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**Permalink** https://escholarship.org/uc/item/8bx3v0t6

**Journal** Applied and Environmental Microbiology, 80(2)

**ISSN** 0099-2240

# **Authors**

Javidpour, Pouya Pereira, Jose H Goh, Ee-Been <u>et al.</u>

**Publication Date** 

2014-01-15

# DOI

10.1128/aem.03194-13

Peer reviewed



# Biochemical and Structural Studies of NADH-Dependent FabG Used To Increase the Bacterial Production of Fatty Acids under Anaerobic Conditions

Pouya Javidpour,<sup>a,b</sup> Jose H. Pereira,<sup>a,b</sup> Ee-Been Goh,<sup>a,b</sup> Ryan P. McAndrew,<sup>a,b</sup> Suzanne M. Ma,<sup>a,b\*</sup> Gregory D. Friedland,<sup>a,c\*</sup> Jay D. Keasling,<sup>a,b,d</sup> Swapnil R. Chhabra,<sup>a,b</sup> Paul D. Adams,<sup>a,b,d</sup> Harry R. Beller<sup>a,e</sup>

Joint BioEnergy Institute, Emeryville, California, USA<sup>a</sup>; Physical Biosciences Division, Lawrence Berkeley National Laboratory, Berkeley, California, USA<sup>b</sup>; Biomass Science and Conversion Technology Department, Sandia National Laboratories, Livermore, California, USA<sup>c</sup>; Department of Bioengineering, University of California, Berkeley, Berkeley, California, USA<sup>d</sup>; Earth Sciences Division, Lawrence Berkeley National Laboratory, Berkeley, California, USA<sup>e</sup>

Major efforts in bioenergy research have focused on producing fuels that can directly replace petroleum-derived gasoline and diesel fuel through metabolic engineering of microbial fatty acid biosynthetic pathways. Typically, growth and pathway induction are conducted under aerobic conditions, but for operational efficiency in an industrial context, anaerobic culture conditions would be preferred to obviate the need to maintain specific dissolved oxygen concentrations and to maximize the proportion of reducing equivalents directed to biofuel biosynthesis rather than ATP production. A major concern with fermentative growth conditions is elevated NADH levels, which can adversely affect cell physiology. The purpose of this study was to identify homologs of *Escherichia coli* FabG, an essential reductase involved in fatty acid biosynthesis, that display a higher preference for NADH than for NADPH as a cofactor. Four potential NADH-dependent FabG variants were identified through bioinformatic analyses supported by crystallographic structure determination (1.3- to 2.0-Å resolution). *In vitro* assays of cofactor (NADH/ NADPH) preference in the four variants showed up to  $\sim$ 35-fold preference for NADH, which was observed with the *Cupriavidus taiwanensis* FabG variant. In addition, FabG homologs were overexpressed in fatty acid- and methyl ketone-overproducing *E. coli* host strains under anaerobic conditions, and the *C. taiwanensis* variant led to a 60% higher free fatty acid titer and 75% higher methyl ketone titer relative to the titers of the control strains. With further engineering, this work could serve as a starting point for establishing a microbial host strain for production of fatty acid-derived biofuels (e.g., methyl ketones) under anaerobic conditions.

recent trend in biofuel research is to produce fuels that can directly replace petroleum-derived products such as gasoline and diesel fuel. Many of these advanced biofuels can be produced by altering native fatty acid biosynthetic pathways in microorganisms such as Escherichia coli and Saccharomyces cerevisiae and take the form of fatty alcohols, esters, and alkanes (1). Studies of these biofuel pathways have typically been conducted under aerobic conditions. It is desirable, however, to establish a microbial host strain that can function under fully anaerobic conditions. A major concern with aerobic culture conditions is that molecular oxygen, being the preferred terminal electron acceptor, consumes reducing equivalents derived from catabolic pathways to support growth and ATP production (2). This diverts reducing power away from metabolic pathways that lead to reduced biofuels. Also, aeration and oxygen-level control on an industrial scale represent additional operating expenses that detract from the profitability of biofuel production and undermine cost competitiveness relative to petroleum-based fuels.

There have been studies of obligate anaerobic production of higher alcohols through fermentation (3). However, in the case of producing fatty acid-based biofuels, fermentative pathways may not be desired, since carbon and electrons are lost through mixed acid fermentation (4). Another issue that arises with anaerobic microbial growth is redox imbalance (e.g., a relatively high NADH/NAD<sup>+</sup> ratio). This can have detrimental effects on cell physiology, both at a regulatory level and at the enzyme function level (5–9).

Several strategies to address redox imbalance focus on enzyme

cofactor usage, including altering the global availability of cofactors through metabolic engineering of the pentose phosphate pathway or overexpression of NADH oxidases, kinases, or transhydrogenases (10). Another strategy involves engineering pathway-specific enzymes that utilize cofactors, either to relax selectivity or change cofactor specificity. These cofactor-based approaches can lead to increased titers of target compounds and productivity (11, 12).

The *E. coli* fatty acid synthetic pathway involves two reductases that utilize NAD cofactors, FabG and FabI. Whereas FabI displays activity with both NADH and NADPH (13), FabG, which belongs to the short-chain dehydrogenase/reductase (SDR) enzyme family, is active only with NADPH in characterized versions (14). In the production of one palmitic acid ( $C_{16}$ ) molecule, FabG oxidizes seven NADPH molecules. FabG is essential, as deletion of the corresponding gene is lethal (15). The vast majority of *E. coli* FabG

Received 23 September 2013 Accepted 30 October 2013 Published ahead of print 8 November 2013

Address correspondence to Harry R. Beller, hrbeller@lbl.gov.

<sup>\*</sup> Present address: Suzanne M. Ma, Amyris, Inc., Emeryville, California, USA; Gregory D. Friedland, Nodality, Inc., South San Francisco, California, USA.

Supplemental material for this article may be found at http://dx.doi.org/10.1128 /AEM.03194-13.

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homologs have been characterized as displaying either absolute specificity for NADPH or a much higher preference for NADPH than NADH. Our concept is that a FabG homolog displaying a higher preference for NADH as a cofactor could be heterologously expressed in *E. coli* to increase fatty acid production under anaerobic conditions. A precedent for the potential of a NADH-specific FabG homolog is the study of mevalonate production using variant 3-hydroxy-3-methylglutaryl (HMG)-coenzyme A (CoA) reductases, in which it was observed that NADH-utilizing reductases produced higher levels of mevalonate during anaerobic growth than variants that preferred NADPH (16).

The goal of this study was to identify FabG homologs with a high preference for NADH that could be expressed in *E. coli* to increase fatty acid production under anaerobic conditions. We report several FabG homologs that, when overexpressed, led to increased production of free fatty acids and methyl ketones (fatty acid-derived biofuels) in an *E. coli* host under anaerobic conditions. With further engineering, this work could serve as a starting point for establishing a microbial host strain for production of fatty acid-derived biofuels under anaerobic conditions.

### MATERIALS AND METHODS

**Reagents, synthesized genes, and oligonucleotides.** Acetoacetyl coenzyme A (acetoacetyl-CoA), NADH, NADPH, and fatty acid methyl and ethyl esters were purchased from Sigma-Aldrich (St. Louis, MO) and were of the highest purity available. Genes were synthesized by GenScript (Piscataway, NJ) and codon optimized for expression in *E. coli* with the proprietary GenScript OptimumGene algorithm. The synthesized gene sequences are listed in Table S1 in the supplemental material. Oligonucleotides were purchased from Integrated DNA Technologies (Coralville, IA). All organic solvents were purchased from Sigma-Aldrich and were pesticide residue analysis grade or better. Highly purified water (18-M $\Omega$ resistance) obtained from a Barnstead Nanopure system (Thermo Scientific, Waltham, MA) was used to prepare the growth medium and all other aqueous solutions described in this article.

**Bioinformatics.** Structural alignments of *E. coli* FabG bound to NADP<sup>+</sup> (17) and SDRs found in the Protein Data Bank were performed with 3D-Hit (18). The aligned structures were then separated into two groups, based on whether NAD(H) or NADP(H) was bound, and the sequences were analyzed for patterns at residues near the 2' position of the cofactor adenine. Putative FabG homologs possessing residues consistent with patterns found in NAD(H)-binding SDRs were identified by BLAST searching (19), and the respective sequences were aligned to that of *E. coli* FabG using MUSCLE (20). Homologs from organisms that have been isolated from environments at near-neutral pH and annotated as mesophilic in the Integrated Microbial Genomes system (Joint Genome Institute) (Table 1) were selected for biochemical characterization and fatty acid production experiments to help ensure that the enzymes would function properly in *E. coli*.

**DNA assembly of** *fabG* variants. Plasmid pPJ100 (Table 1) consists of the wild-type *E. coli fabG* gene and sequence encoding an N-terminal  $6\times$ His tag cloned into the pET-24 expression vector (Novagen Biosciences, Madison, WI) for protein purification. Genes for the other *fabG* homologs were synthesized with sequences encoding N-terminal  $6\times$ His tags and cloned into pET-24. For fatty acid production, each *fabG* variant was PCR amplified from its respective pET-24 vector and then cloned, using the sequence- and ligation-independent cloning (SLIC) method (21), into pPJ132, which was adapted from plasmid pKS1 (22) to express the *lacI* repressor as well as the leaderless thioesterase '*tesA* (22, 23). Plasmids were amplified in *E. coli* strain DH10B during cloning, and protein was expressed in strain BL21(DE3). The fatty acid production host strain was *E. coli* DH1 $\Delta$ *fadE*, which was disabled in  $\beta$ -oxidation in order to accumulate fatty acids (22). For methyl ketone production, the *C. taiwanensis fabG* gene was PCR amplified and cloned, as described above, into pBbE8k-RFP (24), resulting in pEG1600 (Table 1). Subsequently, the *araC*-P<sub>BAD</sub>-*fabG* fragment from pEG1600 was cloned into pEG855 (25) using the SLIC method (21), resulting in pEG1635. pEG1635 was transformed into *E. coli* EGS522 (Table 1) with pEG530 (25) for analysis of anaerobic methyl ketone production *in vivo*.

*fabG* expression and protein purification. An overnight culture of E. coli BL21(DE3) expressing a fabG variant in pET-24 was used to inoculate 1 liter of lysogeny broth (LB) supplemented with 50 µg/ml kanamycin, which was then grown at 37°C to an optical density at 600 nm (OD<sub>600</sub>) of 0.4 to 0.6. At that point, protein expression was induced by addition of 0.5 mM isopropyl-B-D-thiogalactopyranoside (IPTG), and cells were grown overnight at 18°C. The cells were harvested by centrifugation, washed with 50 ml of buffer F (50 mM Tris-Cl [pH 7.4], 250 mM NaCl, and 10% glycerol), and stored as pellets at  $-80^{\circ}$ C. The cells were lysed with an EmulsiFlex-C3 high-pressure homogenizer (Avestin, Ottawa, ON, Canada) after resuspension in 100 ml of buffer F. The lysate was clarified by centrifugation (15,000  $\times$  g for 1 h at 4°C) followed by binding of lysate supernatant to 3 ml of Profinity immobilized metal affinity chromatography (IMAC) Ni resin (Bio-Rad, Hercules, CA) at 4°C for at least 30 min. Bound protein was sequentially washed with 20, 40, and 80 mM imidazole in buffer F. Pure FabG was eluted at 150, 250, and 400 mM imidazole in buffer F. Pure fractions were pooled together, concentrated with an Amicon Ultra-15 10,000-nominal-molecular-weight-limit (NMWL) concentrator (Millipore, Billerica, MA), and exchanged into buffer F using a PD-10 desalting column (GE Healthcare Life Sciences, Pittsburgh, PA).

In vitro assay for FabG specific activity. Activity was determined by monitoring the reduction of acetoacetyl-CoA in the presence of either NADH or NADPH over 10 min using a 96-well plate on a SpectraMax M2 plate reader (Molecular Devices, Sunnyvale, CA). Although the true FabG substrate is a β-ketoacyl-acyl carrier protein (ACP), acetoacetyl-CoA was chosen as an in vitro substrate due to its commercial availability and amenability for assay preparation. Although the absolute specific activity of FabG is considerably higher for acetoacetyl-ACP than for acetoacetyl-CoA (26), assays with acetoacetyl-CoA were sufficiently sensitive for the purposes of this study. The change in 340-nm absorbance from the conversion of NAD(P)H to NAD(P)<sup>+</sup> was used to determine reaction rate, based on a standard curve of NADH concentration versus absorbance. Assays were performed in 100 mM NaPO<sub>4</sub> buffer (pH 7.4) containing 0.5 to 8 µg FabG and 240 µM NADH or NADPH, and were initiated with the addition of 500 µM acetoacetyl-CoA in a total volume of 250 µl. For the control reactions, acetoacetyl-CoA was replaced with an equal volume of water.

Crystallization of fabG homologs in complex with NADH. The Acholeplasma laidlawii FabG (Al\_FabG), Bacillus sp. strain SG-1 FabG (Bs\_FabG), Cupriavidus taiwanensis FabG (Ct\_FabG), and Plesiocystis pacifica FabG (Pp\_FabG) solutions were concentrated to 10 mg/ml and screened using the sparse matrix method (27) with a Phoenix Robot (Art Robbins Instruments, Sunnyvale, CA) using the following crystallization screens: Crystal Screen I and II, Index, PEG/Ion, SaltRx, and PEGRx (Hampton Research, Aliso Viejo, CA) and Berkeley Screen. The optimum conditions for crystallization of the different homologs were as follows: Al\_FabG, 0.2 M ammonium fluoride and 20% polyethylene glycol 3350 (PEG 3350); Bs\_FabG, 0.2 M sodium citrate and 20% PEG 3350; Ct\_FabG, 0.1 M sodium malonate (pH 7.0), 0.03 M citric acid, 0.07 M Bis-Tris propane (pH 7.6), and 20% PEG 3350; and Pp\_FabG, 0.2 M ammonium tartrate dibasic (pH 7.0) and PEG 3350. Crystals were obtained after 2 days by the sitting-drop vapor diffusion method with drops consisting of a mixture of 0.5 µl protein solution and 0.5 µl reservoir solution.

X-ray data collection and structure determination. Crystals were placed in a reservoir solution containing 15 to 20% glycerol and then flash frozen in liquid nitrogen. Data sets for the Al\_FabG, Bs\_FabG, Ct\_FabG, and Pp\_FabG were collected at the Berkeley Center for Structural Biology beamlines 8.2.1 and 8.2.2 of the Advanced Light Source at Lawrence Berkeley National Laboratory (LBNL). The diffraction data were recorded

#### TABLE 1 Bacterial strains and plasmids used in this study

Studio on placesid	Delevent above staristic(a)	Reference
	Relevant characteristic(s)	or source
E. coli strains		10
BL21(DE3)	F omp1 gal acm ion hsats <sub>B</sub> ( $\mathbf{r}_{B}$ m <sub>B</sub> ) $\lambda$ (DE3)	40
	enal recal gyrA96 tm-1 gmV44 retA1 nsak1/ $(r_k - m_{k-1})$ A	41
DHIAfaaE	DHI Ajade	22
DHIUB	F mcrA enaA1 recA1 gale15 galK16 nupG rpsL $\Delta lacX/4 \varphi 80 lacZ\Delta M15$ araD139 $\Delta (ara leu)/69/\Delta (mrr-hsaRMS-mcrBC) R$	42
EGS522		25
EG5895	EG5522 with pEG530 and pEG435	ZO This starter
EGS16/0	EG522 with pEG530 and pEG1635	This study
PJ001	BL21(DE2) with pP/100	This study
PJ002	BL21(DE3) with pP)101	This study
PJ003	BL21(DE3) with pP1102	This study
PJ004	BL21(DE3) with pP)104	This study
PJ005	BL1(DE3) with pP)103	This study
PJ010	DH1 $\Delta jaae$ with pP[133]	This study
PJ011		This study
PJ012		This study
PJ013	DH1 $\Delta jaae$ with pP[136	This study
PJ014	DHIAJaae with pr)157	This study
Plasmids		
pBbE8k-RFP	$Km^r$ ; ColE1 plasmid; $P_{BAD}$ promoter with <i>araC</i> repressor	24
pEG530	Cm <sup>r</sup> ; ' <i>tesA</i> , acyl-CoA oxidase (Mlut_11700) and <i>fadB</i> under <i>lacUV5</i> promoter	25
pEG855	Km <sup>r</sup> ; <i>fadM</i> under P <sub>tre</sub> promoter	25
pEG1600	Km <sup>r</sup> ; <i>C. taiwanensis fabG</i> cloned into pBbE8k-RFP at NdeI and BamHI sites	This study
pEG1635	$Km^r$ ; araC-P <sub>BAD</sub> -fabG fragment from pEG1600 cloned into pEG855 at the NdeI site	This study
pET-24a(+)	Km <sup>r</sup>	Novagen
pKS1	Cm <sup>r</sup> ; p15a vector containing ' <i>tes</i> A under <i>lacUV5</i> promoter	22
pPJ100	$Km^r$ ; <i>E. coli fabG</i> , with N-terminal 6× His tag sequence, cloned into pET-24a(+) at NdeI and BamHI sites	This study
pPJ101	$Km^r$ ; Acholeplasma laidlawii PG-8A ACL-0504 fabG, with N-terminal 6× His tag sequence, in pET24a(+)	This study
pPJ102	$Km^r$ ; <i>Bacillus</i> sp. SG-1 BSG1-13201 <i>fabG</i> , with N-terminal 6× His tag sequence, in pET24a(+)	This study
pPJ104	$Km^r$ ; Cupriavidus taiwanensis LMG 19424 RALTA_A2639 fabG, with N-terminal 6× His tag sequence, in pET24a(+)	This study
pPJ103	$Km^r$ ; <i>Plesiocystis pacifica</i> SIR-1 PPSIR1_02236 <i>fabG</i> , with N-terminal 6× His tag sequence, in pET24a(+)	This study
pPJ132	Cm <sup>r</sup> ; <i>lacI</i> repressor cloned into pKS1	This study
pPJ133	$Cm^r$ ; codon-optimized <i>E. coli fabG</i> , with N-terminal 6× His tag sequence, in pPJ132	This study
pPJ134	Cm <sup>r</sup> ; Acholeplasma laidlawii PG-8A ACL-0504 fabG, with N-terminal 6× His tag sequence, in pPJ132	This study
pPJ135	Cm <sup>r</sup> ; Bacillus sp. SG-1 BSG1-13201 fabG, with N-terminal 6× His tag sequence, in pPJ132	This study
pPJ136	Cm <sup>r</sup> ; Cupriavidus taiwanensis LMG 19424 RALTA_A2639 fabG, with N-terminal 6× His tag sequence, in pPJ132	This study
pPJ137	$Cm^r$ ; <i>Plesiocystis pacifica</i> SIR-1 PPSIR1_02236 <i>fabG</i> , with N-terminal 6× His tag sequence, in pPJ132	This study

using an ADSC-Q315r detector. The data sets were processed using the program HKL-2000 (28).

Crystal structures of Al\_FabG, Bs\_FabG, Ct\_FabG, and Pp\_FabG were determined by the molecular-replacement method with the program PHASER (29) within the Phenix suite (30), using the structure of E. coli FabG (PDB accession no. 1Q7B) as a search model. The atomic positions obtained from molecular replacement and the resulting electron density maps were used to build all the FabG homolog structures and initiate crystallographic refinement and model rebuilding. Structure refinement was performed using the phenix.refine program (31). Translation-liberation-screw (TLS) refinement with each protein chain as a single TLS group was used in the process. Manual rebuilding using COOT (32) and addition of water molecules allowed for construction of the final models. Five percent of the data were randomly selected for cross validation. Root mean square deviation differences from ideal geometries for bond lengths, angles, and dihedrals were calculated with PHENIX (30). The overall stereochemical quality of the final models was assessed using the program MOLPROBITY (33).

**Anaerobic growth conditions for fatty acid production.** Sample handling was primarily conducted in an anaerobic glove box (Coy Laboratory Products, Grass Lake, MI) under an atmosphere of 85% N<sub>2</sub>, 10% CO<sub>2</sub>, and 5% H<sub>2</sub>. Anaerobic reagent water was prepared by autoclaving and then cooling under an atmosphere of ultrahigh-purity nitrogen gas for at least 20 min. EZ Rich medium components (Teknova, Hollister, CA) were mixed, filtered, and then stored in the anaerobic glove box for at least 16 h before being mixed with the appropriate volume of anaerobic water. Sterile 30-ml glass tubes and Mininert caps (VICI, Baton Rouge, LA) were also stored in the anaerobic glove box for at least 16 h before use. Anaerobic cultures, consisting of 20 ml of EZ Rich medium containing 0.2% glucose and supplemented with 30 µg/ml chloramphenicol, were inoculated inside the anaerobic glove box with aerobically grown 10-ml overnight cultures at a 1:100 dilution and sealed with Mininert caps. Sealed cultures were incubated outside the anaerobic glove box at 37°C without shaking, and samples for OD<sub>600</sub> measurements were collected inside the glove box. Protein expression was induced in the glove box by addition of 0.2 mM IPTG in anaerobic water.

**Extraction and analysis of fatty acids.** Fatty acids were extracted from anaerobically grown cells using high-purity methanol and hexane as described previously (34). Based on preliminary experiments, more than 80% of total (intracellular plus extracellular) fatty acids are recovered using this cell pellet extraction method. The hexane phase was concentrated to 100  $\mu$ l under a stream of ultrahigh-purity nitrogen gas and de-



FIG 1 Alignments of short-chain dehydrogenase/reductase (SDR) enzymes with structures deposited in the PDB (identified by species name followed by the PDB accession number in parentheses) that bind either NADH or NADPH. Amino acid numbering refers to the native *E. coli* FabG sequence. Enzymes that prefer NADH possess a conserved aspartate residue (see the text and arrows in figure).

rivatized with ethereal diazomethane prepared with a small-scale diazomethane generator (Sigma-Aldrich) (34). The derivatized extract was concentrated to 100  $\mu$ l for gas chromatography analysis. Care was taken to ensure that organic solvents contacted only glass or polytetrafluoroethylene (PTFE) that were precleaned with high-purity acetone.

Fatty acid extract samples were applied to a Thermo Scientific Focus gas chromatograph (GC) equipped with a TriPlus autosampler, Trace TR-5 column (5-m length, 0.25-mm inner diameter, 0.25-µm film thickness), and a flame ionization detector (FID). The GC oven was programmed from 45°C (held for 2.25 min) to 300°C at 40°C/min; the FID temperature was 350°C. The injection port temperature was 250°C, and the carrier gas, ultrahigh-purity helium, flowed at a constant pressure of 65 kPa. Injections were splitless with the split turned on after 1 min. Fatty acid concentrations were determined by external standard quantification using  $C_8$  to  $C_{20}$  fatty acid methyl ester standards.

Anaerobic growth conditions for methyl ketone production. Preparation of media and cultures for anaerobic growth conditions were performed as described above. Briefly, 120-ml serum bottles with 60 ml of EZ Rich medium containing 0.2% glucose supplemented with 25  $\mu$ g/ml chloramphenicol and 50  $\mu$ g/ml kanamycin were inoculated with overnight aerobic cultures at starting OD<sub>600</sub> values of ~0.02. Serum bottles were then sealed with 20-mm butyl rubber stoppers and crimp seals to maintain an anaerobic environment. Protein expression was induced in the anaerobic glove box by addition of 0.5 mM IPTG and 1 mM arabinose at 6 h. Two milliliters of decane amended with 40 ng/µl of perdeuterated tetracosane (C<sub>24</sub>D<sub>50</sub>) internal standard was also added at 6 h. Sealed cultures were incubated outside the anaerobic glove box at 37°C with mild shaking (120 rpm) to allow partitioning of methyl ketones into the decane overlay, and samples for OD<sub>600</sub> measurements were collected inside the glove box via syringe.

**Extraction and analysis of methyl ketones.** After 96 h of anaerobic growth, the decane overlay was removed for direct gas chromatography-

mass spectrometry (GC-MS) analysis as previously described (25). Briefly, GC-MS analyses were performed with a model 7890A GC (Agilent, Santa Clara, CA) with a DB-5 fused silica capillary column (30-m length, 0.25-mm inner diameter, 0.25- $\mu$ m film thickness; J & W Scientific) coupled to an HP 5975C series quadrupole mass spectrometer; 1- $\mu$ l injections were performed by a model 7683B autosampler. The GC oven was programmed from 40°C (held for 3 min) to 295°C at 15°C/min; the injection port temperature was 250°C, and the transfer line temperature was 280°C. The carrier gas, ultrahigh-purity helium, flowed at a constant rate of 1 ml/min. Injections were splitless, with the split turned on after 0.5 min. Quantification of methyl ketones was carried out with external standards as previously described (25).

**PDB** accession numbers. Coordinates for Al\_FabG, Bs\_FabG, Ct\_FabG, and Pp\_FabG have been deposited in the Protein Data Bank with accession numbers 4NBT, 4NBU, 4NBU, and 4NBW, respectively.

### RESULTS

**FabG homolog selection strategy.** In order to identify potential NADH-utilizing FabG homologs, structural and sequence alignments were made between *E. coli* FabG bound to NADP<sup>+</sup> (17) and SDRs from the Protein Data Bank. The Asp36 residue (*E. coli* FabG numbering) is well conserved among NAD-binding SDRs, whereas in the NADP-binding enzymes, there appear to be only slight preferences for either a tyrosine or serine at that position (Fig. 1). Moreover, there is a preference for a basic amino acid (arginine or lysine) at residue 15. Using these residue motifs as a basis, FabG homologs from other microbial organisms with molecular motifs consistent with NAD-binding SDRs were identified. On the basis of annotations in the Integrated Microbial Genomes system (Joint Genome Institute), we focused on organisms that



FIG 2 Specific activity of FabG homologs from *E. coli* and other species toward acetoacetyl-CoA. The number below each species name is the ratio of activity with NADH to activity with NADPH. *E. coli* FabG was essentially inactive with NADH. Bar heights represent average activities from 3 replicates, and error bars represent 1 standard deviation.

are mesophilic and found in environments at near-neutral pH to help ensure that the homologous enzymes would function properly in *E. coli*. These *fabG* homologs, encoded in plasmids pPJ134-137, are listed in Table 1.

*In vitro* assay indicates FabG homologs that have preference for NADH over NADPH. FabG homologs were purified with Nterminal 6×His tags and assayed *in vitro* with the substrate analog acetoacetyl-CoA in the presence of either NADH or NADPH.

TABLE 2 Data collection and refinement statistics

The specific activities of *E. coli* FabG and four homologs are shown in Fig. 2. As expected from previous reports (14), *E. coli* FabG displayed a specific activity of approximately 2  $\mu$ mol/min/mg with NADPH as a cofactor and was essentially inactive in the presence of NADH. On the other hand, the selected FabG homologs displayed higher activity with NADH as a cofactor than with NADPH, ranging from a 2- to 36-fold-higher preference (Fig. 2). Also, with the exception of the *P. pacifica* variant, each homolog displayed higher absolute specific activity toward the substrate than *E. coli* FabG did. Interestingly, the *C. taiwanensis* variant had almost 7-fold-higher activity than *E. coli* FabG and displayed the highest preference for NADH of all the enzymes assayed.

Structural analyses of FabG homolog cofactor-binding sites. Crystals of the four FabG homologs diffracted between 1.3- and 2.0-Å resolution. The statistics for X-ray data collection and structure refinement are summarized in Table 2. The highly conserved tetrad of Asn110/Ser138/Tyr151/Lys155 residues (E. coli numbering) are essential for FabG catalytic activity (35). A structural comparison between NADPH-utilizing E. coli FabG and the NADHutilizing homologs Al\_FabG, Bs\_FabG, Ct\_FabG, and Pp\_FabG showed that residues surrounding the adenosine ribose moiety of the cofactor differ significantly in these enzymes. The most obvious structural difference between E. coli FabG and the NADHutilizing homologs is the presence of a negatively charged aspartate (corresponding to the Ala36 position in E. coli FabG) interacting with the 2'- and 3'-hydroxyl groups of the adenosine ribose (Fig. 3). NADPH binding is unfavorable as a result of electrostatic repulsion between this aspartate residue and the NADPH

	Value(s) for FabG homolog <sup>a</sup> :					
Parameter	Al_FabG	Bs_FabG	Ct_FabG	Pp_FabG		
Resolution range (Å)	39.49-1.48 (1.533-1.48)	23.33-1.34 (1.387-1.34)	37.33–1.645 (1.703–1.645)	44.83-2.00 (2.072-2.00)		
Space group	P 1	P 1	P 43 21 2	P 21		
Unit cell dimensions ( <i>a</i> , <i>b</i> , and <i>c</i>	61.96, 62.36, 66.76;	63.41, 68.77, 70; 67.85,	111.76, 111.76, 79.19; 90,	77.73, 75.14, 97.72; 90,		
[Å]; α, β, and γ [°])	66.03, 76.63, 79.93	88.65, 62.64	90, 90	113.43, 90		
No. of unique reflections	142,273 (13,758)	201,633 (17,136)	60,813 (5,545)	61,547 (6,103)		
Completeness (%)	96.44 (93.39)	93.71 (79.62)	99.19 (91.94)	88.02 (87.64)		
Mean I/sigma(I)	14.21 (3.43)	11.30 (2.65)	12.64 (1.7)	5.53 (2.30)		
Wilson B-factor	12.29	12.59	19.78	8.35		
R-merge	0.039	0.044	0.102	0.127		
R-work	0.1282 (0.1678)	0.1606 (0.2304)	0.1443 (0.2277)	0.2047 (0.2394)		
R-free	0.1540 (0.1824)	0.1735 (0.2604)	0.1600 (0.2741)	0.2541 (0.3018)		
No. of:						
Atoms	16,056	8,420	7,814	8,164		
Macromolecules	4	4	2	4		
Water	1,328	962	542	1,368		
NADH	4	4		4		
Protein residues	958	962	492	1,008		
RMS(bonds [Å]) <sup>b</sup>	0.017	0.016	0.009	0.016		
RMS(angles [°])	1.59	1.54	1.15	1.19		
Ramachandran favored (%)	97	98	98	98		
Ramachandran outliers (%)	0	0.1	0	0.1		
Average B-factor	15.90	20.40	24.80	11.10		

<sup>a</sup> Al\_FabG, Acholeplasma laidlawii FabG; Bs\_FabG, Bacillus sp. SG-1 FabG; Ct\_FabG, Cupriavidus taiwanensis FabG; Pp\_FabG, Plesiocystis pacifica FabG. Statistics for the highest-resolution shell are shown in parentheses.

<sup>b</sup> RMS, root mean square.



FIG 3 Comparison of cofactor-binding sites in FabG homologs. (a) Structural overlay of the Al\_FabG, Bs\_FabG, Ct\_FabG, and Pp\_FabG homologs with NADPH. (b) Residues interacting with NADPH in the *E. coli* FabG (Ec\_FabG) crystal structure. (c) Overlay of *E. coli* and Ct\_FabG, depicting the clash that occurs between the NADPH 2'-phosphate and Asp36 (*E. coli* numbering) of Ct\_FabG. Dotted lines represent ionic and polar interactions. Numbers represent distances between atoms in angstroms.

2'-phosphate group. A similar conclusion was previously reported for other SDR family enzymes (35, 36).

To understand the structural basis for the differences in FabG homolog activity with NADH versus NADPH (Fig. 2), residues making direct interactions with the NADPH 2'-phosphate from the *E. coli* FabG structure were compared against the respective residues in the NADH-utilizing homologs. The *E. coli* FabG structure in complex with NADPH shows residues Ser14, Arg15, and Thr37 interacting with the NADPH 2'-phosphate through polar and ionic interactions (17) (Fig. 3b). None of these residues is conserved in Al\_FabG, Bs\_FabG, Ct\_FabG, or Pp\_FabG (Table 3). Ser14 is replaced by Ala residues in all the NADH-

utilizing FabGs. Arg15 is replaced by Lys, Asn, Ala, and Asn in Al\_FabG, Bs\_FabG, Ct\_FabG, and Pp\_FabG, respectively. The substitution of a positive-charged Lys residue in Al\_FabG for Arg15 of *E. coli* FabG may be responsible for the higher activity observed with NADPH for the Al\_FabG homolog (Fig. 2). Thr37 of *E. coli* FabG is replaced by the apolar residues Leu, Phe, Val, and Leu in Al\_FabG, Bs\_FabG, Ct\_FabG, and Pp\_FabG, respectively.

Anaerobic fatty acid production. It is possible that because lipid production correlates with cell division (37), and E. coli grows at a relatively lower rate under anaerobic conditions, fatty acid biosynthesis as a whole would also proceed more slowly than during aerobic growth. If so, then the effect of overexpression of fabG may not be experimentally detectable. To address this concern, we chose *E. coli* DH1 $\Delta$ *fadE* expressing the 'tesA thioesterase (22) as the host strain for fatty acid production in this study (Table 1). The thioesterase activity would enable overproduction of fatty acids via hydrolysis of acyl-ACP thioesters and consequent deregulation of fatty acid biosynthesis by precluding acyl-ACP-mediated inhibition. The DH1 $\Delta$ fadE strain was also utilized for the overproduction of fatty acid-based fuels, including fatty acid ethyl esters (FAEEs), alcohols, and waxes, and thus serves as an established model system (22). In order to control gene expression, the lacI repressor was introduced into the pKS1 plasmid, which carries the 'tesA gene, and the resulting vector was used to express each respective fabG homolog under the control of a lacUV5 promoter (24) (Table 1). The control strain consisted of DH1 $\Delta$ fadE expressing a codon-optimized version of the native E. coli fabG from the pKS1 vector, so that all tested strains would be under similar stress from gene overexpression. Codon-optimized fabG was chosen to create a sequence sufficiently distinct from the chromosomal fabG to help prevent possible integration of plasmid sequence into the chromosome via homologous recombination.

Each strain reached a final  $OD_{600}$  of approximately 0.45 after 24 h, and there were no significant differences in growth among the strains (see Fig. S1 in the supplemental material). Fatty acids were extracted from pelleted cultures at the end of the 24-h incubation, the extracts were derivatized with ethereal diazomethane to form fatty acid methyl esters (FAMEs) and then subjected to GC-FID analysis.

The absolute titers of free fatty acids produced by the strains were much lower than the  $\sim 1$  g/liter previously reported under aerobic conditions, although the latter cultures were grown to a higher final cell density (22) (Fig. 4). The distribution of fatty acids was as expected, based on the preference of the TesA thioesterase for C<sub>14</sub> and C<sub>16</sub> acyl groups (38). The major fatty acids produced anaerobically by the strains were saturated C<sub>14</sub>, C<sub>16</sub>, and C<sub>18</sub>, with

**TABLE 3** Sequence comparison of the *E. coli* FabG residues that interact with the NADPH 2'-phosphate with the respective residue positions in NADH-utilizing homologs

	Residue interacting with NADPH 2'-phosphate <sup>a</sup>			
FabG variant	Ser14	Arg15	Thr37	
Al_FabG	Ala15	Lys16	Leu38	
Bs_FabG	Ala22	Asn23	Phe45	
Ct_FabG	Ala14	Ala15	Val37	
Pp_FabG	Ala21	Asn22	Leu44	

<sup>a</sup> Ser14, Arg15, and Thr37 refer to E. coli FabG residues.





FIG 4 Summary of total free fatty acid titer and *in vitro* assay data, normalized to the respective values for *C. taiwanensis* FabG, which produced 11.1 mg/liter total free fatty acids. Titers are from separate *E. coli* DH1 $\Delta$ fadE strains overexpressing *'tesA* and a *fabG* variant under anaerobic conditions. The control strain overexpressed a codon-optimized sequence of the native *E. coli fabG*. Total free fatty acid titer (black bars), NADH specific activity (white bars), and ratio of NADH:NADPH specific activities (hatched bars) are shown. Bar heights represent average titers from 3 replicates, and error bars represent 1 standard deviation.

 $C_{14}$  accounting for approximately 60% of the total free fatty acids. The *Bacillus* sp. SG-1 and *C. taiwanensis* strains also produced small amounts of monounsaturated  $C_{16}$  fatty acid (see Table S2 in the supplemental material). Interestingly, whereas all strains displayed similar growth characteristics, free fatty acid levels differed. Expression of *fabG* variants corresponded with increased fatty acid levels relative to the *E. coli fabG* control strain, except for the *A. laidlawii* variant, which produced a concentration similar to that of the control strain. The strains engineered with *P. pacifica, Bacillus* sp. SG-1, and *C. taiwanensis* FabGs produced, respectively, 27, 52, and 59% more free fatty acids than the control strain under anaerobic conditions.

Anaerobic methyl ketone production. After observing that expression of the various FabG variants resulted in an increase in free fatty acid titers under anaerobic conditions, we wanted to examine whether these improvements also translated to fatty acid-derived biofuels, such as methyl ketones. The top-performing FabG (*C. taiwanensis*) was cloned into an *E. coli* host expressing the methyl ketone pathway, resulting in strain EGS1670 (Table 1). Methyl ketone production in this strain was compared with that of the control strain, EGS895 (25). Production was measured for biological triplicates of each strain.

Methyl ketone production was measured after 96 h by removing the decane overlay for GC-MS analysis.  $OD_{600}$  values of each culture were approximately 0.2 after 96 h, and as observed for the free fatty acid strains, there were no significant differences in growth among the methyl ketone-producing strains.

The methyl ketone titer for strain EGS1670 was 75% higher than that of the control strain (EGS895) under anaerobic conditions (Fig. 5), but titers for both strains were several orders of magnitude lower than the 380 mg/liter reported for EGS895 under aerobic conditions (25). Note that  $O_2$ -limited conditions will adversely affect the methyl ketone pathway as it is currently constituted, since the acyl-CoA oxidase used in this pathway requires  $O_2$  to function (25). Regardless, the relative improvements in methyl ketone titers were consistent with those observed for free fatty acids.



**FIG 5** Summary of total methyl ketone titer in strain EGS895 (without *C. taiwanensis* FabG) and strain EGS1670 (with *C. taiwanensis* FabG) (Table 1). Bar heights represent average titers from 3 biological replicates, and error bars represent 1 standard deviation.

## DISCUSSION

The goal of this study was to identify a homolog of E. coli FabG with a much higher preference for NADH than for NADPH, which would presumably give rise to higher fatty acid levels during anaerobic growth. The in vitro assay identified several candidate variants that had higher activity with NADH than with NADPH. Of these, three gave rise to higher free fatty acid titers than the control strain under anaerobic culture conditions. It appears that a key molecular determinant of cofactor specificity in FabG is the presence of a negatively charged residue interacting with the 2'hydroxyl of the NADH adenine ribose, instead of a basic residue that would participate in ionic interactions with the 2'-phosphate moiety of NADPH. A similar phenomenon was reported in investigations of changing the cofactor specificity of E. coli glutathione reductase (39). In that study, a mutant with increased NADH activity was engineered, in part, by substituting residues that interact with the NADPH 2'-phosphate with negatively charged residues (39).

The in vitro activity assay and fatty acid titer data are compared in Fig. 4. These data are normalized to values for the C. taiwanensis FabG, as this FabG homolog displayed the greatest in vitro specific activity, preference for NADH, and fatty acid titer. Although the data do not reflect a linear relationship between fatty acid titer and FabG in vitro specific activity or NADH preference, it appears that a FabG homolog having both higher absolute activity with NADH and preference for NADH facilitates increased fatty acid production under the tested conditions. The second highest fatty acidproducing strain, expressing the Bacillus sp. SG-1 FabG, also displayed high preference and activity with NADH. In contrast, the A. laidlawii FabG led to a fatty acid titer comparable to that of the control strain. Moreover, this variant displayed less than a 2-fold preference for NADH and an in vitro specific activity comparable to that of E. coli FabG (Fig. 2). The C. taiwanensis FabG, which led to a 60% higher fatty acid production, also led to a 75% higher production of fatty acid-derived methyl ketones. In a study of cofactor dependence in the mevalonate pathway, it was similarly observed that strains expressing the NADH-preferring HMG-CoA reductase with the highest forward reaction rate led to increased amorphadiene production (16).

Given the results of this study, a promising future step would

be to substitute the chromosomal *fabG* in *E. coli* with a variant that led to improved free fatty acid titer under anaerobic conditions, namely, the *C. taiwanensis* homolog. This host strain could then be further engineered and evolved for a more robust growth phenotype under anaerobic conditions and serve as a base strain for biofuel pathways that are fatty acid based, such as for production of fatty acid ethyl esters, fatty alcohols, or methyl ketones. Thus, the identification of FabG homologs that contribute to improved fatty acid titers under anaerobic conditions serves as a preliminary step toward engineering a host strain for anaerobic production of advanced biofuels.

## ACKNOWLEDGMENTS

This work conducted by the Joint BioEnergy Institute was supported by the Office of Science, Office of Biological and Environmental Research, of the U.S. Department of Energy under contract DE-AC02-05CH11231. The Berkeley Center for Structural Biology is supported in part by the National Institutes of Health, National Institute of General Medical Sciences. The Advanced Light Source is supported by the Director, Office of Science, Office of Basic Energy Sciences, of the U.S. Department of Energy under contract DE-AC02-05CH11231.

We are grateful to the staff of the Berkeley Center for Structural Biology at the Advanced Light Source of Lawrence Berkeley National Laboratory.

J.D.K. has a financial interest in LS9, Amyris, and Lygos.

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