control Card
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### B1.1 PROGRAM DESCRIPTION

The computer program DETECT performs the steady state or transient heat transfer analysis of two dimensional planar or axisymmetric structures of arbitrary geometry constructed incrementally. The program was developed primarily for the purpose of evaluating the temperature distribution during the construction of mass concrete structures such as dams, foundations and bridge piers. The solution is based on a finite element technique, and includes the effects of such time-dependent boundary conditions as convective surface heat transfer (insulation forms), nodal temperature or heat flux specifications, internal heat generation and artificial cooling by means of embedded pipes. Material nonlinearities such as temperature dependent thermal conductivity or heat capacity are neglected.

The program is completely general, and is applicable to structures composed of a combination of element types and materials. The present version contains the following element types:

1. Two dimensional 4- to 8-node planar or axisymmetric solid elements.
2. Convection boundary elements.
3. Cooling pipe elements.

### B1.2 PROGRAM CAPACITY

The computer program DETECT uses variable dimensioning in order to make optimum use of available high speed storage. The element data for each group of elements is stored in a block and transferred to disc storage. The required core storage remaining is dynamically allocated into a single array A in blank common.

The program capacity can be controlled by the user through the two fortran statements in the main program of DETECT:

```
COMMON (n)
```

```
MTOT = n
```

The total memory  $n$  required can be changed depending on the size of the problem to be solved. The minimum value of  $n$  needed is given by

$$n = M_{\max} + 2*NPTM*NBCF + NBCF + 4*NNBC + 8*NUMNP + NWK + 1$$

where

$M_{\max}$  = Maximum storage required for element group data

NPTM = Maximum number of time points used to describe any of the boundary condition functions

NBCF = Number of boundary condition functions

NNBC = Number of nodal point boundary conditions

NUMNP = Number of nodes

NWK = Working storage required for conductivity matrix. Approximate by  $MB*NUMNP$  where  $MB$  = maximum bandwidth.

$M_{\max}$  is the maximum value of  $M$  for each of the three element types used in the analysis:

(a) Type 1 - Planar or axisymmetric elements

$$M_1 = 4*MXNODS*NEL1 + 7*NUMAT$$

NEL1 = Number of elements in group 1

NUMAT = Number of material types

MXNODS = Maximum number of nodes defining any element

(b) Type 2 - Convection boundary elements

$$M_2 = 9 * NEL2$$

NEL2 = Number of elements in group 2

(c) Type 3 - Cooling pipe elements

$$M_3 = 6 * NEL3$$

NEL3 = Number of elements in group 3

If the value of n is set too small, an error message is printed which gives the amount by which the storage was exceeded and the program execution is terminated.



### B1.3 PROGRAM INPUT DATA

The following sections describe the necessary sequence of cards which define a given structure to be analyzed.

#### I. PROBLEM INITIATION AND TITLE (A5,3X,18A4) - One card

Columns	Variable	Description
1 - 5	MODE	Problem initiation flag. Punch the word START.
6 - 8	--	Blank
9 - 80	HED	Problem title for labeling output.

#### II. MASTER CONTROL CARD (5I5) - One card

Columns	Variable	Description
1 - 5	NUMNP	Total number of nodal points in structure.
6 - 10	NEG	Number of element groups. See Note 1.
11 - 15	NLT	Total number of layers (time spans) in the structure. Specify (a) Zero or blank: defaults to 1. See Note 2.
16 - 20	NUMEST	Estimated maximum number of high speed storage locations $M_{max}$ required to store each set of element group data. Specify (a) Zero or blank: defaults to 4000.
21 - 25	MODEX	Execution mode. Specify (a) Zero or blank: data check only. (b) 1: execution.

#### NOTE

- (1) An element group is a series of elements of a particular type (e.g. 2/D axisymmetric, 2/D planar, convection etc.). Elements of the same type may also be split into more than one group.
- (2) NLT determines the number of card sets to be read in Section VIII.
  - (a) For a structure constructed incrementally, NLT represents the number of lifts in the structure.
  - (b) For the transient analysis of an already existing structure, NLT represents the number of time span data changes in either the time step increment (DT), the number of solution time steps (NDT) or the output print interval (NPRINT).
  - (c) For the steady state analysis of an already existing structure, NLT must equal 1.

### III. NODAL POINT COORDINATES (I5,5X,2F10.0,I5,I1)

As many cards as needed to generate NUMNP nodal points.

Columns	Variable	Description
1 - 5	N	Node number. See Note 1.
6 - 10	--	Blank
11 - 20	X(N)	X coordinate
21 - 30	Y(N)	Y coordinate
31 - 35	KN	Node number difference between successive generated nodes (given on first card in a sequence). Specify (a) Zero or blank: No generation. See Note 2.
36	JPR	Print suppression flag (on card for node 1 only). Specify (a) Zero or blank: No suppression. (b) 1: Suppress ordered list of node coordinates. See Note 3.

#### NOTE

- (1) Node cards need not be in numerical order. Eventually, however, all nodes from 1 to the total number of nodes (NUMNP) must be identified.
- (2) The mesh generation parameter KN must appear on the first card of a series of nodal points to be generated. The intermediate nodes to be generated between nodes N1 and N2 will be located at equal intervals along the straight line joining the two nodes. KN is the increment to be added to the previous node number. The node difference N2-N1 must be evenly divisible by KN.
- (3) JPR is used to eliminate the second printing of the ordered node coordinates. The JPR character is entered on the card for node 1 only.

IV. BOUNDARY CONDITION FUNCTIONS

A. CONTROL INFORMATION (3I5) - One card

Columns	Variable	Description
1 - 5	NBCF	Number of boundary condition functions. See Note 1.
6 - 10	NPTM	Maximum number of points used to describe any one of the functions. See Note 2.
11 - 15	NNBC	Number of nodal point heat flow or temperature boundary conditions. See Note 3.

NOTE

- (1) NBCF determines the number of card sets to be read in Section IV.B.
- (2) NPTM is the maximum number of  $[f(t),t]$  pairs used to define any one of the NBCF functions. At least two points are required to input any one function, and no function may be input with more than NPTM points.
- (3) NNBC determines the number of cards to be read or generated in Section V.

B. TIME FUNCTION DATA - NBCF sets of cards

Each set consists of a control card followed by as many cards as needed to define the function.

1. CONTROL CARD (2I5) - First card of set.

Columns	Variable	Description
1 - 5	NC	Function number. (GE.1 and LE.NBCF) See Note 1.
6 - 10	NPTS(NC)	Number of time points used to describe this function. (GE.2 and LE.NPTM)

2. [f(t),t] DATA (8F10.0) - Remaining cards of set.

As many cards as needed to define NPTS(NC) pairs of points [TFN(NC,I),FN(NC,I)], four pairs per card. See Note 2.

Columns	Variable	Description
1 - 10	TFN(NC,1)	Time at point 1 : $t_1$
11 - 20	FN (NC,1)	Function value at point 1 : $f(t_1)$
21 - 30	TFN(NC,2)	Time at point 2 : $t_2$
31 - 40	FN (NC,2)	Function value at point 2 : $f(t_2)$
41 - 50	TFN(NC,3)	} Point 3
51 - 60	FN (NC,3)	
61 - 70	TFN(NC,4)	} Point 4
71 - 80	FN (NC,4)	

NEXT CARD(S) - If required

1 - 10	TFN(NC,5)	Time at point 5 : $t_5$
11 - 20	FN (NC,5)	Function value at point 5 : $f(t_5)$
...	...	...

NOTE

- (1) Time functions need not be input in order of increasing function number NC.

- (2) The function tables input in this section are used to prescribe time-dependent boundary conditions such as environmental or nodal point temperatures and nodal point heat flows. The functions may also be used to describe the rate of internal heat generation and the variation of convection coefficient  $H$  with temperature.

Time values at successive points must increase in magnitude. Values of the functions at times (temperatures) other than  $TFN(NC,I)$  are calculated within the program using linear interpolation.

The first time point  $TFN(NC,1)$  must be less than or equal to the time at solution start ( $PLTIME$  for layer 1) and the final time point  $TFN(NC,NPTS(NC))$  must be greater than or equal to the time at the end of solution (the sum of  $NDT*DT$  for all of the layers).

V. NODAL POINT BOUNDARY CONDITIONS (4I5,F10.0,I5) - NNBC cards

Columns	Variable	Description
1 - 5	N	Boundary condition number. See Note 1.
6 - 10	NOD(N)	Global node number. (GE.1 and LE.NUMNP)
11 - 15	KODE(N)	Boundary condition type. Specify (a) Zero or blank : Externally supplied heat flux Q. (b) 1: Prescribed temperature T.
16 - 20	NFN(N)	Function number. (GE.0 and LE.NBCF) See Note 2.
21 - 30	TQ(N)	Boundary value amplitude. Specify (a) Heat flux (KODE(N) = 0). (b) Temperature (KODE(N) = 1). See Note 3.
31 - 35	KN	Node number difference between successive generated nodes (on first card in sequence). See Note 4.

NOTE

- (1) All nodal points not specified in this section are assumed to have externally supplied heat flux of zero for all values of time.
- (2) A function number equal to zero or blank means that the prescribed boundary condition is applied at time zero and remains constant for all time greater than zero (step function). The functions assigned in this section must have been defined previously in Section IV. A given function can be used to describe any number of boundary conditions.
- (3) (a) For the case of flux or temperature boundary conditions which are not step functions, TQ(N) represents a function multiplier used to scale NFN(N) values for all time t.  
(b) For the case of flux or temperature boundary conditions applied as a step function from time zero, TQ(N) represents the actual value of prescribed flux or temperature.
- (4) In the printout of nodal point boundary conditions, all generated node data are prefixed by an asterisk. For use of the generation parameter KN, see Note 2, Section III.

## VI. ELEMENT SPECIFICATION

Elements must be divided into "groups". Input as many blocks of data in the following sections as there are element groups (NEG). An element group is a series of elements of a particular type, and elements of the same type may also be divided into more than one group.

Element groups may be input in any order. The elements in any group must be numbered sequentially starting from the number of the first element as specified on the element group control card.

The following types of element groups may be used:

### Type 1 - Two Dimensional Finite Elements

These are 4- to 8-node isoparametric elements which must be input in the global X-Y plane. When the element is used to represent an axisymmetric solid, the global Y-axis is the axis of revolution.

### Type 2 - Convection Boundary Surface Elements

These are 2-node planar or axisymmetric solid boundary elements which must be input in the global X-Y plane.

### Type 3 - Cooling Pipe Elements

These are 1-node elements which are placed at existing nodal points in the finite element mesh. The axis of the cooling pipe is the Z-axis.

TYPE 1 - TWO DIMENSIONAL FINITE ELEMENTSA. CONTROL INFORMATION (8I5) - One card

Columns	Variable	Description
1 - 5	NGR	Element group indicator. Punch the number "1".
6 - 10	NEL1	Number of elements in this group.
11 - 15	MFST	Element number of first element in group. (a) Zero or blank: defaults to 1. See Note 1.
16 - 20	ITYP2D	Element type code. Specify (a) Zero or blank: axisymmetric (b) 1: planar
21 - 25	MXNODS	Maximum number of nodes used to describe any one element. Specify (a) Zero or blank: defaults to 4. (GE.4 and LE.8)
26 - 30	NINT	Numerical integration order to be used in Gaussian quadrature. Specify (a) Zero or blank: defaults to 2. (GE.2 and LE.4) See Note 2.
31 - 35	NUMAT	Number of material property sets. Specify (a) Zero or blank: defaults to 1.
36 - 40	IHFLG	Internal heat generation flag. Specify (a) Zero or blank: No internal heat generation. (b) 1: Internal heat generation exists.

NOTE

- (1) Element numbers need not begin with number 1 if MFST is specified.
- (2) For rectangular elements, an integration order of 2 is sufficient. If the element is distorted, a higher integration order need be used.



B. MATERIAL PROPERTY INFORMATION (I5,5X,7F10.0) - One card

Columns	Variable	Dimension
1 - 5	M	Material identification number. (GE.1 and LE.NUMAT)
6 - 10	--	Blank
11 - 20	PROP(1)	Thermal conductivity $k_{11}$ .
21 - 30	PROP(2)	Thermal conductivity $k_{22}$ .
31 - 40	PROP(3)	Thermal conductivity $k_{12}$ .
41 - 50	PROP(4)	Thermal heat capacity $c$ .
51 - 60	PROP(5)	Density of material $\rho$ . See Note 1.
61 - 70	PROP(6)	Function number describing the rate of internal heat generation (input as a floating point number). See Note 2.
71 - 80	PROP(7)	Internal heat generation function multiplier.

NOTE

- (1) Consistent units must be used for specification of material properties.
- (2) If no internal heat generation exists, i.e. if IHFLG equals zero, leave columns 61-80 blank. For the case where internal heat generation is considered, the functions PROP(6) assigned in this section must have been defined previously in Section IV. See Note 2, Section V.

C. ELEMENT DATA (12I5,2F10.0)

As many cards as needed to generate NEL1 elements.

Columns	Variable	Description
1 - 5	M	Element number. See Note 1.
6 - 10	NOD(1)	Global node number of element node 1.
11 - 15	NOD(2)	Global node number of element node 2.
16 - 20	NOD(3)	Global node number of element node 3.
21 - 25	NOD(4)	Global node number of element node 4.
26 - 30	NOD(5)	Global node number of element node 5.
31 - 35	NOD(6)	Global node number of element node 6.
36 - 40	NOD(7)	Global node number of element node 7.
41 - 45	NOD(8)	Global node number of element node 8. See Note 2.
46 - 50	MTYP	Material identification number. Specify (a) Zero or blank: defaults to 1. (GE.1 and LE.NUMAT)
51 - 55	IEL	Number of nodes used to describe element. (a) Zero or blank: defaults to MXNODS.
56 - 60	KG	Node number increment for element generation (given on first card in a sequence). (a) Zero or blank: defaults to 1. See Note 3.
61 - 70	TBTH	Time of element birth. See Note 4.
71 - 80	TDTH	Time of element death. Specify (a) Zero or blank: defaults to 10 <sup>10</sup> . See Note 4.

NOTE

- (1) All elements must be input in increasing numerical order, starting with element number MFST. Cards for the first and last element must be included.

- (2) The number of nodes in element M is defined by IEL. For elements containing less than eight nodes (IEL.LT.8), input a zero or blank in NOD(I) for the particular node locations not used. As an example, for a 6-node element (IEL.EQ.6) with nodes 5 and 7 not used, the element node number array would be  $NOD(I) = [X \ X \ X \ X \ 0 \ X \ 0 \ X]$  where the nonzero entries (X) are the global node numbers of the 6 nodes.

Figure VI-1 defines the mapping between the node numbering in the local r-s coordinate system and the global X-Y coordinate system. Nodes 1 through 4 are located at the four corners in a counterclockwise sense, and nodes 5 through 8 are located at the midsides of the element.

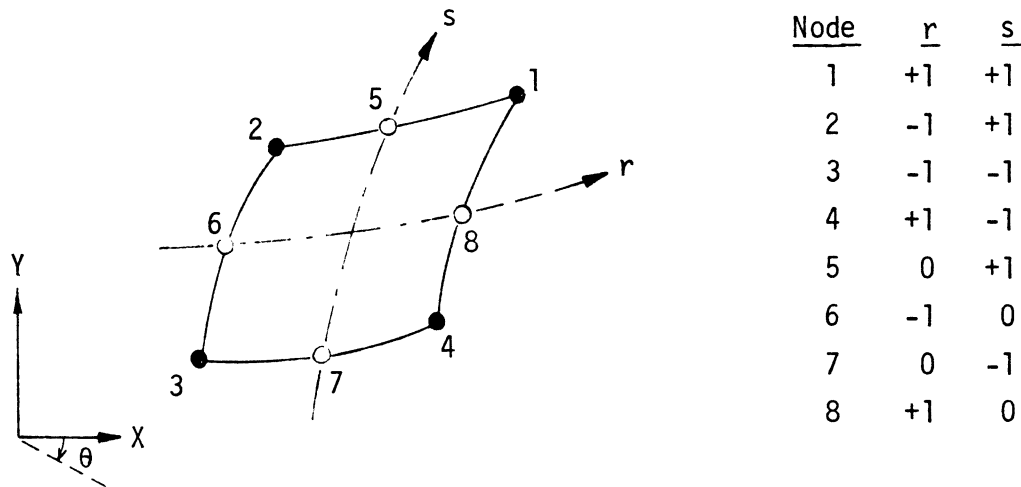


FIG. VI-1 TWO DIMENSIONAL FINITE ELEMENT NODE NUMBER INPUT SEQUENCE

- (3) The node generation parameter KG must appear on the first element card of a sequence, and is used to compute the node numbers for a group of missing elements.

If data for elements  $[M+1, M+2, \dots, M+J]$  are omitted, these "J" missing elements are generated using the same values for material number (MTYP) and number of nodes (IEL) as given on the preceding card for element M, and the node numbers for the successive "J" elements are incremented by the value KG given on the M-th element card. Only the nonzero node numbers appearing on the M-th element card are incremented when generating missing element data.

In the printout of the element data, generated elements are prefixed by an asterisk.

- (4) It is assumed that the structure does not exist at time zero. During the analysis, elements can be either added to or removed from the structure. The variables TBTH and TDTH define the time of element creation or deletion.

If the geometry of the structure does not change with time, TBTH must be set equal to the time at solution start (PLTIME) and TDTH must be either set greater than or equal to the time at the end of solution ( $NDT*DT$ ) or left blank.

TYPE 2 - CONVECTION BOUNDARY ELEMENTSA. CONTROL INFORMATION (4I5) - One card

Columns	Variable	Description
1 - 5	NGR	Element group indicator. Punch the number "2".
6 - 10	NEL2	Number of elements in this group.
11 - 15	MFST	Element number of first element in group. (a) Zero or blank: defaults to 1. See Note 1.
16 - 20	ITYP	Element type code. Specify (a) Zero or blank : axisymmetric solid boundary element. (b) 1: Planar solid boundary element.

NOTE

- (1) Element numbers need not begin with number 1 if MFST is specified.

B. ELEMENT DATA (3I5,F10.0,2I5,3F10.0)

As many cards as needed to generate NEL2 elements.

Columns	Variable	Description
1 - 5	M	Convection surface number. See Note 1.
6 - 10	NOD(1)	Global node number of element node I.
11 - 15	NOD(2)	Global node number of element node J. See Note 2.
16 - 25	HC	Convection coefficient.
26 - 30	NFC	Function number describing the environmental temperature variation with time. See Note 3.
31 - 35	KG	Node number increment for element generation (given on first card in a sequence). (a) Zero or blank: defaults to 1. See Note 4.
36 - 45	TEXT	Environmental temperature function multiplier. See Note 3.
46 - 55	TBTH	Time of element birth. See Note 5.
56 - 65	TDTH	Time of element death (time when insulation surface element is to be removed). Specify (a) Zero or blank: defaults to $10^{10}$ . See Note 5.

NOTE

- (1) All elements must be input in ascending numerical order, starting with element number MFST. Cards for the first and last element must be included.
- (2) Convection boundary elements are 2-node elements on the surface of a planar or axisymmetric solid, as shown in Figure VI-2.
- (3) The variation of environmental temperature with time is computed using  $T_e(t) = \text{TEXT} * \text{NFC}$  where the function number NFC has been defined previously in Section IV. If the environmental temperature does not change with time, input NFC equal to zero or blank and  $\text{TEXT} = T_0$ , constant for all time greater than or equal to zero.

- (4) The node generation parameter KG must be given on the first element card prior to a group of missing elements. All generated elements will have the same element data as that given on the first element card in the sequence. In the printout of the element data, generated elements are prefixed by an asterisk.
- (5) It is assumed that the structure does not exist at time zero. During the analysis, convection boundary elements (insulation forms) can be either added to or removed from the structure. The variables TBTH and TDTH define the time of element creation or deletion.

If the geometry of the structure does not change with time, TBTH must equal PLTIME and TDTH must be either set greater than or equal to  $NDT \cdot DT$  or left blank.

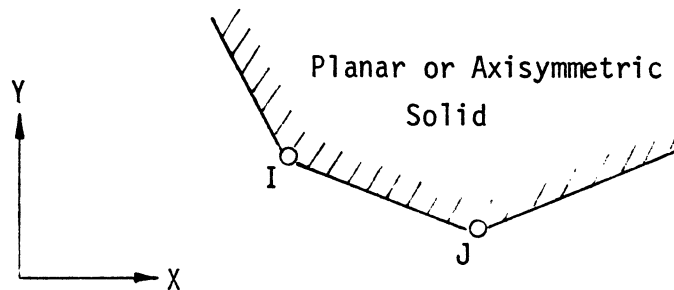


FIG. VI-2 CONVECTION BOUNDARY SURFACE ELEMENTS

TYPE 3 - COOLING PIPE ELEMENTSA. CONTROL INFORMATION (3I5) - One card

Columns	Variable	Description
1 - 5	NGR	Element group indicator. Punch the number "3".
6 - 10	NEL3	Number of elements in this group.
11 - 15	MFST	Element number of first element in group. (a) Zero or blank: defaults to 1. See Note 1.

B. ELEMENT DATA (2I5,F10.0,2I5,3F10.0)

As many cards as needed to generate NEL3 elements.

Columns	Variable	Description
1 - 5	M	Element number. See Note 1.
6 - 10	NOD	Global node number of cooling pipe location.
11 - 20	HP	Empirical constant. See Note 2.
21 - 25	NFC	Function number describing the cooling water temperature variation with time. See Note 3.
26 - 30	KG	Node number increment for element gener- ation (given on first card in a sequence). See Note 4.
31 - 40	TWTR	Cooling water temperature function multiplier. See Note 3.
41 - 50	TBTH	Time at initiation of cooling.
51 - 60	TDTH	Time when cooling is to be stopped.

NOTE

- (1) Element numbers need not begin with number 1 if MFST is specified. All elements must be input in increasing numerical order starting with element MFST. The first and last element cards must be included.



- (2) The rate at which heat is removed from the solid by a cooling pipe is given by:

$$q = HP(T_w - T_o)$$

where

$T_w$  = temperature of the cooling water.

$T_o$  = apparent temperature on the outer surface of the pipe at node NOD in the finite element solution.

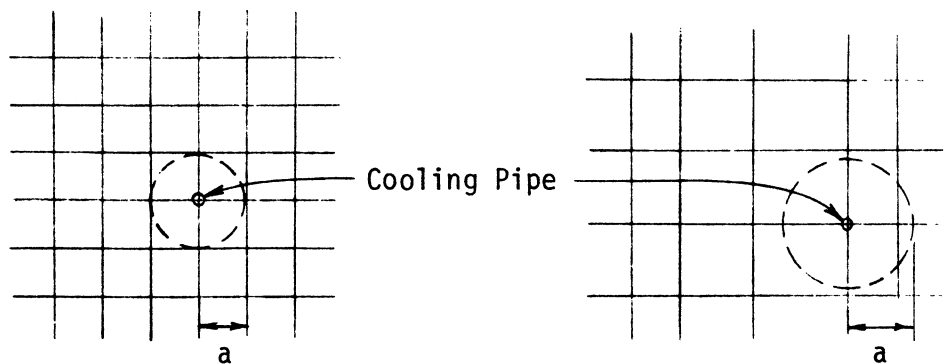
$$HP = \frac{2\pi k}{\ln\left(\frac{a}{R}\right) - 2}, \text{ an empirical constant.}$$

where

$k$  = average conductivity of finite elements adjacent to the cooling pipe.

$R$  = radius of cooling pipe.

$a$  = weighted distance to adjacent node.  
(See Figure VI-3)



(i) Regular Mesh

(ii) Irregular Mesh

FIG. VI-3 DETERMINATION OF 'a' IN EQUATION FOR HP

- (3) If the cooling water temperature  $T_w$  is time-dependent, then a nonzero function number NFC must be specified. If the cooling water temperature  $T_w$  does not change with time, then input NFC equal to zero or blank and TWTR =  $T_o$ , constant for all time greater than zero (step function).
- (4) The node generation parameter KG must appear on the first element card of a sequence, and is used to compute node numbers for missing elements. All data for generated elements is taken to be the same as that given on the first element card in the sequence. In the printout of the element data, all generated elements are prefixed by an asterisk.

VII. SOLUTION TIME SPAN DATA - NLT sets of cards

A. LIFT DATA CONTROL CARD (2I5,3F10.0,2I5) - First card of set.

Columns	Variable	Description
1 - 5	KST	Code for steady state or transient analysis. (a) -1: Steady state analysis. (b) Zero or blank: Transient analysis.
6 - 10	NDT	Number of solution time steps. Specify (a) Zero or blank: defaults to 1.
11 - 20	DT	Time step increment to be used in time span.
21 - 30	PLTIME	Time at beginning of time span.
31 - 40	PLACET	Placement temperature for all elements placed at the beginning of this time span.
41 - 45	ICON	Initial condition flag. Specify (a) Zero or blank: Nodal temperatures of all new elements placed during this time span set automatically to the placement temperature. (b) $n > 0$ : Nodal temperatures of all new elements which differ from the placement temperature (PLACET) are read from data cards.  See Note 1.
46 - 50	NPRINT	Time interval for printout of nodal temperatures, expressed as a multiple of the integration time step. Specify (a) Zero or blank: defaults to 1.

B. INITIAL CONDITIONS (4(I5,5X,E10.0)) - Remaining card(s) of set.

As many cards as needed to specify n nodal temperatures (four values per card) which are not equal to the placement temperature. Omit if the initial condition flag ICON equals zero or blank.

Columns	Variable	Description
1 - 5	ND	Node number.
11 - 20	T(ND)	Temperature.
. . .	. . .	. . .

NOTE

- (1) ICON is used to control the card reading in Section VII.B. For ICON equal to zero, resume input beginning in Section VIII.

VIII. NEW PROBLEM DATA

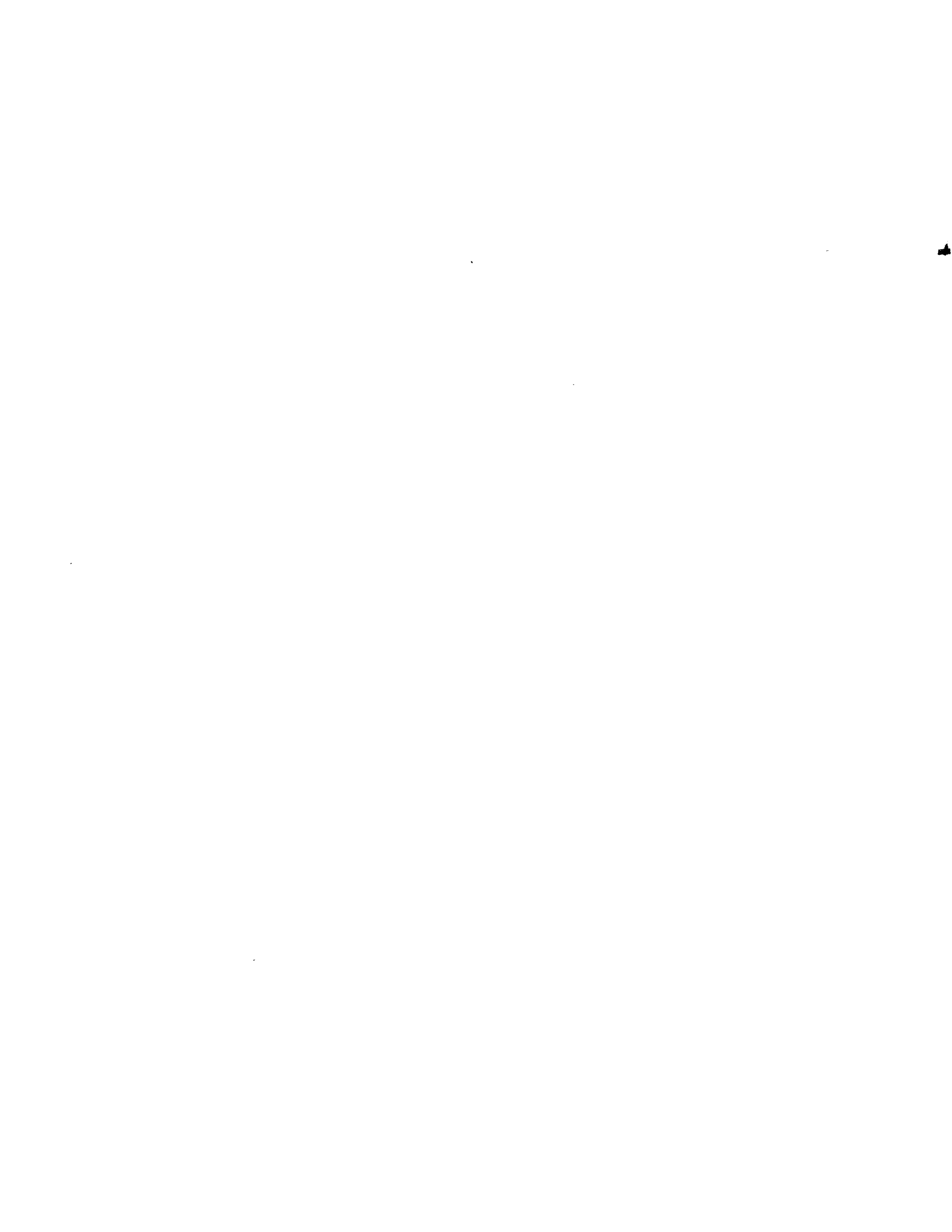
A completely new problem may now be solved by starting with Section I. Any number of heat transfer problems may be solved within a single computer run.

IX. TERMINATION CARD (A4) - One card

Columns	Variable	Description
1 - 4	MODE	Problem(s) termination flag. Punch the word STOP.

APPENDIX B2

DETECT FORTRAN IV LISTING



```

DETC 1 1
DETC 2 2
DETC 3 3
DETC 4 4
DETC 5 5
DETC 6 6
DETC 7 7
DETC 8 8
DETC 9 9
DETC 10 10
DETC 11 11
DETC 12 12
DETC 13 13
DETC 14 14
DETC 15 15
DETC 16 16
DETC 17 17
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DETC 19 19
DETC 20 20
DETC 21 21
DETC 22 22
DETC 23 23
DETC 24 24
DETC 25 25
DETC 26 26
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DETC 32 32
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DETC 66 66
DETC 67 67
DETC 68 68
DETC 69 69
DETC 70 70

PROGRAM DETECT (INPUT,OUTPUT,TAPES=INPUT,TAPES=OUTPUT,TAPE1,TAPE2,
TAPES)
1
*****
DETECT - DETERMINATION OF TEMPERATURES IN CONSTRUCTION.
A LINEAR TWO DIMENSIONAL HEAT TRANSFER ANALYSIS PROGRAM FOR
STRUCTURES OF ARBITRARY GEOMETRY CONSTRUCTED INCREMENTALLY
DEVELOPED BY - R.H. POLIVKA AND E.L. WILSON , FEBRUARY, 1976
*****
COMMON /CNTRL1/ NUMNP,NEG,NLT,MODEX,NPAR(10),NG
COMMON /CNTRL2/ KST,NDT,DT,PLTIME,PLACET,NPRINT,TIME
COMMON /DIM / N1,N2,N3,N4,N5,NG,N7,N8,N9,N10,N11,N12,N13,N14,N15
COMMON /ELSTOR/ NUNEST,MIDEST,MAREST,NELT
COMMON /JUNK / HED(18),RTOT,MLINE
COMMON /ABC / NNBC,NSCT,NPTH
COMMON /WORK / WORK(200)
COMMON /10000/
200
WTOT = 10000
MAXEST = 0
*****
INPUT PHASE
*****
PROGRAM MASTER CONTROL DATA
CALL DETI
INPUT ELEMENT INFORMATION
CALL ELCAL
*****
SOLUTION PHASE
*****
*****
BLANK COMMON STORAGE ALLOCATION
*****
ARRAY -----DESCRIPTION-----
N1 TFN TIME VALUES AT POINTS DIMENSION
N2 FN FUNCTION VALUES AT POINTS NPT#*NBSCF
N3 NPTS NUMBER OF FUNCTION INPUT POINTS NBSCF
N4 NOD NODES HAVING PRESCRIBED BC NNBC
N5 KODE BOUNDARY CONDITION TYPES NNBC
N6 NFN BC FUNCTION NUMBERS NNBC
N7 TO BOUNDARY VALUE AMPLITUDES NNBC
N8 B NODAL TEMPERATURES (IC) NUMNP
N9 T NODAL TEMPERATURES (SOLUTION) NUMNP
N10 ID BC CODE FOR ACTIVE/DELETED JOF NUMNP
N11 MHT ACTIVE COLUMN HEIGHTS NUMNP+1
N12 XAAA ADDRESSES OF KK DIAGONAL ELEMENTS NUMNP
N13 XK EFFECTIVE CONDUCTIVITY MATRIX NUMNP
N14 J EXTERNALLY SUPPLIED HEAT FLUXES NUMNP
N15 C EFFECTIVE HEAT CAPACITY VECTOR NUMNP
N16 E THERMAL RESISTANCE VECTOR NUMNP
*****
SHIFT STORAGE TO ELIMINATE NODAL COORDINATE DATA
I = 1 + MAXEST
*****
DETC 71 N10M = N10 - 1
DETC 72 DO 5 J=N3,N10M
DETC 73 A(IJ) = A(J)
DETC 74
DETC 75 S I = 1 + I
DETC 76
DETC 77 N1 = 1 + MAXEST
DETC 78 N2 = N1 + NOT#NBSCF
DETC 79 N3 = N2 + NOT#NBSCF
DETC 80 N4 = N3 + NBSCF
DETC 81 N5 = N4 + NNBC
DETC 82 N6 = N5 + NNBC
DETC 83 N7 = N6 + NNBC
DETC 84 N8 = N7 + NNBC
DETC 85 N9 = N8 + NUMNP
DETC 86 N10 = N9 + NUMNP
DETC 87 N11 = N10 + NUMNP
DETC 88 N12 = N11 + NUMNP
DETC 89 N13 = N12 + NUMNP + 1
DETC 90 C TIME = 0.0
DETC 91 NLAY = 0
DETC 92
DETC 93
DETC 94 READ SOLUTION TIME SPAN DATA
DETC 95
DETC 96
DETC 97 300 NLAY = NLAY + 1
DETC 98 IF(NLAY.GT.NLT) GO TO 200
DETC 99 C
DETC 100 READ (5,1000) KST,NDT,DT,PLTIME,PLACET,ICON,NPRINT
DETC 101 C
DETC 102 IF(NDT .EQ.0) NOT
DETC 103 IF(NPRINT.EQ.0) NPRINT = 1
DETC 104 CALL TITLE (MHD)
DETC 105 WRITE(6,2000) NLAY,KST,NDT,DT,PLTIME,PLACET,ICON,NPRINT
DETC 106 IF(INDEX.EQ.0) GO TO 200
DETC 107 C
DETC 108 SET INITIAL TEMPERATURE VECTOR (B) TO PLACEMENT TEMPERATURE
DETC 109 C
DETC 110 NOM = N9 - 1
DETC 111 DO 10 I=N8,NOM
DETC 112 10 A(I) = PLACET
DETC 113 C
DETC 114 DEFINE INITIAL TEMPERATURES OTHER THAN PLACEMENT TEMPERATURE
DETC 115 C
DETC 116 IF(ICON.EQ.0) GO TO 15
DETC 117 C
DETC 118 CALL INITIAL (A(N8),ICON)
DETC 119 C
DETC 120 15 IF(NLAY.EQ.1) GO TO 20
DETC 121 C
DETC 122 MOVE (IOLD) INTO INITIAL CONDITION VECTOR (B). ALL NEW NODES
DETC 123 ARE NOW SET TO PLACET AND CONTACT SURFACE TO (IOLD).
DETC 124 C
DETC 125 CALL MOVETB (A(N8),A(N9),A(N10),NUMNP,1)
DETC 126 C
DETC 127 NUMBER EQUATIONS IN COMPACTED FORM
DETC 128 C
DETC 129 20 CALL IDENT (A(N10),NUMNP,NELT,PLTIME,NEQ)
DETC 130 C
DETC 131 MOVE IC VECTOR (B) INTO SOLUTION TEMPERATURE VECTOR (T)
DETC 132 C
DETC 133 CALL MOVETB (A(N9),A(N9),A(N10),NUMNP,2)
DETC 134 C
DETC 135 COMPUTE ACTIVE COLUMN HEIGHTS
DETC 136 C
DETC 137 CALL SKY (A(N10),A(N11),NUMNP,NELT,PLTIME)
DETC 138 C
DETC 139 COMPUTE ADDRESSES OF DIAGONAL ELEMENTS IN (KK)
DETC 140 C

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```

DETC 141 C CALL ADRSK (A(N12),A(N11),NEQ,NWK,MB)
DETC 142 C
DETC 143 C
DETC 144 C
DETC 145 C
DETC 146 C
DETC 147 C
DETC 148 C
DETC 149 C
DETC 150 C
DETC 151 C
DETC 152 C
DETC 153 C
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DETC 155 C
DETC 156 C
DETC 157 C
DETC 158 C
DETC 159 C
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DETC 166 C
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DETC 170 C
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DETC 206 C
DETC 207 C
DETC 208 C
DETC 209 C
DETC 210 C

CALL ADRSK (A(N12),A(N11),NEQ,NWK,MB)
N14 = N13 + NWK
N15 = N14 + NUMNP
N16 = N15 + NUMNP
N17 = N16 + NUMNP
IF(KST.EQ.-1) N17 = N15
IF(N17.GT.MTOT) CALL ERROR (N17-MTOT)
INITIALIZE CONDUCTIVITY MATRIX (K*)
N14M = N14 - 1
DO 25 I=N13,N14M
  A(I) = 0.0
INITIALIZE EFFECTIVE HEAT CAPACITY VECTOR (C)
IF(KST.EQ.-1) GO TO 35
N16M = N16 - 1
DO 30 I=N15,N16M
  A(I) = 0.0
ASSEMBLE THE EFFECTIVE SYSTEM CONDUCTIVITY MATRIX (K*)
35 CALL ASSEK
IF(NBC.EQ.0) GO TO 40
MODIFY CONDUCTIVITY MATRIX FOR TEMPERATURE BOUNDARY CONDITIONS
CALL MODKTB (A(N4),A(N5),A(N10),A(N12),A(N13),NNBC)
40 IF(KST.EQ.-1) GO TO 45
FORM THE INITIAL RESISTANCE VECTOR AT TIME ZERO, E(0)
E(0) = [C*]T(0)
CALL FORME (A(N9),A(N16),A(N15),NEQ)
TRIANGULARIZE THE EFFECTIVE CONDUCTIVITY MATRIX, (K*)
CALL COLSOL (A(N13),A(N14),A(N12),NEQ,MB,NWK,KTR)
45 KTR = 0
INITIALIZE THE TIME STEP COUNTER
KSTEP = 0
*****
TIME MARCHING LOOP
*****
100 KSTEP = KSTEP + 1
TIME = TIME + DT
DEFINE EXTERNALLY SUPPLIED HEAT FLUX VECTOR (Q) FOR THIS TIME STEP
INITIALIZE HEAT FLOW VECTOR (Q)
N15M = N15 - 1
DO 50 I=N14,N15M
  A(I) = 0.0
IF(NBC.EQ.0) GO TO 55
PRESCRIBED (Q)
CALL FORMOP (A(N1),A(N2),A(N3),A(N5),A(N6),A(N7),A(N10),
  A(N14),NPTM)
1

```

```

DETC 211 C CONVECTIVE AND INTERNAL HEAT GENERATION (Q)
DETC 212 C
DETC 213 C
DETC 214 C
DETC 215 C
DETC 216 C
DETC 217 C
DETC 218 C
DETC 219 C
DETC 220 C
DETC 221 C
DETC 222 C
DETC 223 C
DETC 224 C
DETC 225 C
DETC 226 C
DETC 227 C
DETC 228 C
DETC 229 C
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DETC 264 C
DETC 265 C
DETC 266 C
DETC 267 C
DETC 268 C
DETC 269 C
DETC 270 C
DETC 271 C
DETC 272 C
DETC 273 C

55 CALL FORMQ
IF(KST.EQ.-1) GO TO 60
COMPUTE EFFECTIVE HEAT FLUX VECTOR
Q*(TIME) = Q*(TIME) + E*(TIME-1)
CALL DEFF (A(N14),A(N16),NEQ)
SOLVE THE HEAT EQUILIBRIUM EQUATIONS FOR THE SYSTEM TEMPERATURES
T*(TIME) = [K*(TRI)](Q*(TIME))
60 KTR=2
CALL COLSOL (A(N13),A(N14),A(N12),NEQ,MB,NWK,KTR)
Q-VECTOR IS NOW T-VECTOR, SET T(I)=Q(I), I=1,NEQ
DO 65 I=1,NEQ
  IT = N9 + I - 1
  IO = N14 + I - 1
  65 A(IT) = A(IO)
PRINT NODAL TEMPERATURE DISTRIBUTION, IF REQUESTED, AT THIS STEP
K = MOD(KSTEP,NPRINT)
IF(K.NE.0) GO TO 70
CALL OUT (A(N9),A(N10),NUMNP,TIME,KSTEP,NEQ)
COMPUTE THE NEW THERMAL RESISTIVITY VECTOR (E)
70 IF(KST.EQ.-1) GO TO 80
CALL FORME (A(N9),A(N16),A(N15),NEQ)
CHECK FOR FINAL TIME STEP
80 IF(KSTEP.LT.MDT) GO TO 100
READ CONTROL DATA FOR NEXT TIME SPAN
GO TO 300
FORMAT STATEMENTS
1000 FORMAT(2I5,3F10.0,2I5)
2000 FORMAT(3A(1H#)/3I# SOLUTION TIME SPAN DATA, LAYER,13/3A(1H#)///
1 48H CODE FOR STEADY STATE, TRANSIENT ANALYSIS = 15/
2 35H EQ. -1, STEADY STATE ANALYSIS//
3 32H EQ. 0, TRANSIENT ANALYSIS//
4 48H NUMBER OF SOLUTION TIME STEPS ..... = 15/
5 48H SOLUTION TIME STEP INCREMENT ..... = F10.4//
6 48H TIME AT SOLUTION START ..... = F10.4//
7 48H PLACEMENT TEMPERATURE ..... = F10.4//
8 48H INITIAL CONDITION CODE (ICOM) ..... = 15/
9 45H EQ. 0, INITIAL CONDITIONS FOR NEW LAYER/
A 41H SET TO PLACEMENT TEMPERATURE/
B 47H EQ. 1, INITIAL CONDITIONS READ FROM CARDS//
C 48H OUTPUT PRINT INTERVAL ..... = 15//)
END

```





```

COORD 9 C COMMON /JUNK / HED(18),MTOT,NLINE
COORD 10 C WRITE(6,2000)
COORD 11 C WRITE(6,2001)
COORD 12 C NLINE = NLINE + 12
COORD 13 C NOLD = 0
COORD 14 C
COORD 15 C
COORD 16 C 10 READ (5,1000) N,X(N),Y(N),KN,JPR
COORD 17 C IF(N.EQ.1) IPR=JPR
COORD 18 C IF(NLINE.LT.55) GO TO 15
COORD 19 C CALL TITLE (HED)
COORD 20 C WRITE(6,2001)
COORD 21 C NLINE = 10
COORD 22 C
COORD 23 C 15 WRITE(6,2002) N,X(N),Y(N),KN
COORD 24 C NLINE = NLINE + 1
COORD 25 C IF(NOLD.EQ.0) GO TO 30
COORD 26 C
COORD 27 C CHECK IF GENERATION IS REQUIRED
COORD 28 C
COORD 29 C IF(KNOLD.EQ.0) GO TO 30
COORD 30 C NUM = (N-NOLD)/KNOLD
COORD 31 C NUMN = NUM - 1
COORD 32 C RNUM = NUM
COORD 33 C DX = (X(N)-X(NOLD))/RNUM
COORD 34 C DY = (Y(N)-Y(NOLD))/RNUM
COORD 35 C K = NOLD
COORD 36 C DD 20 J=1,NUMN
COORD 37 C KK = K
COORD 38 C K = K + KNOLD
COORD 39 C X(K) = X(KK) + DX
COORD 40 C Y(K) = Y(KK) + DY
COORD 41 C
COORD 42 C 20 NOLD = N
COORD 43 C KNOLD = KN
COORD 44 C IF(M-NUMN) GO TO 10
COORD 45 C
COORD 46 C IF(IPR.EQ.1) GO TO 20
COORD 47 C
COORD 48 C PRINT ALL NODAL POINT DATA
COORD 49 C
COORD 50 C CALL TITLE (HED)
COORD 51 C WRITE(6,2003)
COORD 52 C NLINE = 9
COORD 53 C NROW = NUMN/3 + 1
COORD 54 C NR = C
COORD 55 C
COORD 56 C DO 100 I=1,NUMN/3
COORD 57 C NR = NR + 1
COORD 58 C IP = I + 2
COORD 59 C IF(NR.EQ.NROW) IP = NUMN
COORD 60 C IF(NLINE.LT.55) GO TO 50
COORD 61 C CALL TITLE (HED)
COORD 62 C WRITE(6,2003)
COORD 63 C NLINE = 9
COORD 64 C 50 WRITE(6,2004) (N,X(N),Y(N),N=I,IP)
COORD 65 C 100 NLINE = NLINE + 1
COORD 66 C
COORD 67 C FORMAT STATEMENTS
COORD 68 C
COORD 69 C 1000 FORMAT(15X,2F10.0,15,11)
COORD 70 C 2000 FORMAT(28(1H#)/28H NODAL POINT COORDINATE DATA/28(1H#)/)
COORD 71 C 2001 FORMAT(19(1H#)/19H A INPUT NODE DATA/19(1H#)///)
COORD 72 C 1 4X,4HNODE,5X,7HX-COORD,5X,7HY-COORD,5X,4HDIFF/)
COORD 73 C 2002 FORMAT(3X,15,2F12.3,3X,15)
COORD 74 C 2003 FORMAT(23(1H#)/23H B GENERATED NODE DATA/23(1H#)///)
COORD 75 C 1 3(4X,4HNODE,5X,7HX-COORD,5X,7HY-COORD,5X)///)
COORD 76 C 2004 FORMAT(3(3X,15,2F12.3,5X))
COORD 77 C
COORD 78 C 200 RETURN
END

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COORD 79 END
COORD 80 C
COORD 81 C SUBROUTINE FUNC (TFN,FN,NPTS,NPTM1)
COORD 82 C *****
COORD 83 C DEFINE ALL BOUNDARY CONDITION FUNCTIONS
COORD 84 C *****
COORD 85 C DIMENSION TFN(NPTM1,1),FN(NPTM1,1),NPTS(1)
COORD 86 C COMMON /JUNK / HED(18),MTOT,NLINE
COORD 87 C COMMON /NBC / MNBC,NBCF,NPTM
COORD 88 C COMMON /WORK / FORM(4),WORK(196)
COORD 89 C
COORD 90 C WRITE(6,2001)
COORD 91 C NLINE = NLINE + 3
COORD 92 C
COORD 93 C DO 100 L=1,NBCF
COORD 94 C READ (5,1000) NC,NPTS(NC)
COORD 95 C WRITE(6,2002) NC,NPTS(NC)
COORD 96 C NLINE = NLINE + 1
COORD 97 C IF(NPTS(NC).GE.2.AND.NPTS(NC).LE.NPTM) GO TO 20
COORD 98 C STOP
COORD 99 C
COORD 100 C READ TIME FUNCTION VERSUS TIME TABLE
COORD 101 C 20 NT = NPTS(NC)
COORD 102 C READ (5,1001) (TFNK(NC),FN(K,NC),K=1,NT)
COORD 103 C
COORD 104 C CHECK THAT TIME POINTS ARE IN INCREASING ORDER
COORD 105 C
COORD 106 C TOLD = -1.
COORD 107 C DO 30 K=1,NT
COORD 108 C IF(TFN(K,NC).GT.TOLD) GO TO 30
COORD 109 C WRITE(6,3001)
COORD 110 C STOP
COORD 111 C 30 TOLD = TFNK(NC)
COORD 112 C
COORD 113 C DO 50 K=1,NT
COORD 114 C IF(NLINE.LT.55) GO TO 40
COORD 115 C CALL TITLE (HED)
COORD 116 C WRITE(6,2000)
COORD 117 C NLINE = 10
COORD 118 C 40 WRITE(6,2003) K,TFN(K,NC),FN(K,NC)
COORD 119 C 50 NLINE = NLINE + 1
COORD 120 C
COORD 121 C 100 CONTINUE
COORD 122 C
COORD 123 C FORMAT STATEMENTS
COORD 124 C
COORD 125 C 1000 FORMAT(2I5)
COORD 126 C 1001 FORMAT(8F10.0)
COORD 127 C 2000 FORMAT(25(1H#)/25H TIME DEPENDENT FUNCTIONS/25(1H#)///)
COORD 128 C 2001 FJRMAT(4A,8HFUNTION,4X,9HNUMBER OF,6X,10HTIME POINT,4X,4HTIME,
COORD 129 C 1 4X,5HVALUE,5X,5HVALUE/)
COORD 130 C 2 5X,5HVALUE,5X,5HVALUE/)
COORD 131 C 2002 FORMAT(4X,15,2F12.3)
COORD 132 C 2003 FORMAT(31X,15,2F12.3)
COORD 133 C 3000 FORMAT(//49H **ERROR** (NPTS) MUST BE .GE. 2 AND .LE. (NPTM1))
COORD 134 C 3001 FORMAT(//52H **ERROR** BC FUNCTION TIME POINTS ARE OUT OF ORDER)
COORD 135 C
COORD 136 C RETURN
COORD 137 C END

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NPBC 1 C SUBROUTINE NPBC (NOD,KODE,MFN,TG,NUMNP)
NPBC 2 C *****
NPBC 3 C INPUT NODAL POINT BOUNDARY CONDITIONS *****
NPBC 4 C *****
NPBC 5 C *****
NPBC 6 C *****
NPBC 7 C DIMENSION NOD(1),KODE(1),MFN(1),TG(1)
NPBC 8 C COMMON /JUNK / HED(16),TOT,NLINE
NPBC 9 C COMMON /NBC / NNBC,NBCF,NP1N
NPBC 10 C DIMENSION AST(2)
NPBC 11 C DATA AST/2H 12H #/
NPBC 12 C WRITE(6,2001)
NPBC 13 C WRITE(6,2002)
NPBC 14 C NLINE = NLINE + 7
NPBC 15 C N = 1
NPBC 16 C
NPBC 17 C 100 READ (5,1000) M,ND,KD,MF,TOP,KG
NPBC 18 C
NPBC 19 C IF(KG.EQ.0) KG=1
NPBC 20 C IF(ND.EQ.0) ND=1
NPBC 21 C IF(MF.EQ.0) MF=1
NPBC 22 C WRITE(6,3000)
NPBC 23 C
NPBC 24 C 105 IF(MF.LE.NBCF) GO TO 110
NPBC 25 C WRITE(6,3001)
NPBC 26 C STOP
NPBC 27 C
NPBC 28 C
NPBC 29 C 110 IF(N.M) 200,120,200
NPBC 30 C
NPBC 31 C
NPBC 32 C 120 NDM = ND
NPBC 33 C KDM = KD
NPBC 34 C MFM = MF
NPBC 35 C TGM = TOP
NPBC 36 C KKG = KG
NPBC 37 C AST = AST(1)
NPBC 38 C
NPBC 39 C STORE PERMANENT INFORMATION
NPBC 40 C
NPBC 41 C 200 NOD(N) = NDM
NPBC 42 C KODE(N) = KDM
NPBC 43 C MF(N) = MFM
NPBC 44 C TG(N) = TGM
NPBC 45 C
NPBC 46 C IF(NLINE.LT.55) GO TO 250
NPBC 47 C CALL TITLE (HED)
NPBC 48 C WRITE(6,2000)
NPBC 49 C
NPBC 50 C NLINE = NLINE + 10
NPBC 51 C
NPBC 52 C 250 WRITE(6,2003) AST,N,NDM,KDM,MFM,TGM
NPBC 53 C NLINE = NLINE + 1
NPBC 54 C IF(N.EQ.NNBC) GO TO 300
NPBC 55 C
NPBC 56 C N = N + 1
NPBC 57 C
NPBC 58 C CHECK IF NODAL DATA IS TO BE STORED FOR CURRENT NODE
NPBC 59 C
NPBC 60 C IF(N.E2.M) GO TO 120
NPBC 61 C
NPBC 62 C GENERATE NEXT NODE NUMBER
NPBC 63 C
NPBC 64 C NDM = NDM + KKK
NPBC 65 C
NPBC 66 C CHECK IF NEXT NODE CARD IS TO BE READ
NPBC 67 C
NPBC 68 C AST = AST(2)
NPBC 69 C IF(N.GT.M) GO TO 100
NPBC 70 C

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NPBC 71 C GENERATE INFORMATION FOR NEXT NODE
NPBC 72 C
NPBC 73 C GO TO 200
NPBC 74 C
NPBC 75 C 280 WRITE(6,3002) M
NPBC 76 C STOP
NPBC 77 C
NPBC 78 C
NPBC 79 C
NPBC 80 C 000 FORMAT(4I5,F10.0,I5)
NPBC 81 C 2000 FORMAT(132(I4),/24H NODAL POINT BOUNDARY CONDITIONS/32(I4),/2)
NPBC 82 C 2001 FORMAT(13I,50H BOUNDARY CONDITION TYPE = 0 : EXTERNALLY SUPPLIED,
NPBC 83 C 12H HEAT FLUX 0/2N,
NPBC 84 C 2 3H MEAT : PRESCRIBED, NODAL TEMPERATURE T//)
NPBC 85 C 2002 FORMAT(4I5,MBC,ND,3I5,MNODS,2A7,THBC,TYPE,5K,GMFUNCTION,6X,
NPBC 86 C 5H,GM,0/24H,ND,1I4,1I5,3X,F12.3)
NPBC 87 C 2003 FORMAT(4I5,AST,1I4,1I5,8A1,1I5,3X,F12.3)
NPBC 88 C 3000 FORMAT(1/20H ***** NVAL TO BOUNDARY CONDITION NO. = IS)
NPBC 89 C 3001 FORMAT(1/20H ***** MF(N) MUST BE LE (NBCF))
NPBC 90 C 3002 FORMAT(1/20H ***** ELEMENT CARD = IS ISH OUT OF SEQUENCE)
NPBC 91 C
NPBC 92 C 300 RETURN
NPBC 93 C

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ELCL 1 C SUBROUTINE ELCAL
ELCL 2 C
ELCL 3 C COMMON /CTRL1 / NUMP, NEG, NLT, MODEX, NPAR(10), NG
ELCL 4 C COMMON /DIM / N1, N2, N3, N4, N5, N6, N7, N8, N9, N10, N11, N12, N13, N14, N15
ELCL 5 C COMMON /ELSTOR / N1E1, N1E2, N1E3, N1E4, N1E5, N1E6, N1E7, N1E8, N1E9, N1E10, N1E11, N1E12, N1E13, N1E14, N1E15
ELCL 6 C COMMON /JUNK / HED(16),TOT,NLINE
ELCL 7 C COMMON /NBC / NNBC,NBCF,NP1N
ELCL 8 C COMMON /AST / AST(1)
ELCL 9 C DIMENSION LABEL(2)
ELCL 10 C DATA LABEL/0HAST1,0HMETRIC,0HMP L A ,0HNA R /
ELCL 11 C *****
ELCL 12 C THIS ROUTINE CALLS THE APPROPRIATE ELEMENT ROUTINES FOR READING,
ELCL 13 C GENERATING AND STORING THE ELEMENT DATA
ELCL 14 C
ELCL 15 C TAPE ALLOCATION:
ELCL 16 C TAPE 1 - STORES LINEAR ELEMENT GROUP DATA
ELCL 17 C TAPE 2 - STORES 16,17,19 AND 20 ARRAYS FOR ALL ELEMENTS
ELCL 18 C *****
ELCL 19 C T W O   D I M E N S I O N A L   F I N I T E   E L E M E N T S
ELCL 20 C *****
ELCL 21 C NPAR(1) = 1
ELCL 22 C
ELCL 23 C NPAR(2) = NUMBER OF TWO DIMENSIONAL ELEMENTS (NEL2)
ELCL 24 C NPAR(3) = NUMBER OF FIVE ELEMENTS IN THIS GROUP (NPF5)
ELCL 25 C NPAR(4) = ELEMENT TYPE CODE (ITYPE2D)
ELCL 26 C EQ=0, AXISYMMETRIC
ELCL 27 C EQ=1, PLANNAR
ELCL 28 C NPAR(5) = MAXIMUM NUMBER OF NODES (NMNOD5)
ELCL 29 C NPAR(6) = NUMERICAL INTEGRATION ORDER (NIN)
ELCL 30 C NPAR(7) = NUMBER OF DIFFERENTIALS (NUMAT)
ELCL 31 C NPAR(8) = INTERNAL NEAR GENERATION FLAG (INFLG)
ELCL 32 C *****
ELCL 33 C C O N N E C T I O N   B O U N D A R Y   E L E M E N T S
ELCL 34 C *****
ELCL 35 C NPAR(1) = 2
ELCL 36 C NPAR(2) = NUMBER OF CONVECTION BOUNDARY ELEMENTS (NEL2)
ELCL 37 C NPAR(3) = NUMBER OF FIVE ELEMENTS IN THIS GROUP (NPF5)
ELCL 38 C NPAR(4) = ELEMENT TYPE CODE (ITYP)
ELCL 39 C EQ=0, AXISYMMETRIC, SOLID CONVECTION HC
ELCL 40 C EQ=1, PLANNAR SOLID CONVECTION SC
ELCL 41 C *****

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ELG1 98          IF(IELM+EQ+4) GO TO 250
ELG1 99          NN=IELM - 4
ELG1 100         DO 240 I=1,NN
ELG1 101         240 NODES(I,N)=NODSW(I)
ELG1 102         C
ELG1 103         C   STORE TB,TD, AND LM ARRAY ON TAPE FOR EACH ELEMENT
ELG1 104         C
ELG1 105         C   250 WRITE(2) TBORN,TDEAD,(LM(I,N),I=1,IELM),(LMR(I),I=1,NR)
ELG1 106         C
ELG1 107         C   IF(NLINE+LT.55) GO TO 260
ELG1 108         C   CALL TITLE (HED)
ELG1 109         C   WRITE(6,2003) NG
ELG1 110         C   WRITE(6,2004) (I,I=1,8)
ELG1 111         C   NLINE = 10
ELG1 112         C
ELG1 113         C   260 WRITE(6,2005) ASTT,IMEM,NODM,MTYPE,IELM,FBORN,TDEAD
ELG1 114         C   NLINE = NLINE + 1
ELG1 115         C   IF(IMEM+EQ+NLAST) GO TO 300
ELG1 116         C
ELG1 117         C   N = N + 1
ELG1 118         C   IMEM = IMEM + 1
ELG1 119         C
ELG1 120         C   CHECK IF ELEMENT DATA IS TO BE STORED FOR CURRENT ELEMENT
ELG1 121         C
ELG1 122         C   IF(IMEM+EQ+M) GO TO 120
ELG1 123         C
ELG1 124         C   GENERATE NODE NUMBERS FOR NEXT ELEMENT
ELG1 125         C
ELG1 126         C   DO 270 I=1,8
ELG1 127         C   IF(NODM(I)+EQ.0) GO TO 270
ELG1 128         C   NODM(I)=NODM(I)+KKK
ELG1 129         C   270 CONTINUE
ELG1 130         C
ELG1 131         C   CHECK IF NEXT ELEMENT CARD IS TO BE READ
ELG1 132         C
ELG1 133         C   ASTT=AST(2)
ELG1 134         C   IF(IMEM+GT+M) GO TO 100
ELG1 135         C
ELG1 136         C   GENERATE INFORMATION FOR NEXT ELEMENT
ELG1 137         C
ELG1 138         C   GO TO 200
ELG1 139         C
ELG1 140         C   280 WRITE(6,3001) M
ELG1 141         C   STOP
ELG1 142         C
ELG1 143         C   FORMAT STATEMENTS
ELG1 144         C
ELG1 145         C   1000 FORMAT(15,5X,7F10.0)
ELG1 146         C   1001 FORMAT(12I5,2F10.0)
ELG1 147         C   2000 FORMAT(36(1H*)/33H MATERIAL PROPERTIES TABLE, GROUP,13/36(1HR)///
ELG1 148         C   1   AX,SHMATL,3X,9(1H-),20HTHERMAL CONDUCTIVITY,9(1H-),3X,
ELG1 149         C   2   13MSPECIFIC HEAT,AX,7HDENSITY,AX,HHHEAT,6X,HHHEAT/5X,3HND,
ELG1 150         C   3   7X,5HK(11),9X,5HK(22),9X,5HK(12),3X,8HCAPACITY,17X,4HFUNC,
ELG1 151         C   4   6X,4HAMPL/)
ELG1 152         C   2001 FORMAT(2X,15,5E14+.3,2X,F5.0,E13.3)
ELG1 153         C   2002 FORMAT(//)
ELG1 154         C   2003 FORMAT(30(1H*)/27H ELEMENT INFORMATION, GROUP,13/30(1H*)//)
ELG1 155         C   2004 FORMAT(AX,AHELT,3X,10(1H-),12HNODE NUMBERS,10(1H-),3X,5HMATL,3X,
ELG1 156         C   1   6HND, OF,6X,7HTIME OF,AX,7HTIME OF,5X,3HND,3X,8(3X,11),
ELG1 157         C   2   4X,3HND,5X,5HNODES,7X,5HBIRTH,6X,5HDEATH/)
ELG1 158         C   2005 FORMAT(12,15,4X,8I4,1X,15,4X,15,4X,2E11.3)
ELG1 159         C   3000 FORMAT(//10H **ELEMENT,15,3AH EXCEEDS MAXIMUM NUMBER OF NODES**)
ELG1 160         C   3001 FORMAT(//26H **ERROR** ELEMENT CARD =15,16H JUT OF SEQUENCE)
ELG1 161         C
ELG1 162         C   300 RETURN
ELG1 163         C   END

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SUBROUTINE ADRS2
COMMON /CNTRL1/ NUMNP,NEG,NLT,MODEX,NPAR(10),NG
COMMON /DIM / M1,M2,M3,M4,M5,M6,M7,M8,M9,M10,M11,M12,M13,M14,M15
COMMON /JUNK / NUMST,MIDEST,MAXEST,NELT
COMMON /ENVCV / HED(18),MTOT,NLINE
COMMON /WORK / M1,M2,M3,M4,M5,M6,M7,M8,M9,M10,WORK(100)
COMMON A(11)
*****
B L A N K   C O M M O N   S T O R A G E   A L L O C A T I O N
*****
ARRAY -----DESCRIPTION----- DIMENSION
M1 LM ELEMENT CONNECTIVITY ARRAY 2*NEL2
M2 XX ELEMENT X-COORDINATES 2*NEL2
M3 HL CONVECTION COEFFICIENT*(LENGTH) NEL2
M4 MFCV FUNCTION ID FOR (TE) VARIATION NEL2
M5 TE ENVIRONMENTAL TEMP. AMPLITUDE NEL2
M6 TR TIME OF CONVECTION ELEMENT BIRTH NEL2
M7 TD TIME OF CONVECTION ELEMENT DEATH NEL2
*****
NEL2 = NPAR(2)
*****
M1 = 1 + 2*NEL2
M2 = M1 + 2*NEL2
M3 = M2 + 2*NEL2
M4 = M3 + NEL2
M5 = M4 + NEL2
M6 = M5 + NEL2
M7 = M6 + NEL2
NLAST= M7 - 1
WRITE(6,2000) NLAST
NLINE = NLINE + 4
MIDEST = NLAST
CALL ELGR2 (A(N1),A(N2),A(M1),A(M2),A(M3),A(M4),A(M5),A(M6),A(M7))
2000 FORMAT(3BH LENGTH OF ELEMENT INFORMATION .. = ,15//)
RETURN
END

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```

AD52 1 C
AD52 2 C
AD52 3 C
AD52 4 C
AD52 5 C
AD52 6 C
AD52 7 C
AD52 8 C
AD52 9 C
AD52 10 C
AD52 11 C
AD52 12 C
AD52 13 C
AD52 14 C
AD52 15 C
AD52 16 C
AD52 17 C
AD52 18 C
AD52 19 C
AD52 20 C
AD52 21 C
AD52 22 C
AD52 23 C
AD52 24 C
AD52 25 C
AD52 26 C
AD52 27 C
AD52 28 C
AD52 29 C
AD52 30 C
AD52 31 C
AD52 32 C
AD52 33 C
AD52 34 C
AD52 35 C
AD52 36 C
AD52 37 C
AD52 38 C
AD52 39 C
AD52 40 C
AD52 41 C
AD52 42 C
AD52 43 C
AD52 44 C
AD52 45 C
AD52 46 C

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ELG2 1 C
ELG2 2 C
ELG2 3 C
ELG2 4 C
ELG2 5 C
ELG2 6 C
ELG2 7 C
ELG2 8 C
ELG2 9 C
ELG2 10 C
ELG2 11 C
ELG2 12 C
ELG2 13 C
ELG2 14 C
ELG2 15 C
ELG2 16 C
ELG2 17 C
ELG2 18 C

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ELG2 19 DO 5 I=1,6
ELG2 20 5 LMR(I) = 0
ELG2 21 *****
ELG2 22 READ AND GENERATE ELEMENT INFORMATION
ELG2 23 *****
ELG2 24 *****
ELG2 25 *****
ELG2 26 N = 1
ELG2 27 IVM = MFST
ELG2 28 NLAST = MFST + NEL2 - 1
ELG2 29 WRITE(6,2000) NG
ELG2 30 WRITE(6,2001)
ELG2 31 NLINE = NLINE + 6
ELG2 32 *****
ELG2 33 100 READ (5,1000) M,NOD,MC,NFC,KG,TEXT,TBTH,TDTH
ELG2 34 *****
ELG2 35 IF(KG.EQ.0) KG = 1
ELG2 36 IF(TBTH.EQ.0) TDTH = 1.0E+10
ELG2 37 JJ = NOD(I)
ELG2 38 IF((JJ.EQ.1.AND.(I.LE.NUNNP)) GO TO 10
ELG2 39 WRITE(6,3000) JJ
ELG2 40 STOP
ELG2 41 *****
ELG2 42 10 IF((JJ.EQ.1.AND.(JJ.LE.NUNNP)) GO TO 20
ELG2 43 WRITE(6,3000) JJ
ELG2 44 STOP
ELG2 45 *****
ELG2 46 20 IF(NFC.GE.0.AND.NFC.LE.NBCF) GO TO 110
ELG2 47 WRITE(6,3001)
ELG2 48 STOP
ELG2 49 *****
ELG2 50 110 IF(M-IVM) 280,120,200
ELG2 51 *****
ELG2 52 SAVE ELEMENT INFORMATION FOR GENERATION OF ADDITIONAL ELEMENTS
ELG2 53 *****
ELG2 54 120 NODM(I) = NOD(I)
ELG2 55 NODM(2) = NOD(2)
ELG2 56 HCM = HC
ELG2 57 NFCM = NFC
ELG2 58 TEXTM = TEXT
ELG2 59 TBORN = TBTH
ELG2 60 TDEAD = TDTH
ELG2 61 KKK = KG
ELG2 62 ASTT = AST(I)
ELG2 63 X_ = SORT((X(JJ)-X(I))**2 + (Y(JJ)-Y(I))**2)
ELG2 64 *****
ELG2 65 STORE PERMANENT ELEMENT INFORMATION
ELG2 66 *****
ELG2 67 200 DO 230 I=1,2
ELG2 68 IJ = NODM(I)
ELG2 69 LMI(I,N) = IJ
ELG2 70 LMI(I,N) = X(IJ)
ELG2 71 *****
ELG2 72 MLE(N) = HCM*XL
ELG2 73 NFCV(N) = NFCM
ELG2 74 TE(N) = TEXTM
ELG2 75 TB(N) = TBORN
ELG2 76 TD(N) = TDEAD
ELG2 77 *****
ELG2 78 WRITE(2) TBORN,TDEAD,(LM(I,N),I=1,2),LMR
ELG2 79 *****
ELG2 80 IF(NLINE.LT.55) GO TO 250
ELG2 81 CALL TITLE (HFD)
ELG2 82 WRITE(5,2000) NG
ELG2 83 WRITE(6,2001)
ELG2 84 NLINE = 10
ELG2 85 *****
ELG2 86 250 WRITE(6,2002) ASTT,IVM,NODM,HCM,NFCM,TEXTM,TBORN,TDEAD
ELG2 87 NLINE = NLINE + 1
ELG2 88 IF((IVM.EQ.NLAST) GO TO 300

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```

N = N + 1
IVM = IVM + 1
CHECK IF ELEMENT DATA IS TO BE STORED FOR CURRENT ELEMENT
IF(IVM.EQ.M) GO TO 120
GENERATE NODE NUMBERS FOR NEXT ELEMENT
DO 270 I=1,2
270 NODM(I) = NODM(I) + KKK
CHECK IF NEXT ELEMENT CARD IS TO BE READ
ASTT = AST(I)
IF(IVM.GT.M) GO TO 100
GENERATE INFORMATION FOR NEXT ELEMENT
GO TO 200
280 WRITE(6,3002) M
STOP
FORMAT STATEMENTS
1000 FORMAT(3I5,F10.0,2I5,3F10.0)
2000 FORMAT(30(IH#)/27H ELEMENT INFORMATION, GROUP,(3/30(IH#)))
2001 FORMAT(4X,AHELT,4X,6HI-NODE,4X,6HJ-NODE,4X,10HCONVECTION,5X,
4HTE),5X,AHTE),5X,7HTIME OF 5X,7HTIME OF 5X,3HNO,2X,
2 11HCOEFFICIENT,4X,AHUNC,5X,4HAMPL,6X,5HIRTH,7X,SHDEATH/)
3000 FORMAT(//4AH **ERROR** INVALID CONVECTION NODE NUMBER =,I5)
3001 FORMAT(//39H **ERROR** NFCV(N) MUST BE .LE. (NBCF))
3002 FORMAT(//26H **ERROR** ELEMENT CARD =,I5,10H OUT OF SEQUENCE)
300 RETURN
ELG2 125
ELG2 126

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AD53 1 SUBROUTINE ADRS3
AD53 2 C
AD53 3 COMMON /CNTRL1/ NUMNP,NEG,NLT,MODEX,NPAR(10),NG
AD53 4 COMMON /ELSTOR/ NUMST,MIDST,MAXST,NELT
AD53 5 COMMON /JUNK / HED(10),MTOI,NLINE
AD53 6 COMMON /WORK / M1,M2,M3,M4,M5,M6,M7,M8,M9,M10,WORK(190)
AD53 7 COMMON A(1)
AD53 8 C
AD53 9 *****
AD53 10 BLANK COMMON STORAGE ALLOCATION
AD53 11 C
AD53 12 C
AD53 13 C
AD53 14 C
AD53 15 C
AD53 16 C
AD53 17 C
AD53 18 C
AD53 19 C
AD53 20 C
AD53 21 C
AD53 22 C
AD53 23 C
AD53 24 C
AD53 25 C
AD53 26 C

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DIMENSION
M1 LM ELEMENT LOCATION
M2 H EFFECTIVE CONVECTION COEFFICIENT NEL3
M3 NFCV FUNCTION ID FOR (TW) VARIATION NEL3
M4 TW COOLING WATER TEMP. AMPLITUDE NEL3
M5 T9 TIME OF COOLING ELEMENT BIRTH NEL3
M6 TD TIME OF COOLING ELEMENT DEATH NEL3
*****
NEL3 = NPAR(2)
M1 = 1
M2 = M1 + NEL3

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```

A053 27      M2 = M2 + NEL3
A053 28      M4 = M4 + NEL3
A053 29      M5 = M5 + NEL3
A053 30      M6 = M6 + NEL3
A053 31      M7 = M7 + NEL3
A053 32      NLAST= M7 - 1
A053 33      C
A053 34      WRITE(6,2000) NLAST
A053 35      NLINE = NLINE + 4
A053 36      MIDST = NLAST
A053 37      C
A053 38      CALL ELGR3 (A(M1),A(M2),A(M3),A(M4),A(M5),A(M6))
A053 39      C
A053 40      2000 FORMAT(3BH LENGTH OF ELEMENT INFORMATION .. = ,I5//)
A053 41      C
A053 42      RETURN
A053 43      END

ELG3 1      SUBROUTINE ELGR3 (LM,H,M,NFCP,TW,TB,TD)
ELG3 2      C
ELG3 3      *****
ELG3 4      INPUT INFORMATION FOR COOLING PIPE ELEMENTS
ELG3 5      C
ELG3 6      *****
ELG3 7      DIMENSION LM(11),H(11),NFCP(11),TW(11),TB(11),TD(11)
ELG3 8      COMMON /CNTRL/ NUMNP,NEG,NLT,MODEX,NPAR(10),NG
ELG3 9      COMMON /JUNK/ HED(18),M,TOT,NLINE
ELG3 10     COMMON /NBC/ / NNBC,NBCF,NPTM
ELG3 11     COMMON /WORK/ / DUM(10),LWR(7),WOR(183)
ELG3 12     DIMENSION AST(2)
ELG3 13     DATA AST/2H ,2H #/
ELG3 14     C
ELG3 15     NEL3 = NPAR(2)
ELG3 16     WFST = NPAR(3)
ELG3 17     DO 5 I=1,7
ELG3 18     5 LWR(I) = 0
ELG3 19     C
ELG3 20     *****
ELG3 21     READ AND GENERATE ELEMENT INFORMATION
ELG3 22     C
ELG3 23     *****
ELG3 24     N = 1
ELG3 25     IWER = WFST
ELG3 26     NLAST = WFST + NEL3 - 1
ELG3 27     WRITE(6,2000) NG
ELG3 28     NLINE = NLINE + 8
ELG3 29     C
ELG3 30     100 READ (5,1000) M,NOD,MP,NFC,KG,TWTR,TBTH,TOTH
ELG3 31     C
ELG3 32     IF(KG.EQ.0) KG = 1
ELG3 33     IF(TOTH.EQ.0) TOTH = 1.0E+10
ELG3 34     IF(NOD.LT.1.AND.NOD.LE.NUMNP) GO TO 10
ELG3 35     WRITE(6,3000) NOD
ELG3 36     STOP
ELG3 37     10 IF(NFC.GE.0.AND.NFC.LE.NBCF) GO TO 110
ELG3 38     WRITE(6,3001)
ELG3 39     STOP
ELG3 40     C
ELG3 41     110 IF(M-IMEN) 280,120,200
ELG3 42     C
ELG3 43     SAVE ELEMENT INFORMATION FOR GENERATION OF ADDITIONAL ELEMENTS
ELG3 44     C
ELG3 45     120 NODM = NOD
ELG3 46     HPM = HP
ELG3 47

```

```

ELG3 48     NFCM = NFC
ELG3 49     TW = TWTR
ELG3 50     TBORN = TBTH
ELG3 51     TDEAD = TOTH
ELG3 52     KKK = KG
ELG3 53     ASTT = AST(1)
ELG3 54     C
ELG3 55     STORE PERMANENT ELEMENT INFORMATION
ELG3 56     C
ELG3 57     200 LM(N) = NODM
ELG3 58     H(N) = HPM
ELG3 59     NFCP(N) = NFCM
ELG3 60     TW(N) = TW
ELG3 61     TB(N) = TBORN
ELG3 62     TD(N) = TDEAD
ELG3 63     C
ELG3 64     WRITE(2) TBORN,TDEAD,NODM,LWR
ELG3 65     C
ELG3 66     IF(NLINE.LT.55) GO TO 250
ELG3 67     CALL TITLE (HED)
ELG3 68     WRITE(6,2000) NG
ELG3 69     WRITE(6,2001)
ELG3 70     NLINE = 10
ELG3 71     C
ELG3 72     250 WRITE(6,2002) ASTT,IMEN,NODM,HPM,NFCM,TW,TBORN,TDEAD
ELG3 73     NLINE = NLINE + 1
ELG3 74     IF(IMEN.EQ.NLAST) GO TO 300
ELG3 75     C
ELG3 76     CHECK IF ELEMENT DATA IS TO BE STORED FOR CURRENT ELEMENT
ELG3 77     C
ELG3 78     IF(IMEN.EQ.M) GO TO 120
ELG3 79     C
ELG3 80     GENERATE NODE NUMBERS FOR NEXT ELEMENT
ELG3 81     C
ELG3 82     NODM = NODM + KKK
ELG3 83     C
ELG3 84     CHECK IF NEXT ELEMENT CARD IS TO BE READ
ELG3 85     C
ELG3 86     ASTT = AST(2)
ELG3 87     IF(IMEN.GT.M) GO TO 100
ELG3 88     C
ELG3 89     GENERATE INFORMATION FOR NEXT ELEMENT
ELG3 90     C
ELG3 91     GO TO 200
ELG3 92     C
ELG3 93     280 WRITE(6,3002) M
ELG3 94     STOP
ELG3 95     C
ELG3 96     FORMAT STATEMENTS
ELG3 97     C
ELG3 98     1000 FORMAT(2I5,F10.0,2I5,F10.0)
ELG3 99     2000 FORMAT(30(1H#)/27H ELEMENT INFORMATION, GROUP,13/30(1H#)//)
ELG3 100    2001 FORMAT(4X,4HELT,4X,4HNODE,5X,10HCONVECTION,5X,4HTW,5X,4HTWJ,
ELG3 101    1 5X,7HTIME OF,5X,7HTIME OF,5X,3HND,12X,11HCoeffICIENT,5X,
ELG3 102    2 4HFUNC,5X,4HAMPL,6X,5HBRTH,7X,5HDEATH/)
ELG3 103    2002 FORMAT(2I5,4X,15,3X,E12.3,3X,I5,3(E10.3,2X))
ELG3 104    3000 FORMAT(/46H **ERROR** INVALID COOLING PIPE NODE NUMBER = 15)
ELG3 105    3001 FORMAT(/39H **ERROR** NFCP(M) MUST BE .LE. (NBCF))
ELG3 106    3002 FORMAT(/26H **ERROR** ELEMENT CARD =15,16H OUT OF SEQUENCE)
ELG3 107     C
ELG3 108    300 RETURN
ELG3 109    END

```





```

ADSK 7 C MA = MAXIMUM BAND WIDTH
ADSK 8 C MHT = ACTIVE COLUMN HEIGHTS ABOVE DIAGONAL
ADSK 9 C MAXA = ADDRESSES OF DIAGONAL ELEMENTS
ADSK 10 C NPK = MAXIMUM STORAGE REQUIRED
ADSK 11 C *****
ADSK 12 C DIMENSION MAXA(1),MHT(1)
ADSK 13 C
ADSK 14 C MAXA(1) = 1
ADSK 15 C MAXA(2) = 2
ADSK 16 C MA = 0
ADSK 17 C IF(NEQ,EO,1) GO TO 100
ADSK 18 C DD 10 I=2,NEO
ADSK 19 C IF(MHT(I),GT,MA) MA = MHT(I)
ADSK 20 C IF(MHT(I+1) = MAXA(I) + MHT(I) + 1
ADSK 21 C 10 MAXA(I+1) = MAXA(I) + 1
ADSK 22 C 100 MA = MA + 1
ADSK 23 C NPK = MAXA(NEO+1) - 1
ADSK 24 C RETURN
ADSK 25 C
ADSK 26 C

```

```

ADSK 7 C
ADSK 8 C
ADSK 9 C
ADSK 10 C
ADSK 11 C
ADSK 12 C
ADSK 13 C
ADSK 14 C
ADSK 15 C
ADSK 16 C
ADSK 17 C
ADSK 18 C
ADSK 19 C
ADSK 20 C
ADSK 21 C
ADSK 22 C
ADSK 23 C
ADSK 24 C
ADSK 25 C
ADSK 26 C

```

```

IDNT 34 C
IDNT 35 C WRITE(6,2000)
IDNT 36 C NROW = NUMNP/20 + 1
IDNT 37 C NR = 0
IDNT 38 C
IDNT 39 C DD 100 I=1,NUMNP,20
IDNT 40 C NR = NR + 1
IDNT 41 C IP = I + 19
IDNT 42 C IF(NREQ,NROW) IP = NUMNP
IDNT 43 C WRITE(6,2001) (J,J=1,IP)
IDNT 44 C WRITE(6,2002) (ID(J),J=1,IP)
IDNT 45 C 100 CONTINUE
IDNT 46 C
IDNT 47 C FORMAT STATEMENTS
IDNT 48 C
IDNT 49 C 2000 FORMAT(17H EQUATION NUMBERS)
IDNT 50 C 2001 FORMAT(/XX,8MODE NO.,5A,2015)
IDNT 51 C 2002 FORMAT( 4X,8MODE. NO.,5A,2015)
IDNT 52 C
IDNT 53 C RETURN
IDNT 54 C
IDNT 55 C

```

```

SUBROUTINE ASSEMK
*****
ASSEMBLE THE EFFECTIVE SYSTEM CONDUCTIVITY MATRIX (K*)
*****
COMMON /CNTRL/ NUMNP,NEG,NLT,MODEX,NPAR(10),NG
COMMON /DIM / N1,N2,N3,N4,N5,N6,N7,N8,N9,N10,N11,N12,N13,N14,N15
COMMON /WORK / M1,M2,M3,M4,M5,M6,M7,M8,M9,M10,WORK(100)
COMMON A(1)
DIMENSION NST(10)
EQUIVALENCE (NST(1),M1)
REWIND 1
REWIND 3
LOOP OVER ALL ELEMENT GROUPS
DD 100 NG=1,NEG
READ (1) MIDEST,NPAR,NST,(A(I),I=1,MIDEST)
NGR = NPAR(1)
GO TO (1,2,3) NGR
-----
ELEMENT GROUP 1
-----
1 MKNDS = NPAR(5)
NOM = 2*MKNDS
NOSDIM = MKNDS-4
IF(NOSDIM,EQ,0) NOSDIM = 1
CALL COND1 (A(M1),A(M2),A(M3),A(M4),A(M5),A(M6),A(M7),A(M8),
A(N10),MKNDS,NOM,NOSDIM)
GO TO 100

```

```

ASMK 1 C
ASMK 2 C
ASMK 3 C
ASMK 4 C
ASMK 5 C
ASMK 6 C
ASMK 7 C
ASMK 8 C
ASMK 9 C
ASMK 10 C
ASMK 11 C
ASMK 12 C
ASMK 13 C
ASMK 14 C
ASMK 15 C
ASMK 16 C
ASMK 17 C
ASMK 18 C
ASMK 19 C
ASMK 20 C
ASMK 21 C
ASMK 22 C
ASMK 23 C
ASMK 24 C
ASMK 25 C
ASMK 26 C
ASMK 27 C
ASMK 28 C
ASMK 29 C
ASMK 30 C
ASMK 31 C
ASMK 32 C
ASMK 33 C
ASMK 34 C
ASMK 35 C
ASMK 36 C
ASMK 37 C
ASMK 38 C
ASMK 39 C
ASMK 40 C
ASMK 41 C
ASMK 42 C
ASMK 43 C
ASMK 44 C

```

```

SUBROUTINE SKY (ID,MHT,NUMNP,NELT,PLTIME)
DIMENSION ID(1),MHT(1),L(8)
INITIALIZE MHT ARRAY
DD 10 I=1,NUMNP
10 MHT(I) = 0
CREATE LM ARRAY FOR EACH ACTIVE ELEMENT, CORRESPONDING TO
ID ARRAY WHICH CONTAINS EQUATION NUMBERS
REWIND 2
DD 30 N=1,NELT
READ (2) IP,TD,LM
IF(TD,GT,PLTIME) GO TO 30
IF(ID,LE,PLTIME) GO TO 30
DD 20 I=1,8
JJ = LM(I)
IF(JJ,EQ,0) GO TO 20
LM(I) = ID(JJ)
20 CONTINUE
COMPUTE ACTIVE COLUMN HEIGHTS
CALL COLHT (MHT,8,LM)
30 CONTINUE
RETURN
END

```

```

SKY 1 C
SKY 2 C
SKY 3 C
SKY 4 C
SKY 5 C
SKY 6 C
SKY 7 C
SKY 8 C
SKY 9 C
SKY 10 C
SKY 11 C
SKY 12 C
SKY 13 C
SKY 14 C
SKY 15 C
SKY 16 C
SKY 17 C
SKY 18 C
SKY 19 C
SKY 20 C
SKY 21 C
SKY 22 C
SKY 23 C
SKY 24 C
SKY 25 C
SKY 26 C
SKY 27 C
SKY 28 C
SKY 29 C
SKY 30 C
SKY 31 C

```

```

SUBROUTINE ADSK (MAXA,MHT,NEQ,NPK,MA)
*****
TO CALCULATE ADDRESSES OF DIAGONAL ELEMENTS IN A
BANDED MATRIX WHOSE COLUMN HEIGHTS ARE KNOWN.

```

```

ADSK 1 C
ADSK 2 C
ADSK 3 C
ADSK 4 C
ADSK 5 C
ADSK 6 C

```

```

ASMK 45 C
ASMK 46 C
ASMK 47 C
ASMK 48 C
ASMK 49 C
ASMK 50 C
ASMK 51 C
ASMK 52 C
ASMK 53 C
ASMK 54 C
ASMK 55 C
ASMK 56 C

GO TO 100
-----
ELEMENT GROUP 3
-----
3 CALL COND3 (A(N1),A(N2),A(N3),A(N4))
100 CONTINUE
RETURN
END

SUBROUTINE CONDI (LM,XY,IELT,NODS,MATP,PROP,TB,TD,TD,
  MNODS,NDM,NDSDIM)
*****
FORM THE EFFECTIVE SYSTEM CONDUCTIVITY MATRIX (K*) AND
THE EFFECTIVE HEAT CAPACITY VECTOR (C*)
*****
DIMENSION L*(MNODS,1),XY(NDM,1),IELT(1),NODS(NODS,1),MATP(1),
  PROP(7,1),TB(1),TD(1),ID(1)
COMMON /CTRL1/ NUMNP,NEG,MLT,MODEX,NPAR(10),NG
COMMON /CTRL2/ KST,NDT,DT,PLTIME,PLACET,NPRINT,TIME
COMMON /D14 / N1,N2,N3,N4,N5,N6,N7,N8,N9,N10,N11,N12,N13,N14,N15
COMMON /WORK / DUM(10),SK(64),SC(3),HF(8),LMA(8),WORK(102)
COMMON /TOO14 / NEL,NODS,NTYPE,NND5
COMMON A(1)
NEL1 = NPAR(2)
INFLG = NPAR(8)
DO 100 I=1,NEL1
  IF(IT(N),GT,PLTIME) GO TO 100
  IF(IT(N),LE,PLTIME) GO TO 100
  NODS = IELT(N)
  NTYPE = MATP(N)
  MNDS = IELT(N) - 4
  NDOF = NODS*MNDS
  ZERO ELEMENT CONDUCTIVITY MATRIX SK(NODS,NODS)
  DO 50 I=1,NDOF
    SK(I) = 0.0
  50 SK(I) = 0.0
  ZERO ELEMENT HF(NODS) VECTOR -
  INFLUENCE COEFFICIENTS FOR UNIT INTERNAL HEAT GENERATION
  IF(INFLG.EQ.0) GO TO 56
  DO 55 I=1,NODS
    HF(I) = 0.0
  55 HF(I) = 0.0
  ZERO ELEMENT HEAT CAPACITY VECTOR SC(NODS)
  DO 60 I=1,NODS
    SC(I) = 0.0
  60 SC(I) = 0.0
  CALCULATE ELEMENT CONDUCTIVITY MATRIX USING GAUSS QUADRATURE
  CALL FORMK1 (SK,SC,HF,XY(1,N),NODS(1,N),PROP(1,NTYPE),NODS)
  IF(INFLG.EQ.0) GO TO 75

```

```

CONI 53 C
CONI 54 C
CONI 55 C
CONI 56 C
CONI 57 C
CONI 58 C
CONI 59 C
CONI 60 C
CONI 61 C
CONI 62 C
CONI 63 C
CONI 64 C
CONI 65 C
CONI 66 C
CONI 67 C
CONI 68 C
CONI 69 C
CONI 70 C
CONI 71 C
CONI 72 C
CONI 73 C
CONI 74 C
CONI 75 C

WRITE(3) (HF(I),I=1,NODS)
CREATE LMA ARRAY FOR ACTIVE DEGREES OF FREEDOM
75 DO 80 I=1,NODS
  JJ = LM(I,N)
  80 LMA(I) = 10(JJ)
ASSEMBLE ELEMENT CONDUCTIVITY MATRIX INTO STRUCTURAL CONDUCTIVITY
CALL ADDRAN (A(N1),A(N2),SK,LMA,NODS)
IF(KST.EQ.-1) GO TO 100
ASSEMBLE EFFECTIVE LINEAR HEAT CAPACITY VECTOR (C*)
C* = (1./DT)*C
CALL ADDC (A(N1),SC,LMA,NODS)
100 CONTINUE
RETURN
END

```

```

SUBROUTINE FORMK1 (SK,SC,HF,XY,NODS,PROP,NODS)
*****
ISPARAMETRIC FORMULATION OF ELEMENT CONDUCTIVITY AND HEAT
CAPACITY FOR TWO DIMENSIONAL PLANNAR AND AXISYMMETRIC GEOMETRY
*****
DIMENSION SK(NODS,NODS),SC(NODS),HF(1),XY(1),NODS(1),PROP(1)
COMMON /CTRL1/ NUMNP,NEG,MLT,MODEX,NPAR(10),NG
COMMON /CTRL2/ KST,NDT,DT,PLTIME,PLACET,NPRINT,TIME
COMMON /WORK / DUM(10),M(8),P(2,8),B(2,8),XJ(2,2),EK(3),WORK(55)
DIMENSION XG(4,4),WGT(4,4)
DATA XG / 0., 0., 0., 0.,
  1 --5773502691896, .5773502691896, 0., 0., 0.,
  2 --7745966692415, .000000000000, .7745966692415, 0.,
  3 --8611363115941, -.339981043549, .339981043549, .8611363115941/
DATA WGT / 2.,0., 0., 0.,
  1 1.,0.000000000000,1.,0.000000000000, 0., 0.,
  2 .55555555555556, .888888888889, .555555555556, 0.,
  3 .3478548451375, .6521451548625, .6521451548625, .3478548451375/
ITYP2D = NPAR(4)
NINT = NPAR(6)
IMELG = NPAR(8)
EK11 = PROP(1)
EK22 = PROP(2)
EK12 = PROP(3)
LOOP OVER ALL INTEGRATION POINTS
VOL = 0.0
DO 100 LX=1,NINT
  R = XG(LX,NINT)
  DO 100 LY=1,NINT
    S = XG(LY,NINT)
    WT = WGT(LX,NINT)*WGT(LY,NINT)
  FIND INTERPOLATION FUNCTIONS (H) AND THEIR DERIVATIVES (D).
  FIND JACOBIAN (XJ) AND ITS DETERMINANT (DETJ).

```



```

DER1 8      DIMENSION XY(2,1),H(1),P(2,1),B(2,1),XJ(2,2)
DER1 9      COMMON /TODIM / NEL,NODS,MYTYPE,NND5
DER1 10     COMMON /WORK / DUM(145),XJ(2,2),WORK(51)
DER1 11     C
DER1 12     C
DER1 13     C
DER1 14     C
DER1 15     C
DER1 16     C
DER1 17     C
DER1 18     C
DER1 19     C
DER1 20     C
DER1 21     C
DER1 22     C
DER1 23     C
DER1 24     C
DER1 25     C
DER1 26     C
DER1 27     C
DER1 28     C
DER1 29     C
DER1 30     C
DER1 31     C
DER1 32     C
DER1 33     C
DER1 34     C
DER1 35     C
DER1 36     C
DER1 37     C
DER1 38     C
DER1 39     C
DER1 40     C
DER1 41     C
DER1 42     C

```

```

GO TO (5,6,7,8) NM
5 H(5) = 0.508R2*SP
P(1,5) = -R*SP
P(2,5) = 0.508R2
GO TO 2
6 H(6) = 0.508R*MS2
P(1,6) = -0.508*S2
P(2,6) = -R*MS
GO TO 2
7 H(7) = 0.508R2*SM
P(1,7) = -R*SM
P(2,7) = -0.5C*R2
GO TO 2
8 H(8) = 0.508R*MS2
P(1,8) = 0.508*S2
P(2,8) = -R*MS
GO TO 2
MODIFY INTERPOLATION FUNCTIONS H(1) TO H(4) AND LOCAL DERIVATIVES
40 IH = 0
41 IH = IH + 1
IF(IH.GT.NND5) GO TO 50
IN = NND5(IH)
I1 = IN - 4
I2 = IPERM(I1)
H(I1) = H(I1) - 0.5*H(IN)
H(I2) = H(I2) - 0.5*H(IN)
H(IN+4) = H(IN)
DO 45 J=1,2
P(J,I1) = P(J,I1) - 0.5*P(J,IN)
P(J,I2) = P(J,I2) - 0.5*P(J,IN)
45 P(J,IN+4) = P(J,IN)
GO TO 41
EVALUATE THE JACOBIAN MATRIX AT POINT (R,S)
50 DO 100 I=1,2
DO 100 J=1,2
SUM = 0.0
DO 90 K=1,NODS
90 SUM = SUM + P(I,K)* XY(J,K)
100 XJ(I,J) = SUM
C COMPUTE THE DETERMINANT OF THE JACOBIAN MATRIX AT POINT (R,S)
DETJ = XJ(1,1)* XJ(2,2) - XJ(2,1)* XJ(1,2)
DUM = ABS(DETJ)
IF(DUM.GT.1.0E-9) GO TO 500
WRITE (6,3000) NEL
STOP
3000 FORMAT(//4H **ERROR** ZERO JACOBIAN DETERMINANT FOR ELEMENT,15)
500 RETURN
END

```

```

SUBROUTINE ADDBAN (A,MAXA,5,LM,NDOF)
*****
ASSEMBLES ELEMENT CONDUCTIVITY INTO COMPACTED GLOBAL CONDUCTIVITY
*****
DIMENSION A(1),MAXA(1),S(1),L4(1)
DO 200 J=1,NDOF
JJ = LM(J)
MJ = MAXA(JJ)
DO 200 I=1,NDOF
II = LM(II)
IJ = JJ - II
IF(IJ) 200,100,100
100 KK = MJ + IJ
LS = (J-II)*NDOF + I
AL(KK) = A(KK) + S(LS)
200 CONTINUE
RETURN
END

```

```

SUBROUTINE DERIV1 (XY,H,P,9,XJ,DETJ,RAD,ITYP2D)
*****
EVALUATION OF THE GLOBAL DERIVATIVE OPERATOR (9) AT A POINT (R,S)
FOR A QUADRILATERAL ELEMENT HAVING PLANAR OR AXISYMMETRIC GEOMETRY
*****

```

```

ADBN 1 2 C
ADBN 3 C
ADBN 4 C
ADBN 5 C
ADBN 6 C
ADBN 7 C
ADBN 8 C
ADBN 9 C
ADBN 10 C
ADBN 11 C
ADBN 12 C
ADBN 13 C
ADBN 14 C
ADBN 15 C
ADBN 16 C
ADBN 17 C
ADBN 18 C
ADBN 19 C
ADBN 20 C
ADBN 21 C
ADBN 22 C

```

```

DER1 1 2 C
DER1 3 C
DER1 4 C
DER1 5 C
DER1 6 C
DER1 7 C

```



```

COLS 1  C
COLS 2  C
COLS 3  C
COLS 4  C
COLS 5  C
COLS 6  C
COLS 7  C
COLS 8  C
COLS 9  C
COLS 10 C
COLS 11 C
COLS 12 C
COLS 13 C
COLS 14 C
COLS 15 C
COLS 16 C
COLS 17 C
COLS 18 C
COLS 19 C
COLS 20 C
COLS 21 C
COLS 22 C
COLS 23 C
COLS 24 C
COLS 25 C
COLS 26 C
COLS 27 C
COLS 28 C
COLS 29 C
COLS 30 C
COLS 31 C
COLS 32 C
COLS 33 C
COLS 34 C
COLS 35 C
COLS 36 C
COLS 37 C
COLS 38 C
COLS 39 C
COLS 40 C
COLS 41 C
COLS 42 C
COLS 43 C
COLS 44 C
COLS 45 C
COLS 46 C
COLS 47 C
COLS 48 C
COLS 49 C
COLS 50 C
COLS 51 C
COLS 52 C
COLS 53 C
COLS 54 C
COLS 55 C
COLS 56 C
COLS 57 C
COLS 58 C
COLS 59 C
COLS 60 C
COLS 61 C
COLS 62 C
COLS 63 C
COLS 64 C
COLS 65 C
COLS 66 C
COLS 67 C
COLS 68 C
COLS 69 C
COLS 70 C

SUBROUTINE COLSOL (A,V,MAXA,NN,MA,NWA,XXX)
*****
TO SOLVE SIMULTANEOUS EQUATIONS AX=V IN CORE, USING
COMPACTED STORAGE AND COLUMN REDUCTION SCHEME.
A = MATRIX STORED IN COMPACTED FORM
V = VECTOR TO BE REDUCED
MAXA = VECTOR CONTAINING ADDRESSES OF DIAGONAL ELEMENTS OF A
REDUCTION (LV=V) AND BACKSUBSTITUTION (UX=V):
KKK=0 TRIANGULARIZATION ONLY
KKK=1 TRIANGULARIZATION PLUS SOLUTION
KKK=2 FORWARD REDUCTION AND BACKSUBSTITUTION ONLY
KKK=3 BACKSUBSTITUTION ONLY
*****
DIMENSION A(NWA),V(1),MAXA(1)
MA1=MA - 1
IF (KKK=2) 100,700,800
*****
TRIANGULARIZATION
*****
IF (NN.EQ.1) GO TO 900
N=1
IF (A(1,1)) 90,85,110
90 WRITE (6,3000) N
STOP
85 WRITE (6,3001) N
STOP
80 WRITE (6,3002) N
N=N+1
DO 200 N=2,NN
KL=MAXA(N) + 1
KUM=MAXA(N+1) - 1
IF (KU-KL) 200,210,210
B=0.
DO 210 B=0.
KN=MAXA(N)
K=N
DO 220 KK=KL,KU
K=K - 1
C=A(KK)/A(K)
B=B + C*A(KK)
A(KK)=C
A(KN)=A(KN) - B
DO 220 KK=KL,KU
WRITE (6,3001) N
STOP
224 WRITE (6,3001) N
STOP
226 WR=MINO(MA1,NN-N)
IF (WR) 200,200,228
NN=KU - KL + 1
DO 240 J=1,WR
M1=MAXA(N+1) + J
M2=MAXA(N+1) - J
IF (M2) 240,240,230
N2=MINO(MN,M2)
C=0.
KUM=N + ND
K=N - KN
IC=MJ - KN
DO 300 KK=KL,KU

```

```

COLS 71  C
COLS 72  C
COLS 73  C
COLS 74  C
COLS 75  C
COLS 76  C
COLS 77  C
COLS 78  C
COLS 79  C
COLS 80 C
COLS 81 C
COLS 82 700
COLS 83  C
COLS 84  C
COLS 85  C
COLS 86 410
COLS 87  C
COLS 88  C
COLS 89  C
COLS 90 420
COLS 91  C
COLS 92 400
COLS 93  C
COLS 94  C
COLS 95  C
COLS 96  C
COLS 97  C
COLS 98  C
COLS 99 800
COLS 100 K=MAXA(N)
COLS 101 V(N)=V(N)/A(K)
COLS 102 IF (NN.EQ.1) RETURN
COLS 103 N=NN
COLS 104 DO 500 L=2,NN
COLS 105 KL=MAXA(L) + 1
COLS 106 KU=MAXA(L+1) - 1
COLS 107 IF (KU-KL) 500,510,510
COLS 108 K=N
COLS 109 DO 520 KK=KL,KU
COLS 110 K=K - 1
COLS 111 V(K)=V(K) - A(KK)*V(N)
COLS 112 500
COLS 113 C
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COLS 117 3000 FORMAT(/,45H **STOP** STIFFNESS NOT POSITIVE DEFINITE.../,
COLS 118 10X,27H NEGATIVE PIVOT IN POSITION I4)
COLS 119 3001 FORMAT(/,33H **STOP** ZERO PIVOT IN POSITION I4)
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SUBROUTINE FLUX2 (L4,XX,HL,NFCV,TE,TB,TD,TFN,FM,NPTS,0,1D,NPTM)
*****
THIS ROUTINE MODIFIES FLUX VECTOR (0) FOR CONVECTION BOUNDARIES
*****
DIMENSION LM(2,1),XX(2,1),HL(1),NFCV(1),TE(1),TB(1),TD(1),
1 COMMON /CNTRL1/ NUMNP,NEG,NLT,MODEX,NPAR(10),NG
COMMON /CNTRL2/ KST,NDT,DT,PLTIME,PLACET,NPRINT,TIME
NEL2 = NPAR(2)
ITYP = NPAR(4)
DO 100 N=1,NEL2
IF(TB(N).GT,PLTIME) GO TO 100
IF(TD(N).LE,PLTIME) GO TO 100
HLN = HL(N)
NF = NFCV(N)
TX = TE(N)
N1 = LM(1,N)
N2 = LM(2,N)
II = IO(N1)
JJ = IO(N2)
IF(NF.EQ.0) GO TO 20
NPT = NPTS(NF)
CALL INTERP (TFN(1,NF),FM(1,NF),NPT,TIME,VAL)
20 IF(ITYP.EQ.0) GO TO 30
PLANAR SOLID CONVECTION BOUNDARY ELEMENTS
IF(NF.EQ.0) VAL = 1.0
Q(II) = Q(II) + HLN*TX*VAL/2.
Q(JJ) = Q(JJ) + HLN*TX*VAL/2.
GO TO 100
AXISYMMETRIC SOLID CONVECTION BOUNDARY ELEMENTS
30 IF(NF.EQ.0) VAL = 1.0
VI = XX(1,N)
VJ = XX(2,N)
Q(II) = Q(II) + HLN*TX*VAL*(2.*VI + VJ)/6.
Q(JJ) = Q(JJ) + HLN*TX*VAL*(2.*VJ + VI)/6.
100 CONTINUE
RETURN
END

SUBROUTINE FLUX3 (L4,H,MFCP,TB,T9,TD,TFN,FM,NPTS,0,1D,NPTM)
*****
THIS ROUTINE MODIFIES FLUX VECTOR (0) FOR COOLING PIPES
*****
DIMENSION LM(1),M(1),MFCP(1),TW(1),TB(1),TD(1),TFN(NPTM,1),
1 FN(NPTM,1),NPTS(1),Q(1),ID(1)
COMMON /CNTRL1/ NUMNP,NEG,NLT,MODEX,NPAR(10),NG
COMMON /CNTRL2/ KST,NDT,DT,PLTIME,PLACET,NPRINT,TIME
NEL3 = NPAR(2)
DO 100 N=1,NEL3
IF(TB(N).GT,PLTIME) GO TO 100
IF(TD(N).LE,PLTIME) GO TO 100
NN = LM(N)
II = IO(NN)
NF = MFCP(N)
IF(NF.EQ.0) GO TO 20
NPT = NPTS(NF)
CALL INTERP (TFN(1,NF),FN(1,NF),NPT,TIME,VAL)
20 IF(NF.EQ.0) VAL = 1.0
Q(II) = Q(II) + H(N)*TW(N)*VAL
100 CONTINUE
RETURN
END

SUBROUTINE INTERP (TFN,FM,NPT,TIME,VAL)
*****
THIS ROUTINE INTERPOLATES A GIVEN TIME-DEPENDENT FUNCTION TO FIND
THE VALUE OF THE FUNCTION (VAL) AT A PARTICULAR TIME POINT (TIME)
*****
DIMENSION TFN(1),FM(1)
DO 10 N=1,NPT
DTIME = TFN(N) - TIME
IF(DTIME.GT.0.) GO TO 15
10 CONTINUE
15 DIFF = TFN(N) - TFN(N-1)
VAL = FM(N) - (FM(N) - FM(N-1))*DTIME/DIFF
RETURN
END

SUBROUTINE OEFF (O,E,NEQ)
*****
FORM EFFECTIVE HEAT FLUX VECTOR (J*)
*****
DIMENSION O(1),E(1)
DO 10 I=1,NEQ
O(I) = O(I) + E(I)
10 CONTINUE
RETURN
END

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FLX3 17  
FLX3 18  
FLX3 19  
FLX3 20 C  
FLX3 21  
FLX3 22  
FLX3 23  
FLX3 24 C  
FLX3 25  
FLX3 26  
FLX3 27 C  
FLX3 28  
FLX3 29 C  
FLX3 30  
FLX3 31

INTP 1 C  
INTP 2 C  
INTP 3 C  
INTP 4 C  
INTP 5 C  
INTP 6 C  
INTP 7 C  
INTP 8  
INTP 9 C  
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INTP 14 C  
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INTP 16  
INTP 17 C  
INTP 18  
INTP 19

OEFF 1 C  
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OEFF 3 C  
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OEFF 6 C  
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OEFF 11 C  
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OEFF 13

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FLX3 14

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1 SUBROUTINE OUT (I,IO,NUMNP,TIME,KSTEP,NEQ)
2 C
3 C *****
4 C PRINT NODAL TEMPERATURES FOR *TIME*
5 C *****
6 C THIS ROUTINE PRINTS OUT NODAL TEMPERATURES FOR *TIME*
7 C DIMENSION T(1),ID(1)
8 C COMMON /WORK / IT(6),TT(6),WORK(188)
9 C
10 C WRITE(6,2000) KSTEP,TIME
11 C
12 C L = 0
13 C K = 0
14 C DO 10 I=1,NUMNP
15 C N = ID(I)
16 C IF(N.EQ.0) GO TO 10
17 C K = K + 1
18 C TT(K) = I
19 C TT(K) = T(N)
20 C IF(K.LT.6) GO TO 10
21 C WRITE(6,2001) (IT(J),TT(J),J=1,6)
22 C L = L + 6
23 C K = 0
24 C 10 CONTINUE
25 C
26 C NDIFF = NEQ - L
27 C IF(NDIFF.EQ.0) GO TO 500
28 C WRITE(6,2001) (IT(J),TT(J),J=1,NDIFF)
29 C
30 C FORMAT STATEMENTS
31 C
32 C 2000 FORMAT(2/28H TEMPERATURES AT TIME STEP =15,2X,7HITIME =E11.4,1H)
33 C 2001 FORMAT(16(E14.6))
34 C
35 C 500 RETURN
36 C
37 C END

```

