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# A Bifunctional Ionic Liquid for Capture and Electrochemical Conversion of CO<sub>2</sub> to CO over Silver

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Cite This: ACS Catal. 2023, 13, 7812-7821 **Read Online** ACCESS Metrics & More Article Recommendations s Supporting Information [EMIM]\* ABSTRACT: Electrochemical conversion of CO<sub>2</sub> requires selective catalysts and high solubility of CO<sub>2</sub> in the electrolyte to reduce the energy requirement and increase the current efficiency. In this study, the  $CO_2$  reduction reaction ( $CO_2RR$ ) over Ag [2-CNpyr] CO electrodes in acetonitrile-based electrolytes containing 0.1 M [EMIM][2-CNpyr] (1-ethyl-3-methylimidazolium 2-cyanopyrolide), a reactive ionic liquid (IL), is shown to selectively (>94%) 1000 convert CO<sub>2</sub> to CO with a stable current density (6 mA·cm<sup>-2</sup>) for 1250 man shift (cm-1) at least 12 h. The linear sweep voltammetry experiments show the 2250 2500 -0<u>.9</u> onset potential of CO<sub>2</sub> reduction in acetonitrile shifts positively by 240 mV when [EMIM][2-CNpyr] is added. This is attributed to

carbamate formation via binding to the nucleophilic [2-CNpyr]<sup>-</sup> anion. The analysis of the electrode-electrolyte interface by surface-enhanced Raman spectroscopy (SERS) confirms the catalytic role of the functionalized IL where the accumulation of the IL- $CO_2$  adduct between -1.7 and -2.3 V vs Ag/Ag<sup>+</sup> and the simultaneous CO formation are captured. This study reveals the electrode surface species and the role of the functionalized ions in lowering the energy requirement of  $CO_2RR$  for the design of multifunctional electrolytes for the integrated capture and conversion.

**KEYWORDS:** electrochemical CO<sub>2</sub> reduction, ionic liquid, faradaic efficiency, carbon monoxide, carbon capture and utilization

## INTRODUCTION

The  $CO_2$  concentration in the atmosphere is rapidly increasing due to anthropogenic activities. As a result, the average global atmospheric temperature is increasing, causing a rise in sea levels and ocean acidification.<sup>1,2</sup> Converting CO<sub>2</sub> into fuels or common chemicals offers hope for an energy transition from non-renewable to sustainable energy resources, which mitigates the adverse effects arising from increasing CO<sub>2</sub> in the atmosphere. The  $CO_2$  conversion can be achieved by a variety of methods, including thermochemical,<sup>3,4</sup> biochemical,<sup>5</sup> photochemical,<sup>6</sup> electrochemical,<sup>5</sup> and radiochemical.<sup>7</sup> Among the available CO<sub>2</sub> conversion techniques, electrochemical CO<sub>2</sub> reduction reaction  $(CO_2RR)$  offers certain advantages: (1) mild operating conditions, (2) environmental compatibility (energy required to drive CO<sub>2</sub>RR can be derived from renewable energy resources like solar and wind), (3) easy control of product selectivity by adjusting external parameters such as electrolytes and applied voltages, and (4) engineering and economic feasibility.<sup>8,9</sup> Significant efforts have been devoted in developing metal<sup>10</sup> and non-metal catalysts,<sup>11</sup> modifications to catalyst morphology and composition,<sup>12</sup> and electrolyzer configuration<sup>13</sup> for CO<sub>2</sub>RR in aqueous electrolytes. However, several existing challenges such as low solubility of

the pre-activation of CO<sub>2</sub> through the carboxylate formation via the carbene intermediate of the [EMIM]<sup>+</sup> cation and the

> $CO_2$ , the competing hydrogen evolution reaction, and instability of metal and metal oxide catalysts in (acid) aqueous environments need to be addressed to enhance the efficiency.<sup>14</sup>

> Ionic liquids (ILs) have been considered for CO<sub>2</sub>RR due to their high electrochemical stabilities, high CO<sub>2</sub> solubilities, negligible vapor pressures, and tunable physical properties.<sup>15-18</sup> It has been reported that ILs can activate thermodynamically stable CO2 and accelerate its transfer to the reaction interface, acting as "co-catalysts".<sup>19,20</sup> One of the earlier studies was by Rosen et al.<sup>19</sup> where the reduction of CO<sub>2</sub> to CO on a Ag electrode utilizing 1-ethyl-3methylimidazolium tetrafluoroborate ( $[EMIM][BF_4]$ ) with 18 mol % water was achieved. They reported CO generation at a lower overpotential (difference between the thermodynamic and experimental reduction potentials) compared to aqueous systems and with stable performance for 7 h with

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Faradaic efficiency of >96%. They attributed these improvements to the stabilization of the  $CO_2^{\bullet-}$  intermediate by [EMIM]<sup>+</sup>. Furthermore, Braunschweig's group<sup>21-23</sup> studied the role of imidazolium cations with the same  $[BF_4]^-$  for CO<sub>2</sub> to CO conversion over Pt catalysts by operando IR absorption spectroscopy and in situ sum frequency generation spectroscopy. They reported the reduction of the imidazolium cation to carbene, which was discussed to subsequently react with CO<sub>2</sub> to form an imidazolium-2-carboxylic acid specie. This reactive intermediate underwent a proton-coupled electron transfer (500 mM water as the proton source), thus leading to CO formation and regeneration of the imidazolium cation. Hanc-Scherer et al.<sup>15</sup> and Zhao et al.<sup>24</sup> reported the formation of a stable EMIM-H-CO<sub>2</sub> adduct by a radical-radical coupling after the simultaneous reduction of CO<sub>2</sub> and [EMIM]<sup>+</sup>. In these studies, the EMIM-H-CO<sub>2</sub><sup>-</sup> adduct is discussed to form upon the reaction of radical species: CO2<sup>•-</sup> and [EMIM]<sup>•</sup> (generated by single electron transfer to [EMIM]<sup>+</sup>).

There are also few reports where the role of the IL anions was investigated.<sup>25,26</sup> Golru and Biddinger<sup>25</sup> showed the impact of anions' hydrophilicity, size, and CO<sub>2</sub> affinity on CO<sub>2</sub>RR. They studied ILs with the 1-butyl-3-methylimidazolium ( $[BMIM]^+$ ) cation and the following anions: (bis-(trifluoromethylsulfonyl)imide ([TFSI]<sup>-</sup>), triflate ([OTF]<sup>-</sup>), acetate ([Ac]<sup>-</sup>), chloride ([Cl]<sup>-</sup>), and dicyanamide ([DCA]<sup>-</sup>). They used 10 mM of IL in 0.1 M KHCO<sub>3</sub> solution and examined CO<sub>2</sub>RR on a electropolished copper surface. They found that formate is selectively generated at -0.92 V versus RHE (reference hydrogen electrode) with the exception of the electrolyte with  $[DCA]^-$  where H<sub>2</sub> was the major product. In another study, Kang et al.<sup>26</sup> reported that ILs with fluorinated anions such as trifluoromethylsulfonate ([OTf]-), hexafluorophosphate ( $[PF_6]^-$ ), and tetrafluoroborate ( $[BF_4]^-$ ) when paired with [BMIM]<sup>+</sup> enable conversion of CO<sub>2</sub> to CH<sub>4</sub> with higher total current densities compared to a non-fluorinated perchlorate anion ( $[ClO_4]^-$ ) on Zn-based metal-organic frameworks (Zn-MOFs) as the solid catalyst. The increase in current density was explained to be due to (1) strong interactions between CO<sub>2</sub> and fluorine atoms on the anions and (2) the strong adsorption capacity of CO than  $CH_4$  on the Zn-MOF.

In summary, the majority of the CO<sub>2</sub>RR studies with ILs thus far have focused on common ILs where CO<sub>2</sub> is physisorbed in the absence of electric fields. Specifically, ILs with imidazolium cation are shown to lower the activation energy<sup>19</sup> by co-catalyzing the reaction at the metal electrode surface, suppressing hydrogen evolution reaction (HER),<sup>27</sup> and increasing  $CO_2$  solubility<sup>28,29</sup> with control over the reaction pathway.<sup>30</sup> These studies suggest that surface adsorption of ILs plays an important role in lowering HER; however, the exact mechanism by which ILs lower the overpotential remains unclear. Both an inner sphere e-transfer<sup>31</sup> for surface-adsorbed CO<sub>2</sub> and a carboxylated imidazolium promoted route<sup>19,20</sup> have been discussed. In contrast to these studies, there has been a single report where a reactive IL, trihexyltetradecylphosphonium 1,2,4-triazole ( $[P_{66614}]$ [124Triz]), that chemisorbs  $CO_2$  was studied for  $CO_2RR^{29}$  It was reported that [124Triz]<sup>-</sup> chemisorbs  $CO_2$  in equimolar quantity. The covalently bound  $CO_2$  on  $[124Triz]^-$  was discussed to be reduced on Ag at overpotentials as low as 0.17 V (vs Ag/Ag<sup>+</sup>), generating formate as the major product. However, this study did not provide spectroscopic evidence to the surface species or the reaction mechanism.

Here, we examined the reactive IL [EMIM][2-CNpyr] in acetonitrile, where the chemisorption of  $CO_2$  yields carboxylate and carbamate species as a result of  $CO_2$  binding to  $[EMIM]^+$  and  $[2-CNpyr]^-$ , respectively. Specifically, we studied the role of these species in modulating the  $CO_2RR$  mechanism on Ag by voltammetry and SERS studies with systematic variations in the molecular structure of the IL, thus probing the individual functionality. The role of the local electrolyte environment in the bulk and at the electrode– electrolyte interface is shown to have a critical role in lowering the reduction potentials and reaction efficiency and selectivity.

#### EXPERIMENTAL SECTION

Materials and Methods. 1-Ethyl-3-methyl-imidazolium chloride ([EMIM][Cl]) and 1-ethyl-3-methyl-imidazolium bis(trifluoromethylsulfonyl)imide ([EMIM][TFSI]) were purchased from IoLiTec Inc. Pyrrole 2-carbonitrile (99%) was from Thermo Scientific Chemicals and amberlite IRN-87 anion exchange resin (AER) were purchased from Purolite. Amberlite IRN-87 AER was washed multiple times with methanol and vacuum dried at room temperature to remove impurities present in it. Molecular sieves (3 Å) were received from Merck (Germany) and used after overnight drying at 100 °C under vacuum. 1,2-Dimethyl imidazole (98%) and bromo ethane (99%) were purchased from Alfa Aesar and TCI, respectively. Tetraethylammonium perchlorate (TEAP, 99.0%), choline chloride ([Ch][Cl], 99%), diethyl ether (>99%, anhydrous), and acetonitrile (99.9%) were obtained from Sigma-Aldrich. Methanol (99.8%, HPLC grade) and ethyl acetate (99.9%) were purchased from Fisher. A glass fiber nonwoven filter (Whatman grade GF/A, 260  $\mu$ m in thickness) was purchased from VWR. Silver foil (99.9%) was obtained from Sigma-Aldrich. A Pt mesh electrode (99.9%, 4  $cm^2$  area) and a non-aqueous reference electrode kit-Ag/Ag<sup>+</sup> were purchased from BASi. For NMR characterizations, deuterated dimethyl sulfoxide-d6 (DMSO-d6, 99.9% (isotopic)) and chromium(III) acetylacetonate (99.99%) were purchased from Thermo Scientific and Sigma-Aldrich, respectively. High-purity N<sub>2</sub> (99.999%), Ar (99.999%), CO<sub>2</sub> (99.995%), and He (99.999%) gas were obtained from Airgas, Inc. <sup>13</sup>CO<sub>2</sub> gas (99%) was purchased from Cambridge Isotope Laboratories, Inc.

Quantitative <sup>13</sup>C-NMR (q-<sup>13</sup>C-NMR) solvent was prepared as a 0.1 M solution of chromium acetylacetonate (obtained from Sigma-Aldrich) in DMSO-d6. NMR tubes (5 mm OD; 7" L; wall thickness: 0.38 mm) with coded closed caps were purchased from Bruker. The water contents were measured by a Karl Fischer titrator (Metrohm Coulometric KF 889D) and were below 1000 ppm. Elemental analyses were performed at Atlantic Microlab.

**Synthesis and Characterization of Reactive ILs.** As reported previously for [EMIM][2-CNpyr],<sup>32</sup> ILs were synthesized in a two-step reaction starting from the halide version of the cation precursor salts, where the halide was converted into hydroxide by an anion exchange step and then reacted with anion precursors to get corresponding IL in the second step. Briefly, the chloride or the bromide versions of the cation salts were converted into the hydroxide form in methanol solution using the anion exchange resin. The anion exchange was carried out until no visual silver halide precipitation was observed by the silver nitrate test. The anion precursor was then added into the solution and stirred overnight at room temperature for the acid—base reaction to

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ILs full name	abbreviation	structure	purity	supplier
1-Ethyl-3-methyl- imidazolium 2- cyanopyrrolide	[EMIM][2-CNpyr]		>98%	In-house synthesis
1-Ethyl-3-methyl- imidazolium chloride	[EMIM][Cl]	∽n r cr	>98%	IoLiTec
1-Ethyl-3-methyl- imidazolium bis(trifluoromethyl- sulfonyl)imide	[EMIM][TFSI]		≥97%	IoLiTec
1-Ethyl- 2,3-dimethyl- imidazolium bis(trifluoromethyl- sulfonyl)imide	[EMMIM][2-CNpyr]		>98%	In-house synthesis
Choline 2- cyanopyrrolide	[Ch][2-CNpyr]		>98%	In-house synthesis

<sup>a</sup>Reported purities are determined by NMR for the synthesized samples and as provided by the supplier for commercial samples.

complete, thus forming the IL of interest ( $85 \pm 5\%$  yield) and the water by-product. The excess solvent and residual water were removed via rotary evaporation at 50 °C for an hour, and the sample was further dried under vacuum first for 1 day at room temperature and then 2 days at 50 °C.

For the synthesis of 1-ethyl-2,3-dimethyl imidazolium 2cyanopyrrolide ([EMMIM][2-CNpyr]), the precursor [EMMIM] [Br] was first synthesized via Menshutkin reaction. Briefly, 1,2-dimethylimidazole and 2-bromoethane in a 1:1.3 molar ratio were refluxed at 40 °C for 3 h under an inert atmosphere. The reaction mixture was cooled to room temperature, and the white crystals were immediately formed. The crystals were purified via first washing with ethyl acetate and then drying with diethyl ether to remove any unreacted reactants. The crystals were dried under vacuum at 60 °C for 3 days. Synthesized samples were confirmed by <sup>1</sup>H- and <sup>13</sup>Cnuclear magnetic resonance (NMR) spectroscopy (Bruker Ascend 500 MHz) in DMSO-d6 (Figures S1-S4). All NMR spectroscopy results were performed using the same instrument and solvent unless noted otherwise. The chemical structures and purities of the ILs are shown in Table 1. The halide content of the synthesized samples was determined by elemental analysis and reported to be less than the detection limit of the combustion ion chromatography (0.25%).

Electrochemical Measurements and Product Analysis. Electrochemical Methods. The linear sweep voltammograms (LSVs) were recorded at a potential sweep rate of 10 mV/s at room temperature (22 °C) in both the N<sub>2</sub>- and CO<sub>2</sub>saturated electrolytes. LSV was performed to determine the onset potential for CO<sub>2</sub>RR. LSVs were performed in a singlecompartment glass cell using a three-electrode assembly at the ambient conditions. All glassware parts were cleaned and dried overnight at 110 °C. For the working and counter electrodes, Ag foil (0.38 cm<sup>2</sup> area) and Pt mesh ( $2 \times 2$  cm) were used, respectively. The silver working electrode was prepared by mechanical polishing of Ag foil using a series of abrasive sheets (3000, 5000, and 8000 grit), followed by cleaning ultrasonically in ethanol and water. The reference electrode was a nonaqueous Ag/Ag<sup>+</sup> electrode (0.01 M AgNO<sub>3</sub> and 0.1 M TEAP in acetonitrile). The reported potentials are IR corrected (V-IR<sub> $\Omega$ </sub>) by compensating 80% of the measured resistance with reference to Ag/Ag<sup>+</sup>. The electrochemical cell

was filled with 5 mL of electrolyte solution and purged with dry N<sub>2</sub> gas for at least 30 min prior to the experiments to remove O<sub>2</sub> traces. The CO<sub>2</sub> and N<sub>2</sub> flow rates in the electrochemical cell were maintained with a mass flow controller (Brooks Mass Flow Controller, North Coast Metrology, USA). To prevent moisture accumulation in the electrolyte due to the gas flow from the tanks, moisture traps (VICI Metronics) were installed on N<sub>2</sub> and CO<sub>2</sub> gas lines, which ensured <1 ppb moisture in the feed to the electrochemical cell. A mixture of 0.1 M TEAP in acetonitrile was used as the supporting electrolyte. Acetonitrile was dried with activated molecular sieves prior to use. The water content of the prepared electrolytes was determined by the Karl– Fischer titration, and for all of the samples, the water content was below 500 ppm.

Product Analysis. To identify the reaction products, electrolysis experiments were carried out under continuous purging of  $CO_2$  at a flow rate of 10 mL/min while sampling the headspace of the single-compartment electrochemical cell. The gas outlet of the electrochemical cell was directly connected to a gas chromatography (GC, GC-7890B, Agilent Technologies) sampling valve for online gas sampling. The GC was equipped with six different columns and three detectors for simultaneous separation of CO, CO<sub>2</sub>, H<sub>2</sub>, and hydrocarbons. A thermal conductivity detector (TCD) and a flame ionization detector (FID) were used to perform the quantitative analysis of the gas phase products. The GC apparatus was calibrated for quantitative analysis of the gaseous products (i.e., CO and  $H_2$ ) using a calibration gas obtained from Airgas, Inc. (USA). The calibration gas contains 5 mol % each of CO and 0.2 mol % of H<sub>2</sub> balanced in CO<sub>2</sub>. The known volume of standard samples was automatically injected to GC using He and N<sub>2</sub> as carrier gases for detecting CO and H<sub>2</sub>, respectively. A clear CO peak appeared at 7.85 min on TCD2B while H<sub>2</sub> was detected at 1.15 min on the TCD2C detector. The calibration curves were obtained based on the peak surface area with respect to the number of moles of the injected gases (i.e., CO and  $H_2$ ), as shown in Figure S5. Finally, the molar quantity of products was calculated during the reduction reaction by correlating the product peak area with the obtained calibration curves.

The time needed to reach the steady-state concentration was approximately 15 min, so samples from bulk electrolysis



Figure 1. LSVs of electrolytes examined under  $N_2$  (dotted lines) and  $CO_2$  (solid lines). (a) 0.2 M TEAP in acetonitrile. (b) 0.1 M [EMIM][2-CNpyr] added to the supporting electrolyte of 0.1 M TEAP in acetonitrile. (c) [EMIM][TFSI] and [EMIM][Cl] and (d) [Ch][2-CNpyr] and [EMIMI][2-CNpyr], in comparison to [EMIM][2-CNpyr]; each are 0.1 M in concentration.

experiments were injected at every 20 min with an online gas sampling valve. The liquid products formed during the electrolysis were analyzed by NMR. The NMR samples were prepared by mixing 350  $\mu$ L of DMSO-d6 solvent with 350  $\mu$ L of electrolyte. The electrolyte obtained before and after CO<sub>2</sub>RR was also characterized by ATR-FTIR using a Nicolet iS50 FTIR (Thermo Scientific) with 32 scans, at a resolution of 4 cm<sup>-1</sup>, on a diamond crystal.

The Faradaic efficiency (FE) for  $CO_2RR$  gaseous products during the electrolysis experiments was calculated as follows:

FE (%) = 
$$\frac{e_{\text{out}}}{e_{\text{in}}} \times 100 = \frac{yn}{Q/F} \times 100$$

where y is the measured amount of product in a 0.25 mL sample loop (based on calibration of the GC) with a standard gas (mol), n (=2) is the number of electrons required to form a molecule of CO or H<sub>2</sub>, Q is the measured charge (C), and F is the Faraday constant (96,485 C/mol).

In Situ Raman Spectroscopy. In situ SERS measurements were performed with a homebuilt spectroscopic cell (Figure S6) and a Renishaw InVia spectrometer system with a 785 nm excitation laser source. The Ag foil, Pt coil, and Ag/ Ag<sup>+</sup> were used as working, counter, and reference electrodes, respectively. To obtain SERS active Ag as the working electrode, the Ag foil was electrochemically roughened in 0.1 M KCl solution with a Pt mesh counter electrode and a Ag/ AgCl reference electrode by applying three potential sweeps between 0.25 and -0.4 V (vs Ag/AgCl) to the working electrode with a 5 mV/s scan rate (Figure S7a).<sup>33</sup> The obtained Ag foil was then cleaned and dried to remove residual Cl and moisture from the surface. Scanning electron microscopy (SEM) and atomic force microscopy (AFM) were used to confirm the effectiveness of the roughening process. The SEM and AFM images of pristine Ag foil and electrochemically roughened Ag foil are shown in Figure S7b. The energy-dispersive X-ray (EDX) analysis (Figure S8) shows the absence of oxygen or any other compound, confirming that the roughened Ag surface is free from any impurities and oxides.

The Raman probe was focused on the electrode/electrolyte interface with a  $20\times$  microscope objective (LMPLFL Olympus,  $20\times$ , NA = 0.4,WD = 12 mm). Various combinations of acquisition times per spectrum (integration time) and laser power were evaluated. The high-quality potential-dependent spectral changes with minimum time duration were obtained using a 10 s laser exposer and 1

accumulation at 1% laser power. The resolution for the spectra collected between 300 and 3200 cm<sup>-1</sup> is 0.5 cm<sup>-1</sup>. The obtained SERS data was processed with Origin 2022 (version 9.9.0.225) software for background subtraction and peak normalization.

Electron Paramagnetic Resonance Spectroscopy. Electron paramagnetic resonance (EPR) spectroscopy was performed at the CalEPR center in the University of California, Davis. Samples were prepared following the procedure for constant potential electrolysis for the catalytic generation of CO from CO<sub>2</sub>. After 30 min of electrolysis, 200  $\mu$ L of electrolysis sample was removed from the cell with a syringe and injected into a N2-filled EPR tube, which was then frozen in liquid nitrogen. X-band continuous-wave spectra were recorder on a Bruker BioSpin ELEXSYS E500 spectrometer equipped with a super high Q resonator (ER4122SHQE). Cryogenic temperatures were achieved by using an ESR900 liquid helium cryostat with a temperature controller (Oxford Instruments ITC503) and a gas flow controller. All CW-EPR spectra were recorded under slow-passage, non-saturating conditions. Spectrometer settings were as follows: conversion time = 60 ms, modulation frequency = 100 kHz, modulation amplitude = 0.2 mT, and other settings as given in the corresponding figure captions. The Q-Band Mims ENDOR spectrum was recorded on a Bruker BioSpin ELEXSYS-580 spectrometer with an R.A. Isaacson cylindrical TE011 resonator, a 10 W microwave amplifier, and a 1 kW LPI-10 RF amplifier. The pulse sequences employed were as follows: electron spin-echo detected field swept EPR ( $\pi/2-\tau-\pi-\tau$ -echo) and Mims ENDOR ( $\pi/2-\tau-\pi/2-RF-\pi/2-\tau-echo$ ).

## RESULTS AND DISCUSSION

The co-catalytic activity of [EMIM][2-CNpyr] is studied by LSV using the Ag working electrode (Figure 1). The onset potential for CO<sub>2</sub>RR in the supporting electrolyte (0.1 M TEAP in acetonitrile) is observed at -2.16 V (vs Ag/Ag<sup>+</sup>), as marked in Figure 1a. After addition of 0.1 M [EMIM][2-CNpyr] in this supporting electrolyte, the onset is shifted to -1.92 V (vs Ag/Ag<sup>+</sup>). The 240 mV positive shift in onset potential suggests a reduction in the activation energy of CO<sub>2</sub>. This can be explained by the reactivity of the IL with CO<sub>2</sub>. It is reported previously that the CO<sub>2</sub> absorption by [EMIM][2-CNpyr] forms carbamate ( $-N-COO^-$ ) and carboxylate ( $-C-COO^-$ ) species through binding to the anion and cation (via carbene intermediate), respectively, under anhydrous conditions.<sup>32</sup> Similarly, in this study, the same products



**Figure 2.** (a) Faradaic efficiency (FE<sub>CO</sub>) and partial current density of CO ( $j_{CO}$ ) at different potentials during CO<sub>2</sub>RR over Ag with 0.1 M [EMIM][2-CNpyr] in the supporting electrolyte. (b) Faradaic efficiencies (filled blue squares) for CO production and total current density (red hollow diamonds) during 12 h of continuous CO<sub>2</sub>RR with 0.1 M [EMIM][2-CNpyr] in the supporting electrolyte on the Ag electrode at -2.2 V vs Ag/Ag<sup>+</sup>. (c) Comparison of the charge consumed for CO generation ( $Q_{CO}$ ) measured upon electrolysis at -2.1 V vs Ag/Ag<sup>+</sup> for 1 h among the ILs studied. TEAP/MeCN is 0.2 M TEAP in acetonitrile. ILs were introduced to the supporting electrolyte of 0.1 M TEAP in acetonitrile at 0.1 M concentration.

are confirmed by <sup>1</sup>H and <sup>13</sup>C NMR for [EMIM][2-CNpyr] in acetonitrile (Figures S9 and S10). When the concentration of [EMIM][2-CNpyr] is increased, the CO<sub>2</sub>RR onset potential stays about the same, as seen in Figure S11. However, the current increases as the IL concentration increases from 0.1 to 1 M and then decreases as it reaches to 1.5 and 2 M. At higher concentrations, viscosities substantially increase (Figure S12), thus presenting mass transfer limitations. This dependence on IL concentration could also be related to the changes in the double-layer structure where surface coverage by [EMIM]<sup>+</sup> is more pronounced at higher concentrations, as previously discussed by Liu et al. for [EMIM][BF<sub>4</sub>] in acetonitrile.<sup>34</sup>

Due to the availability of multiple CO<sub>2</sub> binding sites, it is difficult to comment on the most active species responsible for the observed co-catalytic activity for CO<sub>2</sub>RR. Therefore, we further performed LSV measurements by changing the anion and cation structures in a systematic way to probe the role of these CO<sub>2</sub> complexes. In the first set of experiments, we studied the effect of the anion on onset potential by examining the imidazolium ILs with [Cl]<sup>-</sup> and [TFSI]<sup>-</sup> in comparison to [2-CNpyr]<sup>-</sup>. The lowest CO<sub>2</sub>RR onset potential was with [EMIM][2-CNpyr], as seen in Figure 1b. In the second set of experiments, the impact of the cation was investigated by comparing [EMIM][2-CNpyr] to [Ch][2-CNpyr] and [EMMIM][2-CNpyr]. This experiment revealed identical catalytic onset potentials for [EMIM]<sup>+</sup> and [Ch]<sup>+</sup> and similar current densities for both ILs in acetonitrile, as shown in Figure 1c. In addition, we found that when the carbene route for CO<sub>2</sub> binding is eliminated by blocking it with a methyl group on the imidazolium C2 carbon ([EMMIM]<sup>+</sup>), the onset potential is slightly more negative compared to [EMIM][2-CNpyr] for CO<sub>2</sub>RR but still more positive compared to the supporting electrolyte itself. These results confirm that [2-CNpyr]<sup>-</sup> also plays a significant role in the observed catalytic enhancement in addition to [EMIM]<sup>+</sup>.

To investigate the product identity from  $CO_2RR$  in the presence of the synthesized ILs in acetonitrile (0.1 M IL with 0.1 M TEAP-supporting salt), bulk electrolysis experiments were performed on the Ag electrode (0.38 cm<sup>2</sup>) in a single compartment cell. Online gas sampling during the bulk electrolysis experiment showed CO as the only gaseous product in all of the systems studied. Figure 2a shows the

obtained FE for CO at different applied potentials for 1 h with [EMIM][2-CNpyr]. A maximum selectivity of 94% for CO was achieved at -2.1 V (vs Ag/Ag<sup>+</sup>). A very stable current response was obtained at the applied potentials between -2.0 and -2.3 V (vs Ag/Ag<sup>+</sup>), as seen in Figure S13. More importantly, high-resolution <sup>1</sup>H NMR spectroscopic analysis of the electrolyte post electrolysis showed no evidence of the degradation of [EMIM][2-CNpyr] after 1-3 h (Figure S9) of continuous CO<sub>2</sub>RR.

The long-term stability of the [EMIM][2-CNpyr] containing electrolyte was further evaluated by running the CO2 reduction experiment continuously for 12 h at -2.2 V. As shown in Figure 2b, the Faradaic efficiency for CO stays around >94% during the course of CO<sub>2</sub>RR. The electrolyte after 12 h of CO<sub>2</sub>RR was analyzed by NMR (<sup>13</sup>C NMR in Figure S14) and ATR-FTIR (Figure S15) where spectral changes are clearly seen, compared to 1–3 h of CO<sub>2</sub>RR. While the exact mechanism by which degradation occurs is unknown, <sup>1</sup>H NMR analysis, summarized in Table S1, indicates decreased anion peak intensities possibly due to degradation or volatilization of the protonated anion (2-CNpyrH). This specie, which was formed during CO<sub>2</sub> absorption, can interact with either the carboxylate or the carbamate adducts. In the case of the neat IL, these close interactions prevent the escape of 2-CNpyrH from the liquid phase. However, during CO<sub>2</sub>RR in acetonitrile, evaporative escape of 2-CNpyrH is possible.

The CO<sub>2</sub>RR performance in the presence of other ILs are presented in Figure 2c in terms of the charge utilized for CO production during the electrolysis at -2.1 V (vs Ag/Ag<sup>+</sup>) for 1 h. The charge utilization for CO production by the electrolyte containing [EMIM][2-CNpyr] is the highest among the studied ILs. Even when compared to [Ch][2-CNpyr], which has a similar onset potential (Figure 1c), the total charge utilized for CO production with [EMIM][2-CNpyr] is dramatically higher at -2.1 V (vs Ag/Ag<sup>+</sup>) in 1 h. We attribute this enhancement by [EMIM][2-CNpyr] for CO<sub>2</sub>RR due to its superior CO<sub>2</sub> sorption<sup>32</sup> and multiple proton sources to facilitate CO<sub>2</sub>RR<sup>35-37</sup> in comparison to other ILs studied.<sup>38,39</sup> The CO selectivity with [EMIM][2-CNpyr] over the Ag surface is comparable with the other [EMIM]based ILs reported recently (Table S2); however, the proton source and the mechanism are different here where a robust



Figure 3. Potential-dependent SERS on an electrochemically roughened Ag electrode with the  $CO_2$ -saturated electrolyte: 0.1 M [EMIM][2-CNpyr] and 0.1 M TEAP in acetonitrile. Potentials are with respect to Ag/Ag<sup>+</sup>.

electrolysis can be achieved due to the stability of the intermediates at the electrode surface, as explained by SERS analysis.

Literature suggests that the co-catalytic activity of [EMIM]based ILs in CO<sub>2</sub>RR primarily originates from the complexation of the imidazolium cation and  $CO_2$ . The [EMIM] $-CO_2$ complex was suggested to lower the energy barrier for the formation of the CO2<sup>•-</sup> radical anion and to suppress the competing reaction of H<sub>2</sub> production by forming a monolayer on the cathode. However, in the presence of the basic [2-CNpyr]<sup>-</sup>, CO<sub>2</sub> chemically binds to the anion. Furthermore, some of the [2-CNpyr]<sup>-</sup> get protonated by the hydrogen on the C2 carbon of the imidazolium, thus forming a carbone that also binds with  $CO_2$  prior to reduction of  $CO_2$  to  $CO_2^{\bullet-}$ . Since  $CO_2$  is transformed from a linear form to a bent geometry by binding to [EMIM][2-CNpyr], the chemical reaction complexes are believed to serve as the co-catalysts, thus lowering the onset potential. In order to identify the electrode surface species during CO<sub>2</sub>RR and capture the role of the ions, SERS measurements were performed, as seen in Figure 3. The peak at 2269 cm<sup>-1</sup> is the CN stretching of acetonitrile, and this was used as an internal reference and spectral normalization. At open circuit potential (OCP), -0.9 V, as molecules are randomly arranged on the electrode surface, there are not many distinct features besides the acetonitrile peaks. With increased negative polarization, significant spectral changes are visible with the most significant ones due to the enrichment of the electrode surface with [EMIM]<sup>+</sup> (1336, 1348, 1380, 1415  $cm^{-1}$ ).<sup>40,41</sup> This observation is consistent with the earlier reports where surface adsorption of [EMIM]<sup>+</sup> on Ag nanoparticles was observed (with counter ions of  $[BF_4]^{-34}$ and  $[Cl]^{-41}$ ). This shows that the imidazolium cation starts breaking the solvation barrier at about  $-1.5 \text{ V} (\text{vs Ag/Ag}^+)$  and start to adsorb on the Ag surface. It should be noted that [EMIM]<sup>+</sup> enrichment is only seen with a SERS active Ag surface; Figure S16 shows no spectral changes with a smooth Ag surface due to bulk interference and lack of spectral enhancement. Furthermore, [EMIM]<sup>+</sup> migration to the surface is seen even in the absence of CO<sub>2</sub> on SERS surface upon negative polarization as seen in Figure S17, with slight differences in the spectral shapes under N<sub>2</sub>. Additionally, it is

possible that some features related to the anion or 2-CNpyrH (e.g., CNC in-phase stretch, C=C stretch, and out-of-phase C=C stretch) can overlap with the [EMIM]<sup>+</sup> features in the region of 1380–1460 cm<sup>-1.42</sup> Because the concentration of the anionic specie is low at the negatively polarized surface, it is difficult to observe it by SERS. However, stretching of C=N (v(CN)) of [2-CNpyr]<sup>-</sup> under N<sub>2</sub> is observed at 2190 cm<sup>-1</sup> when the IL concentration is increased to 0.5 M in the supporting electrolyte. This vibration shows a blue shift by 33 cm<sup>-1</sup> after CO<sub>2</sub> saturation, as seen in Figure S18, which is interpreted to be due to the [2-CNpyr]-CO<sub>2</sub> complex (carbamate).

Another important feature seen in Figure 3 is the C $\equiv$ O stretching mode of CO<sub>ad</sub> at 2103 cm<sup>-1</sup>. This new peak emerges at a potential of -1.7 vs Ag/Ag<sup>+</sup>, consistent with previous literature where CO surface adsorption is reported.<sup>43-45</sup> This peak is absent under N<sub>2</sub>, as shown in Figure S19. The 2103 cm<sup>-1</sup> peak shifts to lower wavenumbers and decreases in intensity as the potential is swept more negative, demonstrating a Stark shift of 26 cm<sup>-1</sup> V<sup>-1</sup> (Figure S20), which is consistent with ca. 21 cm<sup>-1</sup> V<sup>-1</sup> in literature.<sup>46</sup> Both the reduction in intensity and the redshift in SERS can be explained in terms of surface coverage reduction of CO<sub>ad</sub> and the desorption of CO from the surface with increased polarization as identified by GC analysis upon electrolysis.

There are other emerging vibrations under  $CO_2$ , as indicated along the dotted lines in Figure 3. As the electrode is negatively polarized to -1.1 V, a new peak at 1612 cm<sup>-1</sup> appears (marked with \* in Figure 3 where its intensity is highest) and can be assigned to  $v_{as}(CO_2^{-})$ , likely of the carboxylate via the carbene intermediate.<sup>42,44</sup> This feature is visible up to -1.7 V and then diminishes as the peak at 1565 cm<sup>-1</sup> intensifies. Although the 1565  $\mbox{cm}^{-1}$  peak is also seen in SERS under  $N_2$  at -1.8~V(Figure S17b), its appearance is more prominent under  $CO_2$ saturation and at an earlier potential at -1.1 V. Therefore, there could be two explanations: one where the IL ions are reorienting or breaking solvation and another where [EMIM]<sup>+</sup>-COOH forms.<sup>43,47</sup> Other features related to -COOH at 966 cm<sup>-1</sup> (out-of-plane bending of OH of COOH) and 537 cm<sup>-1</sup> (CO of COOH out-of-plane deformation) are previously reported at CO<sub>2</sub>RR potentials.<sup>42</sup> As illustrated in Figure 4,



Figure 4. Illustration of the possible interactions on the electrode surface. Left: Electron injection to the  $[EMIM]^+$  on the surface coupled with a proton transfer from  $[EMIM]^+$  to  $[EMIM]^+$ -CO<sub>2</sub><sup>-</sup> generates carbene and  $[EMIM]^+$ -COOH. Right: Electron injection to the 2-CNpyrH (protonated anion from CO<sub>2</sub> absorption reaction) on the surface coupled with a proton transfer to  $[EMIM]^+$ -CO<sub>2</sub><sup>-</sup> generates [2-CNpyr]<sup>-</sup> and  $[EMIM]^+$ -COOH.



**Figure 5.** Illustration of  $CO_2$  absorption by the [EMIM][2-CNpyr] based non-aqueous electrolyte and the proposed reaction schemes for  $CO_2RR$  at the electrode–electrolyte interface. The structures highlighted in the middle by the colored circle correspond to the post  $CO_2$  capture species (carboxylate, carbamate, [EMIM]<sup>+</sup>, and the protonated anion, 2-CNpyrH). The two possible reaction routes demonstrate the role of the  $CO_2$ -reactive ions in co-catalyzing CO generation as understood from the combined electrochemistry and spectroscopy analysis. [EMIM]<sup>+</sup> and 2-CNpyrH have protons that can transfer to the carboxylate or the carbamate to carboxylic acid species. However, it is more likely that 2-CNpyrH is the proton source in this case; therefore, [2-CNpyr]<sup>-</sup> release from the surface by the first electron transfer is illustrated.

there are multiple possible proton sources for this complex to form: C2 proton of  $[EMIM]^+$  ( $pK_{a(H2O)} \sim 23$ )<sup>48</sup> and -NHproton of 2-CNpyrH ( $pKa_{(H2O)} \sim 15$ ).<sup>49</sup> The lower  $pK_a$  of 2-CNpyrH makes it more likely being a proton donor. Upon electron injection, both the hydrogen on the C2 carbon of  $[EMIM]^+$  on the surface and 2-CNpyrH close to the surface may transfer proton to the  $[EMIM]^+$ -CO<sub>2</sub><sup>-</sup> adduct on the surface, thus releasing carbene and  $[2-CNpyr]^-$  while forming  $[EMIM]^+$ -COOH. It is possible that there are additional steps to the mechanism where hydrogen is first adsorbed on the surface upon reduction of  $[EMIM]^+$  or 2-CNpyrH and then combining with  $[EMIM]^+$ -CO<sub>2</sub><sup>-</sup>.

To better understand the role of 2-CNpyrH, LSV and SERS experiments were performed by intentionally adding the neutral 2-CNpyrH (0.5 M) to the supporting electrolyte (Figure S21). Current density increased at -1.45 V (vs Ag/  $Ag^+$ ), which is ascribed to the reduction of 2-CNpyrH forming the anion  $[2-CNpyr]^-$  and  $H^+$ . In SERS, it is seen that the intensity of the 2230 cm<sup>-1</sup> peak (CN stretch) increased with polarization up to -2.2 V (vs Ag/Ag<sup>+</sup>), thus confirming the increased surface concentration of the pyrrole, which can act as the proton source in CO<sub>2</sub>RR. However, the in situ SERS setup is not time-resolved to capture the short-lived intermediates to identify the exact mechanism. On the other hand, the FTIR analysis post CO<sub>2</sub>RR confirms the existence of carboxylic acid that was not in the solution prior to electrolysis as seen in Figure S15. The surface-adsorbed carboxylic acid complex ([EMIM]<sup>+</sup>-COOH) can further undergo electro-reduction to form surface-absorbed CO and OH<sup>-</sup>. Wang et al. reported the

favorable CO<sub>2</sub>RR pathways with [EMIM][BF<sub>4</sub>] IL and the possibility of [EMIM]<sup>+</sup>-CO<sup>-</sup> as an intermediate following [EMIM]<sup>+</sup>-COOH formation, similar to this study.<sup>36</sup> Therefore, we hypothesize the overall CO<sub>2</sub>RR reaction to be as shown in Figure 5.

An effective probe for detecting organic radical reaction intermediates generated in a solution is EPR spectroscopy. We therefore undertook a series of experiments to collect samples from electrolysis experiments performed under 1 atm  $N_{2}$  CO<sub>2</sub>, and <sup>13</sup>CO<sub>2</sub>. Aliquots of the electrolysis solution were removed from the sealed electrolysis cell after 30 min of electrolysis at -2.1 V vs Ag/Ag<sup>+</sup> using a gas-tight syringe and transferred to an N2-filled EPR tube, which was then immediately frozen in liquid N2. The sample collected from electrolysis under N2 showed a very weak isotropic signal at g = 2.003, which indicated a small amount of a radical organic species in solution when probed at 45 K (Figure 6). The sample collected from electrolysis under  $CO_2$  or  ${}^{13}CO_2$  showed an isotropic signal with the same g value, but the signal was much higher in intensity. No discernable difference was found in CW EPR on the solutions collected under CO<sub>2</sub> vs <sup>13</sup>CO<sub>2</sub>. We did not detect N hyperfine coupling in any of the samples, which suggests that the radical is localized at a C-atom, in alignment with the proposed mechanism in Figure 5 where the radical is the imidazolium carbene. The higher intensity of the EPR signal observed under CO<sub>2</sub> may be correlated with the current density, which was roughly six times higher under CO<sub>2</sub> as compared with electrolysis run under 1 atm N<sub>2</sub>, and that higher current density likely arises from faster generation of organic



**Figure 6.** X-band continuous-wave EPR spectrum of 0.1 M [EMIM][2-CNpyr] in the supporting electrolyte, before electrolysis under  $N_2$  and after electrolysis at -2.1 V vs Ag/Ag<sup>+</sup> under  $N_2$ , CO<sub>2</sub>, and <sup>13</sup>CO<sub>2</sub> environment. The CO<sub>2</sub>-saturated electrolyte before electrolysis is not shown as it is the same as the top curve under  $N_2$ . There were no observable differences between the samples made from CO<sub>2</sub> and <sup>13</sup>CO<sub>2</sub>. EPR conditions: temperature = 45 K; microwave power = 0.02 mW; modulation amplitude = 0.2 mT.

radicals due to the follow-up reactions with  $CO_2$  to liberate CO. We further analyzed the solutions obtained from electrolysis under <sup>13</sup>CO<sub>2</sub> using electron nuclear double resonance spectroscopy (ENDOR). We did not observe <sup>13</sup>C hyperfine coupling in the Q-band (34 GHz) Mims ENDOR spectrum, and this suggested that there is no radical character associated with  $CO_2$  or with  $CO_2$  bound to the organic radical.

Finally, the impact of water on CO<sub>2</sub>RR was studied by varying the water content of the electrolyte. It is well-known that most of ILs are hygroscopic and may contain some residual water despite rigorous drying procedures. The presence of water (a proton source) in the IL can potentially lead to enhanced reaction rates via proton-coupled electrontransfer pathways. Our results show that the effect of adding water up to 1 vol % does not change the CO<sub>2</sub>RR onset potential or the current as seen in Figure 7a. Further increase of water content to 8 vol % causes a positive shift in onset potentials, which could be due to the competing HER. Bulk electrolysis experiments with water containing electrolytes show an increase in current with increased water content at -2.2. V vs Ag/Ag<sup>+</sup>, as in Figure 7b. This is accompanied by increased selectivity (FE) for CO from 94 to 98% when water content increased from less than 0.1 to 1 vol %, as shown in Figure 7c. Further increase of water content to 8 vol % results

in the reduction of CO selectivity to 84% as a result of parallel  $H_2$  evolution reaction. Our previous work reports on the bicarbonate formation upon CO<sub>2</sub> absorption by [EMIM][2-CNpyr] in the presence of water.<sup>32</sup> Bicarbonate acts as a proton donor for CO<sub>2</sub>RR and HER, thus resulting in CO and  $H_2$ , respectively, on Ag.<sup>50</sup> These results imply that even in the presence of water up to 1 vol %, the electrode surface is covered with IL ions, thus suppressing HER.

## CONCLUSIONS

The CO<sub>2</sub>-reactive IL, [EMIM][2-CNpyr], was demonstrated as a catalytic electrolyte component for the electro-reduction of CO<sub>2</sub> to CO on the Ag surface. A high selectivity (>94%)and a stable current density for at least 12 h were achieved. These enhancements over a conventional acetonitrile-based electrolyte reveal the role of the carbamate and carboxylate species that form by the binding of CO<sub>2</sub> to [2-CNpyr]<sup>-</sup> and [EMIM]<sup>+</sup>, respectively. The spectro-electrochemical studies further revealed the role of these species on CO<sub>2</sub>RR at the electrode surface. In particular, the enrichment of surface species of [EMIM]<sup>+</sup>, 2-CNpyrH, and [EMIM]<sup>+</sup>-CO<sub>2</sub><sup>-</sup>, as captured by SERS between the applied potentials of -1.6 to -2.3 V vs Ag/Ag<sup>+</sup>, suggests the stabilization of the reaction intermediates and support the proposed reaction mechanism involving a radical formation as detected by EPR. The generation of CO on Ag was observed in SERS and CO was detected by the in-line gas chromatography during electrolysis. This study also demonstrated that the heterocyclic anion contributes to lowering of the CO<sub>2</sub>RR onset potential. These findings serve as a basis for improved mechanistic understanding of CO<sub>2</sub>RR in the presence of reactive ILs involving a basic anion.

## ASSOCIATED CONTENT

## **Supporting Information**

The Supporting Information is available free of charge at https://pubs.acs.org/doi/10.1021/acscatal.3c01538.

<sup>1</sup>H and <sup>13</sup>C NMR spectra for all compounds; characterization of the SERS electrode by SEM and EDX; FTIR and NMR analyses of liquidous products of  $CO_2RR$ ; GC calibration curve used for gaseous product analysis; SERS analysis of the control experiments; a comparison table of the examined electrolyte with literature for  $CO_2RR$  (PDF)



**Figure 7.** LSV of 0.1 M [EMIM][2-CNpyr] in supporting electrolyte showing the effect of water content on the onset potential (a); chronoamperometry at -2.2 V vs Ag/Ag<sup>+</sup> with samples containing 0.1, 1, and 8 vol % water (b); Faradaic efficiencies measured from chronoamperometry shown in b (c). Gaseous product composition was determined by GC (orange bars are for CO and green bar is for H<sub>2</sub>).

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## **Author Contributions**

S.D. performed electrochemical measurements and analysis. O.K.C. built the SERS cell to perform the spectro-electrochemical measurements. E.C. synthesized the precursors and ionic liquids and caried out the NMR and ATR-FTIR analyses. K.Y.C.L. conducted the EPR experiments on in situ generated reaction intermediates from electrolysis experiments, and G.R. assisted with collection of EPR data. L.A.B. conceptualized the EPR characterization of samples, and R.D.B. provided expertise in interpretation of EPR data. B.G. conceptualized the study, contributed to the discussions of the results, and oversaw the project. All authors contributed to the writing of the manuscript.

#### Notes

The authors declare no competing financial interest.

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