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### Title

ELECTROCHEMICAL STUDIES OF THE NiO-,CoO-,Fe<sub>0.95</sub>O-Na<sub>2</sub>Si<sub>2</sub>O<sub>5</sub> GLASS SYSTEMS

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### Author

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ELECTROCHEMICAL STUDIES OF THE  
NiO-, CoO-, Fe<sub>0.95</sub>O-Na<sub>2</sub>Si<sub>2</sub>O<sub>5</sub> GLASS SYSTEMS

Alton Monroe Lacy  
(Ph. D. Thesis)

September 1969

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ELECTROCHEMICAL STUDIES OF THE  
NiO-, CoO-, Fe<sub>0.95</sub>O-Na<sub>2</sub>Si<sub>2</sub>O<sub>5</sub> GLASS SYSTEMS

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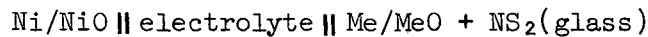
ELECTROCHEMICAL STUDIES OF THE  
NiO-, CoO-, Fe<sub>0.95</sub>O-Na<sub>2</sub>Si<sub>2</sub>O<sub>5</sub> GLASS SYSTEMS

Alton Monroe Lacy

Inorganic Materials Research Division, Lawrence Radiation Laboratory,  
and Department of Materials Science and Engineering,  
College of Engineering, University of California  
Berkeley, California

ABSTRACT

A high temperature galvanic cell of the type



(in which the electrolyte was calcia stabilized zirconia and where Me = Fe, Co, or Ni) has been developed for the measurement of activities and other thermodynamic properties of Fe<sub>0.95</sub>O, CoO and NiO in sodium disilicate glass over the temperature range 700° to 1100°C. The results indicate that these three oxides show increasing negative deviations from Raoult's Law in the order NiO, CoO, Fe<sub>0.95</sub>O. The solubility limits of each oxide in sodium disilicate glass have been measured by this technique and presented as liquidus lines on proposed phase diagrams for the binary systems Fe<sub>0.95</sub>O-, CoO-, NiO-Na<sub>2</sub>Si<sub>2</sub>O<sub>5</sub>. Activities of sodium disilicate have been calculated as a function of composition and temperature by integration of the Gibbs-Duhem equation; and sodium disilicate liquidus lines have been determined by equating the calculated activities with the activity of the pure solid sodium disilicate relative to the super-cooled liquid. The calculated freezing point depression of sodium disilicate by Fe<sub>0.95</sub>O was not coincident with phase diagram data published in the literature, but agreement could be achieved by proposing the existence of at least one previously unreported compound in the ternary

system  $\text{FeO-Na}_2\text{O-SiO}_2$ . Partial molar free energies, entropies and enthalpies, as well as free energies, entropies and enthalpies of mixing for the metal oxides and sodium disilicate glass have also been determined.

## I. INTRODUCTION

An understanding of the thermodynamics of oxide-silicate systems is necessary for any fundamental interpretation of the physical chemistry of these systems. Some areas of investigation where this need has been clearly demonstrated are:

Bonding. In the development of a glass-metal bond, Pask, Fulrath, Borom, et al.<sup>1-4</sup> have demonstrated that two types of bonds may be formed as the product of chemical reaction--a mechanical bond established by corrosion of the metal substrate with subsequent formation of dendritic precipitates on or near the interface; and a chemical bond formed by the establishment of a thermodynamically continuous structure across the glass-metal interface. They have shown that the condition for formation of the latter is the saturation of the glass (at the interface) with the lowest oxide of substrate metal. When this occurs, an oxygen activity balance exists and strongest bonding of the chemical type occurs. This is, however, a limiting condition, since the theory does not account in a quantitative way for any variation in the bond strength with varying degrees of saturation.

If the degree of chemical bonding is to be related to the imbalance in activity between the oxide of the interfacial metal and that dissolved in the glass, then the need for a thorough knowledge of the activity variation of the oxide in the glass solution as functions of composition, temperature and pressure is obvious.

Similarly, if one is concerned with the redox reactions between glass and metal, predictions of their free energies can only be made if one knows the activities of the components involved. To date, little



effort toward this end has been made in complex silicate systems.

Wetting. Aksay<sup>5</sup> has related the degree of wetting in high temperature MgO-silicate liquid reactions to the activities of components of phases in physical contact. He states, "If the liquid and the solid are not at a thermodynamic equilibrium, a redistribution of the components between the liquid and the solid will take place. An equilibrium contact angle will form only after this thermodynamic equilibrium is achieved..." Humenik and Kingery,<sup>6</sup> as well as Gaidos and Pask,<sup>2</sup> have similarly related changes in interfacial energy to interfacial reactions.

Stability. The stability of glasses with respect to their environment is also greatly affected by the activities of the component oxides. Glasses containing oxides with small free energies of formation become very susceptible to decomposition at low oxygen pressure, high temperatures, or when exposed to reducing atmospheres of other gases. Since many of these glasses have properties of special interest (e.g., coatings, composites, electronics), it is particularly important to define carefully and accurately the limits of chemical stability as functions of composition and environment.

Solid-Liquid Phase Equilibria. Many phase relations within glass-forming systems can also be inferred from thermodynamic activity measurements of the components. Such data can be used to calculate or predict liquidus lines, as well as thermodynamic properties of pure components.

Structure. Structure and bonding are also related to thermodynamic properties of solutions. For example, strong positive deviations from Raoult's Law are associated with a tendency for like atomic or molecular species to associate, tending toward immiscibility; whereas

negative deviations often represent formation of complex molecular or ionic species and tendencies toward compound formation. Knowledge of activities in glass may assist one in inferring possible structural models for these systems, which can be valuable in supporting other theories of structure based upon different type of experimental observations.

Kinetics. The kinetics of reactions in glasses may also be controlled by the activities of the components. For example, the rates of those processes that are diffusion-controlled, such as dissolution of many pure oxides by glass,<sup>7,8</sup> will be dictated not by composition gradients per se, but rather by activity gradients, which, in the case of non-ideal solutions, may be quite different from the former.

It is therefore apparent that a lack of specific knowledge of the thermodynamics of glass systems seriously limits one's ability to predict reactions, confirm theories related to chemical equilibrium, or control rate processes. Every study toward overcoming this void in our knowledge will be small relative to the total need, but valuable toward solving some of the present problems and in building the foundation for further work. It is to this end that the present study has been directed.

This work is specifically motivated by the need to obtain the necessary thermodynamic data to define the activity-composition-temperature relations in the systems NiO-, CoO-, and FeO-Na<sub>2</sub>Si<sub>2</sub>O<sub>5</sub>.\* Sodium disilicate

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\* FeO will be used throughout the text to represent that iron oxide composition in thermodynamic equilibrium with Fe metal at the temperature of consideration. That is, over the temperature range 700°-1100°C, "FeO"  $\cong$  Fe.<sub>950</sub>.

was initially chosen because it is a glass composed of one glass-forming and one glass-modifying ion, thus facilitating structural interpretations based on O/Si ratios.

These systems have been used in this laboratory for the past decade in studies of bonding, wetting, and diffusion. Therefore, clarification of questions raised in those investigations would require the same systems for this work.

In addition, the heat capacities, entropies and enthalpies of  $\text{Na}_2\text{Si}_2\text{O}_5$  (solid and liquid) have been measured by Kelley and King<sup>9,10</sup> and a phase diagram for the binary system  $\text{FeO-NS}_2^*$  is published in the literature.<sup>11</sup>

Those activity measurements on molten silicates reported in the literature have been made principally on binary metal oxide-silica systems and on multicomponent slags. Most of these have been carried out by gas equilibration techniques. The electrochemical method is, however, often preferable to the gas equilibration method because of the wider range of oxygen potentials capable of being measured accurately. (Oxygen pressures in the range of  $10^{-20}$  atm require CO/CO<sub>2</sub> ratios of  $\sim 1000/1$  at 1000C. This ratio is near the limit of detection for general experimental measurement but the same O<sub>2</sub> pressure is readily and accurately detected with solid oxygen conducting electrolytic cells.) In spite of these advantages, the number of electrochemical studies reported on liquid silicate systems is relatively small.

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\* The following abbreviations will be used throughout this text:  
N=Na<sub>2</sub>O, F=FeO, S=SiO<sub>2</sub>, and C=CoO. (That is, NS<sub>2</sub>=Na<sub>2</sub>Si<sub>2</sub>O<sub>5</sub>.)

Herring<sup>12</sup> and Didtshenko and Rochow<sup>13</sup> have used concentration cells of the type  $O_2(Pt)/\text{liquid I} :: \text{liquid II}/O_2(Pt)$  in order to determine the activities of  $Na_2O$  in soda-silica glasses and  $Na_2O$ ,  $K_2O$  and  $Li_2O$  in  $PbO-SiO_2$  glasses respectively. In both cases, the cells appeared to function properly (i.e., they were reversible and stable), but there has been no independent verification of the data. This type of cell is generally not suitable for such measurements because of the possibility of errors in emf measurements arising from unknown thermoelectric emfs, liquid junction potentials, poorly defined cell reactions, and indeterminate transference numbers of the conducting species.

Simple formation cells of the type  $M/MO(\text{in solution})/O_2$  are theoretically possible for activity determination in liquid silicates, but practically infeasible because of the unknown magnitude of electronic conductance in most silicate systems at high temperatures. (If not quantitatively accounted for, any electronic transference will short the cell internally, reducing the external emf, and result in erroneous output for activity determination.) This may be particularly true for glasses containing multivalent ions that impart a tendency for semi-conduction. Esin<sup>14</sup> has constructed such a cell to measure the activities of  $FeO$  in complex silicate melts. The procedure he used was technically difficult and the reversibility of the cells is not known.

Solid electrolytes in which the transference number,  $(t)$ , of an ion which can take part in the cell reaction is known (preferably 1.0) appear the most feasible for high temperature thermodynamic studies in glasses. Stabilized  $ZrO_2$  and  $ThO_2$  are oxygen ion conductors ( $t_{O_2} = 1.0$ ),

they are inert to corrosion by many liquid silicates, and have been successfully used since 1957<sup>15</sup> for a variety of high temperature thermodynamic investigations on metals and oxides. The reader is referred to Steele<sup>16\*</sup> for further reference to these works. A search of the literature has indicated that Matsushita and Goto,<sup>17</sup> H. S. Ray,<sup>18</sup> and Charette and Flengas<sup>19</sup> have carried out the only previous studies of glasses with solid electrolyte cells. Matsushita and Goto, and Charette and Flengas have both investigated the activity of PbO and SiO<sub>2</sub> in binary PbO-SiO<sub>2</sub> glasses at 900-1100°C using a cell of the type Ni/NiO || CSZ<sup>\*\*</sup> || Pb/PbO-SiO<sub>2</sub>. Their data corresponds well with that of Richardson and Webb,<sup>20</sup> obtained by other methods. Ray has studied (concurrently with this investigation) activities of Cu<sub>2</sub>O, NiO, CoO and Fe<sub>x</sub>O in ternary Na<sub>2</sub>O-K<sub>2</sub>O-SiO<sub>2</sub> solvents; his study apparently has not been published, and only an abstracted summary was available to the writer.

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\* Steel has presented a very concise survey of the development and application of solid electrolytes and high temperature galvanic cells, together with a complete bibliography referring to their uses. Even though such solid electrolyte cells have not been previously used to study complex glass systems, Steele's article is still relevant to this work. Inclusion of any of his material here, however, would simply be repetitious.

\*\* CSZ will be used throughout this thesis to designate "calcia-stabilized zirconia."

## II. THEORETICAL

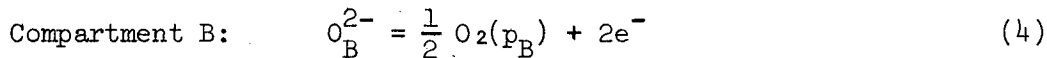
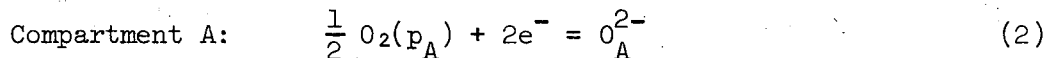
### A. General Cell Theory

The method developed for activity determinations utilized a variation of the oxygen concentration cell containing a CSZ electrolyte, similar in principle to those developed first by Kiukolla and Wagner.<sup>15</sup>



where  $p_A$  and  $p_B$  represent the oxygen pressures in compartments A and B respectively, and  $p_A > p_B$ .

Since CSZ is a pure oxygen conductor from  $p = 1 \text{ atm}$  to  $p = 10^{-20} \text{ atm}$ , we may represent the process of electrochemical oxygen transfer as follows:



The overall cell reaction thus becomes:  $\frac{1}{2} \text{O}_2(p_A) = \frac{1}{2} \text{O}_2(p_B)$ .

The free energy for transfer of one mole of oxygen from  $p_A$  to  $p_B$  may be expressed as

$$\Delta F = RT \ln \frac{p_B^{1/2}}{p_A^{1/2}} \quad (5)$$

From the relation

$$\Delta F = nF\varepsilon \quad (6)$$

where  $n$  = the number of electrons transferred

$F$  = Faraday's Constant - 23011 cal/volt

$\varepsilon$  = measured cell output voltage,

we may relate the cell voltage to the oxygen pressures by:

$$\varepsilon_{\text{measured}} = \frac{-RT}{2nF} \ln \frac{p_B}{p_A} \quad (7)$$

If in either compartment we fix the oxygen pressure either directly or by equilibration of a metal and its oxide, the unknown pressure may be determined by Eq. (7).

When a mixture of solid metal A and its oxide AO are placed in compartment A, an equilibrium oxygen pressure is established, which is related to the standard free energy of formation of AO, according to reaction (8).



The free energy for this reaction may be written

$$\Delta F_{AO} = \Delta F_{AO}^{\circ} + RT (\ln a_{AO} - \ln p_A^{1/2}(O_2)); \quad (9)$$

at equilibrium  $\Delta F_{AO} = 0$ , and

$$-\Delta F_{AO} + RT \ln p_A^{1/2}(O_2) = RT \ln a_{AO}. \quad (10)$$

In compartment B, we place a mixture of metal B and its oxide BO.

The half cell reaction for this compartment may be expressed as



and

$$\Delta F_{BO} = \Delta F_{BO}^{\circ} + RT (\ln p_B^{1/2}(O_2) - \ln a_{BO}). \quad (12)$$

At equilibrium  $\Delta F_{BO} = 0$ , and

$$-\Delta F_{BO}^{\circ} - RT \ln p_B^{1/2}(O_2) = -RT \ln a_{BO}. \quad (13)$$

The overall cell reaction may be expressed as



summing (10) and (13)

$$-(\Delta F_{AO}^{\circ} + F_{BO}^{\circ}) + RT \ln \frac{p_A^{1/2}(O_2)}{p_B^{1/2}(O_2)} = RT \ln \frac{a_{AO}}{a_{BO}} \quad (15)$$

If  $a_{BO} = 1$ , we find from (5), (6) and (7),

$$-nF (\epsilon^{\circ} - \epsilon_{cell}) = RT \ln a_{AO}. \quad (16)$$



In the event that A and B are the same metal, Eq. (16) reduces to

$$-nF\epsilon_{\text{cell}} = RT \ln a_{\text{AO}} . \quad (16b)$$

The emf output of the cell will give directly the activity of the AO in solution, relative to the solid standard state, by the application of Eq. (16b).

$$a_{\text{AO}} = \exp\left(\frac{-nF}{RT} \epsilon_{\text{cell}}\right) . \quad (17)$$

B. Calculation of the Activity of a Second Binary Component When the Activity of One is Known

In a two-component system, the activity of the second component (BO) can now be determined by calculating the activity coefficient,  $\gamma_{\text{BO}}$  (where  $\gamma_{\text{BO}} \equiv a_{\text{BO}}/N_{\text{BO}}$ ), from integration of the Gibbs-Duhem equation

$$N_{\text{AO}} d \ln \gamma_{\text{AO}} + N_{\text{BO}} d \ln \gamma_{\text{BO}} = 0 . \quad (18)$$

The  $\ln \gamma_{\text{BO}}$  can be directly determined from the integration

$$\ln \gamma_{\text{BO}} = - \int_{N_{\text{BO}}=1}^{N_{\text{BO}}=N_{\text{BO}}} \frac{N_{\text{AO}}}{N_{\text{BO}}} d \ln \gamma_{\text{AO}} \quad (19)$$

Darken and Gurry have provided an alternate integration by defining a function,

$$\alpha_{AO} = \frac{\ln \gamma_{AO}}{N_{BO}^2} \quad (20)$$

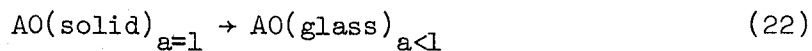
Differentiation of  $\ln \gamma_{AO} = \alpha_{AO} N_{BO}^2$  and substitution into (18) results in the expression

$$\ln \gamma_{BO} = -\alpha_{AO} N_{AO} N_{BO} - \int_{N_{BO}=1}^{N_{BO}=N_{BO}} dN_{BO} \quad (21)$$

This may be evaluated graphically.

### C. Partial Molar and Integral Thermodynamic Functions

If the cell reaction is written



the free energy of this reaction ( $\Delta F_{\text{rxn}}$ ) may be expressed

$$\Delta F_{\text{rxn}} = RT \ln a_{AO(\text{glass})} \quad (16c)$$

The free energy expressed in Eq. (16c) is recognized as the partial molar free energy ( $\overline{\Delta F}_{AO}$ ) of the oxide in solution. Similarly, having obtained  $a_{BO}$  from either Eqs. (19) or (21), the partial molar free energy for the second component may be found from

$$\overline{\Delta F}_{BO} = RT \ln a_{BO} \quad (16d)$$

The integral free energy of mixing (or formation) of the solution from its components according to the reaction



may be obtained from

$$\Delta F_{\text{mix}} = N_{AO} \overline{\Delta F}_{AO} + N_{BO} \overline{\Delta F}_{BO} \quad (24)$$

The partial molar entropies may be calculated from the relation

$$dF = - SdT + VdP \quad (25)$$

where, at constant pressure

$$\left( \frac{\partial \overline{\Delta F}}{\partial T} \right)_P = - \overline{\Delta S} \quad (26)$$

The partial molar entropies for component AO (Eq. (22)) may then be obtained from the slope of the cell voltage vs. temperature according to Eqs. (16b), (16d), and (26).

$$-nF \left( \frac{\partial \mathcal{E}}{\partial T} \right)_P = - \overline{\Delta S}_{AO} \equiv - \Delta S_{\text{cell reaction}} \quad (27)$$

The partial molar enthalpy of component AO is simply the heat of the cell reaction (22), and may be found by either of the following relations:

$$\overline{\Delta H}_{AO} = \overline{\Delta F}_{AO} + T\overline{\Delta S}_{AO} = -nF \left[ \epsilon - T \left( \frac{\partial \epsilon}{\partial T} \right)_p \right] \quad (28a)$$

or

$$\partial \left( \frac{\overline{\Delta F}_{AO}}{T} \right)_p = \overline{\Delta H}_{AO}, \text{ assuming } \overline{\Delta S}_{AO} \text{ constant} \quad (29a)$$

$$\partial \left( \frac{1}{T} \right)$$

with temperature. The integral entropy of mixing may be found by applying the equation

$$\Delta S_{mix} = N_{AO} \overline{\Delta S}_{AO} + N_{BO} \overline{\Delta S}_{BO}, \quad (30)$$

where  $\overline{\Delta S}_{BO}$  has been calculated from (16d) and (26).

The integral enthalpy is readily determined from

$$\Delta H_{mix} = \Delta F_{mix} + T\Delta S_{mix}, \quad (31)$$

$$\partial \left( \frac{\Delta F_{mix}}{T} \right)_p = \Delta H_{mix} \quad (29b)$$

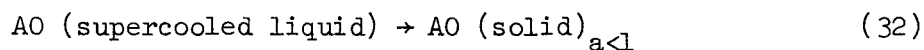
$$\partial \left( \frac{1}{T} \right)$$

or

$$\Delta H_{mix} = N_{AO} \overline{\Delta H}_{AO} + N_{BO} \overline{\Delta H}_{BO}. \quad (28b)$$

D. Activities Referred to Pure Supercooled  
Liquid Standard State

If one wishes to compare calculated partial and integral molar functions with these same quantities for ideal molecular solutions, the activities of AO in solution must be referred to the pure supercooled liquid AO, by adding the appropriate thermodynamic quantities for Eq. (32).



to those same quantities for Eq. (22). By comparison of the resulting sum with the same functions for ideal solutions, excess quantities may be readily determined.

If the heat capacities of both the pure solid and the supercooled liquid are known, as well as the heat of fusion, the free energy for reaction (32) at any temperature may be found by integration of

$$\frac{\Delta F}{T} = - \int_{T_1}^{T_2} \frac{\int_{T_1}^{T_2} \Delta C_p dT}{T} dT = -R \ln \frac{a_{\text{solid}}}{a_{\text{liquid}} \equiv 1} = -R \ln K \quad (33)$$

from which the activity of the pure solid relative to the pure supercooled liquid, (K), may be found.

If heat capacity data are not available,  $K_{\text{AO}}$  may be related to the heat of fusion ( $\Delta H_F$ ) of AO by the relation

$$-\ln K_{AO} = \frac{\Delta H_F}{RT} \left( 1 - \frac{T}{T_F} \right) \quad (34)$$

where  $T_F$  = the melting temperature ( $^{\circ}\text{K}$ ) of pure AO. This assumes that the heat capacities of the pure solid and supercooled liquid are equal below  $T_F$ . This is generally a good first approximation. (See appendix D).

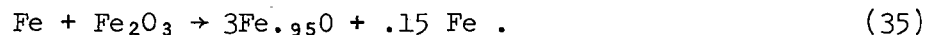
The solubility limits of both components AO and BO may be found by the points of intersection of plots of the measured activities and the activities of the pure solid (when both are referred to the same standard state) vs. temperature.

### III. EXPERIMENTAL PROCEDURE

#### A. Glass Production

The NiO glass was prepared by mechanically mixing weighed quantities of Baker's analyzed NiO with sodium disilicate glass\* obtained from the Philadelphia Quartz Company. Each mixture was then heated in a Pt crucible at 1200°C for 12 hours in air to insure homogeneity. The CoO-NS<sub>2</sub> glass was prepared in a similar fashion, the CoO being prepared before mixing from vacuum decomposition of chemically pure Co<sub>3</sub>O<sub>4</sub> powder at 1000°C.

The Fe<sub>0.95</sub>O-NS<sub>2</sub> glasses were prepared by adding Fe<sub>2</sub>O<sub>3</sub> + Fe in the proper ratio to give hypothetically stoichiometric FeO. This three-component mixture (Fe + Fe<sub>2</sub>O<sub>3</sub> + NS<sub>2</sub>) was packed in Fe crucibles and placed in a vacuum quench furnace. After evacuation to  $\sim 10^{-4}$  torr, the furnace was back filled with purified argon, the glass batch lowered into the hot zone and held in static argon for 12 hours at 1000°C. Upon quenching, the resulting glass was characteristically blue at low total FeO concentrations and greenish-grey with higher ( $\sim 30$  weight %) amounts. There was also a trace of residual Fe metal on the surface, as would be expected from the reaction



All glasses were ground to powder in an Al<sub>2</sub>O<sub>3</sub> mortar just prior to use in the individual cell experiments.

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\* Trade designation: SS-C (powder).

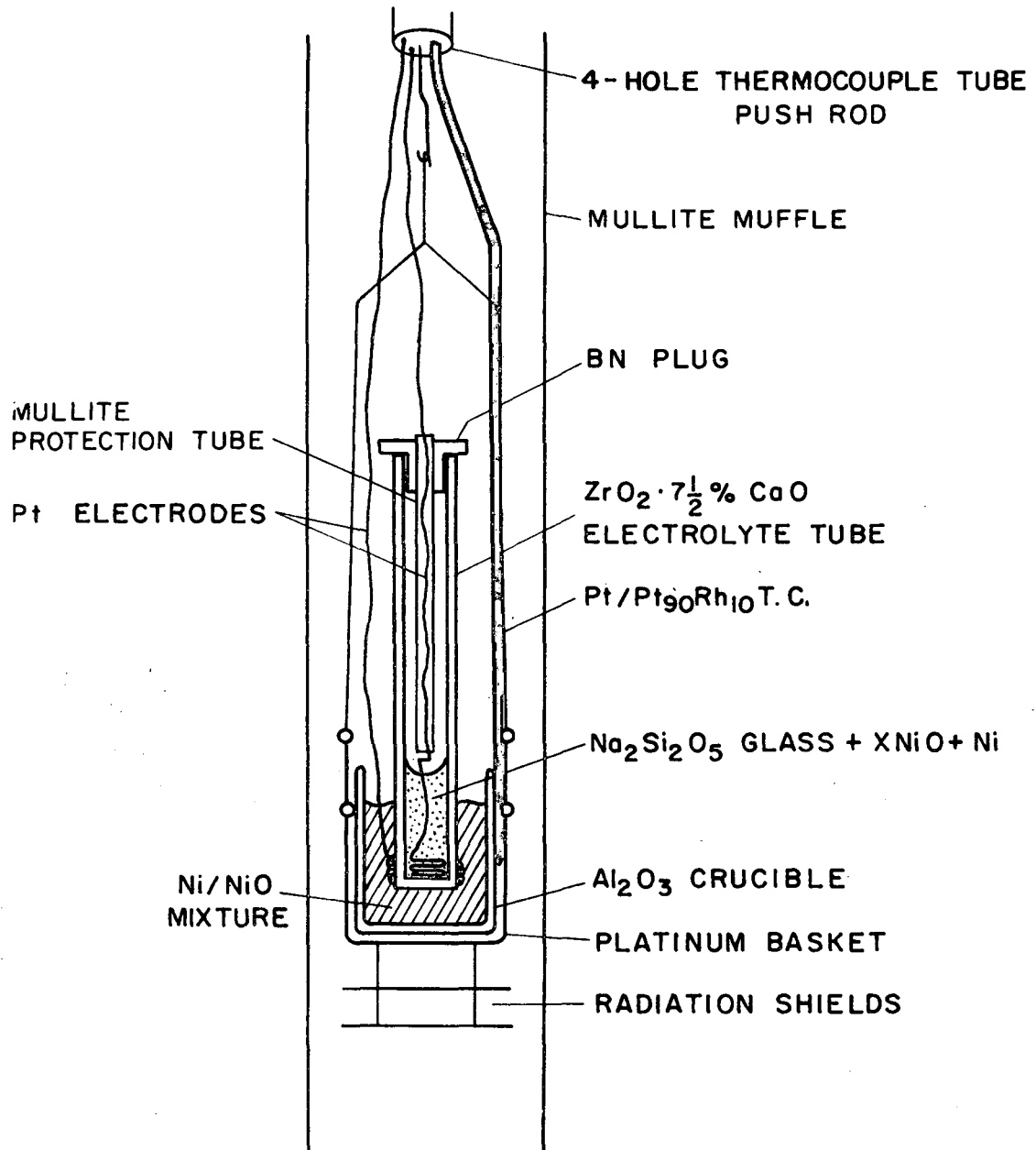
### B. Cell Construction

A schematic diagram of the experimental set-up is illustrated in Fig. 1. The outer electrode was formed by a twisted single wrap of 20 mil Pt wire around the outside of the calcia stabilized zirconia tube; \* the inner electrode was formed by wrapping 20 mil wire in helical fashion (2 times) around a glass rod to form a coil slightly larger than the inside diameter of the CSZ tube. This was then bent so that the free end extended out along the center line of the tube. The coil was then "spring-fitted" on the inside and forced to the bottom with a piece of glass tubing, making a tight fit to the inside. (This snug fit was necessary for successful operation of the cell.) Approximately 1-1/2 grams of glass powder was mixed with about 1/3 gram of the appropriate pure metal powder and put into the tube to a level just above the upper coils. A short piece of mullite thermocouple protection tubing was placed over the exposed electrode inside the tube, resting on a bend in the wire just above the glass level, so as to avoid contact of the CSZ with the wire. A boron nitride plug with a hole just large enough to accommodate the protruding mullite tube was placed over the upper end of the CSZ tube to secure the electrode position and to prevent external material from falling into the glass at any time. The assembly was then seated in a Pt support basket containing a Coors CN-10 cylindrical  $\text{Al}_2\text{O}_3$  (AD998) crucible containing a mixture of powdered Ni metal (certified chemically pure by the A. J. Mackay Co., Inc.) and NiO powder (Bakers' analyzed reagent). Connection from the 20 mil Pt electrodes to the 20

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\* Obtained from Zircoa, Solon, Ohio.





XBL 692-225

Figure 1. Schematic diagram of the experimental cell assembly.

mil Pt extension leads were made with 8 mil Pt wire. This procedure allowed for easy connection and disconnection without physically upsetting the packed powder. Additional powder was then added and tightly packed around the tube.

After sealing in a resistance wound furnace, the system was evacuated to approximately  $10^{-5}$  torr ( $2 \times 10^{-8}$  atm  $O_2$ ) and filled with argon just before lowering the cell from the cool quench zone into the hot zone. It was found that the duration of evacuation (which varied from 1 hr to 2 days) had no effect on the cell performance. Measurements of cell output were begun about one hour after lowering. This seemed to be sufficient time for thermal equilibration and stabilization of the emf. The cell and thermocouple outputs were recorded on a high impedance Honeywell Electronik 19 potentiometric recorder. The thermocouples were Pt-Pt<sub>90</sub>Rh<sub>10</sub>. Chromel-alumel couples were tried, but found unsatisfactory in the reducing atmosphere of the cell environment.

The residual oxygen remaining in the furnace after filling with argon almost certainly reacted with the exposed Ni metal of the outer electrode compartment, reducing the  $O_2$  pressure in the system to the equilibrium pressure of an Ni/NiO mixture. Any possible pickup of residual oxygen by the glass in this static environment would result in inconsequential alterations of the metal oxide content of the glass.

Polarization and reversibility of the cell were checked for either by short circuiting the cell for a few seconds with constant emf monitoring or by imposing briefly an emf (with a potentiometer) across the cell. All cells returned promptly to their original emf when the disturbance was eliminated.

Equilibrium was verified both by holding the cells isothermally for long periods of time (2-3 days) without evidence of drift of the emf output and by continuously monitoring the cell voltage as the temperature was raised and lowered. If in a cooling-heating cycle, the electrochemical equilibrium is not achieved as fast as the temperature changes, at any selected temperature one would expect to see higher emf values upon cooling than upon subsequent heating (i.e., a hysteresis effect of emf vs. temperature). Such was not the case with these cells. It was found that continuous cycling gave a reproducibility for any cell to  $\pm 1$  mv irrespective of the rate of cycling. The fastest rate of furnace cooling or heating was approximately  $1^{\circ}\text{C}/\text{min}$ . At faster rates, it was found that the temperature differences between the cell and furnace wall exceeded  $\pm 1^{\circ}\text{C}$ . Generally, the cooling rates were of the order of to  $5^{\circ}\text{C}/\text{min}$ . All cells were monitored over at least one full cycle of .2 cooling and heating.

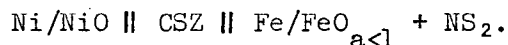
At temperatures above  $1000^{\circ}\text{C}$ , stability and reproducibility became difficult to obtain, due to a tendency for downward drift of the emf of all cells. This behavior is characteristic of some side reaction within the cell not associated with the cell reaction. It was not possible to define the specific nature of the drift, but it may be due to attack of the CSZ electrolyte by the glass, thus altering the metal oxide activity in solution. Such a downward drift would be characteristic of the introduction of oxygen into the glass. Since this drift was similarly noticed in a special cell designed to separate completely the electrode compartments from each other, it is felt not to be the result of  $\text{O}_2$

transfer from the Ni/NiO reference electrode to the glass through the surrounding atmosphere, but rather to some other undefined reaction. This reaction could be dependent on increased oxygen diffusion through the electrolyte at high temperatures since microscopic examination of a sectioned cell showed no evidence of chemical reactions. Consequently, data reported for 1100°C are taken from extrapolations of  $\epsilon$  vs. T curves on the assumption that the partial molar entropy of the dissolved oxide does not change with temperature.

#### IV. RESULTS

##### A. The System FeO-NS<sub>2</sub>

Experimental studies of the activity of FeO in sodium disilicate glass were made in a cell of the type

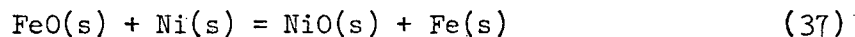


Ni/NiO was used as the reference electrode because its standard free energy of formation, hence its equilibrium oxygen pressure, has been established very accurately. It is perhaps the most common reference electrode used in solid electrolyte galvanic oxygen cells. The standard free energies of formation of both NiO and FeO were taken from the compiled data of Elliot and Gleiser.<sup>21</sup> Ray<sup>22</sup> has reviewed the work of a large number of investigators and concluded that Elliot and Gleiser's tables are more consistent with the accumulated data than values from any one other source and, therefore, should be preferred over others.\*

The overall cell reaction may be written



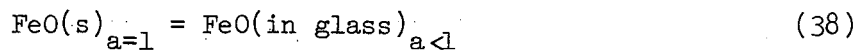
By adding the free energy of the reaction



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\* A cell of the type Ni/NiO || CSZ || Fe/FeO was also set up, and the output found to agree to ± 1 mv with the theoretical output calculated from the tabulated data of Elliot and Gleiser.

to the measured free energy ( $-nF\epsilon$ ) of the cell reaction, one obtains the free energy of reaction



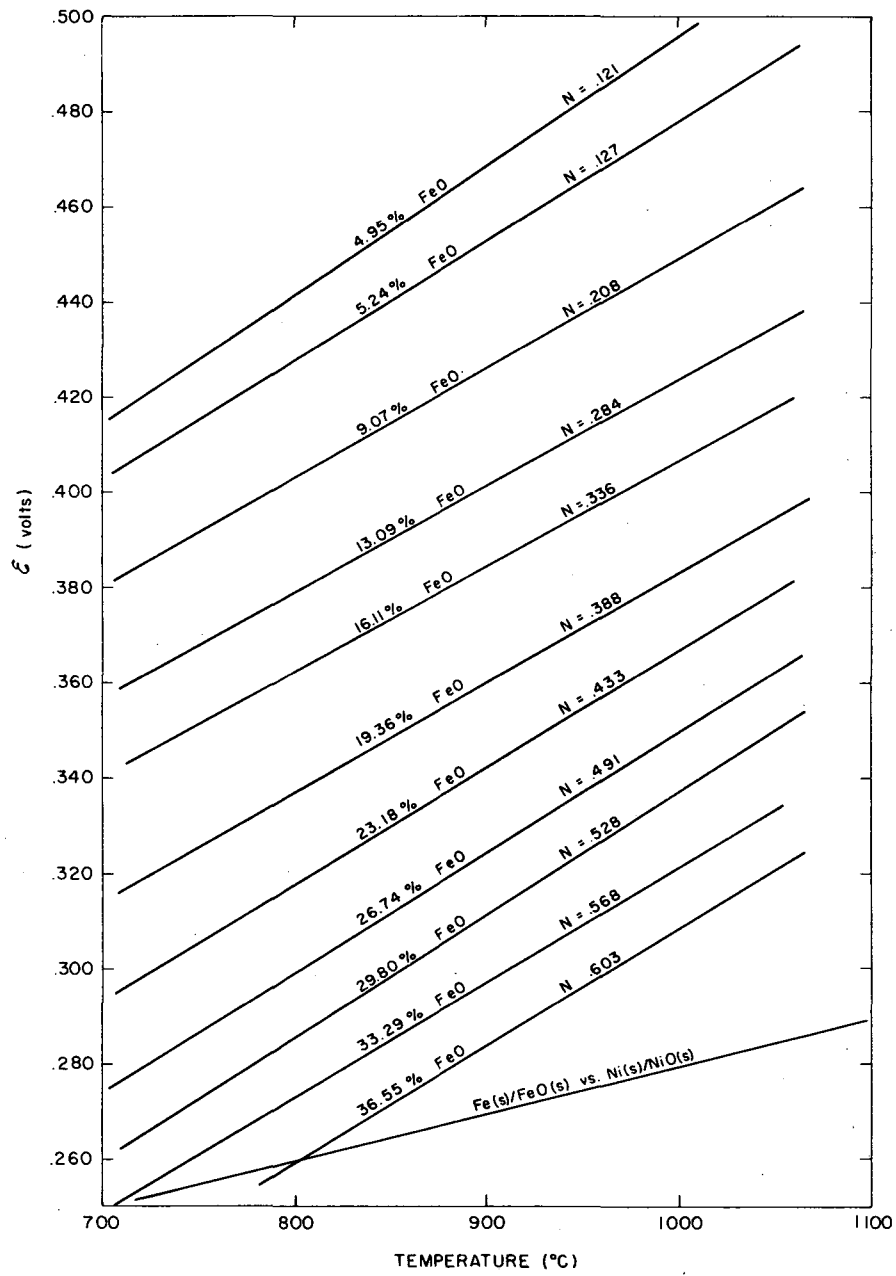
The activity of the dissolved  $\text{FeO}(a_{\text{FeO}}^*)^\dagger$  relative to the solid standard state may be calculated from Eq. (17).

The isocompositional cell output (in volts) vs. temperature is presented in Fig. 2. Each line represents an average of at least two trials for the particular glass under investigation. The variation of calculated activity with temperature for each composition is given in Fig. 3. The isothermal dependence of activity ( $a_{\text{FeO}}^*$ ) on composition may be seen in Fig. 4. For the sake of clarity, error limits are not shown in Figures 3 and 4, but they may be readily calculated from Eq. (17), assuming an average uncertainty in cell output of  $\pm 2$  mv.

The activity of the oxide relative to the pure liquid standard state may be obtained by multiplying the measured activity by the activity of the pure solid referred to the pure liquid standard state-- see Eqs. (33) and (34), and Appendix F. Activities referred to both standard states are listed in Appendix A, and a plot of activity (referred to pure liquid) vs. composition is given in Fig. 5.

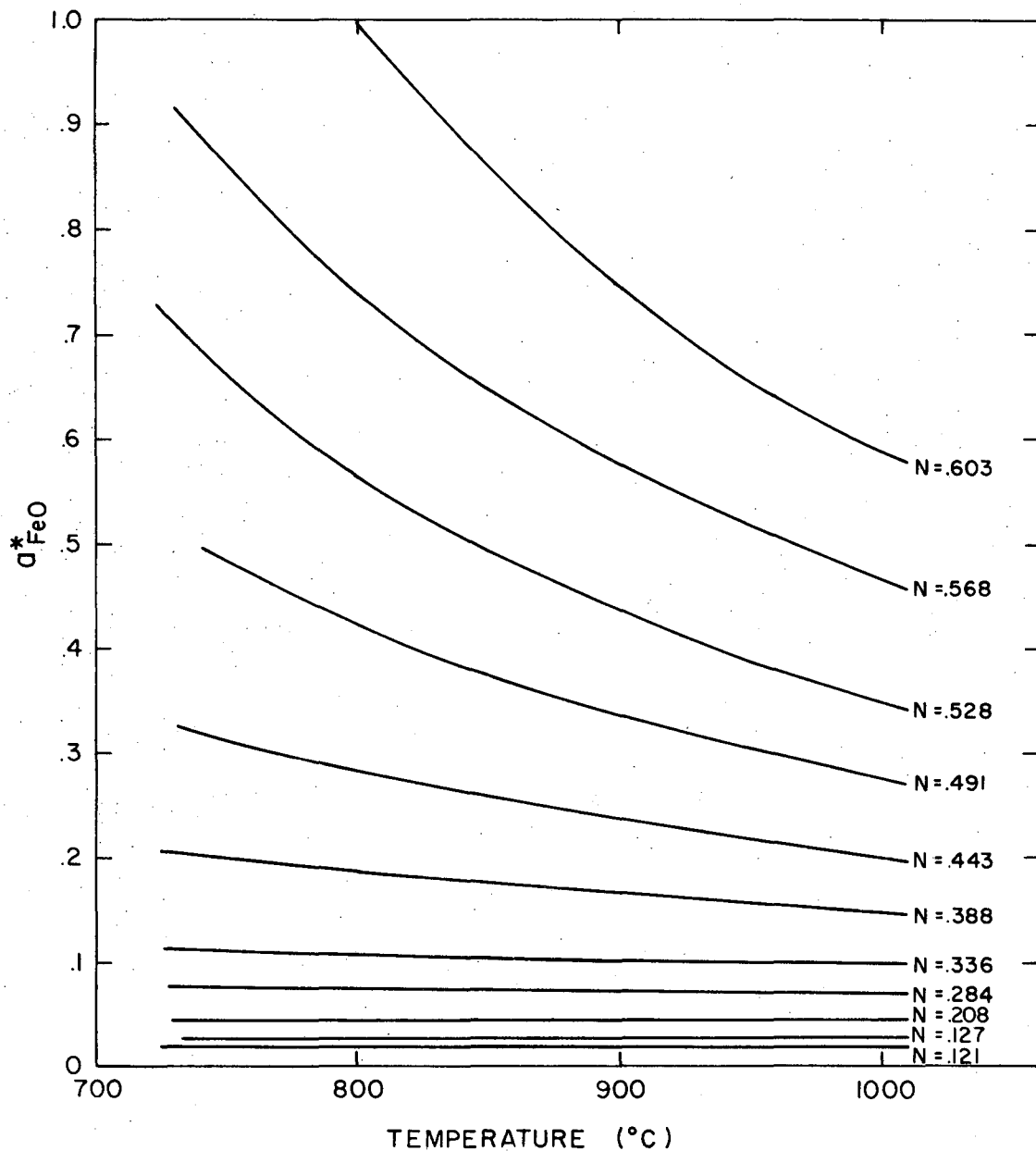
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†  $a^*$  will be used in the remainder of the text to designate activities of oxides relative to the pure solid standard state;  $a^{**}$  will designate activities referred to the pure supercooled liquid standard state.



XBL 699-1434

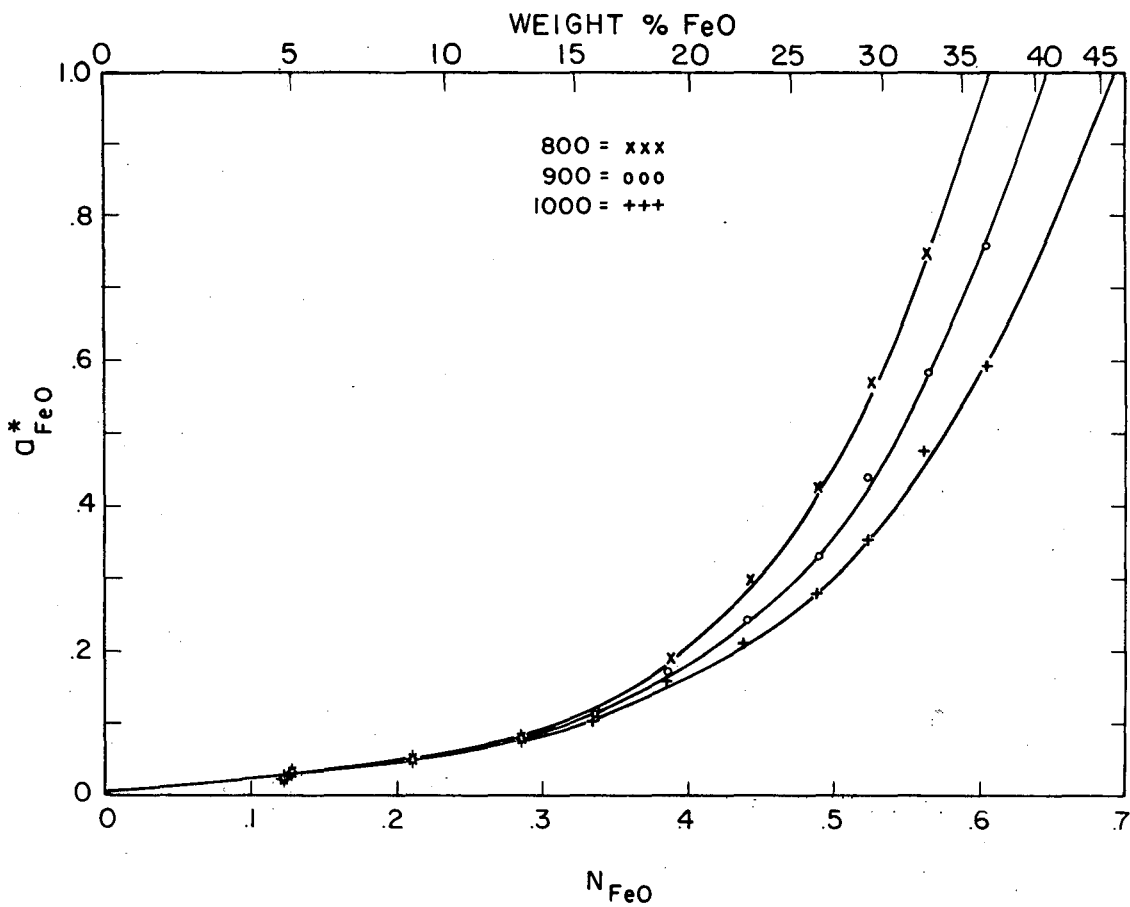
Figure 2. Isocompositional cell output for FeO-NS<sub>2</sub> glasses as a function of temperature.



XBL 699-1398

Figure 3. Variation in the activity of FeO (referred to the pure solid standard state) with temperature for each composition studied.





XBL 699-1399

Figure 4. Isothermal dependence of FeO activity (referred to the pure solid standard state) on composition.

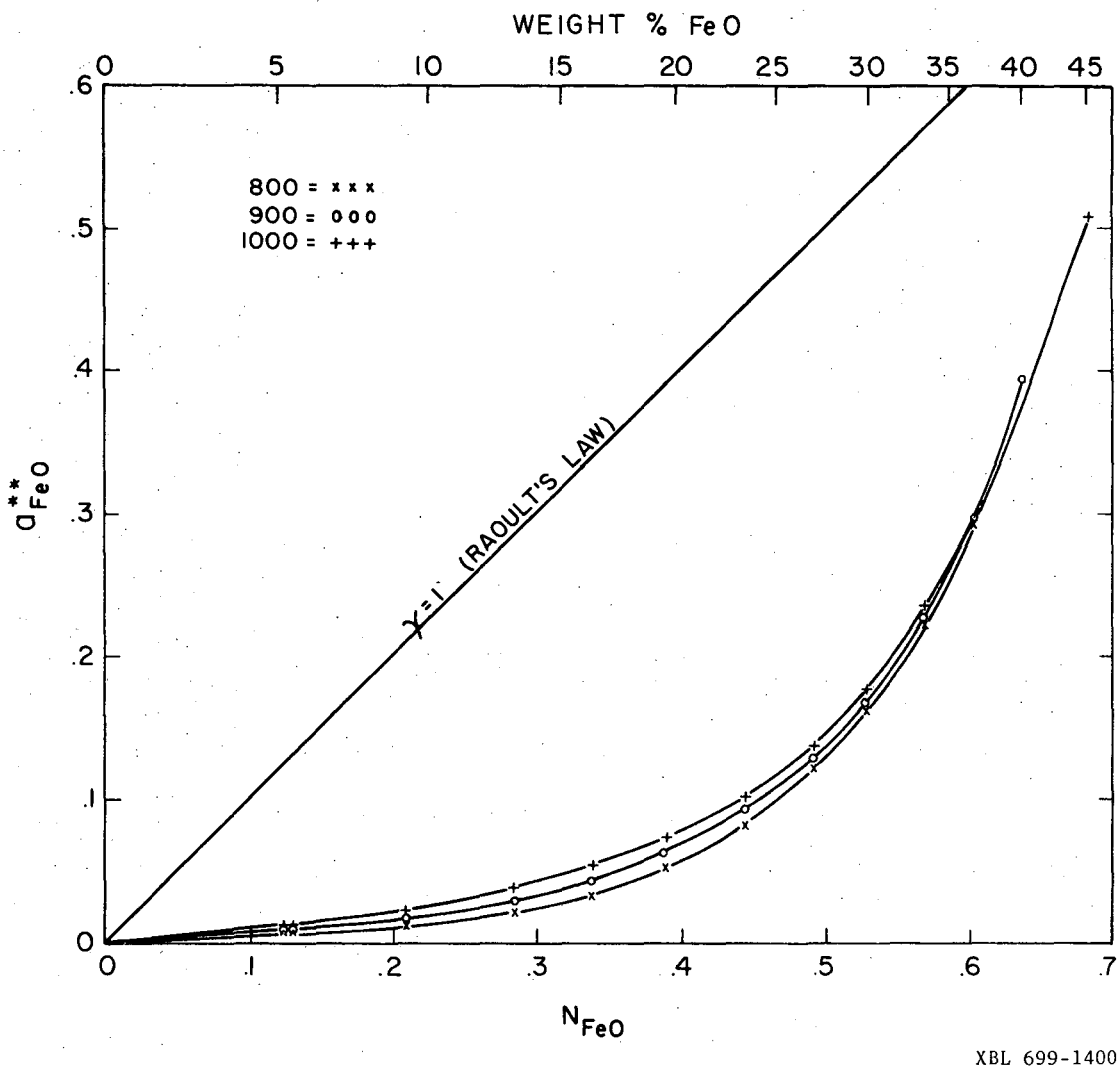


Figure 5. Estimated isothermal dependence of the FeO activity (referred to pure supercooled liquid FeO) on composition.

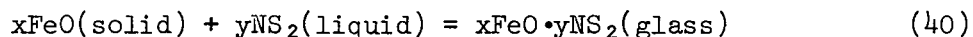
XBL 699-1400

The activity of  $\text{NS}_2$  relative to liquid  $\text{NS}_2$  was found by graphical integration of the Gibbs-Duhem equation. A plot of  $N_{\text{FeO}}/N_{\text{NS}_2}$  vs  $\ln \gamma^*_{\text{FeO}}$  is given in Fig. 6, and the activities of  $\text{NS}_2$  calculated from this method using Eq. (19) are shown in Fig. 7 and tabulated in Appendix A. By determination of the temperature where the activity of the dissolved oxide is equal to the pure oxide (either by measuring directly when the output emf for the cell reaction (37) equals zero, or by extrapolating the activity vs composition curves to the activity of the pure oxide), one can readily ascertain the FeO liquidus line for the binary system. The FeO liquidus obtained in this investigation is shown in Fig. 13 and is seen to be in good agreement with that obtained by quenching methods of Ibrahim and Carter.<sup>11</sup>

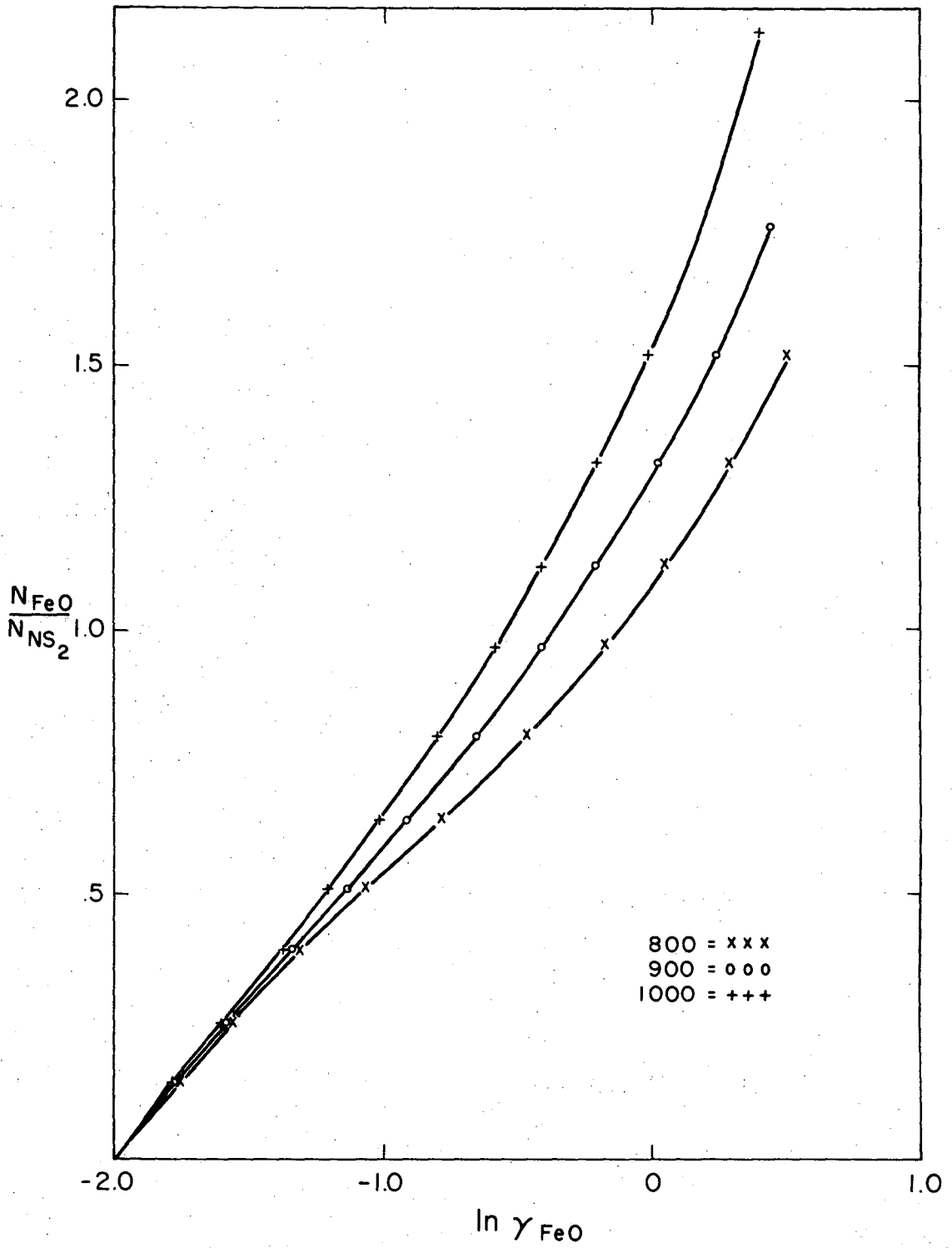
The partial molar free energy of the dissolution of solid FeO in NS glass is obtained directly from the temperature variation of the partial molar free energy of the cell reaction by using Eq. (27). The partial molar free energy for the reaction



may be similarly obtained from Eq. (16d) using activity values calculated from the Gibbs-Duhem integration. The integral free energy of mixing solid FeO with liquid  $\text{NS}_2$  according to reaction



is then calculated from Eq. (24). These data are presented in Appendix A and graphically illustrated in Fig. 8. The partial molar entropies



XBL 699-1401

Figure 6. Gibbs-Duhem integration plot for the determination of the activity of  $NS_2$ .

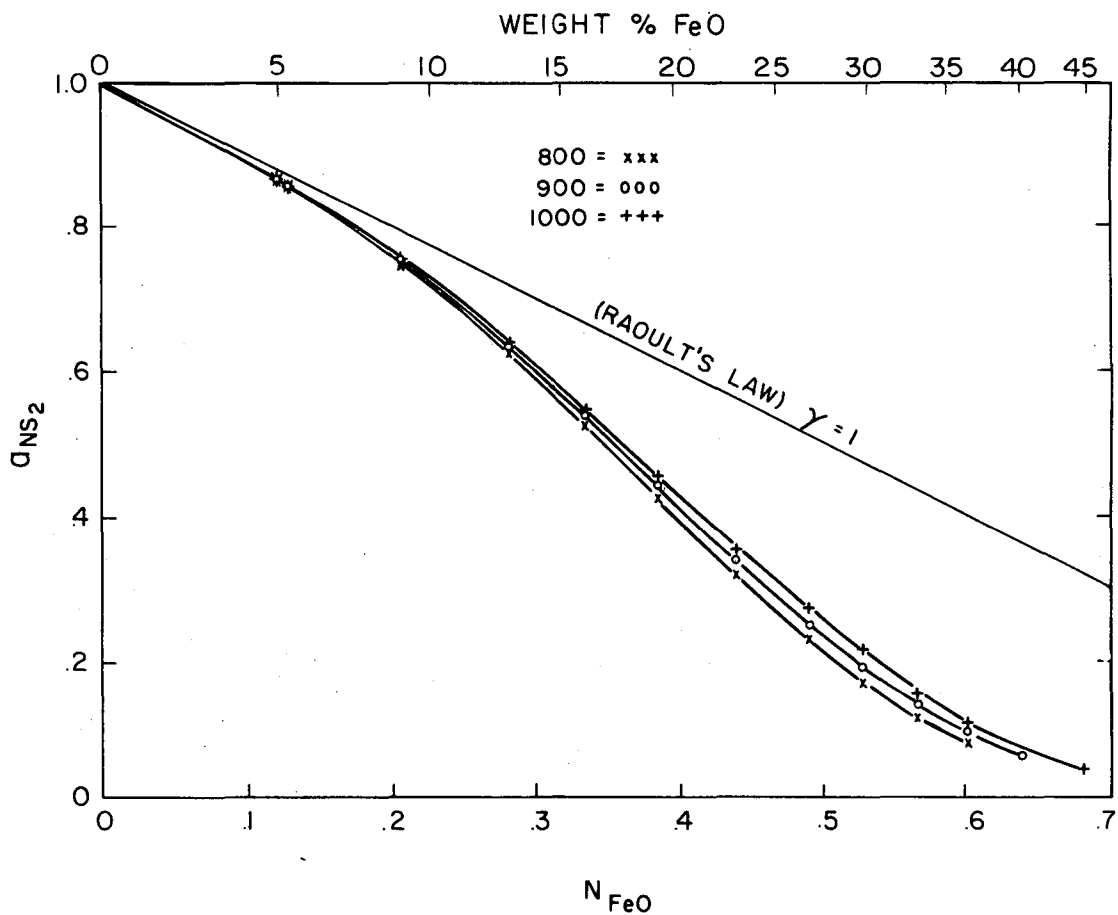
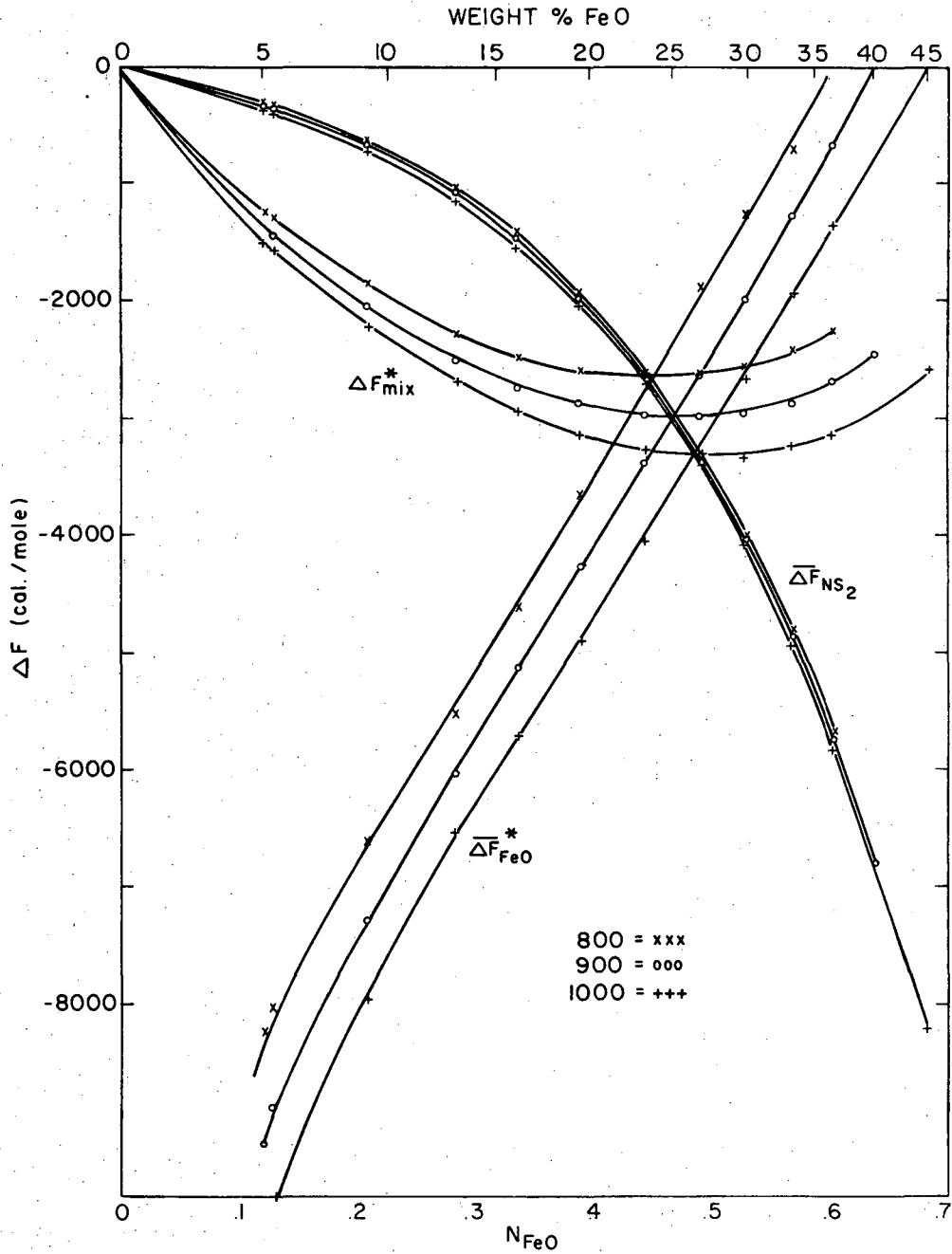


Figure 7. Isothermal activities of  $NS_2$  (referred to liquid standard state) calculated from Gibbs-Duhem integration.

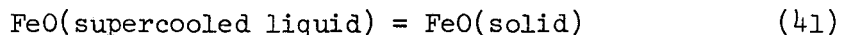


XBL 699-1403

Figure 8. Free energy plots for FeO (referred to the pure solid standard state);  $NS_2$  (referred to the pure liquid).

( $\overline{\Delta S}_{\text{FeO}}^*$ ,  $\overline{\Delta S}_{\text{NS}_2}$ ) and the integral entropy of mixing ( $\Delta S_{\text{mix}}^*$ ) as well as the partial molar enthalpies ( $\overline{\Delta H}_{\text{FeO}}^*$ ,  $\Delta H_{\text{NS}_2}$ ) and the enthalpies of mixing ( $\Delta H_{\text{mix}}^*$ ,  $\Delta H_{\text{mix}}^{**}$ ) are given in Figs. 9 and 10.

The thermodynamic functions pertaining to the mixing of the supercooled hypothetical liquid with pure liquid  $\text{NS}_2$  must take into account the reaction



by adding the partial molar functions for the above reaction to those calculated for reaction (40).

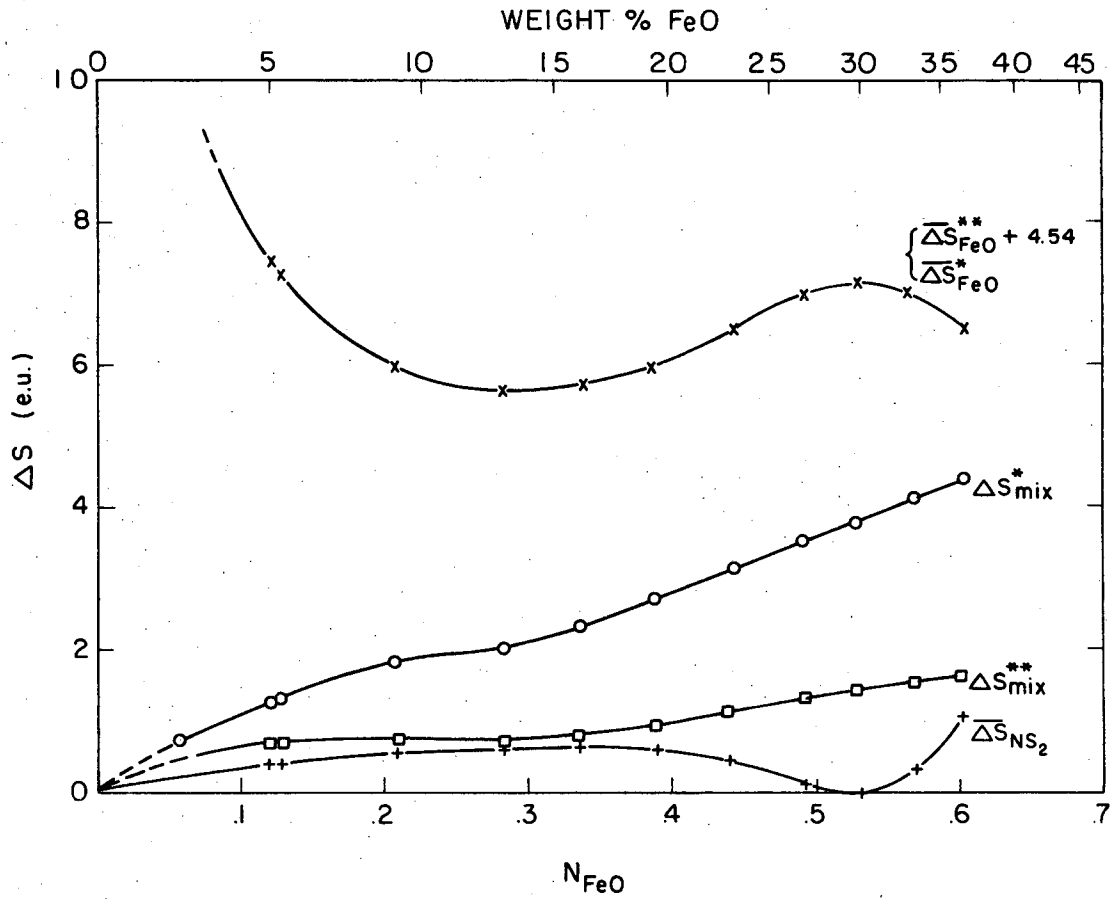
Since the heat capacity data for the supercooled liquid FeO is not available, the activity of the pure solid FeO relative to the pure liquid standard state was estimated from the relation

$$-\ln(a_s/a_l \equiv 1) = \frac{\Delta H_f}{RT} \left(1 - \frac{T}{T_f}\right) \quad (34)$$

where  $H_f = 8500$  cal/mole and  $T_f = 1367^\circ\text{C}$  ( $1650^\circ\text{K}$ ). Eq. (34) results from integration of the van't Hoff equation

$$\frac{d \ln K}{dT} = \frac{\Delta H}{RT} \quad (42)$$

where  $K$  is the equilibrium constant ( $a_{\text{solid}}/a_{\text{liquid}} \equiv 1$ ) for reaction (41), by assuming that the heat capacities of the solid and supercooled liquid are equal over the temperature interval of consideration, partial and



XBL 699-1404

Figure 9. Entropy plots for FeO and NS<sub>2</sub>.



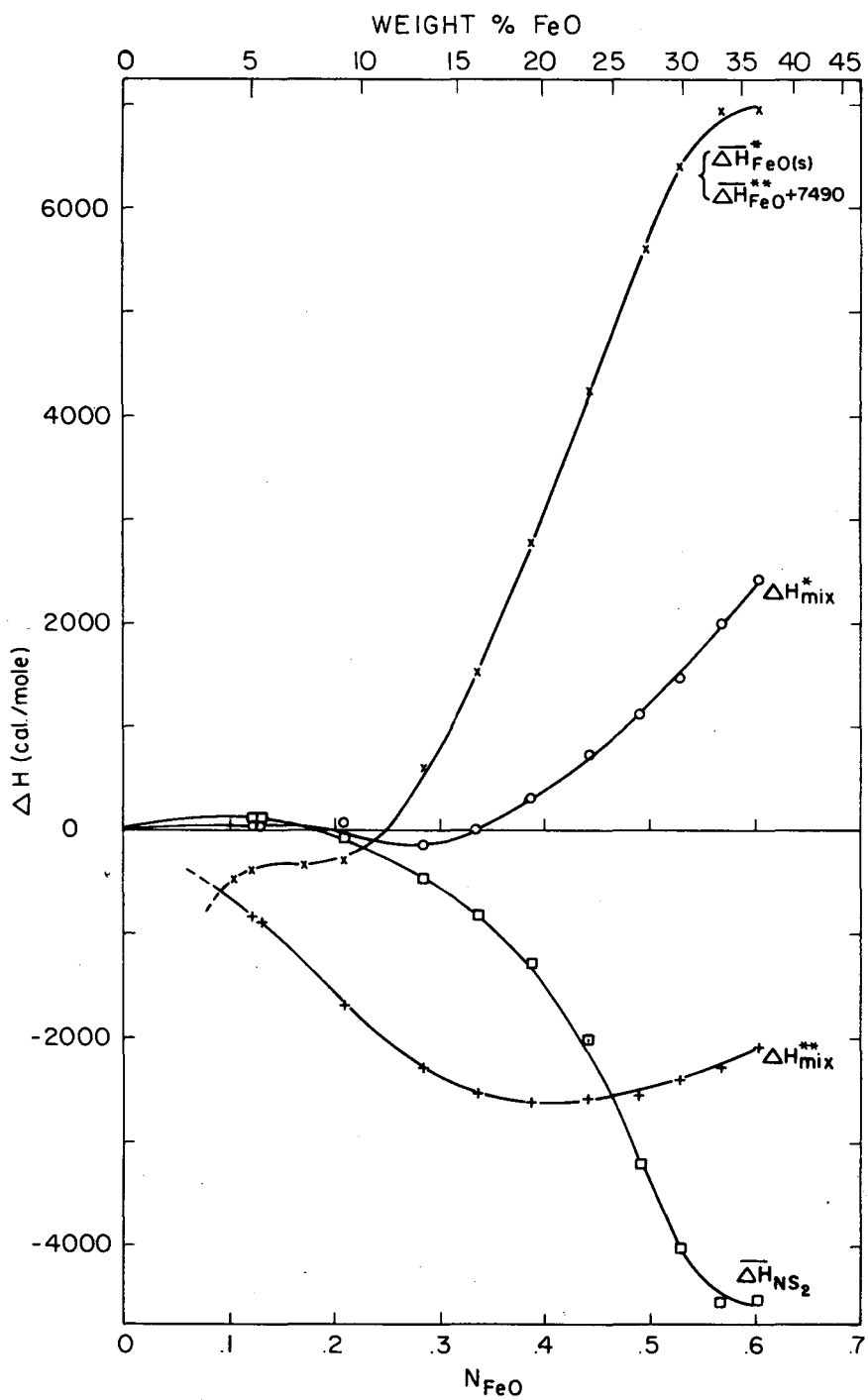
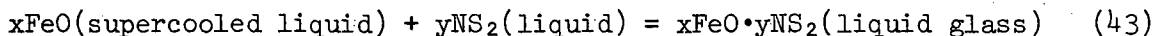


Figure 10. Enthalpy plots for FeO and NS<sub>2</sub>.

integral thermodynamic functions for the reaction



may be calculated from the combination of the measured data with that data calculated for reaction (41). These ( $\overline{\Delta F}_{\text{FeO}}^{**}$ ,  $\Delta S_{\text{mix}}^{**}$ ;  $\overline{\Delta H}_{\text{FeO}}^{**}$ ,  $\Delta H_{\text{mix}}^{**}$ ;  $\overline{\Delta F}_{\text{FeO}}^{**}$ ,  $\Delta F_{\text{mix}}^{**}$ ) are presented in Figs. 9, 10, and 11 respectively.

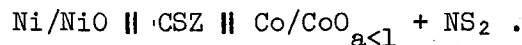
The NS<sub>2</sub> liquidus was found by determining the temperature of intersection of the NS<sub>2</sub> activity vs temperature lines for each glass composition with plots of the activity of solid NS<sub>2</sub> (referred to pure liquid) vs temperature calculated from the free energy change of the reaction



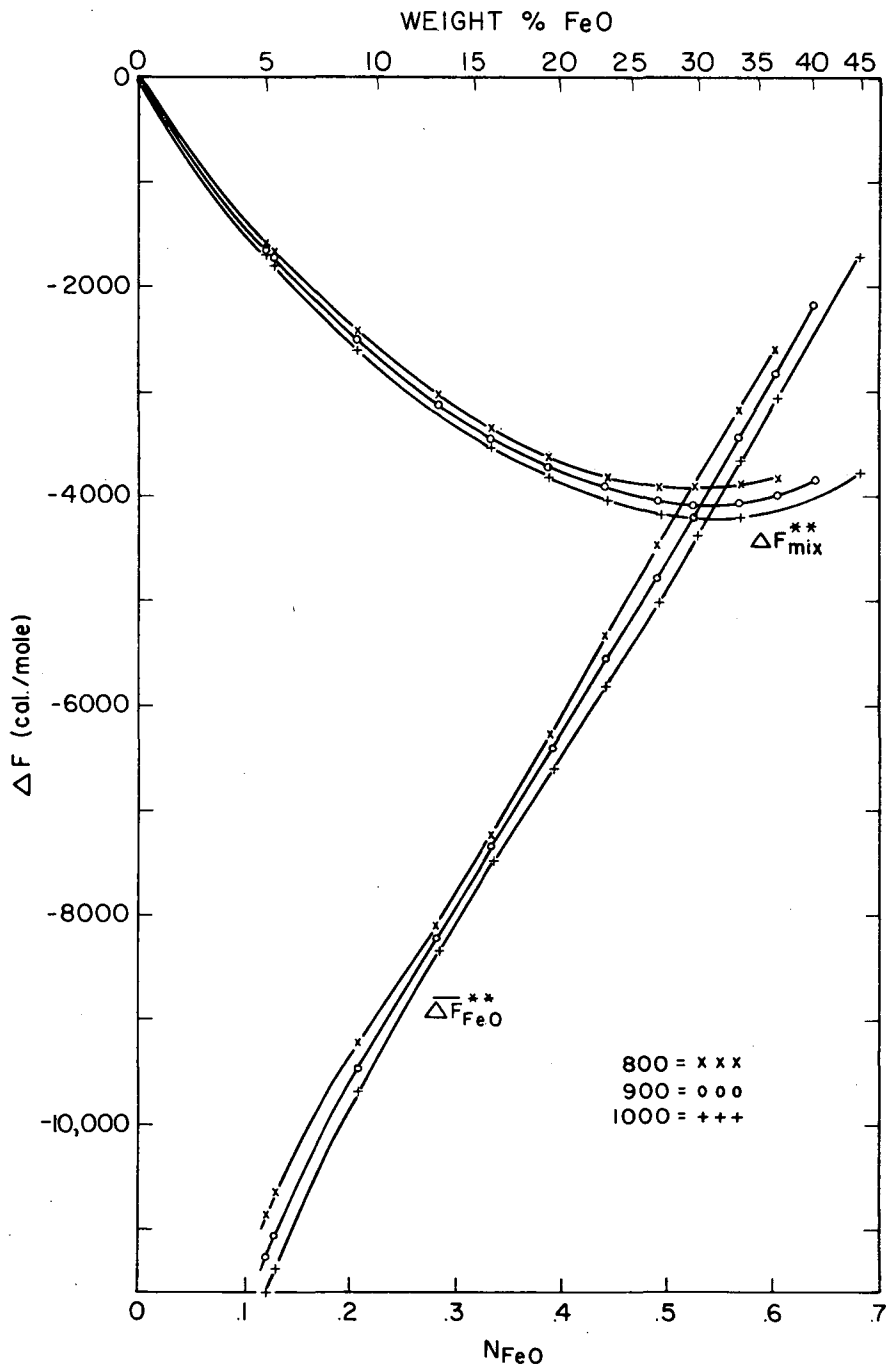
by integrating the heat capacity data of Kelley, according to Eq. (33). These data are presented in Fig. 12, and both liquiduses are plotted on a proposed phase diagram in Figs. 13 and 38. (See page 69 for a discussion of Fig. 38.)

#### B. The System CoO-NS<sub>2</sub>

Experimental determinations of the activity of CoO in NS<sub>2</sub> glass were made in a cell of the type

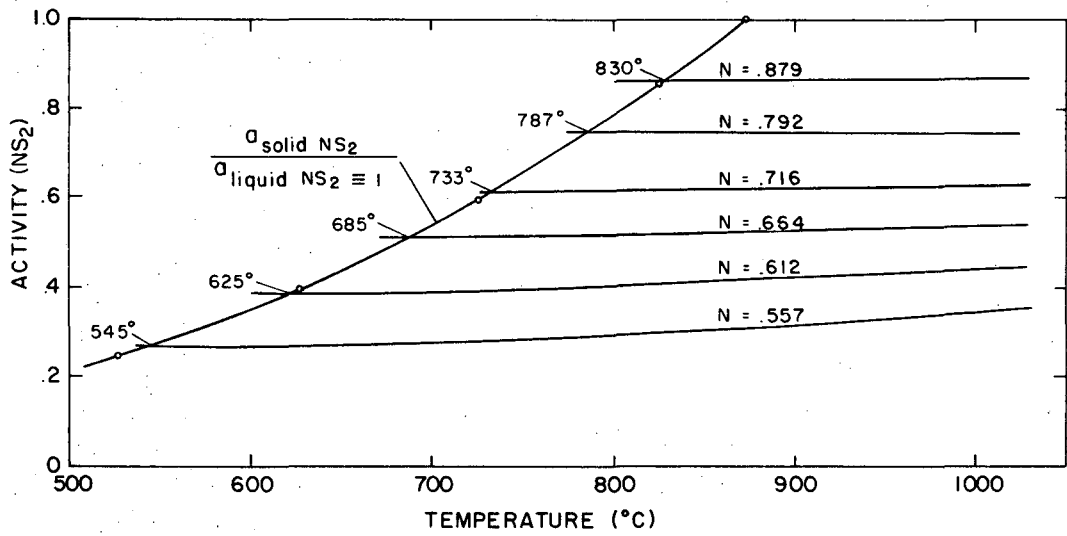


Initially, a mixture of Co/CoO was tried as the reference electrode



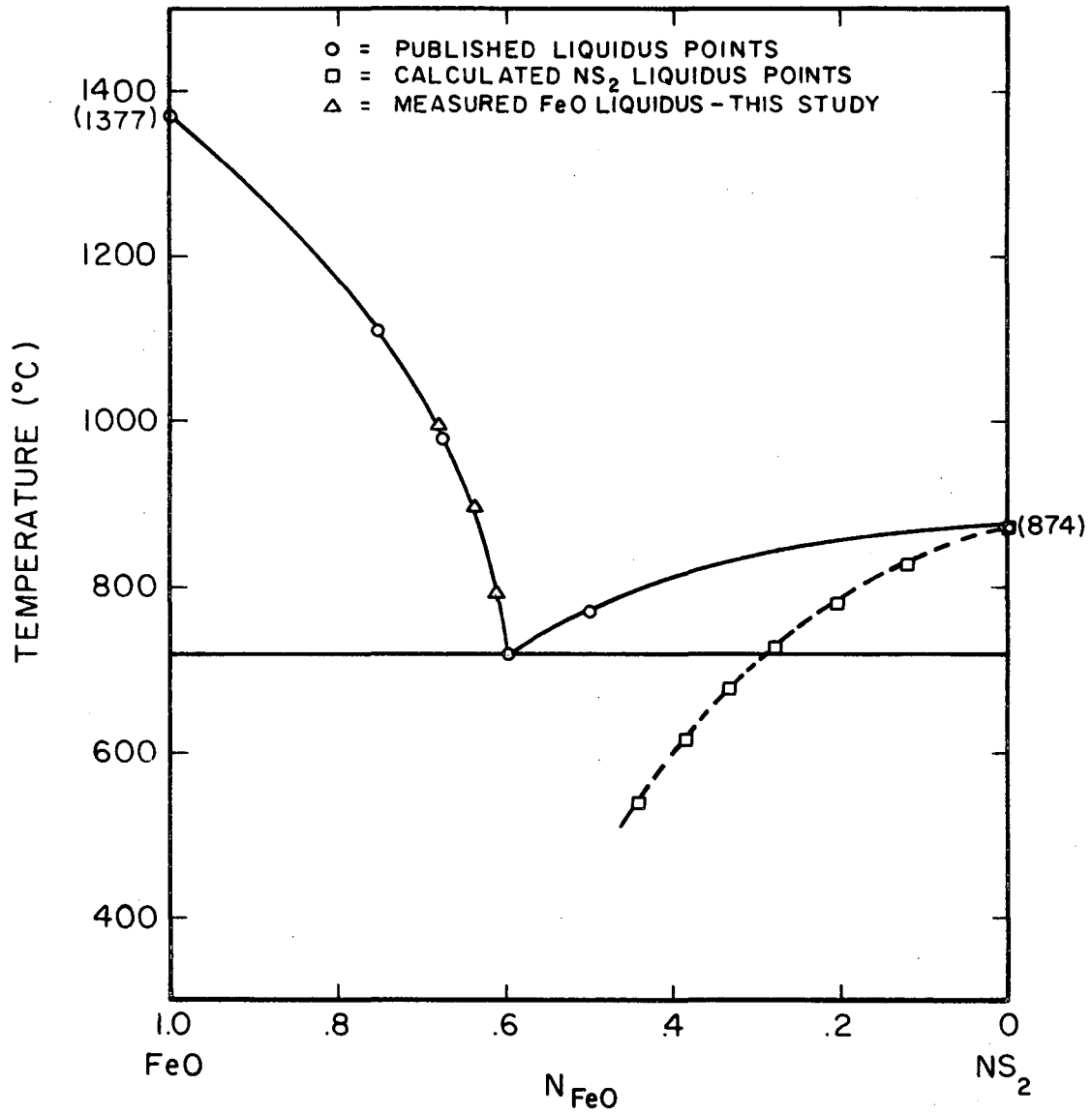
XBL 699-1406

Figure 11. Estimated free energy plots for FeO (referred to the pure supercooled liquid standard state).



XBL 699-1407

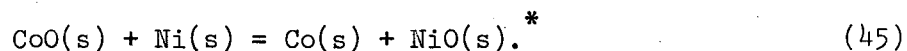
Figure 12. Isocompositional activity plots for NS<sub>2</sub> for determination of the NS<sub>2</sub> liquidus in the FeO-NS<sub>2</sub> system.



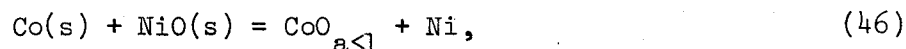
XBL 699-1408

Figure 13. Comparison of the calculated NS<sub>2</sub> and FeO liquiduses with the published phase diagram of Ibrahim and Carter.<sup>11</sup>

rather than Ni/NiO, but it was found that this mixture caused the Pt electrodes to become brittle, and was, therefore, unsatisfactory for extended cell runs. As with the FeO-NS<sub>2</sub> study, the data of Elliot and Gleiser<sup>21</sup> was used to calculate the standard free energy for the reaction



Adding this to the overall cell reaction



one obtains

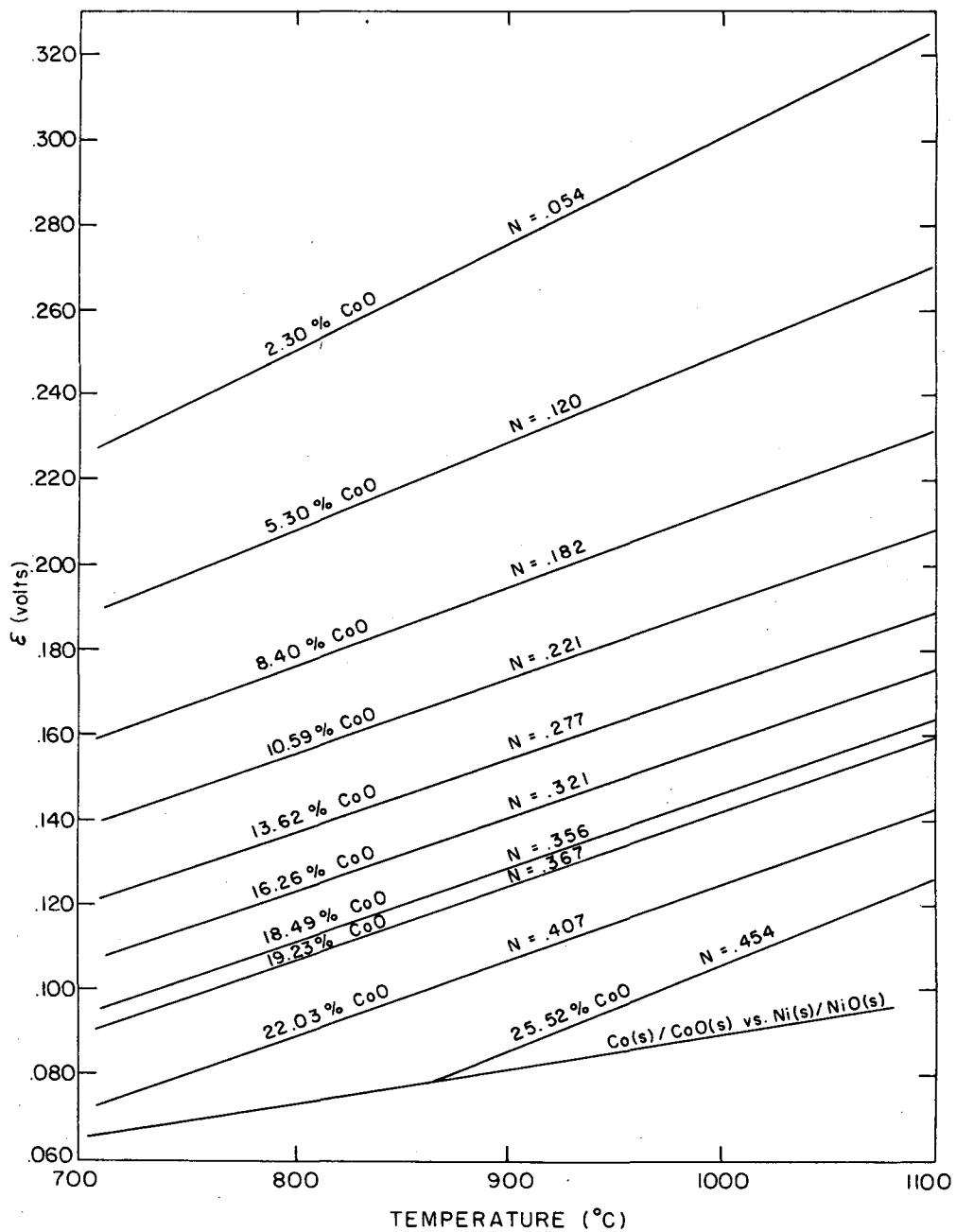


to which Eq. (17) may be applied for activity determination.

The isocompositional cell output (in volts) vs temperature is shown in Fig. 14. Each line represents the average of two or more trials and the uncertainty is  $\pm 2$  mv. The variation in activity of CoO with temperature for each composition is presented in Fig. 15, and the isothermal activity-composition plots are given in Fig. 16. In both figures, the activity of CoO is presented relative to pure solid CoO. The activity of solid CoO relative to the pure supercooled liquid CoO

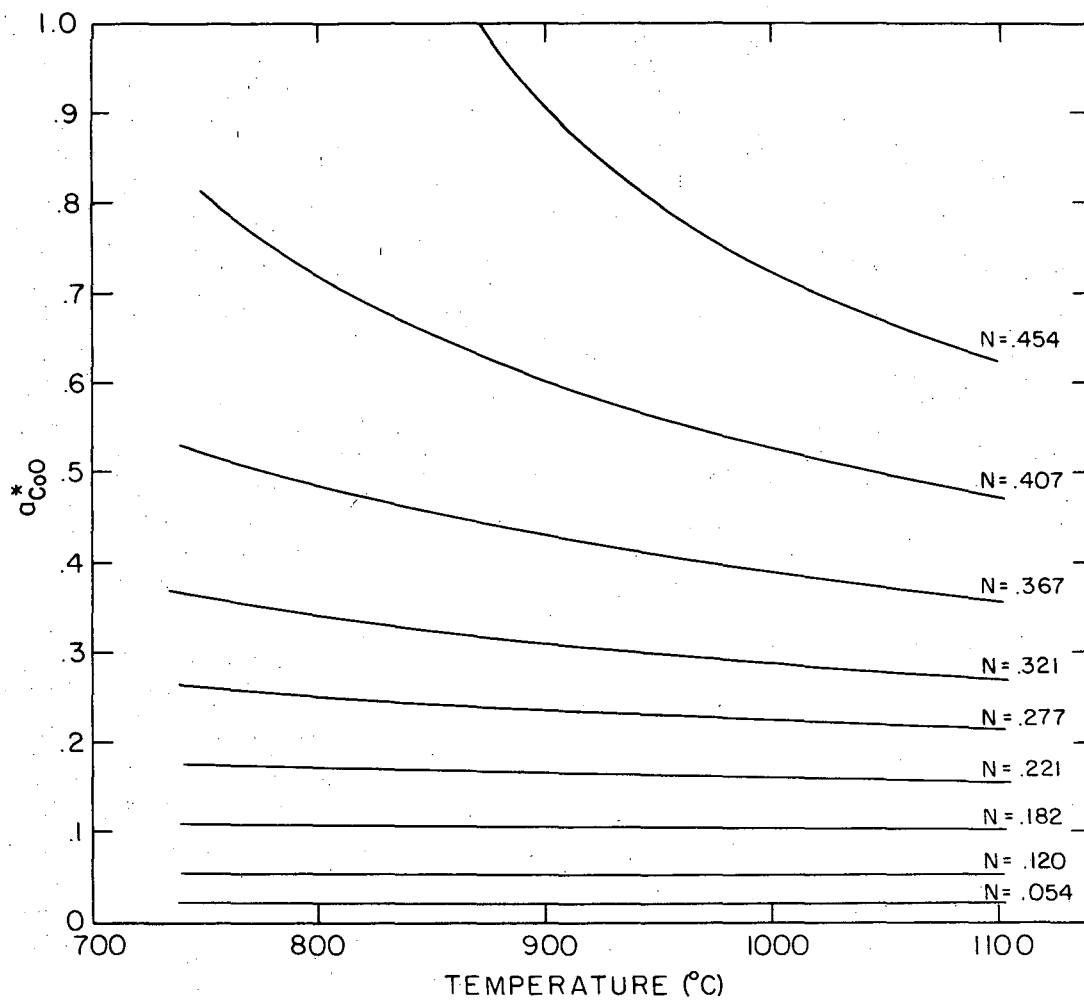
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\* As with the FeO experiments, output of a cell of the type Ni/NiO || CSZ || Co/CoO agreed well with the data of Elliot and Gleiser.<sup>21</sup>



XBL 699-1435

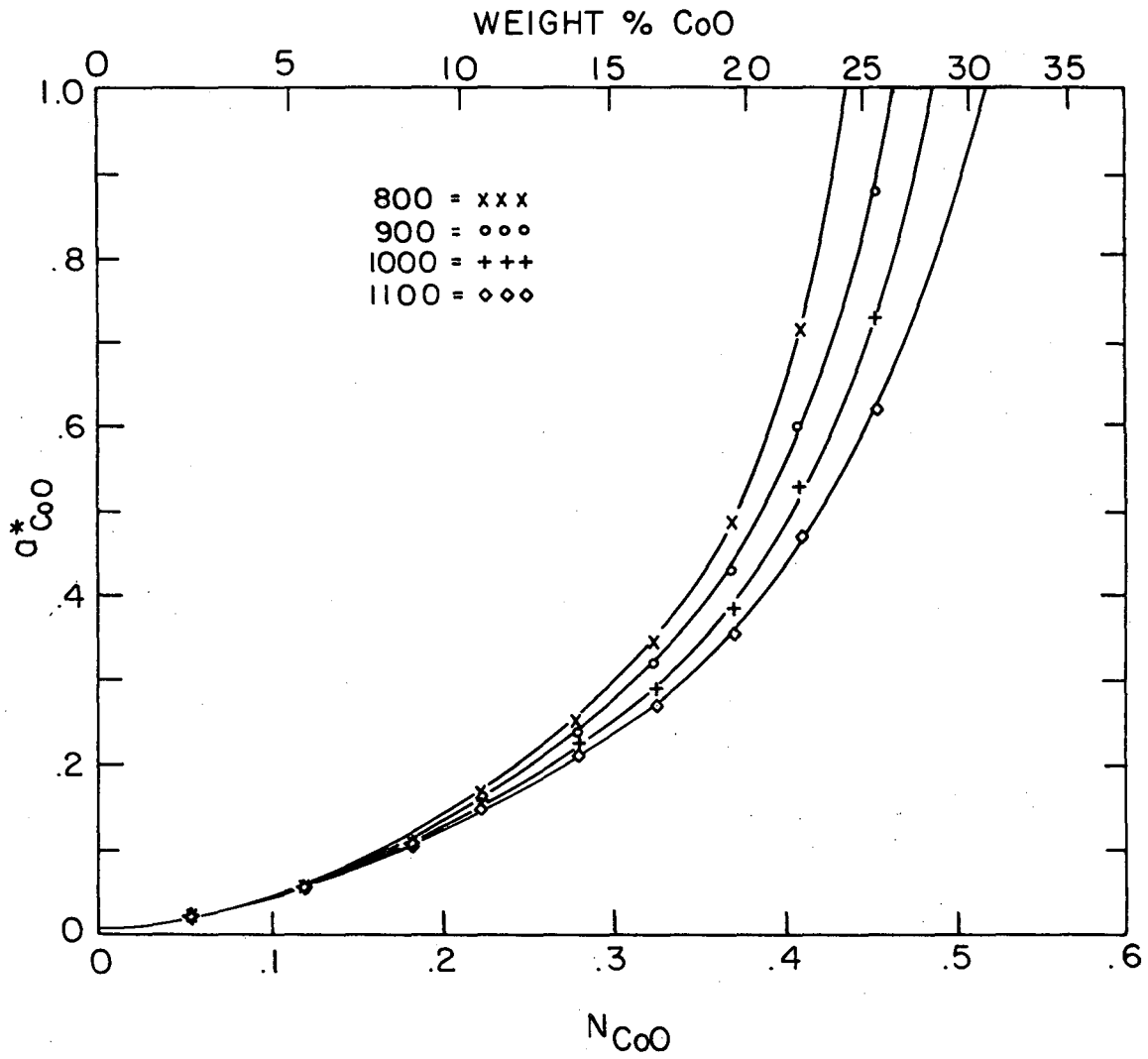
Figure 14. Isocompositional cell output for CoO-NS<sub>2</sub> glasses as a function of temperature ( $\pm 2$  min).



XBL 699-1433

Figure 15. Variation in the activity of CoO (referred to the pure solid standard state) with temperature for each composition studied.

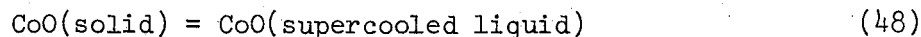




XBL 699-1411

Figure 16. Isothermal dependence of CoO activity (referred to the pure solid standard state) on composition.

was estimated from Eq. (34). The entropy of fusion ( $\Delta S_f$ ) was assumed to be the same as for FeO (4.54 cal/mole $^\circ$ C), and the heat of fusion ( $\Delta H_f$ ) was found from the product  $T_f \Delta S_f$ , ( $T_f=2078^\circ$ K), giving  $\Delta H_f = 9434$  cal/mole. The estimated activities of solid CoO relative to the pure liquid CoO standard state, and the approximate free energies for the reaction



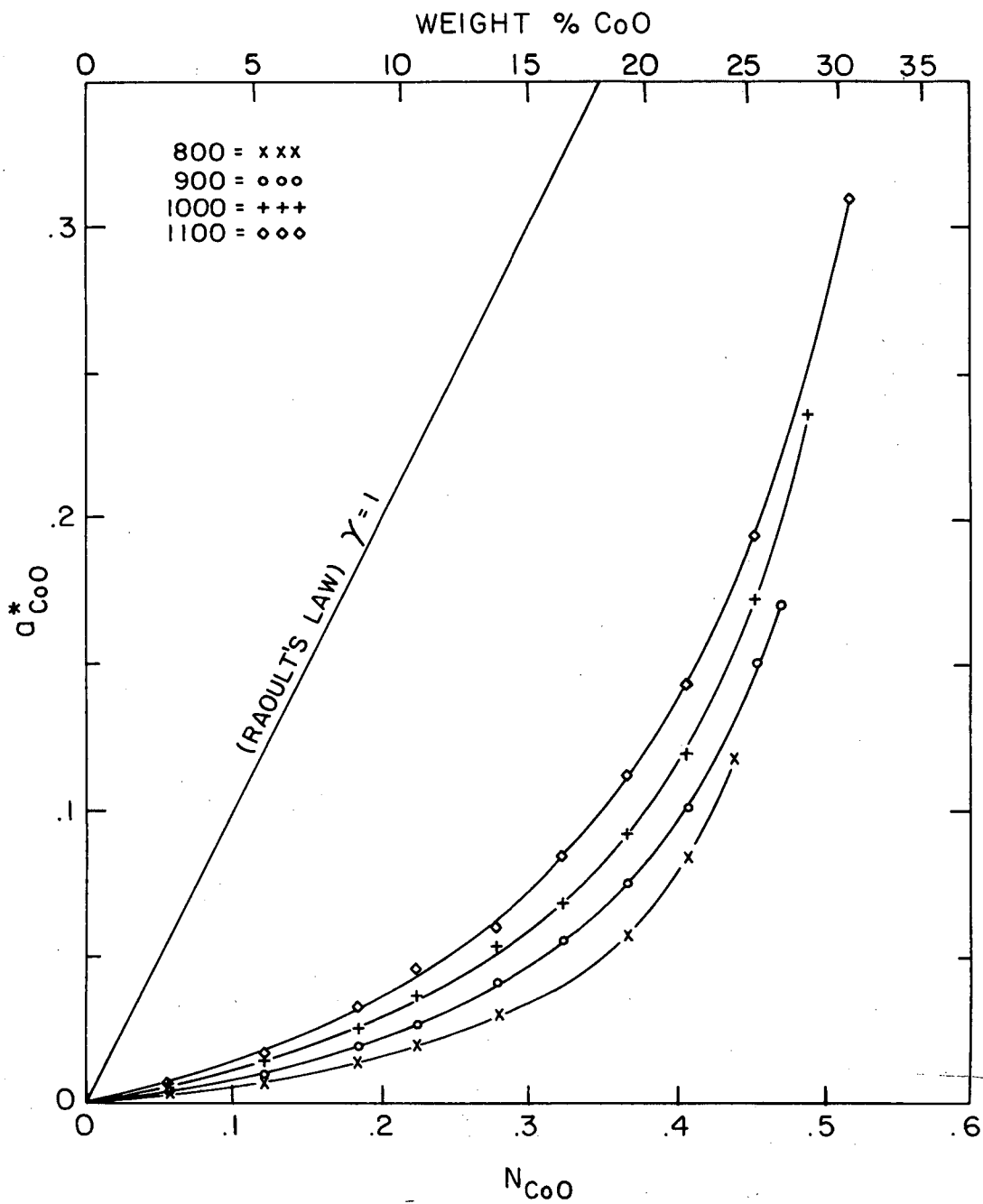
are presented in Appendix F. Activities of CoO in NS<sub>2</sub> glass solution referred to both standard states are listed in Appendix B, and isothermal plots of  $a_{\text{CoO}}^{**}$  vs composition are given in Fig. 17.

The activity coefficient of NS<sub>2</sub> relative to pure liquid NS<sub>2</sub> was found from graphical integration of the modified Gibbs-Duhem equation, as presented in Eq. (21). Plots of the alpha-function for four temperatures are given in Fig. 18, and activities calculated from this integration are presented in Fig. 19. They are similarly listed in Appendix B.

The partial thermodynamic functions for CoO and NS<sub>2</sub> were obtained in the same manner as for FeO (see pp. 11-13). The partial molar free energies for CoO and NS<sub>2</sub>, and the free energy ( $\Delta F_{\text{mix}}^*$ ) for one reaction

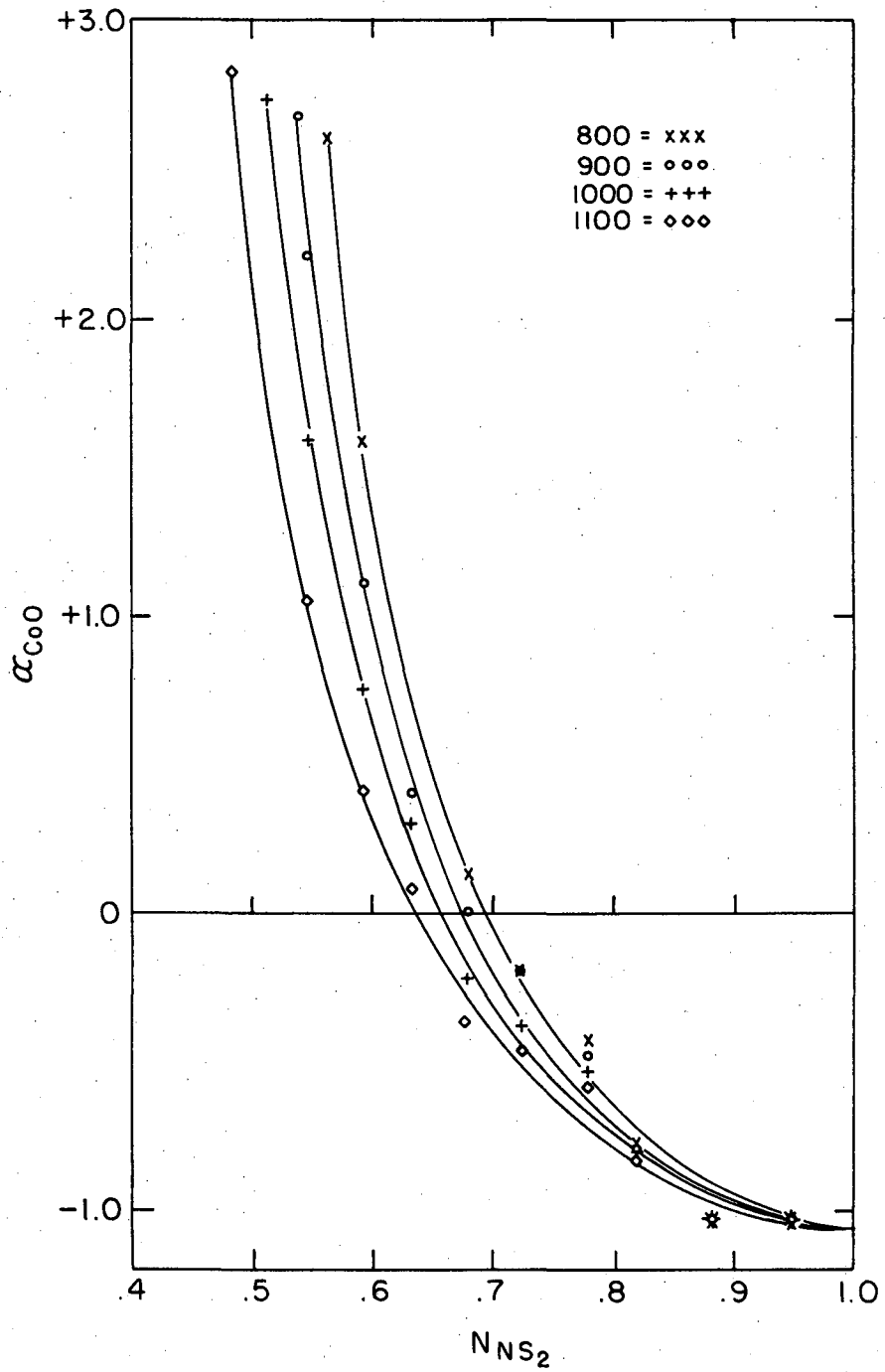


are plotted in Fig. 20 and listed in Appendix B. The partial molar free energy of CoO ( $\overline{\Delta F}_{\text{CoO}}^{**}$ ) and the free energy of mixing ( $\Delta F_{\text{mix}}^{**}$ ) for the



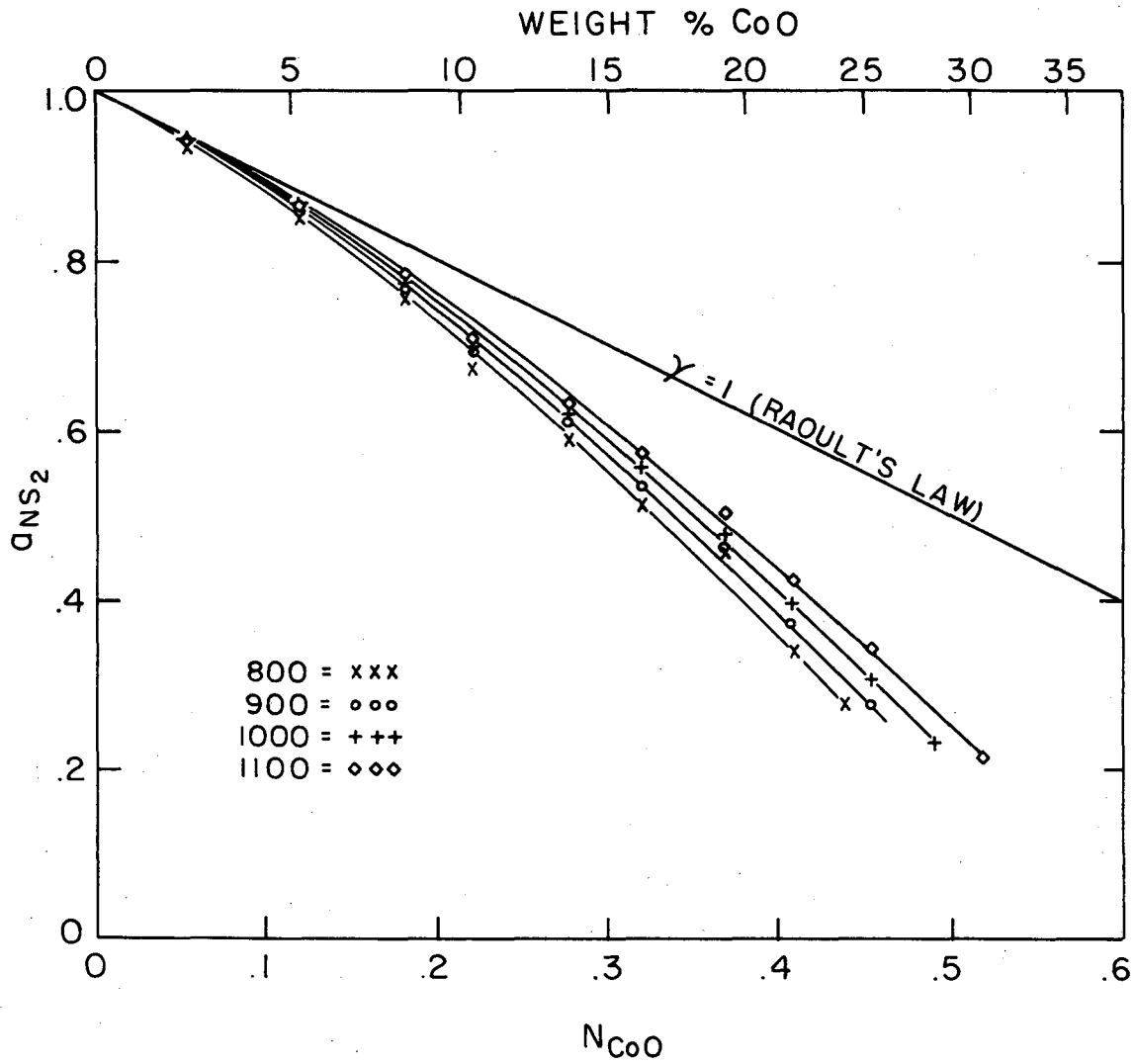
XBL 699-1412

Figure 17. Estimated isothermal dependence of the CoO activity (referred to pure supercooled liquid CoO) on composition.



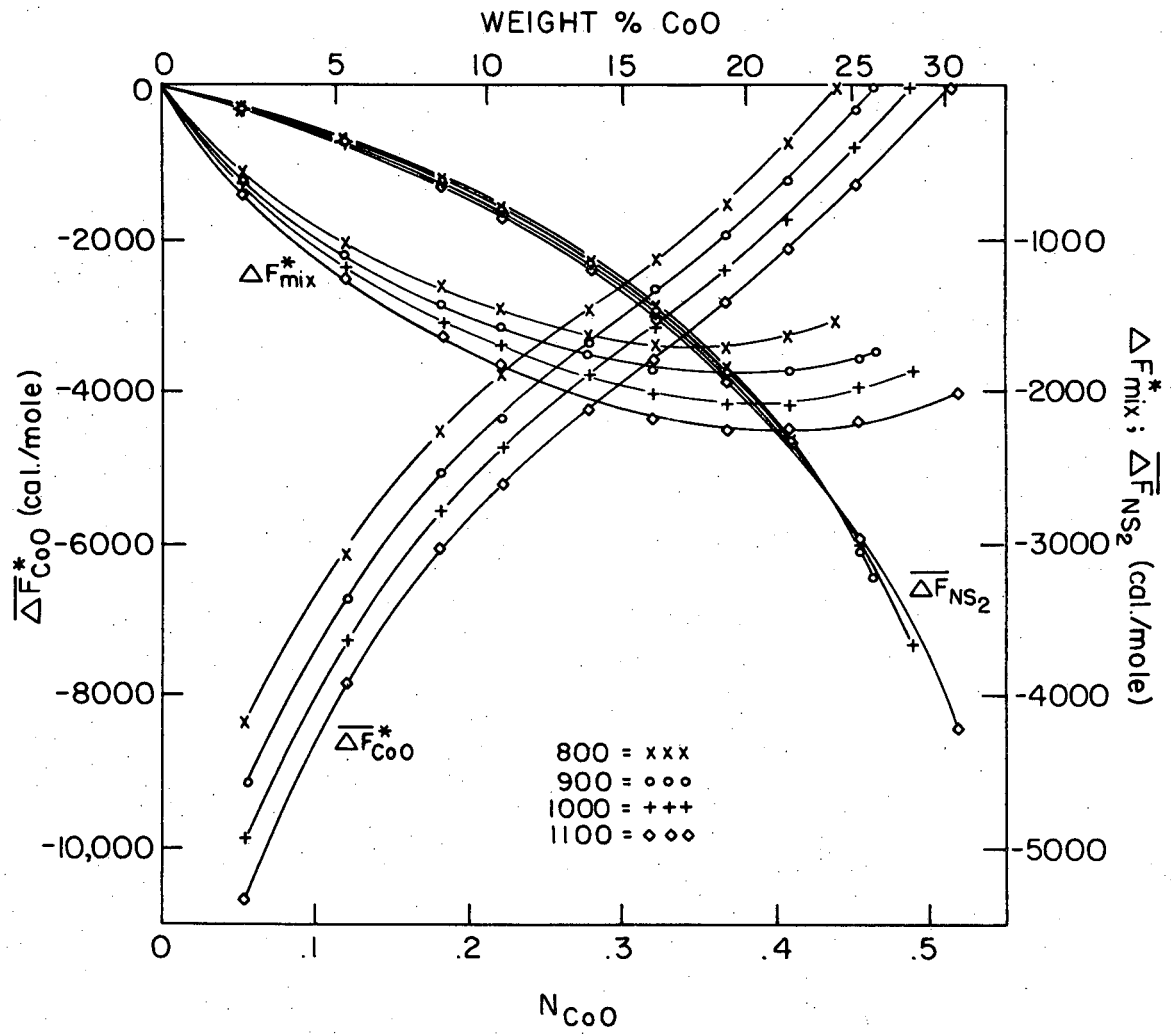
XBL 699-1413

Figure 18. Alpha function plot for determination of the activity of  $NS_2$  in the  $CoO-NS_2$  system by integration of the modified Gibbs-Duhem equation.



XBL 699-1414

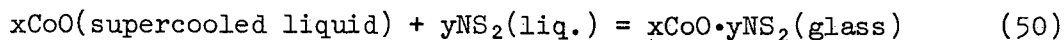
Figure 19. Isothermal activities of  $NS_2$  (referred to the liquid standard state) calculated from integration of the modified Gibbs-Duhem equation.



XBL 699-1415

Figure 20. Free energy plots for CoO (referred to the pure solid standard state); NS<sub>2</sub> (referred to the pure liquid).

reaction

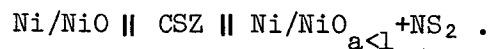


are plotted in Fig. 21 and listed in Appendix B. The partial molar entropies ( $\overline{\Delta S}_{\text{CoO}}^*$ ,  $\overline{\Delta S}_{\text{CoO}}^{**}$ ,  $\overline{\Delta S}_{\text{NS}_2}$ ) and the integral entropies of mixing ( $\Delta S_{\text{mix}}^*$ ,  $\Delta S_{\text{mix}}^{**}$ ); partial molar enthalpies ( $\overline{\Delta H}_{\text{CoO}}^*$ ,  $\overline{\Delta H}_{\text{CoO}}^{**}$ ,  $\overline{\Delta H}_{\text{NS}_2}$ ) and the enthalpies of mixing ( $\Delta H_{\text{mix}}^*$ ,  $\Delta H_{\text{mix}}^{**}$ ) for reactions (49) and (50) are given in Figs. 22 and 23 respectively.

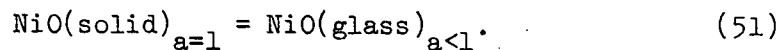
The NS<sub>2</sub> liquidus was determined from the intersection of plots of the measured activity of NS<sub>2</sub> with a plot of the activity of pure solid NS<sub>2</sub> relative to the pure liquid standard state. This is presented in Fig. 24. This solubility data, combined with the CoO liquidus data, determined by intersection of the  $a_{\text{CoO}}^*$  curves with  $a_{\text{CoO}}^* = 1.0$ , allows a tentative phase diagram for the pseudobinary system CoO-NS<sub>2</sub> to be proposed. This is illustrated in Fig. 25.

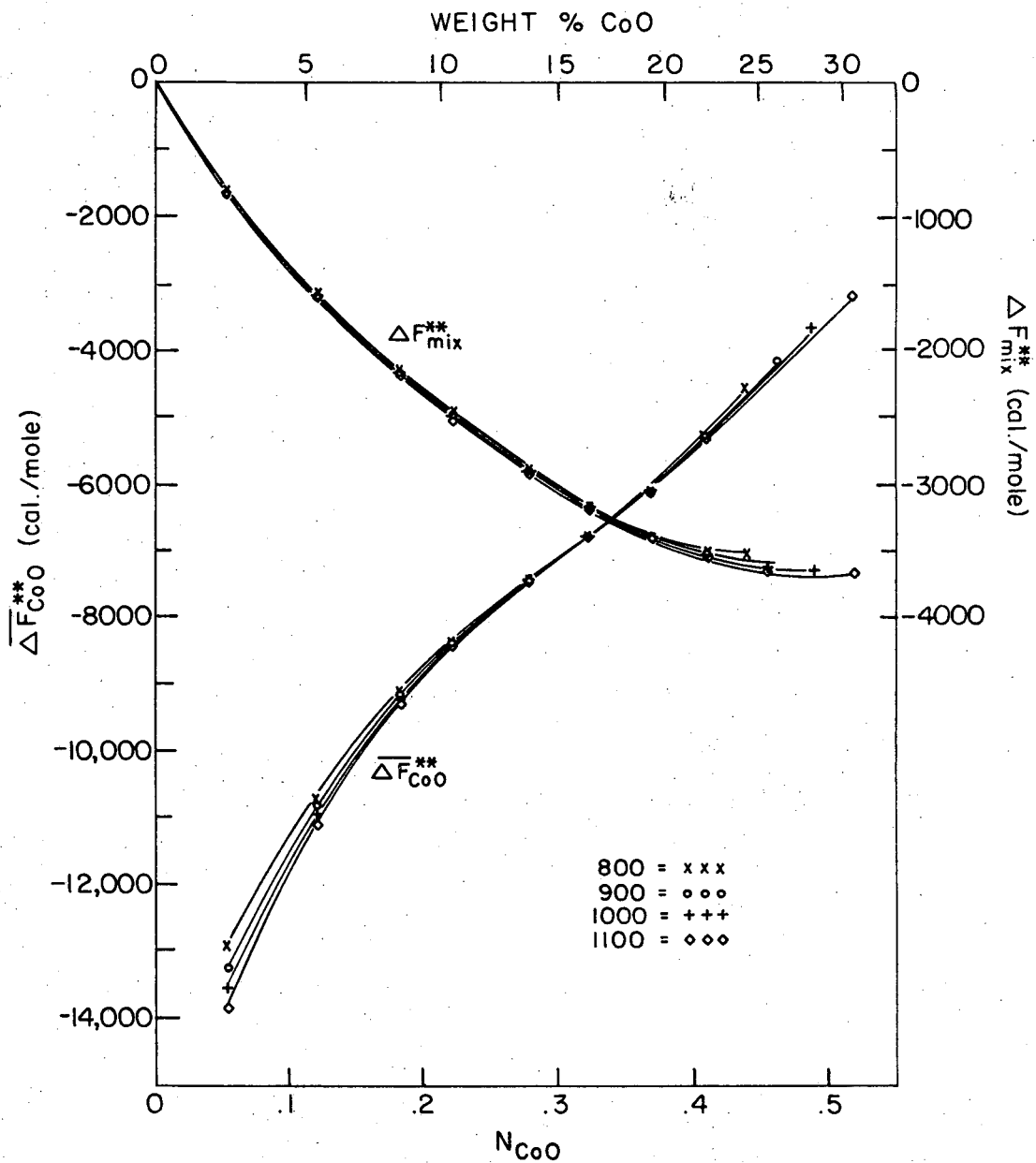
### C. The System NiO-NS<sub>2</sub>

Activity measurements were made in the NiO-NS<sub>2</sub> system by means of a cell of the type



Since Ni/NiO is used as the reference electrode, the overall cell reaction simply becomes

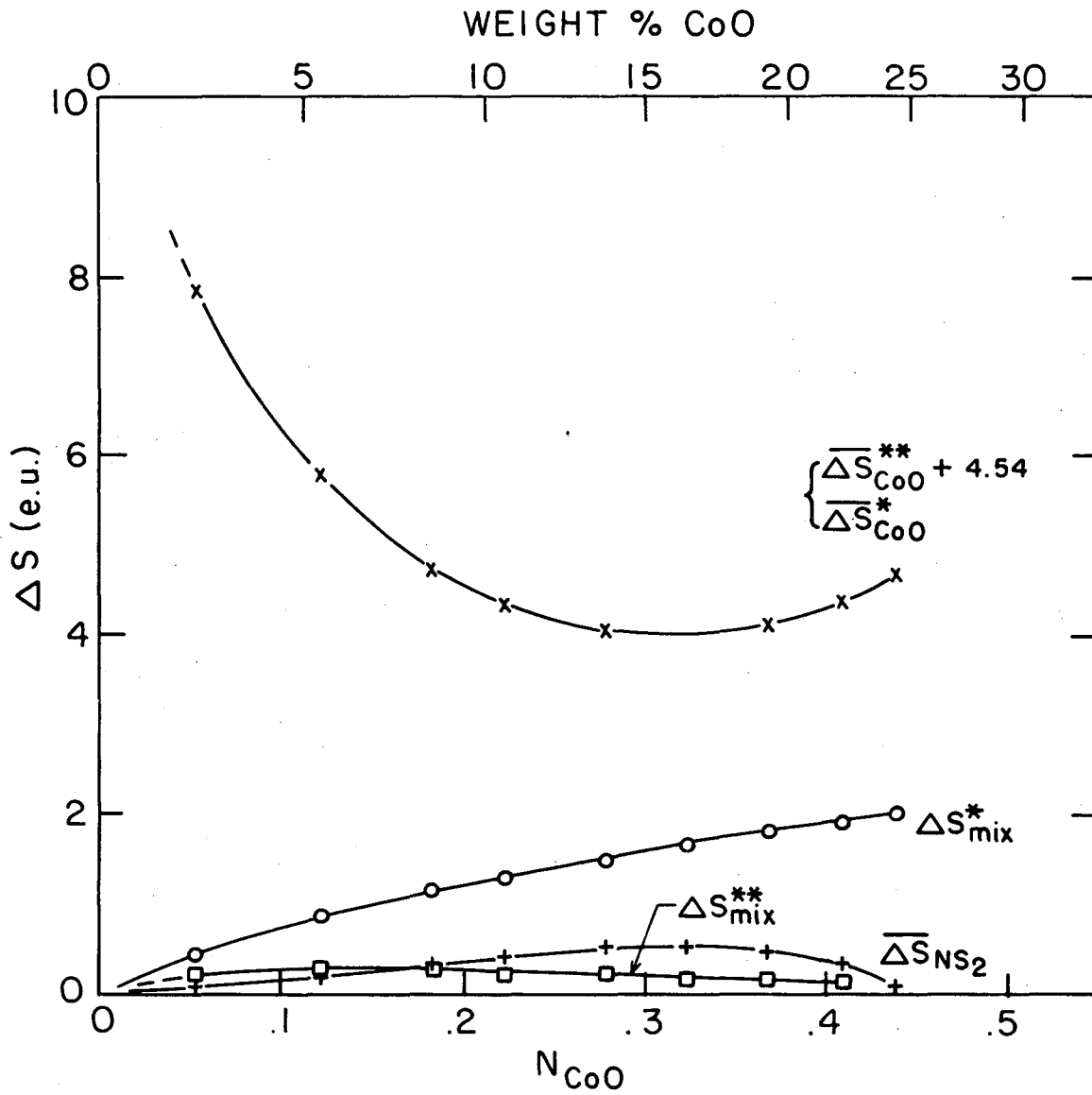




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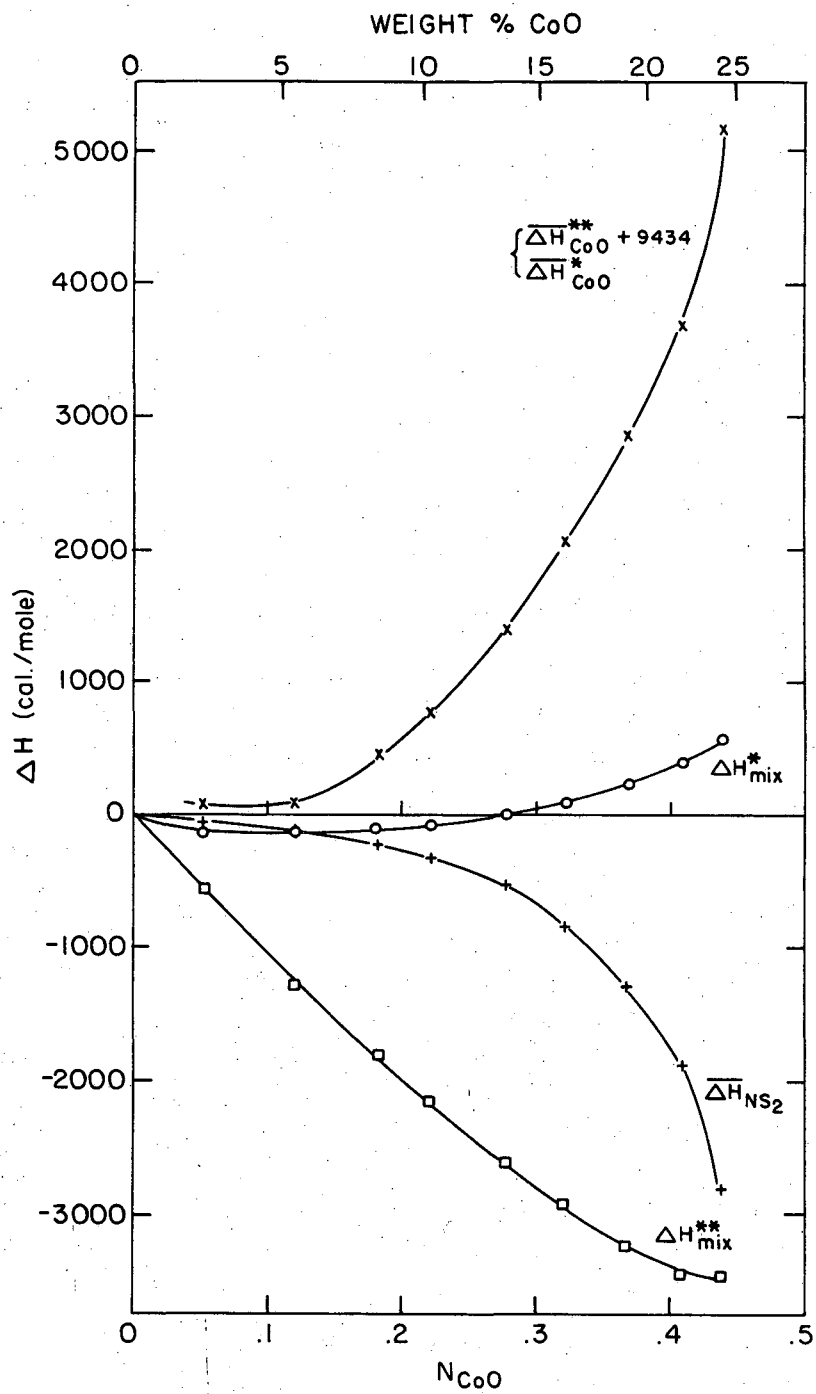
Figure 21. Estimated free energy plots for CoO (referred to the pure supercooled liquid standard state).





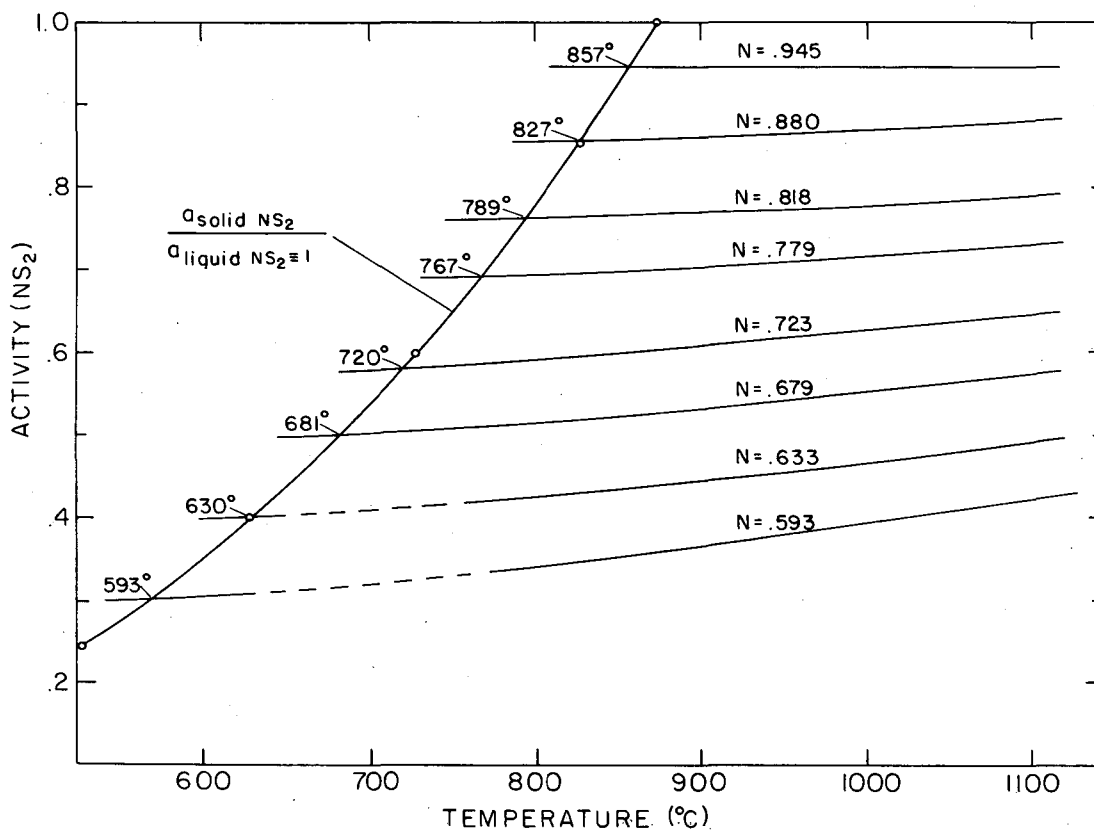
XBL 699-1416

Figure 22. Entropy plots for CoO and NS<sub>2</sub>.



XBL 699-1417

Figure 23. Enthalpy plots for  $\text{CoO}$  and  $\text{NS}_2$ .



XBL 699-1419

Figure 24. Isocompositional activity plots for NS<sub>2</sub> for determination of the NS<sub>2</sub> liquidus in the CoO-NS<sub>2</sub> system. \*

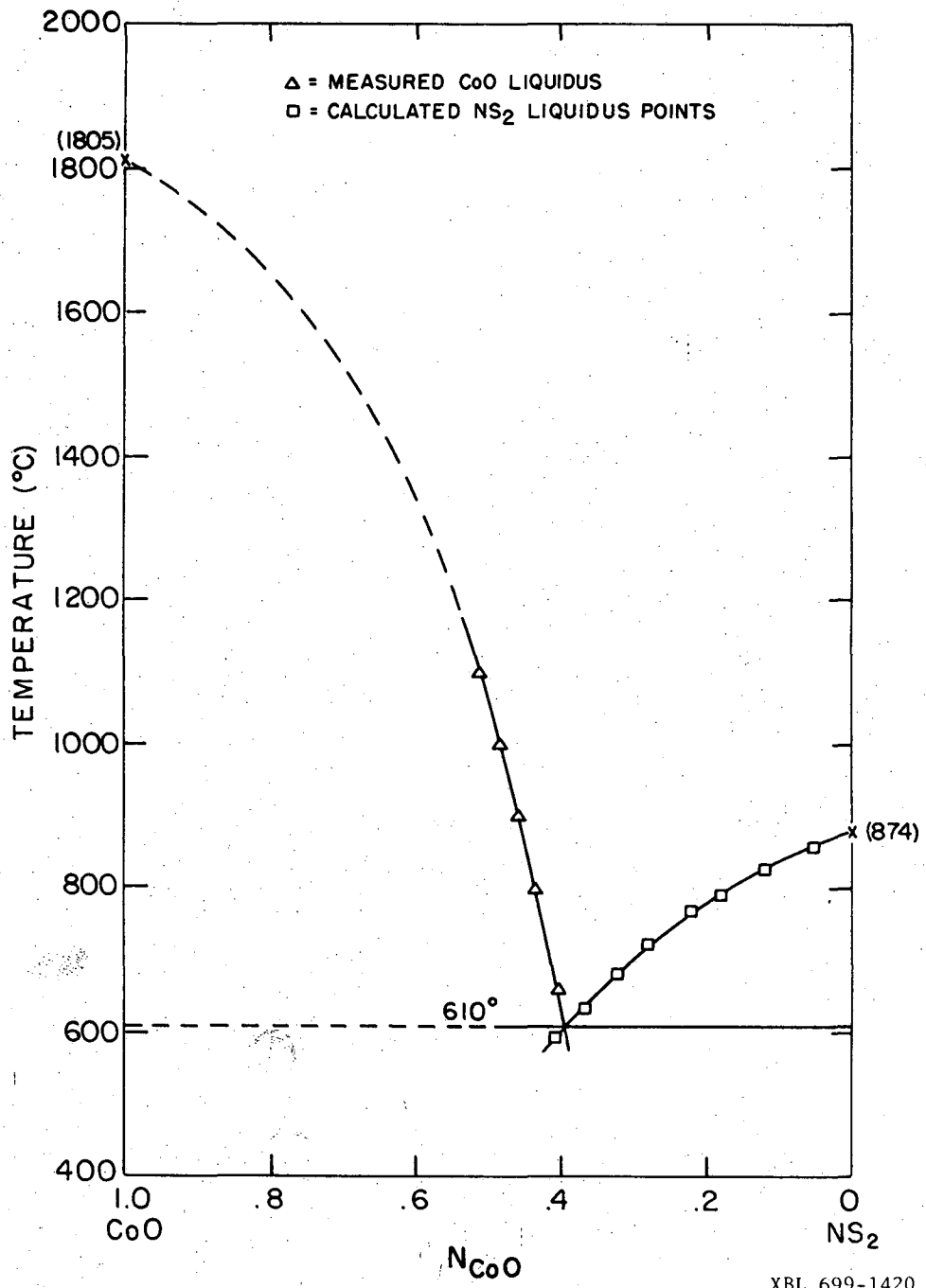
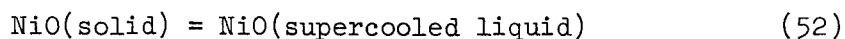


Figure 25. Proposed phase diagram for the CoO-NS<sub>2</sub> system.

XBL 699-1420

Equation (17) is thus applicable for determination of  $a_{\text{NiO}}^*$ .

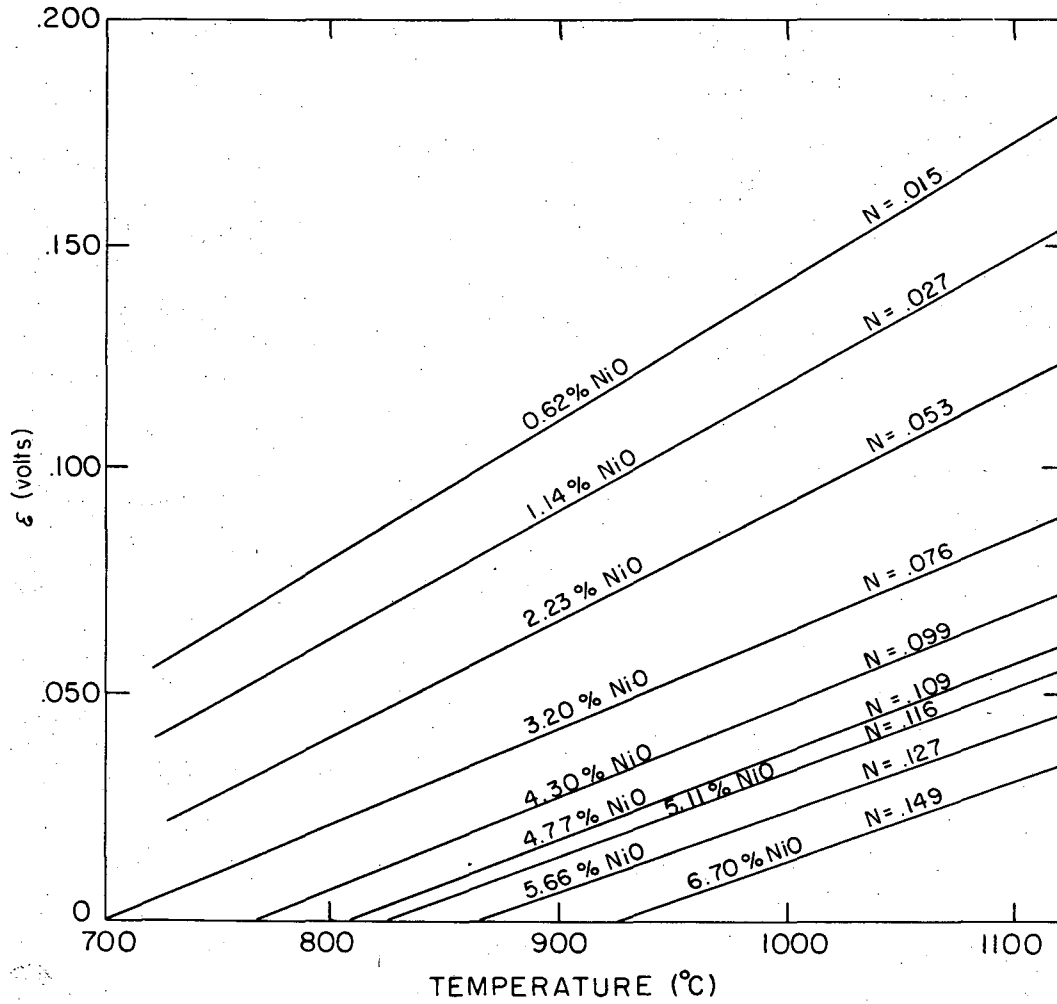
The isocompositional cell output (in volts) vs temperature is shown in Fig. 26. As with the CoO and FeO studies, each line represents the average of a minimum of two experimental determinations for each composition. The uncertainty is  $\pm 2$  mv. The variation of  $a_{\text{NiO}}^*$  with temperature for each composition is shown in Fig. 27, and the isothermal activity-composition plots are given in Fig. 28. Assuming an entropy of fusion of 4.54 e.u. (the reported value for FeO), and enthalpy of fusion ( $\Delta H_f$ ) of 10161 cal/mole was estimated at  $T_f(\text{NiO})=2238^\circ\text{K}$ . The activity of pure solid NiO relative to the hypothetical supercooled liquid NiO was estimated between  $800^\circ$  and  $1100^\circ\text{C}$  from Eq. (34). These activities and the free energies for the reaction



are presented in Appendix F. The estimated activities of NiO referred to this supercooled liquid NiO ( $a_{\text{NiO}}^{**}$ ) are given in Appendix C and graphically presented in Fig. 29.

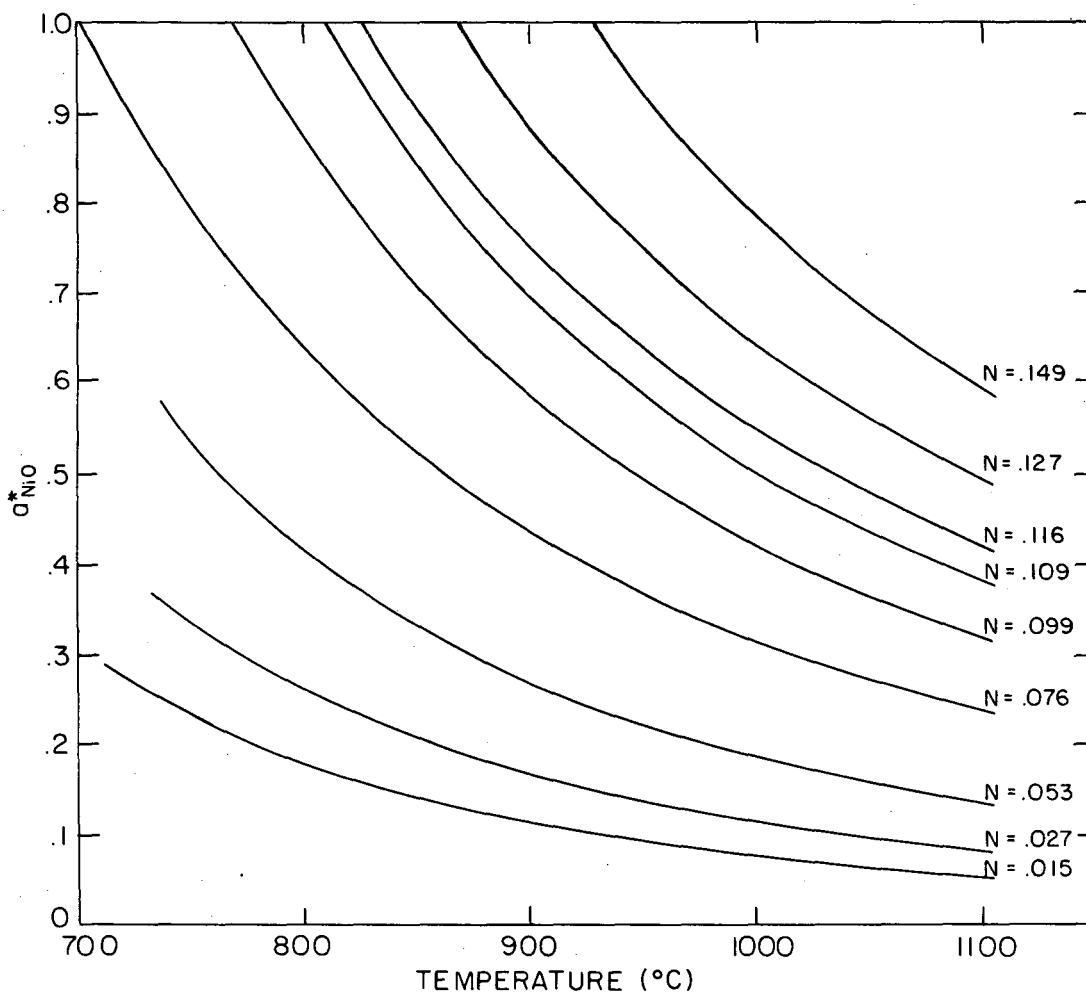
The activity of  $\text{NS}_2$  relative to the pure liquid was calculated from integration of Eq. (21). Plots of the alpha functions for the temperatures of consideration are given in Fig. 30, and the calculated activities are plotted vs. composition in Fig. 31.

The partial molar thermodynamic functions were calculated in the same manner as for the FeO and CoO systems. The partial molar free energies ( $\overline{\Delta F}_{\text{NiO}}^*$ ,  $\overline{\Delta F}_{\text{NS}_2}$ ) and the free energy ( $\Delta F_{\text{mix}}^*$ ) for the reaction



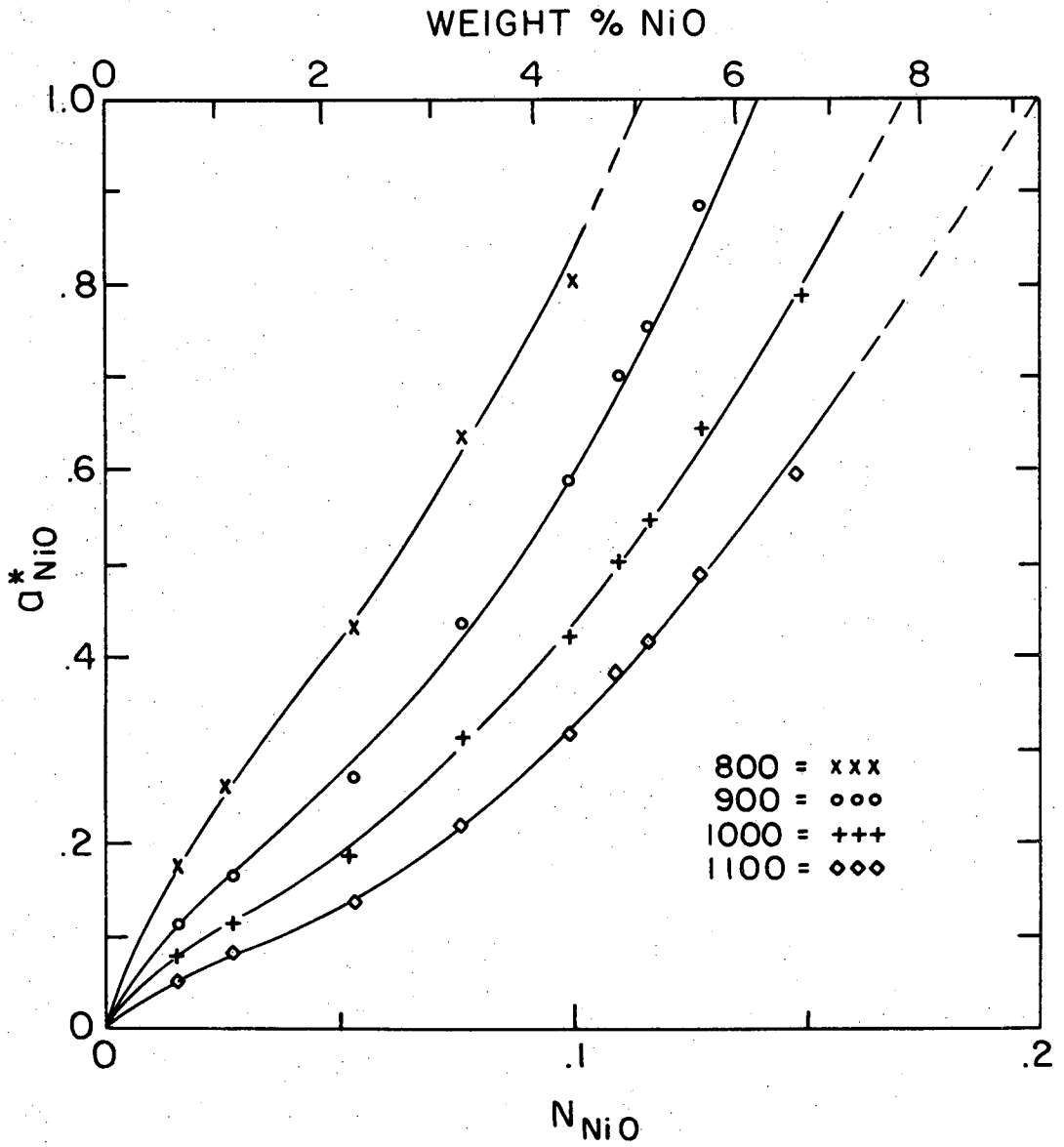
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Figure 26. Isocomposition cell output for NiO-NS<sub>2</sub> glasses as a function of temperature ( $\pm 2$  mv).



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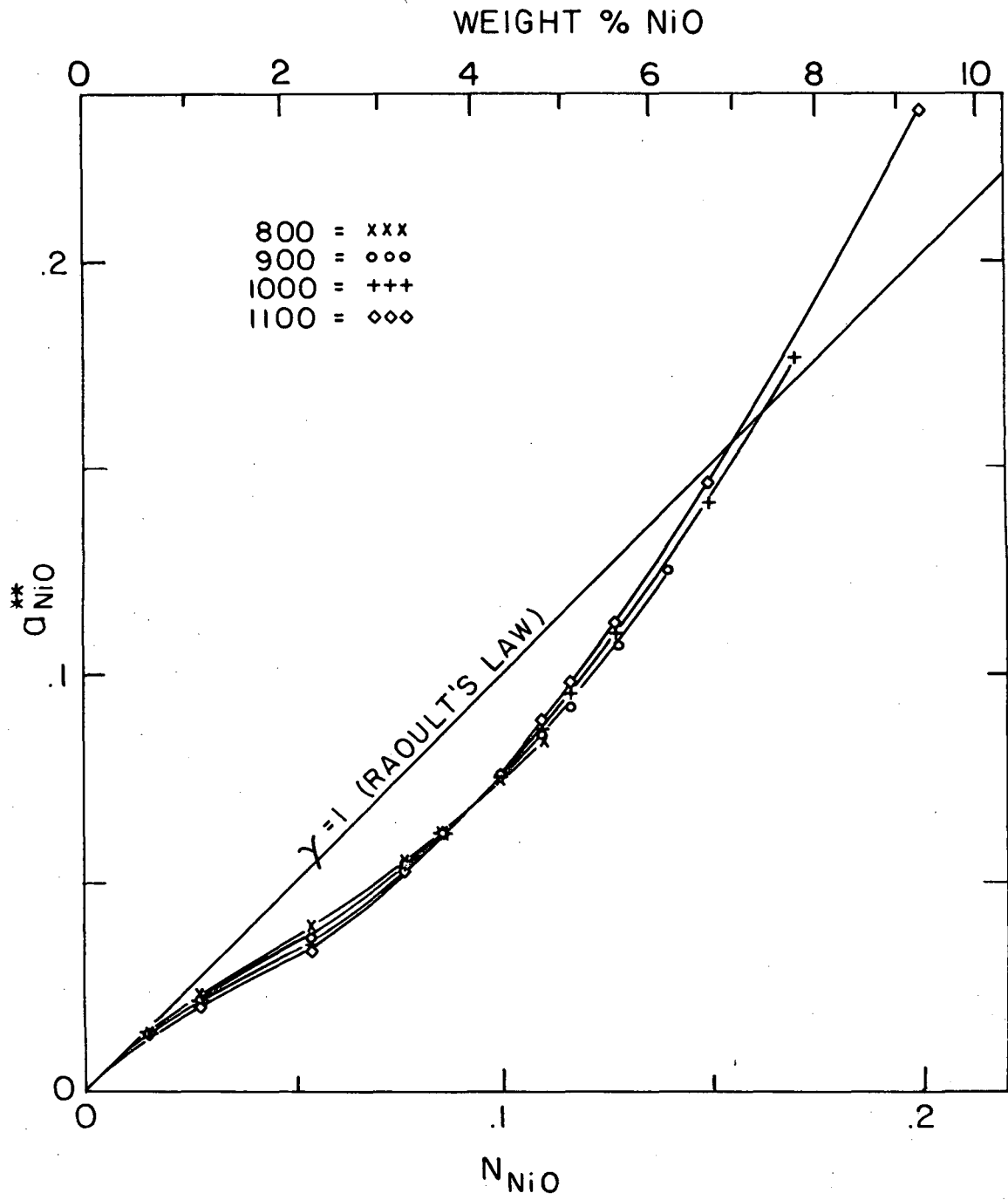
Figure 27. Variation in the activity of NiO (referred to the pure solid standard state) with temperature for each composition studied.



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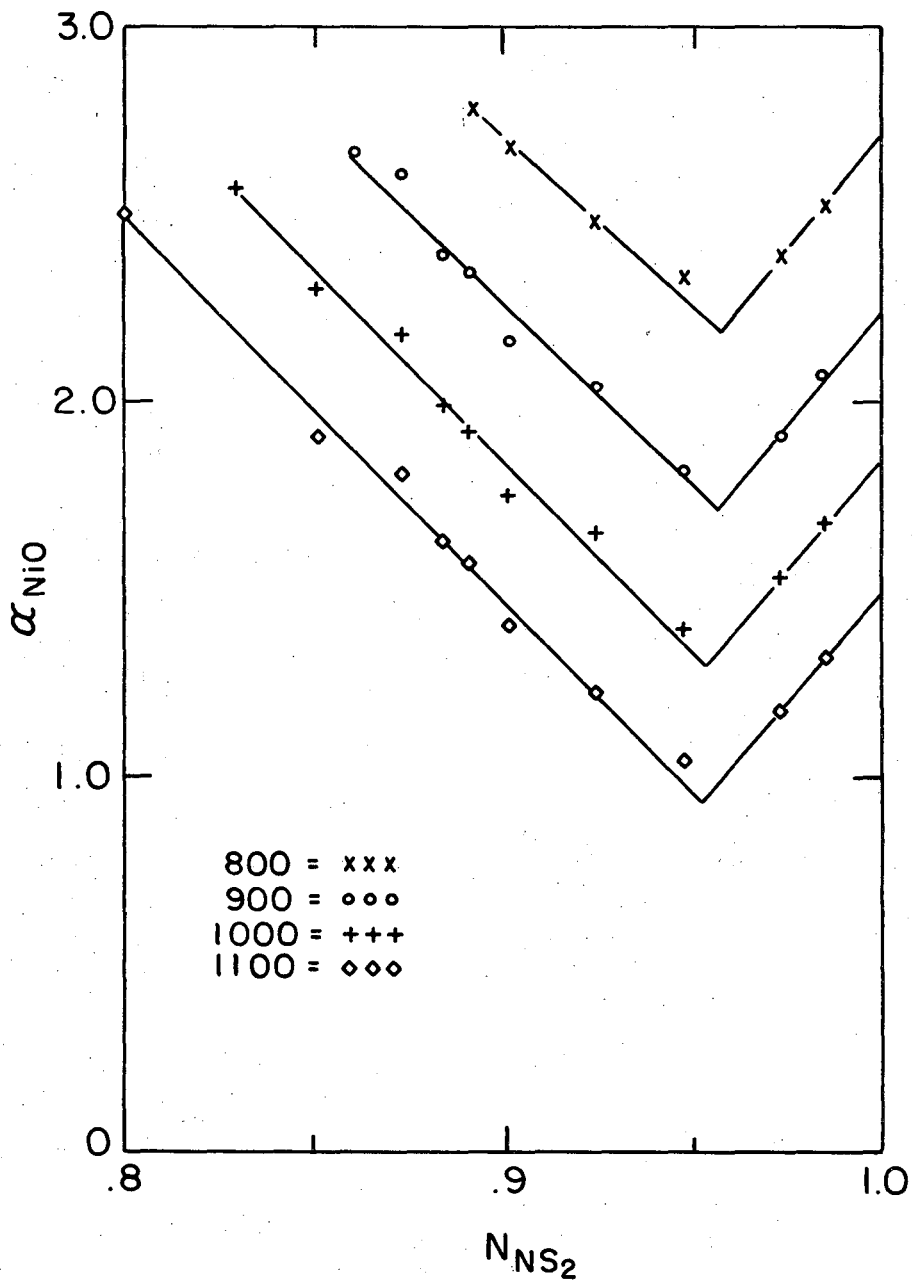
Figure 28. Isothermal dependence of NiO activity (referred to the pure solid standard state) on composition.





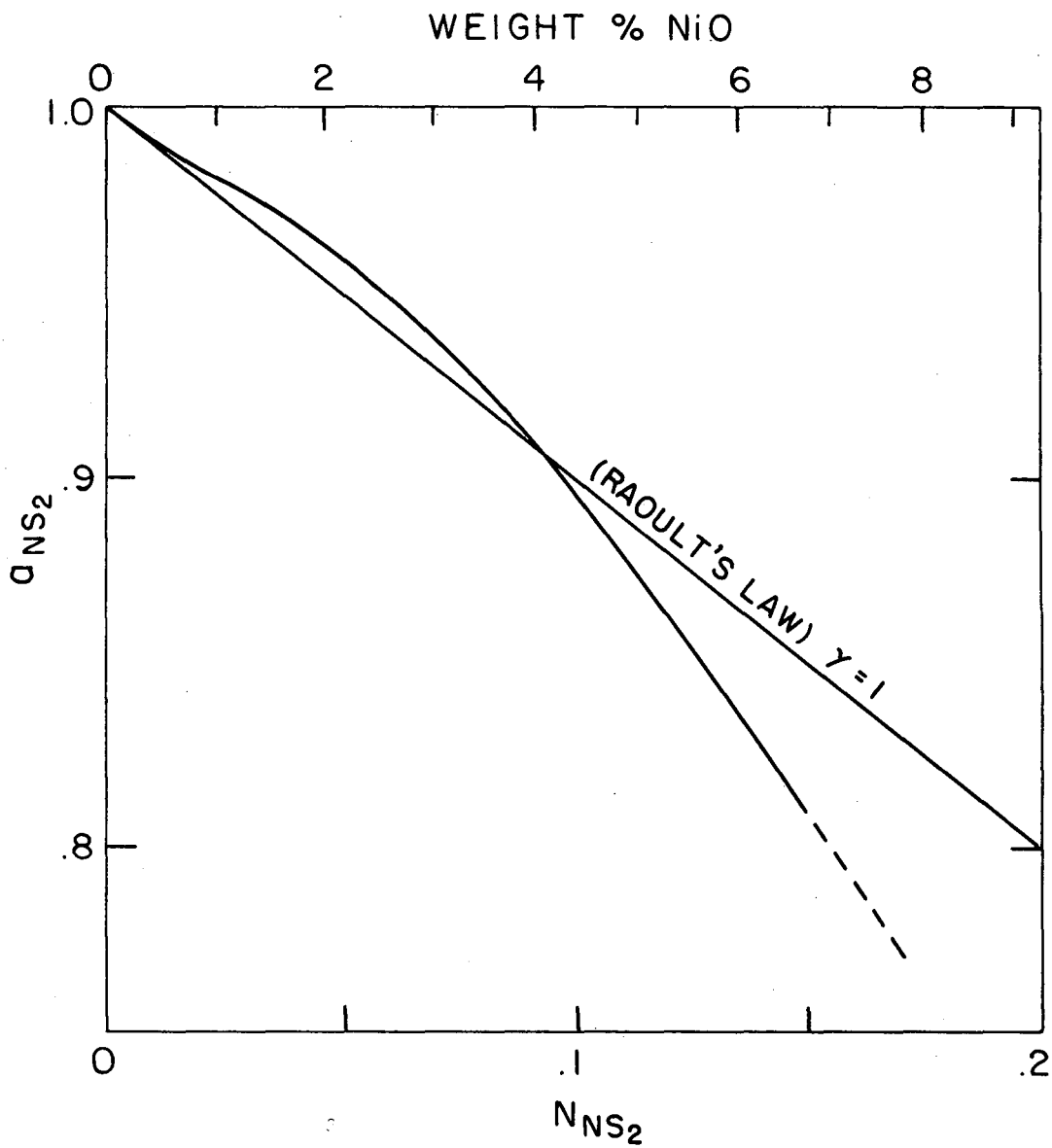
XBL 699-1423

Figure 29. Estimated isothermal dependence of the NiO activity (referred to pure supercooled liquid NiO) on composition.



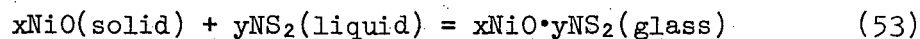
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Figure 30. Alpha function plot for determination of the activity of  $NS_2$  in the  $NiO-NS_2$  system by integration of the modified Gibbs-Duhem equation.

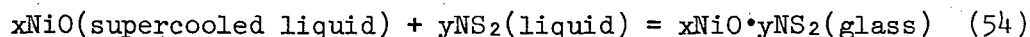


XBL 699-1425

Figure 31. Activity of  $NS_2$  (referred to the liquid standard state) calculated from integration of the modified Gibbs-Duhem equation. (One curve is drawn to represent all temperatures between  $800^\circ$  and  $1100^\circ C$ . Over this small range of concentration, the experimental uncertainty is too large to distinguish precisely the temperature variation on activity of  $NS_2$ ). The estimated uncertainty in these data is 2%.

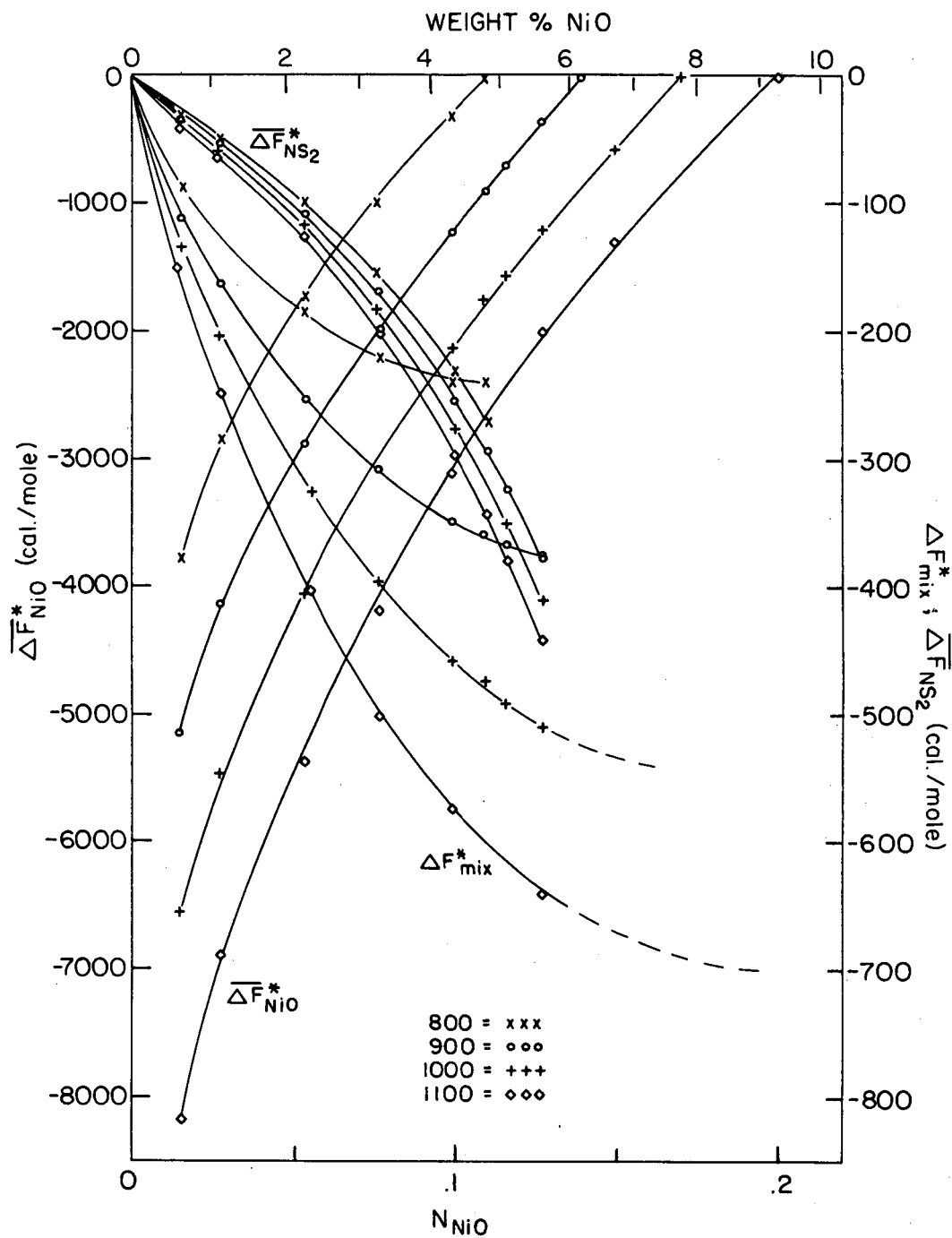


are plotted in Fig. 32 and listed in Appendix C. The partial molar free energy of NiO ( $\overline{\Delta F}_{\text{NiO}}^{**}$ ) and the free energy of mixing ( $\Delta F_{\text{mix}}^{**}$ ) for the reaction



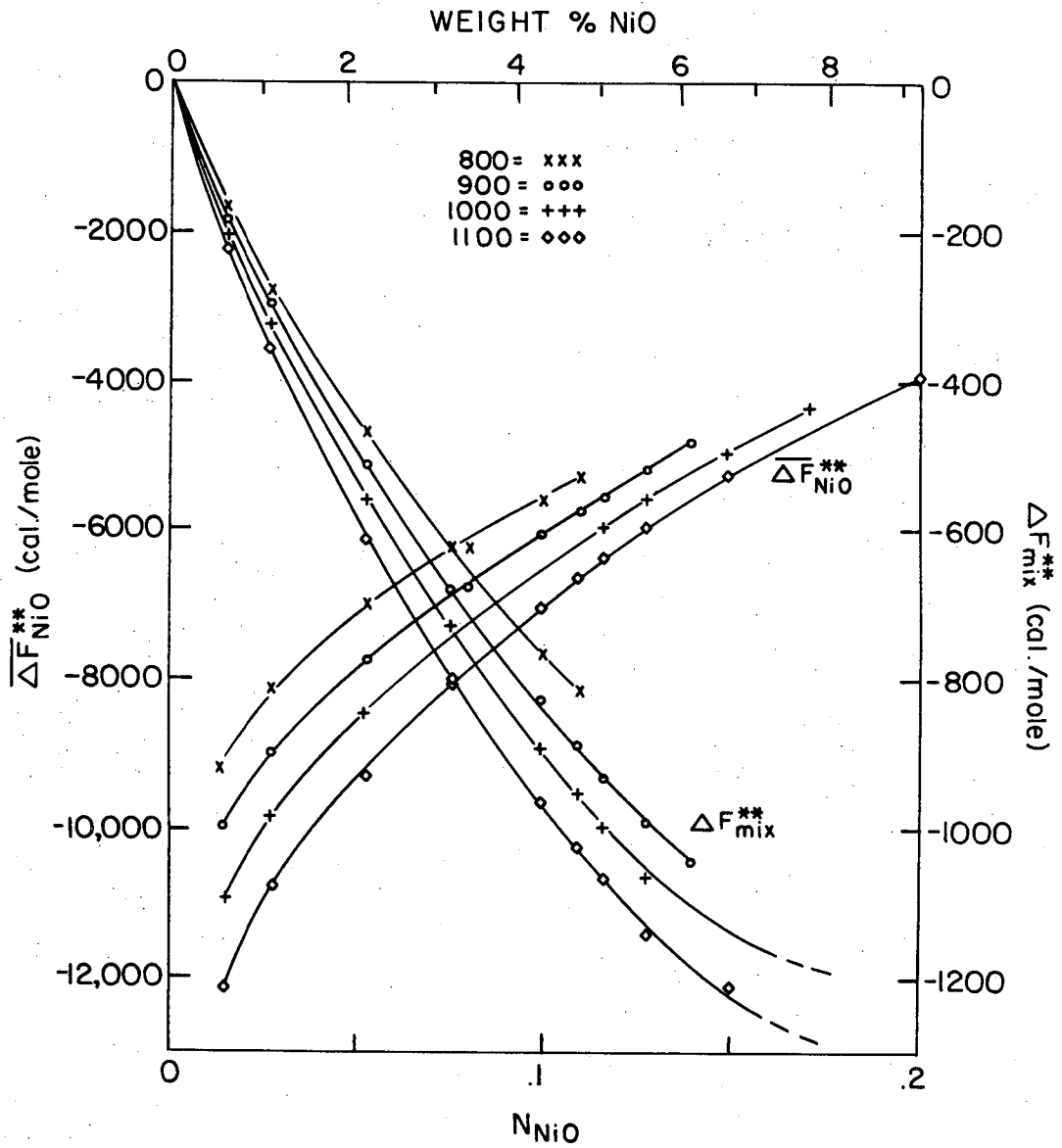
are plotted in Fig. 33 and also listed in Appendix C. The partial molar entropies ( $\overline{\Delta S}_{\text{NiO}}^*$ ,  $\overline{\Delta S}_{\text{NiO}}^{**}$ ,  $\overline{\Delta S}_{\text{NS}_2}$ ) and the integral entropies of mixing ( $\Delta S_{\text{mix}}^*$ ,  $\Delta S_{\text{mix}}^{**}$ ); partial molar enthalpies ( $\overline{\Delta H}_{\text{NiO}}^*$ ,  $\overline{\Delta H}_{\text{NiO}}^{**}$ ,  $\overline{\Delta H}_{\text{NS}_2}$ ) and the enthalpies of mixing ( $\Delta H_{\text{mix}}^*$ ,  $\Delta H_{\text{mix}}^{**}$ ) for reactions (53) and (54) are given in Figs. 34 and 35 respectively.

The NS<sub>2</sub> liquidus was determined by the intersection of the experimentally calculated  $a_{\text{NS}_2}$  vs temperature plots, with the plot of the activity of pure solid NS<sub>2</sub> relative to the pure liquid standard state. This graph is presented in Fig. 36. The solubility data for NiO was determined either by intersection of the  $a_{\text{NiO}}^*$  curves with  $a_{\text{NiO}}^* = 1$  (Fig. 27) or by intersection of  $\epsilon_{\text{cell}}$  vs temperature with  $\epsilon_{\text{cell}} = 0$ . These liquidus data allow one to construct a tentative phase diagram for the NiO-rich end of the pseudobinary NiO-NS<sub>2</sub> system. This is given in Fig. 37.



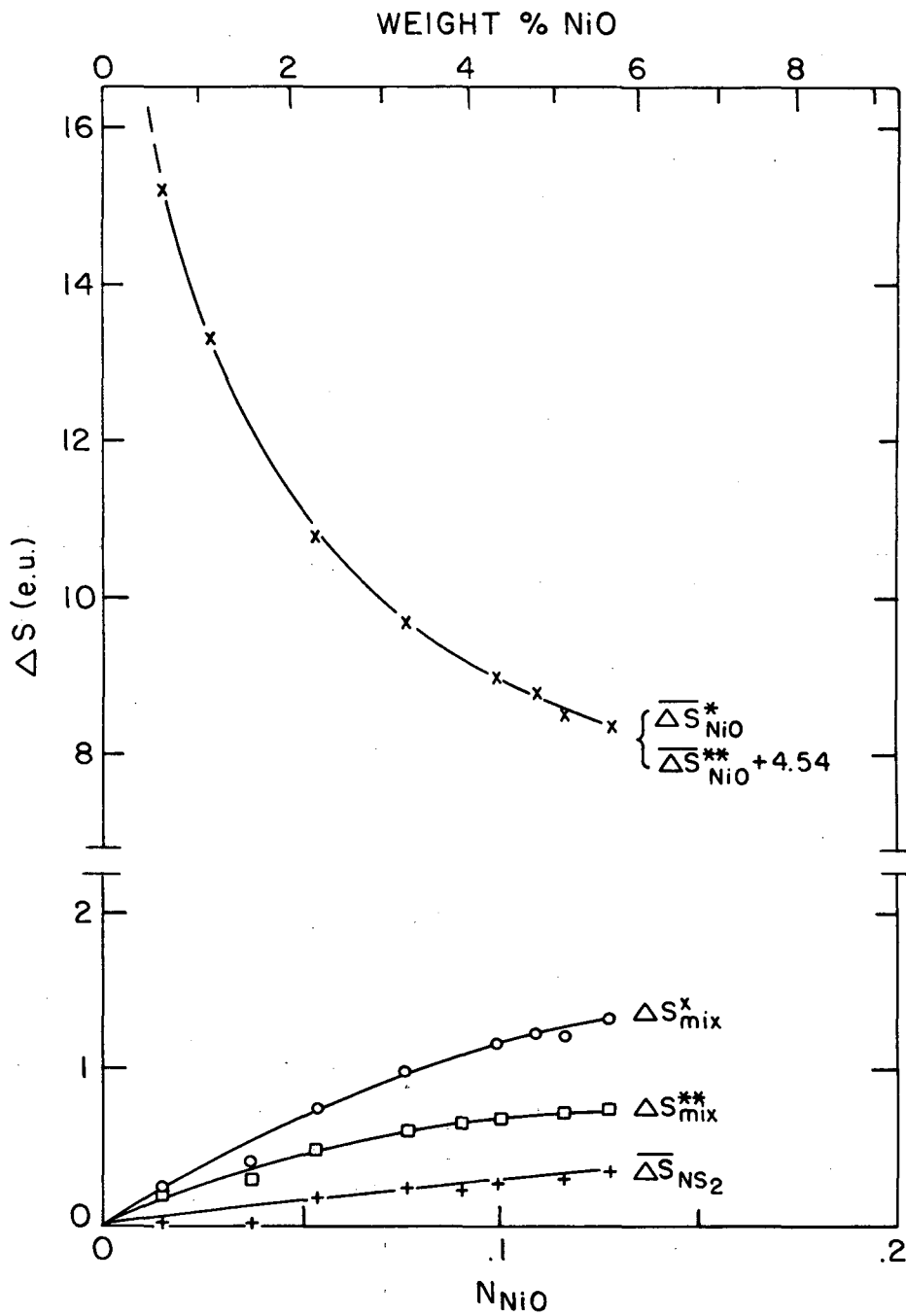
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Figure 32. Free energy plots for NiO (referred to the pure solid standard state); NS<sub>2</sub> (referred to the pure liquid).



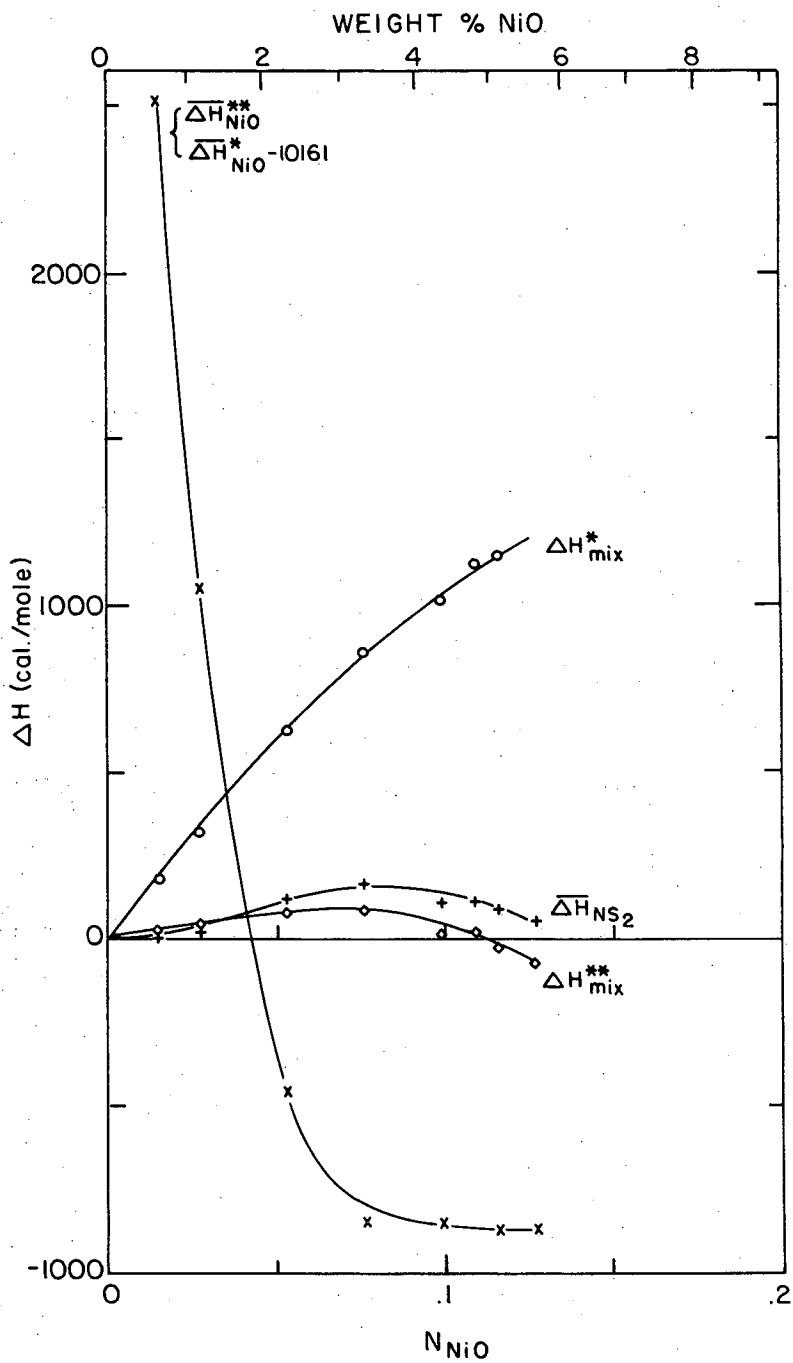
XBL 699-1429

Figure 33. Estimated free energy plots for NiO (referred to the pure supercooled liquid standard state).



XBL 699-1427

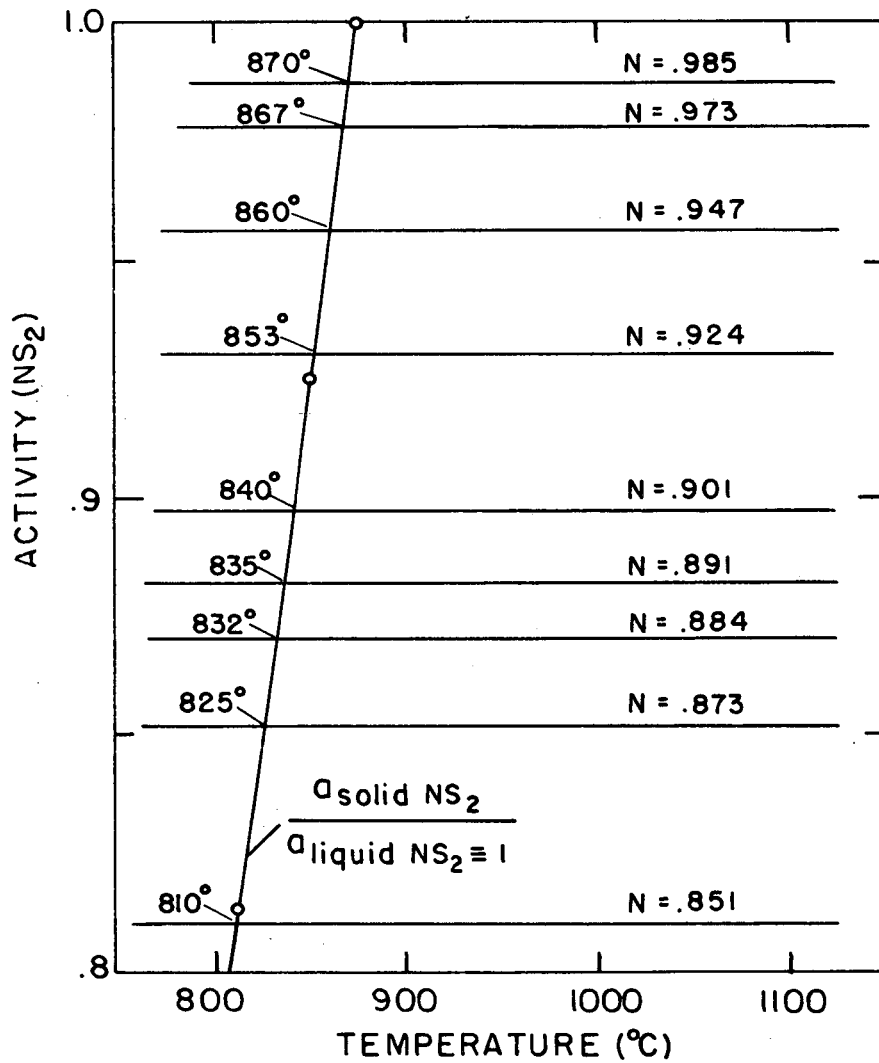
Figure 34. Entropy plots for NiO and  $NS_2$ .



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Figure 35. Enthalpy plots for NiO and NS<sub>2</sub>.





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Figure 36. Isocompositional activity plots for NS<sub>2</sub> for determination of the NS<sub>2</sub> liquidus in the NiO-NS<sub>2</sub> system.

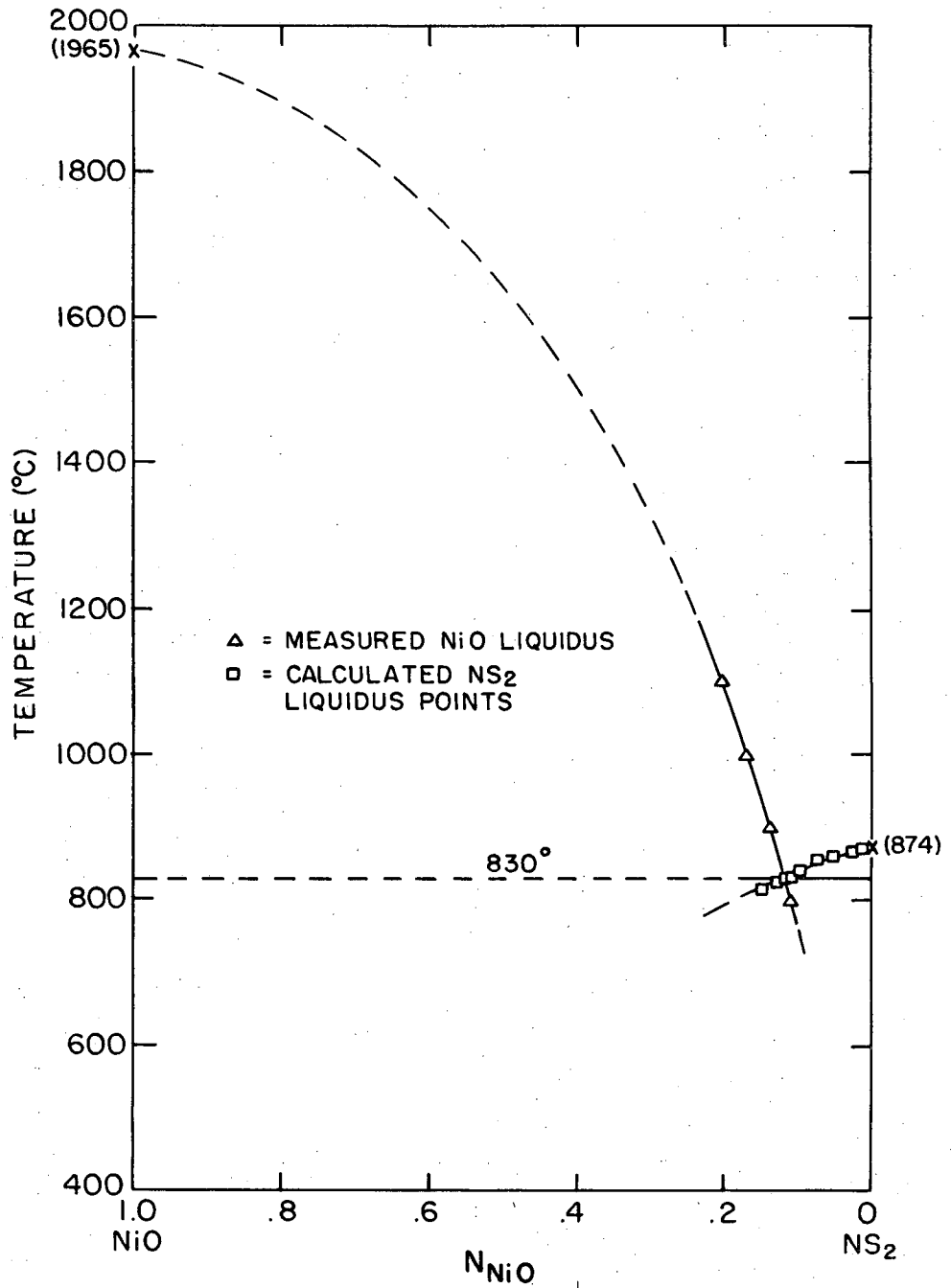


Figure 37. Proposed phase diagram for the NiO-NS<sub>2</sub> system.

## V. DISCUSSION OF RESULTS

### A. The System FeO-NS<sub>2</sub>

#### 1. Phase Relations

A plot of the experimentally determined liquiduses for the precipitation of crystalline FeO and NS<sub>2</sub> is given in Fig. 13, superimposed on the published binary diagram of Ibrahim and Carter.<sup>11</sup> It is seen that there is good agreement between their FeO liquidus, determined by quench methods, and the liquidus found in this study by intersection of the measured activity curves with the activity line for pure solid FeO. The NS<sub>2</sub> liquidus calculated from this study does not agree at all with that of Ibrahim and Carter;<sup>11</sup> the calculated curve being much lower than the published one. In fact, the freezing point depression of the NS<sub>2</sub> by the addition of FeO is so severe that extension of the FeO liquidus to a point of intersection (assuming a simple binary eutectic diagram) would result in a eutectic at an unreasonably low temperature. A freezing point depression of the magnitude proposed by Ibrahim and Carter<sup>11</sup> could result only if the FeO in solution exhibited a positive deviation from ideality.

There is little question as to the reality of the negative deviation indicated by these emf experiments, since this phenomenon has been qualitatively demonstrated by two other independent methods of investigation:

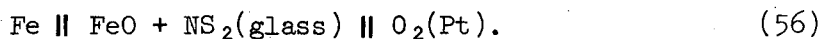
(1) The melting of FeO glasses containing 26.74 weight % FeO ( $N_{\text{FeO}} = .491$ ) and 29.80 weight % FeO ( $N_{\text{FeO}} = .528$ ) was at one time attempted in an atmosphere of CO/CO<sub>2</sub> at a ratio of 10:1 at 1000°C. The results indicated that the 26.74% glass melted satisfactorily, but there was

definite evidence of decomposition of the 29.80% glass. Calculation of the maximum activity of FeO which is stable according to the reaction



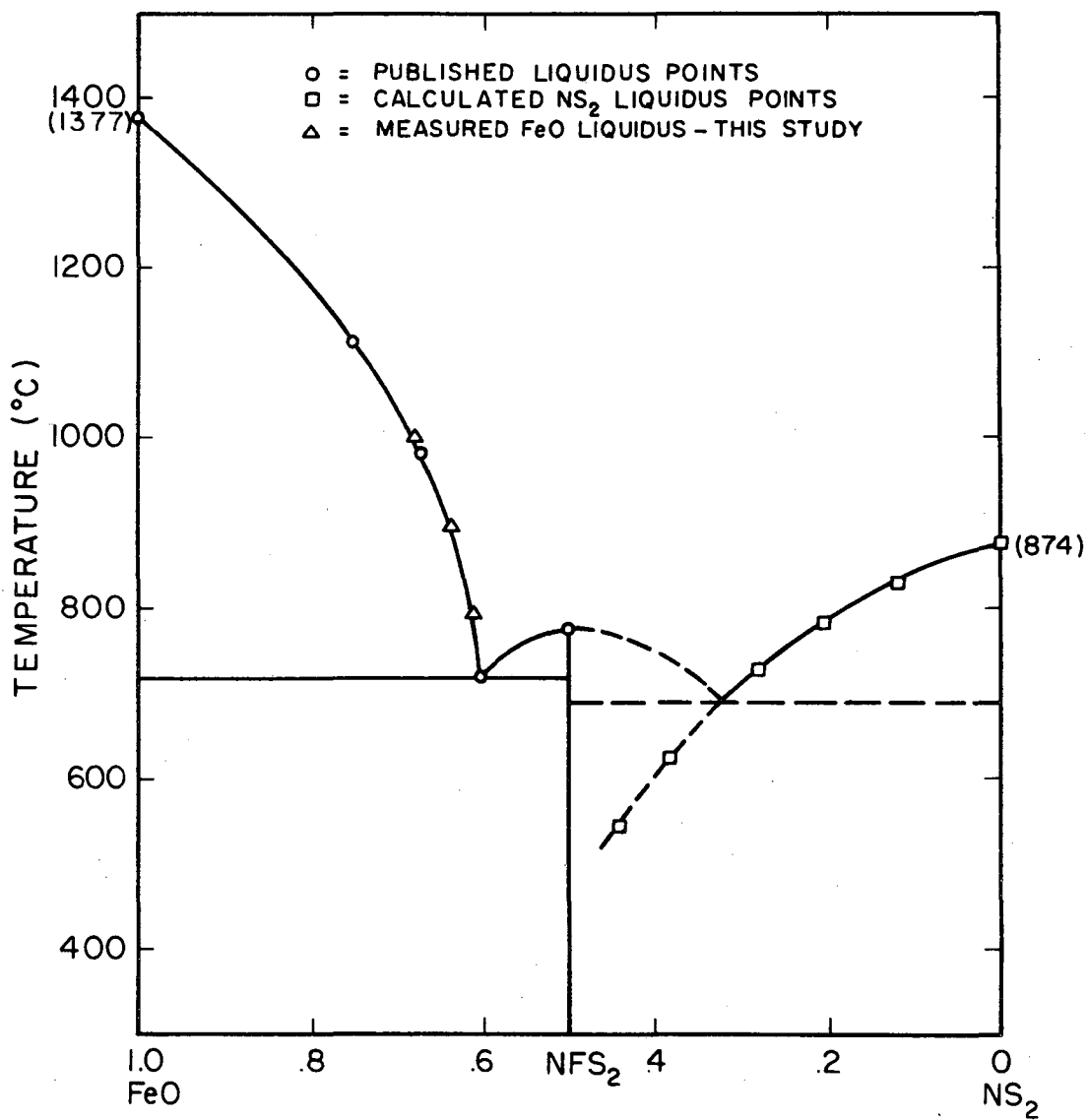
at a 10:1 CO/CO<sub>2</sub> ratio at 1000°C yielded a value of  $a_{\text{FeO}} = 0.233$  (see Appendix E). The successful formation of the 26.74% glass is indication that the activity of FeO in this composition is very near the maximum value of 0.233. This is in accordance with the overall data which has been obtained by emf measurements.

(2) Guiot<sup>23</sup> has also investigated the activities of FeO in NS<sub>2</sub> glass by use of the formation cell



Although the results of this independent experiment are not quantitative, due to the unknown magnitude of the electronic transference in the glass, they compare qualitatively with these data, indicating an even stronger negative deviation than this study indicates. The possibility of any positive deviations of FeO activity from ideality is then ruled out by the coincidence of the results of these three independent observations.

Carter and Ibrahim's<sup>11</sup> NS<sub>2</sub> liquidus is not thermodynamically possible. However, the experimental data of both Carter and Ibrahim<sup>11</sup> and this study can be resolved by reconstruction of the binary phase diagram as presented in Fig. 38. This may be done by postulating the existence of a previously unreported compound of the formula FeNa<sub>2</sub>Si<sub>2</sub>O<sub>6</sub> (alternately



XBL 699-1409

Figure 38. Proposed phase diagram of the FeO-NS<sub>2</sub> system incorporating the postulated compound NFS<sub>2</sub>.

$\text{FeO}\cdot\text{Na}_2\text{O}\cdot 2\text{SiO}_2$ ), and concurrently suggesting that the experimental data of Ibrahim and Carter is too incomplete to warrant the construction of the binary diagram  $\text{FeO}-\text{NS}_2$  as they have presented it.

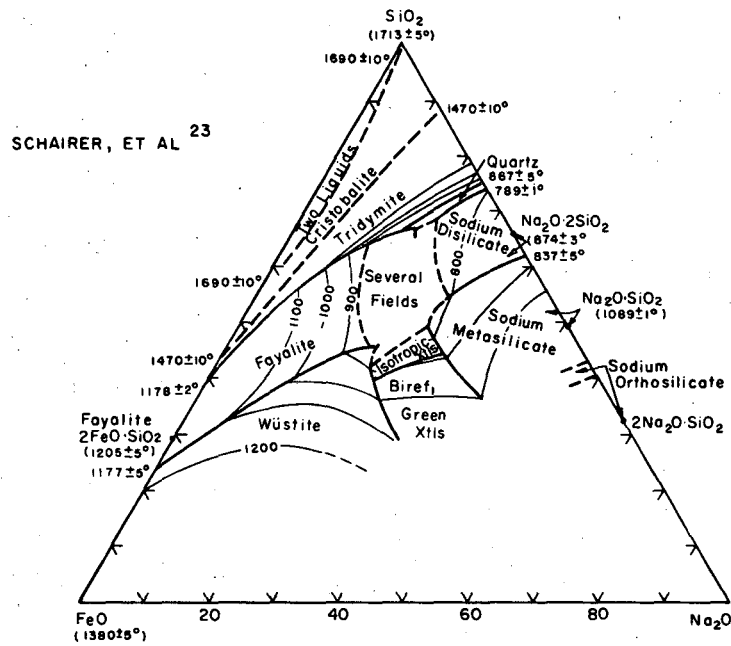
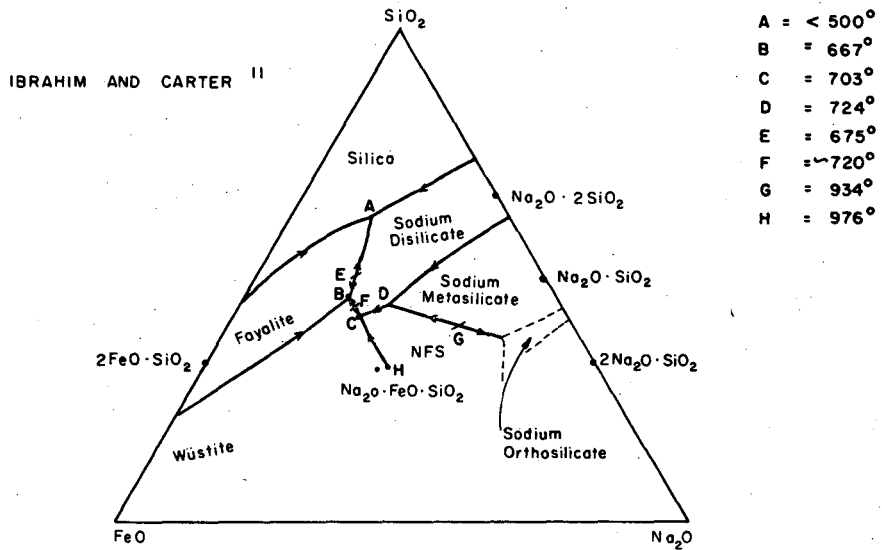
They do not exclude this possibility in the text of their publication by saying on page 149 "... (Melts along the join  $2\text{FeO}\cdot\text{SiO}_2-\text{Na}_2\text{O}\cdot 2\text{SiO}_2$ ) did not crystallize easily, and certain of them required three or four days' heat treatment before the initial crystals appeared..." On page 152 they report, "... Greatest difficulty was experienced in crystallizing compositions (along the  $2\text{FeO}\cdot\text{SiO}_2-\text{Na}_2\text{O}\cdot 2\text{SiO}_2$  join) between 50 and 60 (weight) percent  $\text{NS}_2$ . (These compositions are slightly richer in iron than the postulated compound  $\text{FeO}\cdot\text{Na}_2\text{O}\cdot 2\text{SiO}_2$ ). Thus only one or two crystals were seen after heating the 47/53 melt for one week at  $610^\circ\text{C}$ . The same specimen heated for 125 hours at  $590^\circ\text{C}$  developed (a fine structure) resembling a eutectic, although the (matrix) was glassy..." Further, on page 155 they state "... Melts (along the join  $\text{FeO}\cdot\text{SiO}_2-\text{Na}_2\text{O}\cdot\text{SiO}_2$ ) containing 35 and more (weight) percent  $\text{NS}_2$  were completely glassy after furnace cooling..." The postulated compound composition occurs at the 50/50 point along this join.

Although they present one experimental point for the liquidus at 50 mole percent  $\text{FeO}$  in the  $\text{FeO}-\text{NS}_2$  binary, no other experimental points for definition of this curve are given. If one accepts the validity of this point on the assumption that they may have been incorrect in discerning the nature of the crystalline products resulting, it becomes easy to incorporate all their observations into the modified diagram in Fig. 14. It is not possible by these experiments to ascertain the liquidus between the 50 mole percent composition and the calculated  $\text{NS}_2$

liquidus. A possible liquidus has been drawn in with dashed lines to illustrate the qualitative shape of the diagram. Schairer, Yoder and Keene<sup>24</sup> have also presented a preliminary ternary diagram for the system  $\text{Na}_2\text{O}-\text{FeO}-\text{SiO}_2$ , which differs from that of Ibrahim and Carter.<sup>11</sup> These diagrams are presented in Fig. 39. Schairer, et al.<sup>24</sup> have broken up the primary phase field of  $\text{NS}_2$  into two divisions with a speculative eutectic (indicated by the dashed line) at approximately 16 weight percent FeO ( $N_{\text{FeO}}=0.324$ ) on the FeO- $\text{NS}_2$  join. Assuming the eutectic as this composition, the results of this study indicate the eutectic temperature to be  $\sim 685^\circ\text{C}$ . Schairer et al.<sup>24</sup> show another eutectic at about 35 weight percent FeO ( $N_{\text{FeO}}=0.59$ ) which corresponds to that of Ibrahim and Carter.<sup>11</sup> Between these points, they have suggested "several fields."

They have, however, indicated the  $800^\circ\text{C}$  isotherm intersecting the FeO- $\text{NS}_2$  join at approximately 14 weight percent FeO ( $N_{\text{FeO}}=0.30$ ). This is not in agreement with either Ibrahim and Carter<sup>11</sup> (who establish the  $800^\circ$  liquidus point at 23 weight percent FeO), or this study (which fixes the  $800^\circ$   $\text{NS}_2$  liquidus point at approximately 8 weight percent).

Alternatively, a liquidus of the shape indicated in Fig. 14 may be explained by assuming that the FeO- $\text{NS}_2$  system is not a true binary (as stated by Ibrahim and Carter<sup>11</sup>). This would require that the join FeO- $\text{NS}_2$  extend across the primary phase field of some other compound (not NFS) in the FeO- $\text{Na}_2\text{O}-\text{SiO}_2$  ternary system. To do this, either the boundaries of the primary phase fields shown in the diagrams of Schairer et al.<sup>24</sup> and Ibrahim and Carter<sup>11</sup> must be reconstructed; or one must propose the existence of some compound other than NFS, whose primary phase field will encompass the region between the two eutectics in Fig. 14. Likely



XBL 699-1410

Figure 39. Two ternary diagrams for the FeO-Na<sub>2</sub>O-SiO<sub>2</sub> system taken from published literature.



candidates are  $\text{NF}_4$ ,  $\text{N}_2\text{FS}_3$ ,  $\text{NFS}_3$  and/or  $\text{NF}_2\text{S}_3$ . None of these compounds have been identified, but would be found within the region designated "several fields" by Schairer et al.<sup>24</sup> Confirmation of this will have to await direct observation of these compounds.

The results of this investigation indicate the value and utility of thermodynamic studies in providing information about phase diagrams. It is a tool which can be used to particular advantage in glass systems which tend to supercool readily and crystallize slowly, thus circumventing the difficulties inherent in quenching techniques.

## 2. Structure

Any interpretation of the structure of molten silicates based solely upon thermodynamic studies must be made with great reservation. Bockris<sup>25</sup> has pointed out that thermodynamic properties do not give direct information on problems of structure, but rather act as an important check on structural theories derived from other data, such as electrical conductivity, viscosity, etc. Flood and Knapp<sup>26</sup> have developed models for the structure of borosilicate melts containing a single network modifying cation, based solely upon the thermodynamic properties of the pure components involved and the shapes of the liquidus curves. Such models are of limited applicability, and are not particularly definitive even for selected systems. In general, however, large negative deviations from ideality may be interpreted as a tendency toward complex ion formation by the individual components, and positive deviations indicate tendencies toward exsolution of the particular component. The extremely negative deviations found in the  $\text{FeO-NS}_2$  system are then taken as evidence that  $\text{FeO}$  is readily incorporated into the structure of the solvent  $\text{NS}_2$ .

Additional evidence of structural changes in the glass may be seen from the variation of the entropy of mixing and the partial molar entropy of solution of the components. This study indicates that the  $\overline{\Delta S}_{\text{FeO}}$  tends to a minimum at approximately  $N_{\text{FeO}}=0.3$  and goes through a maximum at  $N_{\text{FeO}}=0.5$ . This is taken as a qualitative indication of a disordering process with respect to the distribution of FeO in the atomic lattice between  $N_{\text{FeO}}=0.3$  and  $N_{\text{FeO}}=0.5$ . The partial molar entropy of  $\text{NS}_2$  falls to zero at  $N_{\text{FeO}}=0.5$ . Since this is the composition of the proposed compound  $\text{FeO}\cdot\text{Na}_2\text{O}\cdot 2\text{SiO}_2$ , this might be interpreted as a partial ordering of the soda-silica lattice as would be necessary for nucleation of a crystalline phase. Richardson<sup>27</sup> has pointed out that liquid compounds are probably structurally similar to the solid phase, except that they are lacking in the long range order of the crystalline structure.

## B. The System CoO-NS<sub>2</sub>

### 1. Phase Relations

From the experimentally determined liquidus lines and the known melting points of CoO and  $\text{NS}_2$ , a simple eutectic phase diagram has been constructed in Fig. 27. There is no known published information on phase relations in either this pseudo-binary system or in the ternary system  $\text{CoO-Na}_2\text{O-SiO}_2$ . The solubility limits of CoO in  $\text{NS}_2$  are, however, in qualitative agreement with interface compositions for CoO- $\text{NS}_2$  diffusion couples.<sup>8</sup> Because of the general chemical similarity between  $\text{Fe}^{2+}$  and  $\text{Co}^{2+}$  in silicate systems Co-silicates analagous to the postulated Fe-silicates may also exist in the system  $\text{CoO-Na}_2\text{O-SiO}_2$ . The displacement of the CoO and FeO liquiduses as functions of composition and

temperature indicate, however, that analagous compounds may have differing stabilities at high temperatures. For example, Figs. 14 and 27 suggest that  $\text{Na}_2\text{O}\cdot\text{FeO}\cdot 2\text{SiO}_2$  may melt congruently, whereas  $\text{Na}_2\text{O}\cdot\text{CoO}\cdot 2\text{SiO}_2$  (if it exists) may melt incongruently. This is speculation, and confirmation rests with further investigation of the phase relations in this system.

## 2. Structure

It may be seen from comparison of Figs. 5 and 19 that CoO exhibits strong negative deviations from ideality in the same manner as FeO in  $\text{NS}_2$  solvent. Figures 9 and 23 further indicate practically parallel variation of the partial molar entropy of the metal oxide with composition up to the solubility limit of CoO. This suggests that CoO and FeO are isostructural on an atomic scale. The negative slope of the partial molar entropy curve of CoO and FeO is the result of a reduction in the available sites for distribution of the CoO and FeO within the  $\text{NS}_2$  matrix as the oxides are added. As original sites are filled, however, the addition of oxygen increases the O/Si ratio above the initial 2.5, thus breaking down the atomic network structure by increasing the number of unshared oxygens. This structural disruption thus provides additional sites for incorporation of the metal oxide cations. The result of these two opposing factors--the filling of the matrix with oxide cations and the structural randomization resulting from an increasing O/Si ratio--is a minimum in each partial molar entropy curve for CoO and FeO.

C. NiO-NS<sub>2</sub>

1. Phase Relations

As with CoO, there are no reported studies of phase relations in the systems NiO-NS<sub>2</sub> or NiO-Na<sub>2</sub>O-SiO<sub>2</sub>. The solubility data determined here enables one to construct a simple eutectic diagram as shown in Fig. 37. The NiO liquidus has been extended to the melting point of pure NiO, since no compounds other than the pure end members have been identified in this system. The eutectic determined from intersection of the liquidus lines occurs at  $N_{NiO} = 0.12$  at 830°C.

2. Structure

Due to the estimation of the heat of fusion of NiO at temperatures far below its melting point, it is not possible to obtain quantitative values of  $a_{NiO}^{**}$  from Eq. (34). The curves presented in Fig. 31 are therefore semiquantitative, based upon the assumption that the heat capacity of the solid NiO and the supercooled liquid NiO are equal--that is, the heat of fusion is constant at all temperatures. At temperatures far below the normal fusion temperature, the assumption may not be valid. For this reason, one cannot say with certainty that the  $a_{NiO}^{**}$  curves of Fig. 31 really extend above the Raoult's Law line, thus indicating a positive deviation from ideality. No interpretation of structure based on such a deviation can be made. Qualitatively, NiO appears to show less negative deviation than either CoO or FeO in NS<sub>2</sub> solution, indicating that it is not as readily incorporated into the glass structure, and probably has less tendency for form complex ionic species with the solvent than do either CoO or FeO. Further structural interpretation requires other non-thermodynamic data.

## VI. SUMMARY

The solid electrolyte galvanic cell method has been adapted to the measurement of thermodynamic properties of FeO, CoO and NiO in sodium disilicate glass solutions over the temperature interval 700°-1100°C. Activities of these oxides (relative to the pure solid oxides) have been determined as a function of composition and temperature, and thus provide a more substantial basis for predicting and interpreting chemical reactions between these glasses and metals or other oxides. It may now be possible, for example, to relate the degree of wetting and chemical bond formation to the glass composition in a more general way than before these studies were carried out. Similarly, these data are fundamental in defining conditions under which metallic dendrites will form in glass-metal systems.

The oxides of iron, cobalt, and nickel all show negative deviations from Raoult's Law with iron being the most negative, and nickel the least. These are interpreted to mean that the oxides are incorporated readily into the glass structure, possibly forming complex ionic species with the silicate solvent. The partial molar entropies of solution for these oxides indicate that definite structural changes in the glass occur as the oxides are added--changes which manifest themselves in an increase in the number of atomic sites available to accommodate additional network modifying ions. This is in agreement with the Zachariason concept of glass structure based on O/Si ratios.

Calculation of a partial phase diagram for the pseudobinary system FeO-NS<sub>2</sub> indicates discrepancies between this study and published studies

of the FeO-NS<sub>2</sub> system. These discrepancies are resolved by the author by postulating the existence of one or more unreported compounds in the ternary system FeO·Na<sub>2</sub>O·2SiO<sub>2</sub>. Such compounds have not been previously identified because of the difficulties involved in getting glasses of approximately that composition to crystallize within reasonable periods of time. It has been further speculated on structural grounds that analagous compounds in the system CoO·Na<sub>2</sub>O·2SiO<sub>2</sub> may also exist; but if so, probably have stabilities different from their FeO counterparts. Simple eutectic phase diagram for the CoO-NS<sub>2</sub> and NiO-NS<sub>2</sub> systems have been proposed, based upon limited data available from this study.

ACKNOWLEDGMENTS

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Appendix A: Tabulation of thermodynamic data for the FeO-NS<sub>2</sub> system

$N_{\text{FeO}}$	$a_{\text{FeO}}^*$	$\ln a_{\text{FeO}}^*$	$a_{\text{FeO}}^{**}$	$\ln a_{\text{FeO}}^{**}$	$N_{\text{NS}_2}$	$a_{\text{NS}_2}$	$\ln a_{\text{NS}_2}$	$\overline{\Delta F}_{\text{FeO}}^{**}$	$\overline{\Delta F}_{\text{FeO}}^*$	$\overline{\Delta F}_{\text{NS}_2}$	$\Delta F_{\text{mix}}^*$	$\Delta F_{\text{mix}}^{**}$	$\gamma_{\text{FeO}}^{**}$
Temperature 800°C													
.121	.021	-3.863	.006	-5.093	.879	.866	-.1439	-10858	-8236	-307	-1266	-1583	.050
.127	.023	-3.772	.007	-5.002	.873	.858	-.1532	-10664	-8042	-327	-1307	-1639	.055
.208	.045	-3.101	.013	-4.331	.782	.747	-.2917	-9233	-6611	-622	-1808	-2413	.063
.284	.075	-2.590	.022	-3.820	.716	.619	-.4797	-8144	-5522	-1023	-2301	-3045	.077
.336	.115	-2.163	.034	-3.393	.664	.518	-.6578	-7234	-4612	-1402	-2481	-3362	.101
.388	.180	-1.715	.053	-2.945	.612	.405	-.9039	-6278	-3656	-1927	-2598	-3616	.137
.443	.280	-1.273	.082	-2.503	.557	.295	-1.2208	-5336	-2714	-2602	-2652	-3814	.185
.491	.415	-.879	.121	-2.109	.509	.207	-1.5750	-4496	-1874	-3358	-2629	-3917	.246
.528	.555	-.589	.162	-1.819	.472	.153	-1.8773	-3878	-1256	-4002	-2552	-3979	.307
.568	.765	-.268	.223	-1.498	.432	.105	-2.2538	-3193	-571	-4805	-2400	-3890	.392
.603	1.000	0	.292	-1.230	.397	.070	-2.6593	-2622	0	-5670	-2251	-3832	.484
Temperature 900°C													
.121	.020	-3.912	.008	-4.841	.879	.867	-.1427	-11283	-9118	-333	-1396	-1658	.066
.127	.022	-3.817	.009	-4.746	.873	.859	-.1520	-11061	-8896	-394	-1439	-1716	.071
.208	.044	-3.124	.017	-4.053	.792	.748	-.2904	-9446	-7281	-677	-2051	-2501	.082
.284	.075	-2.590	.030	-3.519	.716	.625	-.4700	-8202	-6037	-1095	-2499	-3114	.106
.336	.108	-2.226	.043	-3.155	.664	.530	-.6349	-7353	-5188	-1480	-2726	-3453	.128
.388	.160	-1.833	.063	-2.762	.612	.428	-.8486	-6437	-4272	-1978	-2868	-3708	.162
.443	.235	-1.448	.093	-2.377	.550	.324	-1.1270	-5540	-3375	-2627	-2958	-3899	.210
.491	.325	-1.124	.128	-2.053	.509	.240	-1.4271	-4785	-2620	-3326	-2979	-4042	.261
.528	.427	-.851	.167	-1.780	.472	.178	-1.7260	-4148	-1983	-4023	-2946	-4089	.316
.568	.577	-.550	.228	-1.479	.432	.124	-2.0875	-3447	-1282	-4865	-2830	-4060	.401
.603	.750	-.288	.296	-1.217	.397	.085	-2.4651	-2836	-671	-5745	-2685	-3991	.491
.638	1.000	0	.395	-0.929	.362	.054	-2.9188	-2165	0	-6803	-2463	-3844	.619

Note:  $a^*$  refers to the solid st. state for FeO.  
 $a^{**}$  refers to the liquid st. state for FeO.  
 $\Delta F$  and  $\Delta H$  data are listed in terms of cal/mole.  
 $\Delta S$  data is given in cal/mole °K.

Appendix A: Tabulation of thermodynamic data for the FeO-NS<sub>2</sub> system (continued)

$N_{FeO}$	$a_{FeO}^*$	$\ln a_{FeO}^*$	$a_{FeO}^{**}$	$\ln a_{FeO}^{**}$	$N_{NS_2}$	$a_{NS_2}$	$\ln a_{NS_2}$	$\overline{\Delta F}_{FeO}^{***}$	$\overline{\Delta F}_{FeO}^{**}$	$\overline{\Delta F}_{NS_2}$	$\Delta F_{Mix}^*$	$\Delta F_{mix}^{**}$	$\gamma_{FeO}^{**}$
Temperature 1000°C													
.121	.020	-3.912	.010	-4.587	.879	.867	-.1427	-9895	-11602	-361	-1515	-1721	.083
.127	.022	-3.817	.011	-4.492	.873	.860	-.1508	-9655	-1136	-381	-1559	-1776	.087
.208	.043	-3.147	.022	-3.822	.792	.751	-.2864	-7960	-9667	-724	-2229	-2585	.106
.284	.076	-2.577	.039	-3.252	.716	.632	-.4589	-6518	-8225	-1161	-2682	-3167	.137
.336	.105	-2.254	.053	-2.929	.664	.542	-.6125	-5701	-7408	-1549	-2944	-3518	.158
.388	.144	-1.938	.073	-2.613	.612	.449	-.8007	-4902	-6609	-2025	-3141	-3804	.188
.443	.201	-1.604	.102	-2.279	.557	.349	-1.0527	-4057	-5764	-2663	-3281	-4037	.230
.491	.271	-1.306	.138	-1.981	.509	.265	-1.3280	-3303	-5010	-3359	-3332	-4170	.281
.528	.350	-1.050	.178	-1.725	.472	.204	-1.5896	-2656	-4363	-4021	-3300	-4202	.337
.568	.465	-.766	.237	-1.441	.432	.144	-1.9379	-1937	-3644	-4902	-3218	-4188	.417
.603	.585	-.536	.298	-1.211	.397	.101	-2.2926	-1356	-3063	-5799	-3120	-4149	.494
.683	1.000	0	.509	-.675	.317	.039	-3.2442	0	-1707	-8206	-2601	-3767	.745

$\overline{S}_{FeO}^*$	$\overline{S}_{FeO}^{**}$	$\overline{S}_{NS_2}$	$\overline{H}_{FeO}^*$	$\overline{H}_{FeO}^{**}$	$\overline{H}_{NS_2}$	$S_{mix}^*$	$S_{mix}^{**}$	$H_{mix}^*$	$H_{mix}^{**}$
7.40	2.86	.40	-403	-7893	+135	1.25	.70	75	-836
7.25	2.71	.40	-360	-7850	+115	1.27	.69	55	-897
5.95	1.41	.52	-305	-7795	-64	1.81	.71	74	-1672
5.65	1.11	.55	603	-6887	-448	2.00	.71	-155	-2277
5.70	1.16	.61	1519	-5971	-761	2.32	.79	8	-2512
6.00	1.46	.61	2761	-4729	-1261	2.70	.94	299	-2610
6.50	1.96	.49	4243	-3247	-2056	3.15	1.14	728	-2584
7.00	2.46	.12	5612	-1878	-3206	3.50	1.27	1126	-2554
7.15	2.61	-.05	6422	-1068	-4074	3.75	1.40	1472	-2487
7.0	2.46	.29	6948	-542	-4517	4.10	1.52	1999	-2259
6.50	1.96	1.08	6949	-541	-4417	4.35	1.61	2416	-2080

Appendix B: Tabulation of thermodynamic data for the CoO-NS<sub>2</sub> system

$N_{\text{CoO}}$	$a_{\text{CoO}}^*$	$\ln a_{\text{CoO}}^*$	$a_{\text{CoO}}^{**}$	$\ln a_{\text{CoO}}^{**}$	$N_{\text{NS}_2}$	$a_{\text{NS}_2}$	$\ln a_{\text{NS}_2}$	$\overline{\Delta F}_{\text{CoO}}^*$	$\overline{\Delta F}_{\text{CoO}}^{**}$	$\Delta F_{\text{NS}_2}$	$\Delta F_{\text{mix}}^*$	$\Delta F_{\text{mix}}^{**}$	$\gamma_{\text{CoO}}^{**}$
Temperature 800°C													
.054	.020	-3.912	.002	-6.053	.946	.945	-.0566	-8340	-12904	-121	-565	-811	.037
.120	.056	-2.882	.007	-5.023	.880	.855	-.157	-6144	-10708	-334	-1032	-1579	.058
.182	.120	-2.120	.014	-4.261	.818	.760	-.274	-4519	-9083	-584	-1300	-2131	.077
.221	.170	-1.772	.020	-3.913	.779	.690	-.371	-3778	-8342	-791	-1451	-2460	.090
.277	.255	-1.366	.030	-3.502	.723	.590	-.528	-2912	-7476	-1126	-1621	-2885	.108
.321	.345	-1.064	.041	-3.205	.679	.515	-.664	-2268	-6832	-1416	-1689	-3155	.128
.367	.485	-.724	.057	-2.865	.633	.425	-.854	-1543	-6107	-1821	-1722	-3394	.155
.407	.715	-.335	.084	-2.476	.593	.340	-1.074	-714	-5278	-2290	-1655	-3506	.206
.437	1.000	0	.118	-2.141	.563	.280	-1.273	0	-4564	-2714	-1528	-3522	.270
Temperature 900°C													
.054	.020	-3.912	.003	-5.677	.946	.945	-.0566	-9119	-13233	-131	-617	-839	.056
.120	.056	-2.882	.010	-4.647	.880	.862	-.149	-6718	-10832	-347	-1112	-1605	.083
.182	.115	-2.163	.020	-3.928	.818	.772	-.259	-5042	-9156	-604	-1411	-2160	.110
.221	.160	-1.833	.027	-3.598	.779	.710	-.342	-4389	-8503	-797	-1565	-2500	.122
.277	.240	-1.427	.041	-3.192	.723	.610	-.404	-3326	-7440	-1152	-1754	-2894	.148
.321	.325	-1.124	.056	-2.889	.679	.530	-.635	-2620	-6734	-1480	-1846	-3167	.175
.367	.440	-.821	.075	-2.586	.633	.447	-.805	-1914	-6028	-1876	-1890	-3400	.204
.407	.590	-.528	.101	-2.293	.593	.370	-.994	-1231	-5345	-2317	-1875	-3549	.248
.454	.885	-.122	.151	-1.887	.546	.270	-1.309	-284	-4398	-3051	-1795	-3663	.333
.462	1.000	0	.171	-1.765	.538	.252	-1.378	0	-4114	-3212	-1728	-3628	.370

Note: a\* refers to the solid st. state for CoO.  
a\*\* refers to the liquid st. state for CoO.  
 $\Delta F$  and  $\Delta H$  data are listed in terms of cal/mole.  
 $\Delta S$  data is given in cal/mole °K.

Appendix B: Tabulation of thermodynamic data for the CoO-NS<sub>2</sub> system (continued)

$N_{\text{CoO}}$	$a_{\text{CoO}}^*$	$\ln a_{\text{CoO}}^*$	$a_{\text{CoO}}^{**}$	$\ln a_{\text{CoO}}^{**}$	$N_{\text{NS}_2}$	$a_{\text{NS}_2}$	$\ln a_{\text{NS}_2}$	$\overline{\Delta F}_{\text{CoO}}^*$	$\overline{\Delta F}_{\text{CoO}}^{**}$	$F_{\text{NS}_2}$	$\Delta F_{\text{mix}}^*$	$\Delta F_{\text{mix}}^{**}$	$\gamma_{\text{FeO}}^{**}$
Temperature 1000°C													
.054	.020	-3.912	.005	-5.356	.946	.946	-.0555	-9893	-13545	-140	-667	-864	.093
.120	.056	-2.882	.013	-4.326	.880	.870	-.139	-7289	-10941	-352	-1184	-1623	.108
.182	.110	-2.207	.026	-3.651	.818	.780	-.248	-5582	-9234	-627	-1529	-2193	.143
.221	.155	-1.864	.037	-3.308	.779	.720	-.329	-4714	-8366	-832	-1690	-2497	.167
.277	.225	-1.492	.053	-2.936	.723	.630	-.462	-3773	-7425	-1168	-1890	-2901	.191
.321	.290	-1.238	.068	-2.682	.679	.555	-.589	-3131	-6783	-1490	-2016	-3189	.212
.367	.390	-.942	.092	-2.386	.633	.470	-.755	-2382	-6034	-1909	-2083	-3423	.251
.407	.505	-.683	.119	-2.127	.593	.396	-.926	-1727	-5379	-2342	-2092	-3578	.292
.454	.730	-.315	.172	-1.759	.546	.310	-1.171	-797	-4449	-2961	-1979	-3637	.379
.488	1.000	0	.236	-1.444	.512	.235	-1.448	0	-3652	-3662	-1875	-3657	.484
Temperature 1100°C													
.054	.020	-3.912	.006	-5.084	.946	.946	-.0555	-10673	-13870	-151	-720	-892	.111
.120	.056	-2.882	.017	-3.054	.880	.880	-.128	-7863	-11063	-349	-1251	-1634	.142
.182	.107	-2.235	.033	-3.407	.818	.790	-.236	-6097	-9294	-644	-1636	-2218	.181
.221	.147	-1.917	.046	-3.089	.779	.730	-.315	-5230	-8427	-859	-1825	-2532	.208
.277	.210	-1.561	.065	-2.733	.723	.645	-.439	-4259	-7456	-1198	-2045	-2932	.235
.321	.270	-1.309	.084	-2.481	.679	.573	-.557	-3571	-6768	-1520	-2178	-3205	.262
.367	.355	-1.036	.110	-2.208	.633	.400	-.713	-2826	-6023	-1945	-2263	-3442	.300
.407	.460	-.777	.143	-1.949	.593	.425	-.856	-2120	-5317	-2335	-2247	-3549	.351
.454	.625	-.470	.194	-1.642	.546	.340	-1.079	-1282	-4479	-2944	-2189	-3640	.427
.517	1.000	0	.310	-1.172	.483	.215	-1.537	0	-3197	-4193	-2025	-3678	.600

Appendix B: Tabulation of thermodynamic data for the CoO-NS<sub>2</sub> system (continued)

$N_{\text{CoO}}$	$N_{\text{NS}_2}$	$\overline{\Delta S^*}_{\text{CoO}}$	$\overline{\Delta S^{**}}_{\text{CoO}}$	$\overline{\Delta S}_{\text{NS}_2}$	$\overline{\Delta H^*}_{\text{CoO}}$	$\overline{\Delta H^{**}}_{\text{CoO}}$	$\overline{\Delta H}_{\text{NS}_2}$	$\Delta S^*_{\text{mix}}$	$\Delta S^{**}_{\text{mix}}$	$\Delta H^*_{\text{mix}}$	$\Delta H^{**}_{\text{mix}}$
.054	.946	7.83	+3.31	.05	95	-9339	- 75	.40	.23	-144	- 575
.120	.880	5.80	+1.26	.14	90	-9344	- 174	.82	.27	-142	-1274
.182	.818	4.72	+ .18	.32	463	-8971	- 224	1.12	.29	- 99	-1816
.221	.779	4.33	- .21	.41	768	-8666	- 318	1.28	.27	- 68	-2163
.277	.723	4.05	- .49	.52	1386	-8066	- 525	1.50	.24	+ 7	-2614
.321	.679	4.05	- .49	.53	2056	-7378	- 828	1.66	.20	97	-2931
.367	.633	4.18	- .36	.48	2848	-6586	-1301	1.81	.17	233	-3241
.407	.593	4.40	- .14	.36	3689	-5745	-1881	1.92	.16	381	-3454
.437	.563	4.70	+ .16	.10	5157	-4277	-2796	2.00	.13	573	-3443

Appendix C: Tabulation of thermodynamic data for the NiO-NS<sub>2</sub> system

$N_{NiO}$	$a_{NiO}^*$	$\ln a_{NiO}^*$	$a_{NiO}^{**}$	$\ln a_{NiO}^{**}$	$N_{NS_2}$	$a_{NS_2}$	$\ln a_{NS_2}$	$\overline{\Delta F}_{NiO}^{**}$	$\overline{\Delta F}_{NiO}^{***}$	$\overline{\Delta F}_{NS_2}$	$\Delta F_{mix}^{**}$	$\Delta F_{mix}^{***}$	$\gamma_{NiO}^{**}$
Temperature 800°C													
.015	.170	-1.772	.015	-4.255	.985	.985	-0.0111	-3778	-9072	- 32	- 88	-168	1.000
.027	.265	-1.328	.023	-3.811	.977	.977	-0.0233	-2831	-8125	- 50	-125	-268	.852
.053	.445	-0.810	.039	-3.293	.955	.955	-0.0460	-1727	-7021	- 98	-184	-465	.736
.076	.630	-0.462	.055	-2.945	.930	.930	-0.0726	- 984	-6278	-155	-218	-620	.724
.099	.860	-0.151	.075	-2.634	.897	.897	-0.1087	- 322	-5616	-232	-240	-765	.758
.109	1.000	0	.087	-2.483	.882	.882	-0.1256	0	-5294	-268	-239	-816	.798
Temperature 900°C													
.015	.110	-2.207	.014	-4.282	.985	.985	-0.0151	-5145	-9981	- 35	-112	-184	.933
.027	.170	-1.772	.021	-3.847	.973	.977	-0.0233	-4131	-8967	- 54	-164	-295	.778
.053	.290	-1.238	.036	-3.313	.947	.955	-0.0460	-2886	-7722	-107	-254	-511	.679
.076	.422	-0.863	.053	-2.938	.924	.930	-0.0726	-2011	-6847	-169	-309	-677	.697
.099	.590	-0.528	.074	-2.603	.901	.897	-0.1087	-1231	-6067	-253	-350	-829	.747
.109	.680	-0.386	.085	-2.461	.891	.882	-0.1256	- 900	-5736	-293	-359	-886	.780
.116	.740	-0.301	.092	-2.376	.884	.870	-0.1393	- 701	-5537	-325	-368	-930	.793
.127	.855	-0.157	.107	-2.232	.873	.850	-0.1625	- 366	-5202	-378	-376	-991	.843
.139	1.000	0	.125	-2.075	.861	.830	-0.1863	0	-4836	-428	-369	-1041	.899
Temperature 1000°C													
.015	.075	-2.590	.013	-4.321	.988	.985	-0.0151	-6550	-10928	- 38	-136	-201	.867
.027	.115	-2.163	.020	-3.894	.973	.977	-0.0233	-5470	-9849	- 59	-205	-323	.741
.053	.200	-1.609	.035	-3.340	.947	.955	-0.0460	-4069	-8447	-116	-326	-558	.660
.076	.307	-1.181	.054	-2.912	.924	.930	-0.0726	-2987	-7365	-184	-397	-730	.710
.099	.430	-0.844	.076	-2.575	.801	.897	-0.1087	-2134	-6512	-275	-459	-892	.768
.109	.500	-0.693	.089	-2.424	.891	.882	-0.1256	-1753	-6131	-318	-474	-952	.817
.116	.540	-0.616	.096	-2.347	.884	.870	-0.1393	-1558	-5936	-352	-492	-1000	.827
.127	.620	-0.478	.110	-2.209	.873	.850	-0.1625	-1209	-5587	-411	-512	-1068	.866
.149	.795	-0.229	.141	-1.960	.851	.820	-0.1985	- 579	-4957	-471	-530	-1139	.946
.170	1.000	0	.177	-1.731	.830	.770	-0.1863	0	-4378	-471	-550	-1200	1.041

Note:  $a^*$  refers to the solid st. state for NiO.  
 $a^{**}$  refers to the liquid st. state for NiO.  
 $\Delta F$  and  $\Delta H$  data are listed in terms of cal/mole.  
 $\Delta S$  data is given in cal/mole °K.



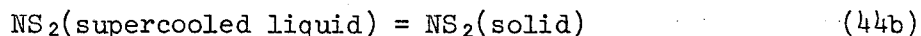
Appendix C: Tabulation of thermodynamic data for the NiO-NS<sub>2</sub> system (continued)

$N_{NiO}$	$a_{NiO}$	$\ln a_{NiO}^*$	$a_{NiO}^{**}$	$\ln a_{NiO}^{**}$	$N_{NS_2}$	$a_{NS_2}$	$\ln a_{NS_2}$	$\overline{\Delta F}_{NiO}^*$	$\overline{\Delta F}_{NiO}^{**}$	$\overline{\Delta F}_{NS_2}$	$\Delta F_{mix}^*$	$\Delta F_{mix}^{**}$	$\gamma_{NiO}^{**}$
Temperature 1100°C													
.015	.050	-2.996	.012	-4.438	.985	.985	-0.0151	-8173	-12107	-41	-163	-222	.800
.027	.080	-2.526	.019	-3.968	.973	.977	-0.0233	-6891	-10825	-64	-248	-355	.704
.053	.140	-1.966	.033	-3.408	.947	.955	-0.0460	-5363	-9297	-125	-403	-611	.623
.076	.215	-1.537	.051	-2.979	.924	.930	-0.0726	-4193	-8127	-198	-502	-801	.671
.099	.320	-1.139	.076	-2.581	.901	.897	-0.1087	-3107	-7041	-297	-575	-965	.768
.109	.375	-0.981	.089	-2.423	.891	.882	-0.1256	-2676	-6610	-343	-597	-1026	.817
.116	.415	-0.879	.098	-2.321	.884	.870	-0.1393	-2398	-6332	-380	-614	-1070	.845
.127	.480	-0.734	.113	-2.176	.873	.850	-0.1625	-2002	-5936	-443	-641	-1141	.890
.149	.620	-0.478	.146	-1.920	.851	.830	-0.1863	-1304	-5238	-508	-680	-1213	.980
.200	1.000	0	.236	-1.442	.800			0	3934		-700	-1320	1.180

$N_{NiO}$	$N_{NS_2}$	$\overline{\Delta S}_{NiO}^*$	$\overline{\Delta S}_{NiO}^{**}$	$\Delta S_{NS_2}$	$\overline{\Delta H}_{NiO}^*$	$\overline{\Delta H}_{NiO}^{**}$	$\Delta H_{NS_2}$	$\overline{\Delta S}_{mix}^*$	$\overline{\Delta S}_{mix}^{**}$	$\Delta H_{mix}^*$	$\Delta H_{mix}^{**}$
.015	.985	15.2	10.7	.03	12678	2517	-9	.25	.19	181	29
.027	.973	13.3	8.8	.05	11218	1057	16	.41	.29	319	44
.053	.947	10.8	6.3	.17	9697	-464	113	.73	.49	621	82
.076	.924	9.7	5.2	.23	9319	-842	163	.95	.61	859	87
.099	.901	9.0	4.5	.22	9305	-856	105	1.17	.64	1016	10
.109	.891	8.8	4.3	.25	9430	-731	108	1.24	.69	1124	17
.116	.884	8.5	4.0	.29	9282	-879	82	1.24	.72	1149	-30
.127	.873	8.2	3.7	.32	9290	-871	48	1.32	.75	1222	-69

Appendix D: Comparison of values obtained for the activity of pure solid  $\text{NS}_2$  relative to the supercooled liquid standard state when (1) the free energy of fusion is known for all temperatures below the normal melting point and (2) when the heat of fusion is assumed invariant with temperature.

Kelley<sup>10</sup> has given heat capacity data for both the crystalline solid sodium disilicate and the supercooled liquid. By integration of the expression for the heat capacity change for the reaction



according to Eq. (33), and taking the heat of fusion of  $\text{NS}_2$  as 8500 cal/mole at 1147°K, one obtains the following expression for the free energy of reaction (44b)

$$\Delta F = 11.47T \ln T - 8.23 \times 10^{-3} T^2 - 4.515 \times 10^5 T^{-1} - 81.234T + 11696$$

From the expression

$$\Delta F = RT \ln \frac{a_{\text{NS}_2(\text{solid})}}{a_{\text{NS}_2(\text{liquid})} \equiv 1} \quad (33)$$

the activity of the solid  $\text{NS}_2$  may be readily calculated.

In the event that free energy data are not available for the solid and supercooled liquid states, Eq. (34) may be used to estimate the activity of the solid referred to the pure supercooled liquid standard state. Following is a table listing the activity values calculated

for solid  $\text{NS}_2$  by the methods of Eq. (33) and Eq. (34).

---

Temperature (°C)	Calculated $a_{\text{NS}_2}$ (solid) - Eq.(33)	Estimated $a_{\text{NS}_2}$ (solid) - Eq.(34)
800	0.245	0.200
900	0.398	0.358
1000	0.597	0.578
1100	0.854	0.853

---

Appendix E: Calculation of the maximum activity of "FeO" stable in a 10:1 CO/CO<sub>2</sub> atmosphere at 1000°C

Consider the reaction:



At 1000°C (from the tables of Elliott and Gleiser)

$$\Delta F_{\text{CO}}^{\circ} = -53676 \text{ cal/mole}$$

$$\Delta F_{\text{CO}_2}^{\circ} = -94687 \text{ cal/mole}$$

$$\Delta F_{\text{"FeO"}}^{\circ} = -43156 \text{ cal/mole}$$

Therefore,  $\Delta F_{\text{reaction}}^{\circ} = -2145 \text{ cal/mole}$ . If

$$\Delta F = \Delta F^{\circ} + RT(2.303) \log \frac{P_{\text{CO}} \cdot a_{\text{"FeO"}}}{P_{\text{CO}_2}}$$

and at equilibrium  $\Delta F = 0$ , then we may write

$$0 = -2145 + 1.987(1273)(2.303) \log 10 \cdot a_{\text{"FeO"}}$$

Solving for  $a_{\text{"FeO"}}$ ,

$$\log a_{\text{"FeO"}} = 0.3682 - 1 = -0.6318$$

and

$$a_{\text{FeO}} = 0.233$$

An activity of "FeO" larger than 0.233 under these environmental conditions will result in the reaction (55) to proceed to the left as written above, and FeO will decompose in a glass, precipitating metallic Fe.

Appendix F: Estimation of free energies, enthalpies, and entropies of fusion of NiO, CoO, and Fe.<sub>95</sub>O at temperatures below their melting points; and estimation of the activity of the pure solid oxide relative to the supercooled liquid (K). (See Eq. (33) and (34).)

$$T_f = 1650^\circ\text{K} (1377^\circ\text{C})$$

$$\text{Fe}_{.95}\text{O} \text{ ----- } \Delta H_f \text{ (at } 1650^\circ\text{K)} = 7490 \text{ cal/mole}$$

$$\Delta S_f = 4.54 \text{ e.u.}$$

<u>T(°C)</u>	<u>T(°K)</u>	<u><math>\Delta F_f</math>(cal/mole)</u>	<u>K</u>
800	1073	-2622	.292
900	1173	-2165	.395
1000	1273	-1707	.509

$$T_f = 2078^\circ\text{K} (1805^\circ\text{C})$$

$$\text{CoO} \text{ ----- } \Delta H_f \cong 4.54(2078) = 9434 \text{ cal/mole}$$

<u>T(°C)</u>	<u>T(°K)</u>	<u><math>\Delta F_f</math>(cal/mole)</u>	<u>K</u>
800	1073	-4564	.118
900	1173	-4114	.171
1000	1273	-3652	.236
1100	1373	-3197	.310

$$T_f = 2238^\circ\text{K} (1965^\circ\text{C})$$

$$\text{NiO} \text{ ----- } \Delta H_f \cong 4.54(2238) = 10161 \text{ cal/mole}$$

<u>T(°C)</u>	<u>T(°K)</u>	<u><math>\Delta F_f</math>(cal/mole)</u>	<u>K</u>
800	1073	-5294	.087
900	1173	-4836	.125
1000	1273	-4378	.177
1100	1373	-3934	.236

Appendix G: Conversions of oxide weight percent values to mole fraction

Gram Formula Weights: NiO = 74.71  
CoO = 74.933  
"FeO" = Fe.950 = 69.055  
Na<sub>2</sub>Si<sub>2</sub>O<sub>5</sub> = 182.152

<u>Weight</u> <u>% NiO</u>	<u>N</u> <u>NiO</u>	<u>Weight</u> <u>% CoO</u>	<u>N</u> <u>CoO</u>	<u>Weight</u> <u>% "FeO"</u>	<u>N</u> <u>"FeO"</u>
0.62	.015	2.30	.054	4.95	.121
1.00	.024	5.00	.113	5.00	.122
1.14	.027	5.30	.120	5.24	.127
2.00	.047	8.40	.182	9.07	.208
2.23	.053	10.00	.213	10.00	.227
3.00	.070	10.59	.221	13.09	.284
3.20	.076	13.62	.277	15.00	.318
4.00	.092	15.00	.300	16.11	.336
4.30	.099	16.26	.321	19.36	.388
4.77	.109	19.23	.367	20.00	.397
5.00	.114	20.00	.378	23.18	.443
5.11	.116	22.03	.407	25.00	.468
5.66	.127	25.00	.447	26.74	.491
6.00	.135	25.52	.454	29.80	.528
6.70	.149	30.00	.510	30.00	.531
7.00	.155	35.00	.567	33.29	.568
8.00	.175			35.00	.587
9.00	.194			36.55	.603
10.00	.213			40.00	.637
				45.00	.683
				50.00	.725

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TECHNICAL INFORMATION DIVISION  
LAWRENCE RADIATION LABORATORY  
UNIVERSITY OF CALIFORNIA  
BERKELEY, CALIFORNIA 94720