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Comparing Fluidized Bed Spray-Coating and Spray-Drying Encapsulation of Non-Spore-Forming Gram-Negative Bacteria

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24 **Keywords**

25 spray-drying; fluidized bed spray-coating; microencapsulation; biocontrol; *Collimonas*

26 **1. Introduction**

27 Microencapsulation is a preservation technique wherein a sensitive cargo is protected within
28 carrier material(s), often polymers such as polysaccharides, that can also feature additional
29 functions, depending on the application¹. For example, in the biomedical industry, drugs are
30 encapsulated for targeted delivery and controlled release². In the food industry, compounds are
31 encapsulated to mask or retain certain flavors³ and for enteric release to maximize bioavailability
32 of bioactives. In the agricultural industry, pesticides are often encapsulated for greater stability
33 and controlled release in cropland to combat a variety of pests^{4,5}. It is of particular interest to
34 encapsulate active ingredients in biopesticides, such as plant-beneficial biocontrol bacteria, as
35 there is a growing need to replace traditional chemical pesticides that are harmful to humans and
36 the environment.

37 The two primary means of applying plant-beneficial bacteria for crop utilization are by
38 spraying in-furrow or in-field, and by coating onto seed. For spray applications, encapsulation of
39 beneficial bacteria can help protect against other ingredients in the spray tank which may damage
40 the bacteria, and against environmental effects in sprayed areas⁶. Microcapsule size is
41 constrained by the nozzle size of the sprayer, on the scale of microns, as to limit blockages,
42 settlement, and aggregation of particulates^{6,7}. For coating applications, the seed coating itself
43 serves as the protective encapsulation matrix for the bacteria. Rotary drum dryers are the most
44 widely used method of coating seed; however, bacterial viability is typically diminished by other
45 ingredients in the seed coating formulation (similar to spray tanks) and by the long drying
46 process^{8,9}.

47 Encapsulation of plant-beneficial bacteria has been demonstrated using alginate. Alginate is a
48 naturally derived polymer desirable as a microcapsule carrier material because it is a relatively

49 low cost ingredient, is safe to handle, and has the ability to form a gel network^{10,11}. Composed of
50 alternating or repeating units of β -D-mannuronic acid and α -L-guluronic acid, the polyuronate
51 backbone of alginate contains carboxylate groups allowing ion-mediated cross-linking to form a
52 gel structure^{12,13}. Alginate beads containing bacteria are typically formed by dripping a
53 suspension of dissolved alginate and bacterial cells into a calcium chloride bath, where cross-
54 linking occurs upon contact at the interface¹⁴⁻¹⁶. This gelling step is followed by a curing step, a
55 washing step, and a drying step, before dry alginate beads are formed. The need for a separate
56 extruder and calcium bath as well as many individual steps make producing alginate beads
57 challenging to scale up¹⁷.

58 Recently, methods for forming in situ cross-linked alginate microcapsules (CLAMs) by
59 spray-drying¹⁸, and in situ cross-linked alginate matrix shell (CLAMshell) particles by fluidized
60 bed spray-coating¹⁹ were developed at UC Davis. Encapsulation of bacteria^{20,21}, enzymes²²,
61 polymers²³, and oils^{24,25} in CLAMs have been demonstrated, as has encapsulation of enzymes in
62 CLAMshell particles²⁶. To produce these microcapsules, atomization at the nozzle evaporates a
63 volatile base, lowering the pH of the droplet to solubilize the calcium salt, facilitating calcium-
64 mediated cross-linking of alginate as the droplets dry into a particle (CLAM) or form a coating
65 (CLAMshell). This single-step encapsulation process can be industrially scalable while still
66 remaining relatively cheap²⁷. In addition, both spray-drying and fluidized bed spray-coating are
67 already widespread in industry, making the in situ cross-linking processes easier to implement.

68 In this study, we compared spray-drying and fluidized bed spray-coating to investigate
69 encapsulation of the potential biocontrol bacterium *Collimonas arenae* Cal35 in CLAMs and
70 CLAMshell particles. Cal35 is a non-spore-forming, Gram-negative soil isolate with
71 demonstrated success as an antifungal agent in laboratory, greenhouse, and field settings²⁸⁻³².

72 Cal35 has also been shown to retain its antifungal properties after spray-drying and shelf
73 storage²¹. Here, the survival of Cal35 in CLAMs and CLAMshells was assessed and compared,
74 and correlated with the sensitivity of Cal35 to heat and desiccation stresses. Furthermore, spray-
75 dried particles and fluidized bed spray-coated particles containing Cal35 were characterized by
76 SEM, moisture content analysis, and water activity analysis.

77 **2. Materials and Methods**

78 **2.1 Materials**

79 Ammonium hydroxide, 28-30% (NH₄OH), dicalcium phosphate (Ca₂HPO₄), glycerol,
80 magnesium sulfate heptahydrate (MgSO₄·7H₂O), peptone, potassium phosphate dibasic (K₂PO₄),
81 and succinic acid were purchased from Fisher (Waltham, MA). Low-viscosity alginate (A1112)
82 and maltodextrin (dextrose equivalent 4.0-7.0) were acquired from Millipore-Sigma (Burlington,
83 MA). Agar was purchased from BTS (Houston, TX). Concentrated (20x) phosphate-buffered
84 saline (PBS) was purchased from VWR (Radnor, PA). HI-CAP 100 modified starch was
85 purchased from Ingredion (Westchester, IL) and impact beads (glass cores) from Grainger (Lake
86 Forest, IL). Milli-Q water from a Millipore Ultrapure Water Purification System was used to
87 prepare all solutions. *C. arenae* Cal35 was originally isolated from forest soil in the Jug Handle
88 State Natural Reserve in Mendocino County, CA³³.

89 **2.2 Methods**

90 **2.2.1 Culture conditions for *Collimonas arenae* Cal35**

91 Fresh cultures of *C. arenae* Cal35 were prepared and grown in King's medium B (KB) using
92 the exact conditions described previously²¹.

93 **2.2.2 Testing sensitivity of Cal35 to temperature and desiccation**

94 Cultures of Cal35 were harvested and collected by centrifugation at 5,000 rpm. Supernatant
95 was removed and the remaining cell pellet was resuspended in 0.01 M phosphate buffered saline
96 (1X PBS). Initial and final viable cell counts were measured using the serial dilution method by
97 plating each dilution onto KB agar and counting colony forming units (CFUs).

98 To assess sensitivity towards temperature, Cal35 suspended in 1X PBS at a density of about
99 $9.5 \log[\text{CFU/mL}]$ was transferred to 15 mL conical tubes. The conical tubes ($n = 3$) were then
100 placed into a heated water bath set to temperatures between 35 and 60°C and sampled
101 periodically over three hours to determine viable cell counts.

102 To assess sensitivity towards desiccation, 3 mL of fresh Cal35 culture resuspended in 1X
103 PBS at a density of about $9.5 \log[\text{CFU/mL}]$ were transferred to the bottom of an empty plastic
104 Petri dishes which were placed open in a biological safety cabinet at room temperature ($\sim 21^\circ\text{C}$),
105 and dried for 24 hr using the airflow of the unit. Dishes containing the dehydrated Cal35
106 suspension were rehydrated with 3 mL of 1X PBS and plated to count CFUs.

107 **2.2.3 Spray-drying formulation of Cal35 encapsulated in CLAMs**

108 To prepare 50 g of feed for spray-drying, a 1.5 L KB culture of Cal35 was harvested after 24
109 h of growth and centrifuged at 4,200 rpm for 15 min to pellet the cells. The supernatant was
110 removed and the cell pellet was resuspended in 12.5 g of 4% filter-sterilized succinic acid, which
111 was previously adjusted with NH_4OH to pH 7. This cell suspension was added to an autoclaved
112 preparation containing modified starch, maltodextrin, sodium alginate, and CaHPO_4 . The final
113 concentration of the feed for spray-drying was: 13% HI-CAP 100 modified starch, 2%
114 maltodextrin, 2% sodium alginate, 1% succinic acid at pH 7, and 0.5% CaHPO_4 .

115 Spray-drying was performed using a BUCHI B-290 benchtop spray-dryer (BUCHI
116 Corporation, New Castle, DE) (**Figure 1**). The control parameters used were: 90°C inlet
117 temperature, 40% spray rate (~12 g/min), 40 mm nozzle pressure (0.5 bar), 100% aspirator. The
118 average outlet temperature was $42 \pm 1^\circ\text{C}$. After the 50 g of feed was sprayed, particles were
119 removed and collected from the product chamber.

120 **2.2.4 Fluidized bed spray-coating formulation of Cal35 encapsulated in CLAMshells**

121 To prepare 200 g of feed for spray-coating, 6 L of culture was harvested and prepared in the
122 same manner as spray-drying, described in the previous section. The final concentration of the
123 feed for spray-coating was the same as the feed for spray-drying: 13% HI-CAP 100 modified
124 starch, 2% maltodextrin, 2% sodium alginate, 1% succinic acid at pH 7, and 0.5% CaHPO_4 .

125 Spray-coating was performed using a UniGlatt 2 L capacity fluidized bed coater in Wurster
126 configuration (Glatt Air Techniques, Inc., Ramsey, NJ) (**Figure 2**). For the core material, 600 g
127 of 250-300 μm glass beads were inserted into the product chamber of the unit. The control
128 parameters used were: 55-60°C inlet temperature (lower and upper limit), 32% spray rate (~10
129 g/min), 3.5 bar nozzle pressure, 25 deg airflow flap angle. The average outlet temperature was 40
130 $\pm 0.6^\circ\text{C}$. In-process samples were taken using the sample port to measure viability during the
131 coating process. Once all 200 g of the feed was applied, fluidization continued for two minutes to
132 allow more drying of the coatings before collection.

133 **2.2.5 Characterization of spray-dried and spray-coated Cal35**

134 Viability of Cal35 before encapsulation was measured by sampling from each feed
135 suspension and using the dilution method to plate onto KB agar and count CFUs. Viability of
136 Cal35 after encapsulation was measured by dissolving 0.03 ± 0.001 g of spray-dried particles and

137 2.0 ± 0.1 g spray-coated particles in 12.5 mL 1X PBS. Samples were mixed by inversion at room
138 temperature for one hour to fully dissolve particles and release all bacteria before being plated
139 onto KB agar to count CFUs.

140 Product yield was calculated by taking the percent of the collected solids to sprayed solids,
141 either as the total spray-dried solids or total coated solids.

142 Particle morphology was visualized by scanning electron microscopy (SEM) using a Thermo
143 Scientific Quattro SEM (Thermo Fisher Scientific, Waltham, MA). Samples of spray-dried and
144 spray-coated particles were mounted onto carbon tape and sputter-coated in gold to a thickness
145 of 120 angstrom. A beam voltage of 10 kV and a spot size of 3.0 were used for imaging.

146 Moisture content was measured gravimetrically by oven drying for three days at 60-70°C.
147 Water activity was measured using an Aqualab Series 3TE water activity meter (METER,
148 Pullman, WA).

149 **2.2.6 Statistical analysis**

150 Data was analyzed using the statistical software JMP (Statistical Discovery from SAS, Cary,
151 NC). One way ANOVA and post hoc multiple comparison tests were used to determine
152 significance of factors and differences between means. P-values less than 0.05 indicated a
153 significant difference.

154 **3. Results and Discussion**

155 Spray-drying and fluidized bed spray-coating are two common industrial high throughput
156 drying processes that can be used for microencapsulation. Spray-drying (**Figure 1**) relies on
157 significantly hotter air currents to quickly dry atomized droplets into particles, whereas spray-

158 coating (**Figure 2**) exploits long drying times of continuously fluidizing particles being coated to
159 require cooler drying temperatures (**Table 1**).

160 **Table 1** Process parameters for spray-drying and fluidized bed spray-coating in this study.

Parameter	Spray-drying	Spray-coating
Inlet Temperature	90°C	55-60°C
Outlet Temperature	42±1°C	40±0.6°C
Residence Time	<1-1.5 sec	20-25 min

161

162 **3.1 Bacterial isolate Cal35 showed greater survival with spray-drying than with fluidized** 163 **bed spray-coating**

164 To produce a collectable product, a blend of maltodextrin and modified starch was used as
165 excipients in the CLAMs and CLAMshell formulations. Previously, these excipients enhanced
166 the survival of Cal35 during spray-drying and shelf-storage in CLAMs²¹.

167 Prior to encapsulation, the viable cell counts of Cal35 in both feed suspensions were above
168 10 log[CFU/g solids] (**Figure 3A**). Cal35 experienced approximately 3 log reduction during
169 spray-drying compared to a 4 log reduction during fluidized bed spray-coating (**Figure 3B**).
170 Even though outlet temperatures for both processes were around 40°C, the inlet temperature of
171 spray-drying was considerably higher than that of fluidized bed spray-coating (90 versus 55-
172 60°C). Another key difference between these encapsulation processes was residence time (**Table**
173 **1**). For the Buchi B-290 benchtop spray-dryer, the residence time can span in the milliseconds to
174 seconds range, as droplets quickly pass through the evaporation chamber and fall into the
175 collection chamber (**Figure 1**). The resulting CLAMs contained more viable bacteria (7
176 log[CFU/g solids]) than CLAMshells that were produced by spray-coating (6 log[CFU/g coated
177 solids]). In the UniGlatt fluidized bed spray-coater, the residence time ranges from minutes to
178 hours, depending on the amount of coating being applied to the fluidized particles (**Figure 2**). In
179 the present study, the residence time for spray-coating was about 22 minutes; 20 minutes for the

180 coating suspension to be applied and two minutes of extra drying time (
181 **Figure 4**). During the coating process, the viability of Cal35 consistently measured about 7.5
182 log[CFU/g coated solids]. However, the end product of spray-coating was lower in viability
183 compared to spray-drying per gram of sprayed solids due to the final drying step. Although the
184 viability of Cal35 was sustained in-process for the short coating duration, it is possible that
185 thicker coatings may be applied to increase the total CFU in the coating. And although the total
186 CFU count in spray-dried CLAMs can be increased by simply spraying a greater volume of feed,
187 the particle size of CLAMs would not change. Perhaps a thicker CLAMshell coating thus larger
188 particle size would confer greater protection and stability to the encapsulated bacteria over time.

189 Here, spray-drying encapsulation, which operates with high temperatures and a short
190 residence time was less damaging to Cal35, yet there is still room to minimize the 3 log
191 reduction in the viable cell count (**Figure 3B**). Cellular accumulation of osmoprotectants, mainly
192 in the form of disaccharides, has been attributed to enhancing desiccation stress resistance³⁴. For
193 example, when grown in media supplemented with trehalose, survival of *Raoultella terrigena*
194 dried in alginate beads was improved¹⁶. Similarly, cellular accumulation of sucrose by
195 *Pseudomonas chlororaphis* enhanced survival during freeze-drying³⁵. Osmoprotectants are
196 beneficial because they help maintain osmotic balance, prevent unfolding of proteins, and
197 preserve membrane fluidity of the cell³⁶. This strategy of introducing osmoprotectants is
198 especially useful because it occurs during the culturing phase of bacteria, prior to formulation,
199 meaning it can be easily implemented.

200 **3.2 Temperature and desiccation sensitivity of Cal35**

201 Cal35 was very sensitive to a temperature of 60°C, with no viable cells countable after five
202 minutes of exposure (**Figure 5**). The number of viable bacteria declined more rapidly with

203 increasing temperature. The viability of Cal35 incubated at 35°C did not change over the three
204 hour period of the experiment. After one hour, Cal35 held at 40°C still showed no decrease in
205 viability; however, raising the temperature to 45°C reduced viability by more than 5 log units,
206 and up to 50°C resulted in colony counts above the limit of detection. In the three hour duration,
207 there was a 2.5 log reduction at 40°C and a 5.5 log reduction at 45°C. At 45 and 50°C, the
208 decline in log CFU begins to flatten, indicative of tolerance to higher temperatures³⁷.

209 Cal35 did not handle desiccation very well. With an initial cell count of ~9.5 log CFU/mL,
210 no viable bacteria were recovered after a culture aliquot was left to dry in a dish for 24 hours at
211 room temperature (21°C)

212 For bacteria that are tolerant of heat but sensitive to drying, it would seem to make sense that
213 a process like fluidized bed spray-coating where very low moisture environments exist for
214 extended periods of time be more detrimental to Cal35 than spray-drying. In fact, the moisture
215 content of spray-coated particles was 0.28%, over ten times less than for spray-dried particles
216 (**Figure 3D**), with no significant difference in the overall product yield (**Figure 3C**). Water
217 activity was also significantly lower in spray-coated particles (**Figure 3E**).

218 **3.3 Outlook and applications**

219 Whether bacterial biopesticides are applied on seed or in-field will largely impact the method
220 of encapsulation. Spray-drying of CLAMs produced particles with a diameter between 5 and 20
221 µm (**Figure 6A**). Particles in this size range can be readily incorporated into spray-tanks for
222 application in-furrow or on foliage. Fluidized bed spray-coating of CLAMshells onto cores
223 produced coated particles between 250-300 µm (**Figure 6B**). Despite resulting in slightly greater
224 losses in viability of Cal35 compared to spray-drying (**Figure 6B**), fluidized bed spray-coating
225 could be an enticing method for coating beneficial bacteria directly onto seeds. Seed coatings are

226 conventionally applied by rotary pan or drum drying, where nutrients, pesticides, and other
227 active compounds that benefit the seed and root are sprayed onto seeds as they are mixing or
228 tumbling in the drum³⁸. Because drying is completed at ambient conditions, the process is long,
229 resulting in bacteria losing viability due to desiccation⁸. However, in addition to the use of
230 osmoprotectants, formulation with polymers such as gum acacia, methylcellulose, polyvinyl
231 alcohol, and polyvinyl pyrrolidone have improved survival of rhizobial legume inoculants in the
232 seed coating process^{9,39}. With bacteria such as Cal35 that are less tolerant to drying, introducing
233 some heat to speed up the coating process, similar to what is happening during fluidized bed
234 spray-coating, may potentially be a more favorable encapsulation method.

235 Continuous fluidized bed spray-coating may also offer a unique solution to address issues of
236 long drying times. While the Wurster configuration of spray-coating used in this study is a batch
237 process, moving towards a continuous process where seeds are fluidized, directly coated, and
238 collected can greatly lower the residence time while maintaining tolerable drying temperatures.
239 Issues of agglomeration and proper coating formation when spraying with polymers can be
240 addressed with optimization experiments of process and formulation parameters^{26,40,41}, however,
241 when coating onto seed specifically, it is important to understand the limits of the drying
242 temperature so as to not negatively impact seed germination efficiency. Seeing that desiccation
243 stress was the more detrimental to Cal35, perhaps the ideal conditions for encapsulating similar
244 bacterial inoculants calls for shorter residence times by elevating drying temperatures, similar to
245 the drying conditions seen in spray-drying where survival of Cal35 was greatest.

246 Ultimately the survival of bacteria during any encapsulation method may mostly be
247 influenced by their structure and mechanisms to tolerate various environmental stresses. Gram-
248 positive probiotic bacteria such as *Bifidobacteria* and *Lactobacillus* lose little viability during

249 spray-drying and can have survival rates greater than 90% due to their more protective
250 membrane structure⁴². Spore-formers such as *Bacillus* are easily encapsulated and are already
251 used in agriculture as biopesticides because of the robust nature of spores⁴³. The ability of a non-
252 spore-forming Gram-negative *Methylobacterium* strain to remain viable during spray-drying may
253 be a consequence of being acclimated to the extreme conditions that characterize the natural
254 habitat of this bacterium, namely the plant leaf surface²⁰. Future work in encapsulation of plant
255 beneficial bacteria and biopesticides will be to consider how these underlying cellular
256 mechanisms to tolerate or adapt to stresses can help design microcapsules for improving the
257 protected bacteria's long-term stability for crop applications.

258 **4. Conclusions**

259 Encapsulation of the non-spore-forming plant-beneficial bacterial strain *Collimonas arenae*
260 Cal35 in CLAMs by spray-drying or in CLAMshells by fluidized bed spray-coating was
261 investigated. Spray-drying encapsulation of Cal35 had greater survival compared to fluidized bed
262 spray-coating, which is consistent with the observation that Cal35 was much more tolerant to
263 heat than to desiccation. However, if the coating process would continue for longer periods of
264 time to create thicker coated CLAMshells, it is possible that the total CFUs per sprayed solids
265 would be comparable or better than spray-drying. During spray-drying, high inlet temperatures
266 allow a very short residence time of bacteria being encapsulated, while during fluidized bed
267 spray-coating, low inlet temperatures rely on a long residence time of continuously fluidizing
268 particles. CLAMs produced by spray-drying were smaller, ranging between 5-20 μm , while
269 CLAMshell particles ranged between 250-300 μm . Both methods of encapsulation are relevant

270 for encapsulation of bacterial biopesticides; CLAMs were sized appropriately for spray
271 applications, while CLAMshells may be more useful for coating onto seed.

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277 **6. Author Disclosure Statement**

278 Author Tina Jeoh is an inventor of the CLAMs process (United States Patent 9,700,519).

279 Authors Tina Jeoh and Ryan Kawakita are inventors of the CLAMshell process (United States
280 Patent Application 63085669).

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384

385 **Figure 1** Schematic of a Buchi B-290 benchtop spray-dryer. Outlet temperature is measured in
386 the bridge between the drying chamber and the cyclone, marked by the 'x'.

387

388 **Figure 2** Schematic of UniGlatt fluidized bed spray-coater in Wurster configuration. Outlet
389 temperature is measured between the filter and exhaust, marked by the 'x'.

390

391 **Figure 3** Feed and product characterization for each encapsulation method. (A) Viable cell count
392 of Cal35 in the feed as log [CFU/g solids]. (B) Viable cell count of Cal35 in the encapsulated
393 product as log [CFU/g solids] for spray-drying, and log [CFU/g coated solids] for spray-coating.
394 (C) Yield as a percentage of recoverable solids. (D) Wet basis moisture content of spray-dried
395 powder or spray-coated particles containing Cal35. (E) Water activity of spray-dried powder or
396 spray-coated particles containing Cal35. Asterisks denote statistically significant differences
397 between encapsulation methods.

398

399 **Figure 4** Viability of Cal35 during the fluidized bed spray-coating process. Viability of the
400 coating suspension before spraying is represented at 0% Batch Progress. Once the coating
401 suspension was fully sprayed (20 min), the coated particles continued to fluidize for two extra
402 minutes to complete drying, represented at 100% Batch Progress.

403

404 **Figure 5** Viability of Cal35 heated between 35 to 60°C for three hours. The limit of detection is
405 indicated by the horizontal red line. Data points on the limit of detection marked with an 'x'
406 indicate no viable bacteria were recovered at this timepoint. Lines are drawn to guide the eye.

407

408 **Figure 6** SEM images of, (A) CLAMs with 30 μm scale bar, and (B) CLAMshell particles with

409 500 μm scale bar.

410